

JAPAN INTERNATIONAL COOPERATION AGENCY (JICA)

**NATIONAL WATER SUPPLY AND DRAINAGE BOARD
MINISTRY OF HOUSING AND PLANTATION INFRASTRUCTURE
DEMOCRATIC SOCIALIST REPUBLIC OF SRI LANKA**

**THE DETAILED DESIGN STUDY
ON
GREATER KANDY WATER SUPPLY
AUGMENTATION PROJECT
IN
THE DEMOCRATIC SOCIALIST REPUBLIC
OF
SRI LANKA**

FINAL REPORT

VOLUME III

DATA AND ATTACHMENTS

MAY 2002

**NJS CONSULTANTS CO., LTD.
NIHON SUIDO CONSULTANTS CO., LTD.**

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Abbreviations and Acronyms

1. Unit

cm	centimeter
ft.	foot
g	gram
gpcd	gram per capita per day
ha	hectare (1 ha = 10,000m ²)
hr	hour
kg	kilogram
km	kilometer
km ² , or sq.km	square kilometer
kV	kilovolt
kW	kilowatt
kWh	kilowatt hour
l, or L	liter
l/day, or l/d	liter per day
l/sec, or l/s	liter per second
lpcd, or Lpcd	liter per capita per day
m	meter
m/s, or m/sec	meters per second
m ² , or sq.m	square meter
m ³ , or cu.m	cubic meter
m ³ /d, or cu.m/day	cubic meter per day
m ³ /min	cubic meter per minute
m ³ /s, or cu.m/sec	cubic meter per second
MCM	million cubic meter
mgd	million gallons per day
mg/l	milligram per liter
mm	millimeter
Mpa	megapascal
ppm	parts per million
Rs.	Sri Lankan Rupee
V	volt

2. Water Quality

BOD ₅	Biochemical Oxygen Demand (20°C, 5 days)
COD	Chemical Oxygen Demand
DO	Dissolved Oxygen
EC	Electrical Conductivity
pH	Hydrogen ion potential
SS	Suspended Solids
TS	Total Solids

3. Organizations

ADB	Asian Development Bank
CEA	Central Environmental Authority
CEB	Ceylon Electricity Board
CPC	Central Provincial Council
FINNIDA	Finnish International Development Agency
GS	Gramasevaka Divison (local administrative unit)
IBRD	International Bank for Reconstruction and Development (World Bank)

ICC	Interagency Co-ordinating Committee
IDA	International Development Association (soft loan facility of IBRD)
IMF	International Monetary Fund
JBIC	Japan Bank for International Cooperation (Japan)
JICA	Japan International Cooperation Agency (Japan)
KMC	Kandy Municipal Council
MASL	Mahaweli Authority of Sri Lanka
MHUD	Ministry of Housing and Urban Development
MOF	Ministry of Finance
MSL	Mean Sea Level
NJS	Nippon Jogesuido Sekkei Co., Ltd.
NSC	Nihon Suido Consultants Co., Ltd.
NWSDB, or NWS&DB	National Water Supply and Drainage Board
OECD	Organization for Economic Cooperation and Development
PS	Pradeshia Sabha (local administrative unit)
RDA	Road Development Authority
RSC	Regional Support Center, NWSDB
UC	Urban Council
UDA	Urban Development Authority

4. Others

BOT	Build - Operate - Transfer
BWL	Bottom Water Level
CED	Central Environmental Division
CPI	Consumer Price Index
EAC	Environmental auditing Commission
EIA	Environmental Impact Assessment
EIRR	Economic Internal Rate of Return
FIRR	Financial Internal Rate of Return
FY	Fiscal Year
GDP	Gross Domestic Product
GL	Ground Level
GNP	Gross National Product
GST	Government Sales Tax
HWL	High Water Level
HH	Household
IEE	Initial Environmental Examination
LWL	Low Water Level
L/S	Lift Station
NGO	Non-Governmental Organization
NRW	Non-revenue Water
ODA	Official Development Assistance
PEU	Project Environmental Unit
P/S	Pumping Station
SLS	Sri Lankan Standards
STP	Sewage Treatment Plant
T.A	Technical Assistance
TWL	Top Water Level
UFW	Unaccounted-For-Water
VAT	Value Added Tax
WID	Women in Development
WTP	Water Treatment Plant
WWTP	Wastewater Treatment Plant (=STP)

01 Intake and Water Treatment Plant Process Calculations

1-1

Grit Chamber

Dimension : Width (m) Length (m) (Sand sedimentation Depth h=0.5m at Inlet Mouth)
 6.00 33.50

	Water Flow	Duty (units)	River Water Level (m)	Diameter of Sand (mm)	Sand Settling Velocity (cm/sec)	Sedi. Sand Depth in G.C.	Grit Chamber H.W.L. (m)	Grit Chamber L.W.L. (m)	Effective Depth (m)	Effective Volume	Required Length (m)	Retention Time (min)	Velocity (cm/sec)	Surface Load Ratio (mm/min)	Remark
Case 1	115,500	2	437.60	0.15	1.5	0.00	437.11	434.06	3.05	1226	7.4	15.29	3.7	200	
Case 2	115,500	2	437.60	0.15	1.5	1.00	437.09	435.06	2.03	816	7.4	10.17	5.5	200	
Case 3	115,500	2	437.60	0.15	1.5	1.94	437.01	436.00	1.01	406	7.4	5.06	11.0	200	
Case 4	115,500	2	438.30	0.15	1.5	1.94	437.80	436.00	1.80	724	7.4	9.02	6.2	200	
Case 5	115,500	2	440.74	0.15	1.5	1.94	440.29	436.00	4.29	1725	7.4	21.50	2.6	200	
Case 6	115,500	2	437.60	0.10	0.8	0.00	437.11	434.06	3.05	1226	13.9	15.29	3.7	200	
Case 7	115,500	2	437.60	0.10	0.8	1.00	437.09	435.06	2.03	816	13.9	10.17	5.5	200	
Case 8	115,500	2	437.60	0.10	0.8	1.94	437.01	436.00	1.01	406	13.9	5.06	11.0	200	
Case 9	115,500	2	438.30	0.10	0.8	1.94	437.80	436.00	1.80	724	13.9	9.02	6.2	200	
Case 10	115,500	2	440.74	0.10	0.8	1.94	440.29	436.00	4.29	1725	13.9	21.50	2.6	200	
Case 11	115,500	1	437.60	0.15	1.5	0.00	436.87	434.06	2.81	565	29.7	7.04	7.9	399	
Case 12	115,500	1	437.60	0.15	1.5	1.00	436.78	435.06	1.72	346	29.7	4.31	13.0	399	
Case 13	115,500	1	437.60	0.15	1.5	1.94	436.47	436.00	0.47	94	29.7	1.18	47.4	399	
Case 14	115,500	1	438.30	0.15	1.5	1.94	437.54	436.00	1.54	310	29.7	3.86	14.5	399	
Case 15	115,500	1	440.74	0.15	1.5	1.94	440.18	436.00	4.18	840	29.7	10.47	5.3	399	
Case 16	115,500	1	437.60	0.10	0.8	0.00	436.87	434.06	2.81	565	55.7	7.04	7.9	399	
Case 17	115,500	1	437.60	0.10	0.8	1.00	436.78	435.06	1.72	346	55.7	4.31	13.0	399	
Case 18	115,500	1	437.60	0.10	0.8	1.94	436.47	436.00	0.47	94	55.7	1.18	47.4	399	
Case 19	115,500	1	438.30	0.10	0.8	1.94	437.54	436.00	1.54	310	55.7	3.86	14.5	399	
Case 20	115,500	1	440.74	0.10	0.8	1.94	437.54	436.00	1.54	310	55.7	3.86	14.5	399	

Case I Capacity Calculation of Grit Chamber (River Water Level + 437.60m) 2 unit duty

(Grit Chamber High Water Level + 437.11 m)
 (Grit Chamber Low Water Level + 434.06 m) no soil

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 7.4 m
 L: Required Length(m)
 K: Safety Factor(-) 2
 H: Effective Depth 3.05 m
 V: Average Velocity 3.7 cm/sec
 U: Sand Settling Velocity (Dia.0.15mm) 1.5 cm/sec
 B: Number of Basins 2
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 3.1× Basin 2

Effective Volume per Basin(m3) 613
 Basin 2 unit duty
 Effective Volume Total(m3) 1226
 Retention Time 15.29 min
 Average Velocity 3.65 cm/sec
 Surface Load Ratio 200 mm/min
 Length/Width 5.6

Case 2 Capacity Calculation of Grit Chamber (River Water Level + 437.60m)

2 unit duty

(Grit Chamber High Water Level + 437.09 m)

(Grit Chamber Low Water Level + 435.06 m)

soil h=1.00m

Flow Rate 110000* 1.05= 115500 cum/day

Average Velocity 2-7 cm/sec

Surface Load Ratio 200-500mm/min

Width/Length 3-8

Effective Depth 3-4m

Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 7.4 m

L: Required Length(m)

K: Safety Factor(-) 2

H: Effective Depth 2.03 m

V: Average Velocity 5.5 cm/sec

U: Sand Settling Velocity (Dia.0.15mm) 1.5 cm/sec

B: Number of Basins 2

W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level

Max. Flood	1447 ft	441.00 m
Max. Operation	1446 ft	440.74 m
Min. Operation	1438 ft	438.30 m
Spillway Crest	1425 ft	434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension

Width(m)	Length(m)	Effective Depth(m)	Basin
6.0x	33.5x	2.0x	2

Effective Volume per Basin(m3) 408

Basin 2 unit duty

Effective Volume Total(m3) 816

Retention Time 10.17 min

Average Velocity 5.49 cm/sec

Surface Load Ratio 200 mm/min

Length/Width 5.6

Case 3 Capacity Calculation of Grit Chamber (River Water Level + 437.60m)

2 unit duty

(Grit Chamber High Water Level + 437.01 m)
 (Grit Chamber Low Water Level + 436.00 m)

soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 7.4 m

L: Required Length(m)
 K: Safety Factor(-) 2
 H: Effective Depth 1.01 m
 V: Average Velocity 11.0 cm/sec
 U: Sand Settling Velocity (Dia.0.15mm) 1.5 cm/sec
 B: Number of Basins 2
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 1.0× Basin 2

Effective Volume per Basin(m3) 203
 Basin 2 unit duty
 Effective Volume Total(m3) 406

Retention Time 5.06 min
 Average Velocity 11.03 cm/sec
 Surface Load Ratio 200 mm/min
 Length/Width 5.6

Case 4 Capacity Calculation of Grit Chamber (River Water Level + 438.30m) 2 unit duty
 (Grit Chamber High Water Level + 437.80 m)
 (Grit Chamber Low Water Level + 436.00 m) soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 7.4 m
 L: Required Length(m)
 K: Safety Factor(-) 2
 H: Effective Depth 1.80 m
 V: Average Velocity 6.2 cm/sec
 U: Sand Settling Velocity (Dia.0.15mm) 1.5 cm/sec
 B: Number of Basins 2
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 1.8× Basin 2
 Effective Volume per Basin(m3) 362
 Basin 2 unit duty
 Effective Volume Total(m3) 724
 Retention Time 9.02 min
 Average Velocity 6.19 cm/sec
 Surface Load Ratio 200 mm/min
 Length/Width 5.6

Case 5 Capacity Calculation of Grit Chamber (River Water Level + 440.74m)

2 unit duty

(Grit Chamber High Water Level + 440.29 m)
 (Grit Chamber Low Water Level + 436.00 m)

soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min
 Required Length

$L=K*(H*V/U)/B=$ 7.4 m
 L: Required Length(m)
 K: Safety Factor(-) 2
 H: Effective Depth 4.3 m
 V: Average Velocity 2.6 cm/sec
 U: Sand Settling Velocity (Dia.0.15mm) 1.5 cm/sec
 B: Number of Basins 2
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 4.3× Basin 2

Effective Volume per Basin(m3) 862
 Basin 2 unit duty
 Effective Volume Total(m3) 1725
 Retention Time 21.50 min
 Average Velocity 2.60 cm/sec
 Surface Load Ratio 200 mm/min
 Length/Width 5.6

Case 6 Capacity Calculation of Grit Chamber (River Water Level + 437.60m)

2 unit duty

(Grit Chamber High Water Level + 437.11 m)
 (Grit Chamber Low Water Level + 434.06 m)

no soil

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 13.9 m

L: Required Length(m) 13.9
 K: Safety Factor(-) 2
 H: Effective Depth 3.05 m
 V: Average Velocity 3.65 cm/sec
 U: Sand Settling Velocity (Dia.0.10mm) 0.8 cm/sec
 B: Number of Basins 2
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 3.1× Basin 2

Effective Volume per Basin(m3) 613
 Basin 2 unit duty
 Effective Volume Total(m3) 1226
 Retention Time 15.29 min
 Average Velocity 3.65 cm/sec
 Surface Load Ratio 200 mm/min
 Length/Width 5.6

Case 7 Capacity Calculation of Grit Chamber (River Water Level + 437.60m)

2 unit duty

(Grit Chamber High Water Level + 437.09 m)

(Grit Chamber Low Water Level + 435.06 m)

soil h=1.00m

Flow Rate 110000* 1.05= 115500 cum/day

Average Velocity 2-7 cm/sec

Surface Load Ratio 200-500mm/min

Width/Length 3-8

Effective Depth 3-4m

Retention Time 10-20min

Reqired Length $L=K*(H*V/U)/B=$ 13.9 m

L: Required Length(m)

K: Safety Factor(-) 2

H: Effective Depth 2.03 m

V: Average Velocity 5.5 cm/sec

U: Sand Settling Velocity (Dia.0.10mm) 0.8 cm/sec

B: Number of Basins 2

W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level Max. Flood 1447 ft 441.00 m

Max. Operation 1446 ft 440.74 m

Min. Operation 1438 ft 438.30 m

Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension Width(m) Length(m) Effective Depth(m) Basin
 6.0× 33.5× 2.0× 2

Effective Volume per Basin(m3) 408

Basin 2 unit duty

Effective Volume Total(m3) 816

Retention Time 10.17 min

Average Velocity 5.49 cm/sec

Surface Load Ratio 200 mm/min

Length/Width 5.6

Case 8 Capacity Calculation of Grit Chamber (River Water Level + 437.60m)

2 unit duty

(Grit Chamber High Water Level + 437.01 m)

(Grit Chamber Low Water Level + 436.00 m)

soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day

Average Velocity 2-7 cm/sec

Surface Load Ratio 200-500mm/min

Width/Length 3-8

Effective Depth 3-4m

Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 13.9 m

L: Required Length(m)

K: Safety Factor(-) 2

H: Effective Depth 1.01 m

V: Average Velocity 11.0 cm/sec

U: Sand Settling Velocity (Dia.0.10mm) 0.8 cm/sec

B: Number of Basins 2

W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level Max. Flood 1447 ft 441.00 m

Max. Operation 1446 ft 440.74 m

Min. Operation 1438 ft 438.30 m

Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension Width(m) Length(m) Effective Depth(m) Basin
 6.0× 33.5× 1.0× 2

Effective Volume per Basin(m3) 203

Basin 2 unit duty

Effective Volume Total(m3) 406

Retention Time 5.06 min

Average Velocity 11.03 cm/sec

Surface Load Ratio 200 mm/min

Length/Width 5.6

Case 9 Capacity Calculation of Grit Chamber (River Water Level + 438.30m) 2 unit duty

(Grit Chamber High Water Level + 437.80 m)
 (Grit Chamber Low Water Level + 436.00 m) soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min
 Required Length $L=K*(H*V/U)/B=$ 13.9 m

L: Required Length(m) 13.9 m
 K: Safety Factor(-) 2
 H: Effective Depth 1.80 m
 V: Average Velocity 6.2 cm/sec
 U: Sand Settling Velocity (Dia.0.10mm) 0.8 cm/sec
 B: Number of Basins 2
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 1.8× Basin 2

Effective Volume per Basin(m3) 362
 Basin 2 unit duty
 Effective Volume Total(m3) 724
 Retention Time 9.02 min
 Average Velocity 6.19 cm/sec
 Surface Load Ratio 200 mm/min
 Length/Width 5.6

Case 10 Capacity Calculation of Grit Chamber (River Water Level + 440.74m)

2 unit duty

(Grit Chamber High Water Level + 440.29 m)

(Grit Chamber Low Water Level + 436.00 m)

soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day

Average Velocity 2-7 cm/sec

Surface Load Ratio 200-500mm/min

Width/Length 3-8

Effective Depth 3-4m

Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 13.9 m

L: Required Length(m)

K: Safety Factor(-) 2

H: Effective Depth 4.29 m

V: Average Velocity 2.6 cm/sec

U: Sand Settling Velocity (Dia.0.10mm) 0.8 cm/sec

B: Number of Basins 2

W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level	Max. Flood	1447 ft	441.00 m
	Max. Operation	1446 ft	440.74 m
	Min. Operation	1438 ft	438.30 m
	Spillway Crest	1425 ft	434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension	Width(m)	Length(m)	Effective Depth(m)	Basin
	6.0x	33.5x	4.3x	2

Effective Volume per Basin(m3) 862

Basin 2 unit duty

Effective Volume Total(m3) 1725

Retention Time 21.50 min

Average Velocity 2.60 cm/sec

Surface Load Ratio 200 mm/min

Length/Width 5.6

Case 11 Capacity Calculation of Grit Chamber (River Water Level + 437.60m) 1 unit duty

(Grit Chamber High Water Level + 436.87 m)
 (Grit Chamber Low Water Level + 434.06 m) no soil

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min
 Required Length $L=K*(H*V/U)/B=$

L: Required Length(m) 29.7 m
 K: Safety Factor(-) 2
 H: Effective Depth 2.81 m
 V: Average Velocity 7.9 cm/sec
 U: Sand Settling Velocity (Dia.0.15mm) 1.5 cm/sec
 B: Number of Basins 1
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 2.8× Basin 1

Effective Volume per Basin(m3) 565
 Basin 1 unit duty
 Effective Volume Total(m3) 565
 Retention Time 7.04 min
 Average Velocity 7.93 cm/sec
 Surface Load Ratio 399 mm/min
 Length/Width 5.6

Case 12 Capacity Calculation of Grit Chamber (River Water Level + 437.60m)
 (Grit Chamber High Water Level + 436.78 m)
 (Grit Chamber Low Water Level + 435.06 m)

1 unit duty
 soil h=1.00m

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min
 Required Length

$L=K*(H*V/U)/B=$ 29.7 m
 L: Required Length(m)
 K: Safety Factor(-) 2
 H: Effective Depth 1.72 m
 V: Average Velocity 13.0 cm/sec
 U: Sand Settling Velocity (Dia.0.15mm) 1.5 cm/sec
 B: Number of Basins 1
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 1.7× Basin 1

Effective Volume per Basin(m3) 346
 Basin 1 unit duty
 Effective Volume Total(m3) 346
 Retention Time 4.31 min
 Average Velocity 12.95 cm/sec
 Surface Load Ratio 399 mm/min
 Length/Width 5.6

Case 13 Capacity Calculation of Grit Chamber (River Water Level + 437.60m)

1 unit duty

(Grit Chamber High Water Level + 436.47 m)

(Grit Chamber Low Water Level + 436.00 m)

soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day

Average Velocity 2-7 cm/sec

Surface Load Ratio 200-500mm/min

Width/Length 3-8

Effective Depth 3-4m

Retention Time 10-20min

Reqired Length $L=K*(H*V/U)/B=$ 29.7 m

L: Required Length(m)

K: Safety Factor(-) 2

H: Effective Depth 0.47 m

V: Average Velocity 47.4 cm/sec

U: Sand Settling Velocity (Dia.0.15mm) 1.5 cm/sec

B: Number of Basins 1

W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level Max. Flood 1447 ft 441.00 m

Max. Operation 1446 ft 440.74 m

Min. Operation 1438 ft 438.30 m

Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension Width(m) Length(m) Effective Depth(m) Basin
 6.0× 33.5× 0.5× 1

Effective Volume per Basin(m3) 94

Basin 1 unit duty

Effective Volume Total(m3) 94

Retention Time 1.18 min

Average Velocity 47.40 cm/sec

Surface Load Ratio 399 mm/min

Length/Width 5.6

Case 14 Capacity Calculation of Grit Chamber (River Water Level + 438.30m) 1 unit duty

(Grit Chamber High Water Level + 437.54 m)
 (Grit Chamber Low Water Level + 436.00 m) soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min
 Required Length

$L=K*(H*V/U)/B=$ 29.7 m
 L: Required Length(m)
 K: Safety Factor(-) 2
 H: Effective Depth 1.54 m
 V: Average Velocity 14.5 cm/sec
 U: Sand Settling Velocity (Dia.0.15mm) 1.5 cm/sec
 B: Number of Basins 1
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 1.5× Basin 1

Effective Volume per Basin(m3) 310
 Basin 1 unit duty
 Effective Volume Total(m3) 310
 Retention Time 3.86 min
 Average Velocity 14.47 cm/sec
 Surface Load Ratio 399 mm/min
 Length/Width 5.6

Case 15 Capacity Calculation of Grit Chamber (River Water Level + 440.74m)

1 unit duty

(Grit Chamber High Water Level + 440.18 m)
 (Grit Chamber Low Water Level + 436.00 m)

soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 29.7 m

L: Required Length(m)
 K: Safety Factor(-) 2
 H: Effective Depth 4.18 m
 V: Average Velocity 5.3 cm/sec
 U: Sand Settling Velocity (Dia.0.15mm) 1.5 cm/sec
 B: Number of Basins 1
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 4.2× Basin 1

Effective Volume per Basin(m3) 840
 Basin 1 unit duty
 Effective Volume Total(m3) 840
 Retention Time 10.47 min
 Average Velocity 5.33 cm/sec
 Surface Load Ratio 399 mm/min
 Length/Width 5.6

Case 16 Capacity Calculation of Grit Chamber (River Water Level + 437.60m)

1 unit duty

(Grit Chamber High Water Level + 436.87 m)
 (Grit Chamber Low Water Level + 434.06 m)

no soil

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 55.7 m

L: Required Length(m)
 K: Safety Factor(-) 2
 H: Effective Depth 2.81 m
 V: Average Velocity 7.9 cm/sec
 U: Sand Settling Velocity (Dia.0.10mm) 0.8 cm/sec
 B: Number of Basins 1
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 2.8× Basin 1

Effective Volume per Basin(m3) 565
 Basin 1 unit duty
 Effective Volume Total(m3) 565
 Retention Time 7.04 min
 Average Velocity 7.93 cm/sec
 Surface Load Ratio 399 mm/min
 Length/Width 5.6

Case 17 Capacity Calculation of Grit Chamber (River Water Level + 437.60m)

1 unit duty

(Grit Chamber High Water Level + 436.78 m)

(Grit Chamber Low Water Level + 435.06 m)

soil h=1.00m

Flow Rate 110000* 1.05= 115500 cum/day

Average Velocity 2-7 cm/sec

Surface Load Ratio 200-500mm/min

Width/Length 3-8

Effective Depth 3-4m

Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 55.7 m

L: Required Length(m)

K: Safety Factor(-) 2

H: Effective Depth 1.72 m

V: Average Velocity 13.0 cm/sec

U: Sand Settling Velocity (Dia.0.10mm) 0.8 cm/sec

B: Number of Basins 1

W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level Max. Flood 1447 ft 441.00 m

Max. Operation 1446 ft 440.74 m

Min. Operation 1438 ft 438.30 m

Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 1.7× Basin 1

Effective Volume per Basin(m3) 346

Basin 1 unit duty

Effective Volume Total(m3) 346

Retention Time 4.31 min

Average Velocity 12.95 cm/sec

Surface Load Ratio 399 mm/min

Length/Width 5.6

Case 18 Capacity Calculation of Grit Chamber (River Water Level + 437.60m)

1 unit duty

(Grit Chamber High Water Level + 436.47 m)
 (Grit Chamber Low Water Level + 436.00 m)

soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 55.7 m

L: Required Length(m)
 K: Safety Factor(-) 2
 H: Effective Depth 0.47 m
 V: Average Velocity 47.4 cm/sec
 U: Sand Settling Velocity (Dia.0.10mm) 0.8 cm/sec
 B: Number of Basins 1
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 0.5× Basin 1

Effective Volume per Basin(m3) 94

Basin 1 unit duty

Effective Volume Total(m3) 94

Retention Time 1.18 min

Average Velocity 47.40 cm/sec

Surface Load Ratio 399 mm/min

Length/Width 5.6

Case 19 Capacity Calculation of Grit Chamber (River Water Level + 438.30m) 1 unit duty
 (Grit Chamber High Water Level + 437.54 m)
 (Grit Chamber Low Water Level + 436.00 m) soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min

Required Length $L=K*(H*V/U)/B=$ 55.7 m
 L: Required Length(m)
 K: Safety Factor(-) 2
 H: Effective Depth 1.54 m
 V: Average Velocity 14.5 cm/sec
 U: Sand Settling Velocity (Dia.0.10mm) 0.8 cm/sec
 B: Number of Basins 1
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 1.5× Basin 1

Effective Volume per Basin(m3) 310
 Basin 1 unit duty
 Effective Volume Total(m3) 310
 Retention Time 3.86 min
 Average Velocity 14.47 cm/sec
 Surface Load Ratio 399 mm/min
 Length/Width 5.6

Case 20 Capacity Calculation of Grit Chamber (River Water Level + 440.74m) 1 unit duty

(Grit Chamber High Water Level + 440.18 m)
 (Grit Chamber Low Water Level + 436.00 m) soil h=1.94m

Flow Rate 110000* 1.05= 115500 cum/day
 Average Velocity 2-7 cm/sec
 Surface Load Ratio 200-500mm/min
 Width/Length 3-8
 Effective Depth 3-4m
 Retention Time 10-20min
 Required Length

$L=K*(H*V/U)/B=$ 55.7 m
 L: Required Length(m)
 K: Safety Factor(-) 2
 H: Effective Depth 4.2 m
 V: Average Velocity 5.3 cm/sec
 U: Sand Settling Velocity (Dia.0.10mm) 0.8 cm/sec
 B: Number of Basins 1
 W: Width 6.0 m

Dia. of Sand(mm)	Sediment Velocity (cm/sec)
0.30	3.2
0.20	2.1
0.15	1.5
0.10	0.8
0.08	0.6

Water Level
 Max. Flood 1447 ft 441.00 m
 Max. Operation 1446 ft 440.74 m
 Min. Operation 1438 ft 438.30 m
 Spillway Crest 1425 ft 434.34 m

River Bottom Level at Intake Point 1430 ft 436.00 m

Grit Chamber Dimension
 Width(m) 6.0× Length(m) 33.5× Effective Depth(m) 4.2× Basin 1

Effective Volume per Basin(m3) 840
 Basin 1 unit duty
 Effective Volume Total(m3) 840
 Retention Time 10.47 min
 Average Velocity 5.33 cm/sec
 Surface Load Ratio 399 mm/min
 Length/Width 5.6

Existing Small Stream Reconstruction Plan outside of Intake site (W=2.0m,H=1.00m,Water Depth h=0.50m,Q2,h=0.67mQ3)
Downstream (gate point of intake site - release point)

1 Existing Open Channel

Bottom Level	at gate point of intake site	h1=	443.500 m	GL	445.000 m
	at release point	h2=	442.000 m	EL	442.500 m
Length		L=	135.00 m		
Average Gradient	$I=(h1-h2)/L$	I=	0.0111		

2 Proposed Water Flow

2.1 Rainfall Discharge Flow

Q1=A*I*CR=	0.693 m3/sec	(Rainfall discharge)
where	A= 24.93 ha	(Catchment area)
	I= 50 mm/h	(Rainfall intensity)
	CR= 0.2	(Coefficient of run-off)

2.2 Balancing Tank Overflow Discharge Flow

Q2=	1.273 m3/sec	(Overflow 110,000m3/day)
Q3=	1.910 m3/sec	(Overflow 110,000*1.5m3/day)

3 Proposed open channel

Bottom Level	at gate point of intake site	h1=	441.500 m	(EL	442.500 m)	Channel Depth H=	1.000 m
	at release point	h2=	441.000 m	(EL	442.500 m)	Channel Depth H=	1.500 m
	Mahaweei River	HHWL=	441.00m				
Level Difference between gate and release point		h0=h1-h2=	0.500 m				
Length		L=	137.00 m		(0+325 - 0+462)		
Adopted Gradient	$I=(h1-h2)/L$	I=	0.003650				

4 Water Depth and Channel Bottom Gradient for Q2=1.273m3/sec

Sectional Area of Reconstruction Stream

Q2= 1.273 m3/sec

Inflow sectional area

a=b*h=	1.01 m2
where	b= 2.00 m (Channel Width)
	h= 0.504 m (Water Depth)

Velocity

V2=Q2/a= 1.26 m/sec

Hydraulic radius

$R=(h*b+(0.3*2*h)/2)/(b+1.044*2*h)= 0.380 m$

Roughness coefficient

n= 0.025

Head losses are calculated using Manning Formula.

$h=n^2*L*v^2/R^{4/3}$
where L= 137.00 m

h= 0.497 = 0.500 m <= 0.500 (Proposed Bottom Level Deference h0) OK

I= h/L = 0.003649635

5 Water Depth and Channel Bottom Gradient for Q3=1.910m3/sec

Sectional Area of Reconstruction Stream

Q3= 1.910 m3/sec

Inflow sectional area

a=b*h=	1.34 m2
where	b= 2.00 m (Channel Width)
	h= 0.670 m (Water Depth)

Velocity

V3=Q3/a= 1.43 m/sec

Hydraulic radius

$R=(h*b+(0.3*2*h)/2)/(b+1.044*2*h)= 0.453 m$

Roughness coefficient

n= 0.025

Head losses are calculated using Manning Formula.

$h=n^2*L*v^2/R^{4/3}$
where L= 137.00 m

h= 0.499 = 0.500 m <= 0.500 (Proposed Bottom Level Deference h0) OK

Appendix 6.2 Sri Lanka - Kandy Water Supply Project
 Capacity Calculation for Katugastota Treatment Plant Q=110,000 cu m/day

Item	Total System	First Stage
Planned Flow	Q= 110,000 cu m/day	Q= 36,670 cu m/day
Plant Capacity (Daily Max)	Q= 115,500 cu m/day	Q= 38,500 cu m/day
	= 4,813 cu m/hour	= 1,604 cu m/hour
	= 80.2 cu m/min	= 26.7 cu m/min
	= 1.337 cu m/sec	= 0.446 cu m/sec
(1) Balancing Tank		
Criteria	Retention Time T = 1.5 min Recirculation a = 0.0 %	Retention Time T = 1.5 min Recirculation a = 0.0 %
Dimension	Rectangular 1 units L m x W m x D m x units 7.0 9.0 2.0 1	Rectangular 1 units L m x W m x D m x units 7.0 9.0 2.0 1
	V= 126.0 cu m T= 1.57 min	V= 126.0 cu m T= 4.49 min

Appendix 6.2 Sri Lanka - Kandy Water Supply Project
Capacity Calculation for Katugastota Treatment Plant Q=110,000 cu m/day

Item	Total System	First Stage
Planned Flow	Q= 110,000 cu m/day	Q= 36,670 cu m/day
Plant Capacity (Daily Max)	Q= 115,500 cu m/day = 4,813 cu m/hour = 80.2 cu m/min = 1.337 cu m/sec	Q= 38,500 cu m/day = 1,604 cu m/hour = 26.7 cu m/min = 0.446 cu m/sec
(1) Receiving Well		
Criteria	Retention Time T= 1.5 min Recirculation a= 3.0 %	Retention Time T= 1.5 min Recirculation a= 3.0 %
Dimension	Rectangular 1 units L m x W m x D m x units 4.5 8.1 5.0 1 4	Rectangular 1 units L m x W m x D m x units 4.5 8.1 5.0 1
	V= 182.3 cu m T= 2.2 min	V= 182.3 cu m T= 6.3 min
(2) Mixing Chamber		
Criteria	Retention Time T= 1 - 5 min Recirculation a= 3.0 %	Retention Time T= 1 - 5 min Recirculation a= 3.0 %
Dimension	Rectangular 6 units L m x W m x D m x units 3.5 2.5 3.90 6	Rectangular 2 units L m x W m x D m x units 3.5 2.5 3.90 2
Unit Volume	UV = 34.1 cu m/unit	UV = 34.1 cu m/unit
Total Volume	V = 205 cu m	V = 68 cu m
Retention Time	t = 2.5 min	t = 2.5 min
Mixing	Hydraulic Mixing	Hydraulic Mixing
(3) Flocculator		
Criteria	Retention Time T= 20 - 40 min Recirculation a= 3.0 % Required Volume V = 1,652 cu.m to 3,305 cu.m	Retention Time T= 20 - 40 min Recirculation a= 3.0 % Required Volume V = 551 cu.m to 1,102 cu.m
Unit Flow	q = 13.4 cu m/min/basin	q = 13.4 cu m/min/basin
Dimension	6 units	2 units
Step 1	W m x L m x D m x No.of Channel 1.1 11.0 3.5 2	W m x L m x D m x No.of Channel 1.1 11.0 3.5 2
Step 2	W m x L m x D m x No.of Channel 1.5 11.0 3.5 2	W m x L m x D m x No.of Channel 1.5 11.0 3.5 2
Step 3	W m x L m x D m x No.of Channel 2.3 11.0 3.5 2	W m x L m x D m x No.of Channel 2.3 11.0 3.5 2
Volume	Step 1 84.7 cu m/unit Step 2 115.5 cu m/unit Step 3 177.1 cu m/unit Volume / Unit 377.3 cu m/unit	Step 1 84.7 cu m/unit Step 2 115.5 cu m/unit Step 3 177.1 cu m/unit Volume / Unit 377.3 cu m/unit
Total Volume	V = 2,264 cu m	V = 755 cu m
Retention Time	28.2 minutes	28.2 minutes

Appendix 6.2 Sri Lanka - Kandy Water Supply Project
Capacity Calculation for Katugastota Treatment Plant Q=110,000 cu m/day

Item	Total System	Phase 1
(4) Seddimentation Basin		
Type	Rectangular, Horizontal Flow	Rectangular, Horizontal Flow
Unit Flow	q = 826 cu m/hr/basin (Recirculation a = 3.0 %)	q = 826 cu m/hr/basin (Recirculation a = 3.0 %)
Criteria	Retention Time T = 2.5 hours Surface Load a = 15 - 30 mm/min Hor. Flow Velocity v < 0.40 m/min L/W Ratio L/W = 3 - 8 times Depth D = 3 - 4 m Depth of 50 cm or more is provided for sludge settlement.	Retention Time T = 2.5 hours Surface Load a = 15 - 30 mm/min Hor. Flow Velocity v < 0.40 m/min L/W Ratio L/W = 3 - 8 times Depth D = 3 - 4 m Depth of 50 cm or more is provided for sludge settlement.
Original Dimension	No. 6 basins W m x L m x D m x N 11 50 4.0 6	No. 2 basins W m x L m x D m x N 11 50 4.0 2
Volume	V = 2,200 cu m/basin	V = 2,200 cu m/basin
Retention Time	T = 2.66 hours	T = 2.7 hours
L/W Ratio	L/W = 4.5	L/W = 4.5
Surface Load	a = 25.0 mm/min	a = 25.0 mm/min
Hor. Flow Velocity	v = 0.313 m/min	v = 0.313 m/min
Revised Dimension	No. 6 basins W m x L m x D m x N 11 41 4.0 6 1st step 11.0 m 100 %Q 2nd step 10.0 m 100 %Q 3rd step 10.0 m 80 %Q 4th step 10.0 m 60 %Q Total Length 41.0 m	No. 2 basins W m x L m x D m x N 11 41 4.0 2 1st step 11.0 m 100 %Q 2nd step 10.0 m 100 %Q 3rd step 10.0 m 80 %Q 4th step 10.0 m 60 %Q Total Length 41.0 m
Volume	V = 1,804 cu m/basin	V = 1,804 cu m/basin
Retention Time	T = 2.18 hours	T = 2.18 hours
L/W Ratio	L/W = 3.7	L/W = 3.7
Surface Load	a = 25.0 mm/min	a = 25.0 mm/min
Hor. Flow Velocity	v = 0.313 m/min	v = 0.313 m/min
Overflow Weir	Load = 500 m ³ /m/day	Load = 500 m ³ /m/day
Trough Length	L = 24 m or longer	L = 24 m or longer
	No. 8 troughs/unit L m x N 2.0 8 L = 32.0 m	No. 8 troughs/unit L m x N 2.0 8 L = 32.0 m
Weir Load	L = 372 m ³ /m/day	L = 372 m ³ /m/day
Sludge Removal	Recipro Type Collector	Recipro Type Collector
Sludge Amount Solid Amount (ton-DS)	So = Q * (K*(T1-T2)+B*156/666)*10 ⁻⁶ where So:Sludge dry weight(ton) Q :Treated water amount(m ³ /d) K :Coefficient converting turbidity to SS (0.8-1.5 ->>1.2) T1 :Turbidity in raw water (ave= 40 T2 :Turbidity after Sedimentation (ave = Q 10 B :Aium dosage rate (ave.= 16.6 B = 4 + 2 * (T1-T2) ^ 0.5 = So = 5.81 ton-DS/day	So = 1.94 ton-DS/day
Water Contents of Drained Sludge (with wash-out water)	w = 98.0 %	w = 98.0 %
Frequency of Cleaning :	Once a Year	Once a Year
Sludge Volume	Total v = 106,115 cu.m/year So = 2,122 ton-DS/year Per tank v = 17,686 cu.m/basin/year So = 354 ton-DS/basin/year	Total v = 35,372 cu.m/year So = 707 ton-DS/year Per tank v = 17,686 cu.m/basin/year So = 354 ton-DS/basin/year

Appendix 6.2 Sri Lanka - Kandy Water Supply Project
Capacity Calculation for Katugastota Treatment Plant Q=110,000 cu m/day

Item	Total System	First Stage
(5) Rapid Sand Filter		
Type	Down Flow, Single Media	Down Flow, Single Media
No.	12 units (wash 3 group)	4 units (wash 1 group)
Unit Flow	q = 9,900 cu m/day/unit (Recirculation a = 3.0 %)	q = 9,900 cu m/day/unit (Recirculation a = 3.0 %)
Criteria	Filtration Rate Fr = 150 m/day (for normal operation) Filter Area per Unit A < 150 sq m	Filtration Rate Fr = 150 m/day (for normal operation) Filter Area per Unit A < 150 sq m
Dimension	W m x L m x N units 7.2 9.6 12 (4 filters/group)	W m x L m x N units 7.2 9.6 4 (4 filters/group)
	A = 69.1 sq m/unit	A = 69.1 sq m/unit
Filtration Rate	Fr = 143.2 m/day	Fr = 143.2 m/day
Filtration Rate during washing	Fr' = 191.0 m/day 3 units out of 12 are washing	Fr' = 191.0 m/day 1 units out of 4 are washing
Filters for Backwashing	2.3 filters/group	2.3 filters/group
Filter Washing Frequency	Once a day for each filter	Once a day for each filter
Water Rate	Backwashing rate = 0.30 m3/m2/min duration = 12 min	Backwashing rate = 0.30 m3/m2/min duration = 12 min
Air Rate	Air Scouring rate = 1.00 m3/m2/min duration = 3 min	Air Scouring rate = 1.00 m3/m2/min duration = 3 min
Water Amount for washing	Backwashing Vb = 248.8 cu m/unit	Backwashing Vb = 248.8 cu m/unit
for Total Units	Total Amount for Washing 2,986.0 cu m/day Percentage for Planned Flow 2.6 %	Total Amount for Washing 995.3 cu m/day Percentage for Planned Flow 2.6 %
Solid Amount in Wastewater (ton-DS)	So = Q*K*(T1-T2)*10^-6 where So:Sludge dry weight(ton) Q :Treated water amount(m3/d) K :Coefficient converting turbidity to SS (0.8-1.5 ->1.2) T1 :Turbidity before filter(ave= 5) T2 :Turbidity after filter(ave = 0) So = 0.69 ton-DS/day	So = 0.23 ton-DS/day
SS Contents	s = 232 mg/l	s = 232 mg/l
(6) Backwash Water Storage Tank		
Location	at the Outlet of the Filtration Units	at the Outlet of the Filtration Units
Criteria	V > Backwash Water for 1 unit	V > Backwash Water for 1 unit
Required Volume	V = 248.8 cu m	V = 248.8 cu m
Dimension	No. 1 units L m x W m x D m m x N units 17.7 8.0 2.09 1	No. 1 units L m x W m x D m m x N units 17.7 8.0 2.09 1
Total Volume	v = 296 cu m	v = 296 cu m

Appendix 6.2 Sri Lanka - Kandy Water Supply Project
Capacity Calculation for Katugastota Treatment Plant Q=110,000 cu m/day

Item	Total System	First Stage
(7) Clear Water Reservoir		
Criteria	Retention Time T > 1.0 hours	Retention Time T > 1.0 hours
Required Volume	V = 4,580 cu m	V = 1,530 cu m
Dimension	No. 6 units L m x W m x D m m x N units 21.0 13.8 3.0 6	No. 2 units L m x W m x D m m x N units 21.0 13.8 3.0 2
Total Volume	V = 5,216 cu m	V = 1,739 cu m
Retention Time	T = 1.14 hours	T = 1.14 hours
(8) Alum Dissolving Tank		
Coagulant	Solid Aluminum Sulphate (Al ₂ (SO ₄) ₃) containing 15 % Al ₂ O ₃	Solid Aluminum Sulphate (Al ₂ (SO ₄) ₃) containing 15 % Al ₂ O ₃
Criteria	Dosage Rate : 10-60 mg-solid alum/l Average 30 mg/l Coagulant Solution : 10 % sg = 1.0525 Retention Time 24 hours Dissolving Time 2 hours	Dosage Rate : 10-60 mg-solid alum/l Average 30 mg/l Coagulant Solution : 10 % sg = 1.0525 Retention Time 24 hours Dissolving Time 2 hours
Dosage Amount	Wt = 3,465 kg-Alum/day (Max dosage) V = 32.9 cu m/day	Wt = 1,155 kg-Alum/day (Max dosage) V = 11.0 cu m/day
Solution Tank Dimension	Square 4 units L m x W m x D m x units 2.0 2.0 2.5 4	Square 2 units L m x W m x D m x units 2.0 2.0 2.5 2
Total Volume	V = 40.0 cu m	V = 20.0 cu m
Retention Time	T = 29.2 hours	T = 43.7 hours
Storage	Period 30 days Bulk s. g. 0.60	Period 30 days Bulk s. g. 0.60
Storage Area	A = 87 m ² at 2.0 m height	A = 29 m ² at 2.0 m height
(9) Lime Dissolving Tank		
pH Control	Hydrated Lime (Ca(OH) ₂) containing 72 % CaO	Hydrated Lime (Ca(OH) ₂) containing 72 % CaO
Criteria	Dosage Rate : 5-30 mg-solid Lime/l Requirement 10.4 mg/l (Pre5-30, Post5-20 mg/l) Average 15.0 mg/l (Pre10, Post5 mg/l) Lime Solution 10 % sg = 1.0607 Retention Time 24 hours Dissolving Time 2 hours	Dosage Rate : 5-30 mg-solid Lime/l Requirement 10.4 mg/l (Pre5-30, Post5-20 mg/l) Average 15.0 mg/l (Pre10, Post5 mg/l) Lime Solution 10 % sg = 1.0607 Retention Time 24 hours Dissolving Time 2 hours
Dosage Amount	Wt = 1,733 kg-Alum/day (Max dosage) V = 16.3 cu m/day	Wt = 578 kg-Alum/day (Max dosage) V = 5.4 cu m/day
Solution Tank Dimension	Square 4 units L m x W m x D m x units 2.0 2.0 2.5 4	Square 2 units L m x W m x D m x units 2.0 2.0 2.5 2
Total Volume	V = 40.0 cu m	V = 20.0 cu m
Retention Time	T = 58.8 hours	T = 88.2 hours
Storage	Period 30 days Bulk s. g. 0.40	Period 30 days Bulk s. g. 0.40
Storage Area	A = 65 m ² at 2.0 m height	A = 22 m ² at 2.0 m height

Appendix 6.2 Sri Lanka - Kandy Water Supply Project
Capacity Calculation for Katugastota Treatment Plant Q=110,000 cu m/day

Item	Total System	First Stage
(10) Chlorination Equipment		
Injection Point	at the Inlet of Clear Water Reservoir and outlet of Sedimentation Basin	at the Inlet of Clear Water Reservoir and outlet of Sedimentation Basin
Type	Liquid Chlorine (900 kg-cylinder)	Liquid Chlorine (900 kg-cylinder)
Criteria	Dosage Rate : 7.0 mg-Cl/l (Pre1.0-5.0, Post1.0-5.0)	Dosage Rate : 7.0 mg-Cl/l (Pre1.0-5.0, Post1.0-5.0)
	Average 3.0 mg/l (Pre2.0, Post1.0 mg/l)	Average 3.0 mg/l (Pre2.0, Post1.0 mg/l)
Dosage Amount	Wt = 347 kg- Cl gas/day	Wt = 116 kg- Cl gas/day
	or 14 kg- Cl gas/hour	or 5 kg- Cl gas/hour
Chlorinator	Vacuum Type	Vacuum Type
No. of unit	3 units (excl. 1 unit stand-by)	1 units (excl. 1 unit stand-by)
	Rate 4.81 kg/hour/unit	Rate 4.81 kg/hour/unit
Operation Rate	60 percent	60 percent
	Capacity 8 kg/hour/unit	Capacity 8 kg/hour/unit
Storage	Period 30 days	Period 30 days
Storage Area	A = 24 m ² as 2.0 m ² /container	A = 9 m ² as 2.0 m ² /container
(11) Backwash Wastewater Storage Tank		
Retention Time	1 hours	1 hours
Backwash Water	Vs + Vb = 249 cu.m/filter unit	Vs + Vb = 249 cu.m/filter unit
Required Volume	1 filters 249 cu.m	1 filters 249 cu.m
No.	N = 2 units	N = 2 units
Dimension	L m x W m x D m m x N units 14.0 6.0 3.00 2	L m x W m x D m m x N units 14.0 6.0 3.00 2
Total Volume	v = 504 cu m	v = 504 cu m
Frequency of Wash	Once a day = 12 filters/day	Once a day = 4 filters/day
(12) Sludge Lagoon		
	So = 5.81 ton-DS/day	So = 1.94 ton-DS/day
	Water Contents in Sludge Lagoon	Water Contents of Drained Sludge (with wash-out water)
	w = 70.0 %	w = 70.0 %
Sludge Amount	Total v = 7,074 cu.m/year	Total v = 2,358 cu.m/year
	So = 2,122 ton-DS/year	So = 707 ton-DS/year
Required Volume	v = 7,074 cu m	v = 2,358 cu m
Dimension	Rectangular 3 units + 1 unit for stand-by	Rectangular 1 units + 1 unit for stand-by
	L m x W m x D m x units 4 70.0 35.0 1.0 4	L m x W m x D m x units 2 70.0 35.0 1.0 2
Total Volume	v = 7,350 cu m	v = 2,450 cu m

02 Intake and Water Treatment Plant Hydraulic Calculations

Intake Facilities Water Level (0.5m settling soil at 1nlet channel)

Quantity	Duty	R.W.L.(m)		G.W.L.	P.C.W.L.	Remark
Q=1.0	1 unit	LLWL	437.60	436.87	436.59	Bottom Level is 434.06m(no soil)
		LLWL	437.60	436.78	436.40	Sedimentation Level is 435.06m(h=1.0m)
		LLWL	437.60	436.47	435.94	Sedimentation Level is 436.00m(h=1.94m)
		LWL	438.30	437.54	437.36	Sedimentation Level is 436.00m(h=1.94m)
		HWL	440.74	440.18	440.12	Sedimentation Level is 436.00m(h=1.94m)
Q=1.0	2 units	LLWL	437.60	437.11	437.03	Bottom Level is 434.06m(no soil)
		LLWL	437.60	437.09	437.01	Sedimentation Level is 435.06m(h=1.0m)
		LLWL	437.60	437.01	436.93	Sedimentation Level is 436.00m(h=1.94m)
		LWL	438.30	437.80	437.75	Sedimentation Level is 436.00m(h=1.94m)
		HWL	440.74	440.29	440.27	Sedimentation Level is 436.00m(h=1.94m)

Note: R.W.L.: River Water Level
G.W.L.: Grit Chamber Water Level
P.C.W.L.: Pump Chamber Water Level

Intake facilities water loss (River water level +437.6m)

2 unit duty

1 River Water Level

L.L.W.L. 437.600 m

2 Intake Flow & Velocity

Q1= 38500 m3/day= 0.446 m3/sec
 Q2= 77000 m3/day= 0.891 m3/sec
 Q3= 115500 m3/day= 1.337 m3/sec

3 Bar Screen Loss

B= 2.00 m (37.5 *44= 1.650 m)
 H= 1.10 m (Bottom Level 436.500 m) Including Sed. Depth h=0.50m
 b= 37.5 mm
 t= 12.5 mm
 θ= 70 °
 V= 0.368 m/s (Q= 1.337 /2= 0.668403)
 H= 0.003 m

Therefore h1= 0.300 m (WL+ 437.300 m, depth 0.800 m)
 (Bottom Level 436.500 m) settling soil 0.5m

4 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm^2 = 2.4 m^2$: Sectional area (H= 0.80 m)

Q= 1.337 m3/sec
 $v = Q/A = 0.557 m/sec$
 $g = 9.8 m/sec^2$
 C= 0.6
 $h4 = 0.0440 m = 0.050 m$

(WL+ 437.250 m, depth 0.750 m)
 (Bottom Level 436.500 m)

5 Rubbish Remover

B= 2.00 m (20 *44= 0.880 m)
 H= 0.75 m (Bottom Level 436.500 m)
 b= 20.0 mm
 t= 3 mm
 θ= 70 °
 V= 2.025 m/s (Q= 1.337 /2= 0.668403)
 H= 0.028 m

Therefore h2= 0.100 m (WL+ 437.150 m, depth 0.650 m)
 (Bottom Level 436.500 m)

6 Head loss in the channel

Q1= 0.668 m3/sec : Water flow of 1 trough (Q= 1.337 /2= 0.668)

Inflow sectional area

$A = B * H = 1.30 m^2$
 where B= 2.00 m
 H= 0.65 m

Velocity

$V(a-b) = Q1/A = 0.51 m/sec$

Hydraulic radius

$R = A / (B + H * 2) = 0.394 m$

Roughness coefficient

n= 0.015

Head losses are calculated using Manning Formula.

$h = n^2 * L * v^2 / R^{4/3}$

where L= 26.0 m

h3= 0.00536 = 0.010 m (WL+ 437.140 m, depth 0.640 m)
 (Bottom Level 436.500 m)

7 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$	1.554 m ²	: Sectional area		
D =	100 mmdia.			
a =	18 pieces			
b =	11 pieces	(Bottom Level	434.060 m =	434.06 + 0.00)
Q =	0.668 m ³ /sec		(Q = 1.337 / 2 =	0.668)
v = Q/A =	0.43 m/sec			
g =	9.8 m/sec ²			
C =	0.6			
h ₅ =	0.026 m	=		0.030 m

8 Grit chamber water level 437.110 m

9 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$	0.989 m ²	: Sectional area		
D =	100 mmdia.			
a =	18 pieces			
b =	7 pieces	(Bottom Level	434.06 m)	
Q =	0.668 m ³ /sec		(Q = 1.337 / 2 =	0.668)
v = Q/A =	0.68 m/sec			
g =	9.8 m/sec ²			
C =	0.6			
h ₅ =	0.065 m	=	0.070 m	(WL+ 437.040 m, depth 2.980 m)
				(Bottom Level 434.060 m)

10 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm^2 =$	4.8 m ²	: Sectional area	(H = 1.60 m)	
Q =	0.668 m ³ /sec		(Q = 1.337 / 2 =	0.668)
v = Q/A =	0.139 m/sec			
g =	9.8 m/sec ²			
C =	0.6			
h ₆ =	0.00275 m	=	0.010 m	(WL+ 437.030 m, depth 3.870 m)
				(Bottom Level 433.160 m)

11 Conveyance Pump chamber water level 437.030 m

Intake facilities water loss (River water level +437.6m)

2 unit duty

1 River Water Level

L.L.W.L. 437.600 m

2 Intake Flow & Verosity

Q1= 38500 m3/day= 0.446 m3/sec
 Q2= 77000 m3/day= 0.891 m3/sec
 Q3= 115500 m3/day= 1.337 m3/sec

3 Bar Screen Loss

B= 2.00 m (37.5 *44= 1.650 m)
 H= 1.10 m (Bottom Level 436.500 m) Including Sed. Depth h=0.50m
 b= 37.5 mm
 t= 12.5 mm
 θ= 70 °
 V= 0.368 m/s (Q= 1.337 /2= 0.668403)
 H= 0.003 m

Threrfore h1= 0.300 m (WL+ 437.300 m, depth 0.800 m)
 (Bottom Level 436.500 m) settling soil 0.5m

4 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm^2 = 2.4 m^2$: Sectional area (H= 0.80 m)

Q= 1.337 m3/sec

$v = Q/A = 0.557 m/sec$

g= 9.8 m/sec²

C= 0.6

$h4 = 0.0440 m = 0.050 m$ (WL+ 437.250 m, depth 0.750 m)
 (Bottom Level 436.500 m) 0.880 m)

5 Rubbish Remover

B= 2.00 m (20 *44= 0.880 m)
 H= 0.75 m (Bottom Level 436.500 m)
 b= 20.0 mm
 t= 3 mm
 θ= 70 °
 V= 2.025 m/s (Q= 1.337 /2= 0.668403)
 H= 0.028 m

Threrfore h2= 0.100 m (WL+ 437.150 m, depth 0.650 m)
 (Bottom Level 436.500 m)

6 Head loss in the channel

Q1= 0.668 m3/sec : Water flow of 1 trough (Q= 1.337 /2= 0.668)

Inflow sectional area

$A = B * H = 1.30 m^2$

where B= 2.00 m
 H= 0.65 m

Velocity

$V(a-b) = Q1/A = 0.51 m/sec$

Hydraulic radius

$R = A / (B + H * 2) = 0.394 m$

Roughness coefficient

n= 0.015

Head losses are calculated using Manning Formula.

$h = n^2 * L * v^2 / R^{4/3}$

where L= 26.0 m

h3= 0.00536 = 0.010 m (WL+ 437.140 m, depth 0.640 m)
 (Bottom Level 436.500 m)

7 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 1.130 m² : Sectional area

D = 100 mmdia.

a = 18 pieces

b = 8 pieces (Sedimentation Level 435.060 m = 434.06 + 1.0)

Q = 0.668 m³/sec (Q = 1.337 / 2 = 0.668)

v = Q / A = 0.59 m/sec

g = 9.8 m/sec²

C = 0.6

h₅ = 0.050 m = 0.050 m

8 Grit chamber water level 437.090 m

9 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 0.989 m² : Sectional area

D = 100 mmdia.

a = 18 pieces

b = 7 pieces (Bottom Level 434.06 m)

Q = 0.668 m³/sec (Q = 1.337 / 2 = 0.668)

v = Q / A = 0.68 m/sec

g = 9.8 m/sec²

C = 0.6

h₅ = 0.065 m = 0.070 m (WL+ 437.020 m, depth 2.960 m)
(Bottom Level 434.060 m)

10 Head loss of Intake gate

Dimension of gate; 1500 x 1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5 * H * m^2 =$ 4.8 m² : Sectional area (H = 1.60 m)

Q = 0.668 m³/sec (Q = 1.337 / 2 = 0.668)

v = Q / A = 0.139 m/sec

g = 9.8 m/sec²

C = 0.6

h₆ = 0.00275 m = 0.010 m (WL+ 437.010 m, depth 3.850 m)
(Bottom Level 433.160 m)

11 Conveyance Pump chamber water level 437.010 m

Intake facilities water loss (River water level +437.6m)

2 unit duty

1 River Water Level

L.L.W.L. 437.600 m

2 Intake Flow & Verosity

Q1= 38500 m3/day= 0.446 m3/sec
 Q2= 77000 m3/day= 0.891 m3/sec
 Q3= 115500 m3/day= 1.337 m3/sec

3 Bar Screen Loss

B= 2.00 m (37.5 *44= 1.650 m)
 H= 1.10 m (Bottom Level 436.500 m) Including Sed. Depth h=0.50m
 b= 37.5 mm
 t= 12.5 mm
 θ = 70 °

V= 0.368 m/s (Q= 1.337 /2= 0.668403)

H= 0.003 m

Therfore h1= 0.300 m (WL+ 437.300 m, depth 0.800 m)
 (Bottom Level 436.500 m) settling soil 0.5m

4 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h=v^2/(2*g*C^2)$

where $A=1.5m*Hm^2= 2.4 m^2$: Sectional area (H= 0.80 m)

Q= 1.337 m3/sec

$v=Q/A= 0.557 m/sec$

g= 9.8 m/sec²

C= 0.6

$h4= 0.0440 m = 0.050 m$ (WL+ 437.250 m, depth 0.750 m)
 (Bottom Level 436.500 m)

5 Rubbish Remover

B= 2.00 m (20 *44= 0.880 m)
 H= 0.75 m (Bottom Level 436.500 m)

b= 20.0 mm

t= 3 mm

θ = 70 °

V= 2.025 m/s (Q= 1.337 /2= 0.668403)

H= 0.028 m

Therfore h2= 0.100 m (WL+ 437.150 m, depth 0.650 m)
 (Bottom Level 436.500 m)

6 Head loss in the channel

Q1= 0.668 m3/sec : Water flow of 1 trough (Q= 1.337 /2= 0.668)

Inflow sectional area

$A=B*H= 1.30 m^2$

where B= 2.00 m

H= 0.65 m

Velocity

$V(a-b)=Q1/A= 0.51 m/sec$

Hydraulic radius

$R=A/(B+H*2)= 0.394 m$

Roughness coefficient

n= 0.015

Head losses are calculated using Manning Formula.

$h=n^2*L*v^2/R^(4/3)$

where L= 26.0 m

h3= 0.00536 = 0.010 m (WL+ 437.140 m, depth 0.640 m)
 (Bottom Level 436.500 m)

7 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$	0.707 m ²	: Sectional area		
D=	100 mmdia.			
a=	18 pieces			
b=	5 pieces	(Sedimentation Level	436.000 m=	434.06 + 1.94)
Q=	0.668 m ³ /sec		(Q= 1.337 /2=	0.668)
v=Q/A=	0.95 m/sec			
g=	9.8 m/sec ²			
C=	0.6			
h ₅ =	0.127 m	=	0.130 m	

8 Grit chamber water level 437.010 m

9 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$	0.989 m ²	: Sectional area		
D=	100 mmdia.			
a=	18 pieces			
b=	7 pieces	(Bottom Level	434.06 m)	
Q=	0.668 m ³ /sec		(Q= 1.337 /2=	0.668)
v=Q/A=	0.68 m/sec			
g=	9.8 m/sec ²			
C=	0.6			
h ₅ =	0.065 m	=	0.070 m	
		(WL+	436.940 m, depth	2.880 m)
		(Bottom Level	434.060 m)	

10 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm * 2 =$	4.8 m ²	: Sectional area	(H= 1.60 m)	
Q=	0.668 m ³ /sec		(Q= 1.337 /2=	0.668)
v=Q/A=	0.139 m/sec			
g=	9.8 m/sec ²			
C=	0.6			
h ₆ =	0.00275 m	=	0.010 m	
		(WL+	436.930 m, depth	3.770 m)
		(Bottom Level	433.160 m)	

11 Conveyance Pump chamber water level 436.930 m

Intake facilities water loss (River water level +438.3m)

2 unit duty

1 River Water Level

H.W.L. 438.300 m

2 Intake Flow & Verosity

Q1= 38500 m3/day= 0.446 m3/sec
 Q2= 77000 m3/day= 0.891 m3/sec
 Q3= 115500 m3/day= 1.337 m3/sec

3 Bar Screen Loss

B= 2.00 m (37.5 *44= 1.650 m)
 H= 1.80 m (Bottom Level 436.500 m) Including Sed. Depth h=0.50m
 b= 37.5 mm
 t= 12.5 mm
 θ = 70 °

V= 0.225 m/s (Q= 1.337 /2= 0.668403)
 H= 0.001 m

Threrfore h1= 0.300 m (WL+ 438.000 m, depth 1.500 m)
 (Bottom Level 436.500 m) settling soil 0.5m

4 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h=v^2/(2*g*C^2)$

where $A=1.5m*Hm*2=$ 3.3 m2 : Sectional area (H= 1.10 m)

Q= 1.337 m3/sec

$v=Q/A=$ 0.405 m/sec

g= 9.8 m/sec2

C= 0.6

$h4=$ 0.0233 m = 0.030 m (WL+ 437.970 m, depth 1.470 m)
 (Bottom Level 436.500 m)

5 Rubbish Remover

B= 2.00 m (20 *44= 0.880 m)
 H= 1.47 m (Bottom Level 436.500 m)
 b= 20.0 mm
 t= 3 mm
 θ = 70 °

V= 1.033 m/s (Q= 1.337 /2= 0.668403)
 H= 0.007 m

Threrfore h2= 0.100 m (WL+ 437.870 m, depth 1.370 m)
 (Bottom Level 436.500 m)

6 Head loss in the channel

Q1= 0.668 m3/sec : Water flow of 1 trough (Q= 1.337 /2= 0.668)

Inflow sectional area

$A=B*H=$ 2.74 m2

where B= 2.00 m
 H= 1.37 m

Velocity

$V(a-b)=Q1/A=$ 0.24 m/sec

Hydraulic radius

$R=A/(B+H*2)=$ 0.578 m

Roughness coefficient

n= 0.015

Head losses are calculated using Manning Formula.

$h=n^2*L*v^2/R^(4/3)$

where L= 26.0 m

h3= 0.00072 = 0.000 m (WL+ 437.870 m, depth 1.370 m)
 (Bottom Level 436.500 m)

7 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) = 0.989 \text{ m}^2$: Sectional area

D = 100 mmdia.

a = 18 pieces

b = 7 pieces

Q = 0.668 m³/sec

v = Q/A = 0.68 m/sec

g = 9.8 m/sec²

C = 0.6

h₅ = 0.065 m = 0.070 m

(Bottom Level 436.000 m = 434.06 + 1.94)
(Q = 1.337 / 2 = 0.668)

8 Grit chamber water level 437.800 m

9 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) = 1.413 \text{ m}^2$: Sectional area

D = 100 mmdia.

a = 18 pieces

b = 10 pieces

Q = 0.668 m³/sec

v = Q/A = 0.47 m/sec

g = 9.8 m/sec²

C = 0.6

h₅ = 0.032 m = 0.040 m

(Bottom Level 434.06 m)
(Q = 1.337 / 2 = 0.668)

(WL+ 437.760 m, depth 1.760 m)
(Bottom Level 436.000 m)

10 Head loss of Intake gate

Dimension of gate; 1500 × 1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5 \text{ m} * H \text{ m} * 2 = 4.8 \text{ m}^2$: Sectional area (H = 1.60 m)

Q = 0.668 m³/sec (Q = 1.337 / 2 = 0.668)

v = Q/A = 0.139 m/sec

g = 9.8 m/sec²

C = 0.6

h₆ = 0.00275 m = 0.010 m

(WL+ 437.750 m, depth 4.590 m)
(Bottom Level 433.160 m)

11 Conveyance Pump chamber water level 437.750 m

Intake facilities water loss (River water level +440.74m)

2 unit duty

1 River Water Level

H.W.L. 440.740 m

2 Intake Flow & Verosity

Q1= 38500 m3/day= 0.446 m3/sec
 Q2= 77000 m3/day= 0.891 m3/sec
 Q3= 115500 m3/day= 1.337 m3/sec

3 Head loss of Inlet Orifice

where $A=a*b=$ 11 m² : Sectional area
 $a=$ 6 m
 $b=$ 1.9 m (Sedimentation Level 436.500 m= 436.000 + 0.5)
 $Q=$ 0.668 m3/sec (Q= 1.337 /2= 0.668403)
 $v=Q/A=$ 0.06 m/sec
 $g=$ 9.8 m/sec²
 $C=$ 0.6
 $h5=$ 0.0005 m = 0.000 m (WL+ 440.740 m, depth 4.240 (Bottom Level 436.500 m) settling soil 0.5m)

4 Bar Screen Loss

$B=$ 2.00 m (37.5 *44= 1.650 m)
 $H=$ 4.24 m (Sedimentation Level 436.50 m)
 $b=$ 37.5 mm
 $t=$ 12.5 mm
 $\theta =$ 70 °
 $V=$ 0.096 m/s (Q= 1.337 /2= 0.668403)
 $H=$ 0.000 m

Threrfore $h1=$ 0.300 m (WL+ 440.440 m, depth 3.940 m) (Bottom Level 436.500 m)

5 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h=v^2/(2*g*C^2)$

where $A=1.5m*Hm*2=$ 3.3 m² : Sectional area (H= 1.10 m)
 $Q=$ 1.337 m3/sec
 $v=Q/A=$ 0.405 m/sec
 $g=$ 9.8 m/sec²
 $C=$ 0.6
 $h4=$ 0.0233 m = 0.030 m (WL+ 440.410 m, depth 3.910 m) (Bottom Level 436.500 m)

6 Rubbish Remover

$B=$ 2.00 m (20 *44= 0.880 m)
 $H=$ 3.91 m (Bottom Level 436.500 m)
 $b=$ 20.0 mm
 $t=$ 3 mm
 $\theta =$ 70 °
 $V=$ 0.389 m/s (Q= 1.337 /2= 0.668403)
 $H=$ 0.001 m

Threrfore $h2=$ 0.100 m (WL+ 440.310 m, depth 3.810 m) (Bottom Level 436.500 m)

7 Head loss in the channel

Q1= 0.668 m3/sec : Water flow of 1 trough (Q= 1.337 /2= 0.668)

Inflow sectional area

$A=B*H=$ 7.62 m²
 where $B=$ 2.00 m
 $H=$ 3.81 m

Velocity

$V(a-b)=Q1/A=$ 0.09 m/sec

Hydraulic radius

$R=A/(B+H*2)=$ 0.792 m

Roughness coefficient
 $n = 0.015$

Head losses are calculated using Manning Formula.

$h = n^2 * L * v^2 / R^{4/3}$
 where $L = 26.0$ m

$h_3 = 0.00006 = 0.000$ m (WL+ 440.310 m, depth 3.810 m)
 (Bottom Level 436.500 m)

8 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) = 2.120$ m² : Sectional area

$D = 100$ mmdia.

$a = 18$ pieces

$b = 15$ pieces (Bottom Level 436.000 m = 434.06 + 1.94)

$Q = 0.668$ m³/sec (Q= 1.337 /2= 0.668)

$v = Q / A = 0.32$ m/sec

$g = 9.8$ m/sec²

$C = 0.6$

$h_5 = 0.014$ m = 0.020 m

9 Grit chamber water level 440.290 m

10 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) = 2.543$ m² : Sectional area

$D = 100$ mmdia.

$a = 18$ pieces

$b = 18$ pieces (Bottom Level 434.06 m)

$Q = 0.668$ m³/sec (Q= 1.337 /2= 0.668)

$v = Q / A = 0.26$ m/sec

$g = 9.8$ m/sec²

$C = 0.6$

$h_5 = 0.010$ m = 0.010 m (WL+ 440.280 m, depth 6.220 m)
 (Bottom Level 434.060 m)

11 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm * 2 = 4.8$ m² : Sectional area (H= 1.60 m)

$Q = 0.668$ m³/sec (Q= 1.337 /2= 0.668)

$v = Q / A = 0.139$ m/sec

$g = 9.8$ m/sec²

$C = 0.6$

$h_6 = 0.00275$ m = 0.010 m (WL+ 440.270 m, depth 7.110 m)
 (Bottom Level 433.160 m)

12 Conveyance Pump chamber water level 440.270 m

Intake facilities water loss (River water level +437.6m)

1 unit duty

1 River Water Level

L.L.W.L. 437.60 m

2 Intake Flow & Verosity

Q1= 38500 m3/day= 0.446 m3/sec
 Q2= 77000 m3/day= 0.891 m3/sec
 Q3= 115500 m3/day= 1.337 m3/sec

3 Bar Screen Loss

B= 2.00 m (37.5 *44= 1.650 m)
 H= 1.10 m (Bottom Level 436.500 m) Including Sed. Depth h=0.50m
 b= 37.5 mm
 t= 12.5 mm
 θ = 70 °
 V= 0.737 m/s
 H= 0.011 m

Threrfore h1= 0.300 m (WL+ 437.300 m, depth 0.800 m)
 (Bottom Level 436.500 m) settling soil 0.5m

4 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h = v^2 / (2 * g * C^2)$

where A=1.5m*Hm= 1.2 m2 : Sectional area (H= 0.80 m)
 Q= 1.337 m3/sec
 v=Q/A= 1.114 m/sec
 g= 9.8 m/sec2
 C= 0.6
 h4= 0.1759 m = 0.180 m (WL+ 437.120 m, depth 0.620 m)
 (Bottom Level 436.500 m)

5 Rubbish Remover

B= 2.00 m (20 *44= 0.880 m)
 H= 0.62 m (Bottom Level 436.500 m)
 b= 20.0 mm
 t= 3 mm
 θ = 70 °
 V= 2.450 m/s
 H= 0.041 m

Threrfore h2= 0.100 m (WL+ 437.020 m, depth 0.520 m)
 (Bottom Level 436.500 m)

6 Head loss in the channel

Q1= 1.337 m3/sec : Water flow of 1 trough

Inflow sectional area

A=B*H= 1.04 m2
 where B= 2.00 m
 H= 0.52 m

Velocity

V(a-b)=Q1/A= 1.29 m/sec

Hydraulic radius

R=A/(B+H*2)= 0.342 m

Roughness coefficient

n= 0.015

Head losses are calculated using Manning Formula.

$h = n^2 * L * v^2 / R^{(4/3)}$

where L= 26.0 m

h3= 0.04040 = 0.040 m (WL+ 436.980 m, depth 0.480 m)
 (Bottom Level 436.500 m)

7 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 1.554 m² : Sectional area
 D= 100 mmdia.
 a= 18 pieces
 b= 11 pieces (Bottom Level 434.060 m= 434.06 + 0.00)
 Q= 1.337 m³/sec
 v=Q/A= 0.86 m/sec
 g= 9.8 m/sec²
 C= 0.6
 h₅= 0.105 m = 0.110 m

8 Grit chamber water level 436.870 m

9 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 0.989 m² : Sectional area
 D= 100 mmdia.
 a= 18 pieces
 b= 7 pieces (Bottom Level 434.060 m)
 Q= 1.337 m³/sec
 v=Q/A= 1.35 m/sec
 g= 9.8 m/sec²
 C= 0.6
 h₅= 0.259 m = 0.260 m (WL+ 436.610 m, depth 2.550 m)
 (Bottom Level 434.060 m)

10 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm * 2 =$ 4.8 m² : Sectional area (H= 1.60 m)
 Q= 1.337 m³/sec
 v=Q/A= 0.279 m/sec
 g= 9.8 m/sec²
 C= 0.6
 h₆= 0.01099 m = 0.020 m (WL+ 436.590 m, depth 3.430 m)
 (Bottom Level 433.160 m)

11 Conveyance Pump chamber water level 436.590 m

Intake facilities water loss (River water level +437.6m)

1 unit duty

1 River Water Level

L.L.W.L. 437.600 m

2 Intake Flow & Verosity

Q1= 38500 m3/day= 0.446 m3/sec
 Q2= 77000 m3/day= 0.891 m3/sec
 Q3= 115500 m3/day= 1.337 m3/sec

3 Bar Screen Loss

B= 2.00 m (37.5 *44= 1.650 m)
 H= 1.10 m (Bottom Level 436.500 m) Including Sed. Depth h=0.50m
 b= 37.5 mm
 t= 12.5 mm
 θ = 70 °
 V= 0.737 m/s
 H= 0.011 m

Threrfore h1= 0.300 m (WL+ 437.300 m, depth 0.800 m)
 (Bottom Level 436.500 m) settling soil 0.5m

4 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h = v^2 / (2 * g * C^2)$

where A=1.5m*Hm= 1.2 m2 : Sectional area (H= 0.80 m)

Q= 1.337 m3/sec

$v = Q/A = 1.114$ m/sec

g= 9.8 m/sec2

C= 0.6

h4= 0.1759 m = 0.180 m (WL+ 437.120 m, depth 0.620 m)
 (Bottom Level 436.500 m)

5 Rubbish Remover

B= 2.00 m (20 *44= 0.880 m)
 H= 0.62 m (Bottom Level 436.500 m)
 b= 20.0 mm
 t= 3 mm
 θ = 70 °
 V= 2.450 m/s
 H= 0.041 m

Threrfore h2= 0.100 m (WL+ 437.020 m, depth 0.520 m)
 (Bottom Level 436.500 m)

6 Head loss in the channel

Q1= 1.337 m3/sec : Water flow of 1 trough

Inflow sectional area

A=B*H= 1.04 m2

where B= 2.00 m
 H= 0.52 m

Velocity

$V(a-b) = Q1/A = 1.29$ m/sec

Hydraulic radius

$R = A / (B + H * 2) = 0.342$ m

Roughness coefficient

n= 0.015

Head losses are calculated using Manning Formula.

$h = n^2 * L * v^2 / R^{(4/3)}$

where L= 26.0 m

h3= 0.04040 = 0.040 m (WL+ 436.980 m, depth 0.980 m)
 (Bottom Level 436.000 m)

Intake Loss (V.Pump)1unitQ=1.0 1.10gate1.5m

7 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 1.130 m² : Sectional area
 D= 100 mmdia.
 a= 18 pieces
 b= 8 pieces (Sedimentation Level 435.060 m= 434.06 + 1.0)
 Q= 1.337 m³/sec
 $v = Q / A =$ 1.18 m/sec
 g= 9.8 m/sec²
 C= 0.6
 $h_5 =$ 0.198 m = 0.200 m

8 Grit chamber water level 436.780 m

9 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 0.848 m² : Sectional area
 D= 100 mmdia.
 a= 18 pieces
 b= 6 pieces (Bottom Level 434.060 m)
 Q= 1.337 m³/sec
 $v = Q / A =$ 1.58 m/sec
 g= 9.8 m/sec²
 C= 0.6
 $h_5 =$ 0.352 m = 0.360 m (WL+ 436.420 m, depth 2.360 m)
 (Bottom Level 434.060 m)

10 Head loss of Intake gate

Dimension of gate; 1500x1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm * 2 =$ 4.8 m² : Sectional area (H= 1.60 m)
 Q= 1.337 m³/sec
 $v = Q / A =$ 0.279 m/sec
 g= 9.8 m/sec²
 C= 0.6
 $h_6 =$ 0.01099 m = 0.020 m (WL+ 436.400 m, depth 3.240 m)
 (Bottom Level 433.160 m)

11 Conveyance Pump chamber water level 436.400 m

Intake facilities water loss (River water level +437.6m)

1 unit duty

1 River Water Level

L.L.W.L. 437.60 m

2 Intake Flow & Velocity

Q1= 38500 m3/day= 0.446 m3/sec
 Q2= 77000 m3/day= 0.891 m3/sec
 Q3= 115500 m3/day= 1.337 m3/sec

3 Bar Screen Loss

B= 2.00 m (37.5 *44= 1.650 m)
 H= 1.10 m (Bottom Level 436.500 m) Including Sed. Depth h=0.50m
 b= 37.5 mm
 t= 12.5 mm
 θ = 70 °
 V= 0.737 m/s
 H= 0.011 m

Therefore h1= 0.300 m (WL+ 437.300 m, depth 0.800 m)
 (Bottom Level 436.500 m) settling soil 0.5m

4 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm = 1.2 m^2$: Sectional area (H= 0.80 m)

Q= 1.337 m3/sec

$v = Q/A = 1.114 m/sec$

g= 9.8 m/sec²

C= 0.6

$h4 = 0.1759 m = 0.180 m$ (WL+ 437.120 m, depth 0.620 m)
 (Bottom Level 436.500 m)

5 Rubbish Remover

B= 2.00 m (20 *44= 0.880 m)
 H= 0.62 m (Bottom Level 436.500 m)
 b= 20.0 mm
 t= 3 mm
 θ = 70 °
 V= 2.450 m/s
 H= 0.041 m

Therefore h2= 0.100 m (WL+ 437.020 m, depth 0.520 m)
 (Bottom Level 436.500 m)

6 Head loss in the channel

Q1= 1.337 m3/sec : Water flow of 1 trough

Inflow sectional area

$A = B * H = 1.04 m^2$

where B= 2.00 m
 H= 0.52 m

Velocity

$V(a-b) = Q1/A = 1.29 m/sec$

Hydraulic radius

$R = A / (B + H * 2) = 0.342 m$

Roughness coefficient

n= 0.015

Head losses are calculated using Manning Formula.

$h = n^2 * L * v^2 / R^{(4/3)}$

where L= 26.0 m

h3= 0.04040 = 0.040 m (WL+ 436.980 m, depth 0.480 m)
 (Bottom Level 436.500 m)

7 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 0.707 m² : Sectional area
 D= 100 mmdia.
 a= 18 pieces
 b= 5 pieces (Sedimentation Level 436.000 m= 434.06 + 1.94)
 Q= 1.337 m³/sec
 v=Q/A= 1.89 m/sec
 g= 9.8 m/sec²
 C= 0.6
 h5= 0.507 m = 0.510 m

8 Grit chamber water level 436.470 m

9 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 0.707 m² : Sectional area
 D= 100 mmdia.
 a= 18 pieces
 b= 5 pieces (Bottom Level 434.060 m)
 Q= 1.337 m³/sec
 v=Q/A= 1.89 m/sec
 g= 9.8 m/sec²
 C= 0.6
 h5= 0.507 m = 0.510 m (WL+ 435.960 m, depth 1.900 m)
 (Bottom Level 434.060 m)

10 Head loss of Intake gate

Dimension of gate; 1500x1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm^2 =$ 4.8 m² : Sectional area (H= 1.60 m)
 Q= 1.337 m³/sec
 v=Q/A= 0.279 m/sec
 g= 9.8 m/sec²
 C= 0.6
 h6= 0.01099 m = 0.020 m (WL+ 435.940 m, depth 2.780 m)
 (Bottom Level 433.160 m)

11 Conveyance Pump chamber water level 435.940 m

Intake facilities water loss (River water level +438.3m)

1 unit duty

1 River Water Level

L.W.L. 438.300 m

2 Intake Flow & Verosity

Q1= 38500 m3/day= 0.446 m3/sec
 Q2= 77000 m3/day= 0.891 m3/sec
 Q3= 115500 m3/day= 1.337 m3/sec

3 Bar Screen Loss

B= 2.00 m (37.5 *44= 1.650 m)
 H= 1.80 m (Bottom Level 436.500 m) Including Sed. Depth h=0.50m
 b= 37.5 mm
 t= 12.5 mm
 $\theta = 70^\circ$
 V= 0.450 m/s
 H= 0.004 m

Threrfore h1= 0.300 m (WL+ 438.000 m, depth 1.500 m)
 (Bottom Level 436.500 m) settling soil 0.5m

4 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm = 1.65 m^2$: Sectional area (H= 1.10 m)
 $Q = 1.337 m^3/sec$
 $v = Q/A = 0.810 m/sec$
 $g = 9.8 m/sec^2$
 $C = 0.6$
 $h4 = 0.0930 m = 0.100 m$ (WL+ 437.900 m, depth 1.400 m)
 (Bottom Level 436.500 m)

5 Rubbish Remover

B= 2.00 m (20 *44= 0.880 m)
 H= 1.40 m (Bottom Level 436.500 m)
 b= 20.0 mm
 t= 3 mm
 $\theta = 70^\circ$
 V= 1.085 m/s
 H= 0.008 m

Threrfore h2= 0.100 m (WL+ 437.800 m, depth 1.300 m)
 (Bottom Level 436.500 m)

6 Head loss in the channel

Q1= 1.337 m3/sec : Water flow of 1 trough

Inflow sectional area

$A = B * H = 2.60 m^2$
 where B= 2.00 m
 H= 1.30 m

Velocity

$V(a-b) = Q1/A = 0.51 m/sec$

Hydraulic radius

$R = A / (B + H * 2) = 0.565 m$

Roughness coefficient

n= 0.015

Head losses are calculated using Manning Formula.

$h = n^2 * L * v^2 / R^{4/3}$

where L= 26.0 m

h3= 0.00331 = 0.000 m (WL+ 437.800 m, depth 1.300 m)
 (Bottom Level 436.500 m)

7 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 0.989 m² : Sectional area
 D= 100 mmdia.
 a= 18 pieces
 b= 7 pieces (Sedimentation Level 436.000 m= 434.06 + 1.94)
 Q= 1.337 m³/sec
 v=Q/A= 1.35 m/sec
 g= 9.8 m/sec²
 C= 0.6
 h5= 0.259 m = 0.260 m

8 Grit chamber water level 437.540 m

9 Head loss of diffusion wall

Diameter of holes and number of holes; $\phi 100@300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 1.272 m² : Sectional area
 D= 100 mmdia.
 a= 18 pieces
 b= 9 pieces (Bottom Level 434.060 m)
 Q= 1.337 m³/sec
 v=Q/A= 1.05 m/sec
 g= 9.8 m/sec²
 C= 0.6
 h5= 0.157 m = 0.160 m (WL+ 437.380 m, depth 3.320 m)
 (Bottom Level 434.060 m)

10 Head loss of Intake gate

Dimension of gate; 1500x1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm^2 =$ 4.8 m² : Sectional area (H= 1.60 m)
 Q= 1.337 m³/sec
 v=Q/A= 0.279 m/sec
 g= 9.8 m/sec²
 C= 0.6
 h6= 0.01099 m = 0.020 m (WL+ 437.360 m, depth 4.200 m)
 (Bottom Level 433.160 m)

11 Conveyance Pump chamber water level 437.360 m

Intake facilities water loss (River water level +440.74m)

1 unit duty

1 River Water Level

H.W.L. 440.740 m

2 Intake Flow & Verosity

Q1= 38500 m3/day= 0.446 m3/sec
 Q2= 77000 m3/day= 0.891 m3/sec
 Q3= 115500 m3/day= 1.337 m3/sec

3 Head loss of Inlet Orifice

where $A=a*b=$ 11 m² : Sectional area
 $a=$ 6 m
 $b=$ 1.9 m (Sedimentation Level 436.500 m= 436.000 #####)
 $Q=$ 1.337 m3/sec
 $v=Q/A=$ 0.12 m/sec
 $g=$ 9.8 m/sec²
 $C=$ 0.6
 $h_5=$ 0.0019 m = 0.000 m (WL+ 440.740 m, depth 4.240 m)
 (Bottom Level 436.500 m)

4 Bar Screen Loss

$B=$ 2.00 m ($37.5 * 44=$ 1.650 m)
 $H=$ 4.24 m (Bottom Level 436.50 m)
 $b=$ 37.5 mm
 $t=$ 12.5 mm
 $\theta =$ 70 °
 $V=$ 0.191 m/s
 $H=$ 0.001 m

Threrfore $h_1=$ 0.300 m (WL+ 440.440 m, depth 3.940 m)
 (Bottom Level 436.500 m) settling soil 0.5m

5 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h=v^2/(2*g*C^2)$

where $A=1.5m*Hm=$ 1.65 m² : Sectional area (H= 1.10 m)
 $Q=$ 1.337 m3/sec
 $v=Q/A=$ 0.810 m/sec
 $g=$ 9.8 m/sec²
 $C=$ 0.6
 $h_4=$ 0.0930 m = 0.100 m (WL+ 440.340 m, depth 3.840 m)
 (Bottom Level 436.500 m)

6 Rubbish Remover

$B=$ 2.00 m ($20 * 44=$ 0.880 m)
 $H=$ 3.84 m (Bottom Level 436.500 m)
 $b=$ 20.0 mm
 $t=$ 3 mm
 $\theta =$ 70 °
 $V=$ 0.396 m/s
 $H=$ 0.001 m

Threrfore $h_2=$ 0.100 m (WL+ 440.240 m, depth 3.740 m)
 (Bottom Level 436.500 m)

7 Head loss in the channel

$Q_1=$ 1.337 m3/sec : Water flow of 1 trough

Inflow sectional area

$A=B*H=$ 7.48 m²

where $B=$ 2.00 m
 $H=$ 3.74 m

Velocity

$V(a-b)=Q_1/A=$ 0.18 m/sec

Hydraulic radius

$R=A/(B+H*2)=$ 0.789 m

Intake Loss (V.Pump)1unitQ=1.0 1.10gate1.5m

Roughness coefficient
n= 0.015

Head losses are calculated using Manning Formula.

$$h = n^2 * L * v^2 / R^{4/3}$$

where L= 26.0 m

h3= 0.00026 = 0.000 m (WL+ 440.240 m, depth 3.740 m)
(Bottom Level 436.500 m)

8 Head loss of diffusion wall

Diameter of holes and number of holes; ϕ 100@300×300

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 2.120 m² : Sectional area

D= 100 mmdia.

a= 18 pieces

b= 15 pieces (Sedimentation Level 436.000 m= 434.06 + 1.94)

Q= 1.337 m³/sec

v=Q/A= 0.63 m/sec

g= 9.8 m/sec²

C= 0.6

h5= 0.056 m = 0.060 m

9 Grit chamber water level 440.180 m

10 Head loss of diffusion wall

Diameter of holes and number of holes; ϕ 100@300×300

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) =$ 2.543 m² : Sectional area

D= 100 mmdia.

a= 18 pieces

b= 18 pieces (Bottom Level 434.060 m)

Q= 1.337 m³/sec

v=Q/A= 0.53 m/sec

g= 9.8 m/sec²

C= 0.6

h5= 0.039 m = 0.040 m (WL+ 440.140 m, depth 6.080 m)
(Bottom Level 434.060 m)

11 Head loss of Intake gate

Dimension of gate; 1500×1500

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 1.5m * Hm * 2 =$ 4.8 m² : Sectional area (H= 1.60 m)

Q= 1.337 m³/sec

v=Q/A= 0.279 m/sec

g= 9.8 m/sec²

C= 0.6

h6= 0.01099 m = 0.020 m (WL+ 440.120 m, depth 6.960 m)
(Bottom Level 433.160 m)

12 Conveyance Pump chamber water level 440.120 m

Hydrodynamic Pressure of Conveyance Pipe Route

Q=1.0Q

1.Phase 1

St.No.	S.D. (m)	A.D. (m)	G.L. (m)	Pipe Dia. (mm)	H.G.	W.L.L. (m)	W.L. (m)	Min.soil Coverage of Pipe (m)	A.D. of L.S. (m)	Remark
Balancing Tank			(HWL+476.00)							Balancing Tank
28-22.00	0.00	0.00	475.00	1000	0.00048	0.000	475.99	-0.99	537.14	Loss etc. 0.008 m
28+0.00	22.00	22.00	472.69	1000	0.00048	0.011	475.98	-3.29	559.14	
30+0.00	41.67	63.67	472.60	1000	0.00048	0.020	475.96	-3.56	600.81	
41+0.00	179.50	243.17	475.42	1000	0.00048	0.086	475.88	-0.46	780.31	
50+0.00	118.52	361.69	477.60	1000	0.00048	0.057	475.82	1.78	898.83	
51+0.00	41.00	402.69	477.48	1000	0.00048	0.020	475.80	1.68	939.83	
53+7.00	45.80	448.49	475.26	1000	0.00048	0.022	475.78	-0.52	985.63	
67+0.00	273.32	721.81	468.09	800	0.00141	0.385	475.39	-7.30	1258.95	
76+0.00	67.50	789.31	455.62	800	0.00141	0.095	475.30	-19.68	1326.45	Valve Loss etc. 11.07067 m
86+0.00	95.40	884.71	461.15	800	0.00141	0.135	475.16	-14.01	1421.85	
105+0.00	186.60	1071.31	446.50	800	0.00141	0.263	474.90	-28.40	1608.45	
105+85.00	91.00	1162.31	(HWL+451.82) 446.50	800	0.00141	0.128	463.70	-11.88	1696.45	Distribution Chamber Horizontal Pipe distance 3 m Valve Loss etc. 11.07067 m

23.371

2.Phase 2

St.No.	S.D. (m)	A.D. (m)	G.L. (m)	Pipe Dia. (mm)	H.G.	W.L.L. (m)	W.L. (m)	Min.soil Coverage of Pipe (m)	A.D. of L.S. (m)	Remark
Balancing Tank			(HWL+476.00)							Balancing Tank
28-22.00	0.00	0.00	475.00	1000	0.00172	0.000	476.00	-1.00	537.14	Loss etc. 0.053 m
28+0.00	22.00	22.00	472.69	1000	0.00172	0.038	475.96	-3.27	559.14	
30+0.00	41.67	63.67	472.60	1000	0.00172	0.072	475.89	-3.29	600.81	
41+0.00	179.50	243.17	475.42	1000	0.00172	0.309	475.58	-0.16	780.31	
50+0.00	118.52	361.69	477.60	1000	0.00172	0.204	475.38	2.22	898.83	
51+0.00	41.00	402.69	477.48	1000	0.00172	0.071	475.31	2.17	939.83	
53+7.00	45.80	448.49	475.26	1000	0.00172	0.079	475.23	0.05	985.63	
67+0.00	273.32	721.81	468.09	800	0.00510	1.394	473.83	-5.74	1258.95	
76+0.00	67.50	789.31	455.62	800	0.00510	0.344	466.22	-10.60	1326.45	Valve Loss etc. 7.274753 m
86+0.00	95.40	884.71	461.15	800	0.00510	0.487	465.73	-4.58	1421.85	
105+0.00	186.60	1071.31	446.50	800	0.00510	0.952	464.78	-18.28	1608.45	
105+85.00	91.00	1162.31	(HWL+451.82) 446.50	800	0.00510	0.464	451.72	0.10	1696.45	Distribution Chamber Horizontal Pipe distance 3 m Valve Loss etc. 12.59775 m

24.317

3.Phase 3

St.No.	S.D. (m)	A.D. (m)	G.L. (m)	Pipe Dia. (mm)	H.G.	W.L.L. (m)	W.L. (m)	Min.soil Coverage of Pipe (m)	A.D. of L.S. (m)	Remark
Balancing Tank			(HWL+476.00)							Balancing Tank
28-22.00	0.00	0.00	475.00	1000	0.00364	0.000	475.93	-0.93	537.14	Loss etc. 0.074 m
28+0.00	22.00	22.00	472.69	1000	0.00364	0.080	475.85	-3.16	559.14	
30+0.00	41.67	63.67	472.60	1000	0.00364	0.152	475.69	-3.09	600.81	
41+0.00	179.50	243.17	475.42	1000	0.00364	0.653	475.04	0.38	780.31	
50+0.00	118.52	361.69	477.60	1000	0.00364	0.431	474.61	2.99	898.83	
51+0.00	41.00	402.69	477.48	1000	0.00364	0.149	474.46	3.02	939.83	
53+7.00	45.80	448.49	475.26	1000	0.00364	0.167	474.29	0.92	985.63	
67+0.00	273.32	721.81	468.09	800	0.01079	2.949	471.34	-3.25	1258.95	
76+0.00	67.50	789.31	455.62	800	0.01079	0.728	467.48	-11.86	1326.45	Valve Loss etc. 3.132 m
86+0.00	95.40	884.71	461.15	800	0.01079	1.029	466.45	-5.30	1421.85	
105+0.00	186.60	1071.31	446.50	800	0.01079	2.013	464.44	-17.94	1608.45	
105+85.00	91.00	1162.31	(HWL+451.82) 446.50	800	0.01079	0.982	451.68	0.14	1696.45	Distribution Chamber Horizontal Pipe distance 3 m Valve Loss etc. 11.77611 m

23.497

Phase1 Q1= 38500 m3/d = 0.446 m3/s (110000*1.05*(1/3))
 Phase2 Q2= 77000 m3/d = 0.891 m3/s (110000*1.05*(2/3))
 Phase3 Q3= 115500 m3/d = 1.337 m3/s (110000*1.05)

Pipe Friction Factor

c= 100

Note

- St.No. : Station Number
- S.D. : Single Distance
- A.D. : Accumulated Distance
- G.L. : Ground Level
- H.G. : Hydraulic Gradient
- W.L.L. : Water Level Loss
- H.W.L. : Hydraulic Water Level
- H.P. : Hydrodynamic Pressure
- A.D. of L.S. : Accumulate Distance of Longitudinal Section

Water Treatment Inlet valve cavitation Incaise of using butterfly valve)

Q=1.0

1.Total flow

Phase1	Q1=	38500 m3/d =	1604 m3/h	(110000*1.05*(1/3))
Phase2	Q2=	77000 m3/d =	3208 m3/h	(110000*1.05*(2/3))
Phase3	Q3=	115500 m3/d =	4813 m3/h	(110000*1.05)

2.Water level

Balancing tank HWL	476.000 m
Balancing tank LWL	474.980 m
Inlet water level of Distribution Chamber	451.680 m
Valve No.2 center level	454.199 m (455.62-1.0-0.842/2)
Valve No.3 level	445.079 m (446.5-1.0-0.842/2)

3.Valve Diameter and flow velocity

Valve Diameter (mm)	Flow velocity (m/sec)		
	Phase1	Phase2	Phase3
300	6.31	12.61	18.92
350	4.63	9.27	13.90
400	3.55	7.10	10.64
500	2.27	4.54	6.81
600	1.58	3.15	4.73
700	1.16	2.32	3.48
800	0.89	1.77	2.66

4.Phase3

Inlet Loss	(Diameter 1000 mm), f= 0.5	V(Q3)= 1.70 m/s	h= 0.074 m	Subtotal 0.074 m
Reducer Loss	(Diameter 800 600 mm), f= 0	V(Q3)= 2.66 m/s	h= 0.000 m	Subtotal
Valve 1 Loss	(Diameter 600 mm), f= 2.58 (60°)	V(Q3)= 4.73 m/s	h= 2.945 m	3.132 m
Orifice 1 Loss	(Diameter 600 mm), f= 0	a/A=1	V(Q3)= 4.73 m/s	h= 0.000 m
Reducer Loss	(Diameter 800 600 mm), f= 0.5	V(Q3)= 2.66 m/s	h= 0.187 m	
Reducer Loss	(Diameter 800 600 mm), f= 0	V(Q3)= 2.66 m/s	h= 0.000 m	Subtotal
Valve 2 Loss	(Diameter 600 mm), f= 5.6 (53°)	V(Q3)= 4.73 m/s	h= 6.392 m	11.776 m
Orifice 2 Loss	(Diameter 600 mm), f= 4.24	a/A=0.70	V(Q3)= 4.73 m/s	h= 4.836 m
Reducer Loss	(Diameter 800 600 mm), f= 0.5	V(Q3)= 2.66 m/s	h= 0.187 m	
Outlet Loss	(Diameter 800 mm), f= 1.0	V(Q3)= 2.66 m/s	h= 0.361 m	
Pipe Friction Loss	(Diameter 1000 mm), I= 0.00364	L= 448.49 m	h= 1.633 m	Subtotal
Pipe Friction Loss	(Diameter 800 mm), I= 0.01079	L= 340.82 m	h= 3.677 m	9.334 m
Pipe Friction Loss	(Diameter 800 mm), I= 0.01079	L= 313.00 m	h= 3.377 m	
Pipe Friction Loss	(Diameter 800 mm), I= 0.01079	L= 60.00 m	h= 0.647 m	
Total	h= 24.316 m			

where c= 100
Q3= 115500 m3/d= 1.337 m3/sec

1 Cavitation coefficient and opening degree of valve No.1

Cavitation coefficient

$\rho = (H2+10)/(H1-H2)$
where H1= 16.417 m :Hydrostatic head of upstream of valve
H2= 13.471 m :Hydrostatic head of downstream of valve
 $\Delta H = H1-H2 = 2.95$ m :Head loss of valve

$\rho = (H2+10)/(H1-H2) = 7.97 (>2.5-3.0)$ No Cavitation OK

Capacity coefficient (Cv)

$Cv = 1.167 * Q3 * (G / \Delta P)^{0.5}$
where Q3= 4813 m3/h (110000*1.05/24)
G= 10.0 m3/m2 (1kg/cm2)
 $\Delta P = 3$ m3/m2 :H1-H2= 2.95 m

$Cv = 1.167 * Q3 * (G / \Delta P)^{0.5} = 10347$

Opening degree of valve

$\theta = 60^\circ$

2 Orifice No.1 (No need Orifice)

$\rho = (H2+10)/(H1-H2+(V^2/2/g))$
 where H1= 13.472 m :Hydrostatic head of upstream of valve
 H2= 13.471 m :Hydrostatic head of downstream of valve
 $\Delta H=H1-H2=$ 0.001 m :Head loss of valve

3 Cavitation coefficient and opening degree of valve No.2 (600mm)

Cavitation coefficient
 $\rho = (H2+10)/(H1-H2)$
 where H1= 19.028 m :Hydrostatic head of upstream of valve
 H2= 12.635 m :Hydrostatic head of downstream of valve
 $\Delta H=H1-H2=$ 6.39 m :Head loss of valve
 $\rho = (H2+10)/(H1-H2)=$ 3.54 (>2.5-3.0) No Cavitation OK

Capacity coefficient (Cv)
 $Cv=1.167*Q3*(G/\Delta P)^{0.5}$
 where Q3= 4813 m3/h (110000*1.05/24)
 G= 10.0 m3/m2 (1kg/cm2)
 $\Delta P=$ 6.39 m3/m2 :H1-H2= 6.39 m
 $Cv=1.167*Q3*(G/\Delta P)^{0.5}=$ 7024

Opening degree of valve
 $\theta=$ 53°

4 Orifice No.2

$\rho = (H2+10)/(H1-H2+(V^2/2/g))$
 where H1= 12.636 m :Hydrostatic head of upstream of valve
 H2= 7.799 m :Hydrostatic head of downstream of valve
 $\Delta H=H1-H2=$ 4.84 m :Head loss of valve

Distribution Chamber water level 451.683 m (476.000 - 24.317) >451.680 m

5.Phase2

Inlet Loss	(Diameter 1000 mm), f=	0.5	V(Q3)=	1.14 m/s	h=	0.033 m	Subtotal	0.033 m
Reducer Loss	(Diameter 800 600 mm), f=	0	V(Q3)=	1.77 m/s	h=	0.000 m	Subtotal	7.275 m
Valve 1 Loss	(Diameter 600 mm), f= 2.8 (59°)		V(Q3)=	3.15 m/s	h=	1.418 m		
Orifice 1 Loss	(Diameter 600 mm), f=	11.40	a/A=0.6	V(Q3)=	3.15 m/s	h=	5.774 m	
Reducer Loss	(Diameter 800 600 mm), f=	0.5	V(Q3)=	1.77 m/s	h=	0.083 m		
Reducer Loss	(Diameter 800 600 mm), f=	0	V(Q3)=	1.77 m/s	h=	0.000 m	Subtotal	12.598 m
Valve 2 Loss	(Diameter 600 mm), f= 13 (31°)		V(Q3)=	3.15 m/s	h=	6.581 m		
Orifice 2 Loss	(Diameter 600 mm), f=	11.40	a/A=0.6	V(Q3)=	3.15 m/s	h=	5.774 m	
Reducer Loss	(Diameter 800 600 mm), f=	0.5	V(Q3)=	1.77 m/s	h=	0.083 m		
Outlet Loss	(Diameter 800 mm), f=	1.0	V(Q3)=	1.77 m/s	h=	0.160 m		
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00172	L=	448.49 m	h=	0.771 m	Subtotal	4.411 m
Pipe Friction Loss	(Diameter 800 mm), I=	0.0051	L=	340.82 m	h=	1.738 m		
Pipe Friction Loss	(Diameter 800 mm), I=	0.0051	L=	313.00 m	h=	1.596 m		
Pipe Friction Loss	(Diameter 800 mm), I=	0.0051	L=	60.00 m	h=	0.306 m		
Total	h=	24.317 m						

where c= 100
 Q2= 77000 m3/d= 0.891 m3/sec

1 Cavitation coefficient and opening degree of valve No.1

Cavitation coefficient
 $\rho = (H2+10)/(H1-H2)$
 where H1= 19.259 m :Hydrostatic head of upstream of valve
 H2= 17.841 m :Hydrostatic head of downstream of valve
 $\Delta H=H1-H2=$ 1.42 m :Head loss of valve
 $\rho = (H2+10)/(H1-H2)=$ 19.63 (>2.5-3.0) No Cavitation OK

Capacity coefficient (Cv)
 $Cv=1.167*Q3*(G/\Delta P)^{0.5}$
 where Q2= 3208 m3/h (110000*1.05*(2/3)/24)
 G= 10.0 m3/m2 (1kg/cm2)
 $\Delta P=$ 1 m3/m2 :H1-H2= 1.42 m
 $Cv=1.167*Q3*(G/\Delta P)^{0.5}=$ 9941

Opening degree of valve
 $\theta=$ 59°

2 Orifice No.1

$\rho = (H2+10)/(H1-H2+(V^2/2/g))$

where H1= 17.841 m :Hydrostatic head of upstream of valve
H2= 12.067 m :Hydrostatic head of downstream of valve
 $\Delta H=H1-H2=$ 5.77 m :Head loss of valve

3 Cavitation coefficient and opening degree of valve No.2 (600mm)

Cavitation coefficient

$\rho = (H2+10)/(H1-H2)$
where H1= 19.508 m :Hydrostatic head of upstream of valve
H2= 12.927 m :Hydrostatic head of downstream of valve
 $\Delta H=H1-H2=$ 6.58 m :Head loss of valve
 $\rho = (H2+10)/(H1-H2)=$ 3.48 (>2.5-3.0) No Cavitation OK

Capacity coefficient (Cv)

$Cv=1.167*Q3*(G/\Delta P)^{0.5}$
where Q2= 3208 m3/h (110000*1.05*(2/3)/24)
G= 10.0 m3/m2 (1kg/cm2)
 $\Delta P=$ 6.58 m3/m2 :H1-H2= 6.58 m
 $Cv=1.167*Q3*(G/\Delta P)^{0.5}=$ 4615

Opening degree of valve

$\theta=$ 31°

4 Orifice No.2

$\rho = (H2+10)/(H1-H2+(V^2/2g))$
where H1= 12.927 m :Hydrostatic head of upstream of valve
H2= 7.153 m :Hydrostatic head of downstream of valve
 $\Delta H=H1-H2=$ 5.77 m :Head loss of valve

Distribution Chamber water level 451.683 m (476.000 - 24.317) >451.680 m

6.Phase1

Inlet Loss	(Diameter 1000 mm), f=	0.5	V(Q3)=	0.57 m/s	h=	0.008 m	Subtotal	0.008 m
Reducer Loss	(Diameter 800 600 mm), f=	0	V(Q3)=	0.89 m/s	h=	0.000 m	Subtotal	0.000 m
Valve 1 Loss	(Diameter 600 mm), f=	7 (49°)	V(Q3)=	1.58 m/s	h=	0.892 m	Subtotal	12.009 m
Orifice 1 Loss	(Diameter 600 mm), f=	87.12	a/A=0.4	V(Q3)=	1.58 m/s	h=	11.096 m	
Reducer Loss	(Diameter 800 600 mm), f=	0.5	V(Q3)=	0.89 m/s	h=	0.021 m	Subtotal	0.021 m
Reducer Loss	(Diameter 800 600 mm), f=	0	V(Q3)=	0.89 m/s	h=	0.000 m	Subtotal	0.000 m
Valve 2 Loss	(Diameter 600 mm), f=	8.6 (47°)	V(Q3)=	1.58 m/s	h=	1.095 m	Subtotal	11.071 m
Orifice 2 Loss	(Diameter 600 mm), f=	77.84	a/A=0.41	V(Q3)=	1.58 m/s	h=	9.915 m	
Reducer Loss	(Diameter 800 600 mm), f=	0.5	V(Q3)=	0.89 m/s	h=	0.021 m	Subtotal	0.021 m
Outlet Loss	(Diameter 800 mm), f=	1.0	V(Q3)=	0.89 m/s	h=	0.040 m	Subtotal	0.040 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00048	L=	448.49 m	h=	0.215 m	Subtotal	0.215 m
Pipe Friction Loss	(Diameter 800 mm), I=	0.00141	L=	340.82 m	h=	0.481 m	Subtotal	1.222 m
Pipe Friction Loss	(Diameter 800 mm), I=	0.00141	L=	313.00 m	h=	0.441 m	Subtotal	0.441 m
Pipe Friction Loss	(Diameter 800 mm), I=	0.00141	L=	60.00 m	h=	0.085 m	Subtotal	0.085 m
Total	h=	24.309 m						

where c= 100
Q2= 38500 m3/d= 0.446 m3/sec

1 Cavitation coefficient and opening degree of valve No.1 (600mm)

Cavitation coefficient

$\rho = (H2+10)/(H1-H2)$
where H1= 21.097 m :Hydrostatic head of upstream of valve
H2= 20.204 m :Hydrostatic head of downstream of valve
 $\Delta H=H1-H2=$ 0.89 m :Head loss of valve
 $\rho = (H2+10)/(H1-H2)=$ 33.84 (>2.5-3.0) No Cavitation OK

Capacity coefficient (Cv)

$Cv=1.167*Q3*(G/\Delta P)^{0.5}$
where Q1= 1604 m3/h (110000*1.05*(1/3)/24)
G= 10.0 m3/m2 (1kg/cm2)
 $\Delta P=$ 0.89 m3/m2 :H1-H2= 0.89 m
 $Cv=1.167*Q3*(G/\Delta P)^{0.5}=$ 6266

Opening degree of valve

$\theta=$ 49°

2 Orifice No.1

$\rho = (H2+10)/(H1-H2+(V^2/2g))$
where H1= 20.205 m :Hydrostatic head of upstream of valve
H2= 9.109 m :Hydrostatic head of downstream of valve

$$\Delta H = H_1 - H_2 = 11.10 \text{ m} \quad \text{:Head loss of valve}$$

3 Cavitation coefficient and opening degree of valve No.2 (600mm)

Cavitation coefficient

$$\rho = (H_2 + 10) / (H_1 - H_2)$$

where $H_1 = 17.767 \text{ m}$:Hydrostatic head of upstream of valve
 $H_2 = 16.672 \text{ m}$:Hydrostatic head of downstream of valve
 $\Delta H = H_1 - H_2 = 1.10 \text{ m}$:Head loss of valve

$$\rho = (H_2 + 10) / (H_1 - H_2) = 24.34 (>2.5-3.0) \quad \text{No Cavitation OK}$$

Capacity coefficient (Cv)

$$C_v = 1.167 * Q^3 * (G / \Delta P)^{0.5}$$

where $Q = 1604 \text{ m}^3/\text{h}$ (110000 * 1.05 * (1/3) / 24)
 $G = 9.102 \text{ m}^3/\text{m}^2$ (1kg/cm²)
 $\Delta P = 1.10 \text{ m}^3/\text{m}^2$:H1-H2= 1.10 m

$$C_v = 1.167 * Q^3 * (G / \Delta P)^{0.5} = 5396$$

Opening degree of valve

$$\theta = 47^\circ$$

4 Orifice No.2

$$\rho = (H_2 + 10) / (H_1 - H_2 + (V^2 / 2g))$$

where $H_1 = 16.672 \text{ m}$:Hydrostatic head of upstream of valve
 $H_2 = 6.757 \text{ m}$:Hydrostatic head of downstream of valve
 $\Delta H = H_1 - H_2 = 9.92 \text{ m}$:Head loss of valve

$$\text{Distribution Chamber water level} \quad 451.690 \text{ m} \quad (476.000 - 24.310) \quad >451.680 \text{ m}$$

Pressure Dissipation with orifice and cavitations coefficient
Cavitations

Phase 3

Q3= 115500 m3/d= 1.337 m3/s

Proposed Orifice No.2 Diameter

Orifice Dia. d (mm)	Pipe Dia. D (mm)	Coefficient d/D	Flow velocity in Pipe V (m/s)	Flow velocity in Orifice V (m/s)	$\beta=(d/D)^2$	α	a	Δh_o	k	$\Delta \omega = \Delta h_o * k$	ξ_o	σ_c
420	600	0.7	4.73	9.65	0.4900	0.6953	0.13847	9.83	0.4917	4.836	4.24	2.31

H1	H2	V ² /(2*g)	Cavitation Coefficient	
			K0	K0 (without V ² /(2*g))
12.636	7.799	1.142	2.98	3.68

$\sigma_c \leq K_0$ OK

Phase 2

Q2= 77000 m3/d= 0.891 m3/s

Proposed Orifice No.1 & No.2 Diameter

Orifice Dia. d (mm)	Pipe Dia. D (mm)	Coefficient d/D	Flow velocity in Pipe V (m/s)	Flow velocity in Orifice V (m/s)	$\beta=(d/D)^2$	α	a	Δh_o	k	$\Delta \omega = \Delta h_o * k$	ξ_o	σ_c
360	600	0.6	3.15	8.76	0.3600	0.6490	0.10174	9.29	0.6212	5.774	11.38	1.98
360	600	0.6	3.15	8.76	0.3600	0.6490	0.10174	9.29	0.6212	5.774	11.38	1.98

H1	H2	V ² /(2*g)	Cavitation Coefficient	
			K0	K0 (without V ² /(2*g))
17.841	12.067	0.507	3.51	3.82
12.927	7.153	0.507	2.73	2.97

$\sigma_c \leq K_0$ OK

Phase 1

Q1= 38500 m3/d= 0.446 m3/s

Proposed Orifice No.1 & No.2 Diameter

Orifice Dia. d (mm)	Pipe Dia. D (mm)	Coefficient d/D	Flow velocity in Pipe V (m/s)	Flow velocity in Orifice V (m/s)	$\beta=(d/D)^2$	α	a	Δh_o	k	$\Delta \omega = \Delta h_o * k$	ξ_o	σ_c
240	600	0.4	1.58	9.85	0.1600	0.6063	0.04522	13.48	0.8231	11.096	87.47	1.32
246	600	0.41	1.58	9.38	0.1681	0.6074	0.04751	12.17	0.8147	9.915	78.16	1.35

水理条件キャビテーション係数

H1	H2	V ² /(2*g)	K ₀	V ² /(2*g) 含まず
20.205	9.109	0.127	1.70	1.72
16.672	6.757	0.127	1.67	1.69

$\sigma_c \leq K_0$ OK

$\sigma_c \leq K_0$ OK

14. Balancing Tank Inlet Weir

1 Inlet weir loss

$$h = (Q / (1.84 * b))^{2/3}$$

where $Q = 1.337 \text{ m}^3/\text{sec} \quad (110000 * 1.05 / 86400)$

$b = 6.10 \text{ m}$

$$h = (Q / (1.84 * b))^{2/3} = 0.242 \text{ m}$$

4 Water loss

The water level of inlet channel is 476.540 m (0.242)

The height of the inlet weir is 476.300 m

The water level at the Balancing tank is 476.000 m (Weir top level - 0.30 m)

17. Hydraulic Calculation of Overflow from Balancing Tank

Phase3

Overflow water level is 476.980 m (476.7000 + 0.276)
 Overflow weir top level is 476.7000
 Overflow weir loss is 0.276
 Overflow Pipe Center Level at Blowoff Point 458.000 m

1 Overflow weir loss

$$h = (Q / (1.84 * b))^{2/3}$$

where Q = 1.337 m³/sec (110000 * 1.05 / 86400)
 b = 5 m (2.5 * 2)
 $h = (Q / (1.84 * b))^{2/3} = 0.276$ m

The water level at the downstream of the weir is 476.400 m in consideration of an allowance of 0.300 m.

1 Overflow pipe loss

Inlet Loss	(Diameter 600 mm), f=	0.5	V=	4.73 m/s	h=	0.571 m
22.5°Bend Loss	(Diameter 600 mm), f=	0.15	V=	4.73 m/s	h=	0.171 m
22.5°Bend Loss	(Diameter 600 mm), f=	0.15	V=	4.73 m/s	h=	0.171 m
45°Bend Loss	(Diameter 600 mm), f=	0.21	V=	4.73 m/s	h=	0.242 m
22.5°Bend Loss	(Diameter 600 mm), f=	0.15	V=	4.73 m/s	h=	0.171 m
22.5°Bend Loss	(Diameter 600 mm), f=	0.15	V=	4.73 m/s	h=	0.171 m
45°Bend Loss	(Diameter 600 mm), f=	0.21	V=	4.73 m/s	h=	0.242 m
90°Bend Loss	(Diameter 600 mm), f=	0.20	V=	4.73 m/s	h=	0.228 m
Outlet Loss	(Diameter 600 mm), f=	1.0	V=	4.73 m/s	h=	1.142 m
Pipe Friction Loss	(Diameter 600 mm), L=	0.03673	L=	59.20 m	h=	2.174 m
Total					h=	5.283 m

where Q = 1.337 m³/sec (110000 * 1.05 / 86400)
 C = 110

The water level at the Blow off site is 471.110 m (476.400 - 5.290) > 458.0000

Outside Stream Bottom Level

No.	Distance (m)	Accumulate Distance (m)	Bottom Gradient (‰)	Bottom Level Diferance (m)	Proposed Channel Bottom Level (m)	Ground Level (m)	Existing Bottom Level (m)	Existing Bottom Gradient (‰)	Depth (m)	Average Depth (m)
1					457.600	458.50	458.00		0.90	
2	20	20	3.65	0.073	457.527	459.00	457.75	12.5	1.47	23.7
3	20	40	3.65	0.073	457.100	458.00	457.50	12.5	0.90	23.7
4	20	60	3.65	0.073	455.100	456.00	455.50	100.0	0.90	18.0
5	20	80	3.65	0.073	453.600	454.50	454.00	75.0	0.90	18.0
6	20	100	3.65	0.073	452.100	453.00	452.50	75.0	0.90	18.0
7	20	120	3.65	0.073	452.027	453.00	452.50	0.0	0.97	18.7
8	20	140	3.65	0.073	449.100	450.00	449.50	150.0	0.90	18.7
9	20	160	3.65	0.073	449.400	450.30	449.40	5.0	0.90	18.0
10	20	180	3.65	0.073	448.900	449.80	449.30	5.0	0.90	18.0
11	20	200	3.65	0.073	448.400	449.30	448.80	25.0	0.90	18.0
12	20	220	3.65	0.073	448.100	449.00	448.50	15.0	0.90	18.0
13	20	240	3.65	0.073	446.100	447.00	446.25	112.5	0.90	18.0
14	20	260	3.65	0.073	446.100	447.00	446.23	1.0	0.90	18.0
15	20	280	3.65	0.073	445.800	446.70	446.20	1.5	0.90	18.0
16	20	300	3.65	0.073	444.700	445.60	445.10	55.0	0.90	18.0
17	20	320	3.65	0.073	444.300	445.20	444.70	20.0	0.90	18.0
17+5000	5	325	3.65	0.01825	441.500	444.50	444.00	140.0	3.00	9.7
18	15	340	3.65	0.05475	441.445	446.00	443.90	6.7	4.55	56.7
19	20	360	3.65	0.073	441.372	446.00	443.70	10.0	4.63	91.8
20	20	380	3.65	0.073	441.299	444.00	443.50	10.0	2.70	73.3
21	20	400	3.65	0.073	441.226	444.90	443.50	0.0	2.77	54.7
22	20	420	3.65	0.073	441.153	443.00	442.50	50.0	1.85	46.2
23	20	440	3.65	0.073	441.080	443.00	442.50	0.0	1.92	37.7
24	22	462	3.65	0.0803	441.000	442.00	441.50	45.5	1.00	32.1
Average										1.522

Note : 1.Existing Bottom Level are assumed above mentioned formula.
 Existing Bottom Level = Existing Ground Level - 0.5m
 Proposed Channel Bottom Level = (Existing Ground Level - 0.9m) >= Bottom Level Diferance (No.1 - 17+5000)

1.Receiving well

1 Receiving well inlet channel water level (6 units) 451.680 m

1 Baffle wall loss

$$Q = 1.375 \text{ m}^3/\text{sec} = 118800 \text{ m}^3/\text{day} (110000 * (1.05 + 0.03))$$

$$h = v^2 / (2 * g * c^2)$$

where $A = 1.88 \text{ m}^2$: Opening area $3.14/4 * 0.1^2 * (15 * 16)$

$$v = 0.73 \text{ m/sec}$$

$$g = 9.8 \text{ m/sec}^2$$

$$c = 0.6$$

Baffle wall loss

$$h = v^2 / (2 * g * c^2) = 0.075 \text{ m}$$

2 Receiving well water level 451.600 m

1 Overflow weir loss (6 line duty)

$$h = (Q / (1.84 * B))^{2/3}$$

where $Q = 0.229 \text{ m}^3/\text{sec} = 19800 \text{ m}^3/\text{day} (110000 * (1.05 + 0.03) / 6)$

$$B = 2.0 \text{ m}$$

Overflow weir loss

$$h = (Q / (1.84 * B))^{2/3} = 0.157$$

The height of the overflow weir is accordingly 451.440 m (451.600 - 0.160).

2. Mixing Well

1 Design G Value

a) Camp's Proposition

GT Value

$$GT \text{ Value} = 23,000 \sim 25,000$$

$$G = (23,000 \sim 25,000) / (40 \sim 100) = 230 \sim 625 \text{ sec}^{-1}$$

b) Dr. Tanpo

$$G = (1000 / \text{verg})^{0.5}$$

where

$$\text{verg} = 0.00898 \text{ cm}^2/\text{sec at } 25^\circ\text{C}$$

$$G = 334 \text{ sec}^{-1}$$

c) Japanese Standard

$$G = (g \cdot h / (v \cdot T))^{0.5}$$

where

$$h = 0.50 \sim 0.60 \text{ m} \quad : \text{Head loss at cone}$$

$$g = 9.8 \text{ m/s}^2$$

$$v = 0.00898 \text{ cm}^2/\text{sec}$$

$$T = 60 \text{ sec}$$

$$G = (g \cdot h / (v \cdot T))^{0.5} = 302 \sim 330 \text{ sec}^{-1}$$

Therefore, design G Value is 330 sec⁻¹.

2 Required Head loss for mixing chamber

$$h = G^2 \cdot \mu \cdot V / (\rho \cdot Q \cdot g)$$

$$G = 330 \text{ sec}^{-1} \quad : \text{Design G value}$$

$$\mu = 0.000898 \text{ kg/m} \cdot \text{sec} \quad : \text{Coefficient of viscosity of water at } 25^\circ\text{C}$$

$$\rho = 0.9971 \text{ g/cm}^3 \text{ at } 25^\circ\text{C}$$

$$g = 980 \text{ cm/sec}^2$$

$$V = 25500000 \text{ cm}^3 = 26 \text{ m}^3 \quad : \text{Volume of mixing chamber}$$

$$(2.50 \text{ m} \cdot 3.00 \text{ m} \cdot 3.40 \text{ m}) \text{ Retention time} \quad 2 \text{ minute}$$

$$Q = 459000 \text{ cm}^3/\text{sec} = 39655 \text{ m}^3/\text{d} \quad : \text{Design flow rate}$$

$$h = G^2 \cdot \mu \cdot V / (\rho \cdot Q \cdot g) = 55.60 \text{ cm} = 60 \text{ cm}$$

3 Overflow weir loss (6 line duty)

$$h = (Q / (1.84 \cdot b))^{2/3}$$

$$\text{where } Q = 0.229 \text{ m}^3/\text{sec} \quad (110000 \cdot (1.05 + 0.03) / 6 / 86400)$$

$$b = 2.00 \text{ m}$$

$$h = (Q / (1.84 \cdot b))^{2/3} = 0.157 \text{ m}$$

4 Water loss

The water level of Receiving well is 451.600 m

The water loss of upstream of the weir is 0.160 m (0.157)

The water loss of downstream of the weir is 0.940 m.

Therefore the water loss (total) is 1.100 m

The height of the overflow weir is accordingly 451.440 m (451.600 - 0.160)

The water level at the downstream of the weir (mixing chamber) is 450.500 m

3.Connection Pipe between Mixing chamber and Flocculation basin

1.Connection Pipe between Mixing chamber and Flocculation basin N0.1

Mixing chamber water level					450.470 m
Outlet pipe loss					
Inlet Loss	(Diameter 700 mm), f=	0.5	V=	0.60 m/s	h= 0.009 m
Valve Loss	(Diameter 700 mm), f=	0.1	V=	0.60 m/s	h= 0.002 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h= 0.005 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h= 0.005 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h= 0.004 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h= 0.004 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h= 0.004 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h= 0.005 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h= 0.005 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h= 0.005 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h= 0.005 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h= 0.004 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h= 0.004 m
Outlet Loss	(Diameter 700 mm), f=	1.0	V=	0.60 m/s	h= 0.018 m
Pipe Friction Loss	(Diameter 700 mm), I=	0.00066	L=	64.96 m	h= 0.043 m
	Total	h=			0.122 m
where	C=	110			
	Q=	19800 m ³ /d=	0.229 m ³ /sec	(110000*(1.05+0.03)/6)	

The Inlet chamber water level of Flocculation basin is 450.340 m (450.470 -0.130)

2.Connection Pipe between Mixing chamber and Flocculation basin N0.3

Mixing chamber water level					450.480 m
Outlet pipe loss					
Inlet Loss	(Diameter 700 mm), f=	0.5	V=	0.60 m/s	h= 0.009 m
Valve Loss	(Diameter 700 mm), f=	0.1	V=	0.60 m/s	h= 0.002 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h= 0.005 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h= 0.004 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h= 0.004 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h= 0.004 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h= 0.005 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h= 0.005 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h= 0.005 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h= 0.005 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h= 0.004 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h= 0.004 m
Outlet Loss	(Diameter 700 mm), f=	1.0	V=	0.60 m/s	h= 0.018 m
Pipe Friction Loss	(Diameter 700 mm), I=	0.00066	L=	94.26 m	h= 0.062 m
	Total	h=			0.136 m
where	C=	110			
	Q=	19800 m ³ /d=	0.229 m ³ /sec	(110000*(1.05+0.03)/6)	

The Inlet chamber water level of Flocculation basin is 450.340 m (450.480 -0.140)

3.Connection Pipe between Mixing chamber and Flocculation basin N0.6

Mixing chamber water level					450.500 m	✓
Outlet pipe loss						
Inlet Loss	(Diameter 700 mm), f=	0.5	V=	0.60 m/s	h=	0.009 m
Valve Loss	(Diameter 700 mm), f=	0.1	V=	0.60 m/s	h=	0.002 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h=	0.005 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h=	0.005 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h=	0.004 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h=	0.005 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h=	0.005 m
45°Bend Loss	(Diameter 700 mm), f=	0.25	V=	0.60 m/s	h=	0.005 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h=	0.004 m
90°Bend Loss	(Diameter 700 mm), f=	0.23	V=	0.60 m/s	h=	0.004 m
Outlet Loss	(Diameter 700 mm), f=	1.0	V=	0.60 m/s	h=	0.018 m
Pipe Friction Loss	(Diameter 700 mm), f=	0.00066	L=	122.86 m	h=	0.081 m
	Total	h=			0.152 m	
where	C=	110				
	Q=	19800 m ³ /d=	0.229 m ³ /sec	(110000*(1.05+0.03)/6)		

The Inlet chamber water level of Flocculation basin is 450.340 m (450.500 -0.160) ✓

4. Flocculation Basin

Flocculation basin inlet channel water level 450.340 m

1 Head loss of Intake gate

Dimension of gate; 600×600

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 0.6m * 0.6m = 0.36 \text{ m}^2$: Sectional area

$Q = 0.229 \text{ m}^3/\text{sec}$

$v = Q/A = 0.637 \text{ m}/\text{sec}$

$g = 9.8 \text{ m}/\text{sec}^2$

$C = 0.6$

$h = 0.05743 \text{ m} = 0.060 \text{ m}$

Flocculation basin inlet water level 450.280 m

2 Required head loss for flocculation basin

$h = 0.290 \text{ m}$ (Confer Capacity calculation)

Flocculation basin outlet water level 449.990 m

3 Outlet Submerged weir loss

$L = Q / (1.8 * (h1 + 1.4 * h2) * h1^{0.5})$

$h2 = Q / (2.52 * L * h1^{0.5}) - h1 / 1.4$

where $Q = 0.229 \text{ m}^3/\text{sec} = 19800 \text{ m}^3/\text{day} (110000 * (1.05 + 0.03) / 3 / 2)$

$h1 = 0.028 \text{ m}$

$L = 11.0 \text{ m}$

$h2 = Q / (2.52 * L * h1^{0.5}) - h1 / 1.4 = 0.029 \text{ m}$

The height of the overflow weir is accordingly 449.930 m (449.990 - 0.030 - 0.030).

The water level at the downstream of the weir (sedimentation basin) is 449.960 m

in consideration of an weir loss of 0.03 m (h1)

Treatment Capacity(m³/d/Unit) 39,600

Hydraulic Flocculation (Baffle Walls, Up and Down)

Item No.	Descriptions	Unit	Symbol	Nos. of Raws						Between Raws				
				No. 1	No. 2	No. 3	No. 4	No. 5	No. 6	No.1&2	No.2&3	No.3&4	No.4&5	No.5&6
1. General Descriptions														
1)	Design capacity	m ³ /d	(Q)	19,800	19,800	19,800	19,800	19,800	19,800	19,800	19,800	19,800	19,800	19,800
2)	Width of wall	m	(Ww)	1.100	1.100	1.500	1.500	2.300	2.300	0.965	0.965	0.965	0.965	0.965
3)	No. of wall in one raw	-	(Nw)	9	9	9	9	9	9	1	1	1	1	1
4)	Depth	m		3.80	3.80	3.60	3.60	3.50	3.50	3.80	3.80	3.60	3.60	3.50
5)	Length of raws	m		11.00	11.00	11.00	11.00	11.00	11.00					
2. Loss of down flow														
1)	Downflow depth	m	(Hb)	0.75	0.80	0.90	0.95	1.00	1.05	0.75	0.80	0.90	1.00	1.00
2)	Downflow velocity	m/s	(vb)	0.278	0.260	0.170	0.161	0.100	0.095	0.317	0.297	0.264	0.237	0.237
3)	Downflow coefficient of friction loss	-	(fb)	3.5	3.5	3.5	3.5	3.5	3.5	3.5	3.5	3.5	3.5	3.5
4)	No. of down flow in one raw	-		4	4	4	4	4	4	1	1	1	1	1
5)	$hf = Hb/2 \cdot 9.8 \cdot vb^2 / \text{no. of walls}/2$	m		0.055	0.048	0.021	0.018	0.007	0.006	0.018	0.016	0.012	0.010	0.010
3. Loss of over flow														
1)	Overflow depth	m	(Ho)	0.75	0.80	0.90	0.95	1.00	1.05					
2)	Overflow velocity	m/s	(vo)	0.278	0.260	0.170	0.161	0.100	0.095					
3)	Downflow coefficient of friction loss	-	(fb)	1.0	1.0	1.0	1.0	1.0	1.0					
4)	No. of down flow in one raw	-		5	5	5	5	5	5					
5)	$hf = vo^2/2 \cdot 9.8 / \text{no. of walls}/2$	m		0.020	0.017	0.007	0.007	0.003	0.002					
4. Loss of friction														
1)	$R = Ww \cdot Lc/2 / (Ww \cdot Lc)$	m	(R)	0.257	0.257	0.294	0.294	0.340	0.340					
2)	n = roughness coefficient	-	(n)	0.015	0.015	0.015	0.015	0.015	0.015					
3)	vc=velocity	m/s	(vc)	0.216	0.216	0.158	0.158	0.103	0.103					
4)	$C^2 = 1/n^2 \cdot R^{1.5}$	-	(C ²)	2,826	2,826	2,954	2,954	3,102	3,102					
5)	Length of ditch	m	(L _d)	10.0	10.0	10.0	10.0	10.0	10.0					
6)	Length of wall	m	(L _w)	30.500	30.000	27.000	26.500	25.000	24.500					
7)	L = L _d + L _w	m	(L)	40.535	40.035	37.035	36.535	35.035	34.535					
8)	$hf = L \cdot n^2 \cdot vc^5 / R^{4/3}$	m		0.003	0.003	0.001	0.001	0.000	0.000					
5. Total Loss of Head														
1)	H = h ₁ + h ₂ + h ₃	m		0.286	0.072	0.068	0.029	0.056	0.010	0.009	0.018	0.016	0.012	0.010
6. G-value														
1)	Volume of raw	m ³	(V)	45.98	45.98	59.40	59.40	88.55	88.55	387.860	m³	(TTL Volume of Flocculation Basin)		
2)	Detention time	min	(T)	3.34	3.34	4.32	4.32	6.44	6.44	28.2	min	(TTL Detention Time)		
3)	Density of Water (at 25 degree)	kg/m ³	(ρ)	997.100										
4)	Viscosity of Water (x 10 ⁻³)	kg/m/s	(μ)	0.898										
5)	Acceleration of Gravity	m/s ²	(g)	9.8										
6)	$G = (H \cdot \rho \cdot Q \cdot g / (V \cdot \mu))^{0.5}$	s ⁻¹	(G)	71.9	67.5	41.7	39.0	23.8	16.0	42.9				37.0
7)	Gt value	-		14,425	13,546	10,811	10,104	9,181	6,178	72,589	(23,000 to 210,00)			

Width of wall
(11-0.15*9)/10= 0.965 m

Water Level and Weir Level of Hydraulic Flocculation (Baffle Walls, Up and Down)										
Item No.	Descriptions	Unit	Symbol	Nos. of Rows						No.1&2
				No. 1	No. 2	No. 3	No. 4	No. 5	No. 6	
1. Water level of each baffle wall										
1)	Inlet water level (No.1 section)	m		450.280	450.185	450.102	450.060	450.024	450.004	
2)	No.2 section			450.276	450.182	450.100	450.059	450.024	450.004	
3)	No.3 section			450.262	450.169	450.095	450.054	450.022	450.002	
4)	No.4 section			450.258	450.166	450.093	450.053	450.022	450.002	
5)	No.5 section			450.244	450.153	450.088	450.048	450.020	450.000	
6)	No.6 section			450.240	450.150	450.087	450.047	450.019	450.000	
7)	No.7 section			450.225	450.137	450.081	450.042	450.017	449.998	
8)	No.8 section			450.221	450.134	450.080	450.041	450.017	449.998	
9)	No.9 section			450.207	450.121	450.074	450.036	450.015	449.996	Total
10)	No.10 section			450.203	450.117	450.073	450.035	450.015	449.995	Loss
				0.0769	0.0678	0.0288	0.0259	0.0099	0.0090	0.285
2. Weir Top level of each baffle wall										
1)	Weir top level (No.1 section)			449.526	449.382	449.200	449.109	449.024	448.954	
2)	No.2 section									
3)	No.3 section			449.508	449.366	449.193	449.103	449.022	448.952	
4)	No.4 section									
5)	No.5 section			449.490	449.350	449.187	449.097	449.019	448.950	
6)	No.6 section									
7)	No.7 section			449.471	449.334	449.180	449.091	449.017	448.948	
8)	No.8 section									
9)	No.9 section			449.453	449.317	449.173	449.085	449.015	448.945	
10)	No.10 section									
3. Distance between Wall Top Level (451-100m) and Weir Top Level of each baffle wall										
1)	Depth of weir top level (No.1 section)			1.574	1.718	1.900	1.991	2.076	2.146	
2)	No.2 section									
3)	No.3 section			1.592	1.734	1.907	1.997	2.078	2.148	
4)	No.4 section									
5)	No.5 section			1.610	1.750	1.913	2.003	2.081	2.150	
6)	No.6 section									
7)	No.7 section			1.629	1.766	1.920	2.009	2.083	2.152	
8)	No.8 section									
9)	No.9 section			1.647	1.783	1.927	2.015	2.085	2.155	
10)	No.10 section									
4. Overflow Depth										
1)	Overflow depth (No.1 section)			0.754	0.803	0.901	0.951	1.001	1.050	
2)	No.2 section									
3)	No.3 section			0.754	0.803	0.901	0.951	1.001	1.050	
4)	No.4 section									
5)	No.5 section			0.754	0.803	0.901	0.951	1.001	1.050	
6)	No.6 section									
7)	No.7 section			0.754	0.803	0.901	0.951	1.001	1.050	
8)	No.8 section									
9)	No.9 section			0.754	0.803	0.901	0.951	1.001	1.050	
10)	No.10 section									

5. Sedimentation Basin

1 Sedimentation basin inlet water level 449.960 m

Head loss of diffusion wall (No.1)

Diameter of holes and number of holes; $\phi 100 @ 300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) = 3.6738 \text{ m}^2$: Sectional area
 $D = 100 \text{ mmdia.}$
 $a = 13 \text{ pieces}$
 $b = 36 \text{ pieces}$
 $Q = 0.229 \text{ m}^3/\text{sec}$ $(110000 * (1.05 + 0.03) / 86400 / 6)$
 $v = Q / A = 0.0624 \text{ m/sec}$
 $g = 9.8 \text{ m/sec}^2$
 $C = 0.6$

$h_1 = 0.00055 \text{ m}$

Head loss of diffusion wall (No.2-4)

Diameter of holes and number of holes; $\phi 100 @ 300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) = 3.3912 \text{ m}^2$: Sectional area
 $D = 100 \text{ mmdia.}$
 $a = 12 \text{ pieces}$
 $b = 36 \text{ pieces}$
 $Q = 0.229 \text{ m}^3/\text{sec}$ $(110000 * (1.05 + 0.03) / 86400 / 6)$
 $v = Q / A = 0.0676 \text{ m/sec}$
 $g = 9.8 \text{ m/sec}^2$
 $C = 0.6$

$h_{2-4} = 0.00065 * 3 \text{ units} = 0.0019 \text{ m}$

Head loss of diffusion wall (No.5)

Diameter of holes and number of holes; $\phi 100 @ 300 \times 300$

Head loss $h = v^2 / (2 * g * C^2)$

where $A = 3.14 / 4 * D^2 * (a * b) = 3.6738 \text{ m}^2$: Sectional area
 $D = 100 \text{ mmdia.}$
 $a = 13 \text{ pieces}$
 $b = 36 \text{ pieces}$
 $Q = 0.229 \text{ m}^3/\text{sec}$ $(110000 * (1.05 + 0.03) / 86400 / 6)$
 $v = Q / A = 0.0624 \text{ m/sec}$
 $g = 9.8 \text{ m/sec}^2$
 $C = 0.6$

$h_5 = 0.00055 \text{ m}$

Total head loss

$h = h_1 \sim h_5 = 0.00304 = 0.000 \text{ m}$

Sedimentation Basin Downstream Water Level 449.960 m

2 End Trough Bottom Level 449.700 m

Water Level above Trough Orifice 0.060 m

Depth between orifice and Trough Bottom 0.200 m

Trough Loss (Total) 0.260 m

The water level at the downstream of the end trough is 449.450 m in consideration of an

allowance of 0.25 m.

3 Intermediate trough bottom level 449.700 m same as End Trough Bottom Level

4 Intermediate trough channel (Intermediate trough - End channel)

Water Level at upstream of Intermediate Trough Channel 449.700 m same as End Trough Bottom Level

Head loss in the intermediated channel is calculated

$Q_1 = 0.023 \text{ m}^3/\text{sec}$: Water flow of 1 trough (20.4%)

$Q_2 = 2Q_1 = 0.047 \text{ m}^3/\text{sec}$: Water flow of 2 trough (40.7%)

Inflow sectional area

$A(a-d) = B * H = 0.15 \text{ m}^2$ (Water Flow Area $A = 0.060 \text{ m}^2$)

where $B = 0.50 \text{ m}$

H= 0.30 m (Water Depth h= 0.120 m)

Velocity

$V(a-b)=Q1/A=$ 0.39 m/sec

$V(b-c)=Q2/A=$ 0.78 m/sec

Hydraulic radius

$R(a-c)=A/(B+H*2)=$ 0.136 m

Roughness coefficient

n= 0.015

Head losses are calculated using Manning Formula.

$h=n^2*L*v^2/R^{4/3}$

where $L(a-b)=$ 10.0 m

$L(b-c)=$ 12.6 m

$h(a-b)=$ 0.00485 = 0.005 m

$h(b-c)=$ 0.02445 = 0.025 m

$I=n^2*v^2/R^{4/3}$

$I(a-b)=$ 0.00049

$I(b-c)=$ 0.00194

Total head loss

$h(a-c)=$ 0.030 m (0.030)

Critical Water Depth at the end of Intermediated Channel

$hc=(\alpha *Qt^2/(g*B^2))^{1/3}$

where $\alpha =$ 1.1

速度エネルギーの補正係数

$B =$ 0.4 m

$g =$ 9.8 m/s²

$hc=(\alpha *Qt^2/(g*B^2))^{1/3}=$ 0.100 m (0.099 m) at downstream

$hc=hc+h(a-c)$ 0.130 m (0.130 m) at upstream

Bottom level at the end of the intermediated channel is 449.500

Accordingly, water level at the end of the intermediated channel is 449.600 m (449.500 + 0.100)

Water level at the upstream of the intermediated channel is 449.630 m (Water Depth is 0.130 m)

The water level at the end channel is 449.450 m in consideration of an allowance of 0.15 m.

Outflow Trough of Sedimentation Basin

1. End trough (Inlet from both side)

1.1. Load factor of end trough weir design criteria

Q=	11733 m ³ /d	: Flow Rate (59.3%)
n=	8 pieces	: Number of trough	
L=	2 m	: Length of trough	
Lf=	367 m ³ /m/d	: Load factor (= < 500m ³ /m/d)	

1.2. Number of orifice holes per trough

$$N = Qt / (C' \cdot \pi / 4 \cdot d^2 \cdot (2gh)^{0.5})$$

Qt=	0.0170 m ³ /sec	: Collecting water amount per trough	
C'=	0.6		
d=	0.03 mm (φ30mm)	: Orifice diameter	
g=	9.8 m/sec ²		
h=	0.06 m (60mm)	: Overflow depth of orifice	
N=Qt/(C'·π/4·d ² ·(2gh) ^{0.5})=		36 holes per each trough	18 holes per each side of trough

Interval between holes

$$In = L / (N/2) \quad 100 \text{ mm} \quad (0.108 \text{ m})$$

1.3. Water level in the trough

$$hc = (\alpha \cdot Qt^2 / (g \cdot B^2))^{1/3}$$

where α=	1.1	: Supplementary factor of velocity energy	
B=	0.4 m	: Weir width	

hc=(α·Qt ² /(g·B ²)) ^{1/3} =	0.060 m	(0.059 m) at downstream
ho=hc·3 ^{1/2}	0.100 m	(0.104 m) at upstream

1.4. Load factor of trough weir

Q=	11733.33333 m ³ /d	: Flow Rate (59.3%)
n=	8 pieces	: Number of trough per unit	
Le=	2.0 m	: length of trough	
Lf=	367 m ³ /m/day	: Load factor (= < 500m ³ /m/d)	

2. Intermediate trough (Inlet from one side)

2.1. Load factor of trough weir design criteria

Q=	8067 m ³ /d	: Flow Rate (40.7%)
n=	2 pieces	: Number of trough in one basin	
L=	11.0 m	: Length of trough	
Lf=	500 m ³ /m/d	: Load factor (= < 500m ³ /m/d)	

2.2. Number of orifice holes per 1/2trough

$$N = Qt / (C' \cdot \pi / 4 \cdot d^2 \cdot (2gh)^{0.5})$$

Qt=	0.0467 m ³ /sec	: Collecting water amount per 1/2trough	
C'=	0.6		
d=	0.03 mm (φ30mm)	: Orifice diameter	
g=	9.8 m/sec ²		
h=	0.06 m (60mm)	: Overflow depth of orifice	
N=Qt/(C'·π/4·d ² ·(2gh) ^{0.5})=		102 holes per each trough	

Interval between holes

$$In = L / (N/2) \quad 100 \text{ mm} \quad (0.108 \text{ m})$$

2.3. Water level in the trough

$$hc = (\alpha \cdot (1/2 \cdot Qt)^2 / (g \cdot B^2))^{1/3}$$

where α=	1.1	速度エネルギーの補正係数	
B=	0.4 m		

hc=(α·(1/2·Qt) ² /(g·B ²)) ^{1/3} =	0.070 m	(0.073 m) at downstream
ho=hc·3 ^{1/2}	0.120 m	(0.121 m) at upstream

2.4. Load factor of trough weir (one side inflow)

Q=	8066.666667 m ³ /d	: Flow Rate (40.7%)
n=	2 pieces	: Number of trough per unit	
Le=	11 m	: length of trough	
Lf=	367 m ³ /m/day	: Load factor (= < 500m ³ /m/d)	

6. Rapid Sand Filter (in case of four units duty)

Phase I

1 Water level at the upstream of the inflow channel of the filter

449.450 m

Head loss in the channel is calculated under the conditions that four units are operated

Q1 = 0.458 m³/sec : Total flow rate for 4 units of 1 system
 Q2 = Q1/4 = 0.115 m³/sec : flow rate for 1 units during 4 units duty in 1 system

Inflow sectional area

A(a-d) = B * H = 2.17 m²
 where B = 1.50 m
 H = 1.45 m

Velocity

V(a-b) = 3 * Q2 / A = 0.11 m/sec
 V(b-c) = 2 * Q2 / A = 0.05 m/sec

Hydraulic radius

R(a-d) = A / (B + H * 2) = 0.494 m

Roughness coefficient

n = 0.015

Head losses are calculated using Manning Formula.

$h = n^2 * L * v^2 / R^{4/3}$
 where L(a-b) = 33.95 m
 L(b-c) = 9.3 m

h(a-b) = 0.00022 = 0 m
 h(b-c) = 0.00001 = 0 m

Total head loss

h(a-d) = 0 m

Accordingly, water level at the downstream of inflow channel is 449.450 m (449.450 - 0.000)

Inlet channel bottom level is 448.000 m (449.450 - 1.450)

2 Weir and inlet gate loss

1 Overflow weir loss

$h = (Q2 / (1.84 * b))^{2/3}$
 where b = 0.80 m
 $h = (Q2 / (1.84 * b))^{2/3} = 0.182$ m (0.190 m)

The height of the overflow weir is accordingly 449.260m (449.450 - 0.190)

The water level at the downstream of the weir is 448.960 m in consideration of an allowance

of 0.30 m.

2 Inlet gate loss

$h = v^2 / (2 * g * c^2)$
 where A = 0.16 m² : Gate Area (400mm x 400mm)
 Q2 = 0.115 m³/sec
 v = Q2 / A = 0.72 m/sec
 g = 9.8 m/sec²
 c = 0.6
 $h = v^2 / (2 * g * c^2) = 0.073$ m (0.080 m)

Total loss h = 0.255 m

The water level at the downstream of the weir is 448.880m (448.960 - 0.080)

3 Inlet pipe loss

Inlet Loss	(Diameter 400 mm), f = 0.5	V(Q1) = 0.91 m/s	h = 0.021 m
Outlet Loss	(Diameter 400 mm), f = 1.0	V(Q2) = 0.91 m/s	h = 0.042 m
Pipe Friction Loss	(Diameter 400 mm), f = 0.00281	L = 0.70 m	h = 0.002 m
Total	h = 0.065 m		(0.070 m)

where Q2 = 0.115 m³/sec
 C = 110

The high water level of filter is 448.810 m (448.880 - 0.070)

Rapid Sand Filter (in case of eight units duty)

Phase2

1 Water level at the inflow channel of the filter

449.450 m

Head loss in the channel is calculated under the conditions that one unit is stopped its operation and one unit is washed.

Q1= 0.458 m³/sec : Total flow rate for 6 units of 1 system
 Q2=Q1/4= 0.115 m³/sec : flow rate for 1 units during 4 units duty in 1 system

Inflow sectional area

A(a-d)=B*H= 2.17 m²
 where B= 1.50 m
 H= 1.45 m

Velocity

V(a-b)=2*Q2/A= 0.16 m/sec
 V(b-c)=Q2/A= 0.05 m/sec
 V(c-d)=3*Q2/A= 0.16 m/sec
 V(d-e)=2*Q2/A= 0.11 m/sec
 V(e-f)=4*Q2/A= 0.21 m/sec
 V(f-g)=3*Q2/A= 0.16 m/sec
 V(g-h)=2*Q2/A= 0.11 m/sec
 V(h-i)=4*Q2/A= 0.21 m/sec
 V(i-j)=3*Q2/A= 0.16 m/sec
 V(j-k)=2*Q2/A= 0.11 m/sec
 V(k-l)=Q2/A= 0.05 m/sec

Hydraulic radius

R(a-d)=A/(B+H*2)= 0.494 m

Roughness coefficient

n= 0.015

Head losses are calculated using Manning Formula.

$h = n^2 * L * v^2 / R^{4/3}$

where L(a-b)= 12.85 m
 L(b-c)= 8.25 m
 L(c-d)= 6.15 m
 L(d-e)= 6.55 m
 L(e-f)= 6.15 m
 L(f-g)= 9.3 m
 L(g-h)= 5.65 m
 L(h-i)= 33.95 m
 L(i-j)= 9.3 m
 L(j-k)= 17.8 m
 L(k-l)= 9.3 m

h(a-b)= 0.00018 = 0 m
 h(b-c)= 0.00001 = 0 m
 h(c-d)= 0.00009 = 0 m
 h(d-e)= 0.00004 = 0 m
 h(e-f)= 0.00016 = 0 m
 h(f-g)= 0.00013 = 0 m
 h(g-h)= 0.00004 = 0 m
 h(h-i)= 0.00087 = 0 m
 h(i-j)= 0.00013 = 0 m
 h(j-k)= 0.00011 = 0 m
 h(k-l)= 0.00001 = 0 m

Total head loss

h(a-d)= 0.00179 = 0.000 m

Accordingly, water level at the inflow channel is 449.450 m (449.450 - 0.000)

Inlet channel bottom level is 448.000 m (449.450 - 1.450)

2 Weir and inlet gate loss

1 Overflow weir loss

$$h = (Q^2 / (1.84 * b))^{2/3}$$

where $b = 0.80 \text{ m}$

$$h = (Q^2 / (1.84 * b))^{2/3} = 0.182 \text{ m} \quad (0.190 \text{ m})$$

The height of the overflow weir is accordingly 449.260 m ($449.450 - 0.190$)

The water level at the downstream of the weir is 448.960 m in consideration of an allowance

of 0.30 m .

2 Inlet gate loss

$$h = v^2 / (2 * g * c^2)$$

where $A = 0.16 \text{ m}^2$: Gate Area ($400 \text{ mm} \times 400 \text{ mm}$)

$$Q_2 = 0.115 \text{ m}^3/\text{sec}$$

$$v = Q_2 / A = 0.72 \text{ m/sec}$$

$$g = 9.8 \text{ m/sec}^2$$

$$c = 0.6$$

$$h = v^2 / (2 * g * c^2) = 0.073 \text{ m} \quad (0.080 \text{ m})$$

The water level at the downstream of the gate is 448.880 m ($448.960 - 0.080$)

3 Inlet pipe loss

Inlet Loss (Diameter 400 mm), $f = 0.5$ $V(Q_1) = 0.91 \text{ m/s}$ $h = 0.021 \text{ m}$

Outlet Loss (Diameter 400 mm), $f = 1.0$ $V(Q_2) = 0.91 \text{ m/s}$ $h = 0.042 \text{ m}$

Pipe Friction Loss (Diameter 400 mm), $I = 0.00281$ $L = 0.70 \text{ m}$ $h = 0.002 \text{ m}$

Total $h = 0.065 \text{ m}$

where $Q_2 = 0.115 \text{ m}^3/\text{sec}$

$C = 110$

The high water level of filter is 448.810 m ($448.880 - 0.070$)

7. Rapid Sand Filter Outflow Water Level (in case of four units duty)

Phase I

Filtered water level (Outlet box) is 447.060 m.

1 Filtered outlet pipe loss

Inlet Loss	(Diameter	350 mm), f=	0.5	V=	1.19 m/s	h=	0.036 m
Valve	(Diameter	350 mm), f=	0.1	V=	1.19 m/s	h=	0.007 m
Outlet Loss	(Diameter	350 mm), f=	1.0	V=	1.19 m/s	h=	0.072 m
Pipe Friction Loss	(Diameter	350 mm), l=	0.00539	L=	2.50 m	h=	0.013 m
Total						h=	0.128 m

where $Q = 0.115 \text{ m}^3/\text{sec}$ $(110000 \cdot (1.05 + 0.03) / 3 / 86400 / 4)$
 $C = 110$

The water level at upstream of weir (b=1.6m) is 446.930 m (447.060 - 0.130)

2 Overflow weir loss (in case of four units duty)

$$h = (Q / (1.84 \cdot b))^{2/3}$$

where $Q = 0.115 \text{ m}^3/\text{sec}$ $(110000 \cdot (1.05 + 0.03) / 3 / 86400 / 4)$
 $b = 1.60 \text{ m}$

$$h = (Q / (1.84 \cdot b))^{2/3} = 0.115 \text{ m}$$

The height of the overflow weir is 446.810 m same as surface level of filter media.

The water level at the downstream of the weir is 446.600 m in consideration of an allowance of 0.21 m.

3 Overflow weir loss (b=8.0m)

$$h = (Q / (1.84 \cdot b))^{2/3}$$

where $Q = 0.458 \text{ m}^3/\text{sec}$ $(110000 \cdot (1.05 + 0.03) / 3 / 86400)$
 $b = 8.00 \text{ m}$

$$h = (Q / (1.84 \cdot b))^{2/3} = 0.099 \text{ m}$$

The height of the overflow weir is 446.500 m (446.600 - 0.100)

The water level at the downstream of the weir (filtered water effluent channel) is 446.030 m in consideration of an allowance of 0.470 m.

Rapid Sand Filter Outflow Water Level (in case of eight units duty)

Phase2

Filtered water level (Outlet box) is 447.060 m.

1 Filtered outlet pipe loss

Inlet Loss	(Diameter	350 mm), f=	0.5	V=	1.19 m/s	h=	0.036 m
Valve	(Diameter	350 mm), f=	0.1	V=	1.19 m/s	h=	0.007 m
Outlet Loss	(Diameter	350 mm), f=	1.0	V=	1.19 m/s	h=	0.072 m
Pipe Friction Loss	(Diameter	350 mm), l=	0.00539	L=	2.50 m	h=	0.013 m
Total						h=	0.128 m

where $Q=0.115 \text{ m}^3/\text{sec}$ $(110000*(1.05+0.03)/3/86400/4)$
 $C=110$

The water level at upstream of weir (b=1.6m) is 446.930 m (447.060 - 0.130)

2 Overflow weir loss (in case of eight units duty)

$$h=(Q/(1.84*b))^{2/3}$$

where $Q=0.115 \text{ m}^3/\text{sec}$ $(110000*(1.05+0.03)/3/86400/4)$

$b=1.60 \text{ m}$

$$h=(Q/(1.84*b))^{2/3}=0.115 \text{ m}$$

The height of the overflow weir is 446.810 m same as surface level of filter media.

The water level at the downstream of the weir is 446.660 m in consideration of an allowance of 0.15 m.

3 Overflow weir loss (b=8.0m)

$$h=(Q/(1.84*b))^{2/3}$$

where $Q=0.917 \text{ m}^3/\text{sec}$ $(110000*(1.05+0.03)/3*2/86400)$

$b=8.00 \text{ m}$

$$h=(Q/(1.84*b))^{2/3}=0.157 \text{ m}$$

The height of the overflow weir is 446.500 m (446.660 - 0.160)

The water level at the downstream of the weir (filtered water effluent channel) is 446.020 m in consideration of an allowance of 0.480 m.

Rapid Sand Filter Outflow Water Level (in case of four units duty)

Phase3

Filtered water level (Outlet box) is 447.060 m.

1 Filtered outlet pipe loss

Inlet Loss	(Diameter	350 mm), f=	0.5	V=	1.19 m/s	h=	0.036 m
Valve	(Diameter	350 mm), f=	0.1	V=	1.19 m/s	h=	0.007 m
Outlet Loss	(Diameter	350 mm), f=	1.0	V=	1.19 m/s	h=	0.072 m
Pipe Friction Loss	(Diameter	350 mm), f=	0.00539	L=	2.50 m	h=	0.013 m
Total						h=	0.128 m
where	Q=	0.115 m ³ /sec	(110000*(1.05+0.03)/3/86400/4)				
	C=	110					

The water level at upstream of weir (b=1.6m) is 446.930 m (447.060 - 0.130)

2 Overflow weir loss (in case of four units duty)

	h=(Q/(1.84*b)) ^(2/3)		
where	Q=	0.115 m ³ /sec	(110000*(1.05+0.03)/3/86400/4)
	b=	1.60 m	
	h=(Q/(1.84*b)) ^(2/3) =	0.115 m	

The height of the overflow weir is 446.810 m same as surface level of filter media.

The water level at the downstream of the weir is 446.600 m in consideration of an allowance of 0.21 m.

3 Overflow weir loss (b=8.0m)

	h=(Q/(1.84*b)) ^(2/3)		
where	Q=	0.458 m ³ /sec	(110000*(1.05+0.03)/3/86400)
	b=	8.00 m	
	h=(Q/(1.84*b)) ^(2/3) =	0.099 m	

The height of the overflow weir is 446.500 m (446.600 - 0.100)

The water level at the downstream of the weir (filtered water effluent channel) is 446.070 m in consideration of an allowance of 0.430 m.

8.Connection Pipe between Filter and Clear Water Reservoir

1.Connection Pipe between Filter(No.1+No.2) and Clear Water Reservoir(No.1-1)

Phase1

Filter Outlet water level				446.030 m	✓
Outlet pipe loss					
Inlet Loss	(Diameter 1000 mm), f=	0.5	V=	1.17 m/s	h= 0.035 m
Tee Branch	(Diameter 1000 1000 mm), f=	0.99	V=	1.17 m/s	h= 0.069 m
Reducer	(Diameter 1000 800 mm), f=	0.00	V=	0.58 m/s	h= 0.000 m
Tee Branch	(Diameter 800 600 mm), f=	0.05	V=	0.91 m/s	h= 0.002 m
Reducer	(Diameter 800 600 mm), f=	0.00	V=	0.46 m/s	h= 0.000 m
90°Bend Loss	(Diameter 600 mm), f=	0.23	V=	0.81 m/s	h= 0.008 m
Valve Loss	(Diameter 600 mm), f=	0.30	V=	0.81 m/s	h= 0.010 m
Outlet Loss	(Diameter 600 mm), f=	1.0	V=	0.81 m/s	h= 0.033 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00152	L=	8.75 m	h= 0.013 m
Pipe Friction Loss	(Diameter 800 mm), I=	0.00125	L=	7.60 m	h= 0.010 m
Pipe Friction Loss	(Diameter 600 mm), I=	0.00141	L=	17.71 m	h= 0.025 m
Total	h=		0.205 m		
where	C=	110			
Q1=	19800 m3/d=	0.229 m3/sec	(110000*(1.05+0.03)/6)		
Q2=	39600 m3/d=	0.458 m3/sec	(110000*(1.05+0.03)/6*2)		
Q3=	59400 m3/d=	0.688 m3/sec	(110000*(1.05+0.03)/6*3)		
Q4=	79200 m3/d=	0.917 m3/sec	(110000*(1.05+0.03)/6*4)		
Q5=	99000 m3/d=	1.146 m3/sec	(110000*(1.05+0.03)/6*5)		
Q6=	118800 m3/d=	1.375 m3/sec	(110000*(1.05+0.03))		

The Inlet water level of Clear Water Reservoir is 445.820 m (446.030 -0.210)

2.Connection Pipe between Filter(No.1+No.2) and Clear Water Reservoir(No.1-2)

Phase1

Filter Outlet water level				446.030 m	
Outlet pipe loss					
Inlet Loss	(Diameter 1000 mm), f=	0.5	V=	1.17 m/s	h= 0.035 m
Tee Branch	(Diameter 1000 1000 mm), f=	0.99	V=	1.17 m/s	h= 0.069 m
Reducer	(Diameter 1000 800 mm), f=	0.00	V=	0.58 m/s	h= 0.000 m
Tee Branch	(Diameter 800 600 mm), f=	0.90	V=	0.91 m/s	h= 0.038 m
Valve Loss	(Diameter 600 mm), f=	0.30	V=	0.81 m/s	h= 0.010 m
Outlet Loss	(Diameter 600 mm), f=	1.0	V=	0.81 m/s	h= 0.033 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00152	L=	5.75 m	h= 0.009 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00042	L=	3.00 m	h= 0.001 m
Pipe Friction Loss	(Diameter 800 mm), I=	0.00125	L=	5.10 m	h= 0.006 m
Pipe Friction Loss	(Diameter 600 mm), I=	0.00141	L=	6.01 m	h= 0.008 m
Total	h=		0.209 m		
where	C=	110			
Q1=	19800 m3/d=	0.229 m3/sec	(110000*(1.05+0.03)/6)		
Q2=	39600 m3/d=	0.458 m3/sec	(110000*(1.05+0.03)/6*2)		
Q3=	59400 m3/d=	0.688 m3/sec	(110000*(1.05+0.03)/6*3)		
Q4=	79200 m3/d=	0.917 m3/sec	(110000*(1.05+0.03)/6*4)		
Q5=	99000 m3/d=	1.146 m3/sec	(110000*(1.05+0.03)/6*5)		
Q6=	118800 m3/d=	1.375 m3/sec	(110000*(1.05+0.03))		

The Inlet water level of Clear Water Reservoir is 445.820 m (446.030 -0.210)

3. Connection Pipe between Filter(No.1+No.2) and Clear Water Reservoir(No2-1)

Phase2

Filter Outlet water level				446.020 m	✓
Outlet pipe loss					
Inlet Loss	(Diameter 1000 mm), f=	0.5	V=	1.17 m/s	h= 0.035 m
Tee Branch	(Diameter 1000 1000 mm), f=	0.99	V=	1.17 m/s	h= 0.069 m
Tee Branch	(Diameter 1000 600 mm), f=	1.20	V=	0.58 m/s	h= 0.021 m
Valve Loss	(Diameter 600 mm), f=	0.30	V=	0.81 m/s	h= 0.010 m
Outlet Loss	(Diameter 600 mm), f=	1.0	V=	0.81 m/s	h= 0.033 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00152	L=	5.75 m	h= 0.009 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00042	L=	20.90 m	h= 0.009 m
Pipe Friction Loss	(Diameter 600 mm), I=	0.00141	L=	6.01 m	h= 0.008 m
	Total	h=	0.194 m		
where	C=	110			
	Q1=	19800 m ³ /d=	0.229 m ³ /sec	(110000*(1.05+0.03)/6)	
	Q2=	39600 m ³ /d=	0.458 m ³ /sec	(110000*(1.05+0.03)/6*2)	
	Q3=	59400 m ³ /d=	0.688 m ³ /sec	(110000*(1.05+0.03)/6*3)	
	Q4=	79200 m ³ /d=	0.917 m ³ /sec	(110000*(1.05+0.03)/6*4)	
	Q5=	99000 m ³ /d=	1.146 m ³ /sec	(110000*(1.05+0.03)/6*5)	
	Q6=	118800 m ³ /d=	1.375 m ³ /sec	(110000*(1.05+0.03))	

The Inlet water level of Clear Water Reservoir is 445.820 m (446.020 -0.200)

4. Connection Pipe between Filter(No.1+No.2) and Clear Water Reservoir(No.2-2)

Phase2

Filter Outlet water level				446.060 m	
Outlet pipe loss					
Inlet Loss	(Diameter 1000 mm), f=	0.5	V=	1.17 m/s	h= 0.035 m
Tee Branch	(Diameter 1000 1000 mm), f=	0.99	V=	1.17 m/s	h= 0.069 m
Tee Branch	(Diameter 1000 600 mm), f=	0.05	V=	0.58 m/s	h= 0.001 m
Tee Combine	(Diameter 1000 1000 mm), f=	0.36	V=	0.88 m/s	h= 0.014 m
Tee Branch	(Diameter 1000 600 mm), f=	1.20	V=	0.88 m/s	h= 0.047 m
Valve Loss	(Diameter 600 mm), f=	0.30	V=	0.81 m/s	h= 0.010 m
Outlet Loss	(Diameter 600 mm), f=	1.0	V=	0.81 m/s	h= 0.033 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00152	L=	5.75 m	h= 0.009 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00042	L=	20.90 m	h= 0.009 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00012	L=	6.20 m	h= 0.001 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00012	L=	8.00 m	h= 0.001 m
Pipe Friction Loss	(Diameter 600 mm), I=	0.00141	L=	6.01 m	h= 0.008 m
	Total	h=	0.237 m		
where	C=	110			
	Q1=	19800 m ³ /d=	0.229 m ³ /sec	(110000*(1.05+0.03)/6)	
	Q2=	39600 m ³ /d=	0.458 m ³ /sec	(110000*(1.05+0.03)/6*2)	
	Q3=	59400 m ³ /d=	0.688 m ³ /sec	(110000*(1.05+0.03)/6*3)	
	Q4=	79200 m ³ /d=	0.917 m ³ /sec	(110000*(1.05+0.03)/6*4)	
	Q5=	99000 m ³ /d=	1.146 m ³ /sec	(110000*(1.05+0.03)/6*5)	
	Q6=	118800 m ³ /d=	1.375 m ³ /sec	(110000*(1.05+0.03))	

The Inlet water level of Clear Water Reservoir is 445.820 m (446.060 -0.240)

5.Connection Pipe between Filter(No.1+No.2+No.3) and Clear Water Reservoir(No.3-1) Phase3

Filter Outlet water level	446.080 m				
Outlet pipe loss					
Inlet Loss	(Diameter 1000 mm), f=	0.5	V=	1.17 m/s	h= 0.035 m
Tee Branch	(Diameter 1000 1000 mm), f=	0.99	V=	1.17 m/s	h= 0.069 m
Tee Branch	(Diameter 1000 600 mm), f=	0.05	V=	0.58 m/s	h= 0.001 m
Tee Combine	(Diameter 1000 1000 mm), f=	0.36	V=	0.88 m/s	h= 0.014 m
Tee Branch	(Diameter 1000 600 mm), f=	0.05	V=	0.88 m/s	h= 0.002 m
Reducer	(Diameter 1000 800 mm), f=	0.00	V=	0.58 m/s	h= 0.000 m
Tee Branch	(Diameter 800 600 mm), f=	0.90	V=	0.91 m/s	h= 0.038 m
Valve Loss	(Diameter 600 mm), f=	0.30	V=	0.81 m/s	h= 0.010 m
Outlet Loss	(Diameter 600 mm), f=	1.0	V=	0.81 m/s	h= 0.033 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00152	L=	5.75 m	h= 0.009 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00042	L=	20.90 m	h= 0.009 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00012	L=	6.20 m	h= 0.001 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00089	L=	8.00 m	h= 0.007 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00042	L=	3.00 m	h= 0.001 m
Pipe Friction Loss	(Diameter 800 mm), I=	0.00125	L=	16.60 m	h= 0.021 m
Pipe Friction Loss	(Diameter 600 mm), I=	0.00141	L=	6.01 m	h= 0.008 m
	Total	h=	0.258 m		
where	C=	110			
	Q1=	19800 m ³ /d=	0.229 m ³ /sec	(110000*(1.05+0.03)/6)	
	Q2=	39600 m ³ /d=	0.458 m ³ /sec	(110000*(1.05+0.03)/6*2)	
	Q3=	59400 m ³ /d=	0.688 m ³ /sec	(110000*(1.05+0.03)/6*3)	
	Q4=	79200 m ³ /d=	0.917 m ³ /sec	(110000*(1.05+0.03)/6*4)	
	Q5=	99000 m ³ /d=	1.146 m ³ /sec	(110000*(1.05+0.03)/6*5)	
	Q6=	118800 m ³ /d=	1.375 m ³ /sec	(110000*(1.05+0.03))	

The Inlet water level of Clear Water Reservoir is 445.820 m (446.080 -0.260)

6.Connection Pipe between Filter(No.1+No.2+No.3) and Clear Water Reservoir(No.3-2) Phase3

Filter Outlet water level	446.070 m ✓				
Outlet pipe loss					
Inlet Loss	(Diameter 1000 mm), f=	0.5	V=	1.17 m/s	h= 0.035 m
Tee Branch	(Diameter 1000 1000 mm), f=	0.99	V=	1.17 m/s	h= 0.069 m
Tee Branch	(Diameter 1000 600 mm), f=	0.05	V=	0.58 m/s	h= 0.001 m
Tee Combine	(Diameter 1000 1000 mm), f=	0.36	V=	0.88 m/s	h= 0.014 m
Tee Branch	(Diameter 1000 600 mm), f=	0.05	V=	0.88 m/s	h= 0.002 m
Reducer	(Diameter 1000 800 mm), f=	0.00	V=	0.58 m/s	h= 0.000 m
Tee Branch	(Diameter 800 600 mm), f=	0.05	V=	0.91 m/s	h= 0.002 m
Reducer	(Diameter 800 600 mm), f=	0.00	V=	0.91 m/s	h= 0.000 m
90°Bend Loss	(Diameter 600 mm), f=	0.23	V=	0.81 m/s	h= 0.008 m
Valve Loss	(Diameter 600 mm), f=	0.30	V=	0.81 m/s	h= 0.010 m
Outlet Loss	(Diameter 600 mm), f=	1.0	V=	0.81 m/s	h= 0.033 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00159	L=	5.75 m	h= 0.009 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00042	L=	20.90 m	h= 0.009 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00012	L=	6.20 m	h= 0.001 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00089	L=	8.00 m	h= 0.007 m
Pipe Friction Loss	(Diameter 1000 mm), I=	0.00042	L=	3.00 m	h= 0.001 m
Pipe Friction Loss	(Diameter 800 mm), I=	0.00125	L=	19.10 m	h= 0.024 m
Pipe Friction Loss	(Diameter 600 mm), I=	0.00141	L=	17.71 m	h= 0.025 m
	Total	h=	0.250 m		
where	C=	110			
	Q1=	19800 m ³ /d=	0.229 m ³ /sec	(110000*(1.05+0.03)/6)	
	Q2=	39600 m ³ /d=	0.458 m ³ /sec	(110000*(1.05+0.03)/6*2)	
	Q3=	59400 m ³ /d=	0.688 m ³ /sec	(110000*(1.05+0.03)/6*3)	
	Q4=	79200 m ³ /d=	0.917 m ³ /sec	(110000*(1.05+0.03)/6*4)	
	Q5=	99000 m ³ /d=	1.146 m ³ /sec	(110000*(1.05+0.03)/6*5)	
	Q6=	118800 m ³ /d=	1.375 m ³ /sec	(110000*(1.05+0.03))	

The Inlet water level of Clear Water Reservoir is 445.820 m (446.070 -0.250)

9. Clear water reservoir

1 Clear water reservoir Water Level

445.820 m

1 Head loss in the channel (under the conditions that two reservoirs are duty)

$$Q = 0.219 \text{ m}^3/\text{sec} = 18883 \text{ m}^3/\text{day} (110000 * 1.03/3/2)$$

Inflow sectional area

$$A = B * H = 12.30 \text{ m}^2$$

where $B = 4.10 \text{ m}$
 $H = 3.00 \text{ m}$

Velocity

$$V = Q/A = 0.02 \text{ m/sec}$$

Hydraulic radius

$$R = A/(B + H * 2) = 1.218 \text{ m}$$

Roughness coefficient

$$n = 0.015$$

Head losses are calculated using Manning Formula.

$$h = n^2 * L * v^2 / R^{4/3}$$

where $L = 57.2 \text{ m}$

$$h = 0.00000 = 0.000 \text{ m}$$

2 Head loss in the channel (under the conditions that one reservoir is duty)

$$Q = 0.437 \text{ m}^3/\text{sec} = 37767 \text{ m}^3/\text{day} (110000 * 1.03/3)$$

Inflow sectional area

$$A = B * H = 12.30 \text{ m}^2$$

where $B = 4.10 \text{ m}$
 $H = 3.00 \text{ m}$

Velocity

$$V = Q/A = 0.04 \text{ m/sec}$$

Hydraulic radius

$$R = A/(B + H * 2) = 1.218 \text{ m}$$

Roughness coefficient

$$n = 0.015$$

Head losses are calculated using Manning Formula.

$$h = n^2 * L * v^2 / R^{4/3}$$

where $L = 57.2 \text{ m}$

$$h = 0.00001 = 0.000 \text{ m}$$

3 Bend loss

$$h = (V1 - V2)^2 / (2 * g) * n$$

where $V1 = 0.018 \text{ m/sec}$
 $V2 = 0 \text{ m/sec}$
 $g = 9.8 \text{ m/sec}^2$
 $n = 4$

$$h = (V1 - V2)^2 / (2 * g) * n = 0.0001 = 0.000 \text{ m}$$

4 Total head loss 0.000 m

Therefore High water level in clear water reservoir is 445.820 m (445.820 - 0.000)

Effective Depth is 3.000 m.

Low Water Level in Clear Water Level is 442.820 m (445.820 - 3.000)

10.Connection Pipe between Clear Water Reservoir (No.3) and Transmission Pump Station

1 Clear Water Reservoir Outlet water level (LWL)

442.820 m

Outlet pipe loss

Inlet Loss	(Diameter 600 mm), f= 0.5	V= 0.77 m/s	h= 0.015 m
Valve Loss	(Diameter 600 mm), f= 0.1	V= 0.77 m/s	h= 0.003 m
90°Bend Loss	(Diameter 600 mm), f= 0.1	V= 0.77 m/s	h= 0.003 m
Gradually Expanded Pipe	(Diameter 800 600 mm), f= 0.494	$\theta= 22.6^\circ$	h= 0.003 m
Tee Combine	(Diameter 800 600 mm), f= 0.47	V= 0.44 m/s	h= 0.005 m
Gradually Expanded Pipe	(Diameter 900 800 mm), f= 0.416	$\theta= 19.7^\circ$	h= 0.001 m
Tee Combine	(Diameter 900 600 mm), f= 0.05	V= 0.69 m/s	h= 0.001 m
Gradually Expanded Pipe	(Diameter 1000 900 mm), f= 0.416	$\theta= 19.7^\circ$	h= 0.001 m
Tee Combine	(Diameter 1000 600 mm), f= 0.05	V= 0.84 m/s	h= 0.002 m
Gradually Expanded Pipe	(Diameter 1100 1000 mm), f= 0.416	$\theta= 19.7^\circ$	h= 0.001 m
Tee Combine	(Diameter 1100 600 mm), f= 0.05	V= 0.92 m/s	h= 0.002 m
Gradually Expanded Pipe	(Diameter 1200 1100 mm), f= 0.416	$\theta= 19.7^\circ$	h= 0.001 m
Tee Loss	(Diameter 1200 1200 mm), f= 1.0	V= 1.16 m/s	h= 0.069 m
Pipe Friction Loss	(Diameter 1200 mm), I= 0.00121	L= 9.54 m	h= 0.012 m
Pipe Friction Loss	(Diameter 1100 mm), I= 0.00132	L= 8.43 m	h= 0.011 m
Pipe Friction Loss	(Diameter 1000 mm), I= 0.00139	L= 10.33 m	h= 0.014 m
Pipe Friction Loss	(Diameter 900 mm), I= 0.00137	L= 14.14 m	h= 0.019 m
Pipe Friction Loss	(Diameter 800 mm), I= 0.00114	L= 19.64 m	h= 0.022 m
Pipe Friction Loss	(Diameter 600 mm), I= 0.00129	L= 17.55 m	h= 0.023 m
Total	h= 0.207 m		

where

C=	110		
Q1=	18883 m ³ /d=	0.219 m ³ /sec	(110000*1.03/3/2)
Q2=	37767 m ³ /d=	0.437 m ³ /sec	(110000*1.03/3/2*2)
Q3=	56650 m ³ /d=	0.656 m ³ /sec	(110000*1.03/3/2*3)
Q4=	75533 m ³ /d=	0.874 m ³ /sec	(110000*1.03/3/2*4)
Q5=	94417 m ³ /d=	1.093 m ³ /sec	(110000*1.03/3/2*5)
Q6=	113300 m ³ /d=	1.311 m ³ /sec	(110000*1.03/3/2*6)

The Inlet water level of Transmission Pump Station is

442.610 m (442.820 -0.210)

(Pipe center Level in the Clear Water Reservoir is

441.320 m (442.820 -0.6*2.5)

(Pipe center Level in the Transmission Pump Station is

440.860 m)

11 Hydraulic Calculation of Sedimentation Basin - Sludge Lagoon

In case of drainage from 4 hoppers (for the purpose of empty of sedimentation basin)

Sedimentation Basin Sludge Pipe - Manhole (DIP Pipe 150mm -250mm)

Manhole - Sludge Lagoon (RC Pipe 700mm)

1. Sedimentation Basin Water Level

H.W.L.	449.960 m	
L.L.W.L.	445.160 m	(Drain Pit Top Level in Sedimentation Basin)

2. Drain Pipe Center Level

W.L.+	443.700 m	(DIP 150 - 250 Drain Pipe Center Level)
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3. First Manhole Water Level

W.L.+	442.800 m	(Drain Pit Top Level in Drain Pipe Gallery +443.000 - 0.20m)
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4. Sludge Lagoon High Water Level

442.000 m

4. Actual Head Loss

6.260 m (449.960 - 443.700)

5 Intake Flow & Velocity

Q1=	0.0414 m ³ /sec=	3577 m ³ /day
Q2=	0.0828 m ³ /sec=	7154 m ³ /day
Q3=	0.1242 m ³ /sec=	10731 m ³ /day
Q4=	0.1656 m ³ /sec=	14308 m ³ /day

6. Water Level Loss

6.1. Suction Pipe Loss C= 100

6.1.1. Inlet Loss	(Diameter 150 mm), f=	0.5	V= 2.34 m/s	h= 0.140 m
6.1.2. Valve Loss	(Diameter 150 mm), f=	0	V= 2.34 m/s	h= 0.000 m
6.1.3. Valve Loss	(Diameter 150 mm), f=	10	V= 2.34 m/s	h= 2.794 m
6.1.4. Tee Combine Loss	(Diameter 250 150 mm), f=	7.00	V= 0.84 m/s	h= 0.252 m
6.1.5. Tee Combine Loss	(Diameter 250 150 mm), f=	2.00	V= 1.69 m/s	h= 0.291 m
6.1.6. Tee Combine Loss	(Diameter 250 150 mm), f=	0.60	V= 2.53 m/s	h= 0.196 m
6.1.7. Tee Combine Loss	(Diameter 250 150 mm), f=	0.20	V= 3.38 m/s	h= 0.117 m
6.1.8. Tee Combine Loss	(Diameter 250 150 mm), f=	0.00	V= 1.69 m/s	h= 0.000 m
6.1.9. Tee Combine Loss	(Diameter 250 150 mm), f=	0.00	V= 2.53 m/s	h= 0.000 m
6.1.10. Tee Combine Loss	(Diameter 250 150 mm), f=	0.00	V= 3.38 m/s	h= 0.000 m
6.1.11. Tee Combine Loss	(Diameter 250 150 mm), f=	0.00	V= 3.38 m/s	h= 0.000 m
6.1.12. Outlet Loss	(Diameter 250 mm), f=	1.0	V= 3.38 m/s	h= 0.583 m
6.1.13. Pipe Friction Loss	(Diameter 150 mm), I=	0.061	L= 2.6 m	h= 0.157 m
6.1.14. Pipe Friction Loss	(Diameter 250 mm), I=	0.065	L= 26.1 m	h= 1.704 m

Sub Total

H= 6.234 m

<6.260 m

6.2. RC Pipe Loss (Sedimentation Basin → Sludge Lagoon)

6.2.1. Pipe Loss 100%	(Diameter 600 mm), I=	0.00080	L= 127.45 m	h= 0.102 m
6.2.2. Pipe Loss 100%	(Diameter 600 mm), I=	0.00080	L= 154.10 m	h= 0.123 m
6.2.3. Manhole Loss	(Diameter 600 mm)	2.0 cm	8 ps	h= 0.160 m
6.2.4. Pipe Loss 100%	(Diameter 450 mm), I=	0.00340	L= 3.64 m	h= 0.012 m
6.2.5. Outlet Loss	(Diameter 450 mm), f=	1.0	V= 1.04 m/s	h= 0.055 m

Sub Total

H= 0.452 m

7. Total Pipe Loss

H= 6.686 m

8 Sludge Lagoon Inlet Water Level 442.348 m (442.800 - 0.452) > 442.000 m OK

RC600mm Pipe Loss Calculation (Sedimentation Basin - Sludge Lagoon)

Manhole No.	Dia.	Gradient(%)	Length(ctc) (m)	Length(m)	Loss(m)			Inlet Pipe		Outlet Pipe		Water Level	Elevation Level(m)	Soil Cover Depth(m)	Manhole Depth(m)
					Pipe	Manhole	Total	Bottom Level	Top Level	Bottom Level	Top Level				
1										442.020	442.660	442.620	446.500	3.84	4.45
2	600	1.0	47.16	46.66	0.047	0.020	0.067	441.973	442.463	441.900	442.540	442.500	446.500	4.04	4.57
3	600	1.0	16.60	15.40	0.015	0.020	0.035	441.885	442.525	441.865	442.505	442.465	446.500	3.98	4.60
6	600	1.0	33.80	32.60	0.033	0.020	0.053	441.832	442.472	441.812	442.452	442.412	446.500	4.03	4.65
9	600	1.0	33.80	32.60	0.033	0.020	0.053	441.779	442.419	441.759	442.399	442.359	446.500	4.08	4.71
10	600	1.0	49.26	48.06	0.048	0.020	0.068	441.711	442.351	441.691	442.331	442.291	444.000	1.65	2.27
11	600	1.0	31.88	30.68	0.031	0.020	0.051	441.661	442.301	441.641	442.281	442.241	443.000	0.70	1.51
12	600	1.0	41.90	40.70	0.041	0.020	0.061	441.600	442.240	441.580	442.220	442.180	443.000	0.76	1.51
13	600	1.0	41.90	40.70	0.041	0.020	0.061	441.539	442.179	441.519	442.159	442.119	443.000	0.82	1.51
14	600	1.0	41.90	40.70	0.041	0.020	0.061	441.479	442.119	441.459	442.099	442.059	443.000	0.88	1.51
Inlet Mouth	450	4.5	2.5	1.65	0.007	0.000	0.007	441.451	442.091			442.051			
Total			338.19	329.74	0.289	0.160	0.449								

Note:

No.1 Manhole Water level 442.620 m (Filter Outlet Gallery Floor drain pipe center level +442.92-0.3m)

No.1 Manhole Outlet Pipe Bottom level 442.020 m (No.1 Manhole Water level +443.27 - Pipe diameter 0.60m)

No.2 Manhole Water level 442.500 m (Sedimentation Drain Pit Floor Level +443.30-0.80m)

No.2 Manhole Outlet Pipe Bottom level 441.900 m (No.2 Manhole Water level +442.50 - Pipe diameter 0.60m)

Total loss 0.449 m

() RC 450mm Outlet Pipe Top Level

RC Pipe Top Level (Bottom Level + Innerdiameter 450mm + Thickness 40mm) = 0.49 m

RC Pipe Top Level (Bottom Level + Innerdiameter 600mm + Thickness 40mm) = 0.64 m

Table of Flow Rate (Manning Formula)

$$v = (1/n) R^{2/3} I^{1/2}$$

$$q = (1/n) (\pi * D^2 / 4) R^{2/3} I^{1/2} = (\pi/4n) D^2 R^{2/3} I^{1/2}$$

$$n = 0.013$$

$$Q = 14308 \text{ m}^3/\text{d} = 0.166 \text{ m}^3/\text{s}$$

Dia	450	450	600	600	750	750	900	900
Hydraulic Gradient	V	Q	V	Q	V	Q	V	Q
0.10	0.179	0.029	0.217	0.061	0.252	0.111	0.285	0.181
0.20	0.254	0.040	0.307	0.087	0.356	0.157	0.402	0.256
0.30	0.310	0.049	0.376	0.106	0.436	0.193	0.493	0.314
0.40	0.359	0.057	0.434	0.123	0.504	0.223	0.569	0.362
0.50	0.401	0.064	0.486	0.137	0.563	0.249	0.636	0.405
0.60	0.439	0.070	0.532	0.150	0.617	0.273	0.697	0.443
0.70	0.474	0.075	0.575	0.162	0.667	0.295	0.753	0.479
0.80	0.507	0.081	0.614	0.174	0.713	0.315	0.805	0.512
0.90	0.538	0.086	0.651	0.184	0.756	0.334	0.854	0.543
1.00	0.567	0.090	0.687	0.194	0.797	0.352	0.900	0.572
1.10	0.595	0.095	0.720	0.204	0.836	0.369	0.944	0.600
1.20	0.621	0.099	0.752	0.213	0.873	0.386	0.986	0.627
1.30	0.646	0.103	0.783	0.221	0.909	0.401	1.026	0.653
1.40	0.671	0.107	0.813	0.230	0.943	0.417	1.065	0.677
1.50	0.694	0.110	0.841	0.238	0.976	0.431	1.102	0.701
1.60	0.717	0.114	0.869	0.246	1.008	0.445	1.138	0.724
1.70	0.739	0.118	0.895	0.253	1.039	0.459	1.173	0.746
1.80	0.761	0.121	0.921	0.261	1.069	0.472	1.207	0.768
1.90	0.781	0.124	0.947	0.268	1.098	0.485	1.240	0.789
2.00	0.802	0.128	0.971	0.275	1.127	0.498	1.273	0.810
2.10	0.821	0.131	0.995	0.281	1.155	0.510	1.304	0.830
2.20	0.841	0.134	1.019	0.288	1.182	0.522	1.335	0.849
2.30	0.860	0.137	1.041	0.294	1.209	0.534	1.365	0.868
2.40	0.878	0.140	1.064	0.301	1.235	0.545	1.394	0.887
2.50	0.896	0.143	1.086	0.307	1.260	0.557	1.423	0.905
2.60	0.914	0.145	1.107	0.313	1.285	0.568	1.451	0.923
2.70	0.931	0.148	1.128	0.319	1.309	0.578	1.479	0.941
2.80	0.949	0.151	1.149	0.325	1.333	0.589	1.506	0.958
2.90	0.965	0.154	1.169	0.331	1.357	0.600	1.532	0.975
3.00	0.982	0.156	1.189	0.336	1.380	0.610	1.559	0.992
3.10	0.998	0.159	1.209	0.342	1.403	0.620	1.584	1.008
3.20	1.014	0.161	1.228	0.347	1.425	0.630	1.610	1.024
3.30	1.030	0.164	1.248	0.353	1.448	0.640	1.635	1.040
3.40	1.045	0.166	1.266	0.358	1.469	0.649	1.659	1.056
3.50	1.061	0.169	1.285	0.363	1.491	0.659	1.683	1.071
3.60	1.076	0.171	1.303	0.368	1.512	0.668	1.707	1.086
3.70	1.090	0.173	1.321	0.373	1.533	0.677	1.731	1.101
3.80	1.105	0.176	1.339	0.379	1.553	0.686	1.754	1.116
3.90	1.119	0.178	1.356	0.383	1.574	0.695	1.777	1.131
4.00	1.134	0.180	1.373	0.388	1.594	0.704	1.800	1.145
4.10	1.148	0.183	1.391	0.393	1.614	0.713	1.822	1.159
4.20	1.162	0.185	1.407	0.398	1.633	0.721	1.844	1.173
4.30	1.176	0.187	1.424	0.403	1.652	0.730	1.866	1.187
4.40	1.189	0.189	1.440	0.407	1.672	0.738	1.888	1.201
4.50	1.203	0.191	1.457	0.412	1.690	0.747	1.909	1.214
4.60	1.216	0.193	1.473	0.416	1.709	0.755	1.930	1.228
4.70	1.229	0.195	1.489	0.421	1.728	0.763	1.951	1.241
4.80	1.242	0.198	1.505	0.425	1.746	0.771	1.972	1.254
4.90	1.255	0.200	1.520	0.430	1.764	0.779	1.992	1.267
5.00	1.268	0.202	1.536	0.434	1.782	0.787	2.012	1.280

12. Hydraulic Calculation of Filter - Backwash Recycle Pump House

Filter - Backwash Recycle Pump House

Manhole - Backwash Recycle Pump House (RC Pipe 600mm, DIP 600mm)

1. Filter Backwash waste water Level

H.W.L. 444.750 m (444.410 m Washwater channel bottom level)

2. Backwash Recycle Pump House Water Level

H.W.L.+ 444.010 m

L.W.L.+ 441.010 m (Effective Depth 3.0 m)

5 Inflow Flow Rate

Q1= 0.346 m³/sec = 20.74 m³/min (7.2m*9.6m*0.3m³/m²/min)

6.2. RC Pipe Loss (Filter → Backwash Recycle Pump House)

6.2.1. Pipe Loss	100%	(Diameter 600 mm), I= 0.0032	L= 6.73 m	h= 0.022 m
6.2.4. Manhole Loss		(Diameter 600 mm)	2.0 cm	1 ps h= 0.020 m
Sub Total				H= 0.042 m

6. Water Level Loss

6.1. DIP Pipe Loss (Filter → Backwash Recycle Pump House)

6.1.1. Inlet Loss	(Diameter 600 mm), f= 0.5	V= 1.22 m/s	h= 0.038 m
6.1.2. Tee Branch	(Diameter 600 mm), f= 0.05	V= 1.22 m/s	h= 0.004 m
6.1.3. 90° Bend Loss	(Diameter 600 mm), f= 0.23	V= 1.22 m/s	h= 0.017 m
6.1.4. Valve Loss	(Diameter 600 mm), f= 1.0	V= 1.22 m/s	h= 0.076 m
6.1.5. Outlet Loss	(Diameter 600 mm), f= 1.0	V= 1.22 m/s	h= 0.076 m
6.1.6. Pipe Friction Loss	(Diameter 600 mm), I= 0.004	L= 17.82 m	h= 0.064 m
Sub Total			H= 0.275 m

Total H= 0.317 m
(0.400 m)

where C= 100

Table of Flow Rate (Manning Formula)

$$v = (1/n) R^{(2/3)} I^{(1/2)}$$

$$q = (1/n) (\pi * D^2 / 4) R^{(2/3)} I^{(1/2)} = (\pi/4n) D^2 R^{(2/3)} I^{(1/2)}$$

$$n = 0.013$$

$$Q = 29851 \text{ m}^3/\text{d} = 0.346 \text{ m}^3/\text{s}$$

Hydraulic Gradient	450 V	450 Q	600 V	600 Q	750 V	750 Q	900 V	900 Q
0.10	0.179	0.029	0.217	0.061	0.252	0.111	0.285	0.181
0.20	0.254	0.040	0.307	0.087	0.356	0.157	0.402	0.256
0.30	0.310	0.049	0.376	0.106	0.436	0.193	0.493	0.314
0.40	0.359	0.057	0.434	0.123	0.504	0.223	0.569	0.362
0.50	0.401	0.064	0.486	0.137	0.563	0.249	0.636	0.405
0.60	0.439	0.070	0.532	0.150	0.617	0.273	0.697	0.443
0.70	0.474	0.075	0.575	0.162	0.667	0.295	0.753	0.479
0.80	0.507	0.081	0.614	0.174	0.713	0.315	0.805	0.512
0.90	0.538	0.086	0.651	0.184	0.756	0.334	0.854	0.543
1.00	0.567	0.090	0.687	0.194	0.797	0.352	0.900	0.572
1.10	0.595	0.095	0.720	0.204	0.836	0.369	0.944	0.600
1.20	0.621	0.099	0.752	0.213	0.873	0.386	0.986	0.627
1.30	0.646	0.103	0.783	0.221	0.909	0.401	1.026	0.653
1.40	0.671	0.107	0.813	0.230	0.943	0.417	1.065	0.677
1.50	0.694	0.110	0.841	0.238	0.976	0.431	1.102	0.701
1.60	0.717	0.114	0.869	0.246	1.008	0.445	1.138	0.724
1.70	0.739	0.118	0.895	0.253	1.039	0.459	1.173	0.746
1.80	0.761	0.121	0.921	0.261	1.069	0.472	1.207	0.768
1.90	0.781	0.124	0.947	0.268	1.098	0.485	1.240	0.789
2.00	0.802	0.128	0.971	0.275	1.127	0.498	1.273	0.810
2.10	0.821	0.131	0.995	0.281	1.155	0.510	1.304	0.830
2.20	0.841	0.134	1.019	0.288	1.182	0.522	1.335	0.849
2.30	0.860	0.137	1.041	0.294	1.209	0.534	1.365	0.868
2.40	0.878	0.140	1.064	0.301	1.235	0.545	1.394	0.887
2.50	0.896	0.143	1.086	0.307	1.260	0.557	1.423	0.905
2.60	0.914	0.145	1.107	0.313	1.285	0.568	1.451	0.923
2.70	0.931	0.148	1.128	0.319	1.309	0.578	1.479	0.941
2.80	0.949	0.151	1.149	0.325	1.333	0.589	1.506	0.958
2.90	0.965	0.154	1.169	0.331	1.357	0.600	1.532	0.975
3.00	0.982	0.156	1.189	0.336	1.380	0.610	1.559	0.992
3.10	0.998	0.159	1.209	0.342	1.403	0.620	1.584	1.008
3.20	1.014	0.161	1.228	0.347	1.425	0.630	1.610	1.024
3.30	1.030	0.164	1.248	0.353	1.448	0.640	1.635	1.040
3.40	1.045	0.166	1.266	0.358	1.469	0.649	1.659	1.056
3.50	1.061	0.169	1.285	0.363	1.491	0.659	1.683	1.071
3.60	1.076	0.171	1.303	0.368	1.512	0.668	1.707	1.086
3.70	1.090	0.173	1.321	0.373	1.533	0.677	1.731	1.101
3.80	1.105	0.176	1.339	0.379	1.553	0.686	1.754	1.116
3.90	1.119	0.178	1.356	0.383	1.574	0.695	1.777	1.131
4.00	1.134	0.180	1.373	0.388	1.594	0.704	1.800	1.145
4.10	1.148	0.183	1.391	0.393	1.614	0.713	1.822	1.159
4.20	1.162	0.185	1.407	0.398	1.633	0.721	1.844	1.173
4.30	1.176	0.187	1.424	0.403	1.652	0.730	1.866	1.187
4.40	1.189	0.189	1.440	0.407	1.672	0.738	1.888	1.201
4.50	1.203	0.191	1.457	0.412	1.690	0.747	1.909	1.214
4.60	1.216	0.193	1.473	0.416	1.709	0.755	1.930	1.228
4.70	1.229	0.195	1.489	0.421	1.728	0.763	1.951	1.241
4.80	1.242	0.198	1.505	0.425	1.746	0.771	1.972	1.254
4.90	1.255	0.200	1.520	0.430	1.764	0.779	1.992	1.267
5.00	1.268	0.202	1.536	0.434	1.782	0.787	2.012	1.280

13. Hydraulic Calculation of Connection Pipe between Backwash Recycle Pump - Receiving Well

Backwash Recycle Pump - Receiving Well

1. Filter Backwash waste water Level

L.W.L. 440.130 m (444.13 m Washwater channel bottom level)

2. Receiving Well Water level

W.L.+ 451.200 m

3. Actual Pump Head

11.070 m

5 Recycle Flow

Q1= 0.104 m³/sec = 6.22 m³/min

6. Water Level Loss

6.1. RC Pipe Loss (Sedimentation Basin → Sludge Lagoon)

6.1.1.	45° Bend Loss	(Diameter 250 mm), f=	0.16	V=	2.11 m/s	h=	0.037 m
6.1.2.	45° Bend Loss	(Diameter 250 mm), f=	0.16	V=	2.11 m/s	h=	0.037 m
6.1.3.	45° Bend Loss	(Diameter 250 mm), f=	0.16	V=	2.11 m/s	h=	0.037 m
6.1.4.	45° Bend Loss	(Diameter 250 mm), f=	0.16	V=	2.11 m/s	h=	0.037 m
6.1.5.	90° Bend Loss	(Diameter 250 mm), f=	0.23	V=	2.11 m/s	h=	0.052 m
6.1.6.	Outlet Loss	(Diameter 250 mm), f=	1.0	V=	2.11 m/s	h=	0.227 m
6.1.7.	Pipe Friction Loss	(Diameter 250 mm), f=	0.027	L=	103.48 m	h=	2.844 m
	Sub Total					H=	3.271 m

where C= 100

14.Receiving Well Overflow Weir

1 Overflow weir loss (2 line duty)

$$h=(Q/(1.84*b))^{2/3}$$

where $Q=$

$$1.375 \text{ m}^3/\text{sec} \quad (110000*(1.05+0.03)/86400)$$

$b=$

$$4.00 \text{ m}$$

$$h=(Q/(1.84*b))^{2/3}=$$

$$0.327 \text{ m}$$

4 Water loss

The water level of Receiving well is 451.680 m

The height of the overflow weir is 451.900 m

The water level of upstream of the weir is 452.230 m (0.327)

The water loss of downstream of the weir is 4.570 m.

Therefore the water loss (total) is 4.897 m

The water level at the downstream of the weir (overflow chamber) is 447.330 m

15. Hydraulic Calculation of Overflow from Receiving Well

1. Water Level at Inlet Chamber of Distribution Chamber

Overflow Water Level 452.330 m (452.00 + 0.33)

2. Top Level of Overflow Weir

H.W.L. 452.000 m

3. Water Level at Downstream of Overflow Weir

H.W.L. 451.800 m (452.00 m Top Level of Overflow Weir. Allowance is 0.20 m)

4. Overflow Pipe Center Level at Blowoff Point

W.L.+ 442.930 m (446.50 m WTP site Elevation Level, Soil Cover 2.2m)

5. Water Loss

8.870 m (451.800 - 442.930 = 8.870 m > 3.933 m OK)

6 Intake Flow & Velocity

Q1= 1.375 m³/sec = 118800.00 m³/day (110000*(1.05+0.03))

7. Water Level Loss

7.1.1. Inlet Loss	(Diameter 600	mm), f= 0.5	V= 4.87 m/s	h= 0.605 m
7.1.2. Valve Loss	θ=5° (Diameter 600	mm), f= 0.3	V= 4.87 m/s	h= 0.363 m
7.1.3. 45°Bend Loss	(Diameter 600	mm), f= 0.16	V= 4.87 m/s	h= 0.197 m
7.1.4. 45°Bend Loss	(Diameter 600	mm), f= 0.16	V= 4.87 m/s	h= 0.197 m
7.1.5. 90°Bend Loss	(Diameter 600	mm), f= 0.23	V= 4.87 m/s	h= 0.278 m
7.1.6. Outlet Loss	(Diameter 600	mm), f= 1.0	V= 4.87 m/s	h= 1.210 m
7.1.7. Pipe Friction Loss	(Diameter 600	mm), I= 0.046	L= 23.47 m	h= 1.083 m
Sub Total				H= 3.933 m

where C= 100

16. Hydraulic Calculation of Overflow from Clear Water Reservoir

Overflow from Clear Water Reservoir
Clear Water Reservoir - Drainage Point

1. Water Level at Clear Water Reservoir

H.W.L. 445.820 m

2. Small Stream

W.L.+ 441.820 m

Stream Bed Level 441.320 m

3. Pipe Bottom Level at Drainage Point

442.090 m (RC Pipe Bottom Level at starting point + 444.525)
(Small Stream Bottom Level + 441.323)

5 Overflow Flow Rate

Q1=	0.212 m3/sec =	18333 m3/day	(110000/6)
Q2=	0.424 m3/sec =	36667 m3/day	(110000/6*2)
Q3=	0.637 m3/sec =	55000 m3/day	(110000/6*3)
Q4=	0.849 m3/sec =	73333 m3/day	(110000/6*4)
Q5=	1.061 m3/sec =	91667 m3/day	(110000/6*5)
Q6=	1.273 m3/sec =	110000 m3/day	(110000/6*6)

6.1. DIP Pipe Loss (Sedimentation Basin → Sludge Lagoon)

6.1.1. Inlet Loss	(Diameter 350	mm), f=	0.5	V=	2.21 m/s	h=	0.125 m
6.1.2. 90° Bend Loss	(Diameter 350	mm), f=	0.20	V=	2.21 m/s	h=	0.050 m
6.1.3. Outlet Loss	(Diameter 350	mm), f=	1.0	V=	2.21 m/s	h=	0.249 m
6.1.4. Pipe Friction Loss	(Diameter 350	mm), I=	0.020	L=	2.82 m	h=	0.057 m
Sub Total						H=	0.481 m

6.2. RC Pipe Loss (Sedimentation Basin → Sludge Lagoon)

6.2.1. Pipe Loss	100%	(Diameter 450	mm), I=	0.013	L=	13.70 m	h=	0.178 m
6.2.2. Pipe Loss	100%	(Diameter 600	mm), I=	0.011	L=	18.60 m	h=	0.205 m
6.2.3. Pipe Loss	100%	(Diameter 750	mm), I=	0.008	L=	13.20 m	h=	0.106 m
6.2.4. Pipe Loss	100%	(Diameter 750	mm), I=	0.014	L=	6.80 m	h=	0.095 m
6.2.5. Pipe Loss	100%	(Diameter 750	mm), I=	0.010	L=	13.20 m	h=	0.132 m
6.2.6. Pipe Loss	100%	(Diameter 750	mm), I=	0.030	L=	5.00 m	h=	0.150 m
6.2.7. Pipe Loss	100%	(Diameter 750	mm), I=	0.030	L=	22.95 m	h=	0.689 m
6.2.8. Pipe Loss	100%	(Diameter 1050	mm), I=	0.005	L=	132.80 m	h=	0.664 m
6.2.9. Manhole Loss		(Diameter 450 - 1050	mm)	2.0	cm	11 ps	h=	0.220 m

Sub Total H= 2.439 m

7. Total Pipe Loss

H= 2.920 m

where C= 100

Pipe Loss Calculation for Clear Water Reservoir Overflow Pipe (RCP450 - 1050mm)

Manhole No.	Dia.	Pipe Thickness	Gradient (%)	Length(m)	Loss(m)			Inlet Pipe		Outlet Pipe		Manhole Depth (m)	Water Level (m)	Elevation Level (m)	Soil Cover Depth (m)	Manhole Distance (ctc)
					Pipe	Manhole	Total	Bottom Level	Top Level	Bottom Level	Top Level					
1										444.500	444.990	1.96	444.950	446.500	1.51	
2	450	40	13	13.10	0.170	0.020	0.190	444.330	444.820	444.310	444.800	2.16	444.760	446.500	1.68	14.20
3	600	40	11	18.50	0.204	0.020	0.224	444.106	444.746	444.086	444.726	2.37	444.536	446.500	1.75	19.70
4	750	50	8	13.00	0.104	0.020	0.124	443.982	444.782	443.962	444.762	2.49	444.412	446.500	1.72	14.20
5	750	50	14	6.70	0.094	0.020	0.114	443.868	444.668	443.848	444.648	2.61	444.298	446.500	1.83	7.90
6	750	50	21	13.00	0.273	0.020	0.293	443.575	444.375	443.555	444.355	2.90	444.005	446.500	2.12	14.20
7	750	50	30	5.55	0.167	0.020	0.187	443.389	444.189	443.369	444.169	3.09	443.819	446.500	2.31	6.75
8	750	50	30	22.84	0.685	0.020	0.705	442.684	443.484	442.664	443.464	3.78	443.114	446.500	3.02	24.19
9	1050	60	4.9	47.85	0.234	0.020	0.254	442.429	443.539	442.409	443.519	4.04	442.859	446.500	2.96	49.35
10	1050	60	4.9	18.75	0.092	0.020	0.112	442.317	443.427	442.297	443.407	4.15	442.747	446.500	3.07	20.25
Small Steam	1050	60	4.9	40.49	0.198		0.198	442.099	443.209				442.549	446.500	3.29	41.24
Total				199.78	2.221	0.180	2.401									211.98

Note: No.1 Manhole Water level 444.950 m (Overflow pipe bottom Level +444.975m)
 No.1 Manhole Outlet Pipe Bottom level 444.500 m (No.1 Manhole Water level +444.950 - Pipe diameter 0.45m)
 Manhole Depth (m) 446.50-(Outlet Pipe Bottom Level)-(Pipe Thickness)
 Total loss 2.401 m

03 Transmission System Calculations

Transmission System Calculation

1. Basic Conditions

The following data/ conclusions/ information was also incorporated in the hydraulic calculation of the pipelines.

Pipeline Data:

The data such as the length, elevation of the existing and new pipelines, together with the type and diameter of the existing ones were collected during the topographical surveys.

High and Low Water Levels of Service Reservoirs (existing and new):

This information was tabulated in Table TM-1.

The Quantity of Flow to each Service Reservoir:

Maximum day demand (m^3/d) was assessed and tabulated in Figure TM-1 for each of the three Phases separately.

Peak Factors:

The peak factor (maximum daily demand to the daily average demand) is assumed to be 1.2.

2. Pipe Materials

For diameters 250mm and larger Ductile Cast Iron (DI) pipes, and for diameters less than 250mm, Unplasticized Polyvinyl Chloride (U-PVC) pipes were basically applied.

DI Pipes:

Straight Pipe -----K=9

Tees -----K=14

Other fittings -----K=12

U-PVC Pipes:

The pipes shall have a minimum working pressure of 10kgf/sq.m or 10 bars for type 1000 pipes, at a temperature of 29°C.

3. Hydraulic Design

Pipelines will be sized using the exponential equation developed by Hazen and Williams shown below in metric units.

$$H = 10.666 \times C^{-1.85} \times D^{-4.87} \times Q^{1.85} \times L$$

- Where, H: friction loss (m)
C: friction coefficient
D: diameter of pipe (m)
Q: rate of flow (m³/sec)
L: Pipe length (m)

Pipelines will be sized using the same Hazen Williams friction coefficient (C) as indicated in Table TM-3.

Table TM-3 Pipe Friction Coefficients

Pipe Material	Existing or New	Friction Coefficient (C)
Cast Iron	Existing	90
u-PVC, ACP	Existing	120
Ductile Iron	New	140
u-PVC	New	140

The appropriate flow velocity shall be taken as economical and reasonable velocity (approximately 1.0 m/sec). Residual pressure of hydraulic grade line at inlet to the Service Reservoir shall be more than 5m.

Table TM-1 Water Level of Service Reservoir

Node No.	Name of the site	Water Level (m)				Capacity (m3)	
		Existing		Proposed		Existing	Proposed
		LWL	HWL	LWL	HWL		
10	Akurana	508.00	512.00			600	
60	Ampitiya	582.50	586.00			900	
AG	Asgiriya			561.50	567.00		4,100
IB	Asgiriya P.S						
57	Bahirawakanda	619.10	620.90	625.00	629.00	204	600
500	Balanagala	513.00	515.00			450	
26	Bangalawatta	519.28	521.28	518.28	521.28		300
66	Dangolla	529.90	531.60	527.60	531.60	118	500
60E	Elhena			611.00	615.00		300
65	Gohagoda (Pallemulla New)			527.20	531.20		200
65	Gohagoda (Pallemulla Old)	521.90	524.10			150	
65G	Gohagoda (Wegiriya)	524.00	528.00			150	
61S	Hantana Place			637.00	641.00		200
54	Heerassagala Low			566.00	570.00		200
55	Heerassagala Middle			613.00	617.00		250
56	Heerassagala Upper			674.00	678.00		200
3	Kahalla			485.00	491.25		600
6	Kahawatta			516.00	522.25		600
5	Kondadeniya	531.25	535.25	531.25	535.25	300	200
-	Kondadeniya Sump.						
14	Kulugamma	579.25	583.25	579.25	583.25	300	100
7	Kurugoda			569.00	573.00		600
60'	Mullepihilla Low Old	672.50	674.36			25	
60+	Mullepihilla Low New			709.00	713.00		100
25	Pihilladeniya	522.14	524.14	522.14	524.14	100	200
582	R2 (KMC)	549.49	555.00			3,636	
8	Thelambugahawatta			561.50	566.75		500
17	Uplands	556.51	558.34	560.09	566.00	27	2,960

(Phase 1)

Node	Node --->	B/G	Flow Rate Q (m3/d)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (%)	Loss h (m)	Dynamic Pressure	LWL HWL	Dynamic Pressure	Pump Type	Required Pump Head	Remark
60	60E-1	B	400	199	199		260	130	0.149	0.163	0.042	620.700	582.500	38.200	B	38.2	PVC
60E-1	60E-2		400	201	201		3,100	130	0.146	0.156	0.482	620.658	555.170	66.488			DIP
60E-2	60E (= Elhena)		400	199	199		520	130	0.149	0.163	0.085	620.175	555.620	64.555			PVC
60	6005	B	580	149	149		1,480	130	0.385	1.329	1.967	720.900	582.500	138.400	B	138.4	DIP
6005	60+ (= Mullpihilla)	B	580	141	141		480	130	0.430	1.739	0.835	718.933	648.760	70.173			PVC
60+	60+1	G	60	141	141		100	130	0.044	0.026	0.003	709.000	709.000	0.000			PVC
60+1	60' (= Mullpihilla (Low))		60	79	79		190	130	0.142	0.439	0.083	708.997	664.330	44.667			PVC
60'	60' (= Mullpihilla (Upper))	B	60	66	66	K	1,400	120	0.203	1.223	1.712	708.914	674.360	34.554			
60	6003	B	1,250	141	141	K	1,500	120	0.927	8.347	12.521	737.800	672.500	65.300	B	65.3	Exist Pipe ϕ 75
6003	60M (= Meekanuwa)	(B)	1,250	141	141	K	485	120	0.927	8.347	4.048	736.088	731.000	5.088			
	Katugastota	Madawala										656.600	582.500	74.100			
PG	601	B	14,390	603	603		650	130	0.583	0.558	0.363	532.580	442.680	89.900	B	89.9	
601	5001	(B)	3,780	603	603		1,790	130	0.153	0.047	0.084	532.217	444.020	88.197			
5001	5002	(B)	2,480	299	299		1,250	130	0.409	0.657	0.822	532.133	442.250	89.883			
5002	5003	(B)	2,480	299	299		2,280	130	0.409	0.657	1.499	531.311	450.000	81.311			
5003	25-1	(B)	1,060	201	201		410	130	0.387	0.944	0.387	529.812	455.220	74.592			DI
25-1	25 (= Pihilladeniya)		1,060	199	199		220	130	0.394	0.991	0.218	529.425	455.200	74.225			PVC
601	601'	(B)	10,620	603	603		890	130	0.430	0.318	0.283	529.207	524.140	5.067			
601'	3 (= Kahalla)	(B)	1,680	199	199		870	130	0.625	2.323	2.021	532.217	444.020	88.197			
												531.934	443.000	88.934			
												530.196	491.250	38.946			

(Phase 1)

Node	Node --->	B/G	Flow Rate Q (m3/d)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (‰)	Loss h (m)	Dynamic Pressure	LWL HWL	Dynamic Pressure	Pump Type	Required Pump Head	Remark
	5001											532.133	442.250	89.883			
5001	- 500	(B)	1,310	199	199	K	1,200	120	0.487	1.700	2.040	530.093	514.350	15.743			Exist Pipe ϕ 225
	500		= Balanagala														
	5003											529.812	465.220	74.592			
5003	- 26'	(B)	1,420	299	299		190	130	0.234	0.234	0.046	529.767	456.990	72.777			
	26'																
	26'	(B)	1,420	252	252		1,150	130	0.330	0.539	0.620	529.148	521.280	7.868			
	26'		= Bangalawatta														
	Katugastota		--> Kahawatta														
	601'											531.934	443.000	88.934			
601'	- 603	(B)	8,940	502	502		3,700	130	0.523	0.565	2.091	529.843	499.600	30.243			
	603																
603	- 6	(B)	6,600	502	502		50	130	0.386	0.322	0.016	529.826	522.250	7.576			
	6		= Kahawatta														
	603											529.826	499.600	30.226			
603	- 10	(B)	2,340	199	199		1,250	130	0.871	4.288	5.360	524.466	512.000	12.466			
	10		= Akurana														
	6											580.550	518.250	62.300			
6	- 7'	B	4,240	350	350		2,500	130	0.510	0.824	2.059	578.491	455.030	123.461	B	62.3	
	7'																
	7'	(B)	2,410	350	350		1,400	130	0.290	0.290	0.405	578.086	573.000	5.086			
	7'		= Kurugoda														
	7'											578.491	455.030	123.461			
7'	- 8	(B)	1,840	252	252		950	120	0.427	1.009	0.959	577.532	566.750	10.782			
	8		= Thelambugawatta														
	Katugastota		--> Kondadeniya, Kurugammana														
	PG											546.780	442.680	104.100			
PG	- 5"	B	4,710	350	350		520	130	0.567	1.000	0.520	546.260	468.410	77.850	B	104.1	
	5"																
5"	- 5" a	(B)	2,760	299	299		890	130	0.455	0.801	0.713	545.547	505.180	40.367			
	5" a																
5" a	- 5	(B)	2,760	184	184	K	520	120	1.208	10.012	5.206	545.547	535.250	10.297			Exist Pipe ϕ 160x2
	5		= Kondadeniya														
	5											598.550	531.250	67.300			
5	- K1	B	1,050	141	141	K	1,525	120	0.778	6.046	9.220	589.330	535.000	54.330	B	67.3	Exist Pipe ϕ 160 PVC
	K1																
K1	- K2	(B)	1,500	199	199	K	350	120	0.558	2.184	0.765	588.565	550.000	38.565			Exist Pipe ϕ 225 PVC
	K2																
K2	- 14	(B)	1,500	201	201	K	106	120	0.547	2.081	0.221	588.345	583.250	5.095			Exist Pipe ϕ 200 DI
	14		= Kurugammana														

(Phase 1)

Node	Node →	Node	B/G	Flow Rate Q (m ³ /d)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (‰)	Loss h (m)	Dynamic Pressure	LWL HWL	Dynamic Pressure	Pump Type	Required Pump Head	Remark
	Katugastota	→	KFG, R2															
PG	-	MR	B	17,600	802	802		650	130	0.403	0.202	0.131	572.780	442.680	130.100			
MR	-	17'	(B)	17,600	700	700		570	130	0.529	0.392	0.223	572.649	442.770	129.879	B	130.1	
17'	-	AG'	(B)	13,210	700	700		830	130	0.397	0.231	0.191	572.425	453.650	118.775			
AG'	-	AG	(B)	11,240	502	502		230	130	0.657	0.863	0.199	572.234	527.400	44.834			
	AG	=	Asgiriya										572.035	567.000	5.035			
AG'	-	(IB)	(B)	1,970	502	502		430	130	0.115	0.034	0.015	572.234	527.400	44.834			
(IB)	-	57	B	1,970	252	252		1,900	130	0.457	0.988	1.877	572.219	530.630	41.589			
	57	=	Bahirawakand										634.043	629.000	5.043	B	63.7	
17'	-	1702	(B)	4,390	395	395		2,000	130	0.415	0.487	0.975	572.425	453.650	118.775			
1702	-	17	(B)	4,390	395	395		70	130	0.415	0.487	0.034	571.451	545.000	26.451			
	17	=	Uplands										571.417	566.000	5.417			
	Katugastota	→	Gohagoda (Pallemitla)															
5"	-	65'	(B)	1,950	252	252		950	130	0.453	0.969	0.921	546.260	488.410	77.850			
65'	-	6501	(B)	1,050	201	201		1,720	130	0.383	0.927	1.595	545.339	490.310	55.029			
6501	-	65	(B)	1,050	201	201	K	90	130	0.383	0.927	0.083	543.744	506.600	37.144			
	65	=	Gohagoda										543.660	531.200	12.460			
65'	-	65G	(B)	900	149	149	K	100	120	0.597	3.475	0.347	545.339	490.310	55.029			
	65G	=	Gohagoda (old)										544.992	528.000	16.992			Exist Pipe ϕ 200

(Phase 2)

Node	Node -->	Node	B/G	Flow Rate Q (m3/d)	Dia. D (mm)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (%)	Loss h (m)	Dynamic Pressure Hd (MSL)	LWL	Dynamic Pressure He (m)	Pump Type	Required Pump Head H (m)	Remark
															HWL (MSL)				
		KMC-Primrose																	
		KMC												642.800	471.000	171.800			
KMC	-	63	B	2,300	0	201	201	K	500	120	0.839	4.588	2.294	640.506	635.500	5.006	B	171.8	Exist Pipe ϕ 200
		63																	
		KMC-Ellyagama																	
		KMC												557.800	471.000	86.800			
KMC	-	36'	B	9,000	0	502	502		2,000	130	0.526	0.572	1.144	556.656	480.000	76.656	B	86.8	
		36'																	
36'	-	36	(B)	9,000	0	350	350		2,000	130	1.083	3.314	6.629	550.027	545.000	5.027			Exist Pipe ϕ 450
		36																	
		KMC-KFG																	
		KMC												575.800	471.000	104.800			
KMC	-	5401	B	19,280	0	502	502	K	200	120	1.127	2.716	0.543	575.257	480.000	95.257	B	104.8	Exist Pipe ϕ 500
		5401																	
5401	-	54'	B	19,280	0	502	502	K	1,000	120	1.127	2.716	2.716	572.540	485.000	87.540			Exist Pipe ϕ 500
		54'																	
54'	-	57'	(B)	14,520	0	502	502	K	1,800	120	0.849	1.608	2.894	569.647	500.000	69.647			Exist Pipe ϕ 500
		57'																	
57'	-	582	(B)	14,520	0	502	502	K	1,400	120	0.849	1.608	2.251	567.396	555.000	12.396			Exist Pipe ϕ 500
		582																	
		KMC												542.100	471.000	71.100			
KMC	-	66	B	2,830	199	0	199		900	130	1.053	6.096	5.486	536.614	531.600	5.014	B	71.1	
		66																	
		54'												572.540	485.000	87.540			
54'	-	54	(B)	4,760	350	0	350		1,050	130	0.573	1.020	1.071	571.469	570.000	1.469			
		54																	
54	-	54a	B	2,350	201	0	201		870	130	0.857	4.117	3.582	627.400	566.000	61.400	B	61.4	DIP
		54a																	
54a	-	55	B	2,350	199	0	199		400	130	0.874	4.322	1.729	623.818	576.330	47.488			PVC
		55																	
		55	= Heeressagala (Middle)											622.089	617.000	5.089			
		55																	
55	-	55a	B	550	149	0	149		350	130	0.365	1.205	0.422	684.200	613.000	71.200	B	71.2	DIP
		55a																	
55a	-	56	B	550	141	0	141		470	130	0.408	1.576	0.741	683.778	636.350	47.428			PVC
		56																	
		56	= Heeressagala (Upper)											683.037	678.000	5.037			
		KMC-R2-KFG																	
		582												624.290	549.490	74.800			
582	-	583	B	8,230	0	328	328	K	500	120	1.127	4.469	2.235	622.055	617.000	5.055	B	74.8	Exist Pipe ϕ 250 \times 2
		583																	

(Phase 2)

Node	Node ---	Node	B/G	Flow Rate Q (m ³ /d)	Dia. D (mm)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (%)	Loss h (m)	Dynamic Pressure Hd (MSL)	LWL	Dynamic Pressure He (m)	Pump Type	Required Pump Head H (m)	Remark
															(MSL)				
		582			2,005	2,010								647.590	549.490	98.100			
582	-	61S	B	1,490	201	0	201		860	130	0.543	1.772	1.524	646.066	641.000	5.066	B	98.1	
		61S												684.200	637.000	47.200			
61S	-	61	B	390	0	199	199	K	900	120	0.145	0.181	0.163	684.037	679.000	5.037	B	47.2	Exist Pipe ϕ 225
		61												679.000	675.000	4.000			
61	-	61H	G	380	0	141	141		1,700	130	0.282	0.795	1.352	677.648	660.000	17.648			
		61H												775.100	675.000	100.100			
61	-	HT	B	130	0	141	141		710	130	0.096	0.109	0.078	775.022	770.000	5.022	B	100.1	
		HT												617.000	613.000	4.000			
		583												616.111	560.000	56.111			
583	-	6001	G	4,070	0	299	299		541	130	0.671	1.644	0.889	613.967	571.450	42.517			
		6001												610.991	586.000	24.991			
6001	-	6002 (G)	(G)	4,070	0	299	299		1,304	130	0.671	1.644	2.144	621.200	582.500	38.700			
		6002												621.118	555.170	65.948			
6002	-	60	(G)	4,070	299	0	299		1,810	130	0.671	1.644	2.976	620.190	555.620	64.570			
		60												620.026	615.000	5.026			
60	-	60E-1	B	570	199	0	199		260	130	0.212	0.314	0.082	723.200	582.500	140.700	B	140.7	PVC
		60E-1												719.551	648.760	70.791			DIP
60E-1	-	60E-2		570	201	0	201		3,100	130	0.208	0.300	0.929	620.190	555.620	64.570			
		60E-2												620.026	615.000	5.026			PVC
60E-2	-	60E (= Elhena)		570	199	0	199		520	130	0.212	0.314	0.164	709.000	709.000	0.000			
		60												708.996	664.330	44.666			
60	-	6005	B	810	149	0	149		1,480	130	0.538	2.466	3.649	718.002	713.000	5.002			
		6005												708.853	674.360	34.493			
6005	-	60+ (B)	(B)	810	141	0	141		480	130	0.600	3.226	1.548	708.853	674.360	34.493			
		60+												739.000	672.500	66.500			
60+	-	60+		80	141	0	141		100	130	0.059	0.045	0.004	736.085	731.000	5.085			
		60+												708.853	674.360	34.493			
60+	-	60+1	G	80	141	0	141		100	130	0.059	0.045	0.004	708.853	674.360	34.493			
		60+1												739.000	672.500	66.500			
60+1	-	60' (= Mullpihilla (Low))		80	79	0	79		190	130	0.189	0.748	0.142	739.000	672.500	66.500			
		60'												736.085	731.000	5.085			
60'	-	60''	B	80	0	66	66	K	1,400	120	0.271	2.082	2.915	736.085	731.000	5.085	B	66.5	Exist Pipe ϕ 75
		60''																	

(Phase 2)

Node	Node	B/G	Flow Rate Q (m ³ /d)	Dia. D (mm)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (‰)	Loss h (m)	Dynamic Pressure Hd (MSL)	LWL HWL (MSL)	Dynamic Pressure He (m)	Pump Type	Required Pump Head H (m)	Remark
60	6003	B	1,770	0	141	184	K	1,500	120	0.774	4.401	6.602	648.800	582.500	66.300	B	66.3	Exist Pipe φ160
6003	60M	(B)	1,770	0	141	184	K	485	120	0.774	4.401	2.135	642.198	600.000	42.198			Exist Pipe φ160
Katugastota-Madawala																		
PG	601	B	29,160	603	0	603		650	130	1.182	2.062	1.341	537.180	442.680	94.500	B	94.5	
601	5001	(B)	17,900	603	0	603		1,790	130	0.725	0.836	1.497	535.839	444.020	91.819			
5001	5002	(B)	16,100	299	603	638		1,250	130	0.584	0.524	0.655	534.343	442.250	92.093			
5002	5003	(B)	4,400	299	0	299		2,280	130	0.725	1.899	4.330	533.688	450.000	83.688			
5003	26'	(B)	3,200	299	0	299		190	130	0.527	1.054	0.200	529.358	455.220	74.138			
26'	26		3,200	252	0	252		1,150	130	0.743	2.423	2.787	529.158	456.990	72.168			
26	= Bangalawatta												526.372	521.280	5.092			
601	601'	(B)	11,260	603	0	603		890	130	0.456	0.355	0.316	535.839	444.020	91.819			
601'	3	(B)	2,190	199	0	199		870	130	0.815	3.794	3.301	535.524	443.000	92.524			
3	(= Kahalla)												532.223	491.250	40.973			
5001	500	(B)	1,800	199	0	199	K	1,200	120	0.670	3.061	3.673	534.343	440.000	94.343			
26	27'	B	1,600	0	199	199		1,300	130	0.595	2.123	2.759	530.670	514.350	16.320			
27'	27	(B)	200	0	79	79		2,700	130	0.472	4.075	11.002	575.780	517.280	58.500	B	58.5	
27													573.021	456.990	116.031			
27'	28	(B)	1,400	0	141	141		1,400	130	1.038	8.878	12.429	562.018	557.000	5.018			
28													573.021	470.000	103.021			
5003	25-1	(B)	1,200	201	0	201		410	130	0.438	1.187	0.487	560.692	550.000	10.592			
25-1	25		1,200	199	0	199		220	130	0.447	1.247	0.274	529.358	455.220	74.138			
25	= Pihilladeniya												528.871	455.200	73.671			
													528.597	524.140	4.457			

(Phase 2)

Node	Node	Node	B/G	Flow Rate Q (m ³ /d)	Dia. D (mm)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (%)	Loss h (m)	Dynamic Pressure Hd (MSL)	LWL	Dynamic Pressure He (m)	Pump Type	Required Pump Head H (m)	Remark
															HWL (MSL)				
Katugastota-Kahawatta																			
601'	-	603	(B)	9,070	502	0	502		3,700	130	0.530	0.581	2.148	535.839	443.000	92.839			
603	-	6	(B)	6,700	502	0	502		50	130	0.392	0.331	0.017	533.692	499.600	34.092			
603	-	10	G	2,370	199	0	199		1,250	130	0.882	4.391	6.488	533.692	499.600	34.092			
6	-	7'	B	4,330	350	0	350		2,500	130	0.521	0.856	2.140	580.650	518.250	62.400	B	62.4	
7'	-	7	(B)	2,450	350	0	350		1,400	130	0.295	0.299	0.418	578.510	455.030	123.480			
7'	-	8	(B)	1,890	252	0	252		950	130	0.439	0.915	0.869	578.510	455.030	123.480			
Katugastota-Uduwala																			
PG	-	5'	B	6,000	0	400	400		700	130	0.553	0.817	0.572	580.108	450.000	130.108	B	138.0	
5'	-	1301	(B)	6,000	0	400	400		1,200	130	0.553	0.817	0.980	579.128	470.000	109.128			
1301	-	14'	(B)	4,000	0	299	299		3,420	130	0.659	1.592	5.445	573.683	560.000	13.683			
14'	-	17N	(B)	4,000	0	299	299		2,300	130	0.659	1.592	3.662	570.021	565.000	5.021			
Katugastota-Kondadeniya, Kurugamana																			
PG	-	5"	B	4,990	350	0	350		520	130	0.600	1.113	0.579	547.180	442.680	104.500	B	104.5	
5"	-	5'a	(B)	2,850	299	0	299		890	130	0.470	0.850	0.757	546.601	468.410	78.191			
5'a	-	5	(B)	2,850	184	0	184	K	520	120	1.247	10.625	5.525	545.844	505.180	40.664			Exist Pipe ϕ 160x2
5	-	K1	B	1,100	0	141	141	K	1,525	120	0.815	6.589	10.049	545.844	535.250	10.594			
K1	-	K2	(B)	1,550	0	199	199	K	350	120	0.577	2.321	0.812	599.350	531.250	68.100	B	68.1	Exist Pipe ϕ 160 PVC
K2	-	14	(B)	1,550	0	201	201	K	106	120	0.565	2.211	0.234	589.301	535.000	54.301			Exist Pipe ϕ 225 PVC
K1	-	14	(B)	1,550	0	201	201	K	106	120	0.565	2.211	0.234	588.489	550.000	38.489			Exist Pipe ϕ 200 DI
Katugastota-KPG, R2																			
PG	-	MR	B	33,190	802	0	802		650	130	0.760	0.653	0.425	576.680	442.680	134.000	B	134.0	
MR	-	17'	(B)	33,190	700	0	700		570	130	0.998	1.267	0.722	576.255	442.770	133.485			
17'	-	AG'	(B)	22,750	700	0	700		830	130	0.684	0.630	0.523	575.533	453.650	121.883			
AG'	-	AG	(B)	19,610	502	0	502		230	130	1.147	2.417	0.566	575.010	527.400	47.610			
AG	-													574.454	567.000	7.454			

(Phase 2)

Node	Node --->	Node	B/G	Flow Rate Q (m ³ /d)	Dia.	Dia.	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (‰)	Loss h (m)	Dynamic Pressure Hd (MSL)	LWL	Dynamic Pressure He (m)	Pump Type	Required Pump Head H (m)	Remark
					D (mm)	D (mm)									HWL (MSL)				
	AG'				2,005	2,010													
AG'	-	(IB)	(B)	3,150	502	0	502		430	130	0.184	0.082	0.035	575.010	527.400	47.610	(B)		
(IB)	-	57	B	2,150	252	0	252		1,900	130	0.499	1.161	2.206	574.975	530.630	44.345	B	61.3	
	57													634.069	629.000	5.069			
	(IB)													574.975	530.630	44.345			
(IB)	-	582	(B)	1,000	0	502	502		3,050	130	0.058	0.010	0.030	574.945	555.000	19.945			
	582													574.945	555.000	19.945			
	17'													575.533	453.650	121.883			
17'	-	1702	(B)	10,440	400	0	400		2,000	130	0.962	2.276	4.552	570.980	545.000	25.980			
	1702													570.980	545.000	25.980			
1702	-	17	(B)	6,440	400	0	400		70	130	0.593	0.931	0.065	570.915	566.000	4.915			
	17													570.915	566.000	4.915			
	1072													570.980	545.000	25.980			
1072	-	18'	(B)	4,000	0	252	252		1,500	120	0.928	4.246	6.369	564.612	480.000	84.612			
	18'													564.612	480.000	84.612			
18'	-	18	(B)	4,000	0	252	252		1,350	120	0.928	4.246	5.732	558.880	540.000	18.880			
	18													558.880	540.000	18.880			
	Katurastota Gohagoda																		
	5"													546.601	456.990	89.611			
5"	-	65'	(B)	2,140	252	0	252		950	130	0.497	1.151	1.094	545.508	490.310	55.198			
	65'													545.508	490.310	55.198			
65'	-	6501	(B)	1,200	201	0	201		1,720	130	0.438	1.187	2.042	543.465	506.600	36.865			
	6501													543.465	506.600	36.865			
6501	-	6401	(B)	100	0	97	97		1,250	130	0.157	0.416	0.520	542.945	455.000	87.945			
	6401													542.945	455.000	87.945			
6401	-	64S	(B)	100	0	97	97		780	130	0.157	0.416	0.324	542.621	530.000	12.621			
	64S													542.621	530.000	12.621			
	65'													545.508	490.310	55.198			
65'	-	65G	(B)	950	0	149	201	K	100	120	0.347	0.894	0.089	545.418	528.000	17.418			Exist Pipe φ150
	65G													545.418	528.000	17.418			
	6501													543.465	506.600	36.865			
6501	-	65	(B)	1,100	201	0	201	K	90	130	0.401	1.011	0.091	543.374	531.200	12.174			
	65													543.374	531.200	12.174			
	64													512.000	512.000	0.000			
64	-	64'	G	1,020	0	141	141		750	130	0.756	4.942	3.706	508.294	460.000	48.294			
	64'													508.294	460.000	48.294			
64'	-	64G	(B)	1,020	0	141	141		3,000	130	0.756	4.942	14.825	493.469	480.000	13.469			
	64G													493.469	480.000	13.469			
	64S													567.200	525.000	41.200			
64S	-	64B	B	100	0	97	97	K	360	120	0.157	0.482	0.174	567.026	562.000	5.026	B	41.2	Exist Pipe φ110
	64B													567.026	562.000	5.026			

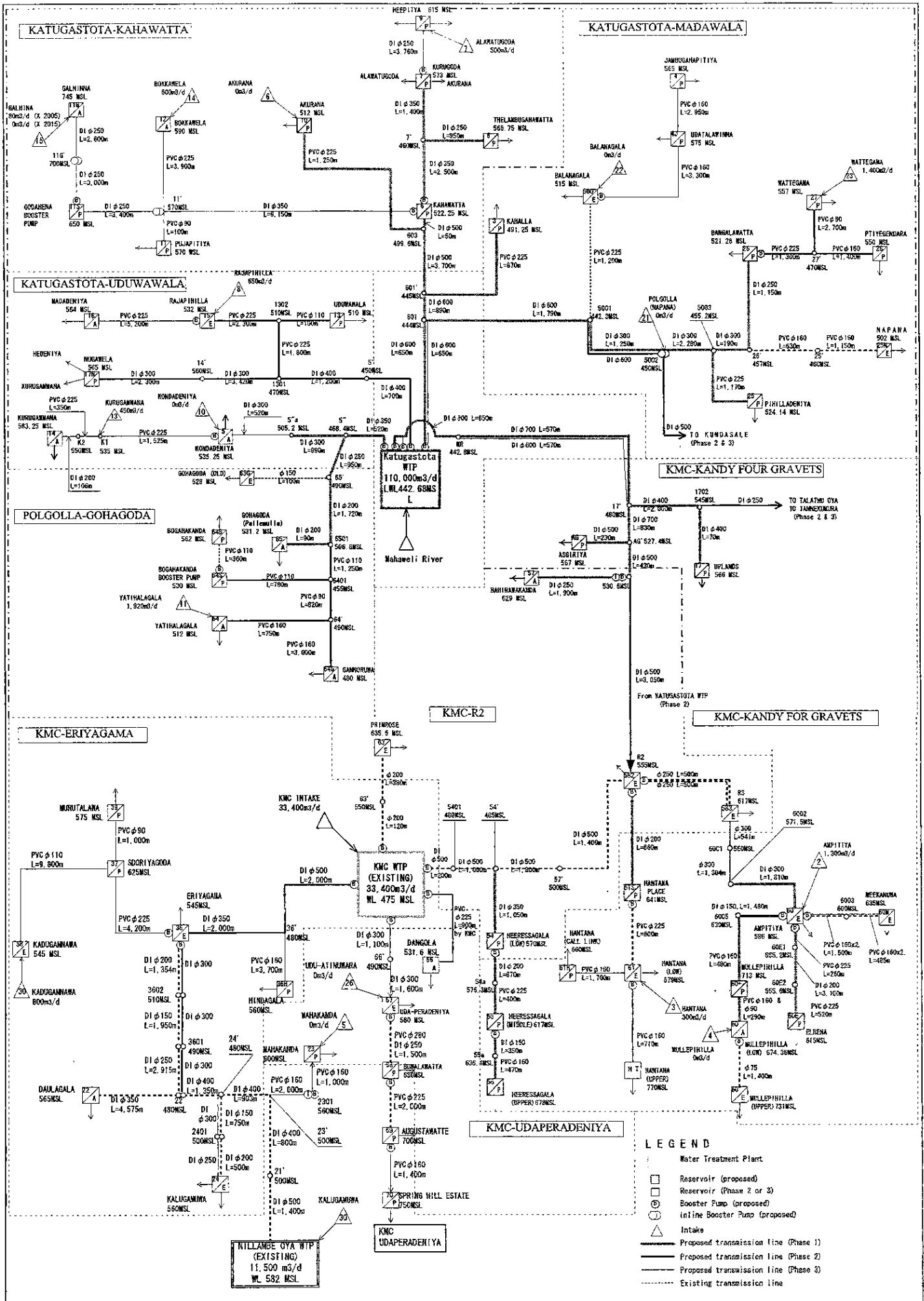


Figure-7.4 Transmission System in Phase 3

(Phase 3)

Node	Node	B/G	Flow Rate Q (m ³ /d)	Dia. D (mm)	Dia. D (mm)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (%)	Loss h (m)	Dynamic Pressure Hd (MSL)	LWL HWL (MSL)	Dynamic Pressure He (m)	Pump Type	Required Pump Head H (m)	Remark	
KMC-Primrose																				
KMC	-	63	B	2,360	0	0	201	201	K	500	120	0.861	4.812	2.406	643.000	471.000	172.000	B	172.0	Exist Pipe ϕ 200
KMC-Eliyagama & Hindagala																				
KMC	-	36'	B	13,700	0	502	0	502		2,000	130	0.801	1.245	2.490	582.000	471.000	111.000	B	111.0	
		36'													579.510	480.000	99.510			
		36'	B	900	0	0	141	141		3,700	130	0.667	3.920	14.505	565.005	560.000	5.005			
KMC-Udaperdeniya																				
KMC	-	66'	B	4,000	0	0	299	299		1,100	130	0.659	1.592	1.751	589.300	471.000	118.300	B	118.3	
		66'													587.549	490.000	97.549			
		66'	(B)	4,000	0	0	299	299		1,600	130	0.659	1.592	2.547						
		67	(= Udaperdeniya)												585.002	580.000	5.002			
		67													636.100	576.000	60.100			
		67	B	3,000	0	0	325	325	K	1,500	120	0.418	0.718	1.077				B	60.1	Exist Pipe ϕ 280 & ϕ 250
		68	(= Udaperdeniya)												635.023	630.000	5.023			
		68													712.500	626.000	86.500			
		68	B	2,000	0	0	199	199	K	2,000	120	0.744	3.719	7.439				B	86.5	Exist Pipe ϕ 225
		69	(= Bowalawatta)												705.061	700.000	5.061			
		69													761.700	696.000	65.700			
		69	B	1,000	0	0	141	141		1,400	130	0.741	4.764	6.669				B	65.7	
		70	(= Spring hill estate)												755.031	750.000	5.031			
KMC-KPG																				
KMC	-	5401	B	10,480	0	0	502	502	K	200	120	0.613	0.879	0.176	576.100	471.000	105.100	B	105.1	Exist Pipe ϕ 500
		5401													575.924	480.000	95.924			
		54'	B	10,480	0	0	502	502	K	1,000	120	0.613	0.879	0.879						
		54'													575.045	485.000	90.045			
		54'	(B)	5,280	0	0	502	502	K	1,800	120	0.309	0.247	0.445						
		57'													574.599	500.000	74.599			
		57'	(B)	5,280	0	0	502	502	K	1,400	120	0.309	0.247	0.346						
		582	= R2												574.253	555.000	19.253			
		582													542.300	471.000	71.300			
KMC	-	66	B	2,870	199	0	0	199		900	130	1.068	6.256	5.631				B	71.3	
		66	= Dangola												536.669	531.600	5.069			
		54'													575.045	485.000	90.045			
		54'	(B)	5,210	350	0	0	350		1,050	130	0.627	1.206	1.266						
		54	= Heeressagala low												573.779	570.000	3.779			

(Phase 3)

Node	Node	B/G	Flow Rate Q (m3/d)	Dia. D (mm)	Dia. D (mm)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (‰)	Loss h (m)	Dynamic Pressure Hd (MSL)	LWL H (MSL)	Dynamic Pressure He (m)	Pump Type	Required Pump Head H (m)	Remark
	54			2,005	2,010	2,015								629.100	566.000	63.100			
54	- 54a	B	2,740	201	0	0	201		870	130	0.999	5.469	4.758	624.342	576.330	48.012	B	63.1	
54a	- 55	B	2,740	199	0	0	199		400	130	1.020	5.742	2.297	622.045	617.000	5.045			
	55	= Heeressagala (Middle)												684.900	613.000	71.900			
65	- 55a	B	700	149	0	0	149		350	130	0.465	1.882	0.659	684.241	636.350	47.891	B	71.9	DIP
55a	- 56	B	700	141	0	0	141		470	130	0.519	2.463	1.157	683.084	678.000	5.084			PVC
	56	= Heeressagala (Upper)												626.190	549.490	76.700			
	KMC-R2, KPG													622.094	617.000	5.094			
582	- 583	B	11,420	0	0	328	328	K	500	120	1.564	8.192	4.096	648.590	549.490	99.100	B	76.7	Exist Pipe φ250×2
	583	= R3												646.059	641.000	5.059			
	582													684.700	637.000	47.700			
582	- 61S	B	1,960	201	0	0	201		860	130	0.715	2.943	2.531	684.057	679.000	5.057	B	99.1	
	61S	= Hantana place												679.000	675.000	4.000			
	61S													675.350	660.000	15.350			
61S	- 61	B	820	0	0	199	199	K	900	120	0.305	0.715	0.643	775.200	675.000	100.200	B	47.7	Exist Pipe φ225
	61	= Hantana low												775.043	770.000	5.043			
	61													617.000	613.000	4.000			
61	- 61H	G	650	0	141	0	141		1,700	130	0.482	2.147	3.650	615.596	560.000	55.596			
	61H	= Hantana call link												612.211	571.450	40.761			
	61													607.512	586.000	21.512			
61	- HT	B	190	0	141	0	141		710	130	0.141	0.221	0.157	624.700	582.500	42.200	B	100.2	
	HT	= Hantana upper												624.376	555.170	69.206			
	583	= R3												620.695	555.620	65.075			
583	- 6001	G	5,210	0	299	0	299		541	130	0.859	2.596	1.404	620.047	615.000	5.047			
	6001													725.400	582.500	142.900			
6001	- 6002	(G)	5,210	0	299	0	299		1,304	130	0.859	2.596	3.385	720.209	630.000	90.209	B	142.9	DIP φ150
	6002													718.006	713.000	5.006			
6002	- 60	(G)	5,210	299	0	0	299		1,810	130	0.859	2.596	4.699						
	60	= Ampitiya																	
	60																		
60	- 60E-1	B	1,200	199	0	0	199		260	130	0.447	1.247	0.324						
	60E-1																		
60E-1	- 60E-2		1,200	201	0	0	201		3,100	130	0.438	1.187	3.681						
	60E-2																		
60E-2	- 60E		1,200	199	0	0	199		520	130	0.447	1.247	0.648						
	60E	= Elhena																	
	60																		
60	- 6005	B	980	149	0	0	149		1,480	130	0.651	3.508	5.191						
	6005																		
6005	- 60+	B	980	141	0	0	141		480	130	0.726	4.589	2.203						
	60+	= Mullepihilla																	

(Phase 3)

Node	Node	B/G	Flow Rate Q (m ³ /d)	Dia. D (mm)	Dia. D (mm)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (%)	Loss h (m)	Dynamic Pressure Hd (MSL)	LWL HWL (MSL)	Dynamic Pressure He (m)	Pump Type	Required Pump Head H (m)	Remark
26	-	27'	B	1,700	0	199	0	199	1,300	130	0.633	2.374	3.087	573.680	517.280	56.400	B	56.4	
27'	-	27	(B)	300	0	97	0	97	2,700	130	0.470	3.175	8.573	570.593	456.990	113.603			
27'	-	27												562.020	557.000	5.020			
27'	-	28	(B)	1,400	0	141	0	141	1,400	130	1.038	8.878	12.429	570.593	470.000	100.593			
28	-													558.165	550.000	8.165			
5003	-	25	(B)	1,200	199	0	0	199	1,170	130	0.447	1.247	1.459	530.439	450.000	80.439			
25	-	(= Pihilladeniya)												528.980	524.140	4.840			
26'	-	25'	(B)	600	0	0	141	141	630	120	0.445	2.147	1.353	530.150	456.990	73.160			Exist Pipe φ160
25'	-	25N	(B)	600	0	0	141	141	1,150	120	0.445	2.147	2.469	528.797	460.000	68.797			Exist Pipe φ160
25N	-	(= Napana)												526.328	502.000	24.328			
601'	-	603	(B)	18,510	502	0	0	502	3,700	130	1.082	2.172	8.038	530.150	456.990	73.160			
603	-	6	(B)	16,110	502	0	0	502	50	130	0.942	1.680	0.084	538.822	443.000	95.822			
6	-	(= Kahawatta)												530.784	499.600	31.184			
6	-	7'	B	7,310	350	0	0	350	2,500	130	0.879	2.256	5.639	530.700	522.250	8.450			
7'	-	7	(B)	5,400	350	0	0	350	1,400	130	0.650	1.288	1.803	585.500	516.000	69.500	B	69.5	
7	-	(= Kurugoda)												579.861	455.030	124.831			
603	-	10	B	2,400	199	0	0	199	1,250	130	0.893	4.494	5.617	578.057	573.000	5.057			
10	-	(= Akurana)												530.700	499.600	31.100			
6	-	11'	B	6,400	0	0	350	350	6,150	130	0.770	1.764	10.848	530.700	499.600	31.100			
11'	-	12	(B)	2,500	0	0	199	199	3,900	130	0.930	4.847	18.901	624.800	516.000	108.800	B	108.8	
12	-	(= Bollaewela)												613.952	570.000	43.952			
11'	-	11	(B)	1,100	0	0	79	79	100	130	2.597	95.453	9.545	595.050	590.000	5.050			
11'	-	11S	IB	2,600	0	0	252	252	3,400	130	0.603	1.650	5.611	613.952	570.000	43.952			
11S	-													604.407	570.000	34.407			
														660.652	566.000	94.652			
														655.041	650.000	5.041			

(Phase 3)

Node	Node	B/G	Flow Rate Q (m3/d)	Dia. D (mm)	Dia. D (mm)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (%)	Loss h (m)	Dynamic Pressure Hd (MSL)	LWL HWL (MSL)	Dynamic Pressure He (m)	Pump Type	Required Pump Head H (m)	Remark
11S	11S			2,005	2,010	2,015								710.000	646.00	64.000			
11S	11G'	B	2,600	0	0	252	252		3,000	130	0.603	1.650	4.951	705.049	700.00	5.049	B	64.0	
11G'	11G'													754.349	700.00	54.349			
11G'	11G	IB	2,600	0	0	252	252		2,600	130	0.603	1.650	4.291	750.059	745.00	5.059	IB	49.3	
7'	7'													579.861	455.030	124.831			
7'	8	(B)	1,910	252	0	0	252		950	130	0.443	0.933	0.886	578.975	566.750	12.225			
	8	(= The lambudahawatta)												628.100	569.000	59.100			
7	7													620.015	615.000	5.015			
7	9	B	3,000	0	0	252	252		3,760	130	0.696	2.150	8.085				B	59.1	
	9													584.980	442.680	142.300			
	Katugastota-Uduwawala																		
PG	PG													583.819	450.000	133.819			
PG	5'	B	8,800	0	400	0	400		700	130	0.811	1.659	1.161	581.827	470.000	111.827	B	142.3	
5'	5'													574.776	560.000	14.776			
5'	1301	(B)	8,800	0	400	0	400		1,200	130	0.811	1.659	1.991	570.034	565.000	5.034			
1301	1301													544.580	442.680	101.900			
1301	14'	(B)	4,600	0	299	0	299		3,420	130	0.758	2.062	7.051	543.798	468.410	75.388			
14'	14'													542.940	505.180	37.760			
14'	17N	(B)	4,600	0	299	0	299		2,300	130	0.758	2.062	4.742	542.940	535.250	7.690			
	17N													591.150	631.250	59.900			
	Katugastota-Kondadeniya, Kurugamana																		
PG	PG													589.393	535.000	54.393			
PG	5"	B	5,870	350	0	0	350		520	130	0.706	1.503	0.782	588.531	550.000	38.531	B	101.9	
5"	5"													588.531	550.000	38.531			
5"	5" a	(B)	3,050	299	0	0	299		890	130	0.503	0.964	0.858	588.283	583.250	5.033			
5" a	5 a													576.880	442.680	134.200			
5" a	5	(B)	3,050	0	0	299	299		520	130	0.503	0.964	0.501	575.936	442.770	133.166	B	134.2	
	5													575.296	453.650	121.646			
5	5													573.816	527.400	46.416			
5	K1	B	1,150	0	0	199	199		1,525	130	0.428	1.152	1.757	572.912	530.630	42.282			
K1	K1													567.911	565.000	12.911			
K1	k2	(B)	1,600	0	0	199	199	K	350	120	0.595	2.461	0.861						Exist Pipe φ225 PVC
k2	k2													572.912	530.630	42.282			
k2	14	(B)	1,600	0	0	201	201	K	106	120	0.584	2.344	0.249	572.912	530.630	42.282			Exist Pipe φ200 DI
	14	(= Kurugamana)												572.912	530.630	42.282			
	Katugastota-KFG, R2																		
PG	PG													575.296	453.650	121.646			
PG	MR	B	51,110	802	0	0	802		650	130	1.171	1.452	0.944	575.296	453.650	121.646	B	134.2	
MR	MR													575.936	442.770	133.166			
MR	17'	(B)	51,110	700	0	592	846		570	130	1.053	1.122	0.640	575.296	453.650	121.646			
17'	17'													573.816	527.400	46.416			
17'	AG'	(B)	39,920	700	0	0	700		830	130	1.201	1.783	1.480	573.816	527.400	46.416			
AG'	AG'													572.912	530.630	42.282			
AG'	(IB)	(B)	18,180	502	0	0	502		430	130	1.063	2.101	0.904	572.912	530.630	42.282			
(IB)	(IB)													572.912	530.630	42.282			
(IB)	582	G	15,900	502	0	0	502		3,050	130	0.930	1.640	5.002	567.911	565.000	12.911			
	582	(= R2)												567.911	565.000	12.911			

(Phase 3)

Node	Node	B/G	Flow Rate Q (m ³ /d)	Dia. D (mm)	Dia. D (mm)	Dia. D (mm)	Mixed Dia Dm (mm)	Exist.	Length L (m)	C	Velocity v (m/sec)	Hyd. Grd I (%)	Loss h (m)	Dynamic Pressure Hd (MSL)	LWL HWL (MSL)	Dynamic Pressure He (m)	Pump Type	Required Pump Head H (m)	Remark
AG'	-	AG	(B)	21,740	502	0	0	502	230	130	1.271	2.925	0.673	573.816	527.400	46.416			
		AG	(= Asgiriya)											573.143	567.000	6.143			
(IB)	-	57	B	2,280	252	0	0	252	1,900	130	0.529	1.294	2.459	572.912	530.630	42.282	B	63.6	
		57	(= Bahirawakand)											634.053	629.000	5.053			
17'	-	1702	(B)	11,200	400	0	0	400	2,000	130	1.032	2.592	5.185	575.296	453.650	121.646			
1702	-	17	(B)	7,200	400	0	0	400	70	130	0.663	1.145	0.080	570.112	545.000	25.112			
		17	(= Upland)											570.032	566.000	4.032			
		Katugastota-Talathu Oya																	
1702	-	18'	(B)	4,000	0	252	0	252	1,500	130	0.928	3.661	5.492	570.112	545.000	25.112			
18'	-	18	(B)	4,000	0	252	0	252	1,350	130	0.928	3.661	4.943	564.620	480.000	84.620			
		18	(Talawatta)											559.677	540.000	19.677			
		Katugastota-Gohagoda																	
5"	-	65'	(B)	2,820	252	0	0	252	950	130	0.654	1.918	1.822	543.798	456.990	86.808			
65'	-	6501	(B)	1,600	201	0	0	201	1,720	130	0.584	2.022	3.477	541.976	490.310	51.666			
6501	-	6401	(B)	200	0	97	0	97	1,250	130	0.313	1.500	1.875	538.499	506.600	31.899			
6401	-	64S	(B)	200	0	97	0	97	780	130	0.313	1.500	1.170	536.625	455.000	81.625			
		64S												535.455	530.000	5.455			
65'	-	65G	(B)	1,220	0	0	149	149	100	120	0.810	6.100	0.610	541.976	490.310	51.666			Exist Pipe φ 200
		65G												541.366	528.410	12.956			
6501	-	65	(B)	1,400	201	0	0	201	90	130	0.511	1.579	0.142	538.499	506.600	31.899			
		65	(=Gohagoda (Palleemulla))											538.357	531.200	7.157			
64	-	64'	G	1,100	0	141	0	141	750	130	0.815	5.682	4.262	512.000	512.000	0.000			
64'	-	64G	G	1,100	0	141	0	141	3,000	130	0.815	5.682	17.047	507.738	460.000	47.738			
		64G												490.691	480.000	10.691			
64S	-	64B	B	200	0	0	97	97	360	120	0.313	1.739	0.626	567.700	526.000	41.700	B	41.7	Exist Pipe φ 110
		64B												567.074	562.000	5.074			

04 Distribution System Calculations

Distribution System Calculation

1. General

This working paper as a report presents the methodology, basic conditions and design criteria, applied for the pipe network analysis for present study.

The network analysis is carried out using US software, which is a user-friendly program based on Kypipes and operated on MS-dos.

And the results of pipe network analysis are described in the following section.

Outline of work procedure for network analysis is presented in Figure 1-1.

2. Condition of Analysis

2.1 Methodology

In the JICA F/S Report on Greater Kandy Water Supply Augmentation Project, prepared in 1999, twenty (20) Service Reservoirs (S.R.) which are shown in Table 2.1-1, were proposed to be constructed newly or expanded for storing the water for distribution. This water is distributed to the consumers in the Phase 1 served area, through the new distribution feeder main, which is planned be installed from S.R. to the existing pipe and/or existing pipe network. To determine the proper pipe diameter of feeder main and pipelines in the distribution network for water supply scheme, the hydraulic network analysis is carried out to meet the design criteria.

The outline of methodology on distribution network analysis for Greater Kandy Water Supply Augmentation Project is presented in the following. Figure 1-1 shows the flow diagram for present pipe network analysis.

2.1.1 Existing Distribution Network of Each Water Scheme

The existing pipeline data is essential matter for analyzing the future pipeline network. For that purpose, the following data are required.

- 1) Drawings of existing distribution pipe network for each water supply scheme together with list of pipe length for each diameter and each material were collected.
- 2) Location of present reservoirs were put on the map of 1:10,000 scale..
- 3) High water, Low water and Ground elevation of existing reservoir were obtained.

2.1.2 Water Demand

The future water demand that was predicted by the F/S is reviewed by taking into account of the latest water consumption data. The water demand required in the new development area, which are not expected in the F/S, will be taken into consideration for the pipe network analysis. However, in principle, the predicted total water demand for Phase 1 project is not changed. Based on the projected and fixed future demand of each water supply scheme, in the years 2005, 2010 and 2015, water demand is distributed in the served area considering the population density, commercial demand, large size consumers and other water demand factors.

2.1.3 Future Distribution Pipeline

The NWSDB's water supply planning for the pipeline expansion for each Water Supply Scheme by the project's target year is indicated on the available map. Distribution pipeline routes from the new Service Reservoirs (SR) to pipe connection points are investigated and used as present data for the pipe network analysis.

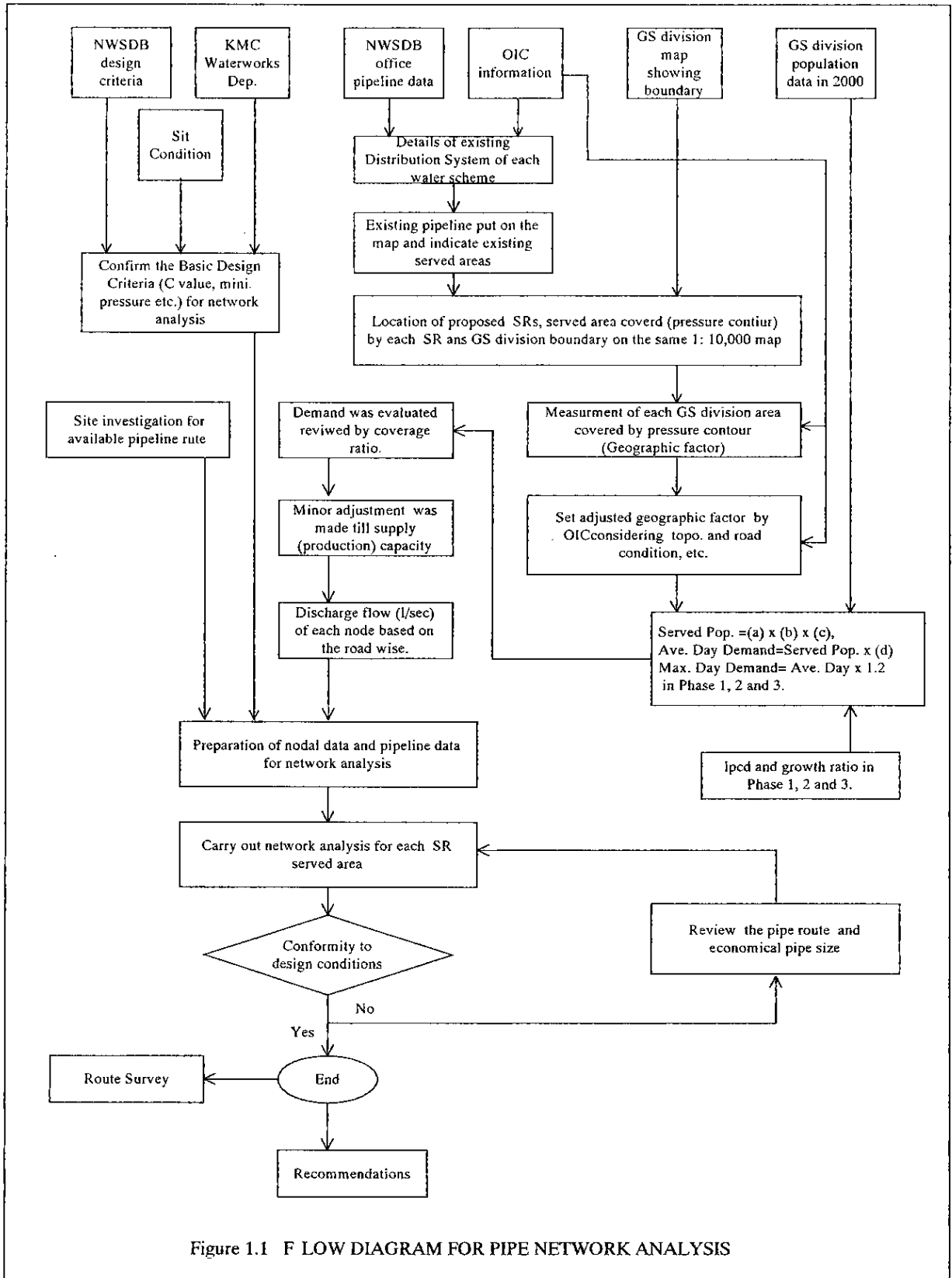


Figure 1.1 FLOW DIAGRAM FOR PIPE NETWORK ANALYSIS

Table 2.1-1 Capacities and Elevations of Proposed Service Reservoirs in Phase 1

SR No.	Name of Service Reservoir	Water Level (m)		Capacity (m ³)	Type
		LWL	HWL		
SR-1	Asgiriya	561.50	567.00	4,100	Ground
SR-2	Bahirawakanda	625.00	629.00	600	Elevated
SR-3	Bangalawatta	518.28	521.28	300	Ground
SR-4	Dangolla	527.60	531.60	500	Ground
SR-5	Elhena	611.00	615.00	300	Ground
SR-6	Gohagoda (Pallemulla New)	527.20	531.20	200	Ground
SR-7	Hantana Place	637.00	641.00	200	Ground
SR-8	Heerassagala Low	566.00	570.00	200	Ground
SR-9	Heerassagala Middle	613.00	617.00	250	Ground
SR-10	Heerassagala Upper	674.00	678.00	200	Ground
SR-11	Kahalla	485.00	491.25	600	Elevated
SR-12	Kahawatta	516.00	522.25	600	Elevated
SR-13	Kondadeniya	531.25	535.25	200	Ground
SR-14	Kulugamma	579.25	583.25	100	Ground
SR-15	Kurugoda	569.00	573.00	600	Ground
SR-16	Mullepihilla Low New	709.00	713.00	100	Ground
SR-17	Pihilladeniya	522.14	524.14	200	Ground
SR-18	Thelambugahawatta	561.50	566.75	500	Elevated
SR-19	Uplands	560.09	566.00	2,960	Ground

2.1.4 Network Analysis

Such design criteria as C value, minimum pressure at the end of network and others, were studied for the present pipe network analysis. Nodal data and pipeline data were also prepared, based on the available information, as shown below.

The network analyses for each water scheme for Full Target Year 2015 (Phase 3) were carried out.

To design the proper diameter of new distribution feeder main/s, pipe route condition and economical pipe size are taken into consideration for the most economical and technically acceptable design.

Distribution of water demands to each node in pipe network is conducted as shown below. The Greater Kandy varies its population, in general, by the class of alongside roads in the district/area. Therefore, the projection of served population by the water system is considered to follow and depend on this characteristic.

The water demand distribution for pipe network analysis was made taking into account the above specialty, and the water demand density per 100m length of main road or pipeline was estimated with the method presented below, for demand distribution to the pipe network.

1. Classify the roads in the respective network, into the three classes, (1) Main road, (2) General road, and (3) Foot-pass.
2. Estimate the population per above classes as unit population per 100m pipelines.
3. Calculate the water demand, applying the length of pipeline, unit population density and the unit per capita water demand.
4. Each node's demand distribution was calculated basically as described in the above. And, the demand for such node, which has intersection of plural number of roads, was calculated by applying the proportional distribution.

2.1.5 KMC Network Analysis

Regarding the KMC distribution network, the Feasibility Study on Water Supply Augmentation and Distribution for Kandy (ADB LOAN NO.1632-SRI [SF]), prepared by Engineering

Consultants Limited in September 2000, has been reviewed. Distribution feeder mains to be implemented by the Phase 1 project were designed based on the result of discussion with KMC officials concerned.

2.2 Basic Conditions

2.2.1 Coverage of Distribution Pipe Design

Distribution feeder main pipe from the new Service Reservoirs (SR) to connected point of the nearby pipe network and the fundamental pipelines for strength or augmentation of network were selected and made detailed design.

2.2.2 Design Criteria for Distribution Network Analysis

The following design criteria for distribution network analysis are applied:

1) Peak Factor

- Maximum daily demand / average daily demand is 1.2
- Hourly demand / Maximum daily demand is 1.78
- Hourly demand / average daily demand is 2.0
- The required hourly peak demand for distribution network analysis of 10 WSS is presented in Table 2.1-2.

2) Node and Pipeline Data

- Discharge flow of each node is hourly demand (l/sec).
- In case of PVC, internal diameter is applied.

3) Software Program

The network analysis is carried out using US software, which is a user-friendly program based on Ky-pipes and operated on MS-dos.

4) C value of Hazen-Williams Formula

Material	DCIP	PVC	ACP	SS or GI
New Pipe	140	140	---	---
Existing Pipe	(CI=) 90	120	120	120

5) Residual Pressure

Minimum pressure is at the end of network is 0.1 Mpa (= 1.0 kgf/cm²), ant any node. 0.6bar (6m water head) residual pressure at the house connection is designed.

6) Break Pressure Tank (BPT)

At the location where dynamic pressure is exceeding 0.7 Mpa (= 7.0 kgf/cm²) break pressure tank facilities are designed.

3. Existing Distribution Network

3.1 Alawathugoda WSS

The present situation of Alawatthugota Water Supply Scheme is briefly presented below. In this scheme, the existing two water reservoirs of Villana with 75 m³ water capacity and Owissa that with 50 m³ is covering the Alwathugoda Scheme distribution system. The far north and the southern part distribution areas are supplied water via break pressure tank/s (BPT) by reducing the pipe system pressure.

3.2 Akurana WSS

The existing Akurana water system has a water reservoir with capacity 600m³, which is receiving the water from two boreholes and supplying to this entire scheme.

3.3 Balanagala WSS

The existing Balanagala water system is located adjacent to the Polgolla Scheme and has a water reservoir with capacity 450m³, which is supplying to the pipe network of this entire scheme.

3.4 Polgolla WSS

In this Scheme, there exist two water reservoirs of Bagalawatta: 100 m³ and Pihilladeniya: 100 m³, located in the Madawale area in north. These two reservoirs cover the entire supply area and have almost the same water level.

Further, there is another water reservoir at Napana: 150 m³, in this Scheme, which is not used at present but, be re-used in the future. This reservoir has its water level/elevation 20m lower than that of the other two reservoirs.

And in the south area, there is an existing Polgolla reservoir, which is planned not be used in the future. As described in the above, this Scheme is adjacent to the Balanagala Scheme.

3.5 Kulugammana WSS

The Existing Kulugammana Service Reservoir (300m³) is covering this entire scheme's water system.

3.6 Kondadeniya WSS

In this Scheme, the existing Kondadeniya Service Reservoir (300m³) is covering the entire system water.

3.7 Gohagoda WSS

In this Scheme, the entire system is covered by the following two sub-systems, which are separated by the gate valve:

- (1) Gohagoda Wegiriya Service Reservoir (Old: 300m³) & Gohagoda Low Service Reservoir (Pallemulla: 150m³)
- (2) Yatihagala Service Reservoir: 150m³

3.8 Ampitiya WSS

This Scheme's entire system is covered by the following two sub-systems:

- (1) Existing Ampitiya Service Reservoir (900m³), which covers the southern part of this Scheme,
- (2) Existing Meekanuwa Service Reservoir (225 m³), which covers the northern part.

This Scheme has not sufficiently developed the pipe network system, compared to the other Scheme. Further, along the trunk main road (Ampitiya Road) in this area, there exists asbestos cement pipe (AC pipe) with 6.1km in length. It is necessary be replaced with the other pipe material for this AC pipe, which has disadvantages as high rate carcinogenic material and less durability for heavy traffic load.

3.9 Mullepihilla WSS

In this Scheme, the entire system is covered by the following two sub-systems:

- (1) Mullepihilla Low Service Reservoir (25 m³) for lower elevation service area, and
- (2) Mullepihilla High Service Reservoir (25 m³) for higher elevation service area.

This Scheme has the most simple service system, as one distribution pipeline. And, the pipeline in high service area is functioning both as transmission and distribution pipeline.

3.10 Hantana WSS

This Scheme's entire system is covered by the following two sub-systems:

Hantana Low/R4 Service Reservoir (1365m³), which covers the lower area this Scheme, and (2) Hantana High/R2 Service Reservoir (25m³), which covers the high area.

3.11 Heeresasagala WSS

This Scheme is the newly included scheme for the present Design Study, for which water supply system is entirely less developed compared to the other WSS. The present water system is composed of as follows:

- (1) Untreated spring water supply for Heeresasagala Low SR, which is diverted from KMC system.
- (2) Treated spring water supply for Heeresasagala Middle SR, which is diverted from KMC system.
- (3) Untreated spring water supply for Heeresasagala Upper SR, which is diverted from the Regional Council.

4. Future Improvement Plan for Distribution Networks

4.1 General

Based on the preceding development plan for distribution system and existing network analysis,

the future distribution network improvement has reviewed and studied for design as presented in the following.

4.2 Vilana & Owissa SR and Kurugoda SR Network (See Appendix- 5.1 Improvement of Distribution Network in 2015)

For this Scheme, a new Kurugoda Service Reservoir (SR) with the capacity 600 m³ is designed in the south. From the system pressure contour line, the distribution area/s covered by the existing and new SRs are identified as follows:

(1) Area covered by Vilana & Owissa (SR):

- Northern part of Alawathugoda,

(2) Area covered by Kurugoda SR:

- Southern part of Alawathugoda and
- A part of northern part of Akurana.

By the above improvement, the coverage or load for water distribution for two SRs Vilana and Owissa could be reduced or eased. And, in the northern part of Akurana, the higher elevation (GL above 510m) than that water elevation of Akurana SR, could be supplied from this improved system.

Through this pipe hydraulic analysis, a pipe system to connect the Kurugoda SR via A9 Road and to the east could be designed. That target is to improve the total system pressures, and to supply water not only the nearby SR but also to cover the higher elevation area.

4.3 Akurana SR, Thelambugahawatta SR and Kahawatta SR Network (See Appendix- 5.2 Improvement of Distribution Network in 2015)

For this Scheme following two new service reservoirs have been planned and designed:

- (1) Thelambugahawatta SR (500 m³) in the north-east of Akurana, and
- (2) Kahawatta SR (600 m³) in the south of Akurana.

In this Scheme, due above improvement, the existing Borehole system is considered as it could be used as the standby system in the future. From the system pressure contour line, the Thelambugahawatta SR is observed capable to supply water to the north-east of Akurana area.

The majority part of this Scheme has high potentiality of future water demand increase. Even though, this area has not covered by the existing pipe system from the Akurana SR.

Some part of this area has rather high ground elevation (GL540m above), compared to the proposed Service Reservoir. Due mainly this reason, it is observed hydraulically difficult to supply water from the proposed entire system. Considering this background, it is urgently required to improve the water system in this service area .

Under the present design/planning, the service reservoir in this area is proposed be elevated from the ground to meet the required system pressure for the Scheme. And, by forming the pipe mesh network, the total system could be analyzed hydraulically in flexible manner, which results for the optimum operation of the distribution network.

While, the system pressure contour line produced by the Akurana SR indicates that, the water supply boundary could be extended/covered to the southern part of this network. This is interpreted that, the present Borehole system, which supply water to almost all the existing system, could be substituted by the gravity/reservoir supply system. The gravity system supply system produces hydraulically more economical and stable water supply in the Scheme.

The network Nodes: 2080 – 2081 could be connected by pipeline, which objects the expanded water supply to the residents in/along this pipe line area. Further, the existing SR Akurana system pressure contour line indicated that, this SR could cover the northern part of Akurana.

As mentioned in the above section, the new construction of Thelambugahawatta and Kahawatta SRs could improve the water supply situation to the north of Akurana from Kurugoda SR. And the burden of the distribution load/coverage was eased or reduced from Akurana SR.

4.4 Balanagala SR and Kahalla SR Network (See Appendix- 5.3 Improvement of Distribution Network in 2015)

This Scheme is planned and designed to be constructed a new Kahalla Service Reservoir (600 m³) in the western part of this Scheme/service area.

The system pressure contour line for this network indicates that, the water distribution coverage areas are:

- (1) Kahalla SR could extend and serve to the Balanagala Scheme and the western part of service area where pipe network is not developed yet, and
- (3) The existing Balanagala SR is planned be connected to the existing pipe network which is covered by the Polgolla SR. These networks are planned/designed to be combined to form bigger size of pipe network, which create more rational and practical water use.

4.5 Bangalawatta SR and Pihilladeniya SR Network (See Appendix- 5.4 Improvement of Distribution Network in 2015)

For this Scheme, any new reservoir construction is not planned. However, the existing two reservoirs are to be expanded: Bangalawatta is planed to expand its capacity by 300m³ to 400 m³, and that of Pihilladeniya by 200 m³ to 300 m³, respectively.

From the system pressure contour line, the all area in this Scheme is observed capable for water supply from the existing/expanded SRs except for the southeastern part of the scheme. It is found that, in future, the Napana SR could be revived its use. Then, the nearby service area only is

capable for service from this SR. Since, the water elevation of this SR is not high enough to cover far/remote area from this reservoir. Therefore, two options for the future have been proposed. (See Appendix 5.4, Option 1 & Option 2).

The above plan would result that, the Balanagala SR could be eased from heavy burden/load to cover larger service area.

While the Polgolla SR is scheduled be abandoned in the future, the connected pipe network should be combined with the aforementioned Balanagala SR service network to form larger pipe network for optimum operation.

4.6 Kulugammana SR Network (See Appendix- 5.5 Improvement of Distribution Network in 2015)

For this Scheme, any new reservoir construction is not planned. However, the existing reservoir Kulugammana SR is planed be expanded its capacity by 300m³ to 400 m³.

From the system pressure contour line, the all area in this Scheme is observed capable for water supply from the existing/expanded SRs, except for the northeastern part of the scheme. This particular area has now been proposed to be isolated and served using an in-line booster station as an interim measure until the proposed SR at Nugawela (Phase 2) is in place. Many reinforcements for the other areas have been proposed to enhance the performance of the scheme.

4.7 Kondadeniya SR Network (See Appendix- 5.6 Improvement of Distribution Network in 2015)

For this Scheme network, any new reservoir construction is not planned. However, the existing reservoir Kondadeniya SR could be expanded its capacity by 200m³ to 500m³.

From the system pressure contour line, the all area in this Scheme is considered as capable for water supply from the existing/expanded SRs. The existing pipe system of this Scheme forms tree-blanch structure. Further, from the geographical location, it is rather difficult to structure

mesh type pipe network.

4.8 Gohagoda SR Network (See Appendix- 5.7 Improvement of Distribution Network in 2015)

For this Scheme network, a new service reservoir Gohagoda New SR (with capacity 200m³ and elevation GL= 524m) is designed next to the existing Gohagoda Low SR, and total capacity is expanded to 350 m³.

From the system pressure contour line, the all area in this Scheme is capable be supplied water from the existing/expanded SRs. However, the Yatihagala sub-system is not included but isolated with the boundary valve. With the pipe network analysis, the service areas of the respective SR were demarcated and the existing Gohagoda Low SR has been proposed to serve the low elevated areas in the southern part of the scheme. At the same time the New Gohagoda SR will contribute to reduce the service coverage burden for Gohagoda Wegiriya (Old) SR while serving the high elevated areas. Furthermore, in case of emergency, the service water could hydraulically be supplied to the Yatihagala Scheme.

4.9 Elhena SR Network (See Appendix- 5.8 Improvement of Distribution Network in 2015)

For this Scheme, a new service reservoir Elhena SR (with capacity 300m³ and elevation GL= 611m) is designed in the eastern part.

From the system pressure contour line, the Elehena SR is capable to cover nearby this SR, which has comparatively higher elevation than that of western part of Ampitiya. With the pipe network analysis, it has been observed that certain areas in the vicinity of the SR would experience excessive pressures. Therefore, Elhena SR is proposed to serve only the high elevated areas in the northeastern and southwestern parts of the existing Ampitiya Scheme. The rest of the service area would continue to be served by the Ampitiya SR.

Further, The existing AC pipe augmenting pipeline (Node 8042 – 8045 line) could be improved, to increase the system pressure. At the same time, this will contribute to reduce the service coverage burden for Ampitiya SR. Furthermore, the aforementioned existing AC pipeline should be replaced or improved to keep stable and safe water to the service.

4.10 Mullepihilla SR Network (See Appendix- 5.9 Improvement of Distribution Network in 2015)

For this Scheme, a new service reservoir Mullepihilla New SR (with capacity 100m^3 and elevation $\text{GL}= 710.5\text{m}$) is designed next to the existing Mullepihilla Low SR (capacity 25m^3), and total capacity is expanded to 125m^3 . From the system pressure contour line, it is observed that geographically capable service area is Mullepihilla Low area in this Scheme.

The existing Mullepihilla High SR could cover the Mullepihilla High area. Further, this could serve rationally to these area covered by Ampitiya SR which has the most highest elevation ($\text{G.L} = 586\text{m}$).

4.11 Hantana Place SR Network (See Appendix- 5.10 Improvement of Distribution Network in 2015)

Under this Scheme network, a new service reservoir Hantana Place SR (with capacity 200m^3) in the south-west.

From the system pressure contour line, it is observed that hydraulically capable service area by Hantana Place SR is the very limited area of south-western part of existing Hantana Scheme. This will contribute to the Hantana Low/R4 to ease and reduce its load of water service coverage.

On the other hand, the Hantana SR could cover the central part of this Scheme and the Hantana High/R2 could cover the higher elevation area with its elevation potential. Therefore, it has now been proposed to serve only the southwestern part of the existing scheme by this new SR. However, at the request of the KMC, some provision have been made to serve the Kandy

Hospital Quarters and the Nagastenna area which lie within the KMC limits.

4.12 Heeresasagala Middle and Upper SRs Network (See Appendix- 5.11 Improvement of Distribution Network in 2015)

For this Scheme, two new service reservoirs (1) Heeressagala Upper SR (200m³) and Heeresasagala Middle SR (250m³) are planned/designed.

From the system pressure contour line, it is geographically observed that the capable area covered by the two reservoirs is:

- (1) Heeressagala Middle SR: Northern part of this Scheme, and
- (2) Heeressagala Upper SR: Southern part of this Scheme.

The distribution networks are planned be supplied by the separate two systems.

One system: Heeresasagala Middle, will be constructed and operated by NWSDB.

From the pipe network analysis for the above, it could be expected the two separate systems will operate the stable and optimum water supply, from each SR respectively.

From the Heeressagala Upper SR, as requested by the KMC, supply to be extended to feed the existing Elagolla SR via a gravity distribution main.

5. Phase 1 Distribution Pipeline

The proposed pipelines in the outside of KMC service area and KMC area are presented in Table 5.1 shown below.

Distribution trunk feeder pipe from the new or expanded SR to the connection point to the distribution network shall be selected considering the economical size, and have some allowance taking consideration on unforeseen future water demand.

In addition, some new distribution pipes which are required to strengthen the existing distribution network and expanded service area, shall also be selected taking into account the opinions given by the OIC of present WSS, for such as future development area, area where ground well yield are poor, intermitted supply area, etc. Among such pipelines, high priority pipe that is quite effective for hydraulically might be selected and included in the detailed design.

The each service zone will be formed the independently of distribution network with existing and new pipelines, and as the result, the following improvement or betterment are predicted.

- (1) Many houses which has been waiting the connection to water supply, can be connected and get clean water.
- (2) Present intermittence water supply condition will be improved to supply continuously.
- (3) Low or negative pressure area will be dissolved and appropriate pressure will be kept.
- (4) Development and expanded area will get water anytime.

Table 5.1 Phase 1 Distribution Pipelines

(1/3)

Name of Service Reservoir	Drawing Number	Route Number	Pipe Diameter (mm)	Material DI/PVC	Pipeline Length (m)
Kurugoda	40-C-01	1	250	DI	1,090
			225	PVC	760
			160	PVC	210
	40-C-02	2	225	PVC	220
			110	PVC	660
	40-C-03	3	90	PVC	1,030
	40-C-04	4	225	PVC	230
	40-C-05	5	160	PVC	560
	40-C-06	6	160	PVC	420
	40-C-07	7	90	PVC	440

(2/3)

Name of Service Reservoir	Drawing Number	Route Number	Pipe Diameter (mm)	Material DI/PVC	Pipeline Length (m)
Thelambugahawatta	40-C-08	8	225	PVC	200
			160	PVC	880
	40-C-09	9	110	PVC	890
			160	PVC	1,400
	40-C-10	10	90	PVC	750
160			PVC	290	
Kahawatta	40-C-12	12	110	PVC	560
			100	DI	30
	40-C-13	13	110	PVC	340
	40-C-14	14	225	PVC	800
	40-C-15	15	300	DI	220
225			PVC	670	
Kahalla	40-C-16	16	300	DI	580
			160	PVC	640
	40-C-17	17	250	DI	130
			225	PVC	720
			160	PVC	470
	40-C-18	18	160	PVC	440
			110	PVC	250
			100	DI	100
90			PVC	880	
40-C-19	19	90	PVC	300	
Bangalawatta &	40-C-20	20	250	DI	240
			225	PVC	1,030
Pihilladeniya	40-C-21	21	225	PVC	1,090
Kurugammana	40-C-22	22	250	DI	170
			100	DI	100
Kondadeniya	40-C-23	23	90	PVC	430
			250	DI	60
Gohagoda New (Pallemulla)	40-C-24	24	225	PVC	170
			300	DI	70
Elhena	40-C-25	25	300	DI	70
			225	PVC	340
Elhena	40-C-27	27	250	DI	140
			225	PVC	670
	40-C-28	28	160	PVC	430
Mullepihilla Low New	40-C-29	29	160	PVC	540
			160	PVC	0
Hantana Place	40-C-30	30	160	PVC	0
	40-C-31	31	225	PVC	380

(3/3)

Name of Service Reservoir	Drawing Number	Route Number	Pipe Diameter (mm)	Material DI/PVC	Pipeline Length (m)
Heerassagala Upper	40-C-32	32	160	PVC	340
	40-C-33	33	225	PVC	140
			160	PVC	370
	40-C-34	34	110	PVC	590
Heerassagala Middle	40-C-35	35	250	DI	220
			200	DI	40
	40-C-36	36	110	PVC	160
Bahirawakanda	40-C-37	37	250	DI	120
Asgiriya	40-C-38	38	250	DI	190
	40-C-39	39	500	DI	680
			450	DI	1,210
40-C-40	40	400	DI	330	
Heerassagala Low	40-C-41	41	250	DI	280

Total 27,690

6 Recommendation/Comment

1) Thelambugahawatta and Kahalla Service Zones

These two service zones are installed less existing pipelines, hence new pipelines and house connections are required to meet the water demand in Phase 1.

When it is necessary, in addition to the pipes, which will be procured under the proposed Phase 1 Project, NWSDB is recommended to prepare the additionally required pipe materials and house-connection piping materials for future installation.

2) High Elevation Area

The Kandy District is geographically comprised of hilly terrain, with elevation varying from 300m to 2,000m above mean sea level (MSL). The major perennial river in this district is the Mahaweli Ganga (River), which has many tributaries in the district. In the service zones in Kandy, there exist some higher elevation areas where water cannot be supplied by gravity. Even in such

areas, water is acutely needed for the resident's daily life. In such case, booster pump/s is required for water distribution.

3) Isolation Valve

This valve is designed for functioning not only isolation of the service zones, but also interconnection of each service zone, in the case of emergency. Therefore, the installed valve location shall be recorded and valve conditions shall be maintained properly, for normal future operation.

4) Reformation of WSS

The present water supply scheme/s might be reformed on the basis of the new service area. If, any scheme has necessary been reformed, a new organization shall be considered.

5) Supply Amount Measurement

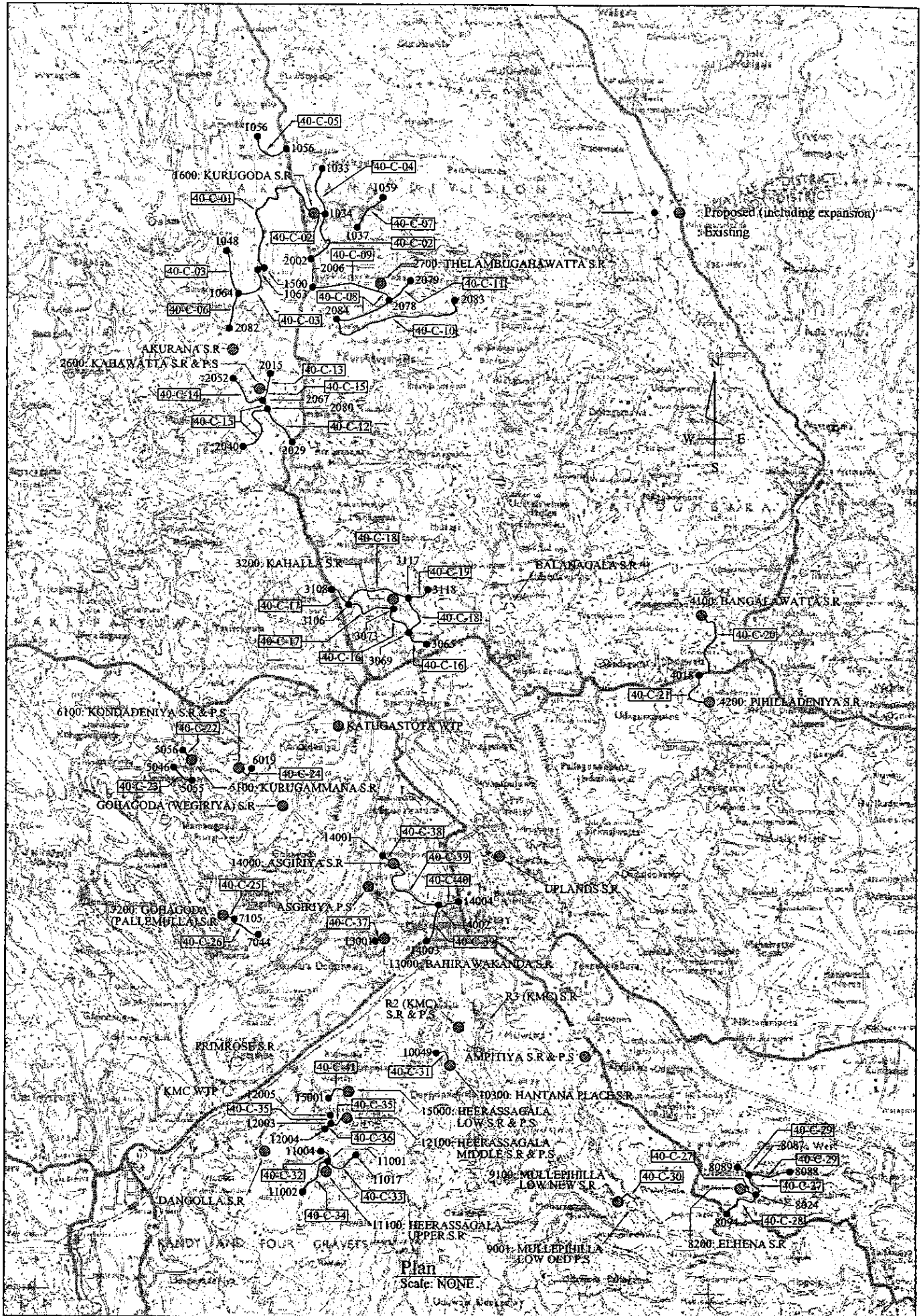
To monitor the total water amount supplied to the consumers and bulk supply to KMC area, flow meters shall be equipped, at the outlet pipe of service reservoirs.

Further, the water amount supplied to each service zone shall be recorded, and analyzed for the water demand situations, which could be reviewed for future water demand projections as well.

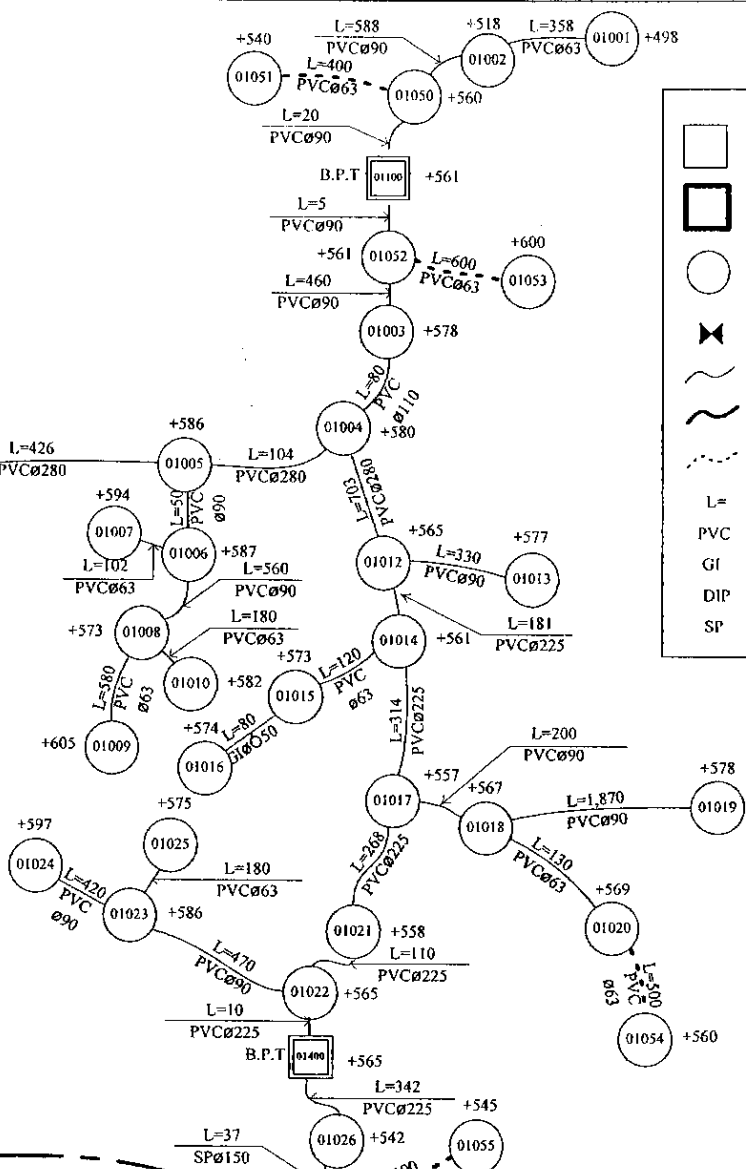
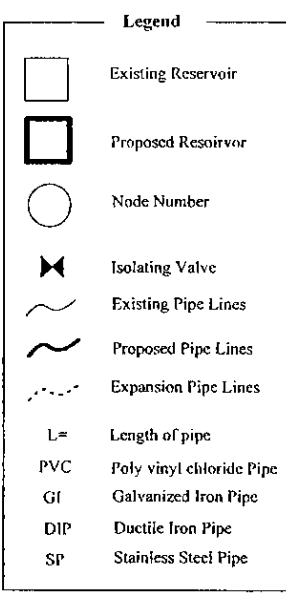
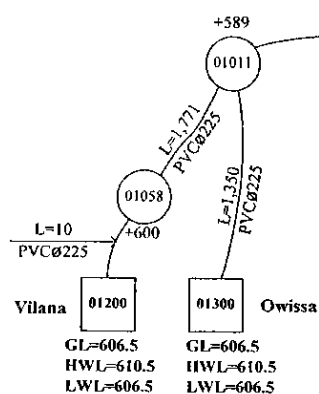
6) ACP in Ampitiya Service Area

In this Water Supply Scheme, many AC pipelines were installed and are existing in use, which are weak material compare with PVC or DCIP, thus it is deteriorated and broken easily affected by external load.

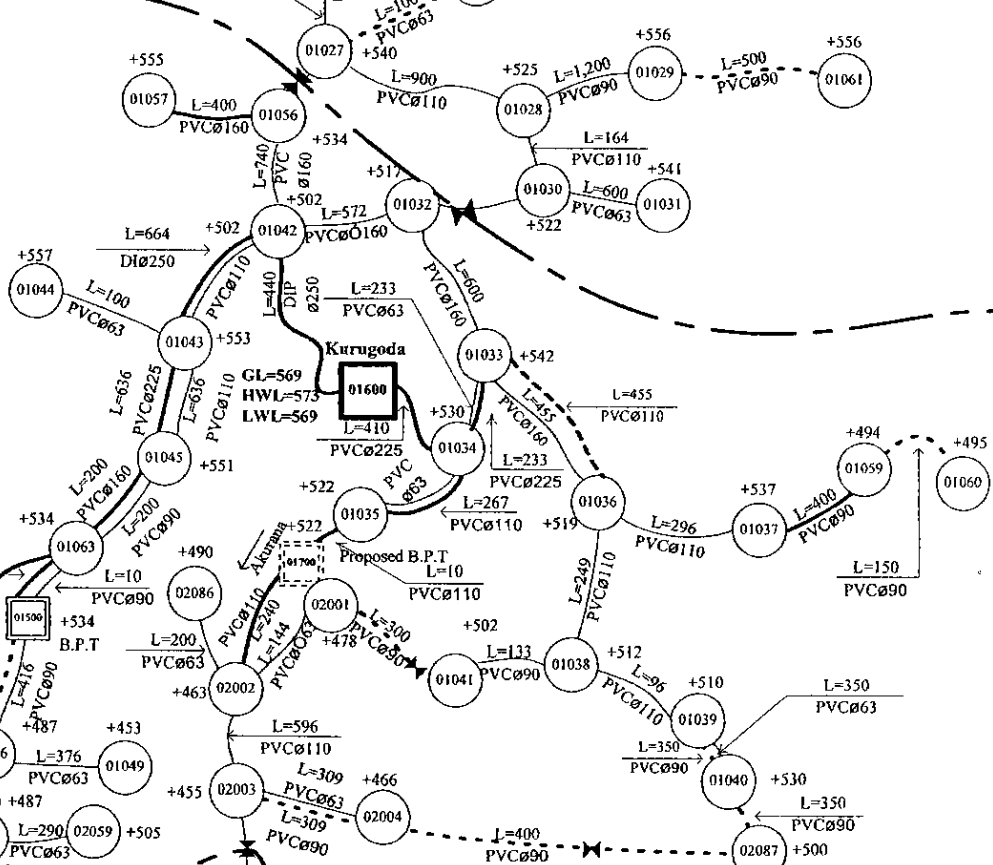
In the future, these AC pipes are recommended replaced with PVC pipes or DCIP, to avoid leakage from broken pipes and to reduce pipe repair works, under a plan for strengthening pipeline.



Vilana & Owissa Reservoir Service Area



Kurugoda Reservoir Service Area



Appendix - 5.1 Improvement of Distribution Network in 2015 (Vilana & Owissa, Kurugoda Reservoir Service Areas)

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* * * * * K Y P I P E 2 * * * * *
*   University of Kentucky Hydraulic Analysis Program   *
* Distribution of Pressure and Flows in Piping Networks *
*           1000 PIPE VERSION - 1.10   (08/25/92)       *
* * * * *
  
```

DATE: 3/ 7/2002
 TIME: 10:29:32

INPUT DATA FILENAME ----- c:\D_nets\2015\KURU2015.DAT
 TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\KURU2015.OUT
 POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\KURU2015.RES

 S U M M A R Y O F O R I G I N A L D A T A

U N I T S S P E C I F I E D

FLOWRATE = liters/second
 HEAD (HGL) = meters
 PRESSURE = kpa

R E G U L A T I N G V A L V E D A T A

VALVE TYPE	POSITION JUNCTION	CONTROLLED PIPE	VALVE SETTING (m or l/s)
PRV-1	1500	14	534.00
PRV-1	1500	47	534.00
PRV-1	1700	59	525.30

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1	2077	2063	100.0	7.9	130.00	.00	

2	2063	2062	130.0	5.5	120.00	.00
3	2062	2061	370.0	7.9	120.00	.00
4	2061	2060	660.0	9.7	120.00	.00
5	2060	2082	380.0	14.0	120.00	.00
6	2082	2058	300.0	14.0	120.00	.00
7	2058	2075	50.0	5.5	120.00	.00
8	1048	1047	400.0	5.5	120.00	.00
9	1064	1046	128.0	7.9	120.00	.00
10	1064	2082	500.0	14.0	130.00	.00
11	2076	2075	200.0	7.9	130.00	.00
12	1046	1049	376.0	5.5	120.00	.00
13	2075	2059	290.0	5.5	120.00	.00
14-RV	1500	1046	416.0	7.9	120.00	.00
15	1045	1063	200.0	7.9	120.00	.00
16	1045	1043	636.0	9.7	120.00	.00
17	1043	1044	100.0	5.5	120.00	.00
18	1043	1042	664.0	9.7	120.00	.00
19	1042	1056	740.0	14.0	120.00	.00
20	1056	1057	400.0	7.9	130.00	.00
21	1042	1032	572.0	14.0	120.00	.00
22-FG	0	1042	440.0	25.0	130.00	.00
23-FG	0	1034	410.0	19.8	130.00	.00
24	1034	1035	267.0	5.5	120.00	.00
25	1035	1700	10.0	9.7	130.00	.00
26	2001	2002	144.0	5.5	120.00	.00
27	2002	2003	396.0	9.7	120.00	.00
28	2003	2004	309.0	5.5	120.00	.00
29	1032	1033	600.0	14.0	120.00	.00
30	1033	1034	233.0	5.5	120.00	.00
31	1033	1036	455.0	14.0	120.00	.00
32	1036	1037	296.0	9.7	120.00	.00
33	1037	1059	400.0	7.9	130.00	.00
34	1059	1060	150.0	7.9	130.00	.00
35	1036	1038	249.0	9.7	120.00	.00
36	1038	1039	96.0	9.7	120.00	.00
37	1039	1040	350.0	5.5	120.00	.00
38	1038	1041	133.0	7.9	120.00	.00
39	1063	1048	1060.0	7.9	130.00	.00
40	1063	1500	10.0	7.9	120.00	.00
41	1034	1035	267.0	9.7	130.00	.00
42	1039	1040	350.0	5.5	120.00	.00
43	1043	1042	664.0	25.0	130.00	.00
44	2003	2004	309.0	7.9	130.00	.00
45	1045	1043	636.0	19.8	130.00	.00
46	1045	1063	200.0	14.0	130.00	.00
47-RV	1500	1046	416.0	14.0	130.00	.00
48	2058	2075	50.0	7.9	130.00	.00
49	2062	2061	370.0	7.9	130.00	.00
50	2063	2062	130.0	7.9	130.00	.00
51	1033	1034	233.0	19.8	130.00	.00
52	1063	1500	10.0	14.0	130.00	.00
53	1064	1047	110.0	7.9	120.00	.00
54	2002	2086	200.0	9.7	120.00	.00

569.
569.

55-XX	2001	1041	300.0	7.9	130.00	.00
56-XX	2004	2087	400.0	7.9	130.00	.00
57	2087	1040	350.0	7.9	130.00	.00
58	1039	1040	350.0	9.7	130.00	.00
59-RV	1700	2002	240.0	9.7	130.00	.00
60	2060	2061	660.0	7.9	130.00	.00
61	2082	2060	380.0	7.9	130.00	.00
62	1046	1064	120.0	7.9	130.00	.00
63	1033	1036	455.0	9.7	130.00	.00

JUNCTION NODE DATA

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	JUNCTION ELEVATION (m)	CONNECTING PIPES				
1032		5.14	517.00	21	29			
1033		.78	542.00	29	30	31	51	63
1034		.81	530.00	23	24	30	41	51
1035		.57	522.00	24	25	41		
1036		.53	519.00	31	32	35	63	
1037		.65	537.00	32	33			
1038		.45	512.00	35	36	38		
1039		.36	510.00	36	37	42	58	
1040		.32	530.00	37	42	57	58	
1041		.19	502.00	38	55			
1042		2.74	502.00	18	19	21	22	43
1043		.90	553.00	16	17	18	43	45
1044		.05	557.00	17				
1045		.44	551.00	15	16	45	46	
1046		2.23	487.00	9	12	14	47	62
1047		.71	482.00	8	53			
1048		.44	529.00	8	39			
1049		.71	453.00	12				
1056		1.34	534.00	19	20			
1057		.14	555.00	20				
1059		.18	494.00	33	34			
1060		4.95	495.00	34				
1063		1.19	534.00	15	39	40	46	52
1064		.85	482.00	9	10	53	62	
1500		.00	.00	14	40	47	52	
1700		.00	.00	25	59			
2001		.21	478.00	26	55			
2002		.93	463.00	26	27	54	59	
2003		2.20	455.00	27	28	44		
2004		3.25	466.00	28	44	56		
2058		.42	500.00	6	7	48		
2059		.31	505.00	13				
2060		.87	489.00	4	5	60	61	
2061		3.70	456.00	3	4	49	60	

2062	1.41	475.00	2	3	49	50
2063	.65	490.00	1	2	50	
2075	.84	500.00	7	11	13	48
2076	.10	480.00	11			
2077	.44	500.00	1			
2082	1.06	495.00	5	6	10	61
2086	.17	490.00	54			
2087	3.06	500.00	56	57		

O U T P U T O P T I O N D A T A

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

S Y S T E M C O N F I G U R A T I O N

NUMBER OF PIPES (p) = 63
 NUMBER OF JUNCTION NODES (j) = 42
 NUMBER OF PRIMARY LOOPS (l) = 20
 NUMBER OF FIXED GRADE NODES (f) = 2
 NUMBER OF SUPPLY ZONES (z) = 1

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 8 TRIALS WITH AN ACCURACY = .00246

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/1000 (m/m)
1	2077	2063	-.44	.02	.00	.00	.09	.1
2	2063	2062	-.29	.07	.00	.00	.12	.5
3	2062	2061	-1.20	.51	.00	.00	.24	1.3
4	2061	2060	-3.80	2.82	.00	.00	.51	4.2
5	2060	2082	-5.70	.58	.00	.00	.37	1.5
6	2082	2058	1.67	.05	.00	.00	.11	.1
7	2058	2075	.33	.04	.00	.00	.14	.7
8	1048	1047	3.46	22.82	.00	.00	1.46	57.0
9	1064	1046	-3.72	1.43	.00	.00	.76	11.1

JOB NAME = GKWSAP - JICA - Kurugoda SR

10	1064	2082	9.80	1.78	.00	.00	.64	3.5
11	2076	2075	-.10	.00	.00	.00	.02	.0
12	1046	1049	.71	1.14	.00	.00	.30	3.0
13	2075	2059	.31	.19	.00	.00	.13	.6
14-RV	1500	1046	1.84	1.26	.00	.00	.38	3.0
15	1045	1063	2.71	1.24	.00	.00	.55	6.2
16	1045	1043	-2.03	.85	.00	.00	.27	1.3
17	1043	1044	.05	.00	.00	.00	.02	.0
18	1043	1042	-1.26	.37	.00	.00	.17	.5
19	1042	1056	1.48	.09	.00	.00	.10	.1
20	1056	1057	.14	.01	.00	.00	.03	.0
21	1042	1032	4.81	.63	.00	.00	.31	1.1
22-FG	0	1042	26.35	.58	.00	.00	.54	1.3
23-FG	0	1034	19.94	1.01	.00	.00	.65	2.4
24	1034	1035	1.26	2.34	.00	.00	.53	8.7
25	1035	1700	6.76	.11	.00	.00	.91	10.7
26	2001	2002	-.21	.05	.00	.00	.09	.3
27	2002	2003	5.45	3.30	.00	.00	.74	8.3
28	2003	2004	.85	1.32	.00	.00	.36	4.2
29	1032	1033	-.33	.00	.00	.00	.02	.0
30	1033	1034	-.36	.20	.00	.00	.15	.8
31	1033	1036	7.57	1.17	.00	.00	.49	2.5
32	1036	1037	5.78	2.75	.00	.00	.78	9.2
33	1037	1059	5.13	6.98	.00	.00	1.05	17.4
34	1059	1060	4.95	2.45	.00	.00	1.01	16.3
35	1036	1038	4.38	1.38	.00	.00	.59	5.5
36	1038	1039	3.74	.40	.00	.00	.51	4.1
37	1039	1040	.50	.55	.00	.00	.21	1.5
38	1038	1041	.19	.01	.00	.00	.04	.0
39	1063	1048	3.90	11.15	.00	.00	.80	10.5
40	1063	1500	1.84	.03	.00	.00	.38	3.0
41	1034	1035	6.07	2.34	.00	.00	.82	8.7
42	1039	1040	.50	.55	.00	.00	.21	1.5
43	1043	1042	-16.06	.35	.00	.00	.33	.5
44	2003	2004	2.40	1.32	.00	.00	.49	4.2
45	1045	1043	-14.34	.85	.00	.00	.47	1.3
46	1045	1063	13.22	1.24	.00	.00	.86	6.2
47-RV	1500	1046	8.99	1.26	.00	.00	.58	3.0
48	2058	2075	.92	.04	.00	.00	.19	.7
49	2062	2061	-1.30	.51	.00	.00	.27	1.3
50	2063	2062	-.80	.07	.00	.00	.16	.5
51	1033	1034	-11.43	.20	.00	.00	.37	.8
52	1063	1500	8.99	.03	.00	.00	.58	3.0
53	1064	1047	-2.75	.70	.00	.00	.56	6.3
54	2002	2086	.17	.00	.00	.00	.02	.0
55-XX	2001	1041						
56-XX	2004	2087						
57	2087	1040	-3.06	2.34	.00	.00	.62	6.7
58	1039	1040	2.39	.55	.00	.00	.32	1.5
59-RV	1700	2002	6.76	2.57	.00	.00	.91	10.7
60	2060	2061	2.40	2.82	.00	.00	.49	4.2
61	2082	2060	1.37	.58	.00	.00	.28	1.5
62	1046	1064	4.17	1.43	.00	.00	.85	11.9

63 1033 1036 3.12 1.17 .00 .00 .42 2.5

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
1032		5.14	567.78	517.00	50.78	498.03
1033		.78	567.79	542.00	25.79	252.90
1034		.81	567.99	530.00	37.99	372.59
1035		.57	565.65	522.00	43.65	428.09
1036		.53	566.62	519.00	47.62	467.03
1037		.65	563.87	537.00	26.87	263.55
1038		.45	565.24	512.00	53.24	522.11
1039		.36	564.84	510.00	54.84	537.82
1040		.32	564.30	530.00	34.30	336.34
1041		.19	565.23	502.00	63.23	620.12
1042		2.74	568.42	502.00	66.42	651.34
1043		.90	568.05	553.00	15.05	147.60
1044		.05	568.05	557.00	11.05	108.35
1045		.44	567.20	551.00	16.20	158.89
1046		2.23	532.74	487.00	45.74	448.51
1047		.71	532.01	482.00	50.01	490.43
1048		.44	554.82	529.00	25.82	253.26
1049		.71	531.60	453.00	78.60	770.77
1056		1.34	568.33	534.00	34.33	336.62
1057		.14	568.32	555.00	13.32	130.60
1059		.18	556.90	494.00	62.90	616.81
1060		4.95	554.45	495.00	59.45	582.99
1063		1.19	565.98	534.00	31.98	313.59
1064		.85	531.31	482.00	49.31	483.53
1500		.00	565.95			
1700		.00	565.55			
2001		.21	522.69	478.00	44.69	438.22
2002		.93	522.73	463.00	59.73	585.77
2003		2.20	519.43	455.00	64.43	631.88
2004		3.25	518.12	466.00	52.12	511.10
2058		.42	529.48	500.00	29.48	289.07
2059		.31	529.25	505.00	24.25	237.83
2060		.87	528.95	489.00	39.95	391.76
2061		3.70	526.13	456.00	70.13	687.73
2062		1.41	525.62	475.00	50.62	496.43
2063		.65	525.55	490.00	35.55	348.61
2075		.84	529.44	500.00	29.44	288.72
2076		.10	529.44	480.00	49.44	484.83
2077		.44	525.53	500.00	25.53	250.36
2082		1.06	529.52	495.00	34.52	338.57
2086		.17	522.73	490.00	32.73	320.96
2087		3.06	561.95	500.00	61.95	607.54

R E G U L A T I N G V A L V E R E P O R T

VALVE TYPE	POSITION NODE	CONTROLLED PIPE	VALVE SETTING (m or l/s)	VALVE STATUS	UPSTREAM GRADE (m)	DOWNSTREAM GRADE (m)	THROUGH FLOW (l/s)
PRV-1	1500	14	534.00	THROTTLED	565.95	532.74	1.84
PRV-1	1500	47	534.00	THROTTLED	565.95	532.74	8.99
PRV-1	1700	59	525.30	THROTTLED	565.55	522.73	6.76

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
22	26.35
23	19.94

NET SYSTEM INFLOW = 46.29
 NET SYSTEM OUTFLOW = .00
 NET SYSTEM DEMAND = 46.29

D A T A C H A N G E S F O R N E X T S I M U L A T I O N

D E M A N D C H A N G E S

DEMAND TYPE = 1 - GDF = .300

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00424

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	#2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1	2077	2063	-.13	.00	.00	.00	.03	.0
2	2063	2062	-.09	.01	.00	.00	.04	.0
3	2062	2061	-.36	.05	.00	.00	.07	.1
4	2061	2060	-1.14	.30	.00	.00	.15	.4
5	2060	2082	-1.71	.06	.00	.00	.11	.1
6	2082	2058	.50	.01	.00	.00	.03	.0
7	2058	2075	.10	.00	.00	.00	.04	.0
8	1048	1047	3.54	23.74	.00	.00	1.49	59.3
9	1064	1046	.06	.00	.00	.00	.01	.0
10	1064	2082	2.94	.19	.00	.00	.19	.3
11	2076	2075	-.03	.00	.00	.00	.01	.0
12	1046	1049	.21	.12	.00	.00	.09	.3
13	2075	2059	.09	.02	.00	.00	.04	.0
14-RV	1500	1046	.13	.01	.00	.00	.03	.0
15	1045	1063	.81	.13	.00	.00	.17	.6
16	1045	1043	-.61	.09	.00	.00	.08	.1
17	1043	1044	.02	.00	.00	.00	.01	.0
18	1043	1042	-.37	.04	.00	.00	.05	.0
19	1042	1056	.44	.01	.00	.00	.03	.0
20	1056	1057	.04	.00	.00	.00	.01	.0
21	1042	1032	1.44	.07	.00	.00	.09	.1
22-FG	0	1042	7.91	.06	.00	.00	.16	.1
23-FG	0	1034	5.98	.11	.00	.00	.19	.2
24	1034	1035	.38	.25	.00	.00	.16	.9
25	1035	1700	2.03	.01	.00	.00	.27	1.1
26	2001	2002	-.06	.00	.00	.00	.03	.0
27	2002	2003	1.63	.35	.00	.00	.22	.9
28	2003	2004	.26	.14	.00	.00	.11	.4
29	1032	1033	-.10	.00	.00	.00	.01	.0
30	1033	1034	-.11	.02	.00	.00	.05	.0
31	1033	1036	2.27	.13	.00	.00	.15	.2
32	1036	1037	1.73	.30	.00	.00	.23	1.0
33	1037	1059	1.54	.75	.00	.00	.31	1.8
34	1059	1060	1.49	.26	.00	.00	.30	1.7
35	1036	1038	1.31	.15	.00	.00	.18	.6
36	1038	1039	1.12	.04	.00	.00	.15	.4
37	1039	1040	.15	.06	.00	.00	.06	.1
38	1038	1041	.06	.00	.00	.00	.01	.0
39	1063	1048	3.67	9.95	.00	.00	.75	9.3
40	1063	1500	.13	.00	.00	.00	.03	.0
41	1034	1035	1.82	.25	.00	.00	.25	.9
42	1039	1040	.15	.06	.00	.00	.06	.1
43	1043	1042	-4.83	.04	.00	.00	.10	.0
44	2003	2004	.72	.14	.00	.00	.15	.4
45	1045	1043	-4.30	.09	.00	.00	.14	.1
46	1045	1063	3.97	.13	.00	.00	.26	.6
47-RV	1500	1046	.62	.01	.00	.00	.04	.0
48	2058	2075	.28	.00	.00	.00	.06	.0
49	2062	2061	-.39	.05	.00	.00	.08	.1

50	2063	2062	-.24	.01	.00	.00	.05	.0
51	1033	1034	-3.43	.02	.00	.00	.11	.0
52	1063	1500	.62	.00	.00	.00	.04	.0
53	1064	1047	-3.33	1.00	.00	.00	.68	9.0
54	2002	2086	.05	.00	.00	.00	.01	.0
55-XX	2001	1041						
56-XX	2004	2087						
57	2087	1040	-.92	.25	.00	.00	.19	.7
58	1039	1040	.72	.06	.00	.00	.10	.1
59-RV	1700	2002	2.03	.28	.00	.00	.27	1.1
60	2060	2061	.72	.30	.00	.00	.15	.4
61	2082	2060	.41	.06	.00	.00	.08	.1
62	1046	1064	-.07	.00	.00	.00	.01	.0
63	1033	1036	.94	.13	.00	.00	.13	.2

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
1032		1.54	568.87	517.00	51.87	508.67
1033		.23	568.87	542.00	26.87	263.50
1034		.24	568.89	530.00	38.89	381.40
1035		.17	568.64	522.00	46.64	457.38
1036		.16	568.74	519.00	49.74	487.83
1037		.20	568.45	537.00	31.45	308.41
1038		.14	568.60	512.00	56.60	555.02
1039		.11	568.55	510.00	58.55	574.21
1040		.10	568.49	530.00	38.49	377.50
1041		.06	568.59	502.00	66.59	653.08
1042		.82	568.94	502.00	66.94	656.44
1043		.27	568.90	553.00	15.90	155.92
1044		.02	568.90	557.00	11.90	116.69
1045		.13	568.81	551.00	17.81	174.64
1046		.67	533.99	487.00	46.99	460.83
1047		.21	534.99	482.00	52.99	519.65
1048		.13	558.73	529.00	29.73	291.54
1049		.21	533.87	453.00	80.87	793.05
1056		.40	568.93	534.00	34.93	342.52
1057		.04	568.93	555.00	13.93	136.57
1059		.05	567.70	494.00	73.70	722.74
1060		1.49	567.43	495.00	72.43	710.35
1063		.36	568.67	534.00	34.67	340.04
1064		.26	533.99	482.00	51.99	509.87
1500		.00	568.67			
1700		.00	568.63			
2001		.06	525.02	478.00	47.02	461.10
2002		.28	525.02	463.00	62.02	608.25
2003		.66	524.67	455.00	69.67	683.22
2004		.98	524.53	466.00	58.53	573.96

2058	.13	533.79	500.00	33.79	331.42
2059	.09	533.77	505.00	28.77	282.15
2060	.26	533.74	489.00	44.74	438.73
2061	1.11	533.43	456.00	77.43	759.38
2062	.42	533.38	475.00	58.38	572.52
2063	.20	533.37	490.00	43.37	425.34
2075	.25	533.79	500.00	33.79	331.38
2076	.03	533.79	480.00	53.79	527.51
2077	.13	533.37	500.00	33.37	327.25
2082	.32	533.80	495.00	38.80	380.50
2086	.05	525.02	490.00	35.02	343.46
2087	.92	568.24	500.00	68.24	669.23

R E G U L A T I N G V A L V E R E P O R T

VALVE TYPE	POSITION NODE	CONTROLLED PIPE	VALVE SETTING (m or l/s)	VALVE STATUS	UPSTREAM GRADE (m)	DOWNSTREAM GRADE (m)	THROUGH FLOW (l/s)
PRV-1	1500	14	534.00	THROTTLED	568.67	533.99	.13
PRV-1	1500	47	534.00	THROTTLED	568.67	533.99	.62
PRV-1	1700	59	525.30	THROTTLED	568.63	525.02	2.03

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

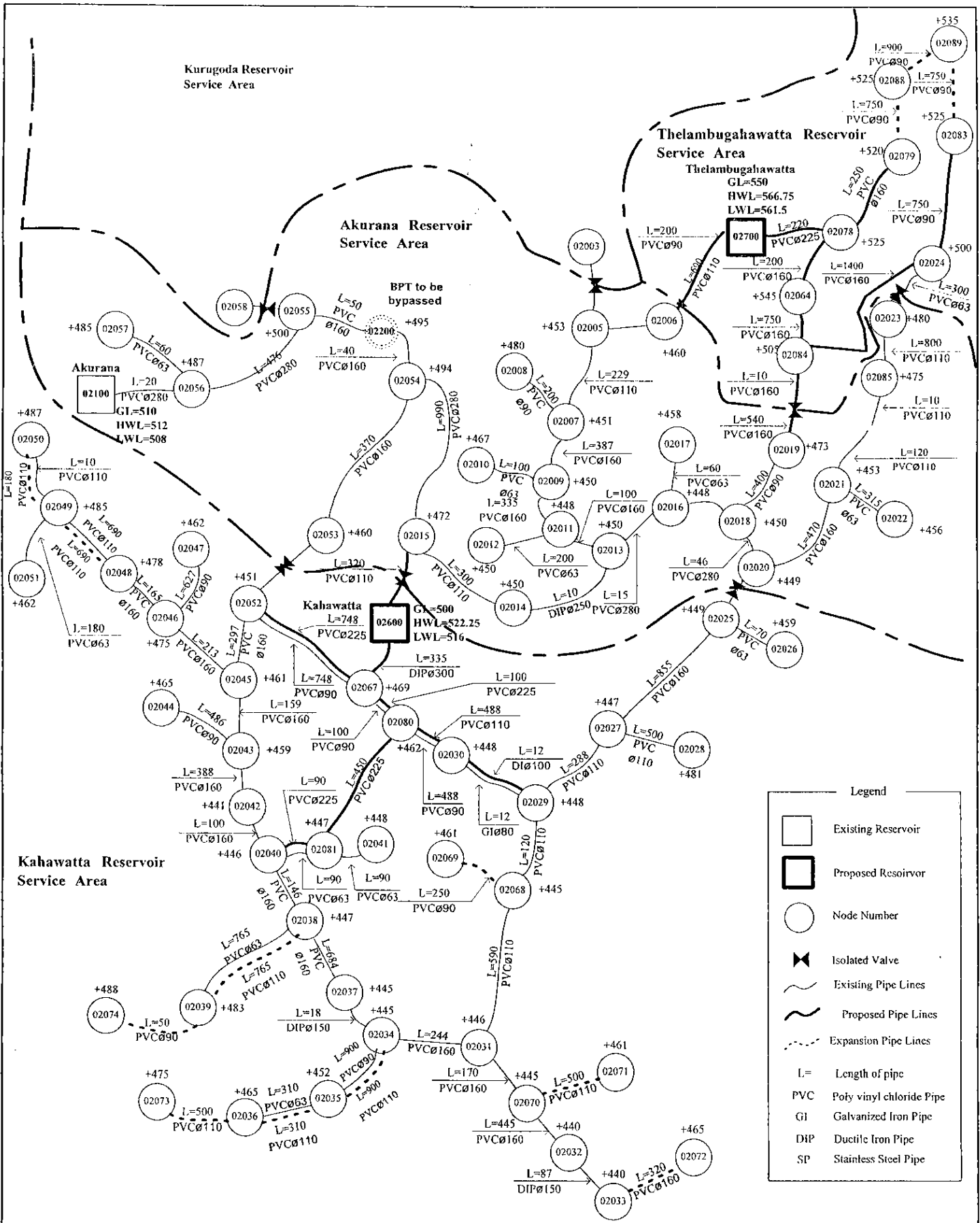
(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
22	7.91
23	5.98

NET SYSTEM INFLOW = 13.89
 NET SYSTEM OUTFLOW = .00
 NET SYSTEM DEMAND = 13.89

**** KYPIPE SIMULATION COMPLETED ****

DATE: 3/ 7/2002
 TIME: 10:29:32



Legend

- Existing Reservoir
- Proposed Reservoir
- Node Number
- Isolated Valve
- Existing Pipe Lines
- Proposed Pipe Lines
- Expansion Pipe Lines
- L= Length of pipe
- PVC Poly vinyl chloride Pipe
- GI Galvanized Iron Pipe
- DIP Ductile Iron Pipe
- SP Stainless Steel Pipe

**Appendix - 5.2 Improvement of Distribution Network in 2015
(Akurana, Thelambughawatta, Kahawatta Reservoir Service Areas)**

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* * * * * K Y P I P E 2 * * * * *
*   University of Kentucky Hydraulic Analysis Program   *
* Distribution of Pressure and Flows in Piping Networks *
*       1000 PIPE VERSION - 1.10   (08/25/92)         *
* * * * *
    
```

DATE: 3/ 7/2002
 TIME: 10:30:33

INPUT DATA FILENAME ----- c:\D_nets\2015\THEL2015.DAT
 TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\THEL2015.OUT
 POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\THEL2015.RES

 S U M M A R Y O F O R I G I N A L D A T A

U N I T S S P E C I F I E D

FLOWRATE = liters/second
 HEAD (HGL) = meters
 PRESSURE = kpa

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1 #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-FG	0 2006	690.0	9.7	130.00	.00	561.
2-FG	0 2078	220.0	19.8	130.00	.00	561.
3	2078 2064	200.0	19.8	130.00	.00	
4	2064 2084	750.0	14.0	130.00	.00	
5	2078 2079	250.0	14.0	130.00	.00	
6	2084 2024	1400.0	14.0	130.00	.00	
7	2024 2083	750.0	7.9	130.00	.00	
8	2083 2089	750.0	7.9	130.00	.00	
9	2079 2088	750.0	7.9	130.00	.00	
10	2088 2089	900.0	7.9	130.00	.00	

JUNCTION NODE DATA

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	JUNCTION ELEVATION (m)	CONNECTING PIPES		
2006		3.50	460.00	1		
2024		3.77	500.00	6	7	
2064		6.40	545.00	3	4	
2078		9.46	525.00	2	3	5
2079		2.50	520.00	5	9	
2083		1.19	525.00	7	8	
2084		7.53	505.00	4	6	
2088		1.12	525.00	9	10	
2089		1.29	535.00	8	10	

OUTPUT OPTION DATA

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

SUPPLY ZONE DATA

THIS SYSTEM HAS MULTIPLE SUPPLY ZONES

ZONE NO. 1 IS SUPPLIED THROUGH THESE PIPES:

2

SYSTEM CONFIGURATION

NUMBER OF PIPES (p) = 10
NUMBER OF JUNCTION NODES (j) = 9
NUMBER OF PRIMARY LOOPS (l) = 1
NUMBER OF FIXED GRADE NODES (f) = 2
NUMBER OF SUPPLY ZONES (z) = 2

SIMULATION RESULTS

THE RESULTS ARE OBTAINED AFTER 4 TRIALS WITH AN ACCURACY = .00134

PIPELINE RESULTS

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	2006	3.50	2.18	.00	.00	.47	3.1
2-FG	0	2078	33.26	1.39	.00	.00	1.08	6.3
3	2078	2064	18.58	.43	.00	.00	.60	2.1
4	2064	2084	12.18	4.00	.00	.00	.79	5.3
5	2078	2079	5.22	.28	.00	.00	.34	1.1
6	2084	2024	4.65	1.26	.00	.00	.30	.9
7	2024	2083	.88	.50	.00	.00	.18	.6
8	2083	2089	-.31	.07	.00	.00	.06	.1
9	2079	2088	2.72	4.03	.00	.00	.55	5.3
10	2088	2089	1.60	1.81	.00	.00	.33	2.0

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTION PRESSURE (kpa)
2006		3.50	559.32	460.00	99.32	973.98
2024		3.77	554.42	500.00	54.42	533.66
2064		6.40	559.67	545.00	14.67	143.91
2078		9.46	560.11	525.00	35.11	344.28
2079		2.50	559.83	520.00	39.83	390.59
2083		1.19	553.92	525.00	28.92	283.57
2084		7.53	555.67	505.00	50.67	496.95
2088		1.12	555.80	525.00	30.80	302.00
2089		1.29	553.99	535.00	18.99	186.20

SUMMARY OF INFLOWS AND OUTFLOWS

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
(-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	3.50
2	33.26
NET SYSTEM INFLOW =	36.76
NET SYSTEM OUTFLOW =	.00
NET SYSTEM DEMAND =	36.76

D A T A C H A N G E S F O R N E X T S I M U L A T I O N

D E M A N D C H A N G E S

DEMAND TYPE = 1 - GDF = .300

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	2006	1.05	.23	.00	.00	.14	.3
2-FG	0	2078	9.98	.15	.00	.00	.32	.6
3	2078	2064	5.57	.05	.00	.00	.18	.2
4	2064	2084	3.65	.43	.00	.00	.24	.5
5	2078	2079	1.57	.03	.00	.00	.10	.1
6	2084	2024	1.40	.14	.00	.00	.09	.1
7	2024	2083	.26	.05	.00	.00	.05	.0
8	2083	2089	-.09	.01	.00	.00	.02	.0
9	2079	2088	.82	.43	.00	.00	.17	.5
10	2088	2089	.48	.19	.00	.00	.10	.2

J U N C T I O N N O D E R E S U L T S

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
2006		1.05	561.27	460.00	101.27	993.08
2024		1.13	560.74	500.00	60.74	595.64
2064		1.92	561.30	545.00	16.30	159.89
2078		2.84	561.35	525.00	36.35	356.47
2079		.75	561.32	520.00	41.32	405.22

2083	.36	560.68	525.00	35.68	349.95
2084	2.26	560.87	505.00	55.87	547.93
2088	.34	560.89	525.00	35.89	351.93
2089	.39	560.69	535.00	25.69	251.95

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

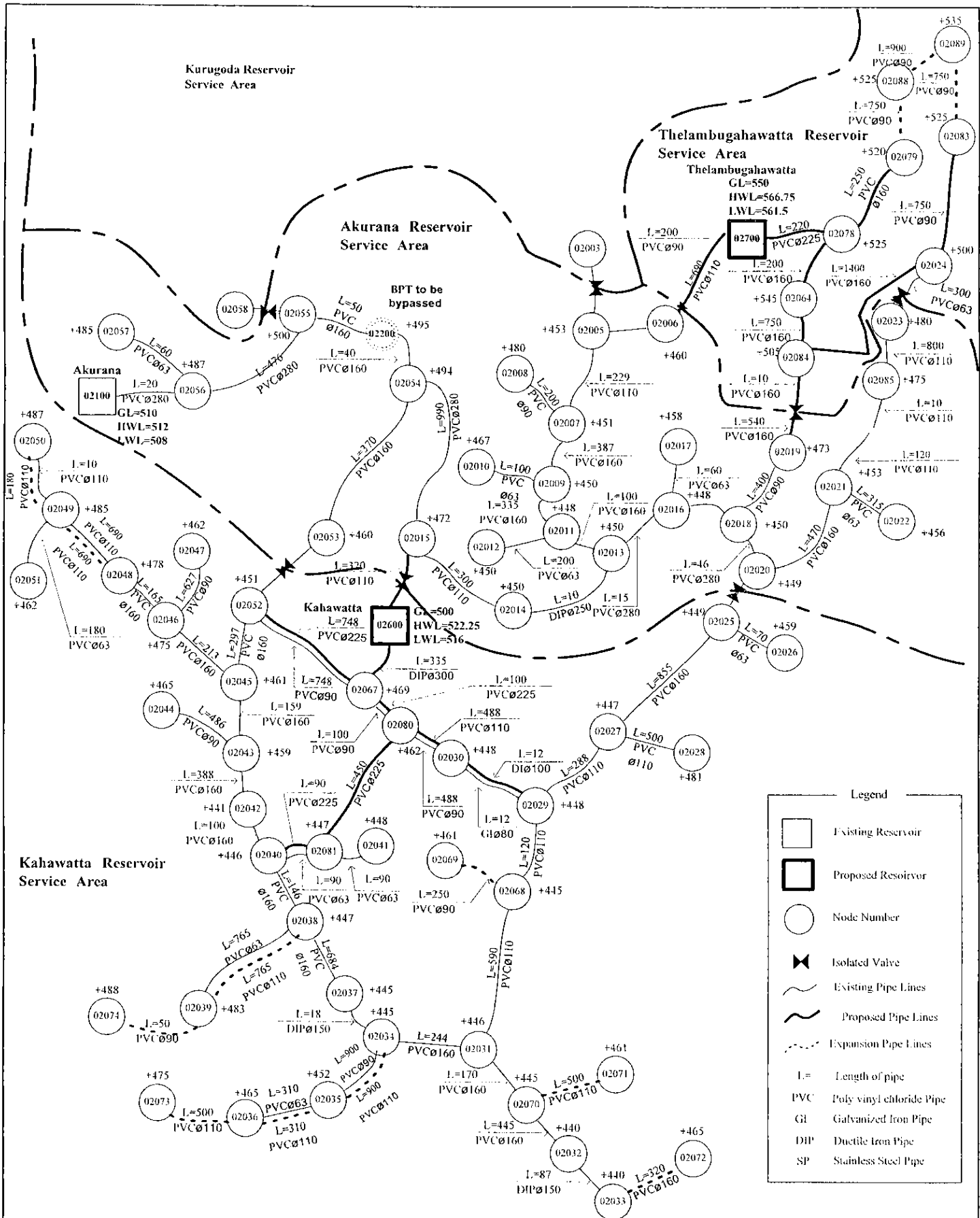
(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
(-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	1.05
2	9.98

NET SYSTEM INFLOW = 11.03
NET SYSTEM OUTFLOW = .00
NET SYSTEM DEMAND = 11.03

**** KYPIPE SIMULATION COMPLETED ****

DATE: 3/ 7/2002
TIME: 10:30:33



Appendix - 5.2 Improvement of Distribution Network in 2015
 (Akurana, Thelambughawatta, Kahawatta Reservoir Service Areas)

***** K Y P I P E 2 *****
 * University of Kentucky Hydraulic Analysis Program *
 * Distribution of Pressure and Flows in Piping Networks *
 * 1000 PIPE VERSION - 1.10 (08/25/92) *

DATE: 3/ 7/2002
 TIME: 10:33: 4

INPUT DATA FILENAME ----- c:\D_nets\2015\KAHW2015.DAT
 TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\KAHW2015.OUT
 POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\KAHW2015.RES

 S U M M A R Y O F O R I G I N A L D A T A

U N I T S S P E C I F I E D

FLOWRATE = liters/second
 HEAD (HGL) = meters
 PRESSURE = kpa

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-FG	0	2067	335.0	30.0	130.00	.00	516.
2	2067	2052	848.0	7.9	120.00	.00	
3	2067	2080	100.0	7.9	120.00	.00	
4	2052	2045	297.0	14.0	120.00	.00	
5	2045	2043	159.0	14.0	120.00	.00	
6	2045	2046	213.0	14.0	120.00	.00	
7	2043	2042	388.0	14.0	120.00	.00	
8	2043	2044	486.0	7.9	120.00	.00	
9	2042	2040	100.0	14.0	120.00	.00	
10	2040	2038	146.0	14.0	120.00	.00	
11	2040	2081	90.0	5.5	120.00	.00	
12	2081	2041	90.0	5.5	120.00	.00	
13	2081	2080	450.0	19.8	130.00	.00	

14	2038	2039	765.0	5.5	120.00	.00
15	2038	2037	684.0	14.0	120.00	.00
16	2039	2074	50.0	7.9	130.00	.00
17	2037	2034	18.0	15.0	120.00	.00
18	2034	2035	900.0	7.9	120.00	.00
19	2034	2031	244.0	14.0	120.00	.00
20	2035	2036	310.0	5.5	120.00	.00
21	2036	2073	500.0	9.7	130.00	.00
22	2031	2070	170.0	14.0	120.00	.00
23	2031	2068	590.0	9.7	120.00	.00
24	2070	2032	445.0	14.0	120.00	.00
25	2070	2071	500.0	9.7	130.00	.00
26	2032	2033	87.0	15.0	120.00	.00
27	2033	2072	320.0	14.0	130.00	.00
28	2068	2029	120.0	9.7	120.00	.00
29	2068	2069	250.0	7.9	130.00	.00
30	2029	2030	12.0	8.0	120.00	.00
31	2029	2027	288.0	9.7	120.00	.00
32	2030	2080	488.0	7.9	120.00	.00
33	2027	2028	500.0	9.7	120.00	.00
34	2027	2025	855.0	14.0	120.00	.00
35	2025	2026	70.0	5.5	120.00	.00
36	2046	2047	627.0	7.9	120.00	.00
37	2046	2048	165.0	14.0	120.00	.00
38	2048	2049	690.0	9.7	120.00	.00
39	2049	2050	10.0	9.7	120.00	.00
40	2049	2051	180.0	5.5	120.00	.00
41	2067	2052	848.0	19.8	130.00	.00
42	2067	2080	100.0	19.8	130.00	.00
43	2040	2081	90.0	19.8	130.00	.00
44	2038	2039	765.0	9.7	130.00	.00
45	2035	2036	310.0	9.7	130.00	.00
46	2029	2030	12.0	10.0	130.00	.00
47	2030	2080	188.0	9.7	130.00	.00
48	2048	2049	690.0	9.7	130.00	.00
49	2049	2050	10.0	9.7	130.00	.00
50	2034	2035	900.0	9.7	130.00	.00

JUNCTION NODE DATA

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	JUNCTION ELEVATION (m)	CONNECTING PIPES			
2025		.49	449.00	34	35		
2026		.02	459.00	35			
2027		1.31	447.00	31	33	34	
2028		.14	481.00	33			
2029		.35	448.00	28	30	31	46
2030		.18	448.00	30	32	46	47

2031	.74	446.00	19	22	23		
2032	1.89	440.00	24	26			
2033	1.90	440.00	26	27			
2034	1.48	445.00	17	18	19	50	
2035	.98	452.00	18	20	45	50	
2036	1.10	465.00	20	21	45		
2037	1.90	445.00	15	17			
2038	4.39	447.00	10	14	15	44	
2039	1.36	483.00	14	16	44		
2040	.48	446.00	9	10	11	43	
2041	.05	448.00	12				
2042	.84	441.00	7	9			
2043	1.22	459.00	5	7	8		
2044	.28	465.00	8				
2045	.65	461.00	4	5	6		
2046	1.52	475.00	6	36	37		
2047	1.61	462.00	36				
2048	3.86	478.00	37	38	48		
2049	1.63	485.00	38	39	40	48	49
2050	.43	487.00	39	49			
2051	.39	462.00	40				
2052	.98	451.00	2	4	41		
2067	1.24	469.00	1	2	3	41	42
2068	.67	445.00	23	28	29		
2069	.23	461.00	29				
2070	1.97	445.00	22	24	25		
2071	.40	461.00	25				
2072	7.05	465.00	27				
2073	.41	475.00	21				
2074	.54	488.00	16				
2080	1.18	462.00	3	13	32	42	47
2081	.44	447.00	11	12	13	43	

OUTPUT OPTION DATA

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

SYSTEM CONFIGURATION

NUMBER OF PIPES(p) = 50
 NUMBER OF JUNCTION NODES(j) = 38
 NUMBER OF PRIMARY LOOPS(l) = 12
 NUMBER OF FIXED GRADE NODES(f) = 1
 NUMBER OF SUPPLY ZONES(z) = 1

 SIMULATION RESULTS

THE RESULTS ARE OBTAINED AFTER 7 TRIALS WITH AN ACCURACY = .00213

PIPELINE RESULTS

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	2067	46.30	.52	.00	.00	.66	1.5
2	2067	2052	.91	.69	.00	.00	.18	.8
3	2067	2080	2.52	.54	.00	.00	.51	5.4
4	2052	2045	10.92	1.50	.00	.00	.71	5.0
5	2045	2043	.83	.01	.00	.00	.05	.0
6	2045	2046	9.44	.82	.00	.00	.61	3.8
7	2043	2042	-.67	.01	.00	.00	.04	.0
8	2043	2044	.28	.05	.00	.00	.06	.0
9	2042	2040	-1.51	.01	.00	.00	.10	.1
10	2040	2038	20.03	2.27	.00	.00	1.30	15.5
11	2040	2081	-.70	.27	.00	.00	.30	2.9
12	2081	2041	.05	.00	.00	.00	.02	.0
13	2081	2080	-22.50	1.38	.00	.00	.73	3.0
14	2038	2039	.33	.55	.00	.00	.14	.7
15	2038	2037	13.74	5.29	.00	.00	.89	7.7
16	2039	2074	.54	.01	.00	.00	.11	.2
17	2037	2034	11.84	.08	.00	.00	.67	4.1
18	2034	2035	.87	.68	.00	.00	.18	.7
19	2034	2031	7.87	.67	.00	.00	.51	2.7
20	2035	2036	.26	.15	.00	.00	.11	.4
21	2036	2073	.41	.03	.00	.00	.06	.0
22	2031	2070	13.21	1.22	.00	.00	.86	7.1
23	2031	2068	-6.08	6.02	.00	.00	.82	10.2
24	2070	2032	10.84	2.22	.00	.00	.70	4.9
25	2070	2071	.40	.03	.00	.00	.05	.0
26	2032	2033	8.95	.22	.00	.00	.51	2.5
27	2033	2072	7.05	.62	.00	.00	.46	1.9
28	2068	2029	-6.98	1.58	.00	.00	.94	13.1
29	2068	2069	.23	.01	.00	.00	.05	.0
30	2029	2030	-3.15	.09	.00	.00	.63	7.7
31	2029	2027	1.96	.36	.00	.00	.27	1.2
32	2030	2080	-2.30	2.24	.00	.00	.47	4.6
33	2027	2028	.14	.00	.00	.00	.02	.0
34	2027	2025	.51	.01	.00	.00	.03	.0
35	2025	2026	.02	.00	.00	.00	.01	.0
36	2046	2047	1.61	1.48	.00	.00	.33	2.3
37	2046	2048	6.31	.30	.00	.00	.41	1.8
38	2048	2049	1.18	.34	.00	.00	.16	.4

39	2049	2050	.21	.00	.00	.00	.03	.0
40	2049	2051	.39	.18	.00	.00	.16	1.0
41	2067	2052	11.00	.69	.00	.00	.36	.8
42	2067	2080	30.63	.54	.00	.00	.99	5.4
43	2040	2081	-21.31	.25	.00	.00	.69	2.7
44	2038	2039	1.57	.55	.00	.00	.21	.7
45	2035	2036	1.25	.15	.00	.00	.17	.4
46	2029	2030	-6.14	.09	.00	.00	.78	7.7
47	2030	2080	-7.17	2.24	.00	.00	.97	11.9
48	2048	2049	1.27	.34	.00	.00	.17	.4
49	2049	2050	.22	.00	.00	.00	.03	.0
50	2034	2035	1.62	.68	.00	.00	.22	.7

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTION PRESSURE (kpa)
2025		.49	512.23	449.00	63.23	620.05
2026		.02	512.23	459.00	53.23	521.98
2027		1.31	512.24	447.00	65.24	639.81
2028		.14	512.24	481.00	31.24	306.33
2029		.35	512.60	448.00	64.60	633.54
2030		.18	512.70	448.00	64.70	634.45
2031		.74	505.00	446.00	59.00	578.61
2032		1.89	501.56	440.00	61.56	603.72
2033		1.90	501.34	440.00	61.34	601.59
2034		1.48	505.66	445.00	60.66	594.84
2035		.98	504.97	452.00	52.97	519.50
2036		1.10	504.83	465.00	39.83	390.58
2037		1.90	505.73	445.00	60.73	595.58
2038		4.39	511.02	447.00	64.02	627.81
2039		1.36	510.47	483.00	27.47	269.38
2040		.48	513.29	446.00	67.29	659.87
2041		.05	513.55	448.00	65.55	642.86
2042		.84	513.29	441.00	72.29	708.95
2043		1.22	513.28	459.00	54.28	532.32
2044		.28	513.24	465.00	48.24	473.04
2045		.65	513.29	461.00	52.29	512.78
2046		1.52	512.47	475.00	37.47	367.43
2047		1.61	510.98	462.00	48.98	480.37
2048		3.86	512.16	478.00	34.16	335.04
2049		1.63	511.83	485.00	26.83	263.11
2050		.43	511.83	487.00	24.83	243.49
2051		.39	511.65	462.00	49.65	486.90
2052		.98	514.79	451.00	63.79	625.57
2067		1.24	515.48	469.00	46.48	455.84
2068		.67	511.02	445.00	66.02	647.46
2069		.23	511.01	461.00	50.01	490.41
2070		1.97	503.78	445.00	58.78	576.44

2071	.40	503.75	461.00	42.75	419.25
2072	7.05	500.72	465.00	35.72	350.34
2073	.41	504.80	475.00	29.80	292.22
2074	.54	510.46	488.00	22.46	220.21
2080	1.18	514.94	462.00	52.94	519.15
2081	.44	513.56	447.00	66.56	652.69

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	46.30
NET SYSTEM INFLOW =	46.30
NET SYSTEM OUTFLOW =	.00
NET SYSTEM DEMAND =	46.30

D A T A C H A N G E S F O R N E X T S I M U L A T I O N

D E M A N D C H A N G E S

DEMAND TYPE = 1 - GDF = .300

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00036

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/1000 (m/m)
1-FG	0	2067	13.89	.06	.00	.00	.20	.1
2	2067	2052	.27	.07	.00	.00	.06	.0

3	2067	2080	.76	.06	.00	.00	.15	.5
4	2052	2045	3.28	.16	.00	.00	.21	.5
5	2045	2043	.25	.00	.00	.00	.02	.0
6	2045	2046	2.83	.09	.00	.00	.18	.4
7	2043	2042	-.20	.00	.00	.00	.01	.0
8	2043	2044	.08	.00	.00	.00	.02	.0
9	2042	2040	-.45	.00	.00	.00	.03	.0
10	2040	2038	6.01	.24	.00	.00	.39	1.6
11	2040	2081	-.20	.03	.00	.00	.09	.3
12	2081	2041	.02	.00	.00	.00	.01	.0
13	2081	2080	-6.75	.15	.00	.00	.22	.3
14	2038	2039	.10	.06	.00	.00	.04	.0
15	2038	2037	4.12	.57	.00	.00	.27	.8
16	2039	2074	.16	.00	.00	.00	.03	.0
17	2037	2034	3.55	.01	.00	.00	.20	.4
18	2034	2035	.26	.07	.00	.00	.05	.0
19	2034	2031	2.36	.07	.00	.00	.15	.3
20	2035	2036	.08	.02	.00	.00	.03	.0
21	2036	2073	.12	.00	.00	.00	.02	.0
22	2031	2070	3.96	.13	.00	.00	.26	.7
23	2031	2068	-1.82	.65	.00	.00	.25	1.1
24	2070	2032	3.25	.24	.00	.00	.21	.5
25	2070	2071	.12	.00	.00	.00	.02	.0
26	2032	2033	2.69	.02	.00	.00	.15	.2
27	2033	2072	2.12	.07	.00	.00	.14	.2
28	2068	2029	-2.09	.17	.00	.00	.28	1.4
29	2068	2069	.07	.00	.00	.00	.01	.0
30	2029	2030	-.95	.01	.00	.00	.19	.8
31	2029	2027	.59	.04	.00	.00	.08	.1
32	2030	2080	-.69	.24	.00	.00	.14	.4
33	2027	2028	.04	.00	.00	.00	.01	.0
34	2027	2025	.15	.00	.00	.00	.01	.0
35	2025	2026	.01	.00	.00	.00	.00	.0
36	2046	2047	.48	.16	.00	.00	.10	.2
37	2046	2048	1.89	.03	.00	.00	.12	.2
38	2048	2049	.35	.04	.00	.00	.05	.0
39	2049	2050	.06	.00	.00	.00	.01	.0
40	2049	2051	.12	.02	.00	.00	.05	.1
41	2067	2052	3.30	.07	.00	.00	.11	.0
42	2067	2080	9.19	.06	.00	.00	.30	.5
43	2040	2081	-6.40	.03	.00	.00	.21	.3
44	2038	2039	.47	.06	.00	.00	.06	.0
45	2035	2036	.38	.02	.00	.00	.05	.0
46	2029	2030	-1.84	.01	.00	.00	.23	.8
47	2030	2080	-2.15	.24	.00	.00	.29	1.2
48	2048	2049	.38	.04	.00	.00	.05	.0
49	2049	2050	.07	.00	.00	.00	.01	.0
50	2034	2035	.49	.07	.00	.00	.07	.0

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
2025		.15	515.59	449.00	66.59	653.07
2026		.01	515.59	459.00	56.59	555.00
2027		.39	515.60	447.00	68.60	672.70
2028		.04	515.60	481.00	34.60	339.27
2029		.10	515.63	448.00	67.63	663.27
2030		.05	515.64	448.00	67.64	663.37
2031		.22	514.82	446.00	68.82	674.87
2032		.57	514.45	440.00	74.45	730.08
2033		.57	514.42	440.00	74.42	729.85
2034		.44	514.89	445.00	69.89	685.38
2035		.29	514.82	452.00	62.82	616.02
2036		.33	514.80	465.00	49.80	488.38
2037		.57	514.90	445.00	69.90	685.46
2038		1.32	515.47	447.00	68.47	671.43
2039		.41	515.41	483.00	32.41	317.80
2040		.14	515.71	446.00	69.71	683.63
2041		.02	515.74	448.00	67.74	664.27
2042		.25	515.71	441.00	74.71	732.65
2043		.37	515.71	459.00	56.71	556.11
2044		.08	515.70	465.00	50.70	497.23
2045		.20	515.71	461.00	54.71	536.51
2046		.46	515.62	475.00	40.62	398.35
2047		.48	515.46	462.00	53.46	524.27
2048		1.16	515.59	478.00	37.59	368.61
2049		.49	515.55	485.00	30.55	299.61
2050		.13	515.55	487.00	28.55	279.99
2051		.12	515.53	462.00	53.53	524.97
2052		.29	515.87	451.00	64.87	636.16
2067		.37	515.94	469.00	46.94	460.37
2068		.20	515.46	445.00	70.46	691.03
2069		.07	515.46	461.00	54.46	534.10
2070		.59	514.69	445.00	69.69	683.39
2071		.12	514.68	461.00	53.68	526.45
2072		2.12	514.36	465.00	49.36	484.03
2073		.12	514.80	475.00	39.80	390.28
2074		.16	515.41	488.00	27.41	268.76
2080		.35	515.89	462.00	53.89	528.44
2081		.13	515.74	447.00	68.74	674.08

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

- (+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
- (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE FLOWRATE
 NUMBER (l/s)

DATE = 03-07-2002
JOB NAME = GKWSAP - JICA - Kahawatta SR

PAGE NO. 9

1 13.89

NET SYSTEM INFLOW = 13.89
NET SYSTEM OUTFLOW = .00
NET SYSTEM DEMAND = 13.89

**** KYPIPE SIMULATION COMPLETED ****

DATE: 3/ 7/2002
TIME: 10:33: 4


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* * * * * K Y P I P E 2 * * * * *
*   University of Kentucky Hydraulic Analysis Program   *
* Distribution of Pressure and Flows in Piping Networks *
*           1000 PIPE VERSION - 1.10   (08/25/92)       *
* * * * *
  
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DATE: 3/ 7/2002
 TIME: 10:40:37

INPUT DATA FILENAME ----- c:\D_nets\2015\KAHL2015.DAT
 TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\KAHL2015.OUT
 POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\KAHL2015.RES

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*****
S U M M A R Y   O F   O R I G I N A L   D A T A
*****
  
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U N I T S S P E C I F I E D

FLOWRATE = liters/second
 HEAD (HGL) = meters
 PRESSURE = kpa

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1 #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-FG	0 3073	50.0	30.0	130.00	.00	485.
2	3073 3095	50.0	6.5	120.00	.00	
3	3095 3074	70.0	6.5	120.00	.00	
4	3074 3070	150.0	6.5	120.00	.00	
5	3074 3101	70.0	5.5	120.00	.00	
6	3070 3091	100.0	5.5	120.00	.00	
7	3091 3092	150.0	5.5	120.00	.00	
8	3091 3097	60.0	5.5	120.00	.00	
9	3097 3076	90.0	5.5	120.00	.00	
10	3073 3068	120.0	5.5	120.00	.00	
11	3073 3072	270.0	6.5	120.00	.00	
12	3072 3071	280.0	6.5	120.00	.00	
13	3071 3069	165.0	6.5	120.00	.00	

14	3069	3067	75.0	6.5	120.00	.00
15	3069	3093	270.0	5.5	120.00	.00
16	3067	3066	210.0	6.5	120.00	.00
17	3066	3065	200.0	6.5	120.00	.00
18	3065	3121	370.0	10.0	120.00	.00
19	3093	3116	30.0	5.5	120.00	.00
20	3116	3096	380.0	5.5	120.00	.00
21	3073	3095	50.0	25.0	130.00	.00
22	3095	3074	70.0	25.0	130.00	.00
23	3074	3070	150.0	19.8	130.00	.00
24	3070	3091	100.0	19.8	130.00	.00
25	3091	3097	60.0	19.8	130.00	.00
26	3097	3076	90.0	19.8	130.00	.00
27	3073	3072	270.0	30.0	130.00	.00
28	3072	3071	280.0	30.0	130.00	.00
29	3069	3067	75.0	14.0	130.00	.00
30	3067	3066	210.0	14.0	130.00	.00
31	3066	3065	200.0	14.0	130.00	.00
32	3092	3102	200.0	7.9	130.00	.00
33	3101	3102	150.0	7.9	130.00	.00
34	3102	3103	900.0	7.9	130.00	.00
35	3103	3099	200.0	7.9	130.00	.00
36	3099	3097	1010.0	7.9	130.00	.00
37	3097	3098	200.0	7.9	130.00	.00
38	3076	3106	230.0	19.8	130.00	.00
39	3106	3107	450.0	14.0	130.00	.00
40	3106	3105	120.0	9.7	130.00	.00
41	3106	3123	380.0	14.0	130.00	.00
42	3105	3104	330.0	7.9	130.00	.00
43	3105	3112	270.0	7.9	130.00	.00
44	3104	3108	650.0	14.0	130.00	.00
45	3108	3123	50.0	14.0	130.00	.00
46	3108	3109	320.0	14.0	130.00	.00
47	3109	3110	300.0	14.0	130.00	.00
48	3109	3111	460.0	7.9	130.00	.00
49	3123	3124	400.0	7.9	130.00	.00
50	3107	3115	400.0	7.9	130.00	.00
51	3107	3117	430.0	7.9	130.00	.00
52	3115	3114	250.0	7.9	130.00	.00
53	3115	3118	700.0	7.9	130.00	.00
54	3117	3116	300.0	7.9	130.00	.00
55	3117	3118	300.0	7.9	130.00	.00
56	3118	3119	100.0	7.9	130.00	.00
57	3119	3120	300.0	7.9	130.00	.00
58	3119	3122	450.0	7.9	130.00	.00
59	3120	3121	300.0	7.9	130.00	.00
60	3071	3069	165.0	14.0	130.00	.00
61	3069	3093	270.0	9.7	130.00	.00
62	3093	3116	30.0	10.0	130.00	.00
63	3074	3101	70.0	7.9	130.00	.00

JUNCTION NODE DATA

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	JUNCTION ELEVATION (m)	CONNECTING PIPES				
3065		1.07	450.00	17	18	31		
3066		1.47	455.00	16	17	30	31	
3067		.43	460.00	14	16	29	30	
3068		.15	456.00	10				
3069		.69	460.00	13	14	15	29	60
3070		.29	462.00	4	6	23	24	
3071		1.00	483.00	12	13	28	60	
3072		.45	470.00	11	12	27	28	
3073		.49	461.00	1	2	10	11	21
3074		.31	458.00	3	4	5	22	23
3076		.32	455.00	9	26	38		
3091		.32	463.00	6	7	8	24	25
3092		.42	459.00	7	32			
3093		.45	462.00	15	19	61	62	
3095		.16	455.00	2	3	21	22	
3096		.80	454.00	20				
3097		1.33	450.00	8	9	25	26	36
3098		.25	445.00	37				
3099		4.03	450.00	35	36			
3101		.28	460.00	5	33	63		
3102		1.52	459.00	32	33	34		
3103		2.11	445.00	34	35			
3104		2.44	442.00	42	44			
3105		.55	455.00	40	42	43		
3106		.77	458.00	38	39	40	41	
3107		4.16	442.00	39	50	51		
3108		2.07	440.00	44	45	46		
3109		1.66	440.00	46	47	48		
3110		1.46	440.00	47				
3111		.30	460.00	48				
3112		.27	460.00	43				
3114		.38	465.00	52				
3115		1.95	465.00	50	52	53		
3116		1.06	451.00	19	20	54	62	
3117		1.01	448.00	51	54	55		
3118		1.59	450.00	53	55	56		
3119		1.46	450.00	56	57	58		
3120		1.03	465.00	57	59			
3121		2.64	450.00	18	59			
3122		1.21	455.00	58				
3123		.30	445.00	41	45	49		
3124		.33	465.00	49				

O U T P U T O P T I O N D A T A

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

S Y S T E M C O N F I G U R A T I O N

NUMBER OF PIPES(p) = 63
 NUMBER OF JUNCTION NODES(j) = 42
 NUMBER OF PRIMARY LOOPS(l) = 21
 NUMBER OF FIXED GRADE NODES(f) = 1
 NUMBER OF SUPPLY ZONES(z) = 1

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 6 TRIALS WITH AN ACCURACY = .00090

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	3073	44.98	.07	.00	.00	.64	1.4
2	3073	3095	.77	.08	.00	.00	.23	1.5
3	3095	3074	.76	.11	.00	.00	.23	1.5
4	3074	3070	1.17	.51	.00	.00	.35	3.4
5	3074	3101	1.08	.46	.00	.00	.46	6.6
6	3070	3091	.76	.34	.00	.00	.32	3.4
7	3091	3092	1.12	1.06	.00	.00	.47	7.0
8	3091	3097	.72	.18	.00	.00	.30	3.0
9	3097	3076	.57	.18	.00	.00	.24	2.0
10	3073	3068	.15	.02	.00	.00	.06	.1
11	3073	3072	.25	.05	.00	.00	.07	.1
12	3072	3071	.24	.05	.00	.00	.07	.1
13	3071	3069	1.46	.84	.00	.00	.44	5.1
14	3069	3067	.86	.14	.00	.00	.26	1.9
15	3069	3093	.83	1.09	.00	.00	.35	4.0
16	3067	3066	.81	.36	.00	.00	.24	1.7
17	3066	3065	.65	.23	.00	.00	.20	1.1

18	3065	3121	4.87	2.16	.00	.00	.62	5.8
19	3093	3116	.70	.09	.00	.00	.30	2.9
20	3116	3096	.80	1.44	.00	.00	.34	3.7
21	3073	3095	28.76	.08	.00	.00	.59	1.5
22	3095	3074	28.61	.11	.00	.00	.58	1.5
23	3074	3070	23.76	.51	.00	.00	.77	3.4
24	3070	3091	23.89	.34	.00	.00	.78	3.4
25	3091	3097	22.49	.18	.00	.00	.73	3.0
26	3097	3076	17.94	.18	.00	.00	.58	2.0
27	3073	3072	14.56	.05	.00	.00	.21	.1
28	3072	3071	14.12	.05	.00	.00	.20	.1
29	3069	3067	6.99	.14	.00	.00	.45	1.9
30	3067	3066	6.60	.36	.00	.00	.43	1.7
31	3066	3065	5.29	.23	.00	.00	.34	1.1
32	3092	3102	.70	.09	.00	.00	.14	.4
33	3101	3102	3.84	1.53	.00	.00	.78	10.2
34	3102	3103	3.02	5.90	.00	.00	.62	6.5
35	3103	3099	.91	.14	.00	.00	.19	.7
36	3099	3097	-3.12	7.00	.00	.00	.64	6.9
37	3097	3098	.25	.01	.00	.00	.05	.0
38	3076	3106	18.19	.48	.00	.00	.59	2.0
39	3106	3107	8.04	1.11	.00	.00	.52	2.4
40	3106	3105	2.39	.19	.00	.00	.32	1.5
41	3106	3123	6.99	.72	.00	.00	.45	1.9
42	3105	3104	1.57	.64	.00	.00	.32	1.9
43	3105	3112	.27	.02	.00	.00	.06	.0
44	3104	3108	-.87	.03	.00	.00	.06	.0
45	3108	3123	-6.36	.08	.00	.00	.41	1.6
46	3108	3109	3.42	.16	.00	.00	.22	.5
47	3109	3110	1.46	.03	.00	.00	.09	.1
48	3109	3111	.30	.04	.00	.00	.06	.0
49	3123	3124	.33	.04	.00	.00	.07	.1
50	3107	3115	2.66	2.07	.00	.00	.54	5.1
51	3107	3117	1.22	.52	.00	.00	.25	1.2
52	3115	3114	.38	.04	.00	.00	.08	.1
53	3115	3118	.33	.08	.00	.00	.07	.1
54	3117	3116	-2.52	1.40	.00	.00	.51	4.6
55	3117	3118	2.72	1.62	.00	.00	.56	5.4
56	3118	3119	1.47	.17	.00	.00	.30	1.7
57	3119	3120	-1.20	.36	.00	.00	.25	1.1
58	3119	3122	1.21	.54	.00	.00	.25	1.2
59	3120	3121	-2.23	1.12	.00	.00	.46	3.7
60	3071	3069	11.90	.84	.00	.00	.77	5.1
61	3069	3093	4.00	1.09	.00	.00	.54	4.0
62	3093	3116	3.67	.09	.00	.00	.47	2.9
63	3074	3101	3.04	.46	.00	.00	.62	6.6

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND	HYDRAULIC GRADE	JUNCTION ELEVATION	PRESSURE HEAD	JUNCTION PRESSURE
-----------------	----------------	-----------------	-----------------	--------------------	---------------	-------------------

	(l/s)	(m)	(m)	(m)	(kpa)
3065	1.07	483.25	450.00	33.25	326.07
3066	1.47	483.48	455.00	28.48	279.27
3067	.43	483.84	460.00	23.84	233.77
3068	.15	484.91	456.00	28.91	283.48
3069	.69	483.98	460.00	23.98	235.17
3070	.29	484.23	462.00	22.23	218.02
3071	1.00	484.82	483.00	1.82	17.88
3072	.45	484.87	470.00	14.87	145.87
3073	.49	484.93	461.00	23.93	234.64
3074	.31	484.74	458.00	26.74	262.24
3076	.32	483.52	455.00	28.52	279.71
3091	.32	483.89	463.00	20.89	204.84
3092	.42	482.83	459.00	23.83	233.71
3093	.45	482.89	462.00	20.89	204.86
3095	.16	484.85	455.00	29.85	292.72
3096	.80	481.36	454.00	27.36	268.36
3097	1.33	483.70	450.00	33.70	330.52
3098	.25	483.69	445.00	38.69	379.43
3099	4.03	476.70	450.00	26.70	261.88
3101	.28	484.28	460.00	24.28	238.08
3102	1.52	482.74	459.00	23.74	232.86
3103	2.11	476.85	445.00	31.85	312.31
3104	2.44	482.22	442.00	40.22	394.38
3105	.55	482.86	455.00	27.86	273.20
3106	.77	483.05	458.00	25.05	245.61
3107	4.16	481.93	442.00	39.93	391.55
3108	2.07	482.24	440.00	42.24	414.25
3109	1.66	482.08	440.00	42.08	412.65
3110	1.46	482.05	440.00	42.05	412.35
3111	.30	482.04	460.00	22.04	216.11
3112	.27	482.84	460.00	22.84	223.97
3114	.38	479.82	465.00	14.82	145.36
3115	1.95	479.86	465.00	14.86	145.71
3116	1.06	482.80	451.00	31.80	311.86
3117	1.01	481.40	448.00	33.40	327.57
3118	1.59	479.78	450.00	29.78	292.06
3119	1.46	479.61	450.00	29.61	290.38
3120	1.03	479.97	465.00	14.97	146.78
3121	2.64	481.09	450.00	31.09	304.89
3122	1.21	479.07	455.00	24.07	236.04
3123	.30	482.32	445.00	37.32	366.00
3124	.33	482.28	465.00	17.28	169.44

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

- (+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
- (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE FLOWRATE

NUMBER	(l/s)
-----	-----
1	44.98

NET SYSTEM INFLOW = 44.98
 NET SYSTEM OUTFLOW = .00
 NET SYSTEM DEMAND = 44.98

D A T A C H A N G E S F O R N E X T S I M U L A T I O N

D E M A N D C H A N G E S

DEMAND TYPE = 1 - GDF = .300

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00017

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	3073	13.49	.01	.00	.00	.19	.1
2	3073	3095	.23	.01	.00	.00	.07	.1
3	3095	3074	.23	.01	.00	.00	.07	.1
4	3074	3070	.35	.05	.00	.00	.11	.3
5	3074	3101	.32	.05	.00	.00	.14	.7
6	3070	3091	.23	.04	.00	.00	.10	.3
7	3091	3092	.34	.11	.00	.00	.14	.7
8	3091	3097	.21	.02	.00	.00	.09	.3
9	3097	3076	.17	.02	.00	.00	.07	.2
10	3073	3068	.05	.00	.00	.00	.02	.0
11	3073	3072	.07	.01	.00	.00	.02	.0
12	3072	3071	.07	.01	.00	.00	.02	.0
13	3071	3069	.44	.09	.00	.00	.13	.5
14	3069	3067	.26	.02	.00	.00	.08	.2
15	3069	3093	.25	.12	.00	.00	.10	.4
16	3067	3066	.24	.04	.00	.00	.07	.1
17	3066	3065	.19	.02	.00	.00	.06	.1

18	3065	3121	1.46	.23	.00	.00	.19	.6
19	3093	3116	.21	.01	.00	.00	.09	.3
20	3116	3096	.24	.15	.00	.00	.10	.4
21	3073	3095	8.63	.01	.00	.00	.18	.1
22	3095	3074	8.58	.01	.00	.00	.17	.1
23	3074	3070	7.13	.05	.00	.00	.23	.3
24	3070	3091	7.17	.04	.00	.00	.23	.3
25	3091	3097	6.75	.02	.00	.00	.22	.3
26	3097	3076	5.38	.02	.00	.00	.17	.2
27	3073	3072	4.37	.01	.00	.00	.06	.0
28	3072	3071	4.24	.01	.00	.00	.06	.0
29	3069	3067	2.10	.02	.00	.00	.14	.2
30	3067	3066	1.98	.04	.00	.00	.13	.1
31	3066	3065	1.59	.02	.00	.00	.10	.1
32	3092	3102	.21	.01	.00	.00	.04	.0
33	3101	3102	1.15	.16	.00	.00	.24	1.1
34	3102	3103	.91	.63	.00	.00	.19	.7
35	3103	3099	.27	.02	.00	.00	.06	.0
36	3099	3097	-.93	.75	.00	.00	.19	.7
37	3097	3098	.08	.00	.00	.00	.02	.0
38	3076	3106	5.46	.05	.00	.00	.18	.2
39	3106	3107	2.41	.12	.00	.00	.16	.2
40	3106	3105	.72	.02	.00	.00	.10	.1
41	3106	3123	2.10	.08	.00	.00	.14	.2
42	3105	3104	.47	.07	.00	.00	.10	.2
43	3105	3112	.08	.00	.00	.00	.02	.0
44	3104	3108	-.26	.00	.00	.00	.02	.0
45	3108	3123	-1.91	.01	.00	.00	.12	.1
46	3108	3109	1.03	.02	.00	.00	.07	.0
47	3109	3110	.44	.00	.00	.00	.03	.0
48	3109	3111	.09	.00	.00	.00	.02	.0
49	3123	3124	.10	.00	.00	.00	.02	.0
50	3107	3115	.80	.22	.00	.00	.16	.5
51	3107	3117	.37	.06	.00	.00	.07	.1
52	3115	3114	.11	.00	.00	.00	.02	.0
53	3115	3118	.10	.01	.00	.00	.02	.0
54	3117	3116	-.75	.15	.00	.00	.15	.5
55	3117	3118	.82	.17	.00	.00	.17	.5
56	3118	3119	.44	.02	.00	.00	.09	.1
57	3119	3120	-.36	.04	.00	.00	.07	.1
58	3119	3122	.36	.06	.00	.00	.07	.1
59	3120	3121	-.67	.12	.00	.00	.14	.4
60	3071	3069	3.57	.09	.00	.00	.23	.5
61	3069	3093	1.20	.12	.00	.00	.16	.4
62	3093	3116	1.10	.01	.00	.00	.14	.3
63	3074	3101	.91	.05	.00	.00	.19	.7

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND	HYDRAULIC GRADE	JUNCTION ELEVATION	PRESSURE HEAD	JUNCTION PRESSURE
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	(l/s)	(m)	(m)	(m)	(kpa)
3065	.32	484.81	450.00	34.81	341.39
3066	.44	484.84	455.00	29.84	292.60
3067	.13	484.88	460.00	24.88	243.95
3068	.05	484.99	456.00	28.99	284.30
3069	.21	484.89	460.00	24.89	244.10
3070	.09	484.92	462.00	22.92	224.74
3071	.30	484.98	483.00	1.98	19.43
3072	.14	484.99	470.00	14.99	146.97
3073	.15	484.99	461.00	23.99	235.28
3074	.09	484.97	458.00	26.97	264.51
3076	.10	484.84	455.00	29.84	292.64
3091	.10	484.88	463.00	21.88	214.57
3092	.13	484.77	459.00	25.77	252.69
3093	.14	484.77	462.00	22.77	223.33
3095	.05	484.98	455.00	29.98	294.04
3096	.24	484.61	454.00	30.61	300.18
3097	.40	484.86	450.00	34.86	341.87
3098	.08	484.86	445.00	39.86	390.89
3099	1.21	484.11	450.00	34.11	334.48
3101	.08	484.92	460.00	24.92	244.41
3102	.46	484.76	459.00	25.76	252.60
3103	.63	484.12	445.00	39.12	383.67
3104	.73	484.70	442.00	42.70	418.75
3105	.17	484.77	455.00	29.77	291.94
3106	.23	484.79	458.00	26.79	262.72
3107	1.25	484.67	442.00	42.67	418.45
3108	.62	484.70	440.00	44.70	438.39
3109	.50	484.69	440.00	44.69	438.22
3110	.44	484.68	440.00	44.68	438.19
3111	.09	484.68	460.00	24.68	242.04
3112	.08	484.77	460.00	24.77	242.89
3114	.11	484.44	465.00	19.44	190.68
3115	.59	484.45	465.00	19.45	190.72
3116	.32	484.76	451.00	33.76	331.11
3117	.30	484.61	448.00	36.61	359.06
3118	.48	484.44	450.00	34.44	337.74
3119	.44	484.42	450.00	34.42	337.56
3120	.31	484.46	465.00	19.46	190.83
3121	.79	484.58	450.00	34.58	339.12
3122	.36	484.36	455.00	29.36	287.95
3123	.09	484.71	445.00	39.71	389.44
3124	.10	484.71	465.00	19.71	193.26

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

- (+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
- (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE FLOWRATE

DATE = 03-07-2002
JOB NAME = GKWSAP - JICA - Kahalla SR

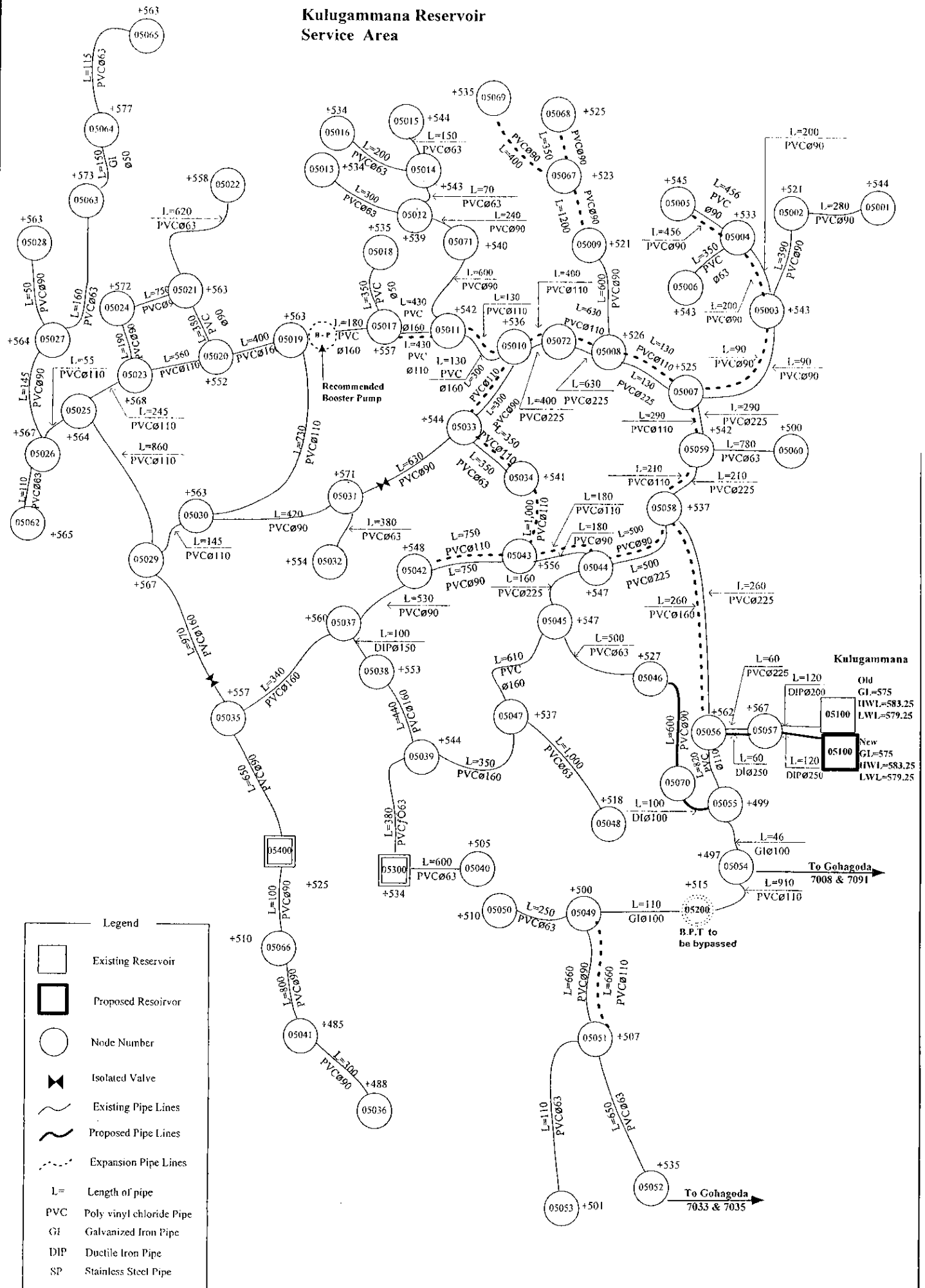
PAGE NO. 10

NUMBER	(l/s)
1	13.49
NET SYSTEM INFLOW =	13.49
NET SYSTEM OUTFLOW =	.00
NET SYSTEM DEMAND =	13.49

**** KYPIPE SIMULATION COMPLETED ****

DATE: 3/ 7/2002
TIME: 10:40:37

Kulugamma Reservoir Service Area



Appendix - 5.5 Improvement of Distribution Network in 2015
(Kulugamma Reservoir Service Area)

* * * * * K Y P I P E 2 * * * * *
* University of Kentucky Hydraulic Analysis Program *
* Distribution of Pressure and Flows in Piping Networks *
* 1000 PIPE VERSION - 1.10 (08/25/92) *
* * * * *

DATE: 3/ 7/2002
TIME: 13:53: 9

INPUT DATA FILENAME ----- c:\D_nets\2015\KULU2015.DAT
TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\KULU2015.OUT
POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\KULU2015.RES

S U M M A R Y O F O R I G I N A L D A T A

U N I T S S P E C I F I E D

FLOWRATE = liters/second
HEAD (HGL) = meters
PRESSURE = kpa

R E G U L A T I N G V A L V E D A T A

VALVE TYPE	POSITION JUNCTION	CONTROLLED PIPE	VALVE SETTING (m or l/s)
PRV-1	5300	77	534.00
PRV-1	5400	73	525.00

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-FG	0	5057	120.0	20.0	120.00	.00	579.
2	5057	5056	60.0	19.8	120.00	.00	

3	5056	5055	820.0	9.7	120.00	.00
4	5055	5054	46.0	10.0	120.00	.00
5	5054	5200	910.0	9.7	120.00	.00
6	5200	5049	110.0	10.0	120.00	.00
7	5049	5050	250.0	5.5	120.00	.00
8	5049	5051	660.0	7.9	120.00	.00
9	5051	5053	110.0	5.5	120.00	.00
10	5051	5052	650.0	5.5	120.00	.00
11	5056	5058	260.0	19.8	120.00	.00
12	5058	5059	210.0	19.8	120.00	.00
13	5059	5060	780.0	5.5	120.00	.00
14	5059	5007	290.0	19.8	120.00	.00
15	5007	5003	90.0	7.9	120.00	.00
16	5003	5004	200.0	7.9	120.00	.00
17	5004	5005	456.0	7.9	120.00	.00
18	5004	5006	350.0	5.5	120.00	.00
19	5003	5002	390.0	7.9	120.00	.00
20	5001	5002	280.0	7.9	120.00	.00
21	5007	5008	130.0	19.8	120.00	.00
22	5008	5009	600.0	7.9	120.00	.00
23	5009	5067	1200.0	7.9	130.00	.00
24	5067	5069	400.0	7.9	130.00	.00
25	5058	5044	500.0	19.8	120.00	.00
26	5044	5045	160.0	19.8	120.00	.00
27	5045	5046	500.0	5.5	120.00	.00
28	5046	5055	600.0	7.9	130.00	.00
29	5008	5072	630.0	19.8	120.00	.00
30	5072	5010	400.0	19.8	120.00	.00
31	5010	5011	130.0	14.0	120.00	.00
32	5011	5071	600.0	7.9	120.00	.00
33	5071	5012	240.0	7.9	120.00	.00
34	5012	5013	300.0	5.5	120.00	.00
35	5012	5014	70.0	5.5	120.00	.00
36	5014	5015	150.0	5.5	120.00	.00
37	5014	5016	200.0	5.5	120.00	.00
38	5011	5017	430.0	14.0	120.00	.00
39	5017	5018	350.0	4.4	120.00	.00
40-XX	5017	5019	180.0	14.0	120.00	.00
41	5019	5020	400.0	14.0	120.00	.00
42	5020	5021	380.0	7.9	120.00	.00
43	5021	5022	620.0	5.5	120.00	.00
44	5020	5023	560.0	9.7	120.00	.00
45	5023	5024	190.0	7.9	120.00	.00
46	5024	5021	750.0	7.9	120.00	.00
47	5023	5025	245.0	9.7	120.00	.00
48	5025	5026	55.0	9.7	120.00	.00
49	5026	5062	110.0	5.5	120.00	.00
50	5026	5027	145.0	7.9	120.00	.00
51	5027	5028	50.0	7.9	120.00	.00
52	5027	5063	160.0	5.5	120.00	.00
53	5063	5064	150.0	5.5	120.00	.00
54	5064	5065	115.0	5.5	120.00	.00
55	5025	5029	860.0	9.7	120.00	.00

56	5029	5030	145.0	9.7	120.00	.00	
57	5030	5019	730.0	9.7	120.00	.00	
58	5030	5031	420.0	7.9	120.00	.00	
59	5031	5032	380.0	5.5	120.00	.00	
60-XX	5031	5033	630.0	7.9	120.00	.00	
61	5033	5034	350.0	5.5	120.00	.00	
62	5042	5043	750.0	7.9	120.00	.00	
63	5043	5044	180.0	7.9	120.00	.00	
64	5042	5037	530.0	7.9	120.00	.00	
65	5037	5038	100.0	15.0	120.00	.00	
66	5038	5039	440.0	14.0	120.00	.00	
67	5039	5047	350.0	14.0	120.00	.00	
68	5047	5045	610.0	14.0	120.00	.00	
69	5047	5048	1000.0	5.5	120.00	.00	
70-XX	5029	5035	970.0	14.0	120.00	.00	
71	5035	5037	340.0	14.0	120.00	.00	
72	5035	5400	650.0	7.9	120.00	.00	
73-RV	5400	5066	100.0	7.9	120.00	.00	
74	5066	5041	800.0	7.9	120.00	.00	
75	5041	5036	300.0	7.9	120.00	.00	
76	5039	5300	380.0	5.5	120.00	.00	
77-RV	5300	5040	600.0	5.5	120.00	.00	
78	5010	5033	300.0	7.9	120.00	.00	
79	5034	5043	1000.0	9.7	130.00	.00	
80	5067	5068	350.0	7.9	130.00	.00	
81-FG	0	5057	120.0	25.0	130.00	.00	579.
82	5057	5056	60.0	25.0	130.00	.00	
83	5033	5034	350.0	9.7	130.00	.00	
84	5042	5043	750.0	9.7	130.00	.00	
85	5043	5044	180.0	9.7	130.00	.00	
86	5058	5044	500.0	7.9	130.00	.00	
87	5010	5033	300.0	9.7	130.00	.00	
88	5007	5003	90.0	7.9	130.00	.00	
89	5003	5004	200.0	7.9	130.00	.00	
90	5004	5005	456.0	7.9	130.00	.00	
91	5056	5058	260.0	14.0	130.00	.00	
92	5058	5059	210.0	9.7	130.00	.00	
93	5059	5007	290.0	9.7	130.00	.00	
94	5007	5008	130.0	9.7	130.00	.00	
95	5008	5072	630.0	9.7	130.00	.00	
96	5010	5011	130.0	9.7	130.00	.00	
97	5011	5017	430.0	9.7	130.00	.00	
98-FG	0	5019	90.0	14.0	130.00	.00	590.
99	5049	5051	660.0	9.7	130.00	.00	

JUNCTION NODE DATA

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	JUNCTION ELEVATION (m)	CONNECTING PIPES
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5001	.08	544.00	20					
5002	.19	521.00	19	20				
5003	.28	543.00	15	16	19	88	89	
5004	.51	533.00	16	17	18	89	90	
5005	3.40	545.00	17	90				
5006	.21	543.00	18					
5007	.23	525.00	14	15	21	88	93	
5008	.54	526.00	21	22	29	94	95	
5009	.75	521.00	22	23				
5010	.50	536.00	30	31	78	87	96	
5011	.70	542.00	31	32	38	96	97	
5012	.48	539.00	33	34	35			
5013	.09	534.00	34					
5014	.12	543.00	35	36	37			
5015	.05	544.00	36					
5016	.07	534.00	37					
5017	.66	557.00	38	39	40	97		
5018	.09	535.00	39					
5019	.70	563.00	40	41	57	98		
5020	.42	552.00	41	42	44			
5021	.39	563.00	42	43	46			
5022	.40	558.00	43					
5023	.07	568.00	44	45	47			
5024	.03	572.00	45	46				
5025	.53	564.00	47	48	55			
5026	.15	567.00	48	49	50			
5027	.19	564.00	50	51	52			
5028	.05	563.00	51					
5029	.26	567.00	55	56	70			
5030	.16	563.00	56	57	58			
5031	.25	571.00	58	59	60			
5032	.33	554.00	59					
5033	.18	544.00	60	61	78	83	87	
5034	1.18	541.00	61	79	83			
5035	1.44	557.00	70	71	72			
5036	.29	488.00	75					
5037	.48	560.00	64	65	71			
5038	.14	553.00	65	66				
5039	.58	544.00	66	67	76			
5040	.32	505.00	77					
5041	.82	485.00	74	75				
5042	.45	548.00	62	64	84			
5043	.44	556.00	62	63	79	84	85	
5044	.28	547.00	25	26	63	85	86	
5045	.34	547.00	26	27	68			
5046	.37	527.00	27	28				
5047	.38	537.00	67	68	69			
5048	.19	518.00	69					
5049	.73	500.00	6	7	8	99		
5050	.12	510.00	7					
5051	.52	507.00	8	9	10	99		

5052	.49	535.00	10					
5053	1.27	501.00	9					
5054	.92	497.00	4	5				
5055	.47	499.00	3	4	28			
5056	.43	562.00	2	3	11	82	91	
5057	.07	567.00	1	2	81	82		
5058	.45	537.00	11	12	25	86	91	
5059	.37	542.00	12	13	14	92	93	
5060	.22	500.00	13					
5062	.04	565.00	49					
5063	.06	573.00	52	53				
5064	.06	577.00	53	54				
5065	.03	563.00	54					
5066	1.04	510.00	73	74				
5067	1.04	523.00	23	24	80			
5068	.57	525.00	80					
5069	.19	535.00	24					
5071	.41	540.00	32	33				
5072	.60	532.00	29	30	95			
5200	.00	515.00	5	6				
5300	.00	534.00	76	77				
5400	.00	525.00	72	73				

O U T P U T O P T I O N D A T A

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

S Y S T E M C O N F I G U R A T I O N

NUMBER OF PIPES(p) = 99
 NUMBER OF JUNCTION NODES(j) = 73
 NUMBER OF PRIMARY LOOPS(l) = 24
 NUMBER OF FIXED GRADE NODES(f) = 3
 NUMBER OF SUPPLY ZONES(z) = 1

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 8 TRIALS WITH AN ACCURACY = .00016

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE

CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1 #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0 5057	9.07	.08	.00	.00	.29	.6
2	5057 5056	8.89	.04	.00	.00	.29	.6
3	5056 5055	3.92	3.70	.00	.00	.53	4.5
4	5055 5054	4.05	.19	.00	.00	.52	4.1
5	5054 5200	3.13	2.71	.00	.00	.42	2.9
6	5200 5049	3.13	.28	.00	.00	.40	2.5
7	5049 5050	.12	.03	.00	.00	.05	.1
8	5049 5051	.80	.43	.00	.00	.16	.6
9	5051 5053	1.27	.98	.00	.00	.53	8.8
10	5051 5052	.49	.99	.00	.00	.21	1.5
11	5056 5058	15.55	.47	.00	.00	.51	1.8
12	5058 5059	11.07	.20	.00	.00	.36	.9
13	5059 5060	.22	.27	.00	.00	.09	.3
14	5059 5007	10.56	.25	.00	.00	.34	.8
15	5007 5003	2.24	.39	.00	.00	.46	4.3
16	5003 5004	1.98	.69	.00	.00	.40	3.4
17	5004 5005	1.63	1.11	.00	.00	.33	2.4
18	5004 5006	.21	.11	.00	.00	.09	.3
19	5003 5002	.27	.03	.00	.00	.06	.0
20	5001 5002	-.08	.00	.00	.00	.02	.0
21	5007 5008	6.36	.04	.00	.00	.21	.3
22	5008 5009	2.55	3.33	.00	.00	.52	5.5
23	5009 5067	1.80	3.01	.00	.00	.37	2.5
24	5067 5069	.19	.02	.00	.00	.04	.0
25	5058 5044	8.18	.27	.00	.00	.27	.5
26	5044 5045	5.81	.05	.00	.00	.19	.2
27	5045 5046	.97	2.72	.00	.00	.41	5.4
28	5046 5055	.60	.20	.00	.00	.12	.3
29	5008 5072	3.71	.08	.00	.00	.12	.1
30	5072 5010	3.73	.05	.00	.00	.12	.1
31	5010 5011	1.89	.03	.00	.00	.12	.2
32	5011 5071	1.22	.85	.00	.00	.25	1.4
33	5071 5012	.81	.16	.00	.00	.17	.6
34	5012 5013	.09	.02	.00	.00	.04	.0
35	5012 5014	.24	.03	.00	.00	.10	.4
36	5014 5015	.05	.00	.00	.00	.02	.0
37	5014 5016	.07	.01	.00	.00	.03	.0
38	5011 5017	.53	.01	.00	.00	.03	.0
39	5017 5018	.09	.07	.00	.00	.06	.2
40-XX	5017 5019						
41	5019 5020	2.22	.11	.00	.00	.14	.2
42	5020 5021	.75	.22	.00	.00	.15	.5
43	5021 5022	.40	.65	.00	.00	.17	1.0
44	5020 5023	1.04	.22	.00	.00	.14	.3
45	5023 5024	.07	.00	.00	.00	.01	.0
46	5024 5021	.04	.00	.00	.00	.01	.0
47	5023 5025	.91	.07	.00	.00	.12	.3

48	5025	5026	.58	.01	.00	.00	.08	.1
49	5026	5062	.04	.00	.00	.00	.02	.0
50	5026	5027	.39	.02	.00	.00	.08	.1
51	5027	5028	.05	.00	.00	.00	.01	.0
52	5027	5063	.15	.03	.00	.00	.06	.1
53	5063	5064	.09	.01	.00	.00	.04	.0
54	5064	5065	.03	.00	.00	.00	.01	.0
55	5025	5029	-.20	.02	.00	.00	.03	.0
56	5029	5030	-.46	.01	.00	.00	.06	.0
57	5030	5019	-1.20	.37	.00	.00	.16	.5
58	5030	5031	.58	.15	.00	.00	.12	.3
59	5031	5032	.33	.28	.00	.00	.14	.7
60-XX	5031	5033						
61	5033	5034	.06	.01	.00	.00	.03	.0
62	5042	5043	-.57	.26	.00	.00	.12	.3
63	5043	5044	-1.01	.18	.00	.00	.21	.9
64	5042	5037	1.18	.71	.00	.00	.24	1.3
65	5037	5038	-2.89	.03	.00	.00	.16	.3
66	5038	5039	-3.03	.21	.00	.00	.20	.4
67	5039	5047	-3.93	.27	.00	.00	.26	.7
68	5047	5045	-4.50	.60	.00	.00	.29	.9
69	5047	5048	.19	.26	.00	.00	.08	.2
70-XX	5029	5035						
71	5035	5037	-3.59	.22	.00	.00	.23	.6
72	5035	5400	2.15	2.63	.00	.00	.44	4.0
73-RV	5400	5066	2.15	.40	.00	.00	.44	4.0
74	5066	5041	1.11	.95	.00	.00	.23	1.1
75	5041	5036	.29	.03	.00	.00	.06	.1
76	5039	5300	.32	.26	.00	.00	.13	.6
77-RV	5300	5040	.32	.42	.00	.00	.13	.6
78	5010	5033	.20	.01	.00	.00	.04	.0
79	5034	5043	-.80	.21	.00	.00	.11	.2
80	5067	5068	.57	.10	.00	.00	.12	.3
81-FG	0	5057	17.67	.08	.00	.00	.36	.6
82	5057	5056	17.78	.04	.00	.00	.36	.6
83	5033	5034	.31	.01	.00	.00	.04	.0
84	5042	5043	-1.06	.26	.00	.00	.14	.3
85	5043	5044	-1.87	.18	.00	.00	.25	.9
86	5058	5044	.79	.27	.00	.00	.16	.5
87	5010	5033	.36	.01	.00	.00	.05	.0
88	5007	5003	2.43	.39	.00	.00	.50	4.3
89	5003	5004	2.14	.69	.00	.00	.44	3.4
90	5004	5005	1.77	1.11	.00	.00	.36	2.4
91	5056	5058	6.77	.47	.00	.00	.44	1.8
92	5058	5059	1.84	.20	.00	.00	.25	.9
93	5059	5007	1.75	.25	.00	.00	.24	.8
94	5007	5008	1.06	.04	.00	.00	.14	.3
95	5008	5072	.62	.08	.00	.00	.08	.1
96	5010	5011	.78	.03	.00	.00	.11	.2
97	5011	5017	.22	.01	.00	.00	.03	.0
98-FG	0	5019	4.12	.06	.00	.00	.27	.7
99	5049	5051	1.48	.43	.00	.00	.20	.6

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
5001		.08	577.78	544.00	33.78	331.30
5002		.19	577.79	521.00	56.79	556.88
5003		.28	577.82	543.00	34.82	341.47
5004		.51	577.13	533.00	44.13	432.74
5005		3.40	576.02	545.00	31.02	304.21
5006		.21	577.02	543.00	34.02	333.59
5007		.23	578.21	525.00	53.21	521.84
5008		.54	578.17	526.00	52.17	511.60
5009		.75	574.84	521.00	53.84	528.01
5010		.50	578.04	536.00	42.04	412.25
5011		.70	578.01	542.00	36.01	353.16
5012		.48	577.00	539.00	38.00	372.69
5013		.09	576.98	534.00	42.98	421.53
5014		.12	576.98	543.00	33.98	333.18
5015		.05	576.97	544.00	32.97	323.34
5016		.07	576.97	534.00	42.97	421.36
5017		.66	578.00	557.00	21.00	205.98
5018		.09	577.94	535.00	42.94	421.05
5019		.70	589.94	563.00	26.94	264.15
5020		.42	589.83	552.00	37.83	370.99
5021		.39	589.61	563.00	26.61	260.95
5022		.40	588.96	558.00	30.96	303.62
5023		.07	589.61	568.00	21.61	211.94
5024		.03	589.61	572.00	17.61	172.70
5025		.53	589.54	564.00	25.54	250.44
5026		.15	589.53	567.00	22.53	220.95
5027		.19	589.51	564.00	25.51	250.13
5028		.05	589.51	563.00	26.51	259.93
5029		.26	589.55	567.00	22.55	221.18
5030		.16	589.57	563.00	26.57	260.52
5031		.25	589.42	571.00	18.42	180.60
5032		.33	589.14	554.00	35.14	344.58
5033		.18	578.02	544.00	34.02	333.65
5034		1.18	578.01	541.00	37.01	362.95
5035		1.44	577.03	557.00	20.03	196.43
5036		.29	523.62	488.00	35.62	349.27
5037		.48	577.25	560.00	17.25	169.16
5038		.14	577.28	553.00	24.28	238.11
5039		.58	577.49	544.00	33.49	328.39
5040		.32	533.58	505.00	28.58	280.32
5041		.82	523.65	485.00	38.65	378.98
5042		.45	577.96	548.00	29.96	293.78
5043		.44	578.22	556.00	22.22	217.88
5044		.28	578.40	547.00	31.40	307.88
5045		.34	578.35	547.00	31.35	307.43

5046	.37	575.63	527.00	48.63	476.91
5047	.38	577.75	537.00	40.75	399.65
5048	.19	577.49	518.00	59.49	583.39
5049	.73	572.25	500.00	72.25	708.49
5050	.12	572.22	510.00	62.22	610.15
5051	.52	571.82	507.00	64.82	635.67
5052	.49	570.83	535.00	35.83	351.37
5053	1.27	570.84	501.00	69.84	684.92
5054	.92	575.24	497.00	78.24	767.30
5055	.47	575.43	499.00	76.43	749.55
5056	.43	579.14	562.00	17.14	168.05
5057	.07	579.17	567.00	12.17	119.39
5058	.45	578.67	537.00	41.67	408.63
5059	.37	578.47	542.00	36.47	357.62
5060	.22	578.20	500.00	78.20	766.86
5062	.04	589.53	565.00	24.53	240.55
5063	.06	589.48	573.00	16.48	161.60
5064	.06	589.47	577.00	12.47	122.27
5065	.03	589.47	563.00	26.47	259.56
5066	1.04	524.60	510.00	14.60	143.14
5067	1.04	571.83	523.00	48.83	478.89
5068	.57	571.73	525.00	46.73	458.25
5069	.19	571.82	535.00	36.82	361.05
5071	.41	577.16	540.00	37.16	364.44
5072	.60	578.09	532.00	46.09	451.97
5200	.00	572.53	515.00	57.53	564.16
5300	.00	577.22	534.00	43.22	423.88
5400	.00	574.40	525.00	49.40	484.48

R E G U L A T I N G V A L V E R E P O R T

VALVE TYPE	POSITION NODE	CONTROLLED PIPE	VALVE SETTING (m or l/s)	VALVE STATUS	UPSTREAM GRADE (m)	DOWNSTREAM GRADE (m)	THROUGH FLOW (l/s)
PRV-1	5300	77	534.00	THROTTLED	577.22	533.58	.32
PRV-1	5400	73	525.00	THROTTLED	574.40	524.60	2.15

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

- (+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
- (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	9.07
81	17.67
98	4.12

NET SYSTEM INFLOW = 30.86
 NET SYSTEM OUTFLOW = .00
 NET SYSTEM DEMAND = 30.86

D A T A C H A N G E S F O R N E X T S I M U L A T I O N

D E M A N D C H A N G E S

DEMAND TYPE = 1 - GDF = .300

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	5057	2.72	.01	.00	.00	.09	.0
2	5057	5056	2.67	.00	.00	.00	.09	.0
3	5056	5055	1.17	.40	.00	.00	.16	.4
4	5055	5054	1.22	.02	.00	.00	.15	.4
5	5054	5200	.94	.29	.00	.00	.13	.3
6	5200	5049	.94	.03	.00	.00	.12	.2
7	5049	5050	.04	.00	.00	.00	.02	.0
8	5049	5051	.24	.05	.00	.00	.05	.0
9	5051	5053	.38	.11	.00	.00	.16	.9
10	5051	5052	.15	.11	.00	.00	.06	.1
11	5056	5058	4.67	.05	.00	.00	.15	.1
12	5058	5059	3.32	.02	.00	.00	.11	.1
13	5059	5060	.07	.03	.00	.00	.03	.0
14	5059	5007	3.17	.03	.00	.00	.10	.0
15	5007	5003	.67	.04	.00	.00	.14	.4
16	5003	5004	.59	.07	.00	.00	.12	.3
17	5004	5005	.49	.12	.00	.00	.10	.2
18	5004	5006	.06	.01	.00	.00	.03	.0
19	5003	5002	.08	.00	.00	.00	.02	.0
20	5001	5002	-.02	.00	.00	.00	.00	.0

21	5007	5008	1.91	.00	.00	.00	.06	.0
22	5008	5009	.77	.36	.00	.00	.16	.6
23	5009	5067	.54	.32	.00	.00	.11	.2
24	5067	5069	.06	.00	.00	.00	.01	.0
25	5058	5044	2.45	.03	.00	.00	.08	.0
26	5044	5045	1.74	.00	.00	.00	.06	.0
27	5045	5046	.29	.29	.00	.00	.12	.5
28	5046	5055	.18	.02	.00	.00	.04	.0
29	5008	5072	1.11	.01	.00	.00	.04	.0
30	5072	5010	1.12	.01	.00	.00	.04	.0
31	5010	5011	.57	.00	.00	.00	.04	.0
32	5011	5071	.37	.09	.00	.00	.07	.1
33	5071	5012	.24	.02	.00	.00	.05	.0
34	5012	5013	.03	.00	.00	.00	.01	.0
35	5012	5014	.07	.00	.00	.00	.03	.0
36	5014	5015	.02	.00	.00	.00	.01	.0
37	5014	5016	.02	.00	.00	.00	.01	.0
38	5011	5017	.16	.00	.00	.00	.01	.0
39	5017	5018	.03	.01	.00	.00	.02	.0
40-XX	5017	5019						
41	5019	5020	.67	.01	.00	.00	.04	.0
42	5020	5021	.23	.02	.00	.00	.05	.0
43	5021	5022	.12	.07	.00	.00	.05	.1
44	5020	5023	.31	.02	.00	.00	.04	.0
45	5023	5024	.02	.00	.00	.00	.00	.0
46	5024	5021	.01	.00	.00	.00	.00	.0
47	5023	5025	.27	.01	.00	.00	.04	.0
48	5025	5026	.17	.00	.00	.00	.02	.0
49	5026	5062	.01	.00	.00	.00	.01	.0
50	5026	5027	.12	.00	.00	.00	.02	.0
51	5027	5028	.02	.00	.00	.00	.00	.0
52	5027	5063	.05	.00	.00	.00	.02	.0
53	5063	5064	.03	.00	.00	.00	.01	.0
54	5064	5065	.01	.00	.00	.00	.00	.0
55	5025	5029	-.06	.00	.00	.00	.01	.0
56	5029	5030	-.14	.00	.00	.00	.02	.0
57	5030	5019	-.36	.04	.00	.00	.05	.0
58	5030	5031	.17	.02	.00	.00	.04	.0
59	5031	5032	.10	.03	.00	.00	.04	.0
60-XX	5031	5033						
61	5033	5034	.02	.00	.00	.00	.01	.0
62	5042	5043	-.17	.03	.00	.00	.03	.0
63	5043	5044	-.30	.02	.00	.00	.06	.1
64	5042	5037	.35	.08	.00	.00	.07	.1
65	5037	5038	-.87	.00	.00	.00	.05	.0
66	5038	5039	-.91	.02	.00	.00	.06	.0
67	5039	5047	-1.18	.03	.00	.00	.08	.0
68	5047	5045	-1.35	.06	.00	.00	.09	.1
69	5047	5048	.06	.03	.00	.00	.02	.0
70-XX	5029	5035						
71	5035	5037	-1.08	.02	.00	.00	.07	.0
72	5035	5400	.65	.28	.00	.00	.13	.4
73-RV	5400	5066	.65	.04	.00	.00	.13	.4

74	5066	5041	.33	.10	.00	.00	.07	.1
75	5041	5036	.09	.00	.00	.00	.02	.0
76	5039	5300	.10	.03	.00	.00	.04	.0
77-RV	5300	5040	.10	.04	.00	.00	.04	.0
78	5010	5033	.06	.00	.00	.00	.01	.0
79	5034	5043	-.24	.02	.00	.00	.03	.0
80	5067	5068	.17	.01	.00	.00	.03	.0
81-FG	0	5057	5.30	.01	.00	.00	.11	.0
82	5057	5056	5.33	.00	.00	.00	.11	.0
83	5033	5034	.09	.00	.00	.00	.01	.0
84	5042	5043	-.32	.03	.00	.00	.04	.0
85	5043	5044	-.56	.02	.00	.00	.08	.1
86	5058	5044	.24	.03	.00	.00	.05	.0
87	5010	5033	.11	.00	.00	.00	.01	.0
88	5007	5003	.73	.04	.00	.00	.15	.4
89	5003	5004	.64	.07	.00	.00	.13	.3
90	5004	5005	.53	.12	.00	.00	.11	.2
91	5056	5058	2.03	.05	.00	.00	.13	.1
92	5058	5059	.55	.02	.00	.00	.07	.1
93	5059	5007	.53	.03	.00	.00	.07	.0
94	5007	5008	.32	.00	.00	.00	.04	.0
95	5008	5072	.18	.01	.00	.00	.02	.0
96	5010	5011	.23	.00	.00	.00	.03	.0
97	5011	5017	.07	.00	.00	.00	.01	.0
98-FG	0	5019	1.24	.01	.00	.00	.08	.0
99	5049	5051	.44	.05	.00	.00	.06	.0

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTION PRESSURE (kpa)
5001		.02	579.09	544.00	35.09	344.14
5002		.06	579.09	521.00	58.09	569.70
5003		.08	579.10	543.00	36.10	353.98
5004		.15	579.02	533.00	46.02	451.32
5005		1.02	578.90	545.00	33.90	332.47
5006		.06	579.01	543.00	36.01	353.14
5007		.07	579.14	525.00	54.14	530.92
5008		.16	579.13	526.00	53.13	521.07
5009		.23	578.78	521.00	57.78	566.59
5010		.15	579.12	536.00	43.12	422.86
5011		.21	579.12	542.00	37.12	363.99
5012		.14	579.01	539.00	40.01	392.35
5013		.03	579.01	534.00	45.01	441.36
5014		.04	579.01	543.00	36.01	353.09
5015		.02	579.00	544.00	35.00	343.28
5016		.02	579.00	534.00	45.00	441.34
5017		.20	579.12	557.00	22.12	216.88
5018		.03	579.11	535.00	44.11	432.56

5019	.21	589.99	563.00	26.99	264.71
5020	.13	589.98	552.00	37.98	372.48
5021	.12	589.96	563.00	26.96	264.37
5022	.12	589.89	558.00	31.89	312.72
5023	.02	589.96	568.00	21.96	215.34
5024	.01	589.96	572.00	17.96	176.11
5025	.16	589.95	564.00	25.95	254.49
5026	.05	589.95	567.00	22.95	225.06
5027	.06	589.95	564.00	25.95	254.45
5028	.02	589.95	563.00	26.95	264.26
5029	.08	589.95	567.00	22.95	225.08
5030	.05	589.95	563.00	26.95	264.32
5031	.08	589.94	571.00	18.94	185.71
5032	.10	589.91	554.00	35.91	352.13
5033	.05	579.12	544.00	35.12	344.39
5034	.35	579.12	541.00	38.12	373.80
5035	.43	579.01	557.00	22.01	215.86
5036	.09	524.85	488.00	36.85	361.39
5037	.14	579.03	560.00	19.03	186.67
5038	.04	579.04	553.00	26.04	255.35
5039	.17	579.06	544.00	35.06	343.83
5040	.10	533.96	505.00	28.96	283.96
5041	.25	524.85	485.00	39.85	390.84
5042	.14	579.11	548.00	31.11	305.10
5043	.13	579.14	556.00	23.14	226.92
5044	.08	579.16	547.00	32.16	315.37
5045	.10	579.15	547.00	32.15	315.32
5046	.11	578.86	527.00	51.86	508.58
5047	.11	579.09	537.00	42.09	412.75
5048	.06	579.06	518.00	61.06	598.80
5049	.22	578.50	500.00	78.50	769.79
5050	.04	578.49	510.00	68.49	671.70
5051	.16	578.45	507.00	71.45	700.70
5052	.15	578.34	535.00	43.34	425.07
5053	.38	578.35	501.00	77.35	758.51
5054	.28	578.82	497.00	81.82	802.37
5055	.14	578.84	499.00	79.84	782.96
5056	.13	579.24	562.00	17.24	169.05
5057	.02	579.24	567.00	12.24	120.05
5058	.14	579.19	537.00	42.19	413.72
5059	.11	579.17	542.00	37.17	364.47
5060	.07	579.14	500.00	79.14	776.07
5062	.01	589.95	565.00	24.95	244.67
5063	.02	589.94	573.00	16.94	166.16
5064	.02	589.94	577.00	12.94	126.93
5065	.01	589.94	563.00	26.94	264.22
5066	.31	524.96	510.00	14.96	146.67
5067	.31	578.45	523.00	55.45	543.80
5068	.17	578.44	525.00	53.44	524.08
5069	.06	578.45	535.00	43.45	426.11
5071	.12	579.03	540.00	39.03	382.71
5072	.18	579.13	532.00	47.13	462.14
5200	.00	578.53	515.00	63.53	622.99

5300	.00	579.03	534.00	45.03	441.62
5400	.00	578.73	525.00	53.73	526.90

R E G U L A T I N G V A L V E R E P O R T

VALVE TYPE	POSITION NODE	CONTROLLED PIPE	VALVE SETTING (m or l/s)	VALVE STATUS	UPSTREAM GRADE (m)	DOWNSTREAM GRADE (m)	THROUGH FLOW (l/s)
PRV-1	5300	77	534.00	THROTTLED	579.03	533.96	.10
PRV-1	5400	73	525.00	THROTTLED	578.73	524.96	.65

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

- (+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
- (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

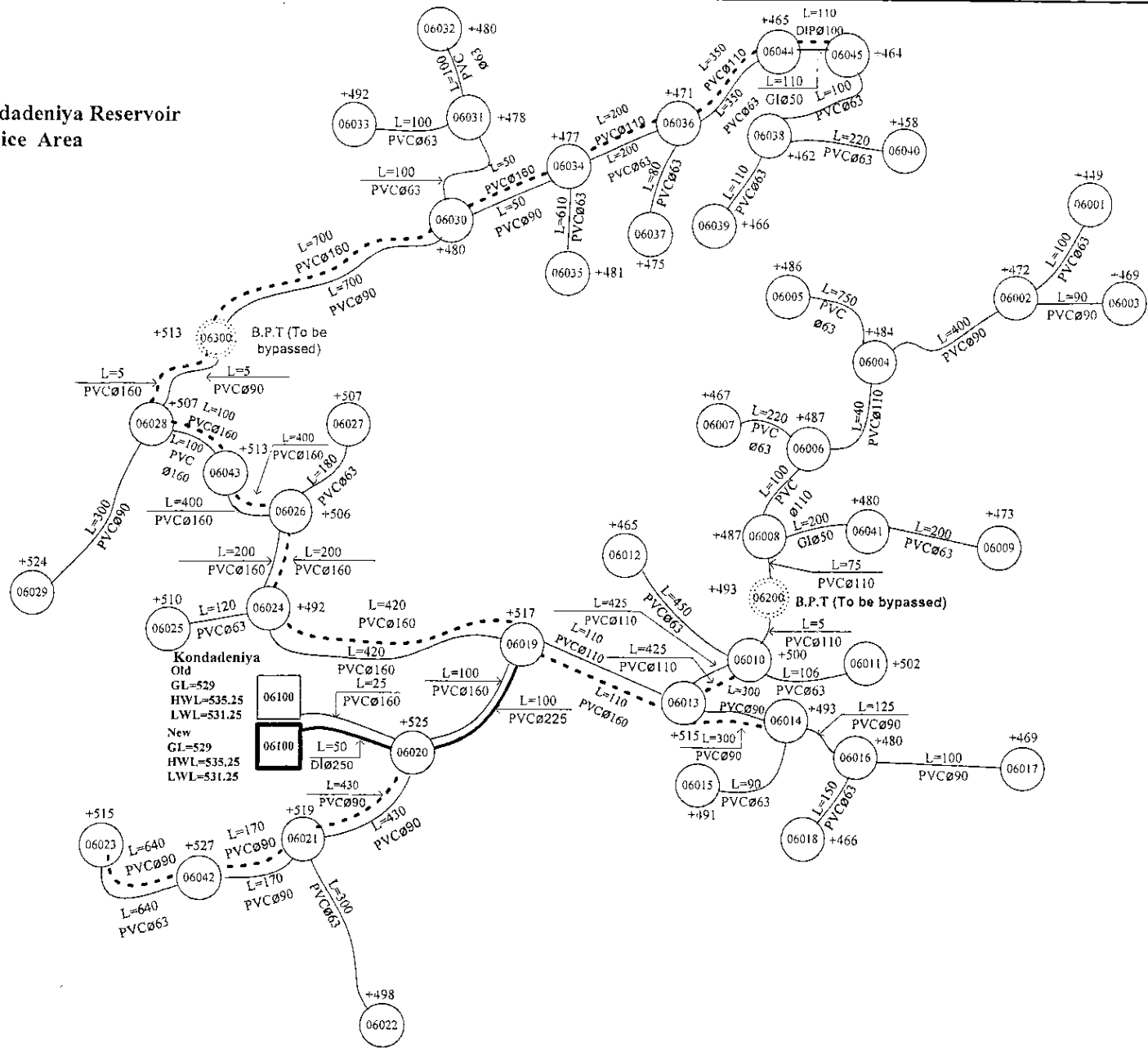
PIPE NUMBER	FLOWRATE (l/s)
1	2.72
81	5.30
98	1.24

NET SYSTEM INFLOW = 9.26
 NET SYSTEM OUTFLOW = .00
 NET SYSTEM DEMAND = 9.26

**** KYPIPE SIMULATION COMPLETED ****

DATE: 3/ 7/2002
 TIME: 13:53: 9

Kondadeniya Reservoir Service Area



Legend	
	Existing Reservoir
	Proposed Reservoir
	Node Number
	Isolated Valve
	Existing Pipe Lines
	Proposed Pipe Lines
	Expansion Pipe Lines
L=	Length of pipe
PVC	Poly vinyl chloride Pipe
GI	Galvanized Iron Pipe
DIP	Ductile Iron Pipe
SP	Stainless Steel Pipe

Appendix - 5.6 Improvement of Distribution Network in 2015
(Kondadeniya Reservoir Service Area)

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* * * * * K Y P I P E 2 * * * * *
*   University of Kentucky Hydraulic Analysis Program   *
* Distribution of Pressure and Flows in Piping Networks *
*           1000 PIPE VERSION - 1.10   (08/25/92)       *
* * * * *
  
```

DATE: 3/ 7/2002
 TIME: 13:57:39

INPUT DATA FILENAME ----- c:\D_nets\2015\KOND2015.DAT
 TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\KOND2015.OUT
 POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\KOND2015.RES

 S U M M A R Y O F O R I G I N A L D A T A

U N I T S S P E C I F I E D

FLOWRATE = liters/second
 HEAD (HGL) = meters
 PRESSURE = kpa

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-FG	0	6020	25.0	14.0	120.00	.00	531.
2	6020	6021	430.0	7.9	120.00	.00	
3	6020	6019	100.0	14.0	120.00	.00	
4	6021	6042	170.0	7.9	120.00	.00	
5	6021	6022	300.0	5.5	120.00	.00	
6	6042	6023	640.0	5.5	120.00	.00	
7	6019	6024	420.0	14.0	120.00	.00	
8	6019	6013	110.0	9.7	120.00	.00	
9	6024	6026	200.0	14.0	120.00	.00	
10	6024	6025	120.0	5.5	120.00	.00	
11	6026	6043	400.0	14.0	120.00	.00	
12	6026	6027	180.0	5.5	120.00	.00	
13	6043	6028	100.0	14.0	120.00	.00	

14	6028	6029	300.0	7.9	120.00	.00
15	6028	6300	5.0	7.9	120.00	.00
16	6300	6030	700.0	7.9	120.00	.00
17	6030	6034	50.0	7.9	120.00	.00
18	6030	6031	100.0	5.5	120.00	.00
19	6031	6032	100.0	5.5	120.00	.00
20	6031	6033	100.0	5.5	120.00	.00
21	6034	6036	200.0	5.5	120.00	.00
22	6034	6035	610.0	5.5	120.00	.00
23	6036	6044	350.0	5.5	120.00	.00
24	6036	6037	80.0	5.5	120.00	.00
25	6044	6045	110.0	5.0	120.00	.00
26	6045	6038	100.0	5.5	120.00	.00
27	6038	6039	110.0	5.5	120.00	.00
28	6038	6040	220.0	5.5	120.00	.00
29	6013	6010	425.0	9.7	120.00	.00
30	6013	6014	300.0	7.9	120.00	.00
31	6014	6016	125.0	7.9	120.00	.00
32	6014	6015	90.0	5.5	120.00	.00
33	6016	6017	100.0	7.9	120.00	.00
34	6016	6018	150.0	5.5	120.00	.00
35	6010	6200	5.0	9.7	120.00	.00
36	6010	6011	106.0	5.5	120.00	.00
37	6200	6008	75.0	9.7	120.00	.00
38	6008	6006	100.0	9.7	120.00	.00
39	6008	6041	200.0	5.0	120.00	.00
40	6041	6009	200.0	5.5	120.00	.00
41	6006	6004	40.0	9.7	120.00	.00
42	6006	6007	220.0	5.5	120.00	.00
43	6004	6002	400.0	7.9	120.00	.00
44	6004	6005	750.0	5.5	120.00	.00
45	6002	6003	90.0	7.9	120.00	.00
46	6002	6001	100.0	5.5	120.00	.00
47	6010	6012	450.0	5.5	120.00	.00
48-FG	0	6020	25.0	25.0	130.00	.00
49	6020	6021	430.0	14.0	130.00	.00
50	6020	6019	100.0	19.8	130.00	.00
51	6021	6042	170.0	7.9	130.00	.00
52	6042	6023	640.0	7.9	130.00	.00
53	6019	6024	420.0	14.0	130.00	.00
54	6019	6013	110.0	14.0	130.00	.00
55	6024	6026	200.0	14.0	130.00	.00
56	6026	6043	400.0	14.0	130.00	.00
57	6043	6028	100.0	14.0	130.00	.00
58	6028	6300	5.0	14.0	130.00	.00
59	6300	6030	700.0	14.0	130.00	.00
60	6030	6034	50.0	14.0	130.00	.00
61	6034	6036	200.0	9.7	130.00	.00
62	6036	6044	350.0	9.7	130.00	.00
63	6044	6045	110.0	10.0	130.00	.00
64-XX	6045	6038	100.0	9.7	130.00	.00
65	6013	6010	425.0	9.7	130.00	.00
66	6013	6014	300.0	7.9	130.00	.00

JUNCTION NODE DATA

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	JUNCTION ELEVATION (m)	CONNECTING PIPES					
6001		.28	449.00	46					
6002		1.41	472.00	43	45	46			
6003		.21	469.00	45					
6004		2.80	484.00	41	43	44			
6005		1.04	486.00	44					
6006		.86	487.00	38	41	42			
6007		.30	467.00	42					
6008		.86	487.00	37	38	39			
6009		.38	473.00	40					
6010		2.40	500.00	29	35	36	47	65	
6011		.22	502.00	36					
6012		.68	465.00	47					
6013		1.70	515.00	8	29	30	54	65	
6014		1.22	493.00	30	31	32	66		
6015		.19	491.00	32					
6016		1.04	480.00	31	33	34			
6017		.32	469.00	33					
6018		.32	466.00	34					
6019		1.28	517.00	3	7	8	50	53	
6020		1.14	525.00	1	2	3	48	49	
6021		1.76	519.00	2	4	5	49	51	
6022		.40	498.00	5					
6023		1.09	515.00	6	52				
6024		1.22	492.00	7	9	10	53	55	
6025		.16	510.00	10					
6026		.14	506.00	9	11	12	55	56	
6027		.02	507.00	12					
6028		.10	507.00	13	14	15	57	58	
6029		.09	524.00	14					
6030		.92	480.00	16	17	18	59	60	
6031		.07	478.00	18	19	20			
6032		.02	480.00	19					
6033		.03	492.00	20					
6034		.39	477.00	17	21	22	60	61	
6035		.24	481.00	22					
6036		.36	471.00	21	23	24	61	62	
6037		.02	475.00	24					
6038		3.45	462.00	26	27	28	64		
6039		.63	466.00	27					
6040		1.24	458.00	28					

6041	1.02	480.00	39	40		
6042	1.83	527.00	4	6	51	52
6043	.10	513.00	11	13	56	57
6044	.29	465.00	23	25	62	63
6045	2.40	464.00	25	26	63	64
6200	.00	493.00	35	37		
6300	.00	513.00	15	16	58	59

O U T P U T O P T I O N D A T A

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

S Y S T E M C O N F I G U R A T I O N

NUMBER OF PIPES (p) = 66
 NUMBER OF JUNCTION NODES (j) = 47
 NUMBER OF PRIMARY LOOPS (l) = 18
 NUMBER OF FIXED GRADE NODES (f) = 2
 NUMBER OF SUPPLY ZONES (z) = 1

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 5 TRIALS WITH AN ACCURACY = .00061

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	6020	6.13	.04	.00	.00	.40	1.7
2	6020	6021	.86	.32	.00	.00	.18	.7
3	6020	6019	8.23	.30	.00	.00	.53	2.9
4	6021	6042	1.40	.31	.00	.00	.29	1.8
5	6021	6022	.40	.31	.00	.00	.17	1.0
6	6042	6023	.29	.36	.00	.00	.12	.5
7	6019	6024	5.71	.64	.00	.00	.37	1.5
8	6019	6013	4.49	.64	.00	.00	.61	5.8
9	6024	6026	5.04	.24	.00	.00	.33	1.2
10	6024	6025	.16	.02	.00	.00	.07	.1

11	6026	6043	4.97	.47	.00	.00	.32	1.1
12	6026	6027	.02	.00	.00	.00	.01	.0
13	6043	6028	4.92	.12	.00	.00	.32	1.1
14	6028	6029	.09	.00	.00	.00	.02	.0
15	6028	6300	1.71	.01	.00	.00	.35	2.6
16	6300	6030	1.71	1.85	.00	.00	.35	2.6
17	6030	6034	1.53	.11	.00	.00	.31	2.1
18	6030	6031	.12	.01	.00	.00	.05	.1
19	6031	6032	.02	.00	.00	.00	.01	.0
20	6031	6033	.03	.00	.00	.00	.01	.0
21	6034	6036	1.44	2.25	.00	.00	.61	11.2
22	6034	6035	.24	.25	.00	.00	.10	.4
23	6036	6044	1.38	3.62	.00	.00	.58	10.3
24	6036	6037	.02	.00	.00	.00	.01	.0
25	6044	6045	1.00	1.00	.00	.00	.51	9.1
26	6045	6038	5.32	12.62	.00	.00	2.24	126.2
27	6038	6039	.63	.27	.00	.00	.27	2.4
28	6038	6040	1.24	1.87	.00	.00	.52	8.5
29	6013	6010	5.98	4.20	.00	.00	.81	9.8
30	6013	6014	1.48	.61	.00	.00	.30	2.0
31	6014	6016	1.68	.32	.00	.00	.34	2.5
32	6014	6015	.19	.02	.00	.00	.08	.2
33	6016	6017	.32	.01	.00	.00	.07	.1
34	6016	6018	.32	.10	.00	.00	.13	.6
35	6010	6200	9.16	.11	.00	.00	1.24	21.7
36	6010	6011	.22	.04	.00	.00	.09	.3
37	6200	6008	9.16	1.63	.00	.00	1.24	21.7
38	6008	6006	6.90	1.29	.00	.00	.93	12.8
39	6008	6041	1.40	3.39	.00	.00	.71	16.9
40	6041	6009	.38	.19	.00	.00	.16	.9
41	6006	6004	5.74	.37	.00	.00	.78	9.1
42	6006	6007	.30	.14	.00	.00	.13	.6
43	6004	6002	1.90	1.29	.00	.00	.39	3.2
44	6004	6005	1.04	4.61	.00	.00	.44	6.1
45	6002	6003	.21	.00	.00	.00	.04	.0
46	6002	6001	.28	.05	.00	.00	.12	.5
47	6010	6012	.68	1.26	.00	.00	.29	2.8
48-FG	0	6020	30.51	.04	.00	.00	.62	1.7
49	6020	6021	4.22	.32	.00	.00	.27	.7
50	6020	6019	22.19	.30	.00	.00	.72	2.9
51	6021	6042	1.52	.31	.00	.00	.31	1.8
52	6042	6023	.80	.36	.00	.00	.16	.5
53	6019	6024	6.18	.64	.00	.00	.40	1.5
54	6019	6013	12.76	.64	.00	.00	.83	5.8
55	6024	6026	5.47	.24	.00	.00	.36	1.2
56	6026	6043	5.38	.47	.00	.00	.35	1.1
57	6043	6028	5.33	.12	.00	.00	.35	1.1
58	6028	6300	8.35	.01	.00	.00	.54	2.6
59	6300	6030	8.35	1.85	.00	.00	.54	2.6
60	6030	6034	7.49	.11	.00	.00	.49	2.1
61	6034	6036	6.95	2.25	.00	.00	.94	11.2
62	6036	6044	6.63	3.62	.00	.00	.90	10.3
63	6044	6045	6.72	1.00	.00	.00	.86	9.1

64-XX	6045	6038							
65	6013	6010	6.48	4.20	.00	.00	.88	9.8	
66	6013	6014	1.61	.61	.00	.00	.33	2.0	

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
6001		.28	521.32	449.00	72.32	709.27
6002		1.41	521.38	472.00	49.38	484.24
6003		.21	521.37	469.00	52.37	513.62
6004		2.80	522.66	484.00	38.66	379.17
6005		1.04	518.06	486.00	32.06	314.38
6006		.86	523.03	487.00	36.03	353.35
6007		.30	522.90	467.00	55.90	548.16
6008		.86	524.32	487.00	37.32	365.99
6009		.38	520.74	473.00	47.74	468.19
6010		2.40	526.06	500.00	26.06	255.60
6011		.22	526.03	502.00	24.03	235.62
6012		.68	524.81	465.00	59.81	586.49
6013		1.70	530.27	515.00	15.27	149.73
6014		1.22	529.66	493.00	36.66	359.50
6015		.19	529.63	491.00	38.63	378.88
6016		1.04	529.34	480.00	49.34	483.85
6017		.32	529.33	469.00	60.33	591.60
6018		.32	529.23	466.00	63.23	620.12
6019		1.28	530.91	517.00	13.91	136.38
6020		1.14	531.21	525.00	6.21	60.87
6021		1.76	530.88	519.00	11.88	116.55
6022		.40	530.57	498.00	32.57	319.41
6023		1.09	530.21	515.00	15.21	149.19
6024		1.22	530.27	492.00	38.27	375.30
6025		.16	530.25	510.00	20.25	198.55
6026		.14	530.03	506.00	24.03	235.63
6027		.02	530.03	507.00	23.03	225.82
6028		.10	529.44	507.00	22.44	220.08
6029		.09	529.44	524.00	5.44	53.34
6030		.92	527.57	480.00	47.57	466.55
6031		.07	527.56	478.00	49.56	486.05
6032		.02	527.56	480.00	47.56	466.43
6033		.03	527.56	492.00	35.56	348.75
6034		.39	527.47	477.00	50.47	494.91
6035		.24	527.22	481.00	46.22	453.25
6036		.36	525.21	471.00	54.21	531.67
6037		.02	525.21	475.00	50.21	492.44
6038		3.45	507.97	462.00	45.97	450.84
6039		.63	507.71	466.00	41.71	408.99
6040		1.24	506.10	458.00	48.10	471.71
6041		1.02	520.93	480.00	40.93	401.41

6042	1.83	530.57	527.00	3.57	35.05
6043	.10	529.56	513.00	16.56	162.37
6044	.29	521.60	465.00	56.60	555.05
6045	2.40	520.60	464.00	56.60	555.01
6200	.00	525.95	493.00	32.95	323.17
6300	.00	529.43	513.00	16.43	161.11

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	6.13
48	30.51

NET SYSTEM INFLOW = 36.64
 NET SYSTEM OUTFLOW = .00
 NET SYSTEM DEMAND = 36.64

D A T A C H A N G E S F O R N E X T S I M U L A T I O N

D E M A N D C H A N G E S

DEMAND TYPE = 1 - GDF = .300

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00001

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/1000 (m/m)
1-FG	0	6020	1.84	.00	.00	.00	.12	.1

2	6020	6021	.26	.03	.00	.00	.05	.0
3	6020	6019	2.47	.03	.00	.00	.16	.3
4	6021	6042	.42	.03	.00	.00	.09	.2
5	6021	6022	.12	.03	.00	.00	.05	.1
6	6042	6023	.09	.04	.00	.00	.04	.0
7	6019	6024	1.71	.07	.00	.00	.11	.1
8	6019	6013	1.35	.07	.00	.00	.18	.6
9	6024	6026	1.51	.03	.00	.00	.10	.1
10	6024	6025	.05	.00	.00	.00	.02	.0
11	6026	6043	1.49	.05	.00	.00	.10	.1
12	6026	6027	.01	.00	.00	.00	.00	.0
13	6043	6028	1.48	.01	.00	.00	.10	.1
14	6028	6029	.03	.00	.00	.00	.01	.0
15	6028	6300	.51	.00	.00	.00	.10	.2
16	6300	6030	.51	.20	.00	.00	.10	.2
17	6030	6034	.46	.01	.00	.00	.09	.2
18	6030	6031	.04	.00	.00	.00	.02	.0
19	6031	6032	.01	.00	.00	.00	.00	.0
20	6031	6033	.01	.00	.00	.00	.00	.0
21	6034	6036	.43	.24	.00	.00	.18	1.2
22	6034	6035	.07	.03	.00	.00	.03	.0
23	6036	6044	.41	.39	.00	.00	.17	1.1
24	6036	6037	.01	.00	.00	.00	.00	.0
25	6044	6045	.30	.11	.00	.00	.15	.9
26	6045	6038	1.60	1.36	.00	.00	.67	13.5
27	6038	6039	.19	.03	.00	.00	.08	.2
28	6038	6040	.37	.20	.00	.00	.16	.9
29	6013	6010	1.79	.45	.00	.00	.24	1.0
30	6013	6014	.44	.07	.00	.00	.09	.2
31	6014	6016	.50	.03	.00	.00	.10	.2
32	6014	6015	.06	.00	.00	.00	.02	.0
33	6016	6017	.10	.00	.00	.00	.02	.0
34	6016	6018	.10	.01	.00	.00	.04	.0
35	6010	6200	2.75	.01	.00	.00	.37	2.3
36	6010	6011	.07	.00	.00	.00	.03	.0
37	6200	6008	2.75	.18	.00	.00	.37	2.3
38	6008	6006	2.07	.14	.00	.00	.28	1.3
39	6008	6041	.42	.36	.00	.00	.21	1.8
40	6041	6009	.11	.02	.00	.00	.05	.1
41	6006	6004	1.72	.04	.00	.00	.23	.9
42	6006	6007	.09	.01	.00	.00	.04	.0
43	6004	6002	.57	.14	.00	.00	.12	.3
44	6004	6005	.31	.50	.00	.00	.13	.6
45	6002	6003	.06	.00	.00	.00	.01	.0
46	6002	6001	.08	.01	.00	.00	.04	.0
47	6010	6012	.20	.14	.00	.00	.09	.3
48-FG	0	6020	9.15	.00	.00	.00	.19	.1
49	6020	6021	1.26	.03	.00	.00	.08	.0
50	6020	6019	6.66	.03	.00	.00	.22	.3
51	6021	6042	.46	.03	.00	.00	.09	.2
52	6042	6023	.24	.04	.00	.00	.05	.0
53	6019	6024	1.85	.07	.00	.00	.12	.1
54	6019	6013	3.83	.07	.00	.00	.25	.6

55	6024	6026	1.64	.03	.00	.00	.11	.1
56	6026	6043	1.61	.05	.00	.00	.10	.1
57	6043	6028	1.60	.01	.00	.00	.10	.1
58	6028	6300	2.50	.00	.00	.00	.16	.2
59	6300	6030	2.50	.20	.00	.00	.16	.2
60	6030	6034	2.25	.01	.00	.00	.15	.2
61	6034	6036	2.08	.24	.00	.00	.28	1.2
62	6036	6044	1.99	.39	.00	.00	.27	1.1
63	6044	6045	2.02	.11	.00	.00	.26	.9
64-XX	6045	6038						
65	6013	6010	1.94	.45	.00	.00	.26	1.0
66	6013	6014	.48	.07	.00	.00	.10	.2

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTION PRESSURE (kpa)
6001		.08	530.18	449.00	81.18	796.13
6002		.42	530.19	472.00	58.19	570.64
6003		.06	530.19	469.00	61.19	600.05
6004		.84	530.33	484.00	46.33	454.31
6005		.31	529.83	486.00	43.83	429.84
6006		.26	530.37	487.00	43.37	425.28
6007		.09	530.35	467.00	63.35	621.27
6008		.26	530.50	487.00	43.50	426.64
6009		.11	530.12	473.00	57.12	560.16
6010		.72	530.69	500.00	30.69	300.99
6011		.07	530.69	502.00	28.69	281.34
6012		.20	530.56	465.00	65.56	642.90
6013		.51	531.14	515.00	16.14	158.32
6014		.37	531.08	493.00	38.08	373.43
6015		.06	531.08	491.00	40.08	393.02
6016		.31	531.04	480.00	51.04	500.58
6017		.10	531.04	469.00	62.04	608.44
6018		.10	531.03	466.00	65.03	637.76
6019		.38	531.21	517.00	14.21	139.38
6020		.34	531.25	525.00	6.25	61.25
6021		.53	531.21	519.00	12.21	119.75
6022		.12	531.18	498.00	33.18	325.36
6023		.33	531.14	515.00	16.14	158.27
6024		.37	531.14	492.00	39.14	383.88
6025		.05	531.14	510.00	21.14	207.33
6026		.04	531.12	506.00	25.12	246.33
6027		.01	531.12	507.00	24.12	236.52
6028		.03	531.06	507.00	24.06	235.91
6029		.03	531.06	524.00	7.06	69.19
6030		.28	530.85	480.00	50.85	498.72
6031		.02	530.85	478.00	52.85	518.32
6032		.01	530.85	480.00	50.85	498.70

6033	.01	530.85	492.00	38.85	381.02
6034	.12	530.84	477.00	53.84	528.02
6035	.07	530.82	481.00	49.82	488.53
6036	.11	530.60	471.00	59.60	584.49
6037	.01	530.60	475.00	55.60	545.26
6038	1.04	528.75	462.00	66.75	654.56
6039	.19	528.72	466.00	62.72	615.05
6040	.37	528.55	458.00	70.55	691.81
6041	.31	530.14	480.00	50.14	491.71
6042	.55	531.18	527.00	4.18	40.97
6043	.03	531.07	513.00	18.07	177.19
6044	.09	530.21	465.00	65.21	639.51
6045	.72	530.10	464.00	66.10	648.26
6200	.00	530.68	493.00	37.68	369.52
6300	.00	531.05	513.00	18.05	177.05

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

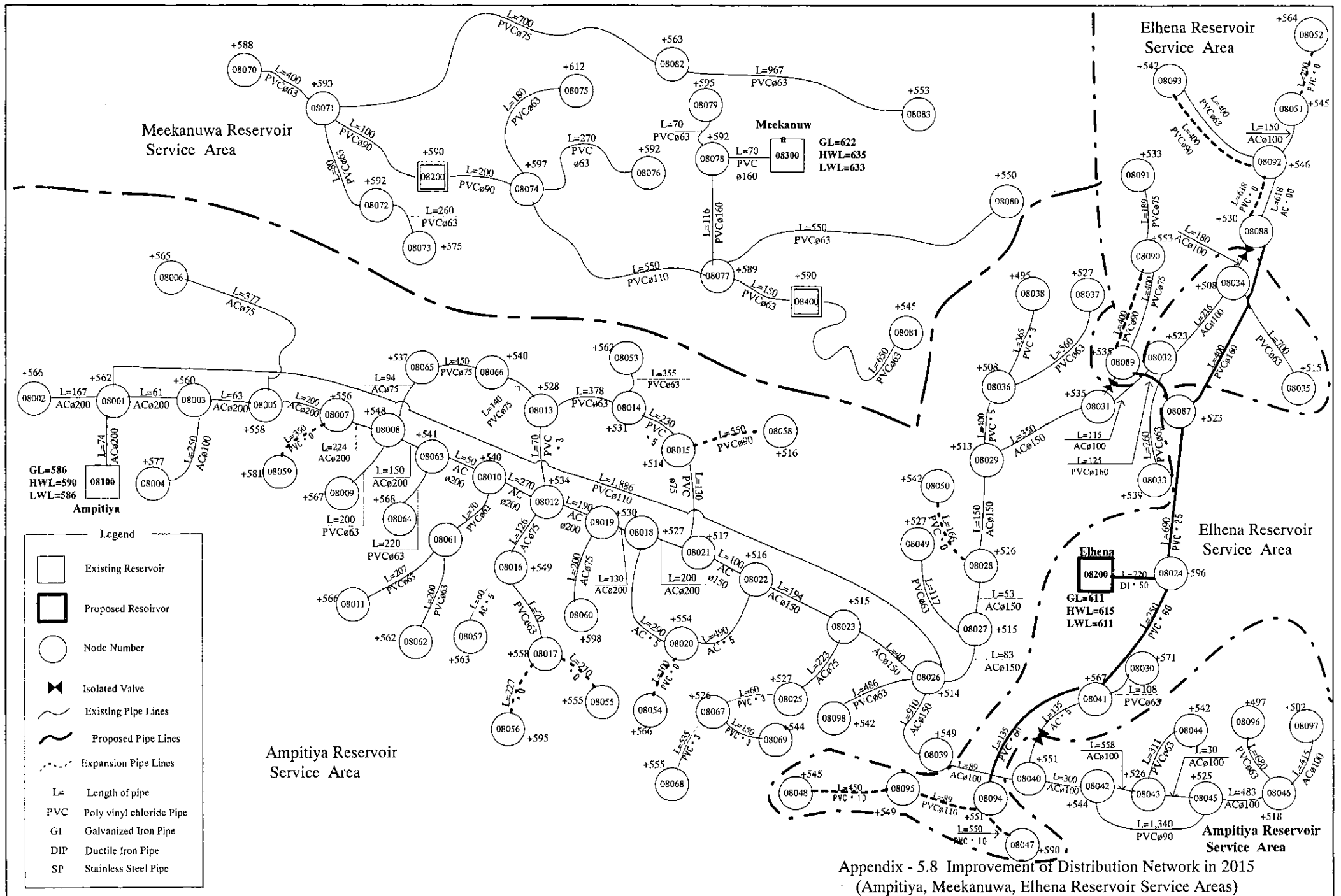
(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
(-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	1.84
48	9.15

NET SYSTEM INFLOW = 10.99
NET SYSTEM OUTFLOW = .00
NET SYSTEM DEMAND = 10.99

**** KYPIPE SIMULATION COMPLETED ****

DATE: 3/ 7/2002
TIME: 13:57:39



* * * * * K Y P I P E 2 * * * * *
 * University of Kentucky Hydraulic Analysis Program *
 * Distribution of Pressure and Flows in Piping Networks *
 * 1000 PIPE VERSION - 1.10 (08/25/92) *
 * * * * *

DATE: 3/ 7/2002
 TIME: 13:58:47

INPUT DATA FILENAME ----- c:\D_nets\2015\ELHE2015.DAT
 TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\ELHE2015.OUT
 POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\ELHE2015.RES

 S U M M A R Y O F O R I G I N A L D A T A

U N I T S S P E C I F I E D

FLOWRATE = liters/second
 HEAD (HGL) = meters
 PRESSURE = kpa

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-FG	0	8024	220.0	20.0	130.00	.00	611.
2	8024	8041	250.0	14.0	130.00	.00	
3	8041	8094	135.0	14.0	130.00	.00	
4	8094	8047	550.0	9.7	130.00	.00	
5	8094	8095	89.0	9.7	130.00	.00	
6	8095	8048	450.0	9.7	130.00	.00	
7	8024	8087	690.0	19.8	130.00	.00	
8	8087	8089	125.0	14.0	130.00	.00	
9	8087	8088	400.0	14.0	130.00	.00	
10	8089	8090	390.0	6.5	120.00	.00	
11	8090	8091	189.0	6.5	120.00	.00	
12	8088	8092	618.0	10.0	120.00	.00	
13	8092	8093	400.0	5.5	120.00	.00	

14	8092	8051	150.0	10.0	120.00	.00
15	8051	8052	200.0	9.7	130.00	.00
16	8041	8030	108.0	5.5	130.00	.00

JUNCTION NODE DATA

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	JUNCTION ELEVATION (m)	CONNECTING PIPES		
8024		.75	596.00	1	2	7
8030		.75	571.00	16		
8041		.75	567.00	2	3	16
8047		.89	590.00	4		
8048		.89	545.00	6		
8051		.21	545.00	14	15	
8052		1.21	564.00	15		
8087		.00	523.00	7	8	9
8088		.00	520.00	9	12	
8089		.75	535.00	8	10	
8090		.75	553.00	10	11	
8091		2.89	533.00	11		
8092		1.21	546.00	12	13	14
8093		1.21	542.00	13		
8094		.00	551.00	3	4	5
8095		.89	549.00	5	6	

OUTPUT OPTION DATA

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

SYSTEM CONFIGURATION

NUMBER OF PIPES (p) = 16
 NUMBER OF JUNCTION NODES (j) = 16
 NUMBER OF PRIMARY LOOPS (l) = 0
 NUMBER OF FIXED GRADE NODES (f) = 1
 NUMBER OF SUPPLY ZONES (z) = 1

 SIMULATION RESULTS

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

PIPELINE RESULTS

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	8024	13.15	.24	.00	.00	.42	1.0
2	8024	8041	4.17	.18	.00	.00	.27	.7
3	8041	8094	2.67	.04	.00	.00	.17	.3
4	8094	8047	.89	.14	.00	.00	.12	.2
5	8094	8095	1.78	.08	.00	.00	.24	.9
6	8095	8048	.89	.11	.00	.00	.12	.2
7	8024	8087	8.23	.33	.00	.00	.27	.4
8	8087	8089	4.39	.10	.00	.00	.29	.8
9	8087	8088	3.84	.25	.00	.00	.25	.6
10	8089	8090	3.64	10.81	.00	.00	1.10	27.7
11	8090	8091	2.89	3.42	.00	.00	.87	18.0
12	8088	8092	3.84	2.32	.00	.00	.49	3.7
13	8092	8093	1.21	3.25	.00	.00	.51	8.1
14	8092	8051	1.42	.09	.00	.00	.18	.5
15	8051	8052	1.21	.09	.00	.00	.16	.4
16	8041	8030	.75	.31	.00	.00	.32	2.8

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTION PRESSURE (kpa)
8024		.75	610.76	596.00	14.76	144.77
8030		.75	610.27	571.00	39.27	385.08
8041		.75	610.58	567.00	43.58	427.36
8047		.89	610.40	590.00	20.40	200.04
8048		.89	610.34	545.00	65.34	640.79
8051		.21	607.77	545.00	62.77	615.59
8052		1.21	607.68	564.00	43.68	428.39
8087		.00	610.43	523.00	87.43	857.43
8088		.00	610.18	520.00	90.18	884.38
8089		.75	610.33	535.00	75.33	738.76
8090		.75	599.53	553.00	46.53	456.27
8091		2.89	596.11	533.00	63.11	618.90
8092		1.21	607.86	546.00	61.86	606.65
8093		1.21	604.61	542.00	62.61	613.99
8094		.00	610.54	551.00	59.54	583.85
8095		.89	610.46	549.00	61.46	602.67

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	13.15

NET SYSTEM INFLOW = 13.15
 NET SYSTEM OUTFLOW = .00
 NET SYSTEM DEMAND = 13.15

D A T A C H A N G E S F O R N E X T S I M U L A T I O N

D E M A N D C H A N G E S

DEMAND TYPE = 1 - GDF = .300

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/1000 (m/m)
1-FG	0	8024	3.95	.03	.00	.00	.13	.1
2	8024	8041	1.25	.02	.00	.00	.08	.0
3	8041	8094	.80	.00	.00	.00	.05	.0
4	8094	8047	.27	.01	.00	.00	.04	.0
5	8094	8095	.53	.01	.00	.00	.07	.1
6	8095	8048	.27	.01	.00	.00	.04	.0
7	8024	8087	2.47	.04	.00	.00	.08	.0
8	8087	8089	1.32	.01	.00	.00	.09	.0

9	8087	8088	1.15	.03	.00	.00	.07	.0
10	8089	8090	1.09	1.16	.00	.00	.33	2.9
11	8090	8091	.87	.37	.00	.00	.26	1.9
12	8088	8092	1.15	.25	.00	.00	.15	.4
13	8092	8093	.36	.35	.00	.00	.15	.8
14	8092	8051	.43	.01	.00	.00	.05	.0
15	8051	8052	.36	.01	.00	.00	.05	.0
16	8041	8030	.23	.03	.00	.00	.09	.3

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTION PRESSURE (kpa)
8024		.23	610.97	596.00	14.97	146.85
8030		.23	610.92	571.00	39.92	391.49
8041		.23	610.95	567.00	43.95	431.05
8047		.27	610.94	590.00	20.94	205.31
8048		.27	610.93	545.00	65.93	646.55
8051		.06	610.65	545.00	65.65	643.84
8052		.36	610.64	564.00	46.64	457.42
8087		.00	610.94	523.00	87.94	862.39
8088		.00	610.91	520.00	90.91	891.55
8089		.23	610.93	535.00	75.93	744.61
8090		.23	609.77	553.00	56.77	556.69
8091		.87	609.40	533.00	76.40	749.22
8092		.36	610.66	546.00	64.66	634.13
8093		.36	610.31	542.00	68.31	669.92
8094		.00	610.95	551.00	59.95	587.91
8095		.27	610.94	549.00	61.94	607.44

SUMMARY OF INFLOWS AND OUTFLOWS

- (+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
- (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	3.95
NET SYSTEM INFLOW =	3.95
NET SYSTEM OUTFLOW =	.00
NET SYSTEM DEMAND =	3.94

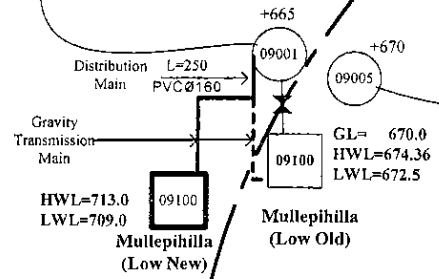
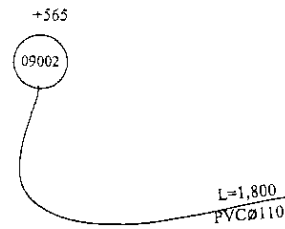
**** KYPIPE SIMULATION COMPLETED ****

DATE = 03-07-2002
JOB NAME = GKWSAP - JICA - Elhena SR

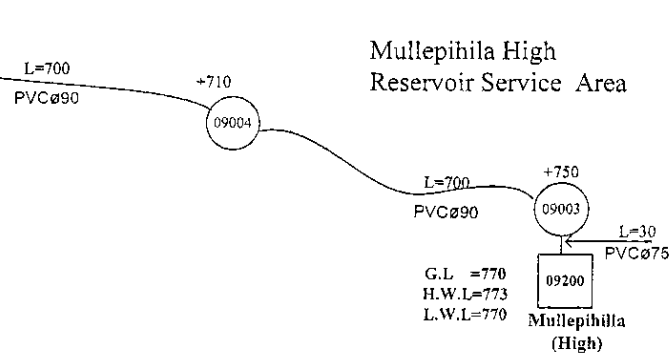
PAGE NO. 6

DATE: 3/ 7/2002
TIME: 13:58:47

Mullepihilla Low & Mullepihilla New Reservoir Service Area



Mullepihilla High Reservoir Service Area



Legend	
	Existing Reservoir
	Proposed Reservoir
	Node Number
	Isolated Valve
	Non-return Valve
	Existing Pipe Lines
	Proposed Pipe Lines
	Expansion Pipe Lines
L=	Length of pipe
PVC	Poly vinyl chloride Pipe
GI	Galvanized Iron Pipe
DIP	Ductile Iron Pipe
SP	Stainless Steel Pipe

Appendix - 5.9 Improvement of Distribution Network in 2015
 (Mullepihilla Low (Old), Mullepihilla Low (New), Mullepihilla(High) Reservoir Service Areas)

```

* * * * * K Y P I P E 2 * * * * *
*   University of Kentucky Hydraulic Analysis Program   *
* Distribution of Pressure and Flows in Piping Networks *
*           1000 PIPE VERSION - 1.10   (08/25/92)       *
* * * * *
    
```

DATE: 3/ 7/2002
 TIME: 14: 0: 6

INPUT DATA FILENAME ----- c:\D_nets\2015\MULL2015.DAT
 TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\MULL2015.OUT
 POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\MULL2015.RES

 S U M M A R Y O F O R I G I N A L D A T A

U N I T S S P E C I F I E D

FLOWRATE = liters/second
 HEAD (HGL) = meters
 PRESSURE = kpa

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1 #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-XXFG	0 9001	25.0	9.7	120.00	.00	672.
2-FG	0 9001	250.0	14.0	130.00	.00	709.
3	9001 9002	1800.0	9.7	120.00	.00	

J U N C T I O N N O D E D A T A

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	JUNCTION ELEVATION (m)	CONNECTING PIPES

9001	2.43	665.00	1	2	3
9002	14.65	565.00	3		

O U T P U T O P T I O N D A T A

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

S Y S T E M C O N F I G U R A T I O N

NUMBER OF PIPES(p) = 3
 NUMBER OF JUNCTION NODES(j) = 2
 NUMBER OF PRIMARY LOOPS(l) = 0
 NUMBER OF FIXED GRADE NODES(f) = 2
 NUMBER OF SUPPLY ZONES(z) = 1

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1 #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-XXFG	0 9001						
2-FG	0 9001	17.08	2.49	.00	.00	1.11	9.9
3	9001 9002	14.65	93.57	.00	.00	1.98	51.9

J U N C T I O N N O D E R E S U L T S

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
9001		2.43	706.51	665.00	41.51	407.04
9002		14.65	612.93	565.00	47.93	470.05

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
2	17.08
NET SYSTEM INFLOW =	17.08
NET SYSTEM OUTFLOW =	.00
NET SYSTEM DEMAND =	17.08

D A T A C H A N G E S F O R N E X T S I M U L A T I O N

D E M A N D C H A N G E S

DEMAND TYPE = 1 - GDF = .300

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/1000 (m/m)
1-XXFG	0	9001						
2-FG	0	9001	5.12	.27	.00	.00	.33	1.0
3	9001	9002	4.39	10.06	.00	.00	.59	5.5

J U N C T I O N N O D E R E S U L T S

JUNCTION JUNCTION EXTERNAL HYDRAULIC JUNCTION PRESSURE JUNCTIO

NUMBER	TITLE	DEMAND (l/s)	GRADE (m)	ELEVATION (m)	HEAD (m)	PRESSUR (kpa)
9001		.73	708.73	665.00	43.73	428.86
9002		4.39	698.67	565.00	133.67	1310.84

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
2	5.12

NET SYSTEM INFLOW = 5.12
 NET SYSTEM OUTFLOW = .00
 NET SYSTEM DEMAND = 5.12

**** KYPIPE SIMULATION COMPLETED ****

DATE: 3/ 7/2002
 TIME: 14: 0: 6


```

* * * * * K Y P I P E 2 * * * * *
*   University of Kentucky Hydraulic Analysis Program   *
* Distribution of Pressure and Flows in Piping Networks *
*           1000 PIPE VERSION - 1.10   (08/25/92)       *
* * * * *
  
```

DATE: 3/ 7/2002
 TIME: 14: 0:49

INPUT DATA FILENAME ----- c:\D_nets\2015\HANP2015.DAT
 TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\HANP2015.OUT
 POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\HANP2015.RES

 S U M M A R Y O F O R I G I N A L D A T A

U N I T S S P E C I F I E D

FLOWRATE = liters/second
 HEAD (HGL) = meters
 PRESSURE = kpa

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-FG	0	1040	80.0	19.8	130.00	.00	637.
2	1040	1048	180.0	19.8	130.00	.00	
3	1048	1049	200.0	19.8	130.00	.00	
4	1040	1038	15.0	5.5	120.00	.00	
5	1038	1037	195.0	5.5	120.00	.00	
6	1038	1039	16.0	5.5	120.00	.00	

J U N C T I O N N O D E D A T A

JUNCTION JUNCTION EXTERNAL JUNCTION

NUMBER	TITLE	DEMAND (l/s)	ELEVATION (m)	CONNECTING PIPES		
1037		1.92	622.00	5		
1038		1.92	631.00	4	5	6
1039		1.92	634.00	6		
1040		1.92	624.00	1	2	4
1048		6.10	600.00	2	3	
1049		8.26	575.00	3		

OUTPUT OPTION DATA

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

SYSTEM CONFIGURATION

NUMBER OF PIPES(p) = 6
 NUMBER OF JUNCTION NODES(j) = 6
 NUMBER OF PRIMARY LOOPS(l) = 0
 NUMBER OF FIXED GRADE NODES(f) = 1
 NUMBER OF SUPPLY ZONES(z) = 1

 SIMULATION RESULTS

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

PIPELINE RESULTS

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1 #2		FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	1040	22.04	.24	.00	.00	.72	2.9
2	1040	1048	14.36	.24	.00	.00	.47	1.3
3	1048	1049	8.26	.10	.00	.00	.27	.4
4	1040	1038	5.76	2.19	.00	.00	2.42	146.2
5	1038	1037	1.92	3.73	.00	.00	.81	19.1
6	1038	1039	1.92	.31	.00	.00	.81	19.1

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTION PRESSURE (kpa)
1037		1.92	630.84	622.00	8.84	86.71
1038		1.92	634.57	631.00	3.57	35.01
1039		1.92	634.26	634.00	.26	2.59
1040		1.92	636.76	624.00	12.76	125.17
1048		6.10	636.52	600.00	36.52	358.17
1049		8.26	636.43	575.00	61.43	602.39

SUMMARY OF INFLOWS AND OUTFLOWS

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	22.04
NET SYSTEM INFLOW =	22.04
NET SYSTEM OUTFLOW =	.00
NET SYSTEM DEMAND =	22.04

DATA CHANGES FOR NEXT SIMULATION

DEMAND CHANGES

DEMAND TYPE = 1 - GDF = .300

 SIMULATION RESULTS

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

PIPELINE RESULTS

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	1040	6.61	.03	.00	.00	.21	.3
2	1040	1048	4.31	.03	.00	.00	.14	.1
3	1048	1049	2.48	.01	.00	.00	.08	.0
4	1040	1038	1.73	.24	.00	.00	.73	15.7
5	1038	1037	.58	.40	.00	.00	.24	2.0
6	1038	1039	.58	.03	.00	.00	.24	2.0

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTION PRESSURE (kpa)
1037		.58	636.34	622.00	14.34	140.60
1038		.58	636.74	631.00	5.74	56.28
1039		.58	636.71	634.00	2.71	26.53
1040		.58	636.97	624.00	12.97	127.24
1048		1.83	636.95	600.00	36.95	362.34
1049		2.48	636.94	575.00	61.94	607.41

SUMMARY OF INFLOWS AND OUTFLOWS

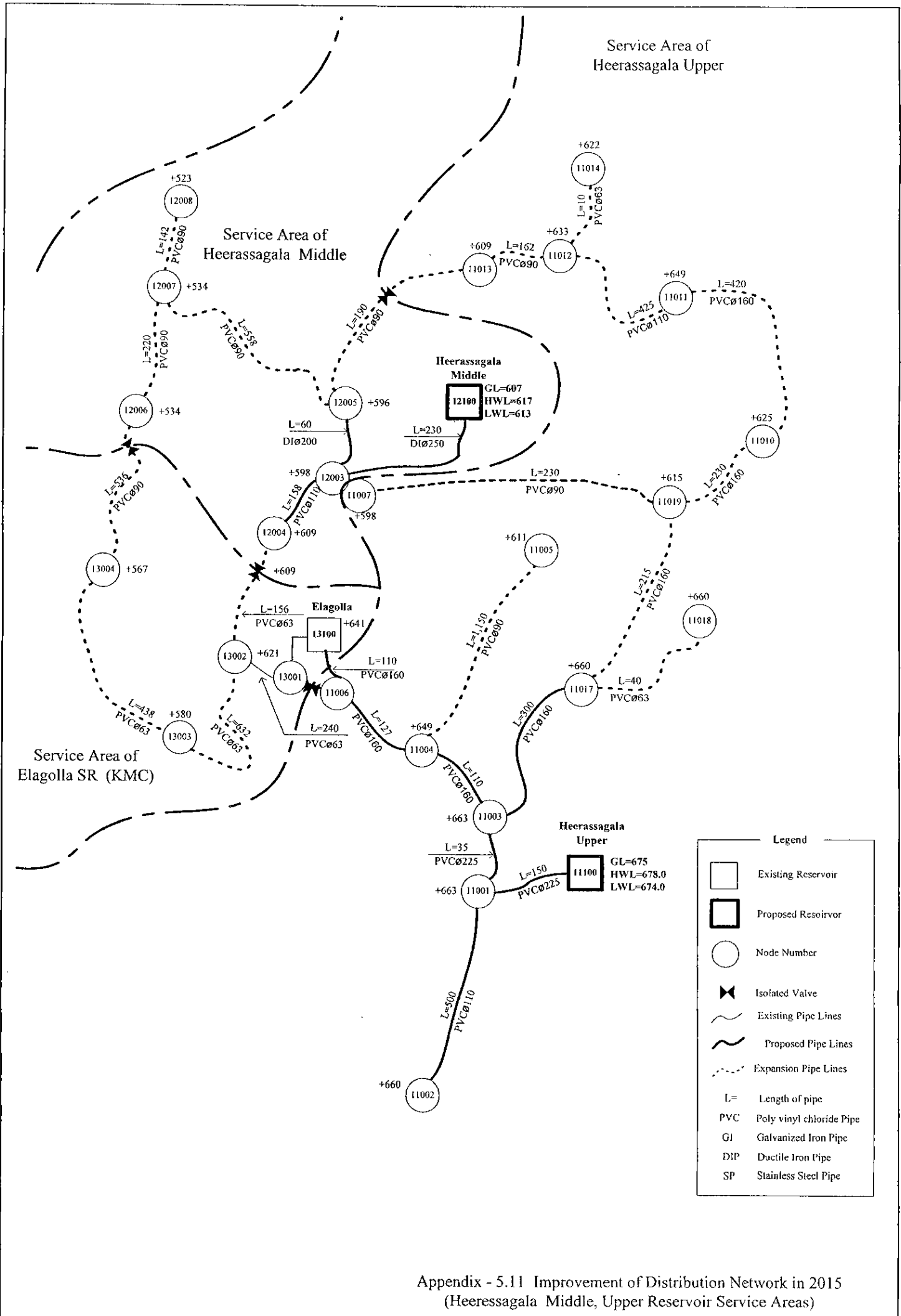
- (+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
- (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	6.61

NET SYSTEM INFLOW = 6.61
 NET SYSTEM OUTFLOW = .00
 NET SYSTEM DEMAND = 6.61

**** KYPIPE SIMULATION COMPLETED ****

DATE: 3/ 7/2002
 TIME: 14: 0:49



Appendix - 5.11 Improvement of Distribution Network in 2015
 (Heeressagala Middle, Upper Reservoir Service Areas)

```

* * * * * K Y P I P E 2 * * * * *
*   University of Kentucky Hydraulic Analysis Program   *
* Distribution of Pressure and Flows in Piping Networks *
*           1000 PIPE VERSION - 1.10   (08/25/92)       *
* * * * *
    
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DATE: 3/ 7/2002
 TIME: 14:11:58

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 TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\HEEU2015.OUT
 POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\HEEU2015.RES

 S U M M A R Y O F O R I G I N A L D A T A

U N I T S S P E C I F I E D

FLOWRATE = liters/second
 HEAD (HGL) = meters
 PRESSURE = kpa

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1 #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-FG	0 1101	150.0	19.8	130.00	.00	674.
2	1101 1102	500.0	9.7	130.00	.00	
3	1101 1103	1.0	19.8	130.00	.00	
4	1103 1104	110.0	14.0	130.00	.00	
5	1103 1117	300.0	14.0	130.00	.00	
6	1104 1105	1150.0	7.9	130.00	.00	
7	1117 1118	40.0	5.5	130.00	.00	
8	1117 1119	215.0	14.0	130.00	.00	
9	1119 1110	230.0	14.0	130.00	.00	
10	1110 1111	420.0	14.0	130.00	.00	
11	1111 1112	425.0	9.7	130.00	.00	
12	1112 1113	162.0	7.9	130.00	.00	
13	1112 1114	10.0	5.5	130.00	.00	

JOB NAME = GKWSAP - JICA - Heeressagala Upper SR

14	1119	1107	230.0	7.9	130.00	.00
15	1104	1106	127.0	14.0	130.00	.00
16	1106	1300	110.0	14.0	130.00	.00

JUNCTION NODE DATA

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	JUNCTION ELEVATION (m)	CONNECTING PIPES		
1101		.89	663.00	1	2	3
1102		.89	660.00	2		
1103		.89	663.00	3	4	5
1104		.89	647.00	4	6	15
1105		.90	611.00	6		
1106		.89	659.00	15	16	
1107		.89	598.00	14		
1110		.89	625.00	9	10	
1111		.89	649.00	10	11	
1112		.90	633.00	11	12	13
1113		.89	609.00	12		
1114		.89	622.00	13		
1117		.89	660.00	5	7	8
1118		.89	660.00	7		
1119		.90	615.00	8	9	14
1300		17.99	649.00	16		

OUTPUT OPTION DATA

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

SYSTEM CONFIGURATION

NUMBER OF PIPES (p)	=	16
NUMBER OF JUNCTION NODES (j)	=	16
NUMBER OF PRIMARY LOOPS (l)	=	0
NUMBER OF FIXED GRADE NODES (f)	=	1
NUMBER OF SUPPLY ZONES (z)	=	1

 SIMULATION RESULTS

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

JOB NAME = GKWSAP - JICA - Heeressagala Upper SR

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	#2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	1101	31.37	.85	.00	.00	1.02	5.6
2	1101	1102	.89	.13	.00	.00	.12	.2
3	1101	1103	29.59	.01	.00	.00	.96	5.1
4	1103	1104	20.67	1.56	.00	.00	1.34	14.2
5	1103	1117	8.03	.74	.00	.00	.52	2.4
6	1104	1105	.90	.80	.00	.00	.18	.6
7	1117	1118	.89	.16	.00	.00	.37	3.9
8	1117	1119	6.25	.33	.00	.00	.41	1.5
9	1119	1110	4.46	.19	.00	.00	.29	.8
10	1110	1111	3.57	.23	.00	.00	.23	.5
11	1111	1112	2.68	.82	.00	.00	.36	1.9
12	1112	1113	.89	.11	.00	.00	.18	.6
13	1112	1114	.89	.04	.00	.00	.37	3.9
14	1119	1107	.89	.16	.00	.00	.18	.6
15	1104	1106	18.88	1.53	.00	.00	1.23	12.0
16	1106	1300	17.99	1.21	.00	.00	1.17	10.9

J U N C T I O N N O D E R E S U L T S

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
1101		.89	673.65	663.00	10.65	104.41
1102		.89	673.52	660.00	13.52	132.61
1103		.89	673.64	663.00	10.64	104.36
1104		.89	672.08	647.00	25.08	245.95
1105		.90	671.28	611.00	60.28	591.16
1106		.89	670.55	659.00	11.55	113.32
1107		.89	672.41	598.00	74.41	729.74
1110		.89	672.38	625.00	47.38	464.63
1111		.89	672.15	649.00	23.15	227.00
1112		.90	671.33	633.00	38.33	375.87
1113		.89	671.22	609.00	62.22	610.15
1114		.89	671.29	622.00	49.29	483.36
1117		.89	672.90	660.00	12.90	126.53
1118		.89	672.74	660.00	12.74	124.97
1119		.90	672.57	615.00	57.57	564.57
1300		17.99	669.35	649.00	20.35	199.54

132?

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	31.37

NET SYSTEM INFLOW = 31.37
 NET SYSTEM OUTFLOW = .00
 NET SYSTEM DEMAND = 31.37

D A T A C H A N G E S F O R N E X T S I M U L A T I O N

D E M A N D C H A N G E S

DEMAND TYPE = 1 - GDF = .300

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1 #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0 1101	9.41	.09	.00	.00	.31	.6
2	1101 1102	.27	.01	.00	.00	.04	.0
3	1101 1103	8.88	.00	.00	.00	.29	.5
4	1103 1104	6.20	.17	.00	.00	.40	1.5
5	1103 1117	2.41	.08	.00	.00	.16	.2
6	1104 1105	.27	.09	.00	.00	.06	.0
7	1117 1118	.27	.02	.00	.00	.11	.4
8	1117 1119	1.88	.04	.00	.00	.12	.1

JOB NAME = GKWSAP - JICA - Heeressagala Upper SR

9	1119	1110	1.34	.02	.00	.00	.09	.0
10	1110	1111	1.07	.02	.00	.00	.07	.0
11	1111	1112	.80	.09	.00	.00	.11	.2
12	1112	1113	.27	.01	.00	.00	.05	.0
13	1112	1114	.27	.00	.00	.00	.11	.4
14	1119	1107	.27	.02	.00	.00	.05	.0
15	1104	1106	5.66	.16	.00	.00	.37	1.2
16	1106	1300	5.40	.13	.00	.00	.35	1.1

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
1101		.27	674.41	663.00	11.41	111.88
1102		.27	674.39	660.00	14.39	141.17
1103		.27	674.41	663.00	11.41	111.87
1104		.27	674.24	647.00	27.24	267.13
1105		.27	674.15	611.00	63.15	619.33
1106		.27	674.08	659.00	15.08	147.84
1107		.27	674.28	598.00	76.28	748.01
1110		.27	674.27	625.00	49.27	483.19
1111		.27	674.25	649.00	25.25	247.59
1112		.27	674.16	633.00	41.16	403.63
1113		.27	674.15	609.00	65.15	638.88
1114		.27	674.15	622.00	52.15	511.46
1117		.27	674.33	660.00	14.33	140.51
1118		.27	674.31	660.00	14.31	140.34
1119		.27	674.29	615.00	59.29	581.46
1300		5.40	673.95	649.00	24.95	244.64

SUMMARY OF INFLOWS AND OUTFLOWS

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES

(-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	9.41
NET SYSTEM INFLOW =	9.41
NET SYSTEM OUTFLOW =	.00
NET SYSTEM DEMAND =	9.41

**** KYPIPE SIMULATION COMPLETED ****

DATE = 03-07-2002

JOB NAME = GKWSAP - JICA - Heeressagala Upper SR

PAGE NO. 6

DATE: 3/ 7/2002

TIME: 14:11:58

* * * * * K Y P I P E 2 * * * * *
 * University of Kentucky Hydraulic Analysis Program *
 * Distribution of Pressure and Flows in Piping Networks *
 * 1000 PIPE VERSION - 1.10 (08/25/92) *
 * * * * *

DATE: 3/ 7/2002
 TIME: 14:20:22

INPUT DATA FILENAME ----- c:\D_nets\2015\HEEM2015.DAT
 TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\HEEM2015.OUT
 POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\HEEM2015.RES

 S U M M A R Y O F O R I G I N A L D A T A

U N I T S S P E C I F I E D

FLOWRATE = liters/second
 HEAD (HGL) = meters
 PRESSURE = kpa

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1 #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-FG	0 1203	230.0	25.0	130.00	.00	613.
2	1203 1204	158.0	9.7	130.00	.00	
3	1203 1205	40.0	20.0	130.00	.00	
4	1205 1207	558.0	7.9	130.00	.00	
5	1207 1206	220.0	7.9	130.00	.00	
6	1207 1208	142.0	7.9	130.00	.00	

J U N C T I O N N O D E D A T A

JUNCTION JUNCTION EXTERNAL JUNCTION

NUMBER	TITLE	DEMAND (l/s)	ELEVATION (m)	CONNECTING PIPES		
1203		3.56	598.00	1	2	3
1204		3.56	609.00	2		
1205		3.57	596.00	3	4	
1206		3.56	534.00	5		
1207		3.56	534.00	4	5	6
1208		3.56	523.00	6		

OUTPUT OPTION DATA

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

SYSTEM CONFIGURATION

NUMBER OF PIPES(p) = 6
 NUMBER OF JUNCTION NODES(j) = 6
 NUMBER OF PRIMARY LOOPS(l) = 0
 NUMBER OF FIXED GRADE NODES(f) = 1
 NUMBER OF SUPPLY ZONES(z) = 1

 SIMULATION RESULTS

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

PIPELINE RESULTS

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1 #2		FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	1203	21.37	.21	.00	.00	.44	.9
2	1203	1204	3.56	.52	.00	.00	.48	3.2
3	1203	1205	14.25	.05	.00	.00	.45	1.2
4	1205	1207	10.68	37.85	.00	.00	2.18	67.8
5	1207	1206	3.56	1.95	.00	.00	.73	8.8
6	1207	1208	3.56	1.26	.00	.00	.73	8.8

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
1203		3.56	612.79	598.00	14.79	145.08
1204		3.56	612.28	609.00	3.28	32.15
1205		3.57	612.74	596.00	16.74	164.20
1206		3.56	572.94	534.00	38.94	381.91
1207		3.56	574.89	534.00	40.89	401.04
1208		3.56	573.63	523.00	50.63	496.56

SUMMARY OF INFLOWS AND OUTFLOWS

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	21.37
NET SYSTEM INFLOW =	21.37
NET SYSTEM OUTFLOW =	.00
NET SYSTEM DEMAND =	21.37

DATA CHANGES FOR NEXT SIMULATION

DEMAND CHANGES

DEMAND TYPE = 1 - GDF = .300

 SIMULATION RESULTS

THE RESULTS ARE OBTAINED AFTER 2 TRIALS WITH AN ACCURACY = .00000

PIPELINE RESULTS

STATUS CODE:	XX -CLOSED PIPE	FG -FIXED GRADE NODE	PU -PUMP LINE
	CV -CHECK VALVE	RV -REGULATING VALVE	TK -STORAGE TANK

PIPE NUMBER	NODE NOS.		FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
	#1	#2						
1-FG	0	1203	6.41	.02	.00	.00	.13	.1
2	1203	1204	1.07	.06	.00	.00	.14	.3
3	1203	1205	4.27	.01	.00	.00	.14	.1
4	1205	1207	3.20	4.07	.00	.00	.65	7.3
5	1207	1206	1.07	.21	.00	.00	.22	.9
6	1207	1208	1.07	.14	.00	.00	.22	.9

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
1203		1.07	612.98	598.00	14.98	146.88
1204		1.07	612.92	609.00	3.92	38.46
1205		1.07	612.97	596.00	16.97	166.44
1206		1.07	608.69	534.00	74.69	732.48
1207		1.07	608.90	534.00	74.90	734.54
1208		1.07	608.77	523.00	85.77	841.08

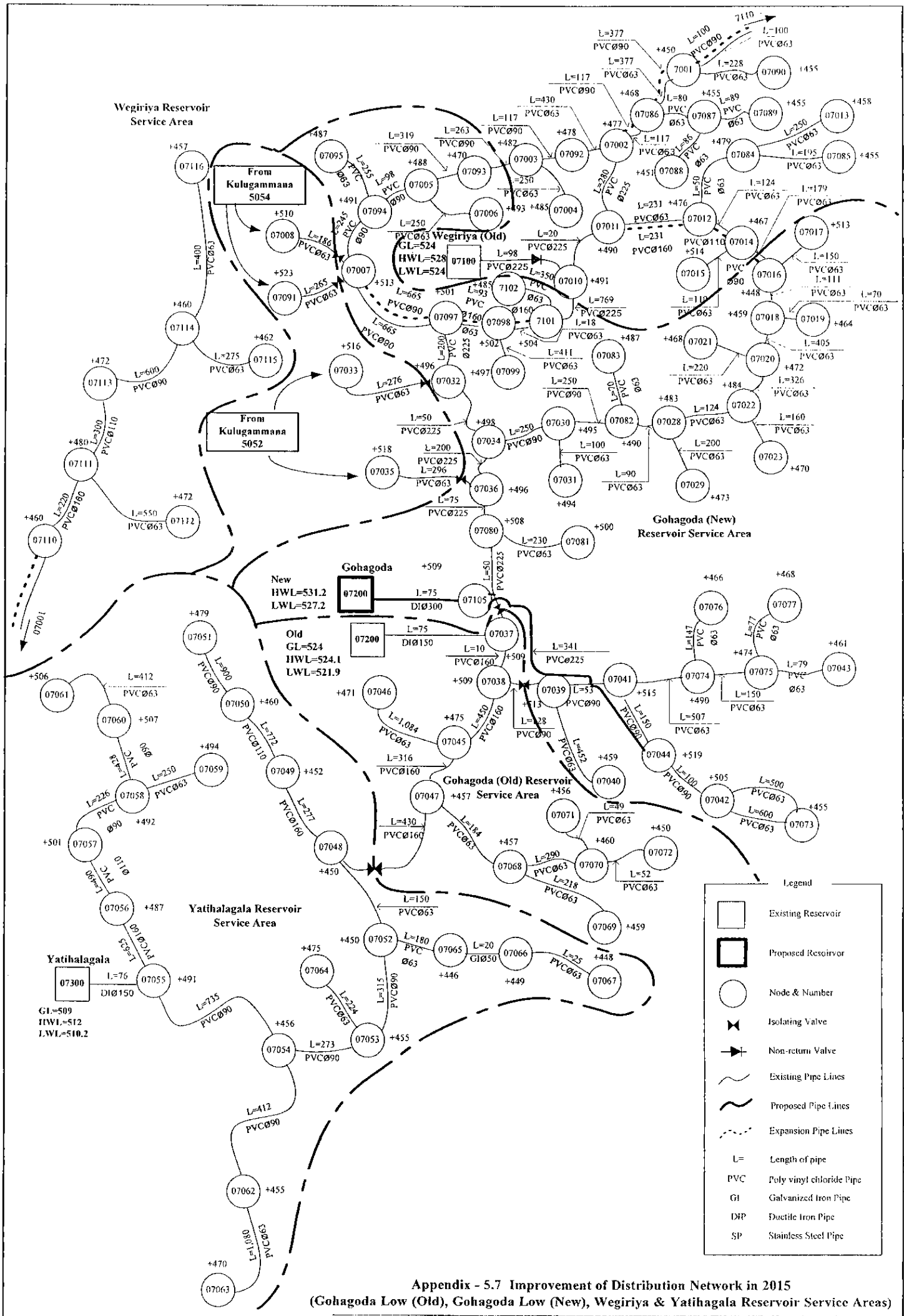
SUMMARY OF INFLOWS AND OUTFLOWS

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	6.41
NET SYSTEM INFLOW =	6.41
NET SYSTEM OUTFLOW =	.00
NET SYSTEM DEMAND =	6.41

**** KYPIPE SIMULATION COMPLETED ****

DATE: 3/ 7/2002
 TIME: 14:20:22



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* * * * * K Y P I P E 2 * * * * *
*   University of Kentucky Hydraulic Analysis Program   *
* Distribution of Pressure and Flows in Piping Networks *
*           1000 PIPE VERSION - 1.10   (08/25/92)       *
* * * * *
  
```

DATE: 3/12/2002
 TIME: 8:50:25

INPUT DATA FILENAME ----- c:\D_nets\2015\GOHA2015.DAT
 TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\GOHA2015.OUT
 POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\GOHA2015.RES

 S U M M A R Y O F O R I G I N A L D A T A

U N I T S S P E C I F I E D

FLOWRATE = liters/second
 HEAD (HGL) = meters
 PRESSURE = kpa

P I P E L I N E D A T A

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-FG	0	7037	75.0	15.0	120.00	.00	521.
2	7037	7038	10.0	14.0	120.00	.00	
3	7038	7045	450.0	14.0	120.00	.00	
4	7045	7047	316.0	14.0	120.00	.00	
5	7045	7046	1084.0	5.5	120.00	.00	
6	7047	7068	184.0	5.5	120.00	.00	
7	7068	7069	218.0	5.5	120.00	.00	
8	7068	7070	290.0	5.5	120.00	.00	
9	7070	7072	52.0	5.5	120.00	.00	
10	7070	7071	49.0	5.5	120.00	.00	
11-XX	7038	7039	128.0	7.9	120.00	.00	
12	7039	7041	53.0	7.9	120.00	.00	
13	7039	7040	452.0	5.5	120.00	.00	

14	7041	7074	507.0	5.5	120.00	.00
15	7041	7044	150.0	7.9	120.00	.00
16	7044	7042	100.0	7.9	120.00	.00
17	7074	7076	147.0	5.5	120.00	.00
18	7074	7075	150.0	5.5	120.00	.00
19	7075	7043	79.0	5.5	120.00	.00
20-XX	7037	7080	50.0	19.8	120.00	.00
21	7081	7080	230.0	5.5	120.00	.00
22	7036	7080	75.0	19.8	120.00	.00
23-XX	7035	7036	296.0	5.5	120.00	.00
24	7036	7034	200.0	19.8	120.00	.00
25	7034	7030	250.0	7.9	120.00	.00
26	7034	7032	50.0	19.8	120.00	.00
27	7030	7031	100.0	5.5	120.00	.00
28	7030	7082	250.0	7.9	120.00	.00
29	7082	7083	70.0	5.5	120.00	.00
30	7082	7028	90.0	5.5	120.00	.00
31	7028	7029	200.0	5.5	120.00	.00
32	7028	7022	124.0	5.5	120.00	.00
33	7022	7023	160.0	5.5	120.00	.00
34	7022	7020	326.0	5.5	120.00	.00
35	7021	7020	220.0	5.5	120.00	.00
36	7020	7018	405.0	5.5	120.00	.00
37	7018	7019	70.0	5.5	120.00	.00
38	7018	7016	111.0	5.5	120.00	.00
39	7016	7017	150.0	5.5	120.00	.00
40	7016	7014	179.0	5.5	120.00	.00
41	7014	7015	110.0	5.5	120.00	.00
42	7014	7012	124.0	5.5	120.00	.00
43	7012	7011	231.0	5.5	120.00	.00
44	7012	7084	50.0	5.5	120.00	.00
45	7084	7013	250.0	5.5	120.00	.00
46	7084	7085	195.0	5.5	120.00	.00
47	7011	7010	20.0	19.8	120.00	.00
48	7010	7101	769.0	19.8	120.00	.00
49-FGCV	0	7010	98.0	19.8	120.00	.00
50	7101	7102	350.0	5.5	120.00	.00
51	7101	7098	18.0	5.5	120.00	.00
52	7098	7099	411.0	5.5	120.00	.00
53	7098	7097	93.0	5.5	120.00	.00
54	7097	7032	200.0	19.8	120.00	.00
55-XX	7032	7033	276.0	5.5	120.00	.00
56	7097	7007	665.0	7.9	120.00	.00
57	7007	7091	265.0	5.5	120.00	.00
58	7007	7008	186.0	5.5	120.00	.00
59	7007	7094	245.0	7.9	120.00	.00
60	7094	7095	255.0	5.5	120.00	.00
61	7094	7005	98.0	7.9	120.00	.00
62	7005	7006	250.0	5.5	120.00	.00
63	7005	7093	319.0	7.9	120.00	.00
64	7093	7003	263.0	7.9	120.00	.00
65	7003	7004	250.0	5.5	120.00	.00
66	7003	7092	117.0	7.9	120.00	.00

67	7092	7002	430.0	5.5	120.00	.00	
68	7011	7002	280.0	19.8	120.00	.00	
69	7002	7086	117.0	5.5	120.00	.00	
70	7086	7001	377.0	5.5	120.00	.00	
71	7086	7087	80.0	5.5	120.00	.00	
72	7087	7088	86.0	5.5	120.00	.00	
73	7087	7089	89.0	5.5	120.00	.00	
74	7001	7090	228.0	5.5	120.00	.00	
75	7001	7110	100.0	5.5	120.00	.00	
76	7110	7111	220.0	14.0	120.00	.00	
77	7112	7111	550.0	5.5	120.00	.00	
78	7111	7113	300.0	9.7	120.00	.00	
79	7113	7114	600.0	7.9	120.00	.00	
80	7114	7115	275.0	5.5	120.00	.00	
81	7114	7116	400.0	5.5	120.00	.00	
82	7075	7077	77.0	5.5	120.00	.00	
83-FG	0	7105	75.0	30.0	130.00	.00	527.
84	7105	7080	50.0	19.8	120.00	.00	
85	7012	7011	231.0	14.0	130.00	.00	
86	7101	7098	18.0	14.0	130.00	.00	
87	7098	7097	93.0	14.0	130.00	.00	
88	7002	7086	117.0	9.7	130.00	.00	
89	7086	7001	377.0	9.7	130.00	.00	
90	7001	7110	100.0	7.9	130.00	.00	
91	7012	7014	124.0	14.0	130.00	.00	
92	7014	7016	179.0	9.7	130.00	.00	
93	7097	7007	665.0	9.7	130.00	.00	
94	7105	7044	341.0	19.8	130.00	.00	
95	7042	7073	500.0	5.5	120.00	.00	
96	7042	7073	600.0	5.5	120.00	.00	
97	7034	7030	250.0	7.9	130.00	.00	
98	7030	7082	250.0	7.9	130.00	.00	
99-FGCV	0	7010	98.0	19.8	130.00	.00	526.

JUNCTION NODE DATA

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	JUNCTION ELEVATION (m)	CONNECTING PIPES				
7001		1.53	450.00	70	74	75	89	90
7002		.89	477.00	67	68	69	88	
7003		.89	482.00	64	65	66		
7004		1.13	485.00	65				
7005		.20	488.00	61	62	63		
7006		.20	493.00	62				
7007		.20	513.00	56	57	58	59	93
7008		.00	510.00	58				
7010		.89	491.00	47	48	49	99	
7011		.89	490.00	43	47	68	85	

JOB NAME = GKWSAP - JICA - Gohagoda New & Old SR

7012	.71	476.00	42	43	44	85	91
7013	.89	458.00	45				
7014	.71	467.00	40	41	42	91	92
7015	.71	514.00	41				
7016	.89	448.00	38	39	40	92	
7017	.89	513.00	39				
7018	.15	459.00	36	37	38		
7019	.18	464.00	37				
7020	.15	472.00	34	35	36		
7021	.15	468.00	35				
7022	.15	484.00	32	33	34		
7023	.15	470.00	33				
7028	.15	483.00	30	31	32		
7029	.15	473.00	31				
7030	.12	495.00	25	27	28	97	98
7031	.18	494.00	27				
7032	.65	496.00	26	54	55		
7033	.00	516.00	55				
7034	.18	498.00	24	25	26	97	
7035	.00	518.00	23				
7036	.18	496.00	22	23	24		
7037	.72	509.00	1	2	20		
7038	.72	509.00	2	3	11		
7039	.10	513.00	11	12	13		
7040	.10	459.00	13				
7041	.10	515.00	12	14	15		
7042	.10	512.00	16	95	96		
7043	.10	461.00	19				
7044	.10	519.00	15	16	94		
7045	.72	475.00	3	4	5		
7046	2.43	471.00	5				
7047	1.17	457.00	4	6			
7068	1.16	457.00	6	7	8		
7069	1.17	459.00	7				
7070	1.16	460.00	8	9	10		
7071	1.17	456.00	10				
7072	1.16	450.00	9				
7073	.10	455.00	95	96			
7074	.10	490.00	14	17	18		
7075	.10	474.00	18	19	82		
7076	.10	466.00	17				
7077	.10	468.00	82				
7080	.10	508.00	20	21	22	84	
7081	.10	500.00	21				
7082	.10	490.00	28	29	30	98	
7083	.10	487.00	29				
7084	.71	479.00	44	45	46		
7085	.89	455.00	46				
7086	.89	468.00	69	70	71	88	89
7087	.89	455.00	71	72	73		
7088	1.60	451.00	72				
7089	1.60	455.00	73				
7090	1.60	455.00	74				

7091	.00	523.00	57					
7092	.92	478.00	66	67				
7093	.13	470.00	63	64				
7094	.13	491.00	59	60	61			
7095	.13	487.00	60					
7097	.13	501.00	53	54	56	87	93	
7098	1.03	502.00	51	52	53	86	87	
7099	.13	497.00	52					
7101	1.03	504.00	48	50	51	86		
7102	.13	485.00	50					
7105	.00	509.00	83	84	94			
7110	1.60	460.00	75	76	90			
7111	1.60	480.00	76	77	78			
7112	1.60	472.00	77					
7113	1.60	472.00	78	79				
7114	1.60	460.00	79	80	81			
7115	1.60	462.00	80					
7116	1.60	457.00	81					

O U T P U T O P T I O N D A T A

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

S Y S T E M C O N F I G U R A T I O N

NUMBER OF PIPES(p) = 99
 NUMBER OF JUNCTION NODES(j) = 81
 NUMBER OF PRIMARY LOOPS(l) = 15
 NUMBER OF FIXED GRADE NODES(f) = 4
 NUMBER OF SUPPLY ZONES(z) = 1

 S I M U L A T I O N R E S U L T S

*** WARNING - A PORTION OF THE SYSTEM IS DISCONNECTED BY CLOSED LINES FROM A
 **** A FIX WILL BE ATTEMPTED

*** WARNING - THE FOLLOWING JUNCTION NODES ARE DISCONNECTED FROM THE SYSTEM
 DEMANDS AT THESE JUNCTION NODES ARE SET TO ZERO:
 7033 7035

PIPE NO. 23 HAS BEEN OPENED TO REMOVE DISCONNECTION

JOB NAME = GKWSAP - JICA - Gohagoda New & Old SR

*** WARNING - A PORTION OF THE SYSTEM IS DISCONNECTED BY CLOSED LINES FROM A
 **** A FIX WILL BE ATTEMPTED

*** WARNING - THE FOLLOWING JUNCTION NODES ARE DISCONNECTED FROM THE SYSTEM
 DEMANDS AT THESE JUNCTION NODES ARE SET TO ZERO:

7033

PIPE NO. 55 HAS BEEN OPENED TO REMOVE DISCONNECTION

THE RESULTS ARE OBTAINED AFTER 7 TRIALS WITH AN ACCURACY = .00495

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	#2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FG	0	7037	11.58	.30	.00	.00	.66	4.0
2	7037	7038	10.86	.05	.00	.00	.71	5.0
3	7038	7045	10.14	1.98	.00	.00	.66	4.4
4	7045	7047	6.99	.70	.00	.00	.45	2.2
5	7045	7046	2.43	32.06	.00	.00	1.02	29.5
6	7047	7068	5.82	27.43	.00	.00	2.45	149.0
7	7068	7069	1.17	1.67	.00	.00	.49	7.6
8	7068	7070	3.49	16.77	.00	.00	1.47	57.8
9	7070	7072	1.16	.39	.00	.00	.49	7.5
10	7070	7071	1.17	.37	.00	.00	.49	7.6
11-XX	7038	7039						
12	7039	7041	-.20	.00	.00	.00	.04	.0
13	7039	7040	.10	.04	.00	.00	.04	.0
14	7041	7074	.50	.80	.00	.00	.21	1.5
15	7041	7044	-.80	.10	.00	.00	.16	.6
16	7044	7042	.20	.00	.00	.00	.04	.0
17	7074	7076	.10	.01	.00	.00	.04	.0
18	7074	7075	.30	.09	.00	.00	.13	.6
19	7075	7043	.10	.01	.00	.00	.04	.0
20-XX	7037	7080						
21	7081	7080	-.10	.02	.00	.00	.04	.0
22	7036	7080	-14.15	.11	.00	.00	.46	1.5
23-XX	7035	7036	.00	.00	.00	.00	.00	.0
24	7036	7034	13.97	.29	.00	.00	.45	1.4
25	7034	7030	.72	.13	.00	.00	.15	.5
26	7034	7032	12.29	.06	.00	.00	.40	1.1
27	7030	7031	.18	.02	.00	.00	.08	.2
28	7030	7082	.57	.09	.00	.00	.12	.3

JOB NAME = GKWSAP - JICA - Gohagoda New & Old SR

29	7082	7083	.10	.01	.00	.00	.04	.0
30	7082	7028	1.00	.51	.00	.00	.42	5.6
31	7028	7029	.15	.03	.00	.00	.06	.1
32	7028	7022	.70	.36	.00	.00	.29	2.9
33	7022	7023	.15	.03	.00	.00	.06	.1
34	7022	7020	.40	.33	.00	.00	.17	1.0
35	7021	7020	-.15	.04	.00	.00	.06	.1
36	7020	7018	.10	.03	.00	.00	.04	.0
37	7018	7019	.18	.02	.00	.00	.08	.2
38	7018	7016	-.23	.04	.00	.00	.10	.3
39	7016	7017	.89	.69	.00	.00	.37	4.6
40	7016	7014	-.54	.32	.00	.00	.23	1.8
41	7014	7015	.71	.33	.00	.00	.30	3.0
42	7014	7012	-.26	.06	.00	.00	.11	.4
43	7012	7011	-.51	.38	.00	.00	.21	1.6
44	7012	7084	2.49	1.55	.00	.00	1.05	30.9
45	7084	7013	.89	1.15	.00	.00	.37	4.6
46	7084	7085	.89	.90	.00	.00	.37	4.6
47	7011	7010	-28.82	.11	.00	.00	.94	5.6
48	7010	7101	-6.36	.26	.00	.00	.21	.3
49-FGCV	0	7010	11.21	.10	.00	.00	.36	.9
50	7101	7102	.13	.05	.00	.00	.05	.1
51	7101	7098	-.55	.03	.00	.00	.23	1.9
52	7098	7099	.13	.05	.00	.00	.05	.1
53	7098	7097	-.64	.23	.00	.00	.27	2.4
54	7097	7032	-11.64	.21	.00	.00	.38	1.0
55-XX	7032	7033	.00	.00	.00	.00	.00	.0
56	7097	7007	.99	.64	.00	.00	.20	.9
57	7007	7091	.00	.00	.00	.00	.00	.0
58	7007	7008	.00	.00	.00	.00	.00	.0
59	7007	7094	2.63	1.44	.00	.00	.54	5.8
60	7094	7095	.13	.03	.00	.00	.05	.1
61	7094	7005	2.37	.48	.00	.00	.48	4.8
62	7005	7006	.20	.07	.00	.00	.08	.2
63	7005	7093	1.97	1.10	.00	.00	.40	3.4
64	7093	7003	1.84	.80	.00	.00	.38	3.0
65	7003	7004	1.13	1.79	.00	.00	.48	7.1
66	7003	7092	-.18	.00	.00	.00	.04	.0
67	7092	7002	-1.10	2.91	.00	.00	.46	6.7
68	7011	7002	21.30	.90	.00	.00	.69	3.2
69	7002	7086	3.32	6.17	.00	.00	1.40	52.7
70	7086	7001	2.46	11.44	.00	.00	1.04	30.3
71	7086	7087	4.09	6.21	.00	.00	1.72	77.5
72	7087	7088	1.60	1.17	.00	.00	.67	13.6
73	7087	7089	1.60	1.21	.00	.00	.67	13.6
74	7001	7090	1.60	3.11	.00	.00	.67	13.6
75	7001	7110	2.94	4.21	.00	.00	1.24	42.1
76	7110	7111	9.60	.88	.00	.00	.62	3.9
77	7112	7111	-1.60	7.50	.00	.00	.67	13.6
78	7111	7113	6.40	3.36	.00	.00	.87	11.2
79	7113	7114	4.80	10.73	.00	.00	.98	17.8
80	7114	7115	1.60	3.75	.00	.00	.67	13.6
81	7114	7116	1.60	5.46	.00	.00	.67	13.6

82	7075	7077	.10	.01	.00	.00	.04	.0
83-FG	0	7105	15.44	.02	.00	.00	.22	.2
84	7105	7080	14.35	.08	.00	.00	.47	1.5
85	7012	7011	-6.13	.34	.00	.00	.40	1.4
86	7101	7098	-6.96	.03	.00	.00	.45	1.8
87	7098	7097	-8.04	.23	.00	.00	.52	2.4
88	7002	7086	15.99	6.17	.00	.00	2.16	52.7
89	7086	7001	11.87	11.44	.00	.00	1.61	30.3
90	7001	7110	8.26	4.21	.00	.00	1.68	42.1
91	7012	7014	3.18	.05	.00	.00	.21	.4
92	7014	7016	1.48	.11	.00	.00	.20	.6
93	7097	7007	1.84	.64	.00	.00	.25	.9
94	7105	7044	1.10	.00	.00	.00	.04	.0
95	7042	7073	.05	.01	.00	.00	.02	.0
96	7042	7073	.05	.01	.00	.00	.02	.0
97	7034	7030	.78	.13	.00	.00	.16	.5
98	7030	7082	.62	.09	.00	.00	.13	.3
99-FGCV	0	7010	12.14	.10	.00	.00	.39	.9

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
7001		1.53	507.29	450.00	57.29	561.78
7002		.89	524.89	477.00	47.89	469.64
7003		.89	521.97	482.00	39.97	392.01
7004		1.13	520.18	485.00	35.18	345.02
7005		.20	523.87	488.00	35.87	351.80
7006		.20	523.80	493.00	30.80	302.05
7007		.20	525.79	513.00	12.79	125.44
7008		.00	525.79	510.00	15.79	154.86
7010		.89	525.90	491.00	34.90	342.29
7011		.89	525.79	490.00	35.79	350.99
7012		.71	525.41	476.00	49.41	484.59
7013		.89	522.72	458.00	64.72	634.65
7014		.71	525.36	467.00	58.36	572.29
7015		.71	525.02	514.00	11.02	108.11
7016		.89	525.04	448.00	77.04	755.46
7017		.89	524.34	513.00	11.34	111.25
7018		.15	524.99	459.00	65.99	647.16
7019		.18	524.98	464.00	60.98	597.97
7020		.15	525.02	472.00	53.02	519.97
7021		.15	524.98	468.00	56.98	558.83
7022		.15	525.61	484.00	41.61	408.03
7023		.15	525.58	470.00	55.58	545.06
7028		.15	525.97	483.00	42.97	421.39
7029		.15	525.94	473.00	52.94	519.12
7030		.12	526.57	495.00	31.57	309.57
7031		.18	526.54	494.00	32.54	319.14

7032	.65	526.64	496.00	30.64	300.49
7033	.00	526.64	516.00	10.64	104.36
7034	.18	526.70	498.00	28.70	281.45
7035	.00	526.99	518.00	8.99	88.20
7036	.18	526.99	496.00	30.99	303.95
7037	.72	521.60	509.00	12.60	123.55
7038	.72	521.55	509.00	12.55	123.06
7039	.10	527.08	513.00	14.08	138.09
7040	.10	527.04	459.00	68.04	667.29
7041	.10	527.08	515.00	12.08	118.50
7042	.10	527.18	512.00	15.18	148.83
7043	.10	526.18	461.00	65.18	639.23
7044	.10	527.18	519.00	8.18	80.23
7045	.72	519.57	475.00	44.57	437.05
7046	2.43	487.51	471.00	16.51	161.89
7047	1.17	518.87	457.00	61.87	606.72
7068	1.16	491.44	457.00	34.44	337.72
7069	1.17	489.77	459.00	30.77	301.77
7070	1.16	474.67	460.00	14.67	143.86
7071	1.17	474.30	456.00	18.30	179.42
7072	1.16	474.28	450.00	24.28	238.09
7073	.10	527.16	455.00	72.16	707.69
7074	.10	526.28	490.00	36.28	355.80
7075	.10	526.19	474.00	52.19	511.81
7076	.10	526.27	466.00	60.27	591.05
7077	.10	526.18	468.00	58.18	570.59
7080	.10	527.11	508.00	19.11	187.38
7081	.10	527.09	500.00	27.09	265.65
7082	.10	526.48	490.00	36.48	357.74
7083	.10	526.47	487.00	39.47	387.11
7084	.71	523.87	479.00	44.87	440.00
7085	.89	522.97	455.00	67.97	666.56
7086	.89	518.72	468.00	50.72	497.42
7087	.89	512.52	455.00	57.52	564.06
7088	1.60	511.34	451.00	60.34	591.78
7089	1.60	511.30	455.00	56.30	552.15
7090	1.60	504.18	455.00	49.18	482.25
7091	.00	525.79	523.00	2.79	27.37
7092	.92	521.98	478.00	43.98	431.28
7093	.13	522.77	470.00	52.77	517.53
7094	.13	524.35	491.00	33.35	327.04
7095	.13	524.32	487.00	37.32	365.95
7097	.13	526.43	501.00	25.43	249.40
7098	1.03	526.20	502.00	24.20	237.34
7099	.13	526.15	497.00	29.15	285.85
7101	1.03	526.17	504.00	22.17	217.39
7102	.13	526.12	485.00	41.12	403.27
7105	.00	527.18	509.00	18.18	178.33
7110	1.60	503.07	460.00	43.07	422.39
7111	1.60	502.20	480.00	22.20	217.67
7112	1.60	494.69	472.00	22.69	222.56
7113	1.60	498.83	472.00	26.83	263.13
7114	1.60	488.10	460.00	28.10	275.56

7115	1.60	484.35	462.00	22.35	219.17
7116	1.60	482.64	457.00	25.64	251.48

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES

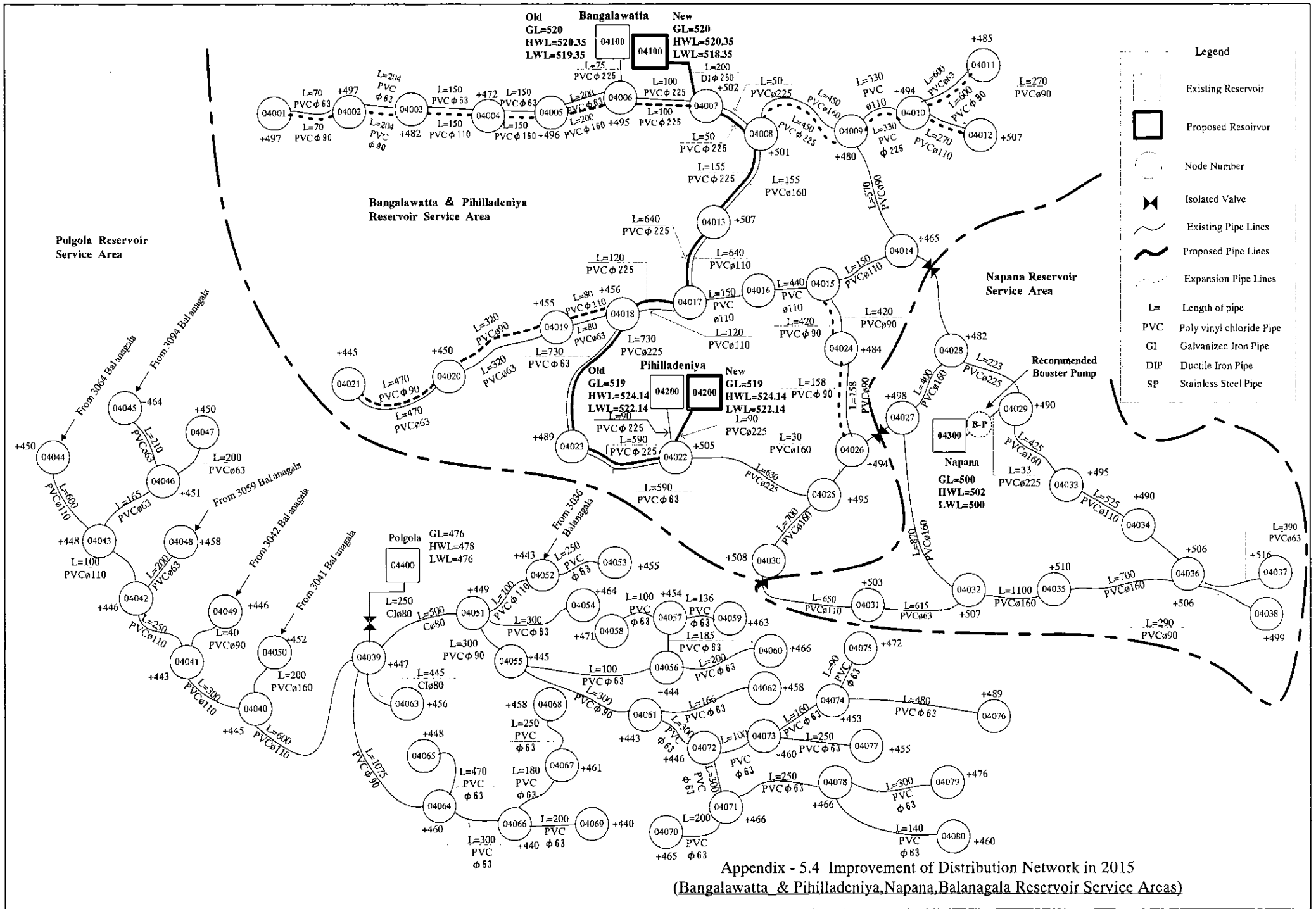
(-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	11.58
49	11.21
83	15.44
99	12.14

NET SYSTEM INFLOW	=	50.38
NET SYSTEM OUTFLOW	=	.00
NET SYSTEM DEMAND	=	50.38

**** KYPIPE SIMULATION COMPLETED ****

DATE: 3/12/2002
TIME: 8:50:25



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* * * * * K Y P I P E 2 * * * * *
* University of Kentucky Hydraulic Analysis Program *
* Distribution of Pressure and Flows in Piping Networks *
* 1000 PIPE VERSION - 1.10 (08/25/92) *
* * * * *

```

DATE: 3/12/2002

TIME: 8:47:44

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INPUT DATA FILENAME ----- c:\D_nets\2015\B&P2015.DAT
TABULATED OUTPUT FILENAME ----- c:\D_nets\2015\B&P2015.OUT
POSTPROCESSOR RESULTS FILENAME --- c:\D_nets\2015\B&P2015.RES

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*****
SUMMARY OF ORIGINAL DATA
*****

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U N I T S S P E C I F I E D

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FLOWRATE ..... = liters/second
HEAD (HGL) ..... = meters
PRESSURE ..... = kpa

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P I P E L I N E D A T A

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STATUS CODE:  XX -CLOSED PIPE      FG -FIXED GRADE NODE      PU -PUMP LINE
                CV -CHECK VALVE   RV -REGULATING VALVE

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PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	LENGTH (m)	DIAMETER (cm)	ROUGHNESS COEFF.	MINOR LOSS COEFF.	FGN-H (m)
1-FGCV	0	4006	75.0	19.8	120.00	.00	519.
2	4006	4005	200.0	5.5	120.00	.00	
3	4006	4007	100.0	19.8	120.00	.00	
4	4005	4004	150.0	5.5	120.00	.00	
5	4004	4003	150.0	5.5	120.00	.00	
6	4003	4002	204.0	5.5	120.00	.00	
7	4002	4001	70.0	5.5	120.00	.00	
8	4007	4008	50.0	19.8	120.00	.00	
9	4008	4013	155.0	14.0	120.00	.00	
10	4008	4009	450.0	14.0	120.00	.00	
11	4009	4010	330.0	9.7	120.00	.00	
12	4009	4014	570.0	7.9	120.00	.00	
13	4010	4011	600.0	5.5	120.00	.00	

14	4010	4012	270.0	7.9	120.00	.00	
15	4014	4015	150.0	9.7	120.00	.00	
16	4015	4016	440.0	9.7	120.00	.00	
17	4015	4024	420.0	7.9	120.00	.00	
18	4016	4017	150.0	9.7	120.00	.00	
19	4017	4013	640.0	9.7	120.00	.00	
20	4017	4018	120.0	9.7	120.00	.00	
21	4018	4019	80.0	5.5	120.00	.00	
22	4018	4023	730.0	5.5	120.00	.00	
23	4019	4020	320.0	5.5	120.00	.00	
24	4020	4021	470.0	5.5	120.00	.00	
25	4022	4023	590.0	5.5	120.00	.00	
26	4022	4025	640.0	19.8	120.00	.00	
27-FG	0	4022	90.0	19.8	120.00	.00	522.
28	4024	4026	158.0	7.9	120.00	.00	
29	4025	4026	30.0	14.0	120.00	.00	
30	4025	4030	700.0	14.0	120.00	.00	
31-XX	4030	4031	650.0	9.7	120.00	.00	
32	4031	4032	615.0	5.5	120.00	.00	
33	4032	4035	1100.0	14.0	120.00	.00	
34	4035	4036	700.0	14.0	120.00	.00	
35	4036	4037	390.0	5.5	120.00	.00	
36	4036	4038	290.0	7.9	120.00	.00	
37-FGCV	0	4007	200.0	25.0	130.00	.00	518.
38	4018	4019	80.0	9.7	130.00	.00	
39	4007	4008	50.0	25.0	130.00	.00	
40	4008	4013	155.0	19.8	130.00	.00	
41	4013	4017	640.0	19.8	130.00	.00	
42	4017	4018	120.0	19.8	130.00	.00	
43-FG	0	4022	90.0	19.8	130.00	.00	522.
44	4022	4023	590.0	19.8	130.00	.00	
45	4023	4018	730.0	19.8	130.00	.00	
46	4008	4009	450.0	19.8	130.00	.00	
47	4009	4010	330.0	14.0	130.00	.00	
48	4010	4012	270.0	9.7	130.00	.00	
49-XX	4015	4024	420.0	7.9	130.00	.00	
50-XX	4024	4026	158.0	7.9	130.00	.00	
51	4031	4032	615.0	7.9	130.00	.00	
52	4006	4005	200.0	14.0	130.00	.00	
53	4005	4004	150.0	14.0	130.00	.00	
54	4004	4003	150.0	9.7	130.00	.00	
55	4003	4002	204.0	7.9	130.00	.00	
56	4002	4001	70.0	7.9	130.00	.00	
57	4010	4011	600.0	9.7	130.00	.00	
58	4019	4020	320.0	7.9	130.00	.00	
59	4020	4021	470.0	7.9	130.00	.00	
60	4006	4007	100.0	19.8	130.00	.00	
61-FG	0	4029	25.0	19.8	120.00	.00	540.
62-XXFG	0	4029	33.0	19.8	120.00	.00	500.
63	4029	4028	223.0	19.8	120.00	.00	
64	4029	4033	425.0	19.8	120.00	.00	
65	4028	4027	400.0	14.0	120.00	.00	
66	4033	4034	525.0	9.7	120.00	.00	

67-XX	4014	4028	300.0	9.7	120.00	.00
68-XX	4026	4027	100.0	9.7	120.00	.00
69	4027	4032	870.0	14.0	120.00	.00
70	4034	4036	490.0	5.5	120.00	.00

JUNCTION NODE DATA

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	JUNCTION ELEVATION (m)	CONNECTING PIPES					
4001		.79	497.00	7	56				
4002		1.84	497.00	6	7	55	56		
4003		1.64	482.00	5	6	54	55		
4004		2.61	472.00	4	5	53	54		
4005		3.51	496.00	2	4	52	53		
4006		3.34	495.00	1	2	3	52	60	
4007		4.59	502.00	3	8	37	39	60	
4008		3.62	501.00	8	9	10	39	40	
4009		4.66	480.00	10	11	12	46	47	
4010		5.51	494.00	11	13	14	47	48	
4011		3.92	485.00	13	57				
4012		2.49	507.00	14	48				
4013		2.22	507.00	9	19	40	41		
4014		6.96	465.00	12	15	67			
4015		1.05	463.00	15	16	17	49		
4016		.89	456.00	16	18				
4017		.61	457.00	18	19	20	41	42	
4018		.55	456.00	20	21	22	38	42	
4019		.35	455.00	21	23	38	58		
4020		.56	450.00	23	24	58	59		
4021		.44	445.00	24	59				
4022		.71	505.00	25	26	27	43	44	
4023		.34	489.00	22	25	44	45		
4024		.13	484.00	17	28	49	50		
4025		.15	495.00	26	29	30			
4026		.16	494.00	28	29	50	68		
4027		.52	498.00	65	68	69			
4028		1.31	482.00	63	65	67			
4029		1.51	490.00	61	62	63	64		
4030		.37	503.00	30	31				
4031		1.61	493.00	31	32	51			
4032		3.01	507.00	32	33	51	69		
4033		1.13	495.00	64	66				
4034		1.13	490.00	66	70				
4035		1.32	510.00	33	34				
4036		.02	506.00	34	35	36	70		

4037	.01	516.00	35
4038	.01	499.00	36

O U T P U T O P T I O N D A T A

OUTPUT SELECTION: ALL RESULTS ARE INCLUDED IN THE TABULATED OUTPUT

S Y S T E M C O N F I G U R A T I O N

NUMBER OF PIPES	(p) =	70
NUMBER OF JUNCTION NODES	(j) =	38
NUMBER OF PRIMARY LOOPS	(l) =	27
NUMBER OF FIXED GRADE NODES	(f) =	6
NUMBER OF SUPPLY ZONES	(z) =	1

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 7 TRIALS WITH AN ACCURACY = .00159

P I P E L I N E R E S U L T S

STATUS CODE:	XX -CLOSED PIPE	FG -FIXED GRADE NODE	PU -PUMP LINE
	CV -CHECK VALVE	RV -REGULATING VALVE	TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1	NODE NOS. #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-FGCV	0	4006	30.86	.48	.00	.00	1.00	6.3
2	4006	4005	.76	.69	.00	.00	.32	3.4
3	4006	4007	8.22	.06	.00	.00	.27	.5
4	4005	4004	.50	.24	.00	.00	.21	1.6
5	4004	4003	.73	.48	.00	.00	.31	3.2
6	4003	4002	.69	.59	.00	.00	.29	2.8
7	4002	4001	.21	.02	.00	.00	.09	.3
8	4007	4008	4.18	.01	.00	.00	.14	.1
9	4008	4013	-2.60	.05	.00	.00	.17	.3
10	4008	4009	5.01	.54	.00	.00	.33	1.1
11	4009	4010	3.10	.97	.00	.00	.42	2.9
12	4009	4014	1.94	1.91	.00	.00	.40	3.3
13	4010	4011	.67	1.65	.00	.00	.28	2.7
14	4010	4012	.87	.20	.00	.00	.18	.7
15	4014	4015	-5.02	1.07	.00	.00	.68	7.1

16	4015	4016	-3.01	1.22	.00	.00	.41	2.7
17	4015	4024	-3.06	3.26	.00	.00	.62	7.7
18	4016	4017	-3.90	.67	.00	.00	.53	4.4
19	4017	4013	1.46	.47	.00	.00	.20	.7
20	4017	4018	-2.03	.16	.00	.00	.27	1.3
21	4018	4019	.23	.03	.00	.00	.10	.3
22	4018	4023	-.56	1.43	.00	.00	.24	1.9
23	4019	4020	.26	.15	.00	.00	.11	.4
24	4020	4021	.12	.05	.00	.00	.05	.1
25	4022	4023	.57	1.20	.00	.00	.24	2.0
26	4022	4025	3.87	.09	.00	.00	.13	.1
27-FG	0	4022	11.11	.09	.00	.00	.36	.9
28	4024	4026	-3.19	1.32	.00	.00	.65	8.3
29	4025	4026	3.35	.02	.00	.00	.22	.5
30	4025	4030	.37	.01	.00	.00	.02	.0
31-XX	4030	4031						
32	4031	4032	-.42	.71	.00	.00	.18	1.1
33	4032	4035	.70	.03	.00	.00	.05	.0
34	4035	4036	-.62	.02	.00	.00	.04	.0
35	4036	4037	.01	.00	.00	.00	.00	.0
36	4036	4038	.01	.00	.00	.00	.00	.0
37-XXFG	0	4007						
38	4018	4019	1.12	.03	.00	.00	.15	.3
39	4007	4008	8.36	.01	.00	.00	.17	.1
40	4008	4013	-7.01	.05	.00	.00	.23	.3
41	4013	4017	-10.36	.47	.00	.00	.34	.7
42	4017	4018	-14.31	.16	.00	.00	.46	1.3
43-FG	0	4022	12.04	.09	.00	.00	.39	.9
44	4022	4023	18.00	1.20	.00	.00	.58	2.0
45	4023	4018	17.68	1.43	.00	.00	.57	1.9
46	4008	4009	13.51	.54	.00	.00	.44	1.1
47	4009	4010	8.82	.97	.00	.00	.57	2.9
48	4010	4012	1.62	.20	.00	.00	.22	.7
49-XX	4015	4024						
50-XX	4024	4026						
51	4031	4032	-1.19	.71	.00	.00	.24	1.1
52	4006	4005	9.63	.69	.00	.00	.63	3.4
53	4005	4004	6.38	.24	.00	.00	.41	1.6
54	4004	4003	3.54	.48	.00	.00	.48	3.2
55	4003	4002	1.94	.59	.00	.00	.40	2.8
56	4002	4001	.58	.02	.00	.00	.12	.3
57	4010	4011	3.25	1.65	.00	.00	.44	2.7
58	4019	4020	.74	.15	.00	.00	.15	.4
59	4020	4021	.32	.05	.00	.00	.07	.1
60	4006	4007	8.91	.06	.00	.00	.29	.5
61-FG	0	4029	11.58	.03	.00	.00	.38	1.0
62-XXFG	0	4029						
63	4029	4028	7.15	.09	.00	.00	.23	.4
64	4029	4033	2.92	.03	.00	.00	.09	.0
65	4028	4027	5.84	.63	.00	.00	.38	1.5
66	4033	4034	1.79	.56	.00	.00	.24	1.0
67-XX	4014	4028						
68-XX	4026	4027						

69	4027	4032	5.32	1.16	.00	.00	.35	1.3
70	4034	4036	.66	1.31	.00	.00	.28	2.6

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
4001		.79	516.78	497.00	19.78	193.94
4002		1.84	516.80	497.00	19.80	194.16
4003		1.64	517.39	482.00	35.39	347.02
4004		2.61	517.87	472.00	45.87	449.82
4005		3.51	518.11	496.00	22.11	216.83
4006		3.34	518.80	495.00	23.80	233.40
4007		4.59	518.75	502.00	16.75	164.22
4008		3.62	518.74	501.00	17.74	173.95
4009		4.66	518.20	480.00	38.20	374.62
4010		5.51	517.23	494.00	23.23	227.83
4011		3.92	515.58	485.00	30.58	299.91
4012		2.49	517.03	507.00	10.03	98.34
4013		2.22	518.79	507.00	11.79	115.64
4014		6.96	516.29	465.00	51.29	503.02
4015		1.05	517.37	463.00	54.37	533.15
4016		.89	518.59	456.00	62.59	613.76
4017		.61	519.26	457.00	62.26	610.55
4018		.55	519.42	456.00	63.42	621.93
4019		.35	519.39	455.00	64.39	631.44
4020		.56	519.23	450.00	69.23	678.97
4021		.44	519.19	445.00	74.19	727.52
4022		.71	522.05	505.00	17.05	167.24
4023		.34	520.85	489.00	31.85	312.38
4024		.13	520.62	484.00	36.62	359.17
4025		.15	521.97	495.00	26.97	264.44
4026		.16	521.95	494.00	27.95	274.08
4027		.52	539.25	498.00	41.25	404.48
4028		1.31	539.88	482.00	57.88	567.60
4029		1.51	539.97	490.00	49.97	490.08
4030		.37	521.96	503.00	18.96	185.93
4031		1.61	537.37	493.00	44.37	435.16
4032		3.01	538.09	507.00	31.09	304.86
4033		1.13	539.94	495.00	44.94	440.71
4034		1.13	539.38	490.00	49.38	484.27
4035		1.32	538.05	510.00	28.05	275.11
4036		.02	538.07	506.00	32.07	314.51
4037		.01	538.07	516.00	22.07	216.44
4038		.01	538.07	499.00	39.07	383.15

SUMMARY OF INFLOWS AND OUTFLOWS

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES
 (-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
1	30.86
27	11.11
43	12.04
61	11.58

NET SYSTEM INFLOW	=	65.59
NET SYSTEM OUTFLOW	=	.00
NET SYSTEM DEMAND	=	65.59

D A T A C H A N G E S F O R N E X T S I M U L A T I O N

D E M A N D C H A N G E S

DEMAND TYPE = 1 - GDF = .300

 S I M U L A T I O N R E S U L T S

THE RESULTS ARE OBTAINED AFTER 3 TRIALS WITH AN ACCURACY = .00408

P I P E L I N E R E S U L T S

STATUS CODE: XX -CLOSED PIPE FG -FIXED GRADE NODE PU -PUMP LINE
 CV -CHECK VALVE RV -REGULATING VALVE TK -STORAGE TANK

PIPE NUMBER	NODE NOS. #1 #2	FLOWRATE (l/s)	HEAD LOSS (m)	PUMP HEAD (m)	MINOR LOSS (m)	LINE VELO. (m/s)	HL/ 1000 (m/m)
1-XXFG	0 4006						
2	4006 4005	.23	.07	.00	.00	.10	.3
3	4006 4007	-1.98	.00	.00	.00	.06	.0
4	4005 4004	.15	.03	.00	.00	.06	.1
5	4004 4003	.22	.05	.00	.00	.09	.3
6	4003 4002	.21	.06	.00	.00	.09	.3
7	4002 4001	.06	.00	.00	.00	.03	.0
8	4007 4008	-1.83	.00	.00	.00	.06	.0
9	4008 4013	-3.02	.07	.00	.00	.20	.4

10	4008	4009	1.24	.04	.00	.00	.08	.0
11	4009	4010	.93	.10	.00	.00	.13	.3
12	4009	4014	-.38	.09	.00	.00	.08	.1
13	4010	4011	.20	.18	.00	.00	.09	.3
14	4010	4012	.26	.02	.00	.00	.05	.0
15	4014	4015	-2.47	.29	.00	.00	.33	1.9
16	4015	4016	-.91	.13	.00	.00	.12	.3
17	4015	4024	-1.87	1.31	.00	.00	.38	3.1
18	4016	4017	-1.18	.07	.00	.00	.16	.4
19	4017	4013	1.47	.47	.00	.00	.20	.7
20	4017	4018	-1.64	.11	.00	.00	.22	.9
21	4018	4019	.07	.00	.00	.00	.03	.0
22	4018	4023	-.42	.85	.00	.00	.18	1.1
23	4019	4020	.08	.02	.00	.00	.03	.0
24	4020	4021	.03	.01	.00	.00	.01	.0
25	4022	4023	.43	.70	.00	.00	.18	1.1
26	4022	4025	2.12	.03	.00	.00	.07	.0
27-FG	0	4022	7.78	.04	.00	.00	.25	.5
28	4024	4026	-1.91	.51	.00	.00	.39	3.2
29	4025	4026	1.96	.01	.00	.00	.13	.2
30	4025	4030	.11	.00	.00	.00	.01	.0
31-XX	4030	4031						
32	4031	4032	-.13	.08	.00	.00	.05	.1
33	4032	4035	.21	.00	.00	.00	.01	.0
34	4035	4036	-.19	.00	.00	.00	.01	.0
35	4036	4037	.00	.00	.00	.00	.00	.0
36	4036	4038	.00	.00	.00	.00	.00	.0
37-XXFG	0	4007						
38	4018	4019	.34	.00	.00	.00	.05	.0
39	4007	4008	-3.66	.00	.00	.00	.07	.0
40	4008	4013	-8.15	.07	.00	.00	.26	.4
41	4013	4017	-10.38	.47	.00	.00	.34	.7
42	4017	4018	-11.57	.11	.00	.00	.38	.9
43-FG	0	4022	8.43	.04	.00	.00	.27	.5
44	4022	4023	13.45	.70	.00	.00	.44	1.1
45	4023	4018	13.35	.85	.00	.00	.43	1.1
46	4008	4009	3.35	.04	.00	.00	.11	.0
47	4009	4010	2.65	.10	.00	.00	.17	.3
48	4010	4012	.49	.02	.00	.00	.07	.0
49-XX	4015	4024						
50-XX	4024	4026						
51	4031	4032	-.36	.08	.00	.00	.07	.1
52	4006	4005	2.89	.07	.00	.00	.19	.3
53	4005	4004	1.91	.03	.00	.00	.12	.1
54	4004	4003	1.06	.05	.00	.00	.14	.3
55	4003	4002	.58	.06	.00	.00	.12	.3
56	4002	4001	.17	.00	.00	.00	.04	.0
57	4010	4011	.97	.18	.00	.00	.13	.3
58	4019	4020	.22	.02	.00	.00	.05	.0
59	4020	4021	.10	.01	.00	.00	.02	.0
60	4006	4007	-2.14	.00	.00	.00	.07	.0
61-FG	0	4029	3.47	.00	.00	.00	.11	.1
62-XXFG	0	4029						

63	4029	4028	2.14	.01	.00	.00	.07	.0
64	4029	4033	.88	.00	.00	.00	.03	.0
65	4028	4027	1.75	.07	.00	.00	.11	.1
66	4033	4034	.54	.06	.00	.00	.07	.1
67-XX	4014	4028						
68-XX	4026	4027						
69	4027	4032	1.59	.12	.00	.00	.10	.1
70	4034	4036	.20	.14	.00	.00	.08	.2

JUNCTION NODE RESULTS

JUNCTION NUMBER	JUNCTION TITLE	EXTERNAL DEMAND (l/s)	HYDRAULIC GRADE (m)	JUNCTION ELEVATION (m)	PRESSURE HEAD (m)	JUNCTIO PRESSUR (kpa)
4001		.24	519.67	497.00	22.67	222.33
4002		.55	519.67	497.00	22.67	222.36
4003		.49	519.74	482.00	37.74	370.08
4004		.78	519.79	472.00	47.79	468.65
4005		1.05	519.82	496.00	23.82	233.55
4006		1.00	519.89	495.00	24.89	244.08
4007		1.38	519.89	502.00	17.89	175.47
4008		1.09	519.89	501.00	18.89	185.30
4009		1.40	519.85	480.00	39.85	390.84
4010		1.65	519.75	494.00	25.75	252.52
4011		1.18	519.57	485.00	34.57	339.04
4012		.75	519.73	507.00	12.73	124.82
4013		.67	519.97	507.00	12.97	127.17
4014		2.09	519.94	465.00	54.94	538.82
4015		.31	520.23	463.00	57.23	561.25
4016		.27	520.36	456.00	64.36	631.19
4017		.18	520.44	457.00	63.44	622.10
4018		.17	520.54	456.00	64.54	632.96
4019		.10	520.54	455.00	65.54	642.74
4020		.17	520.52	450.00	70.52	691.61
4021		.13	520.52	445.00	75.52	740.59
4022		.21	522.10	505.00	17.10	167.65
4023		.10	521.40	489.00	32.40	317.70
4024		.04	521.55	484.00	37.55	368.21
4025		.05	522.07	495.00	27.07	265.43
4026		.05	522.06	494.00	28.06	275.18
4027		.16	539.92	498.00	41.92	411.09
4028		.39	539.99	482.00	57.99	568.66
4029		.45	540.00	490.00	50.00	490.31
4030		.11	522.07	503.00	19.07	186.97
4031		.48	539.72	493.00	46.72	458.14
4032		.90	539.79	507.00	32.79	321.60
4033		.34	539.99	495.00	44.99	441.24
4034		.34	539.93	490.00	49.93	489.68
4035		.40	539.79	510.00	29.79	292.15
4036		.01	539.79	506.00	33.79	331.39

4037	.00	539.79	516.00	23.79	233.33
4038	.00	539.79	499.00	40.79	400.04

S U M M A R Y O F I N F L O W S A N D O U T F L O W S

(+) INFLOWS INTO THE SYSTEM FROM FIXED GRADE NODES

(-) OUTFLOWS FROM THE SYSTEM INTO FIXED GRADE NODES

PIPE NUMBER	FLOWRATE (l/s)
-----	-----
27	7.78
43	8.43
61	3.47

NET SYSTEM INFLOW	=	19.68
NET SYSTEM OUTFLOW	=	.00
NET SYSTEM DEMAND	=	19.68

**** KYPIPE SIMULATION COMPLETED ****

DATE: 3/12/2002

TIME: 8:47:44

05 Mechanical Design Calculations

Pump List

Location	NO.	Direction	Phase (Year)	Pump Capacity		Required Head (m)	Total Head (m)	Number of Units		Pump	Control
				(m ³ /day)	(m ³ /min)			Duty	Standby		
Gohagoda Intake		To WTP	2005	38,500	26.74	40.5	44.0	1	1	C	A
			2010	77,000	53.47	39.4	43.0	2	1		
			2015	115,500	80.21	40.6	44.0	3	1		
Katugastota W.T.P.	A-1	To Upland, Asgiriya SR	2005	17,600	12.22	130.5	134.0	1	1	C	B
			2010	33,190	23.05	135.2	136.0	2	1		
			2015	51,110	35.49	135.6	137.0	3	1		
	A-2	To Gphagoda SR	2005	4,710	3.27	103.9		1	1	B	B
			2010	4,990	3.47	104.3		1	1		
			2015	5,870	4.08	101.7	104.0	1	1		
	A-3	To Kahawatta SR & other SRs	2005	14,390	9.99	90.9	93.0	1	1	C	B
			2010	29,160	20.25	96.4	99.0	2	1		
			2015	44,240	30.72	99.5	102.0	3	1		
Heerasagala Low SR	B	To Heerasagala Middle SR	2005	1,650	1.15	59.0		1	1	A	B
			2010	2,350	1.63	61.8		1	1		
			2015	2,740	1.90	65.8	68.0	1	1		
Heerasagala Middle SR	C	To Heerasagala Upper SR	2005	280	0.19	54.5		1	1	A	B
			2010	550	0.38	71.7		1	1		
			2015	700	0.49	72.6	77.0	1	1		
Ampitiya SR (existing)	D-1	To Elhena SR	2005	400	0.28	38.1		1	1	A	B
			2010	570	0.40	38.7		1	1		
			2015	1,200	0.83	42.1	45.0	1	1		
	D-2	To Mullepihilla SR	2005	580	0.40	138.6		1	1	B	B
			2010	810	0.56	141.3		1	1		
			2015	980	0.68	143.7	146.0	1	1		
	D-3	To Meekanuwa SR	2005	1250	0.87	74.1		1	1	A	B
			2010	1770	1.23	66.2		1	1		
			2015	2150	1.49	70.0	73.0	1	1		
Kahawatta SR	E	To Kurugoda SR and Telambugahawatta SR	2005	4,240	2.94	62.4	65.0	1	1	A	B
			2010	4,330	3.01	62.5		2	1		
			2015	7,310	5.08	70.0	73.0	2	1		
R2 SR (existing)	F	To Hantana Place SR	2005	1,050	0.73	97.3		1	1	A	B
			2010	1,490	1.03	98.0		1	1		
			2015	1,960	1.36	99.0	102.0	1	1		
Asgiriya SR	G	In-line pump to Bahirawakanda SR	2005	1,970	1.37	86.5		1	1	A	B
			2010	2,150	1.49	86.9		1	1		
			2015	2,280	1.58	87.2	88.0	1	1		
Kondadeniya (existing)	H	To Kulugamana SR	2005	1,050	0.73	67.2		1	1	A	B
			2010	1,100	0.76	68.1		1	1		
			2015	1,600	1.11	59.9	64.0	1	1		

Pump Type : A End Suction Volute Pump
 B Multi-Stage Volute Pump
 C Double Suction Volute Pump

Control Type : A Pump Speed Control Operation with Flowmeter/Pressure Sensor
 B Pump On-Off Operation with Flowmeter

1-1. Intake (Stage 1)

Total Capacity	38,500 m ³ /day =	26.74 m ³ /min
Quantity of pump	1 sets + 1 set for stand-by	
Pump Capacity	38,500 m ³ /day	
	Q=	26.74 m ³ /min 1,604.2 m ³ /hr
	q=	0.446 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	616 mm to 436 mm
	=	400 x 300 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ =	42.5
		= 44.0 m

actual head :

$$h_1 = h_d - h_s = 38.33 \text{ m}$$

$$\text{suction level } h_s = 436.67 \text{ m}$$

$$\text{delivery level } h_d = 475.00 \text{ m}$$

friction loss : pipeline (Hazen Williams)

$$h_2 = 10.666 \times c^{(-1.85)} \times D^{(-4.87)} \times q^{(1.85)} \times L = 2.13 \text{ m}$$

$$\text{where, } c = 110$$

$$D = 800 \text{ mm dia / 1000}$$

$$L = 1,800 \text{ m}$$

$$(v = 0.886 \text{ m/sec})$$

friction loss : fittings around pump

$$h_3 = f_1 \times (v_1^2 / 2g) + f_2 \times (v_2^2 / 2g)$$

$$= 0.05 \text{ m} + 1.98 \text{ m}$$

$$= 2.03 \text{ m}$$

$$\text{where, } D = 500 \text{ mm dia / 1000}$$

$$(v_1 = 2.269 \text{ m/sec})$$

<u>f1</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
bell mouth	1	0.06	0.06
sluice valve	1	0.10	0.10
deducer	1	0.04	0.04
		f ₁ total	0.20

$$\text{where, } D = 400 \text{ mm dia / 1000}$$

$$(v_2 = 3.546 \text{ m/sec})$$

<u>f2</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
check valve	1	1.50	1.50
sluice valve	1	0.10	0.10
increase	1	0.15	0.15
90deg	1	0.18	0.18
tee	1	1.15	1.15
		f ₂ total	3.08

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)
	= 265.7
	= 280.0 kW
	where, r = 1.00
	e = 0.83
	a = 0.15

Specification

Type	Vertical Double-Suction Centrifugal Pump
Diameter	400 x 300 mm
Capacity	26.74 m ³ /min
Head	44.0 m
Motor Output	280 kW
Quantity	2 (1) sets including 1 set for future

1-3. Intake (Stage 3)

Total Capacity	115,500 m ³ /day =	80.21 m ³ /min
Quantity of pump	3 sets + 1 set for stand-by	
Pump Capacity	38,500 m ³ /day	
	Q=	26.74 m ³ /min 1,604.2 m ³ /hr
	q=	0.446 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	616 mm to 436 mm
	=	400 x 300 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ =	42.6
		= 44.0 m

actual head :

$$h_1 = h_d - h_s = 38.33 \text{ m}$$

$$\text{suction level } h_s = 436.67 \text{ m}$$

$$\text{delivery level } h_d = 475.00 \text{ m}$$

friction loss : pipeline (Hazen Williams)

$$h_2 = 10.666 \times c^{(-1.85)} \times D^{(-4.87)} \times q^{(1.85)} \times L = 2.22 \text{ m}$$

$$\text{where, } c = 110$$

$$D = 1,204 \text{ mm dia /1000}$$

$$L = 1,800 \text{ m}$$

$$(v = 1.174 \text{ m/sec})$$

friction loss : fittings around pump

$$h_3 = f_1 \times (v_1^2 / 2g) + f_2 \times (v_2^2 / 2g)$$

$$= 0.05 \text{ m} + 1.98 \text{ m}$$

$$= 2.03 \text{ m}$$

$$\text{where, } D = 500 \text{ mm dia /1000}$$

$$(v_1 = 2.269 \text{ m/sec})$$

<u>f1</u>	<u>Qty</u>	<u>f/pc</u>	<u>f</u>
bell mouth	1	0.06	0.06
sluice valve	1	0.10	0.10
deducer	1	0.04	0.04
		f ₁ total	0.20

$$\text{where, } D = 400 \text{ mm dia /1000}$$

$$(v_2 = 3.546 \text{ m/sec})$$

<u>f2</u>	<u>Qty</u>	<u>f/pc</u>	<u>f</u>
check valve	1	1.50	1.50
sluice valve	1	0.10	0.10
increase	1	0.15	0.15
90deg	1	0.18	0.18
tee	1	1.15	1.15
		f ₂ total	3.08

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)
	= 265.7
	= 280.0 kW
	where, r = 1.00
	e = 0.83
	a = 0.15

Specification

Type	Vertical Double-Suction Centrifugal Pump
Diameter	400 x 300 mm
Capacity	26.74 m ³ /min
Head	44.0 m
Motor Output	280 kW
Quantity	4 (1) sets including 1 set for future

2-1. Clear Water Pump (A-1) - Phase 1

Total Capacity	20,360 m ³ /day =	14.14 m ³ /min
Quantity of pump	1 sets + 1 set for stand-by	
Pump Capacity	20,360 m ³ /day	
	Q=	14.14 m ³ /min 848.3 m ³ /hr
	q=	0.236 m ³ /sec

Diameter	Diameter = $146 \times (Q / v)^{(1/2)}$	
	=	448 mm to 317 mm
	=	300 x 200 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	132.0
		= 134.0 m

actual head : Asgiriya
h₁ = hd - hs = 124.39 m

suction header pipe hs = 442.61 m
delivery level hd = 567.00 m

friction loss : pipeline (Hazen Williams)
h₂ = $10.666 \times c^{(-1.85)} \times D^{(-4.87)} \times q^{(1.85)} \times L =$ 0.91 m

friction loss : fittings around pump
h₃ = f₁ x (v₁² / 2g) + f₂ x (v₂² / 2g)
= 0.02 m + 1.71 m
= 1.73 m

where, D= 400 mm dia /1000
(v₁ = 1.875 m/sec)

<u>f1</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
sluice valve	1	0.10	0.10
reducer	1	<u>0.03</u>	<u>0.03</u>
		f ₁ total	0.13

where, D= 300 mm dia /1000
(v₂ = 3.334 m/sec)

<u>f2</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
increase	1	0.48	0.48
check valve	1	1.00	1.00
butterfly valve	1	0.20	0.20
90deg	1	0.18	0.18
tee	1	<u>1.15</u>	<u>1.15</u>
		f ₂ total	3.01

friction loss : float type butterfly valve
h₄ = 5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)
	= 433.1 kW
	= 450.0 kW
	where, r = 1.00
	e = 0.82
	a = 0.15

Specification	
Type	Horizontal Double-Suction Centrifugal Pump
Diameter	300 x 200 mm
Capacity	14.14 m ³ /min
Head	134.0 m
Motor Output	450 kW
Quantity	2 (1) sets including 1 set for future

2-2. Clear Water Pump (A-1) - Phase 2

Total Capacity	36,040 m ³ /day =	25.03 m ³ /min
Quantity of pump	2 sets + 1 set for stand-by	
Pump Capacity	18,020 m ³ /day	
	Q=	12.51 m ³ /min 750.8 m ³ /hr
	q=	0.209 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)		
	=	422 mm	to 298 mm
	=	300 x 200 mm	
	where, v=	1.5	to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	134.1
		= 136.0 m

actual head : Asgiriya

$$h_1 = h_d - h_s = 124.39 \text{ m}$$

$$\text{suction header pipe } h_s = 442.61 \text{ m}$$

$$\text{delivery level } h_d = 567.00 \text{ m}$$

friction loss : pipeline (Hazen Williams)

$$h_2 = 10.666 \times c^{(-1.85)} \times D^{(-4.87)} \times q^{(1.85)} \times L = 3.31 \text{ m}$$

friction loss : fittings around pump

$$h_3 = f_1 \times (v_1^2 / 2g) + f_2 \times (v_2^2 / 2g)$$

$$= 0.02 \text{ m} + 1.34 \text{ m}$$

$$= 1.36 \text{ m}$$

$$\text{where, } D = 400 \text{ mm dia / 1000}$$

$$(v_1 = 1.660 \text{ m/sec})$$

<u>f_l</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
sluice valve	1	0.10	0.10
reducer	1	<u>0.03</u>	<u>0.03</u>
		<u>f₁ total</u>	<u>0.13</u>

$$\text{where, } D = 300 \text{ mm dia / 1000}$$

$$(v_2 = 2.951 \text{ m/sec})$$

<u>f₂</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
increase	1	0.48	0.48
check valve	1	1.00	1.00
butterfly valve	1	0.20	0.20
90deg	1	0.18	0.18
tee	1	<u>1.15</u>	<u>1.15</u>
		<u>f₂ total</u>	<u>3.01</u>

friction loss : float type butterfly valve

$$h_4 = 5.00 \text{ m}$$

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)
	= 389 kW
	= 400.0 kW
	where, r = 1.00
	e = 0.82
	a = 0.15

Specification

Type	Horizontal Double-Suction Centrifugal Pump
Diameter	300 x 200 mm
Capacity	12.51 m ³ /min
Head	136.0 m
Motor Output	400 kW
Quantity	3 (1) sets including 1 set for future

2-3 Clear Water Pump (A-1) - Phase 3

Total Capacity	54,160 m ³ /day =	37.61 m ³ /min
Quantity of pump	3 sets + 1 set for stand-by	
Pump Capacity	18,053 m ³ /day	
	Q=	12.54 m ³ /min 752.2 m ³ /hr
	q=	0.209 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	422 mm to 298 mm
	=	300 x 200 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	135.2
		= 137.0 m

actual head : Asgiriya
h₁ = hd - hs = 124.39 m

suction header pipe hs = 442.61 m
delivery level hd = 567.00 m

friction loss : pipeline (Hazen Williams)
h₂ = 10.666 x c^(-1.85) x D^(-4.87) x q^(1.85) x L = 4.41 m

friction loss : fittings around pump
h₃ = f₁ x (v₁² / 2g) + f₂ x (v₂² / 2g)
= 0.02 m + 1.34 m
= 1.36 m

where, D= 400 mm dia /1000
(v₁ = 1.663 m/sec)

<u>f1</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
sluice valve	1	0.10	0.10
reducer	1	<u>0.03</u>	<u>0.03</u>
		f ₁ total	0.13

where, D= 300 mm dia /1000
(v₂ = 2.956 m/sec)

<u>f2</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
increase	1	0.48	0.48
check valve	1	1.00	1.00
butterfly valve	1	0.20	0.20
90deg	1	0.18	0.18
tee	1	<u>1.15</u>	<u>1.15</u>
		f ₂ total	3.01

friction loss : float type butterfly valve
h₄ = 5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)
	= 392.6 kW
	= 400.0 kW
	where, r = 1.00
	e = 0.82
	a = 0.15

Specification	
Type	Horizontal Double-Suction Centrifugal Pump
Diameter	300 x 200 mm
Capacity	12.54 m ³ /min
Head	137.0 m
Motor Output	400 kW
Quantity	4 (1) sets including 1 set for future

3-1. Clear Water Pump (A-2) - Phase 3

Total Capacity	2,820 m ³ /day =	1.96 m ³ /min
Quantity of pump	1 sets + 1 set for stand-by	
Pump Capacity	2,820 m ³ /day	
	Q=	1.96 m ³ /min 117.5 m ³ /hr
	q=	0.033 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	167 mm to 118 mm
	=	125 x 125 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	102.4 m
	=	104.0 m
	actual head : Asgiriya	
	h ₁ = hd - hs =	87.40 m
	suction header pipe hs =	442.60 m
	delivery level hd =	530.00 m
	friction loss : pipeline (Hazen Williams)	
	h ₂ = 10.666 x c ^(-1.85) x D ^(-4.87) x q ^(1.85) x L =	9.30 m
	friction loss : fittings around pump	
	h ₃ = f ₁ x (v ₁ ² / 2g) + f ₂ x (v ₂ ² / 2g)	
	=	0.22 m + 0.52 m
	=	0.74 m
	where, D=	150 mm dia /1000
	(v ₁ =	1.847 m/sec)
	<u>f1</u>	<u>Q'ty</u> <u>f/pc</u> <u>f</u>
	sluice valve	1 0.10 0.10
	tee	1 1.15 1.15
	reducer	1 <u>0.03</u> <u>0.03</u>
		f ₁ total 1.28
	where, D=	150 mm dia /1000
	(v ₂ =	1.847 m/sec)
	<u>f2</u>	<u>Q'ty</u> <u>f/pc</u> <u>f</u>
	increase	1 0.48 0.48
	check valve	1 1.00 1.00
	butterfly valve	1 0.20 0.20
	90deg	1 0.18 0.18
	tee	1 <u>1.15</u> <u>1.15</u>
		f ₂ total 3.01

friction loss : float type butterfly valve
h₄ = 5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)
	= 54.5 kW
	= 55.0 kW
	where, r = 1.00
	e = 0.70
	a = 0.15

Specification	
Type	Horizontal Multi-turbine Pump
Diameter	125 x 125 mm
Capacity	1.96 m ³ /min
Head	104.0 m
Motor Output	55 kW
Quantity	2 (1) sets including 1 set for stand-by

4-1. Clear Water Pump (A-3) - Phase 1

Total Capacity	14,390 m ³ /day =	9.99 m ³ /min
Quantity of pump	1 sets + 1 set for stand-by	
Pump Capacity	14,390 m ³ /day	
	Q=	9.99 m ³ /min 599.6 m ³ /hr
	q=	0.167 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	377 mm to 266 mm
	=	300 x 200 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	91.7
		= 93.0 m

actual head : Asgiriya
h₁ = hd - hs = 78.67 m

suction header pipe hs = 442.61 m
delivery level hd = 521.28 m

friction loss : pipeline (Hazen Williams)
h₂ = 10.666 x c^(-1.85) x D^(-4.87) x q^(1.85) x L = 7.13 m

friction loss : fittings around pump
h₃ = f₁ x (v₁² / 2g) + f₂ x (v₂² / 2g)
= 0.01 m + 0.85 m
= 0.86 m

where, D= 400 mm dia /1000
(v₁ = 1.325 m/sec)

<u>f1</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
sluice valve	1	0.10	0.10
reducer	1	<u>0.03</u>	<u>0.03</u>
		f ₁ total	0.13

where, D= 300 mm dia /1000
(v₂ = 2.356 m/sec)

<u>f2</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
increase	1	0.48	0.48
check valve	1	1.00	1.00
butterfly valve	1	0.20	0.20
90deg	1	0.18	0.18
tee	1	<u>1.15</u>	<u>1.15</u>
		f ₂ total	3.01

friction loss : float type butterfly valve
h₄ = 5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)
	= 212.4 kW
	= 250.0 kW
	where, r = 1.00
	e = 0.82
	a = 0.15

Specification	
Type	Horizontal Double-Suction Centrifugal Pump
Diameter	300 x 200 mm
Capacity	9.99 m ³ /min
Head	93.0 m
Motor Output	250 kW
Quantity	2 (1) sets including 1 set for future

4-2. Clear Water Pump (A-3) - Phase 2

Total Capacity	29,160 m ³ /day =	20.25 m ³ /min
Quantity of pump	2 sets + 1 set for stand-by	
Pump Capacity	14,580 m ³ /day	
	Q=	10.13 m ³ /min 607.5 m ³ /hr
	q=	0.169 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)		
	=	379 mm	to 268 mm
	=	300 x 200 mm	
	where, v=	1.5	to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =		
		97.2	
		=	99.0 m
	actual head :	Asgiriya	
	h ₁ = hd - hs =		78.67 m
		suction header pipe hs =	442.61 m
		delivery level hd =	521.28 m
	friction loss : pipeline (Hazen Williams)		
	h ₂ = 10.666 x c ^(-1.85) x D ^(-4.87) x q ^(1.85) x L =		12.63 m
	friction loss : fittings around pump		
	h ₃ = f ₁ x (v ₁ ² / 2g) + f ₂ x (v ₂ ² / 2g)		
	=	0.01 m +	0.88 m
	=	0.89 m	
	where, D=	400 mm dia /1000	
	(v ₁ =	1.343 m/sec)	
	<u>f1</u>	<u>Q'ty</u>	<u>f/pc</u>
	sluice valve	1	0.10
	reducer	1	<u>0.03</u>
			<u>0.03</u>
		f ₁ total	0.13
	where, D=	300 mm dia /1000	
	(v ₂ =	2.387 m/sec)	
	<u>f2</u>	<u>Q'ty</u>	<u>f/pc</u>
	increase	1	0.48
	check valve	1	1.00
	butterfly valve	1	0.20
	90deg	1	0.18
	tee	1	<u>1.15</u>
		f ₂ total	3.01

friction loss : float type butterfly valve
h₄ = 5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)		
	=	229.1 kW	
	=	250.0 kW	
	where, r =	1.00	
	e =	0.82	
	a =	0.15	

Specification	
Type	Horizontal Double-Suction Centrifugal Pump
Diameter	300 x 200 mm
Capacity	10.13 m ³ /min
Head	99.0 m
Motor Output	250 kW
Quantity	3 (1) sets including 1 set for future

4-3. Clear Water Pump (A-3) - Phase 3

Total Capacity	44,240 m ³ /day =	30.72 m ³ /min
Quantity of pump	3 sets + 1 set for stand-by	
Pump Capacity	14,747 m ³ /day	
	Q=	10.24 m ³ /min 614.4 m ³ /hr
	q=	0.171 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	381 mm to 270 mm
	=	300 x 200 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	100.2
		= 102.0 m

actual head : Asgiriya
h₁ = hd - hs = 78.67 m

suction header pipe hs = 442.61 m
delivery level hd = 521.28 m

friction loss : pipeline (Hazen Williams)
h₂ = 10.666 x c^(-1.85) x D^(-4.87) x q^(1.85) x L = 15.63 m

friction loss : fittings around pump
h₃ = f₁ x (v₁² / 2g) + f₂ x (v₂² / 2g)
= 0.01 m + 0.9 m
= 0.91 m

where, D= 400 mm dia /1000
(v₁ = 1.358 m/sec)

f1	Q'ty	f/pc	f
sluice valve	1	0.10	0.10
reducer	1	0.03	0.03
		f ₁ total	0.13

where, D= 300 mm dia /1000
(v₂ = 2.415 m/sec)

f2	Q'ty	f/pc	f
increase	1	0.48	0.48
check valve	1	1.00	1.00
butterfly valve	1	0.20	0.20
90deg	1	0.18	0.18
tee	1	1.15	1.15
		f ₂ total	3.01

friction loss : float type butterfly valve
h₄ = 5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)	
	=	238.8 kW
	=	250.0 kW
	where, r =	1.00
	e =	0.82
	a =	0.15

Specification	
Type	Horizontal Double-Suction Centrifugal Pump
Diameter	300 x 200 mm
Capacity	10.24 m ³ /min
Head	102.0 m
Motor Output	250 kW
Quantity	4 (1) sets including 1 set for future

5-1. Ampitiya Booster Pump (D-1) - Phase 3

Total Capacity	1,200 m ³ /day =	0.83 m ³ /min
Quantity of pump	1 sets + 1 set for stand-by	
Pump Capacity	1,200 m ³ /day	
	Q=	0.83 m ³ /min 50.0 m ³ /hr
	q=	0.014 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	109 mm to 77 mm
	=	80 x 65 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	43.6 m
		= 45.0 m
	actual head : Elhena	
	h ₁ = hd - hs =	32.50 m

suction level hs = 582.50 m
 delivery level hd = 615.00 m

friction loss : pipeline (Hazen Williams)
 $h_2 = 10.666 \times c^{(-1.85)} \times D^{(-4.87)} \times q^{(1.85)} \times L = 4.60 \text{ m}$

friction loss : fittings around pump
 $h_3 = f_1 \times (v_1^2 / 2g) + f_2 \times (v_2^2 / 2g)$
 = 0.12 m + 1.37 m
 = 1.49 m

where, D= 80 mm dia /1000
 (v₁ = 2.763 m/sec)

<u>f1</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
bell mouth	1	0.20	0.20
sluice valve	1	0.10	0.10
reducer	1	<u>0.02</u>	<u>0.02</u>
		f ₁ total	0.32

where, D= 80 mm dia /1000
 (v₂ = 2.763 m/sec)

<u>f2</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
increase	2	0.20	0.40
check valve	1	1.00	1.00
butterfly valve	1	0.20	0.20
90deg	1	0.18	0.18
tee	1	1.50	1.50
sluice valve	2	0.10	0.20
reducer	1	<u>0.03</u>	<u>0.03</u>
		f ₂ total	3.51

friction loss : float type butterfly valve
 h₄ = 5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)	
	=	10.3 kW
	=	11.0 kW
	where, r =	1.00
	e =	0.68
	a =	0.15

Specification	
Type	Horizontal End-Suction Centrifugal Pump
Diameter	80 x 65 mm
Capacity	0.83 m ³ /min
Head	45.0 m
Motor Output	11 kW
Quantity	2 (1) sets including 1 set for future

5-2. Ampitiya Booster Pump (D-2) - Phase 3

Total Capacity	980 m ³ /day =	0.68 m ³ /min
Quantity of pump	1 sets + 1 set for stand-by	
Pump Capacity	980 m ³ /day	
	Q=	0.68 m ³ /min 40.8 m ³ /hr
	q=	0.011 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	98 mm to 70 mm
	=	65 x 50 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	144.7 m
		= 146.0 m
	actual head : Mullepihilla	
	h ₁ = hd - hs =	130.50 m

suction level hs = 582.50 m
 delivery level hd = 713.00 m

friction loss : pipeline (Hazen Williams)
 $h_2 = 10.666 \times c^{(-1.85)} \times D^{(-4.87)} \times q^{(1.85)} \times L = 8.20 \text{ m}$

friction loss : fittings around pump
 $h_3 = f_1 \times (v_1^2 / 2g) + f_2 \times (v_2^2 / 2g)$
 = 0.08 m + 0.91 m
 = 0.99 m

where, D= 80 mm dia /1000
 (v₁ = 2.257 m/sec)

	<u>f1</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
bell mouth		1	0.20	0.20
sluice valve		1	0.10	0.10
reducer		1	<u>0.02</u>	<u>0.02</u>
			f ₁ total	0.32

where, D= 80 mm dia /1000
 (v₂ = 2.257 m/sec)

	<u>f2</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
increase		2	0.20	0.40
check valve		1	1.00	1.00
butterfly valve		1	0.20	0.20
90deg		1	0.18	0.18
tee		1	1.50	1.50
sluice valve		2	0.10	0.20
reducer		1	<u>0.03</u>	<u>0.03</u>
			f ₂ total	3.51

friction loss : float type butterfly valve
 h₄ = 5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)
	= 28.7 kW
	= 30.0 kW
	where, r = 1.00
	e = 0.65
	a = 0.15

Specification	
Type	Horizontal Multi-stage Pump
Diameter	65 x 50 mm
Capacity	0.68 m ³ /min
Head	146.0 m
Motor Output	30 kW
Quantity	2 (1) sets including 1 set for future

5-3. Ampitiya Booster Pump (D-3) - Phase 3

Total Capacity	2,150 m ³ /day =	1.49 m ³ /min
Quantity of pump	1 sets + 1 set for stand-by	
Pump Capacity	2,150 m ³ /day	
	Q=	1.49 m ³ /min 89.6 m ³ /hr
	q=	0.025 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	146 mm to 103 mm
	=	100 x 80 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	72.0 m
		= 73.0 m
	actual head : Meekanuwa	
	h ₁ = hd - hs =	52.50 m

suction level hs = 582.50 m
 delivery level hd = 635.00 m

friction loss : pipeline (Hazen Williams)
 $h_2 = 10.666 \times c^{(-1.85)} \times D^{(-4.87)} \times q^{(1.85)} \times L =$ 12.50 m

friction loss : fittings around pump
 $h_3 = f_1 \times (v_1^2 / 2g) + f_2 \times (v_2^2 / 2g)$
 = 0.16 m + 1.8 m
 = 1.96 m

where, D= 100 mm dia /1000
 (v₁ = 3.168 m/sec)

<u>f₁</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
bell mouth	1	0.20	0.20
sluice valve	1	0.10	0.10
reducer	1	<u>0.02</u>	<u>0.02</u>
		f ₁ total	0.32

where, D= 100 mm dia /1000
 (v₂ = 3.168 m/sec)

<u>f₂</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
increase	2	0.20	0.40
check valve	1	1.00	1.00
butterfly valve	1	0.20	0.20
90deg	1	0.18	0.18
tee	1	1.50	1.50
sluice valve	2	0.10	0.20
reducer	1	<u>0.03</u>	<u>0.03</u>
		f ₂ total	3.51

friction loss : float type butterfly valve
 h₄ = 5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)
	= 28 kW
	= 30.0 kW
	where, r = 1.00
	e = 0.73
	a = 0.15

Specification	
Type	Horizontal End-Suction Centrifugal Pump
Diameter	100 x 80 mm
Capacity	1.49 m ³ /min
Head	73.0 m
Motor Output	30 kW
Quantity	2 (1) sets including 1 set for future

6-1. Kahawatta Booster Pump (E) - Phase 1

Total Capacity	4,240 m ³ /day =	2.94 m ³ /min
Quantity of pump	1 sets + 1 set for stand-by	
Pump Capacity	4,240 m ³ /day	
	Q=	2.94 m ³ /min 176.7 m ³ /hr
	q=	0.049 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)		
	=	205 mm	to 145 mm
	=	150 x 125 mm	
	where, v=	1.5	to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =		
		63.9 m	
		=	68.0 m
	actual head :	Kurugoda	
	h ₁ = hd - hs =		57.00 m
		suction level hs =	516.00 m
		delivery level hd =	573.00 m

friction loss : pipeline (Hazen Williams)			
h ₂ =	10.666 x c ^(-1.85) x D ^(-4.87) x q ^(1.85) x L =		0.40 m
friction loss : fittings around pump			
h ₃ =	f ₁ x (v ₁ ² / 2g) + f ₂ x (v ₂ ² / 2g)		
	=	0.13 m +	1.38 m
	=	1.51 m	
	where, D=	150 mm dia /1000	
	(v ₁ =	2.777 m/sec)	

	<u>f_l</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
bell mouth		1	0.20	0.20
sluice valve		1	0.10	0.10
reducer		1	<u>0.02</u>	<u>0.02</u>
			f ₁ total	0.32

where, D=	150 mm dia /1000
(v ₂ =	2.777 m/sec)

	<u>f₂</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
increase		2	0.20	0.40
check valve		1	1.00	1.00
butterfly valve		1	0.20	0.20
90deg		1	0.18	0.18
tee		1	1.50	1.50
sluice valve		2	0.10	0.20
reducer		1	<u>0.03</u>	<u>0.03</u>
			f ₂ total	3.51

friction loss : float type butterfly valve	
h ₄ =	5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)		
	=	49.4 kW	
	=	55.0 kW	
	where, r =	1.00	
	e =	0.76	
	a =	0.15	

Specification	
Type	Horizontal End-Suction Centrifugal Pump
Diameter	150 x 125 mm
Capacity	2.94 m ³ /min
Head	68.0 m
Motor Output	55 kW
Quantity	2 (1) sets including 1 set for future

6-2. Kahawatta Booster Pump (E) - Phase 3

Total Capacity	7,310 m ³ /day =	5.08 m ³ /min
Quantity of pump	2 sets + 1 set for stand-by	
Pump Capacity	3,655 m ³ /day	
	Q=	2.54 m ³ /min 152.3 m ³ /hr
	q=	0.042 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	190 mm to 134 mm
	=	150 x 125 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	71.1 m
		= 72.0 m
	actual head : Kurugoda	
	h ₁ = hd - hs =	57.00 m

suction level hs =	516.00 m
delivery level hd =	573.00 m

friction loss : pipeline (Hazen Williams)	
h ₂ = 10.666 x c ^(-1.85) x D ^(-4.87) x q ^(1.85) x L =	8.00 m

friction loss : fittings around pump	
h ₃ = f ₁ x (v ₁ ² / 2g) + f ₂ x (v ₂ ² / 2g)	
=	0.09 m + 1.03 m
=	1.12 m

where, D=	150 mm dia /1000
(v ₁ =	2.394 m/sec)

<u>f1</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
bell mouth	1	0.20	0.20
sluice valve	1	0.10	0.10
reducer	1	<u>0.02</u>	<u>0.02</u>
		f ₁ total	0.32

where, D=	150 mm dia /1000
(v ₂ =	2.394 m/sec)

<u>f2</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
increase	2	0.20	0.40
check valve	1	1.00	1.00
butterfly valve	1	0.20	0.20
90deg	1	0.18	0.18
tee	1	1.50	1.50
sluice valve	2	0.10	0.20
reducer	1	<u>0.03</u>	<u>0.03</u>
		f ₂ total	3.51

friction loss : float type butterfly valve	
h ₄ =	5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)
	= 45.1 kW
	= 55.0 kW
where, r =	1.00
e =	0.76
a =	0.15

Specification	
Type	Horizontal End-Suction Centrifugal Pump
Diameter	150 x 125 mm
Capacity	2.54 m ³ /min
Head	72.0 m
Motor Output	55 kW
Quantity	3 (1) sets including 1 set for future

7-1. R2 Booster Pump (F) - Phase 3

Total Capacity	1,960 m ³ /day =	1.36 m ³ /min
Quantity of pump	1 sets + 1 set for stand-by	
Pump Capacity	1,960 m ³ /day	
	Q=	1.36 m ³ /min 81.7 m ³ /hr
	q=	0.023 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	139 mm to 98 mm
	=	100 x 80 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	100.6 m
		= 102.0 m
	actual head : Hantana Place	
	h ₁ = hd - hs =	91.51 m

suction level hs = 549.49 m
 delivery level hd = 641.00 m

friction loss : pipeline (Hazen Williams)
 $h_2 = 10.666 \times c^{(-1.85)} \times D^{(-4.87)} \times q^{(1.85)} \times L =$ 2.49 m

friction loss : fittings around pump
 $h_3 = f_1 \times (v_1^2 / 2g) + f_2 \times (v_2^2 / 2g)$
 = 0.14 m + 1.49 m
 = 1.63 m

where, D= 100 mm dia /1000
 (v₁ = 2.888 m/sec)

<u>f1</u>	<u>Q/ty</u>	<u>f/pc</u>	<u>f</u>
bell mouth	1	0.20	0.20
sluice valve	1	0.10	0.10
reducer	1	0.02	0.02
		f ₁ total	0.32

where, D= 100 mm dia /1000
 (v₂ = 2.888 m/sec)

<u>f2</u>	<u>Q/ty</u>	<u>f/pc</u>	<u>f</u>
increase	2	0.20	0.40
check valve	1	1.00	1.00
butterfly valve	1	0.20	0.20
90deg	1	0.18	0.18
tee	1	1.50	1.50
sluice valve	2	0.10	0.20
reducer	1	0.03	0.03
		f ₂ total	3.51

friction loss : float type butterfly valve
 h₄ = 5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)	
	=	36.7 kW
	=	37.0 kW
	where, r =	1.00
	e =	0.71
	a =	0.15

Specification	
Type	Horizontal End-Suction Centrifugal Pump
Diameter	100 x 80 mm
Capacity	1.36 m ³ /min
Head	102.0 m
Motor Output	37 kW
Quantity	2 (1) sets including 1 set for future

8-1. Asgiriya In-Line Booster Pump (G) - Phase 3

Total Capacity 2,280 m³/day = 1.58 m³/min
 Quantity of pump 1 sets + 1 set for stand-by
 Pump Capacity 2,280 m³/day
 Q= 1.58 m³/min 95.0 m³/hr
 q= 0.026 m³/sec

Diameter Diameter = 146 x (Q / v)^(1/2)
 = 150 mm to 106 mm
 = 100 x 80 mm
 where, v= 1.5 to 3

Total Head Total Head H = h₁ + h₂ + h₃ + h₄ = 66.7 m
 = 68.0 m
 actual head : Bahirawakanda
 h₁ = hd - hs = 56.3 m

floor level hf = 532.50 m
 suction pressure hs = 40.25 m
 delivery level hd = 629.00 m

friction loss : pipeline (Hazen Williams)
 $h_2 = 10.666 \times c^{(-1.85)} \times D^{(-4.87)} \times q^{(1.85)} \times L = 3.22 \text{ m}$

friction loss : fittings around pump
 $h_3 = f_1 \times (v_1^2 / 2g) + f_2 \times (v_2^2 / 2g)$
 = 0.18 m + 2.02 m
 = 2.2 m

where, D= 100 mm dia /1000
 (v₁ = 3.360 m/sec)

<u>f1</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
bell mouth	1	0.20	0.20
sluice valve	1	0.10	0.10
reducer	1	<u>0.02</u>	<u>0.02</u>
		f ₁ total	0.32

where, D= 100 mm dia /1000
 (v₂ = 3.360 m/sec)

<u>f2</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
increase	2	0.20	0.40
check valve	1	1.00	1.00
butterfly valve	1	0.20	0.20
90deg	1	0.18	0.18
tee	1	1.50	1.50
sluice valve	2	0.10	0.20
reducer	1	<u>0.03</u>	<u>0.03</u>
		f ₂ total	3.51

friction loss : float type butterfly valve
 h₄ = 5.00 m

Motor Output Motor Output = (0.163 x r x Q x H / e) x (1 + a)
 = 28 kW
 = 30.0 kW
 where, r = 1.00
 e = 0.72
 a = 0.15

Specification
 Type Horizontal End-Suction Centrifugal Pump
 Diameter 100 x 80 mm
 Capacity 1.58 m³/min
 Head 68.0 m
 Motor Output 30 kW
 Quantity 2 (1) sets including 1 set for future

9-1. Kondadeniya Booster Pump (H) - Phase 3

Total Capacity	1,600 m ³ /day =	1.11 m ³ /min
Quantity of pump	1 sets + 1 set for stand-by	
Pump Capacity	1,600 m ³ /day	
	Q=	1.11 m ³ /min 66.7 m ³ /hr
	q=	0.019 m ³ /sec

Diameter	Diameter = 146 x (Q / v) ^(1/2)	
	=	126 mm to 89 mm
	=	80 x 65 mm
	where, v=	1.5 to 3

Total Head	Total Head H = h ₁ + h ₂ + h ₃ + h ₄ =	62.6 m
		= 64.0 m
	actual head : Kulugammana	
	h ₁ = hd - hs =	52.00 m
	suction level hs =	531.25 m
	delivery level hd =	583.25 m

friction loss : pipeline (Hazen Williams)
 $h_2 = 10.666 \times c^{(-1.85)} \times D^{(-4.87)} \times q^{(1.85)} \times L =$ 2.90 m

friction loss : fittings around pump
 $h_3 = f_1 \times (v_1^2 / 2g) + f_2 \times (v_2^2 / 2g)$
 = 0.22 m + 2.43 m
 = 2.65 m

where, D= 80 mm dia /1000
 (v₁ = 3.684 m/sec)

<u>f1</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
bell mouth	1	0.20	0.20
sluice valve	1	0.10	0.10
reducer	1	<u>0.02</u>	<u>0.02</u>
		f ₁ total	0.32

where, D= 80 mm dia /1000
 (v₂ = 3.684 m/sec)

<u>f2</u>	<u>Q'ty</u>	<u>f/pc</u>	<u>f</u>
increase	2	0.20	0.40
check valve	1	1.00	1.00
butterfly valve	1	0.20	0.20
90deg	1	0.18	0.18
tee	1	1.50	1.50
sluice valve	2	0.10	0.20
reducer	1	<u>0.03</u>	<u>0.03</u>
		f ₂ total	3.51

friction loss : float type butterfly valve
 h₄ = 5.00 m

Motor Output	Motor Output = (0.163 x r x Q x H / e) x (1 + a)
	= 19 kW
	= 30.0 kW
	where, r = 1.00
	e = 0.70
	a = 0.15

Specification	
Type	Horizontal End-Suction Centrifugal Pump
Diameter	80 x 65 mm
Capacity	1.11 m ³ /min
Head	64.0 m
Motor Output	30 kW
Quantity	2 (1) sets including 1 set for future

Sri Lanka - Greater Kandy Water Supply Augmentation Project
Chemical Facility Capacity Calculation for Katugastota Treatment Plant Q=110,000 cu m/day

Item	Total System	First Stage
Plant Capacity (Daily Max)	Q= 110,000 cu m/day	Q= 36,670 cu m/day
Planned Flow	Q= 115,500 cu m/day = 4,813 cu m/hour = 80.2 cu m/min = 1.337 cu m/sec	Q= 38,500 cu m/day = 1,604 cu m/hour = 26.7 cu m/min = 0.446 cu m/sec
(1) Alum Dissolving Tank		
Coagulant	Solid Aluminum Sulphate (Al ₂ (SO ₄) ₃) containing 15 % Al ₂ O ₃	Solid Aluminum Sulphate (Al ₂ (SO ₄) ₃) containing 15 % Al ₂ O ₃
Criteria	Dosage Rate : 10-60 mg-solid alum/l - Maximum 60 mg/l - Average 30 mg/l - Minimum 10 mg/l Coagulant Solution : 10 % sg = 1.0525 Retention Time 24 hours Dissolving Time 2 hours	Dosage Rate : 10-60 mg-solid alum/l - Maximum 60 mg/l - Average 30 mg/l - Minimum 10 mg/l Coagulant Solution : 10 % sg = 1.0525 Retention Time 24 hours Dissolving Time 2 hours
Dosage Amount Coagulant Solution	Wt = 3,465 kg-Alum/day (Ave dosage) Vmax = 32.9 cu m/day (Max dosage) Vave = 16.5 cu m/day (Ave dosage)	Wt = 1,155 kg-Alum/day (Ave dosage) Vmax = 11.0 cu m/day (Max dosage) Vave = 5.5 cu m/day (Ave dosage)
Solution Tank Dimension	Square 4 units L m x W m x D m x units 2.0 2.0 2.5 4	Square 2 units L m x W m x D m x units 2.0 2.0 2.5 2
Total Volume Retention Time	V = 40.0 cu m T = 29.2 hours for maximum dosing	V = 20.0 cu m T = 43.7 hours for maximum dosing
Alum Pump Capacity	2 units each (excl. 1 unit stand-by) Qmax = 11.3 liter/min 0.69 cu m/hr Qmin = 1.9 liter/min 0.11 cu m/hr	1 units (excl. 1 unit stand-by) Qmax = 7.6 liter/min 0.46 cu m/hr Qmin = 1.3 liter/min 0.08 cu m/hr
Storage	Period 30 days Bulk s. g. 0.60	Period 30 days Bulk s. g. 0.60
Storage Area	A = 87 m ² at 2.0 m height	A = 29 m ² at 2.0 m height
(2) Lime Dissolving Tank		
pH Control	Hydrated Lime (Ca(OH) ₂) containing 72 % CaO	Hydrated Lime (Ca(OH) ₂) containing 72 % CaO
Criteria Requirement by Alum Dosage	Dosage Rate : 5-30 mg-solid Lime/l - Maximum 20.8 mg/l - Average 10.4 mg/l - Minimum 3.5 mg/l Lime Solution 10 % sg = 1.0607 Retention Time 24 hours Dissolving Time 2 hours	Dosage Rate : 5-30 mg-solid Lime/l - Maximum 20.8 mg/l - Average 10.4 mg/l - Minimum 3.5 mg/l Lime Solution 10 % sg = 1.0607 Retention Time 24 hours Dissolving Time 2 hours
Dosage Amount Alkali Solution	Wt max = 2,401 kg-Lime/day (for Max Alum dosage) V max = 22.6 cu m/day (for Max Alum dosage)	Wt max = 800 kg-Lime/day (for Max Alum dosage) V max = 7.5 cu m/day (for Max Alum dosage)
Solution Tank Dimension	Square 4 units L m x W m x D m x units 2.0 2.0 2.5 4	Square 2 units L m x W m x D m x units 2.0 2.0 2.5 2
Total Volume Retention Time	V = 40.0 cu m T = 42.4 hours (for Max Alum dosage)	V = 20.0 cu m T = 63.6 hours (for Max Alum dosage)
Dosage Rate	Maximum Average Minimum Pre (5-30 mg/l) 30 15 5 Post (5-20 mg/l) 20 5 5	Maximum Average Minimum Pre (5-30 mg/l) 30 15 5 Post (5-20 mg/l) 20 5 5
Pump Capacity	Pre- 2 units each (excl. 1 unit stand-by) Qmax = 11.3 liter/min 0.68 cu m/hr Qmin = 1.9 liter/min 0.11 cu m/hr Post- 2 units each (excl. 1 unit stand-by) Qmax = 7.6 liter/min 0.45 cu m/hr Qmin = 1.9 liter/min 0.11 cu m/hr	Pre- 1 units each (excl. 1 unit stand-by) Qmax = 7.6 liter/min 0.45 cu m/hr Qmin = 1.3 liter/min 0.08 cu m/hr Post- 1 units each (excl. 1 unit stand-by) Qmax = 5.0 liter/min 0.30 cu m/hr Qmin = 1.3 liter/min 0.08 cu m/hr
Storage	Period 30 days Bulk s. g. 0.40	Period 30 days Bulk s. g. 0.40
Storage Area	A = 87 m ² at 2.0 m height	A = 29 m ² at 2.0 m height

(3) Chlorination Equipment												
Injection Point	Pre-Chlorine Post-Chlorine				at the Inlet of Distribution Chamber and outlet of Filter			Pre-Chlorine Post-Chlorine		at the Inlet of Distribution Chamber and outlet of Filter		
Type	Liquid Chlorine (900 kg-cylinder)											
Dosage Rate	Maximum			Average	Minimum	Maximum			Average	Minimum		
	Pre	(1.0-5.0 mg/	5.0	2.0	1.0	Pre	(1.0-5.0 mg/	5.0	2.0	1.0		
	Post	(0.5-1.0 mg/	2.0	1.0	0.5	Post	(0.5-1.0 mg/	2.0	1.0	0.5		
Dosage Amount	Wt =	347 kg- Cl gas/day (Average)				Wt =	116 kg- Cl gas/day (Average)					
	or	14.4 kg- Cl gas/hour (Average)				or	4.8 kg- Cl gas/hour (Average)					
Chlorinator Capacity	Vacuum Type											
	Pre-	2 units each		(excl. 1 unit stand-by)			Pre-	1 units each		(excl. 1 unit stand-by)		
	Qmax =	12.0	kg/hr	288.75 kg/day			Qmax =	8.0	kg/hr	192.50 kg/day		
	Qmin =	2.4	kg/hr	57.75 kg/day			Qmin =	1.6	kg/hr	38.50 kg/day		
	Post-	2 units each		(excl. 1 unit stand-by)			Post-	1 units each		(excl. 1 unit stand-by)		
	Qmax =	4.8	kg/hr	115.50 kg/day			Qmax =	3.2	kg/hr	77.00 kg/day		
	Qmin =	1.2	kg/hr	28.88 kg/day			Qmin =	0.8	kg/hr	19.25 kg/day		
Storage No. of Container	Period	30 days			Period	30 days						
		14 units				6 units						
Storage Area	A =	28 m2 as			A =	12 m2 as						
		2.0 m2/container				2.0 m2/container						

Alum - Specific Gravity (% as Al ₂ (SO ₄) ₃ ·18H ₂ O)		Lime - Specific Gravity (% as Ca (OH) ₂)	
5	1.0254	5	1.0308
10	1.0525	10	1.0607
15	1.0804	15	1.0923

Sri Lanka - Greater Kandy Water Supply Augmentation Project
Chemical Facility Capacity Calculation for Kahawwatta Reservoir Q=7,310 cu m/day

Item	Total System	First Stage
Plant Capacity (Daily Max)	Q= 7,310 cu m/day	Q= 4,240 cu m/day
Planned Flow	Q= 7,310 cu m/day	Q= 4,240 cu m/day
	= 305 cu m/hour	= 177 cu m/hour
	= 5.1 cu m/min	= 2.9 cu m/min
	= 0.085 cu m/sec	= 0.049 cu m/sec
Chlorine Dissolving Tank		
Chlorine	Calcium Hypochlorite (Ca(Ocl)2·4H2O) containing 60 % cl2	Calcium Hypochlorite (Ca(Ocl)2·4H2O) containing 60 % cl2
Criteria	Dosage Rate : 0.5 - 2 mg-solid alum/l	Dosage Rate : 0.5 - 2 mg-solid alum/l
	- Maximum 2 mg/l	- Maximum 2 mg/l
	- Average 1 mg/l	- Average 1 mg/l
	- Minimum 0.5 mg/l	- Minimum 0.5 mg/l
	Solution : 5 % sg = 1.0247	Solution : 5 % sg = 1.0247
Retention Time	24 hours	24 hours
Dissolving Time	2 hours	2 hours
Dosage Amount Chlorine Solution	Wt = 12.18 kg-chlorine/day (Ave dosage)	Wt = 7.07 kg-Alum/day (Ave dosage)
	Vmax = 0.48 cu m/day (Max dosage)	Vmax = 0.28 cu m/day (Max dosage)
	Vave = 0.24 cu m/day (Ave dosage)	Vave = 0.14 cu m/day (Ave dosage)
Solution Tank Dimension	Square 1 units	Square 1 units
	L m x W m x D m x units 0.9 0.9 0.9 1	L m x W m x D m x units 0.9 0.9 0.9 1
Total Volume Retention Time	V = 0.7 cu m	V = 0.7 cu m
	T = 36.8 hours for maximum dosing	T = 63.4 hours for maximum dosing
Chlorination Pump Capacity	1 units each (excl. 1 unit stand-by)	1 units (excl. 1 unit stand-by)
	Qmax = 0.33 liter/min 0.02 cu m/hr	Qmax = 0.19 liter/min 0.01 cu m/hr
	Qmin = 0.08 liter/min 0.00 cu m/hr	Qmin = 0.05 liter/min 0.00 cu m/hr
Storage No. of Container	Period 30 days	Period 30 days
	3 units	3 units
Storage Area	A = 0.375 m2 as 0.125 m2/container	A = 0.375 m2 as 0.125 m2/container

Hypo-chlorite
 (% as Ca(Ocl)2·4H2O)
 5 1.0247

SURGE ANALYSIS

ウォーターハンマ計算条件

Calculation No. 計算番号 C2-10101N PAGE 1

Sample

Intake Pump

Standard Level 基準レベル 436.940 m
 Calculation Time Unit 計算時間単位 .06140 sec

【 管路仕様 】 Pipeline Specifications

No.	Length	Materials	Diameter		Modulus of Elasticity	Upstream Pipeline	Pump No.	Valve No.			Flow	Pipe Loss	Valve Loss	Pressure Wave Reciprocation Time	Pipeline Constant	Division
			Thickness	Thickness				Surge Tank No.	Pipeline End	Pipeline End						
管路名称 1	管長 m 420.0	管種 SS 1	管径 mm 800	管厚 mm 7.0	ヤング率 2.100	上流の管路	ポンプ番号 1 0 0	サージタンク番号 0	弁番号 0	終点条件 1	管路流量 m3/m 80.210	配管損失 m 4.400	弁絞損失 m .000	圧力波往復時間 sec .8596	管路定数 1.6539	分割 14

【 ポンプ仕様 】 Pump Specifications

Pump No.	Valve Close Type	Valve No.	Total Head	Capacity	Motor Output	Pole	Type	Pump/Motor	Flywheel	Speed	Inertial Effect		Head	Capacity	Speed	Torque		
											Efficiency	Efficiency						
番号 1	台数 3	形式 1	弁閉鎖 1	弁番号 0	全揚程 m 44.000	吐出量 m3/m 26.740	出力 kw 250.0	極数 4	型式 1	ポンプ・モータ kg-m2 30.000	フライホイール kg-m2 .000	回転数 min-1 1480	効率 % 87	減衰定数 k 1.2263	初期状態 揚程 m 44.000	吐出量 m3/m 26.740	回転数 1.000	トルク 1.000

【 圧力線図仕様 】 Pressure Gradients

Pipeline No.

管路名称 1

【 縦断仕様 】 Pipeline Profile

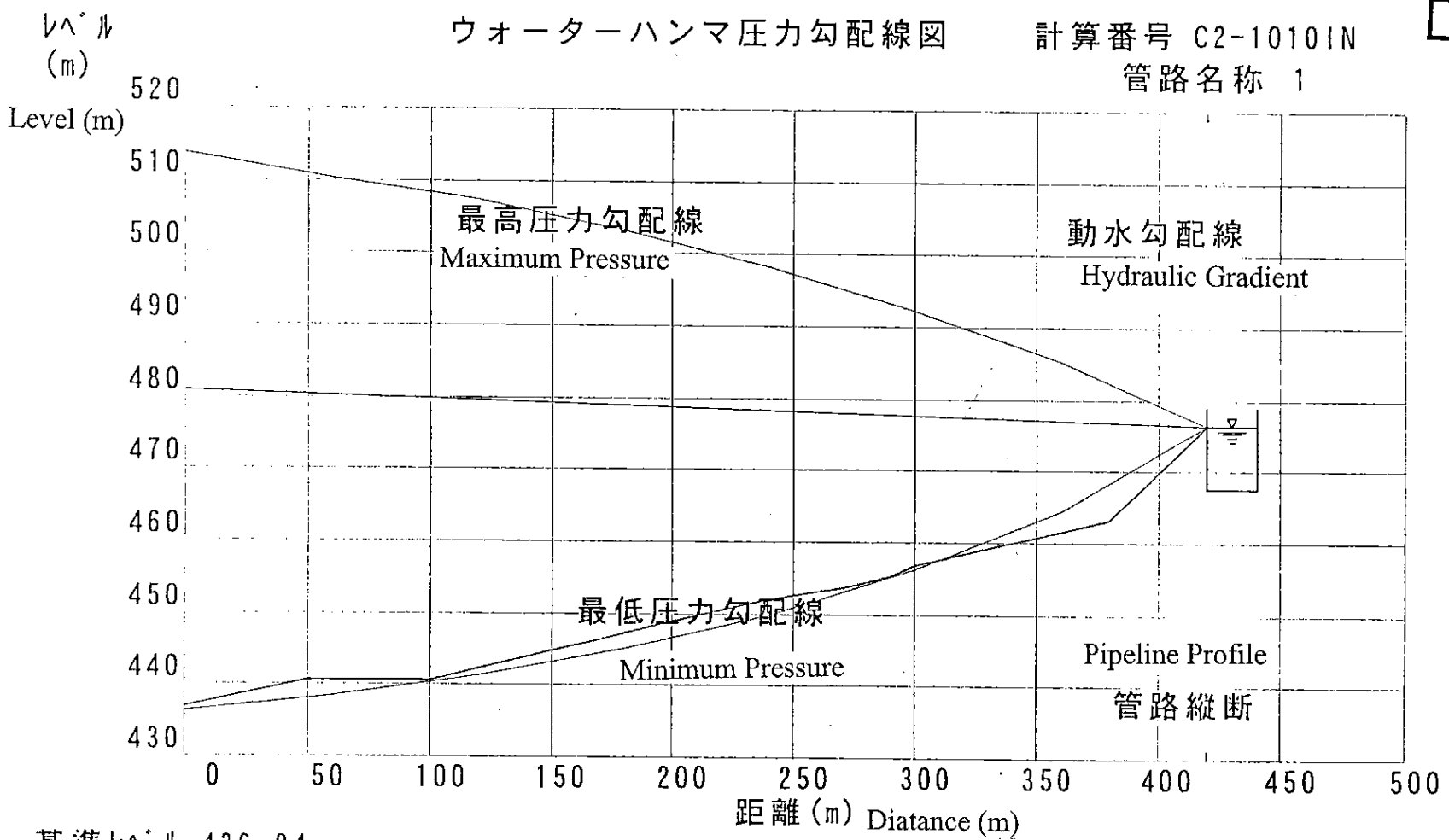
Pipeline No.	Cumulative Distance (m)	Level (m)	Cumulative Distance (m)	Level (m)	Cumulative Distance (m)	Level (m)	Cumulative Distance (m)	Level (m)
管路名称 1	追加距離 m 0	レベル m 436.94	追加距離 m 50.0	レベル m 440.83	追加距離 m 100.0	レベル m 440.83	追加距離 m 120.0	レベル m 442.43
	150.0	444.83	170.0	446.43	200.0	448.83	240.0	452.03
	270.0	453.63	290.0	455.23	300.0	456.83	340.0	460.03
	360.0	461.63	380.0	463.23	410.0	472.83	420.0	476.54

5.24

Sample

ウォーターハンマ圧力勾配線図

計算番号 C2-10101N
管路名称 1



基準レベル 436.94

INTAKE PUMP

5-25

ウォーターハンマ計算条件

計算番号 C2-10101N

PAGE 1

Intake Pump

基準レベル 436.940 m
計算時間単位 .06140 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m ³ /m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	420.0	SS 1	800	7.0	2.100		1 0 0	0	0	1	80.210	4.400	.000	.8596	1.6539	14

【 ポンプ仕様 】

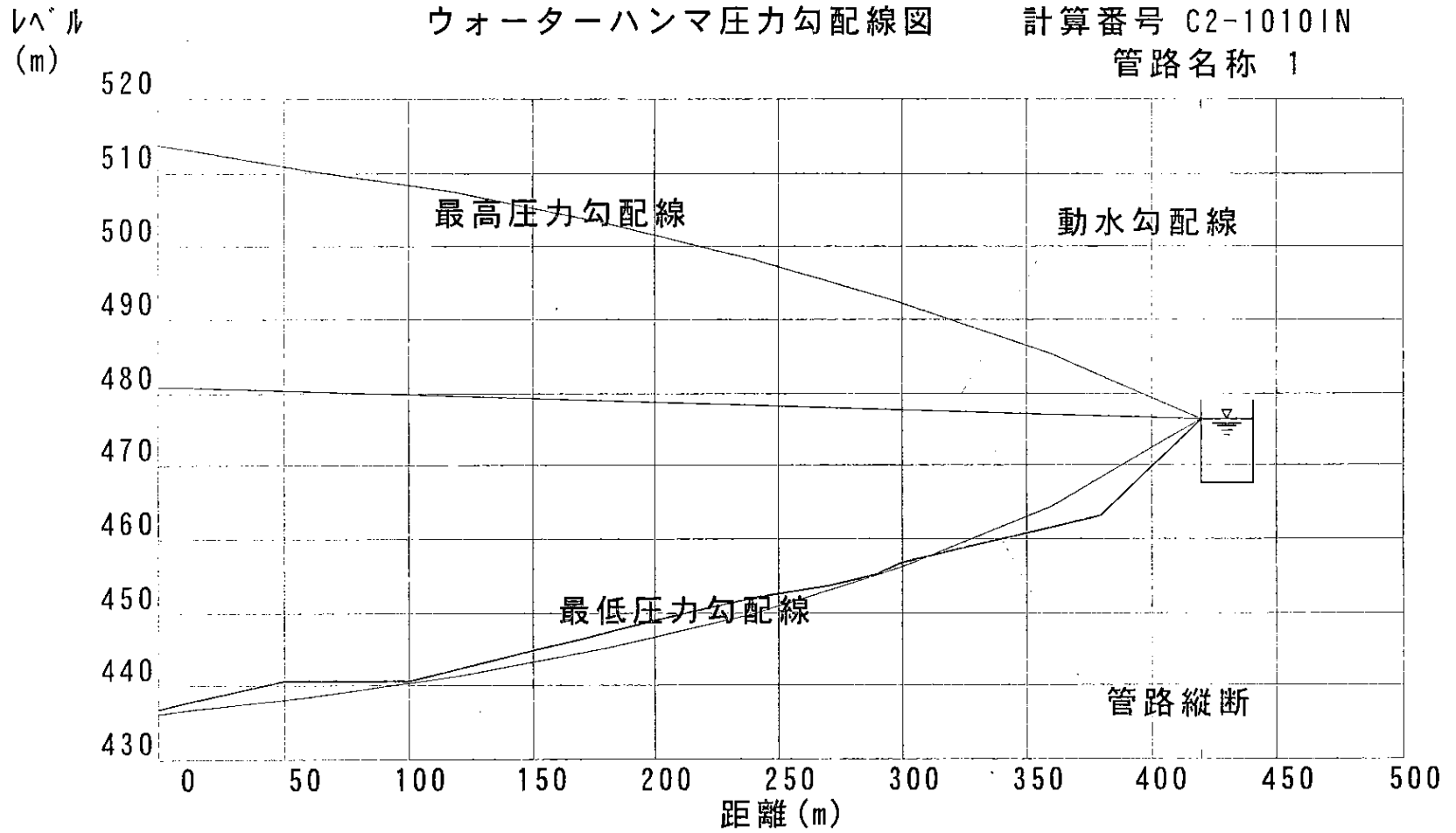
番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m ³ /m	出力 kw	極数	型式	ポンプ・モータ kg-m ²	フライール kg-m ²	回転数 min-1	効率 %	減衰 定数 k	初期状態 揚程 m	吐出量 m ³ /m	回転数	トルク
1	3	1	1	0	44.000	26.740	250.0	4	1	30.000	.000	1480	87	1.2263	44.000	26.740	1.000	1.000

【 圧力線図仕様 】

管路名称 1

【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	436.94	50.0	440.83	100.0	440.83	120.0	442.43
	150.0	444.83	170.0	446.43	200.0	448.83	240.0	452.03
	270.0	453.63	290.0	455.23	300.0	456.83	340.0	460.03
	360.0	461.63	380.0	463.23	410.0	472.83	420.0	476.54



基準レベル 436.94

INTAKE PUMP

5-27

ウォーターハンマ計算条件

計算番号 C2-1010-A1

PAGE 1

Clear Water Pump (A1)

基準レベル 442.610 m
 計算時間単位 .01023 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	10.0	SS 1	800	7.0	2.100		1 0 0	0	0	0	12.215	.100	.000	.0205	1.6539	2
2	1384.0	FCD3	700	10.0	1.600	1	0 0 0	0	0	0	12.215	.800	.000	2.6815	2.2820	264
3	2059.0	FCD3	400	7.0	1.600	2	0 0 0	0	0	1	3.044	1.300	.000	3.8112	7.3153	372
4	1308.0	FCD3	700	10.0	1.600	2	0 0 0	0	0	0	9.171	.500	.000	2.5342	2.2820	248
5	237.0	FCD3	500	8.0	1.600	4	0 0 0	0	0	1	7.803	.300	.000	.4473	4.5912	44
6	100.0	FCD3	200	6.0	1.600	4	0 0 0	0	0	0	1.368	.100	.000	.1679	32.2567	16
7	2198.0	FCD3	200	6.0	1.600	6	2 0 0	0	0	1	1.368	10.000	.000	3.6906	32.2567	360

【 ポンプ仕様 】

番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライホイール kg-m2	回転数 min-1	効率 %	減衰 定数 k	揚程 m	初期状態 吐出量 m3/m	回転数	トルク
1	1	1	1	0	130.300	12.215	450.0	4	1	63.000	100.000	1475	80	.3343	130.300	12.215	1.000	1.000
2	1	1	1	0	60.000	1.368	30.0	4	1	1.960	.000	1470	77	1.4996	60.000	1.368	1.000	1.000

【 圧力線図仕様 】

管路名称	1	2	4	6	7
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【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	440.86	10.0	440.86				
2	10.0	440.86	300.0	445.00	450.0	441.59	500.0	442.50
	510.0	445.00	640.0	445.00	650.0	441.25	970.0	440.90
	1270.0	454.00	1384.0	451.63				
3	1384.0	451.63	1391.0	448.09	1418.0	445.29	1464.0	447.75
	1486.0	451.70	2035.0	494.90	2114.0	494.90	2433.0	506.80
	2691.0	494.01	3129.0	526.80	3262.0	547.92	3393.0	557.92
	3443.0	558.50						

ウォーターハンマ計算条件

計算番号 C2-1010-A1

PAGE 2

【縦断仕様】

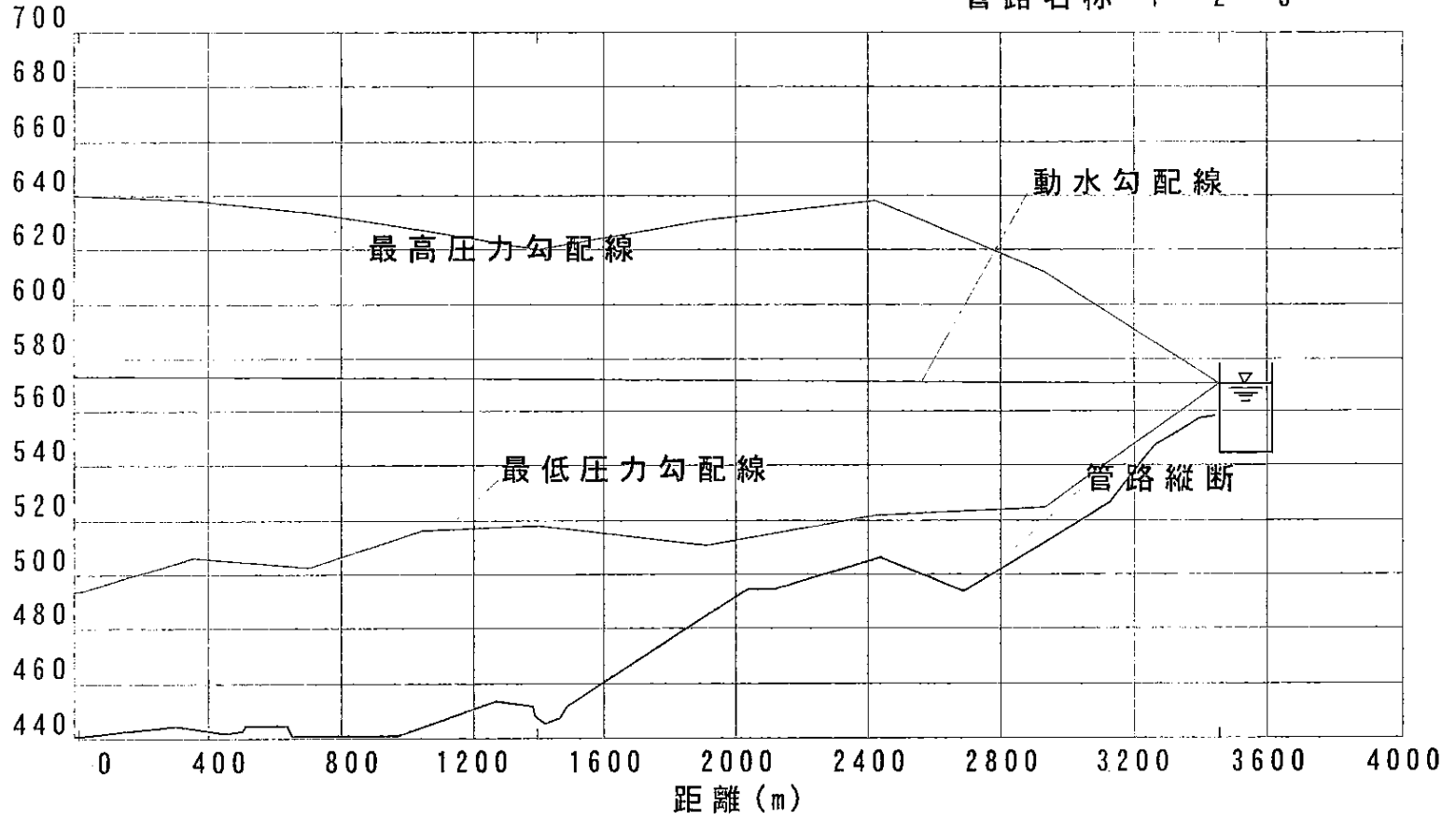
管路 名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
4	1384.0	451.63	1444.0	450.70	1958.0	483.25	2039.0	481.70
	2316.0	524.62	2586.0	524.30	2692.0	524.40		
5	2692.0	524.40	2716.0	527.03	2783.0	524.38	2833.0	535.58
	2879.0	562.98	2929.0	563.00				
6	2692.0	524.40	2702.0	524.40				
	2702.0	524.40	2711.0	524.79	2793.0	519.34	3480.0	553.58
7	3580.0	548.90	3697.0	554.22	3822.0	551.25	4172.0	570.03
	4665.0	552.25	4693.0	553.24	4809.0	562.07	4940.0	590.27
	4990.0	604.00						

レベル
(m)

ウォーターハンマ圧力勾配線図

計算番号 C2-1010-A1

管路名称 1 2 3



基準レベル 442.61

A1 Pump

意図: (Handwritten note)

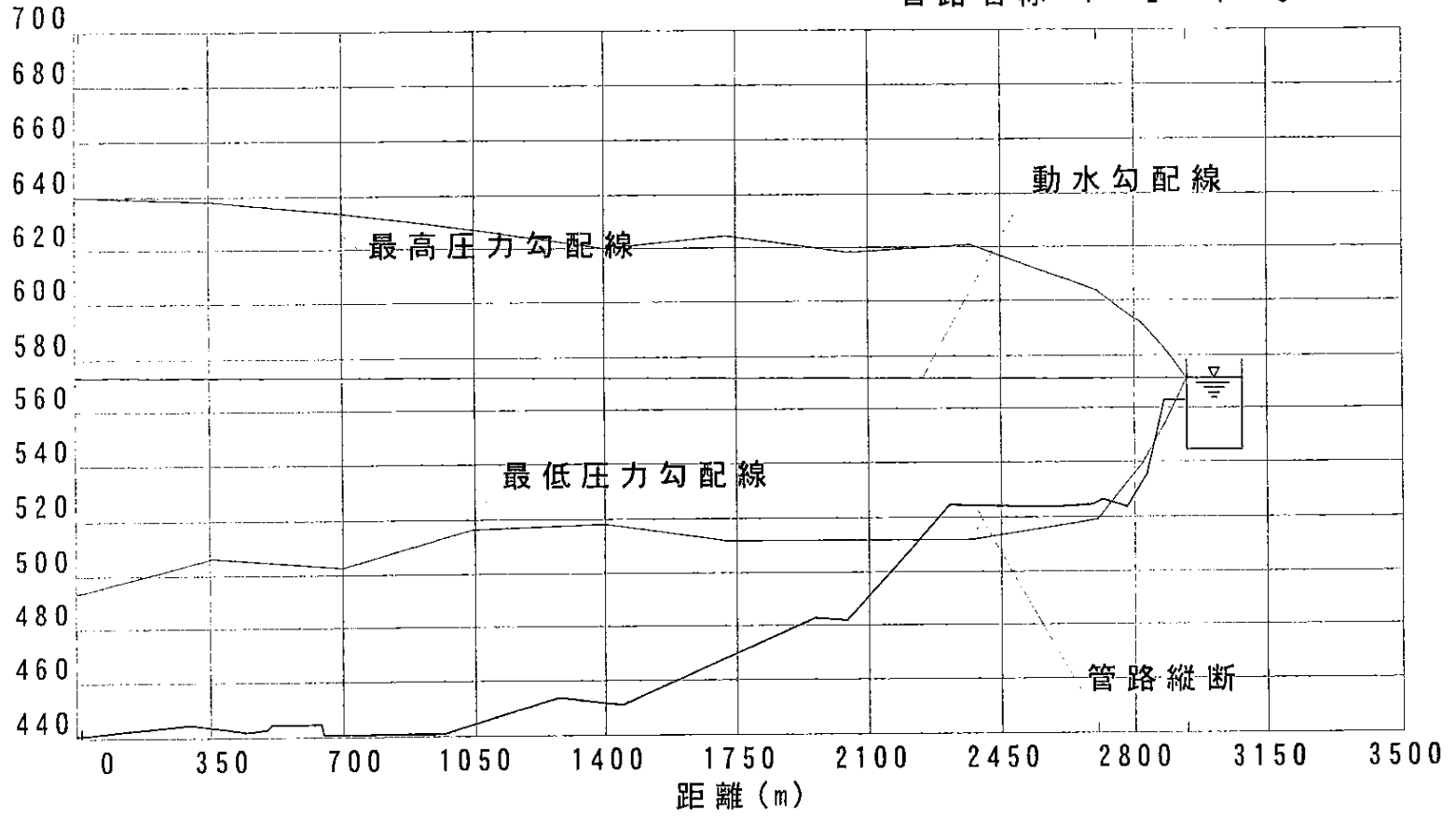
To upland Reservoir

レベル
(m)

ウォーターハンマ圧力勾配線図

計算番号 C2-1010-A1

管路名称 1 2 4 5



基準レベル 442.61

A1 Pump.

目的地:

To Asgiriya Reservoir

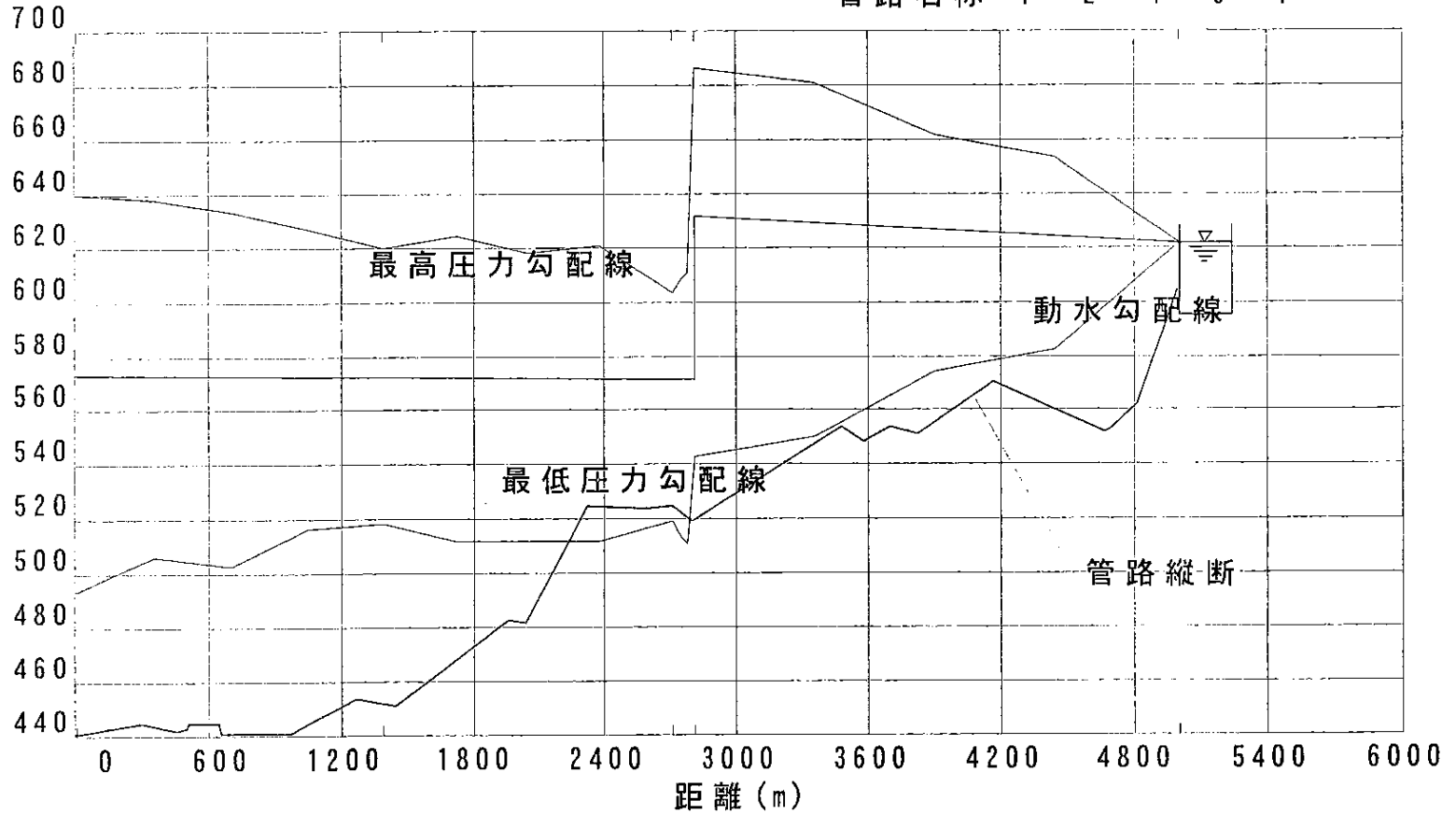
5-31

レベル
(m)

ウォーターハンマ圧力勾配線図

計算番号 C2-1010-A1

管路名称 1 2 4 6 7



基準レベル 442.61

A1 Pump

無水時 To Bahirawakada Reservoir

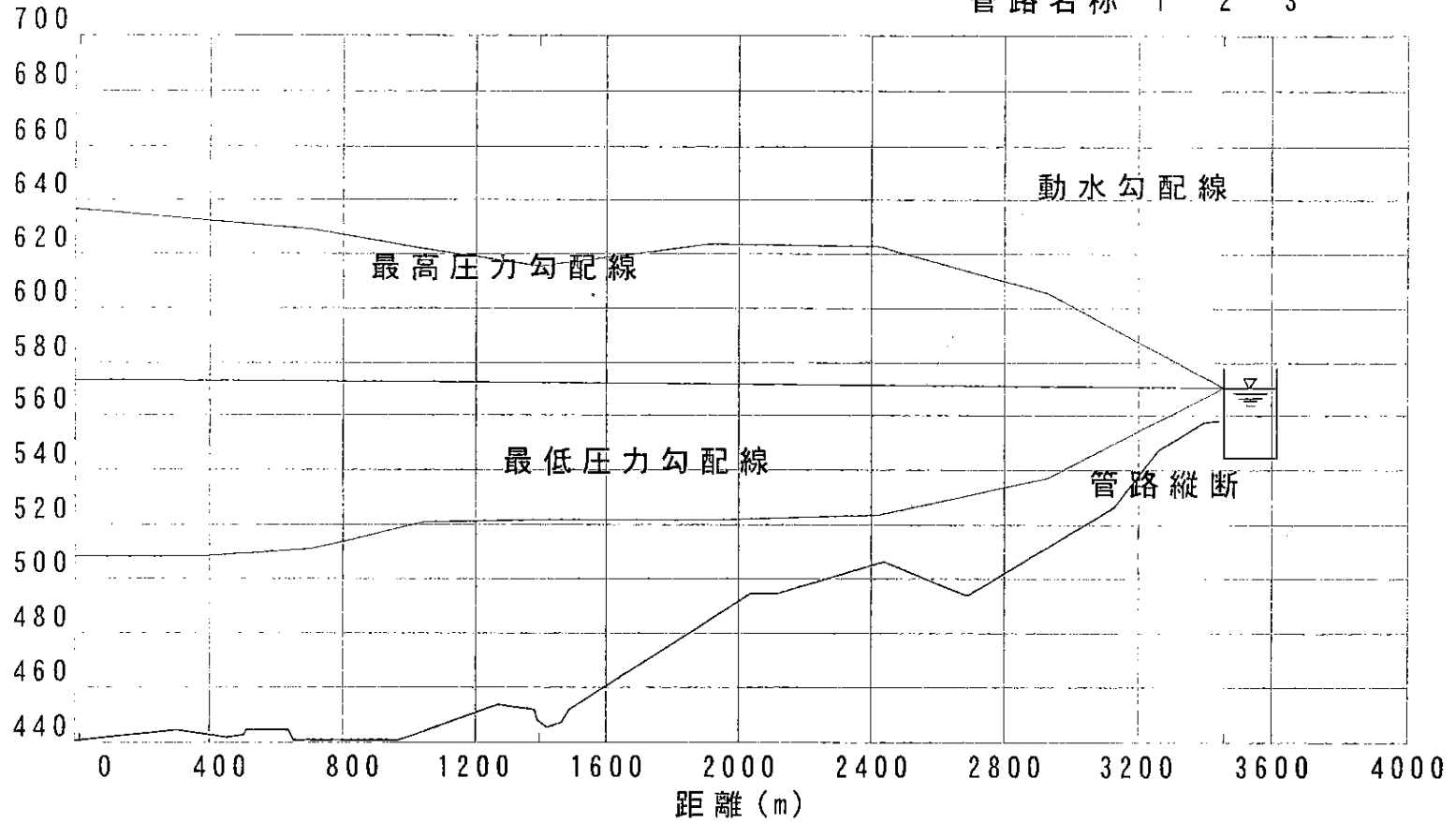
25.7

レベル
(m)

ウォーターハンマ圧力勾配線図

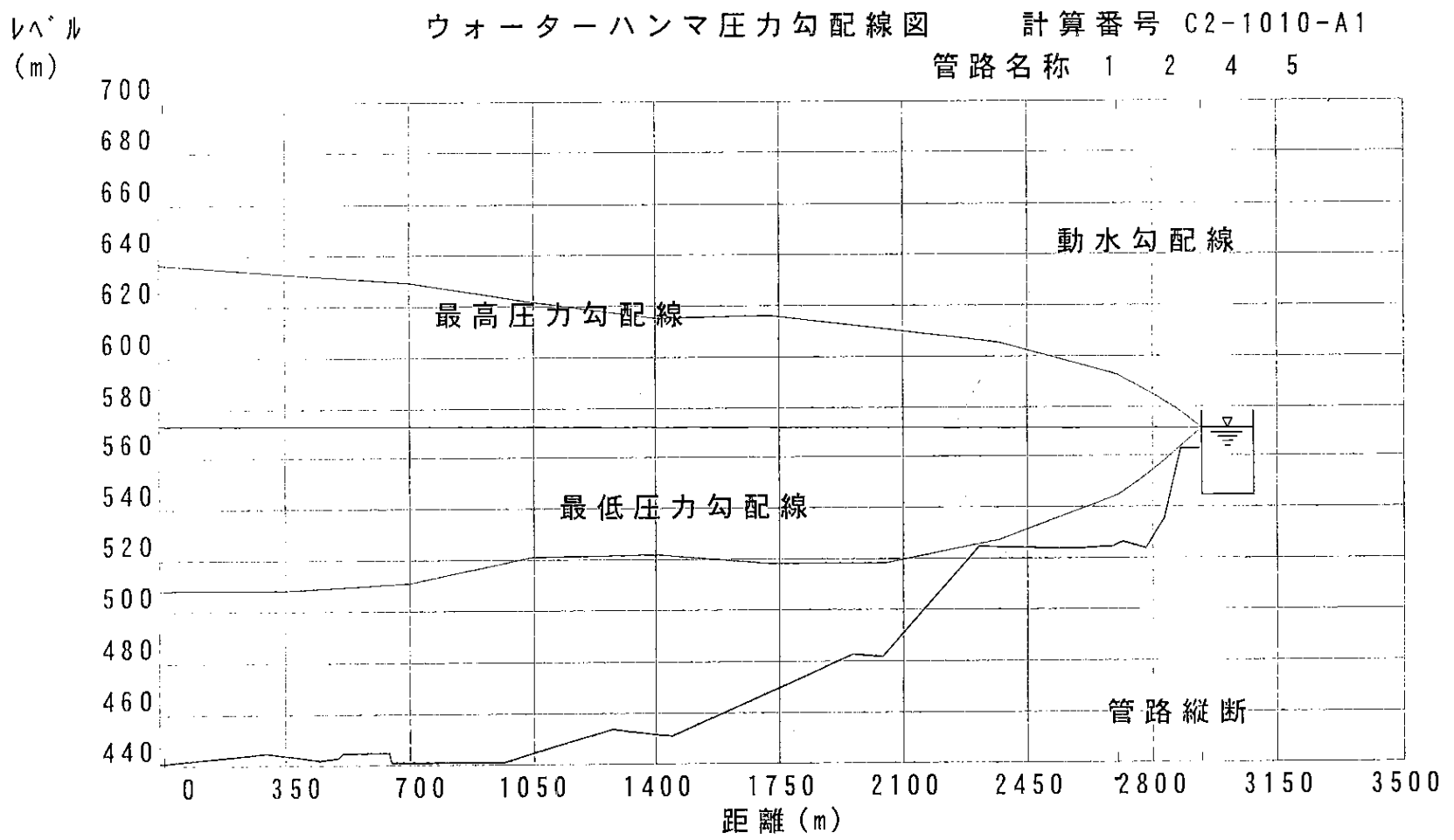
計算番号 C2-1010-A1

管路名称 1 2 3



基準レベル 442.61

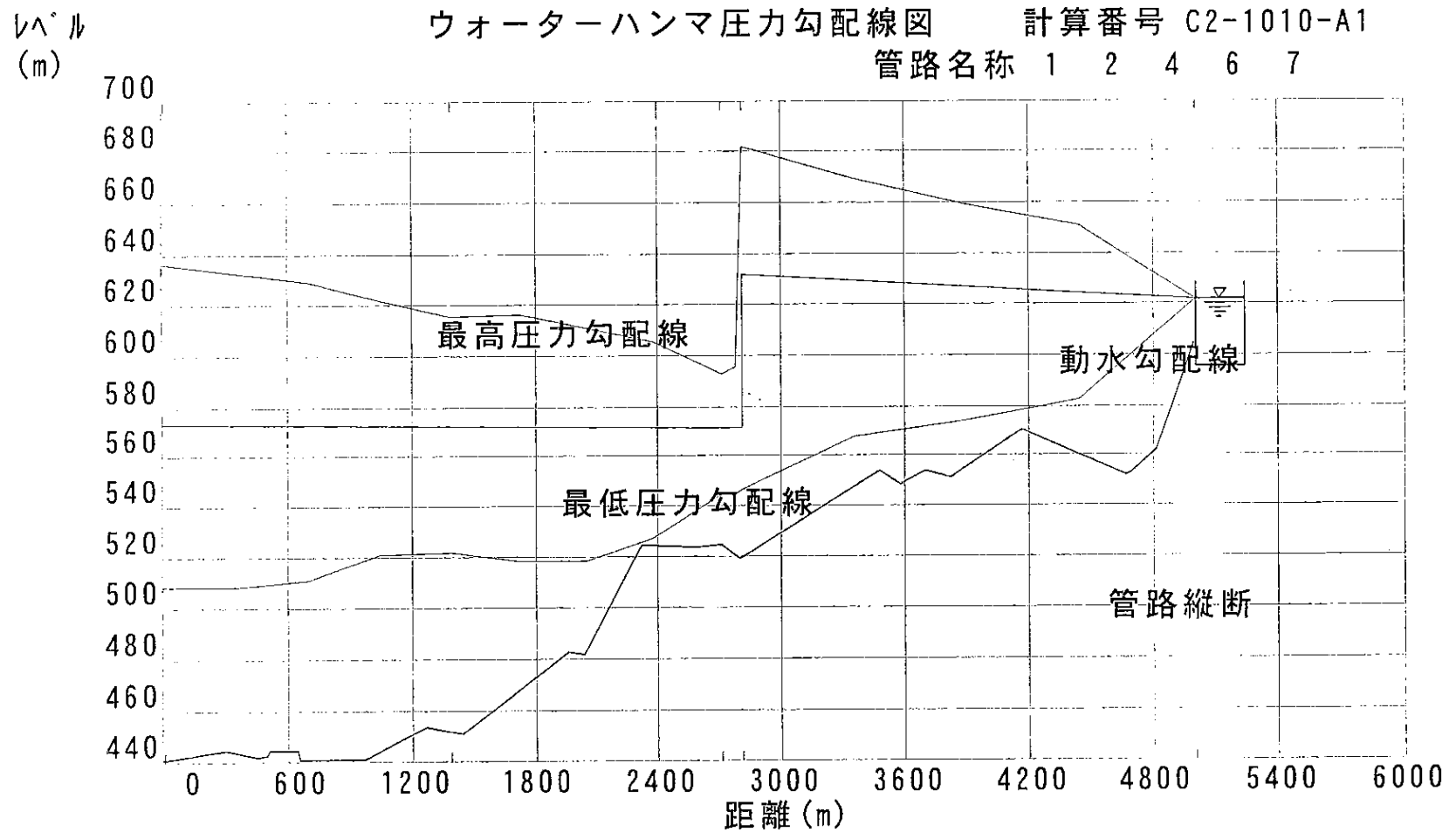
with Flywheel $1000 \text{ kg} \cdot \text{m}^2$ To upland Reservoir



基準レベル 442.61

with flywheel 1000000 m² to Asgirija Reservoir

653



基準レベル 442.61

with Flywheel 1000g/m²

To Bahirawakada Reservoir

Clear Water Pump (A1)

基準レベル 442.610 m
計算時間単位 .01023 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	10.0	SS 1	800	7.0	2.100		1 0 0	0	0	0	12.215	.100	.000	.0205	1.6539	2
2	1384.0	FCD3	700	10.0	1.600	1	0 0 0	0	0	0	12.215	.800	.000	2.6815	2.2820	264
3	2059.0	FCD3	400	7.0	1.600	2	0 0 0	0	0	1	3.044	1.300	.000	3.8112	7.3153	372
4	1308.0	FCD3	700	10.0	1.600	2	0 0 0	0	0	0	9.171	.500	.000	2.5342	2.2820	248
5	237.0	FCD3	500	8.0	1.600	4	0 0 0	0	0	1	7.803	.300	.000	.4473	4.5912	44
6	100.0	FCD3	200	6.0	1.600	4	0 0 0	0	0	0	1.368	.100	.000	.1679	32.2567	16
7	2198.0	FCD3	200	6.0	1.600	6	2 0 0	0	0	1	1.368	10.000	.000	3.6906	32.2567	360

【 ポンプ仕様 】

番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライホイール kg-m2	回転数 min-1	効率 %	減衰 定数 k	初期状態 揚程 m	吐出量 m3/m	回転数	トルク
1	1	1	1	0	147.000	2.400	450.0	4	1	63.000	100.000	1475	35	.1694	147.000	2.400	1.000	1.000
2	1	1	1	0	46.000	2.400	30.0	4	1	1.960	.000	1470	55	2.8239	46.000	2.400	1.000	1.000

【 圧力線図仕様 】

管路名称	1	2	4	6	7
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【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	440.86	10.0	440.86				
2	10.0	440.86	300.0	445.00	450.0	441.59	500.0	442.50
	510.0	445.00	640.0	445.00	650.0	441.25	970.0	440.90
	1270.0	454.00	1384.0	451.63				
3	1384.0	451.63	1391.0	448.09	1418.0	445.29	1464.0	447.75
	1486.0	451.70	2035.0	494.90	2114.0	494.90	2433.0	506.80
	2691.0	494.01	3129.0	526.80	3262.0	547.92	3393.0	557.92
	3443.0	558.50						

【縦断仕様】

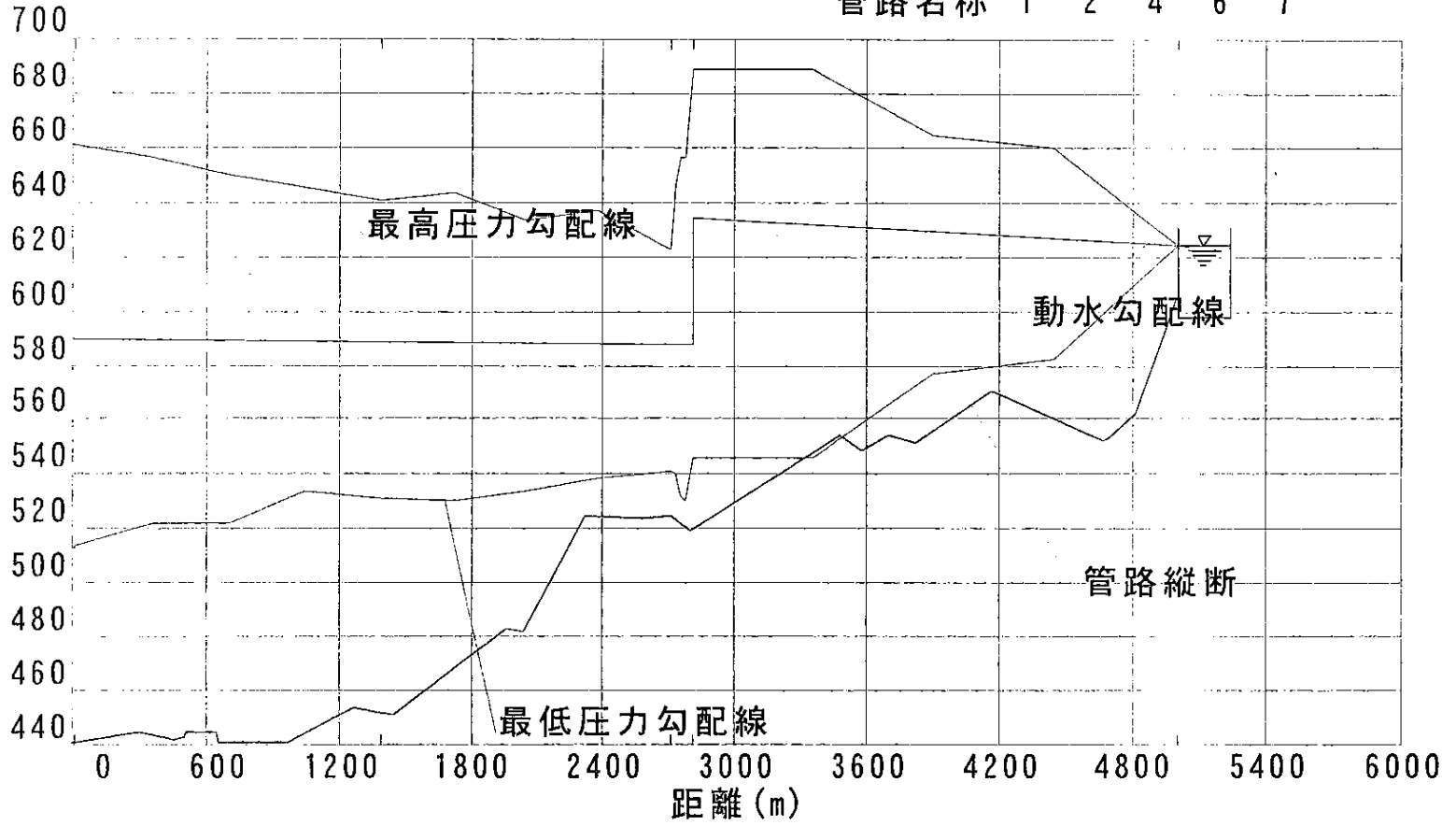
管路 名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
4	1384.0	451.63	1444.0	450.70	1958.0	483.25	2039.0	481.70
	2316.0	524.62	2586.0	524.30	2692.0	524.40		
5	2692.0	524.40	2716.0	527.03	2783.0	524.38	2833.0	535.58
	2879.0	562.98	2929.0	563.00				
6	2692.0	524.40	2702.0	524.40				
7	2702.0	524.40	2711.0	524.79	2793.0	519.34	3480.0	553.58
	3580.0	548.90	3697.0	554.22	3822.0	551.25	4172.0	570.03
	4665.0	552.25	4693.0	553.24	4809.0	562.07	4940.0	590.27
	4990.0	604.00						

レベル
(m)

ウォーターハンマ圧力勾配線図

計算番号 C2-1010-A1

管路名称 1 2 4 6 7



基準レベル 442.61

A1 Pump:

Bahiraokata Reservoir 12月 18日 16時

ウォーターハンマ計算条件

計算番号 1010A2PE

PAGE 1

ClearWaterPump(A2)Ph3

基準レベル 442.610 m
計算時間単位 .00848 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング率	上流の管路	ポンプ番号	サージタンク番号	弁番号	終点条件	管路流量 m3/m	配管損失 m	弁絞損失 m	圧力波 往復時間 sec	管路定数	分割
1	612.0	FCD3	350	6.5	1.600		1 0 0	0	0	0	3.852	2.510	.000	1.1188	9.6740	132
2	890.0	FCD3	300	6.5	1.600	1	0 0 0	0	0	0	2.118	3.360	.000	1.5786	13.5715	188
3	793.0	FCD3	250	6.0	1.600	1	0 0 0	0	0	0	1.734	.990	.000	1.3808	19.9081	164
4	100.0	FCD3	200	6.0	1.600	3	0 0 0	0	0	1	.841	.180	.000	.1679	32.2567	20
5	1785.8	FCD3	200	6.0	1.600	3	0 0 0	0	0	0	.893	1.210	.000	2.9985	32.2567	352
6	50.0	FCD3	200	6.0	1.600	5	0 0 0	0	0	1	.476	.130	.000	.0840	32.2567	10
7	10.0	FCD3	200	6.0	1.600	5	0 0 0	0	0	1	.417	.180	.000	.0168	32.2567	2
10	520.0	FCD3	300	6.5	1.600	2	0 0 0	0	0	1	2.118	1.740	.000	.9223	13.5715	108

【 ポンプ仕様 】

番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライホイール kg-m2	回転数 min-1	効率 %	減衰 定数 k	初期状態 揚程 m	吐出量 m3/m	回転数	トルク
1	1	1	1	0	104.000	3.852	90.0	4	1	8.300	20.000	1470	74	.5275	104.000	3.852	1.000	1.000

【 圧力線図仕様 】

管路名称	1	2	10	
管路名称	1	3	4	
管路名称	1	3	5	6
管路名称	1	3	5	7

【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	444.67	225.1	456.51	282.2	454.34	349.7	466.71
2	487.0	467.00	612.0	467.00	779.1	474.34	887.9	453.74
3	612.0	467.10	699.3	469.83				
	1502.0	503.85						
	612.0	467.00	833.7	476.33	1405.0	489.06		

Flywheel : 20kgf-m²

A2 . Phase 3

ウォーターハンマ計算条件

計算番号 1010A2PE

PAGE 2

【縦断仕様】

管路 名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
4	1405.0	489.06	1505.0	524.00				
5	1405.0	489.06	1872.1	493.39	2230.7	502.73	2521.9	486.26
	2672.4	497.54	2824.9	505.23	2979.8	507.98	3124.0	507.42
	3190.8	519.59						
6	3190.8	519.59	3240.8	529.00				
7	3190.8	519.59	3200.8	529.00				
10	1502.0	503.85	1510.0	503.85	1585.0	496.42	1759.0	514.59
	1805.0	513.54	1865.0	515.98	1925.0	516.47	2012.0	523.27
	2022.0	529.75						

1. 計算インターバル 14

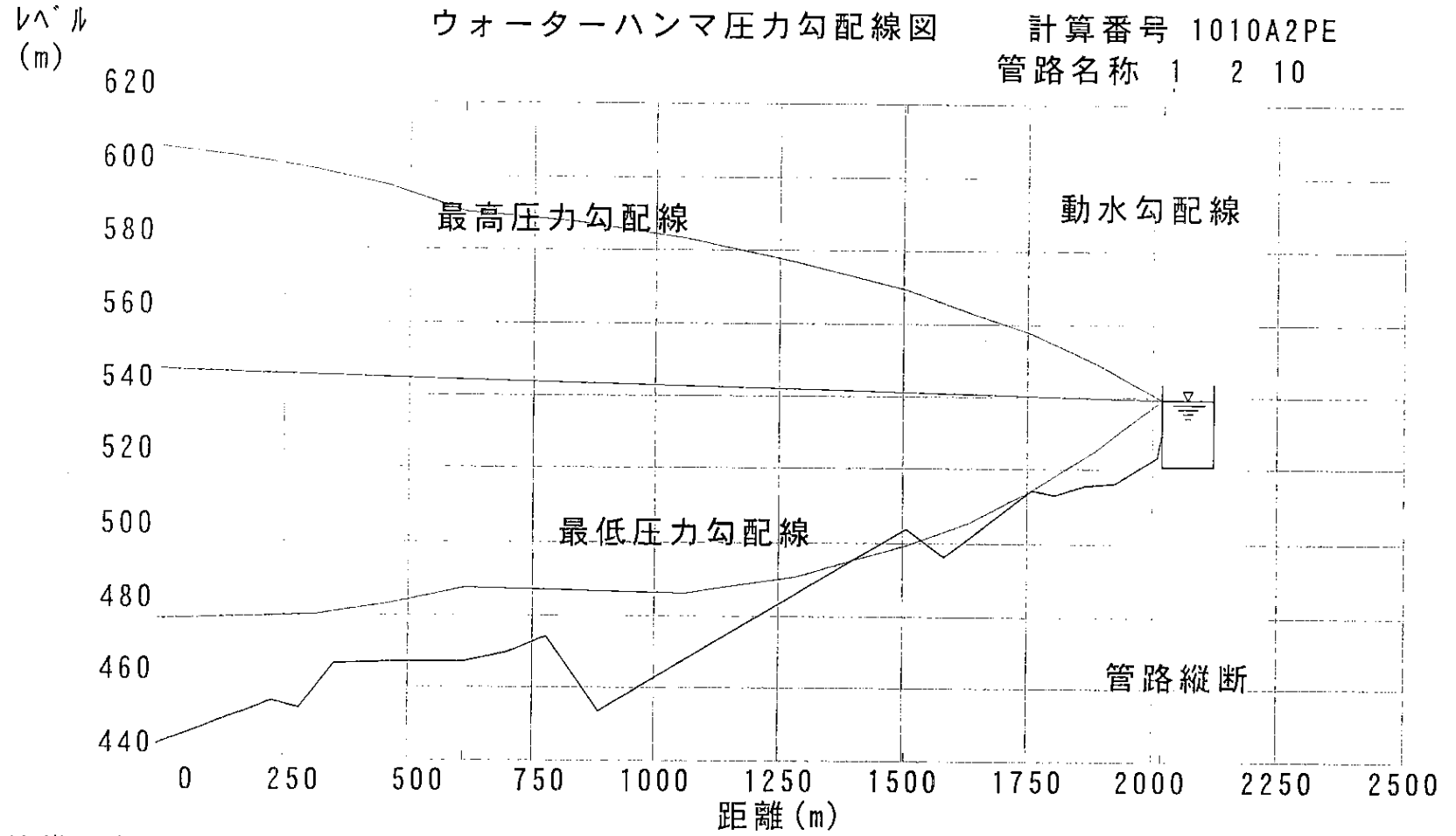
3. 管路の圧力変化

管路 番号	追加 距離 m	----- 最高圧力 -----				----- 最低圧力 -----			
		経過時間 sec	流量 m ³ /m	圧力 (水頭) m	圧力 (バル表示) m	経過時間 sec	流量 m ³ /m	圧力 (水頭) m	圧力 (バル表示) m
1	.0	5.187	.000	164.599	607.209	2.060	.001	35.860	478.470
1	153.0	5.217	.014	161.972	604.582	2.199	-.030	36.443	479.053
1	306.0	5.399	.228	158.777	601.387	2.339	-.073	37.288	479.898
1	459.0	5.268	.021	154.513	597.123	2.259	.060	40.388	482.998
2	.0	5.136	.452	147.790	590.400	2.288	.072	44.953	487.563
2	222.5	5.717	.886	145.263	587.873	2.352	.082	44.041	486.651
2	445.0	5.670	.859	140.758	583.368	2.517	.094	43.619	486.229
2	667.5	5.734	.933	134.256	576.866	2.471	.254	47.751	490.361
3	.0	5.136	-.761	147.790	590.400	2.288	-.070	44.953	487.563
3	198.3	5.573	-.155	139.278	581.888	1.945	.453	52.614	495.224
3	396.5	11.536	-.541	129.901	572.511	1.771	.663	60.891	503.501
3	594.8	11.523	-.578	120.307	562.917	8.802	-.956	72.216	514.826
4	.0	11.697	-1.092	111.239	553.849	1.593	.311	87.121	529.731
4	25.0	4.420	-2.491	108.717	551.327	1.572	.359	90.190	532.800
4	50.0	4.399	-2.535	106.269	548.879	1.551	.409	93.411	536.021
4	75.0	4.403	-2.524	103.471	546.081	1.530	.462	96.788	539.398
5	.0	11.697	.741	111.239	553.849	1.593	.686	87.121	529.731
5	446.5	4.577	.806	115.680	558.290	8.272	.742	87.315	529.925
5	892.9	4.984	.875	111.474	554.084	9.578	.652	89.532	532.142
5	1339.4	5.221	.792	113.798	556.408	6.001	.809	87.386	529.996
6	.0	5.425	.406	99.915	542.525	2.831	.459	98.187	540.797
6	10.0	5.331	.385	99.874	542.484	2.822	.459	98.176	540.786
6	20.0	5.323	.385	99.828	542.438	2.814	.460	98.182	540.792
6	30.0	5.314	.384	99.753	542.363	2.806	.461	98.239	540.849
6	40.0	5.306	.382	99.596	542.206	2.797	.465	98.453	541.063

3. 管路の圧力変化

管路 番号	追加 距離 m	----- 最高圧力 -----				----- 最低圧力 -----			
		経過時間 sec	流量 m3/m	圧力 (水頭) m	圧力 (レベル表示) m	経過時間 sec	流量 m3/m	圧力 (水頭) m	圧力 (レベル表示) m
7	.0	5.425	.464	99.915	542.525	2.831	.287	98.187	540.797
7	5.0	5.344	.390	99.514	542.124	2.835	.279	98.648	541.258
10	.0	5.899	1.140	126.555	569.165	2.272	.593	56.737	499.347
10	130.0	5.785	.911	120.243	562.852	2.157	.836	63.262	505.872
10	260.0	5.670	.710	114.780	557.390	2.043	1.152	71.660	514.270
10	390.0	5.556	.415	106.801	549.411	1.928	1.572	82.596	525.206

5-42

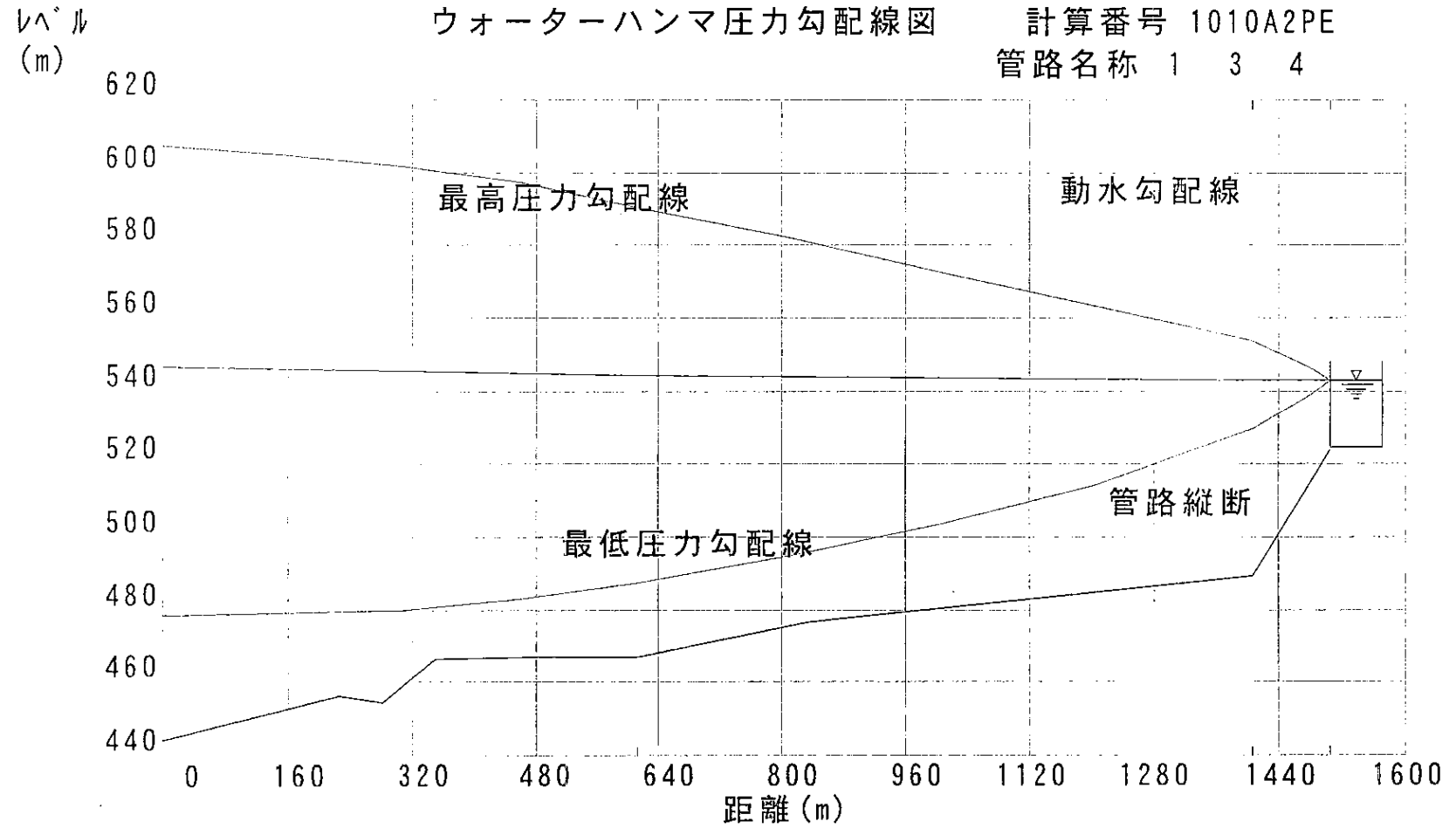


基準レベル 442.61

to Kondadeniya

Phase 3

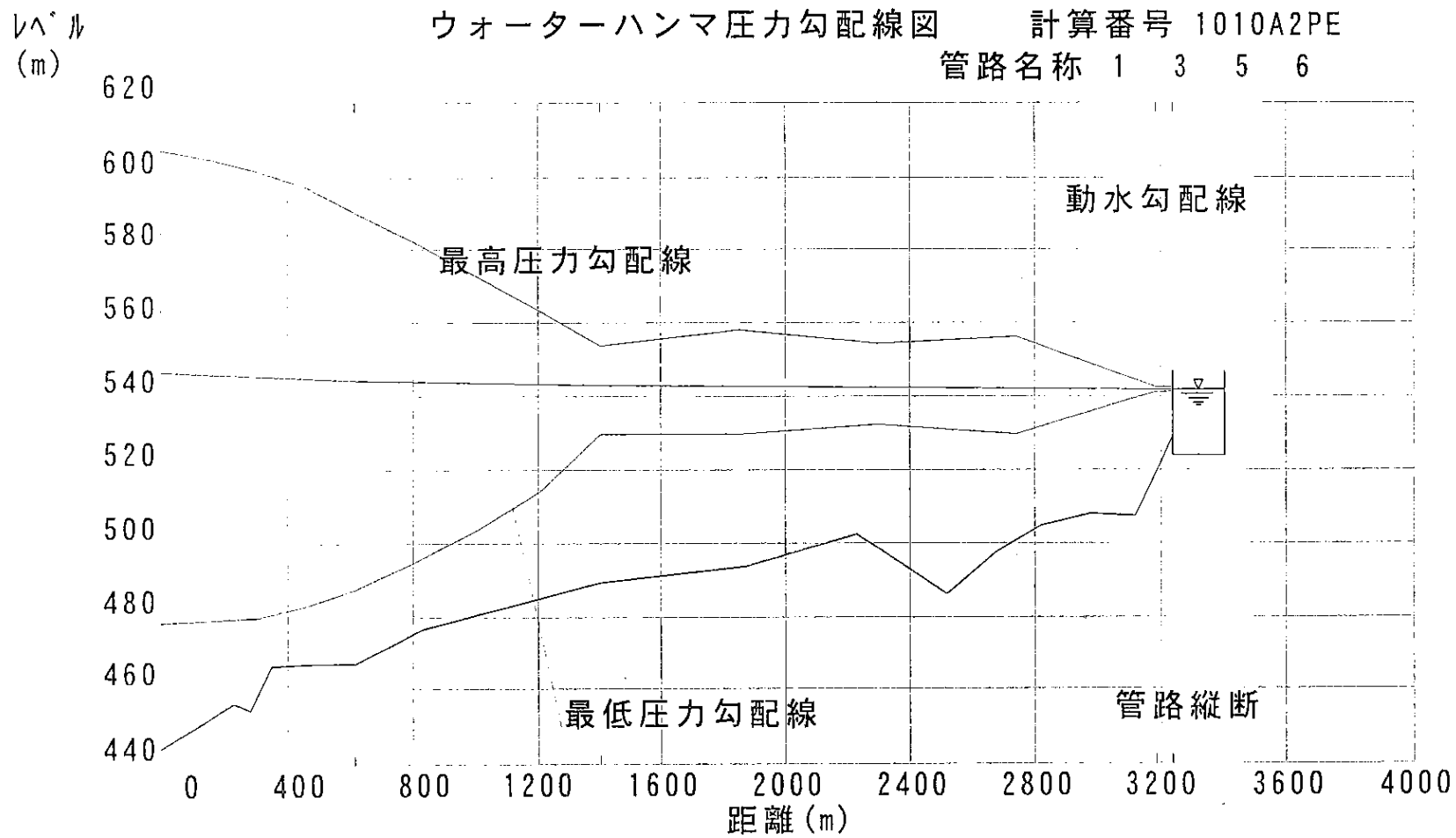
Flywheel : 20 kgf-m²



基準レベル 442.61

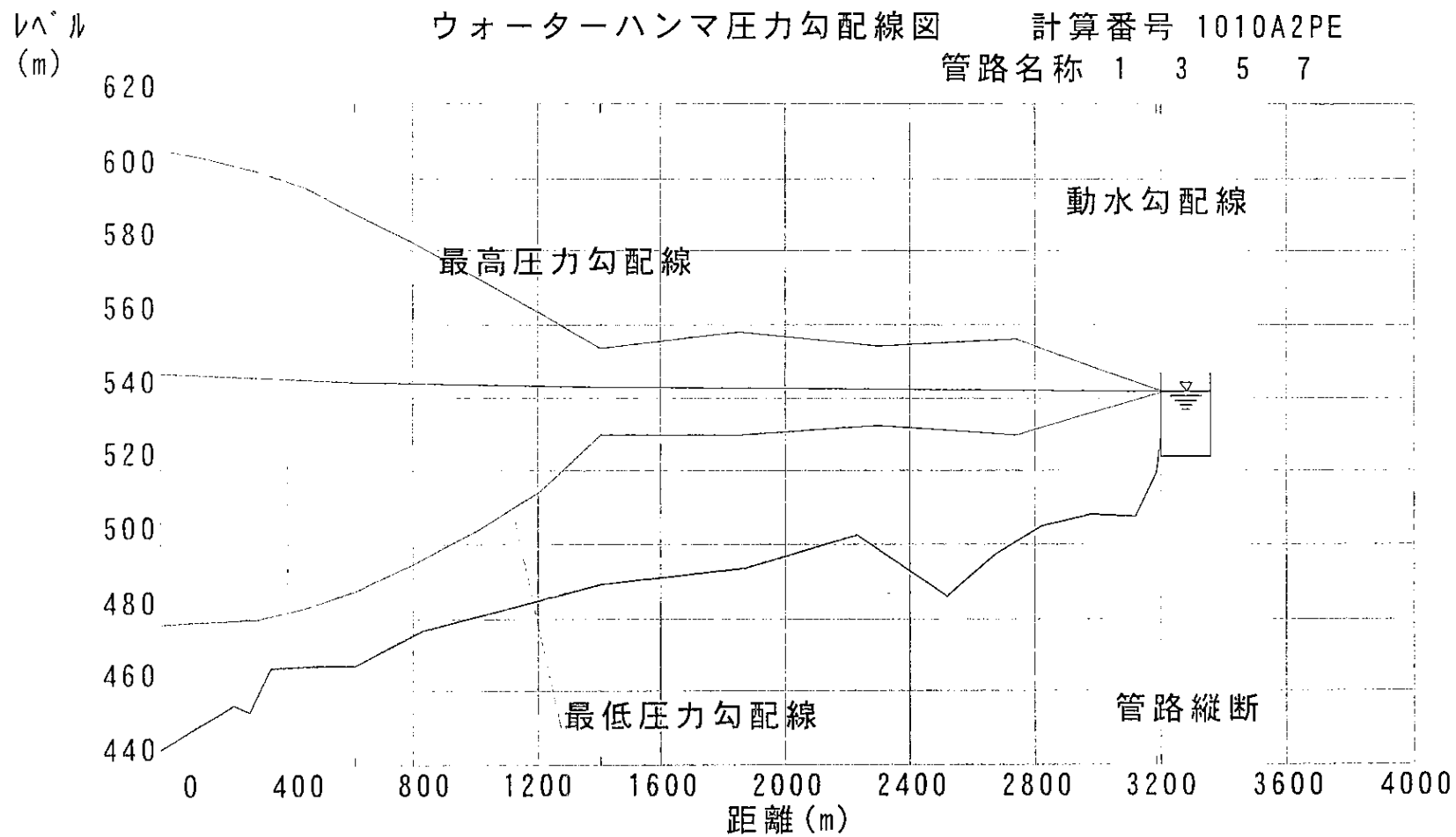
to Gohagoda (Wegiriya) Phase 3 Flywheel: 20 kgf-m²

加-3



基準レベル 442.61

to Gohagoda (New) Phase 3. Flywheel: 20kgf-m²



to Gohagoda (Old)

Phase 3.

Flywheel: 20kgf-m²

95.5

ウォーターハンマ計算条件

計算番号 C2-1010-A3

PAGE 1

Clear Water Pump (A3)

基準レベル 442.610 m
 計算時間単位 .04819 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サ-ジ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	1107.0	FCD3	600	9.0	1.600		1 0 0	0	0	0	9.989	.900	.000	2.1204	3.1419	44
2	888.0	FCD3	600	9.0	1.600	1	0 0 0	0	0	0	7.369	.400	.000	1.7009	3.1419	36
3	1783.0	FCD3	600	9.0	1.600	1	0 0 0	0	0	0	2.620	.200	.000	3.4152	3.1419	70
4	882.0	FCD3	200	6.0	1.600	2	0 0 0	0	0	1	1.166	1.400	36.000	1.4810	32.2567	30
5	3653.0	FCD3	500	8.0	1.600	2	0 0 0	0	0	0	6.203	2.900	.000	6.8950	4.5912	144
6	3541.0	FCD3	300	6.5	1.600	3	0 0 0	0	0	0	1.713	3.200	.000	6.2807	13.5715	132
7	904.0	VP 1	225	12.7	.027	3	0 0 0	0	0	1	.907	.900	7.000	4.8451	7.9846	100
8	921.0	FCD3	200	6.0	1.600	6	0 0 0	0	0	0	.732	.600	.000	1.5464	32.2567	32
10	1305.0	FCD3	250	6.0	1.600	6	0 0 0	0	0	1	.981	1.000	2.000	2.2722	19.9081	48
9	252.0	VP 1	225	12.7	.027	8	0 0 0	0	0	1	.732	.200	1.000	1.3506	7.9846	28
11	1294.0	FCD3	200	6.0	1.600	5	0 0 0	0	0	1	1.620	3.600	10.000	2.1727	32.2567	44
12	50.0	FCD3	500	8.0	1.600	5	0 0 0	0	0	1	4.583	.100	4.000	.0944	4.5912	2

【 ポンプ仕様 】

番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライール kg-m2	回転数 min-1	効率 %	減衰定数 k	初期状態 揚程 m	吐出量 m3/m	回転数	トルク
1	1	1	1	0	93.000	9.990	250.0	4	1	29.000	.000	1475	78	1.1249	93.000	9.990	1.000	1.000

【 圧力線図仕様 】

管路名称	1	3	6	10
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【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	440.86	50.0	440.86	350.0	445.00	500.0	441.59
	509.0	442.85	522.0	441.23	701.0	446.85	1107.0	442.52
2	1107.0	442.52	1366.0	443.49	1995.0	441.50		
3	1107.0	442.52	1367.0	444.57	1687.0	441.08	1906.0	445.22

6-57

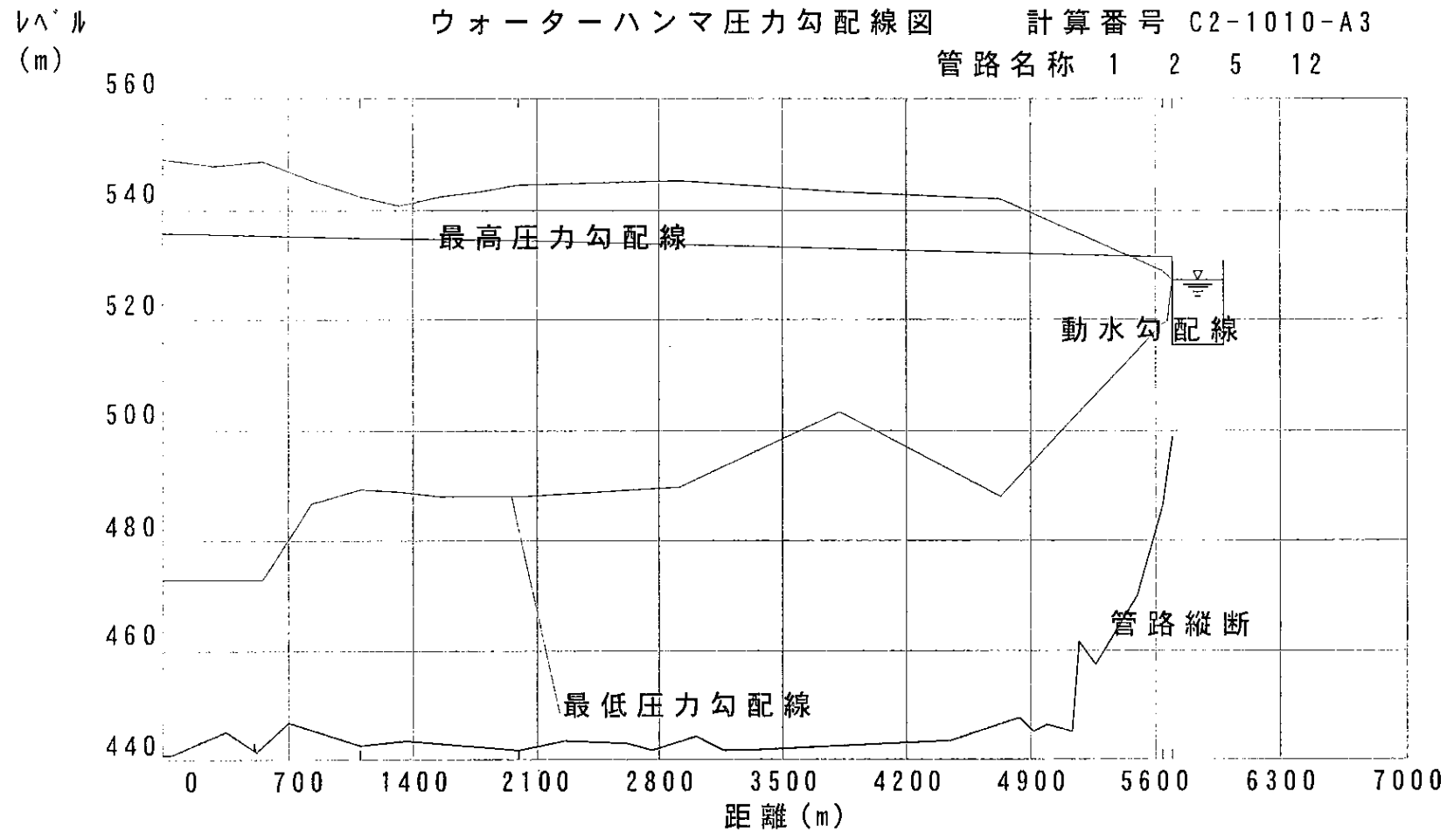
ウォーターハンマ計算条件

計算番号 C2-1010-A3

PAGE 2

【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
4	2404.0	440.54	2890.0	440.74				
	1995.0	441.50	2135.0	452.30	2276.0	455.76	2315.0	461.79
	2518.0	471.90	2639.0	465.30	2676.0	466.13	2785.0	457.89
5	2827.0	460.88	2877.0	463.50				
	1995.0	441.50	2254.0	443.33	2614.0	442.85	2750.0	441.67
	2997.0	444.30	3153.0	441.82	3293.0	441.63	4451.0	443.21
6	4837.0	447.52	4912.0	445.08	4993.0	446.47	5131.0	445.05
	5171.0	461.28	5269.0	457.12	5494.0	469.87	5648.0	486.14
	2890.0	440.74	3330.0	444.28	3509.0	443.59	3669.0	447.10
7	3770.0	445.99	3890.0	448.68	4027.0	443.86	4570.0	449.46
	5064.0	442.95	6431.0	453.72				
	2890.0	440.74	2895.0	441.42	2987.0	448.14	3053.0	449.40
8	3078.0	452.65	3231.0	460.39	3261.0	461.12	3444.0	482.80
	3525.0	486.70	3548.0	490.70	3574.0	490.83	3696.0	505.07
	3722.0	510.68	3744.0	511.70	3794.0	511.50		
9	6431.0	453.72	6485.0	454.37	6700.0	476.21	6781.0	463.97
	6836.0	464.56	6918.0	480.58	7097.0	490.81	7135.0	486.09
	7176.0	486.09	7321.0	500.53				
10	7321.0	500.53	7352.0	503.62	7420.0	499.19	7479.0	504.30
	7504.0	510.79	7604.0	517.50				
	6431.0	453.72	6602.0	456.24	6652.0	460.17	6672.0	466.20
11	6691.0	465.15	6832.0	479.26	6931.0	484.09	7109.0	506.15
	7180.0	504.74	7230.0	506.01	7300.0	500.53	7350.0	501.53
	7459.0	500.05	7516.0	503.96	7636.0	494.99	7736.0	518.50
12	5648.0	486.14	5745.0	484.10	5833.0	487.52	5921.0	484.14
	6008.0	476.10	6084.0	475.32	6162.0	485.85	6484.0	495.12
	6524.0	498.43	6627.0	490.87	6665.0	494.40	6739.0	488.58
	6832.0	496.09	6892.0	507.61	6942.0	508.50		
	5648.0	486.14	5698.0	498.50				

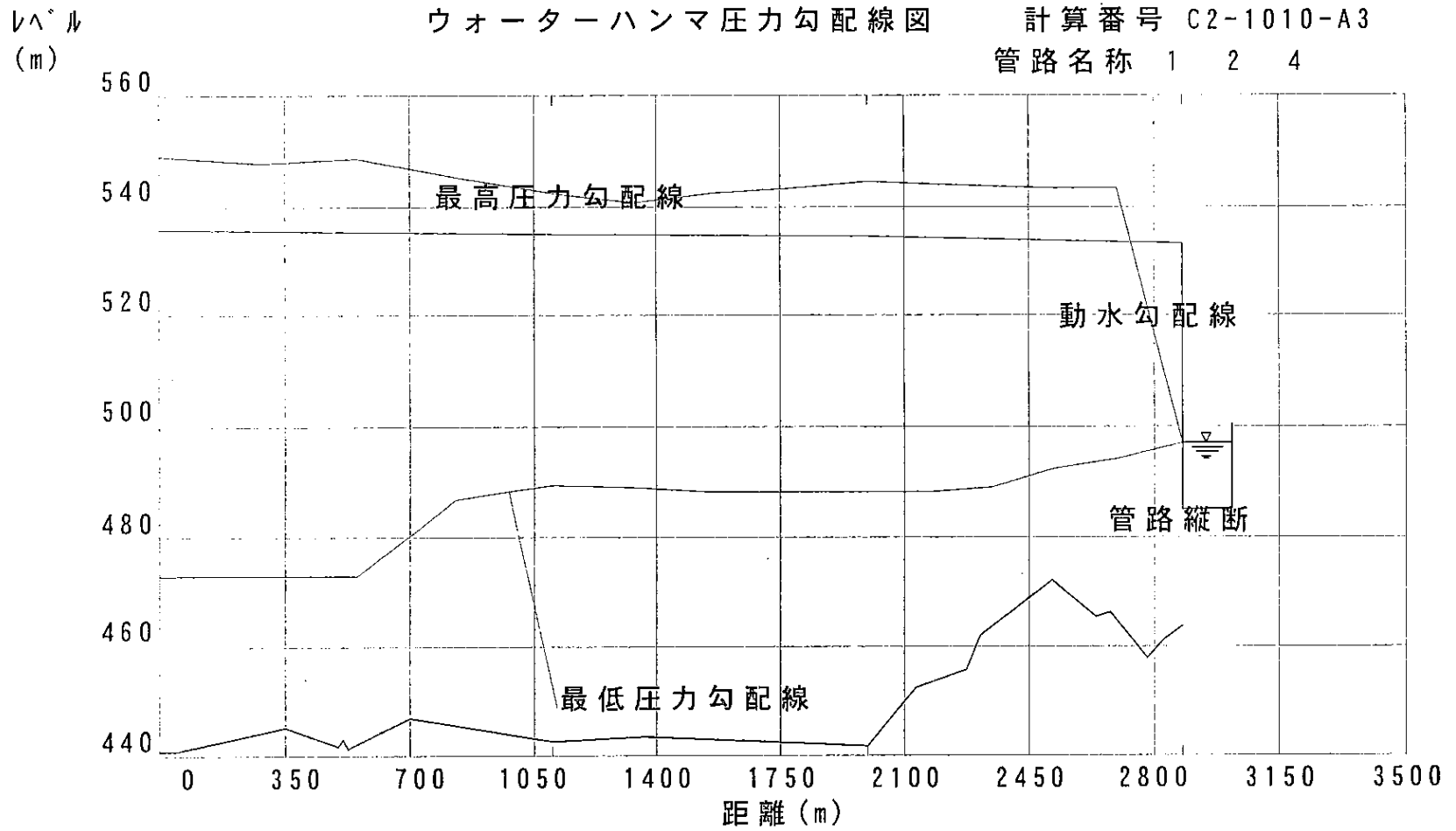


基準レベル 442.61

A3 Pump

To Kawatta Reservoir

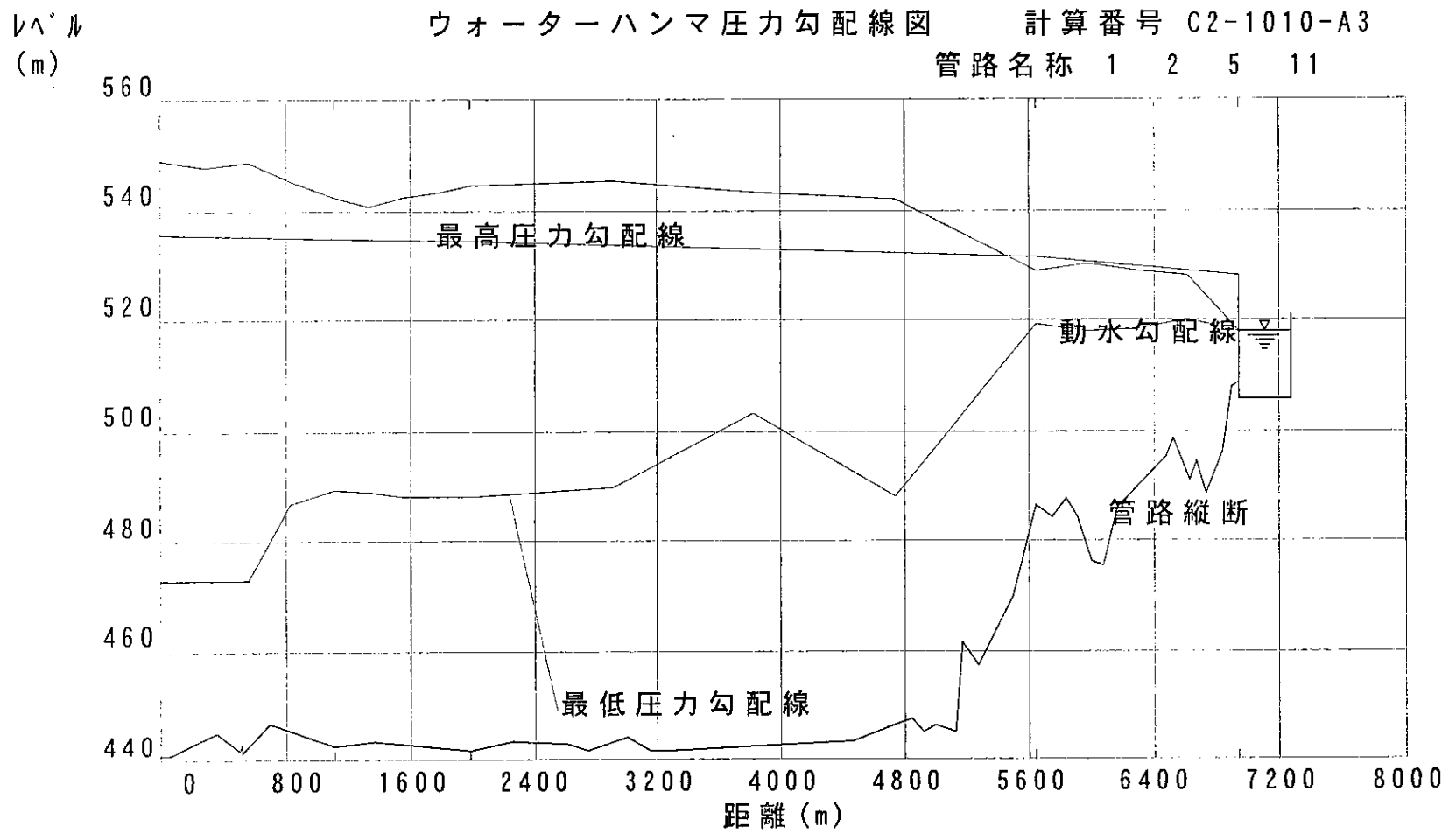
1-59



基準レベル 442.61

A3 Pump:

To Kahalla Reservoir

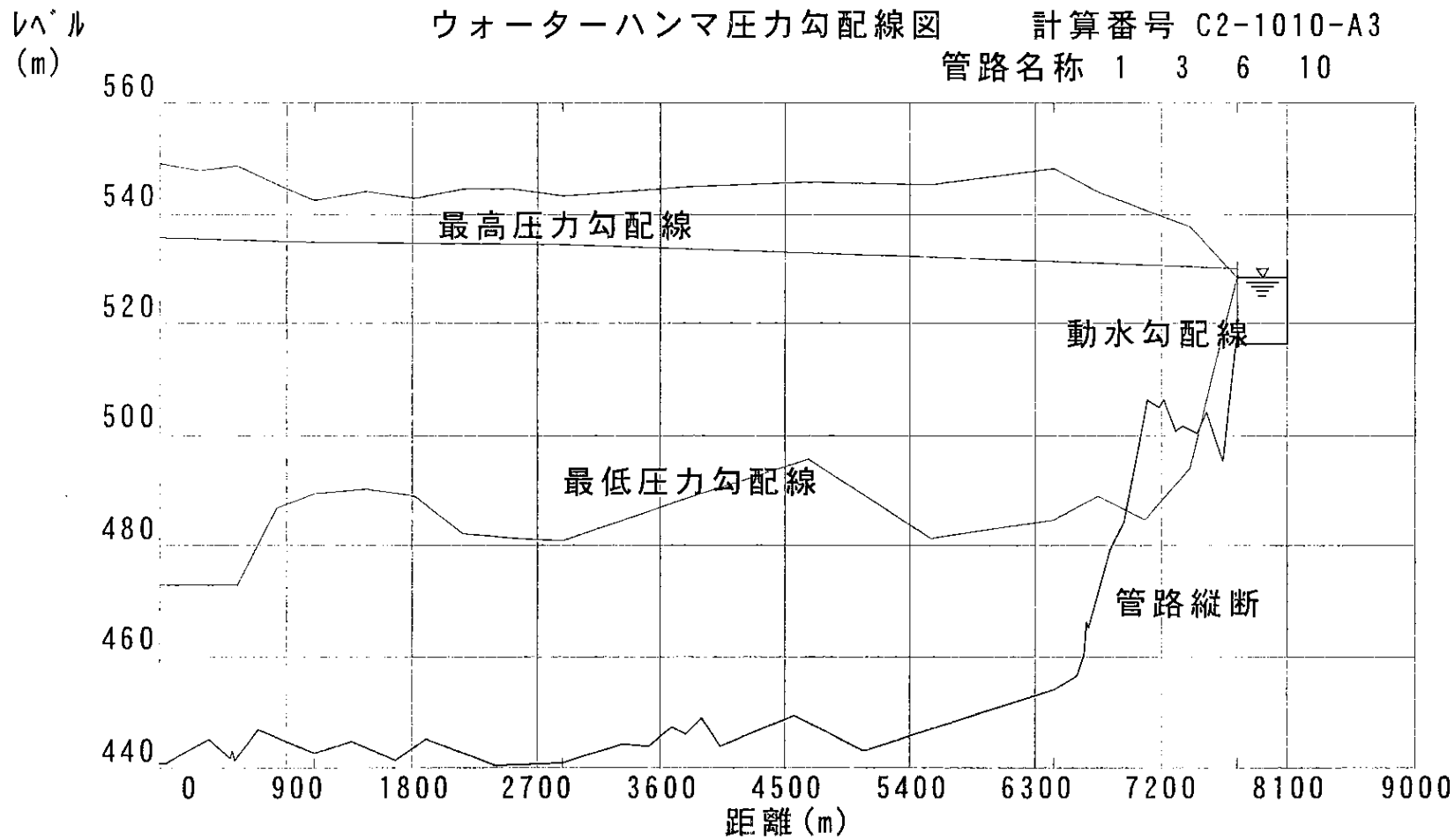


基準レベル 442.61

A3 Pump:

To Akurana Reservoir

19.7



基準レベル 442.61

A3 Pump:

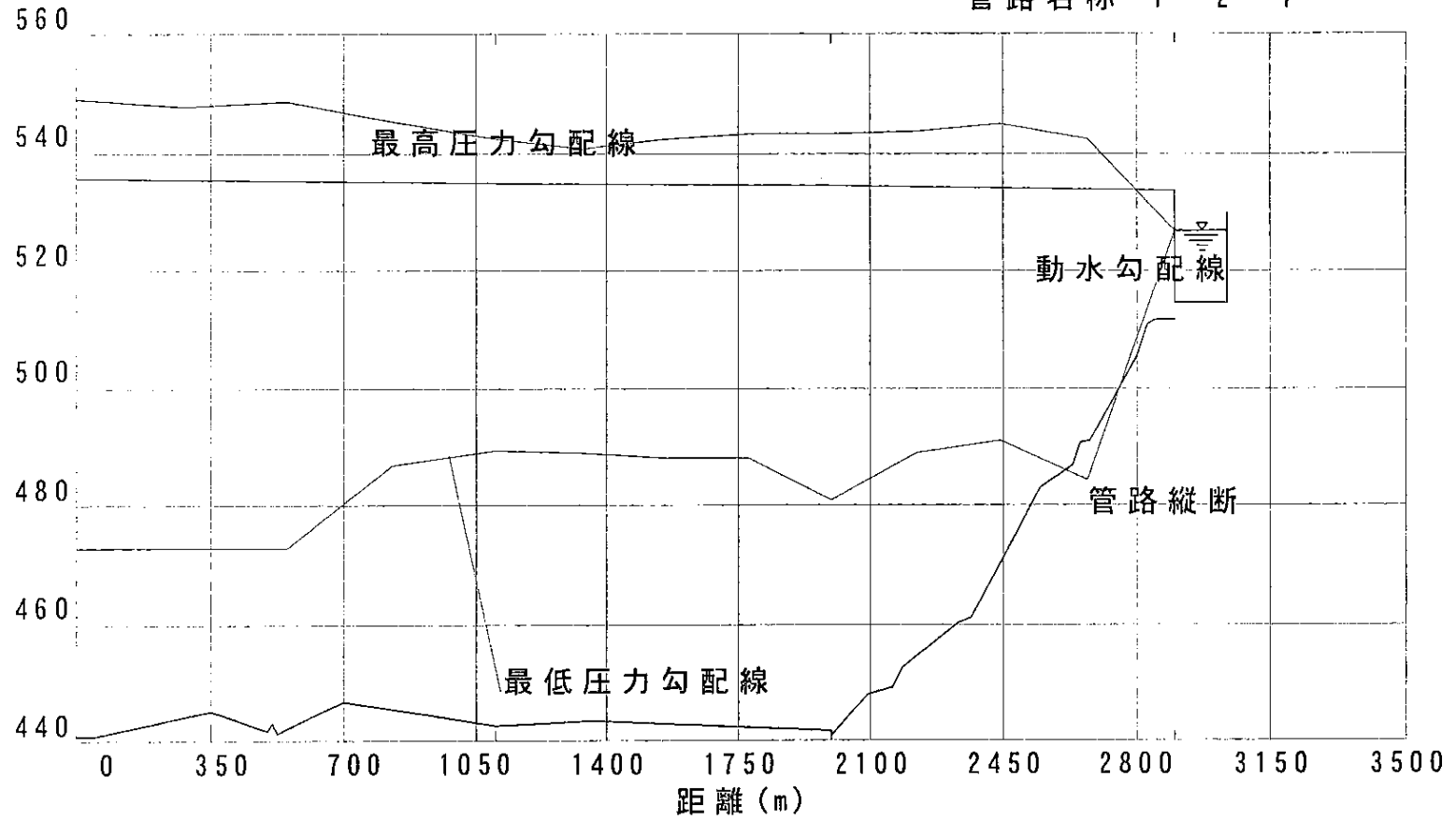
To Banjalawatta Reservoir

19.62

レベル
(m)

ウォーターハンマ圧力勾配線図

計算番号 C2-1010-A3
管路名称 1 2 7



基準レベル 442.61

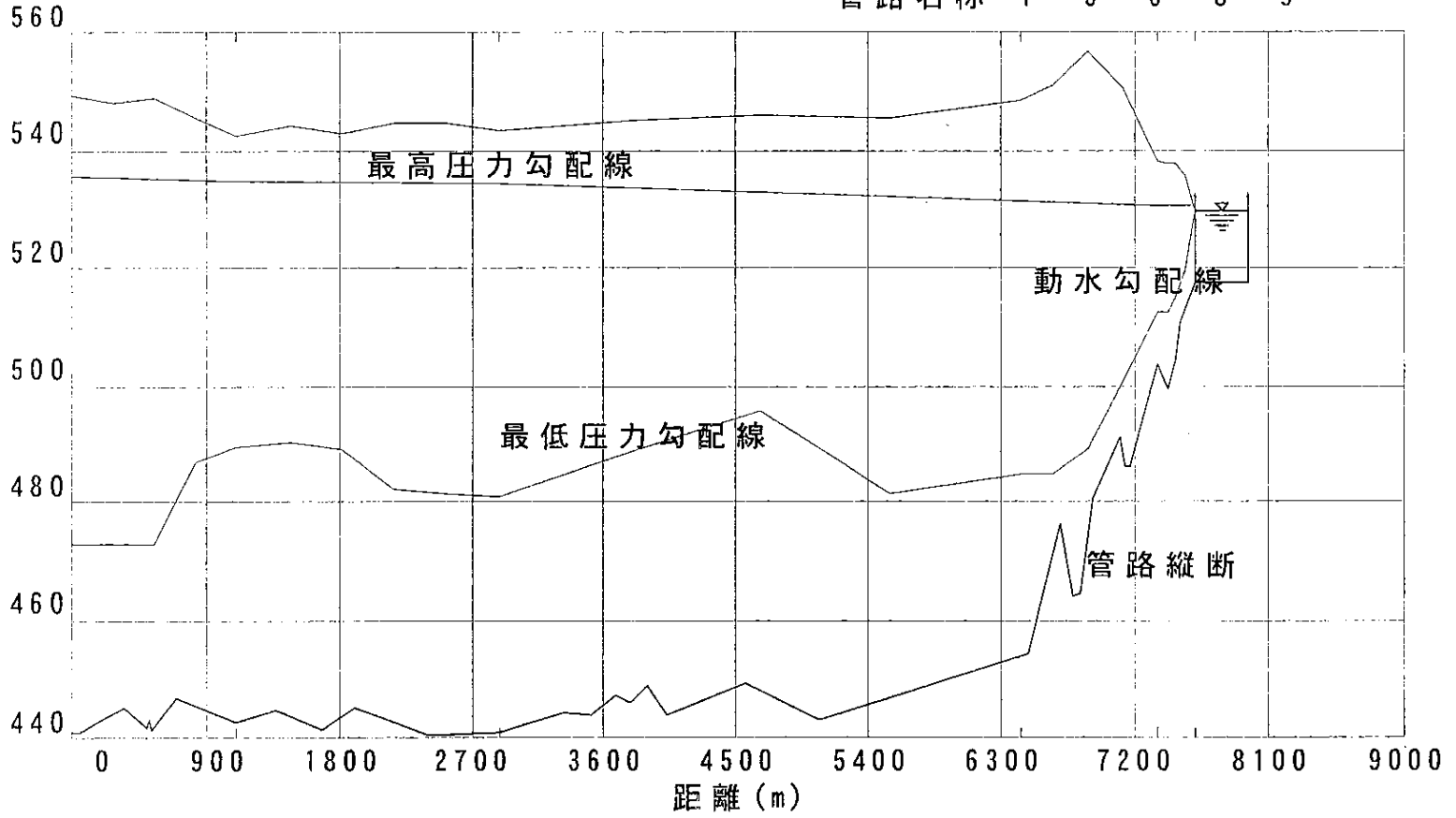
A3 pump
to Balanaga Reservoir

レベル
(m)

ウォーターハンマ圧力勾配線図

計算番号 C2-1010-A3

管路名称 1 3 6 8 9



基準レベル 442.61

A3 Pump:

To Pihladoriya Reservoir

Clear Water Pump (A3)

基準レベル 442.610 m
 計算時間単位 .04819 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	リジ タツ 番号	弁 番号	終点 条件	管路流量 m ³ /m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	1107.0	FCD3	600	9.0	1.600		1 0 0	0	0	0	9.989	.900	.000	2.1204	3.1419	44
2	888.0	FCD3	600	9.0	1.600	1	0 0 0	0	0	0	7.369	.400	.000	1.7009	3.1419	36
3	1783.0	FCD3	600	9.0	1.600	1	0 0 0	0	0	0	2.620	.200	.000	3.4152	3.1419	70
4	882.0	FCD3	200	6.0	1.600	2	0 0 0	0	0	1	1.166	1.400	36.000	1.4810	32.2567	30
5	3653.0	FCD3	500	8.0	1.600	2	0 0 0	0	0	0	6.203	2.900	.000	6.8950	4.5912	144
6	3541.0	FCD3	300	6.5	1.600	3	0 0 0	0	0	0	1.713	3.200	.000	6.2807	13.5715	132
7	904.0	VP 1	225	12.7	.027	3	0 0 0	0	0	1	.907	.900	7.000	4.8451	7.9846	100
8	921.0	FCD3	200	6.0	1.600	6	0 0 0	0	0	0	.732	.600	.000	1.5464	32.2567	32
10	1305.0	FCD3	250	6.0	1.600	6	0 0 0	0	0	1	.981	1.000	2.000	2.2722	19.9081	48
9	252.0	VP 1	225	12.7	.027	8	0 0 0	0	0	1	.732	.200	1.000	1.3506	7.9846	28
11	1294.0	FCD3	200	6.0	1.600	5	0 0 0	0	0	1	1.620	3.600	10.000	2.1727	32.2567	44
12	50.0	FCD3	500	8.0	1.600	5	0 0 0	0	0	1	4.583	.100	4.000	.0944	4.5912	2

【 ポンプ仕様 】

番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m ³ /m	出力 kw	極数	型式	ポンプ・モータ kg-m ²	万休イ・M kg-m ²	回転数 min-1	効率 %	減衰 定数 k	揚程 m	初期状態 吐出量 m ³ /m	回転数	トルク
1	1	1	1	0	93.000	9.990	250.0	4	1	29.000	50.000	1475	78	.4129	93.000	9.990	1.000	1.000

【 圧力線図仕様 】

管路名称	1	3	6	10
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【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	440.86	50.0	440.86	350.0	445.00	500.0	441.59
	509.0	442.85	522.0	441.23	701.0	446.85	1107.0	442.52
2	1107.0	442.52	1366.0	443.49	1995.0	441.50		
3	1107.0	442.52	1367.0	444.57	1687.0	441.08	1906.0	445.22

5-6F

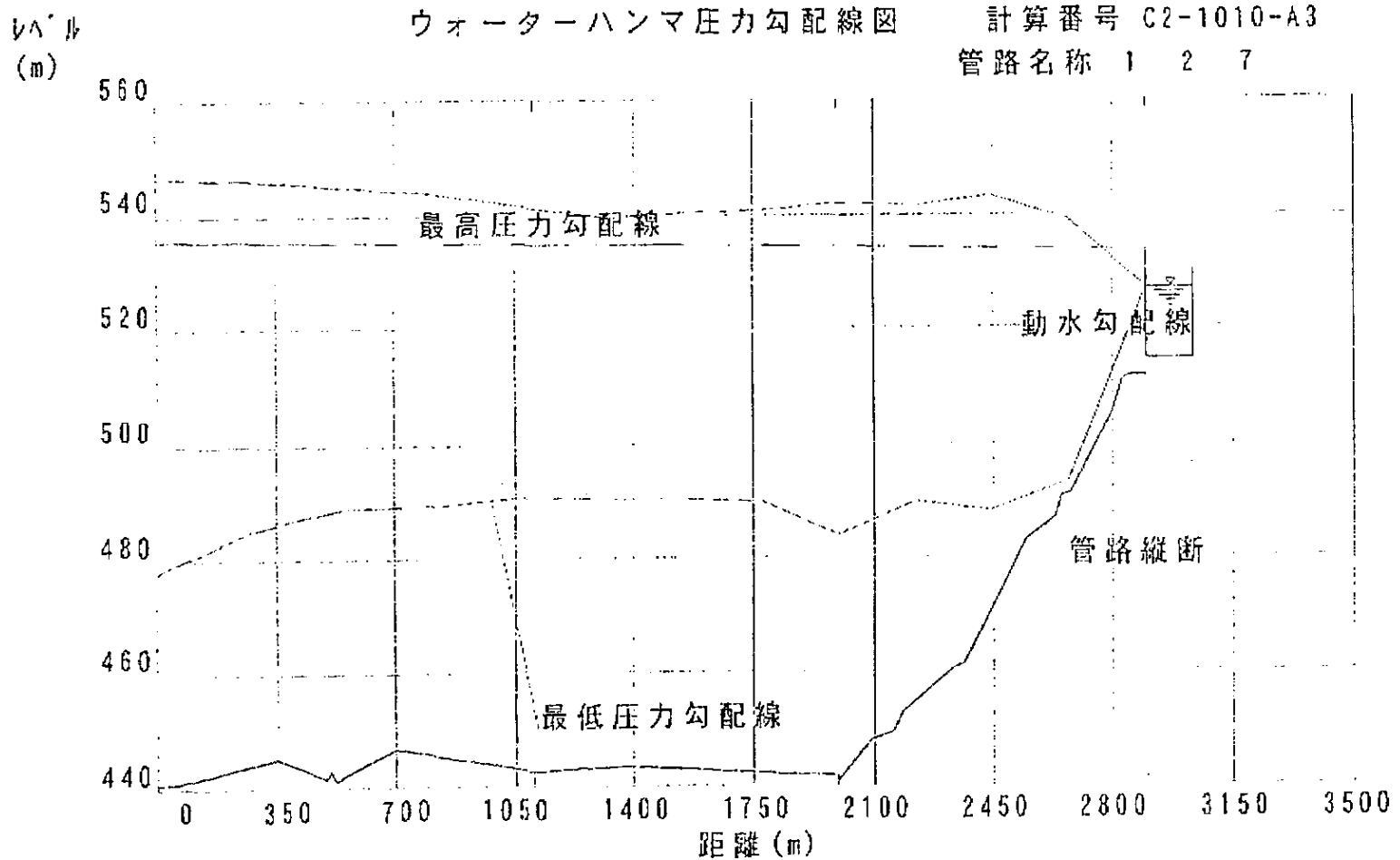
ウォーターハンマ計算条件

計算番号 C2-1010-A3

PAGE 2

【 縦断仕様 】

管路 名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
	2404.0	440.54	2890.0	440.74				
4	1995.0	441.50	2135.0	452.30	2276.0	455.76	2315.0	461.79
	2518.0	471.90	2639.0	465.30	2676.0	466.13	2785.0	457.89
	2827.0	460.88	2877.0	463.50				
5	1995.0	441.50	2254.0	443.33	2614.0	442.85	2750.0	441.67
	2997.0	444.30	3153.0	441.82	3293.0	441.63	4451.0	443.21
	4837.0	447.52	4912.0	445.08	4993.0	446.47	5131.0	445.05
	5171.0	461.28	5269.0	457.12	5494.0	469.87	5648.0	486.14
6	2890.0	440.74	3330.0	444.28	3509.0	443.59	3669.0	447.10
	3770.0	445.99	3890.0	448.68	4027.0	443.86	4570.0	449.46
	5064.0	442.95	6431.0	453.72				
7	2890.0	440.74	2895.0	441.42	2987.0	448.14	3053.0	449.40
	3078.0	452.65	3231.0	460.39	3261.0	461.12	3444.0	482.80
	3525.0	486.70	3548.0	490.70	3574.0	490.83	3696.0	505.07
	3722.0	510.68	3744.0	511.70	3794.0	511.50		
8	6431.0	453.72	6485.0	454.37	6700.0	476.21	6781.0	463.97
	6836.0	464.56	6918.0	480.58	7097.0	490.81	7135.0	486.09
	7176.0	486.09	7321.0	500.53				
9	7321.0	500.53	7352.0	503.62	7420.0	499.19	7479.0	504.30
	7504.0	510.79	7604.0	517.50				
10	6431.0	453.72	6602.0	456.24	6652.0	460.17	6672.0	466.20
	6691.0	465.15	6832.0	479.26	6931.0	484.09	7109.0	506.15
	7180.0	504.74	7230.0	506.01	7300.0	500.53	7350.0	501.53
	7459.0	500.05	7516.0	503.96	7636.0	494.99	7736.0	518.50
11	5648.0	486.14	5745.0	484.10	5833.0	487.52	5921.0	484.14
	6008.0	476.10	6084.0	475.32	6162.0	485.85	6484.0	495.12
	6524.0	498.43	6627.0	490.87	6665.0	494.40	6739.0	488.58
	6832.0	496.09	6892.0	507.61	6942.0	508.50		
12	5648.0	486.14	5698.0	498.50				

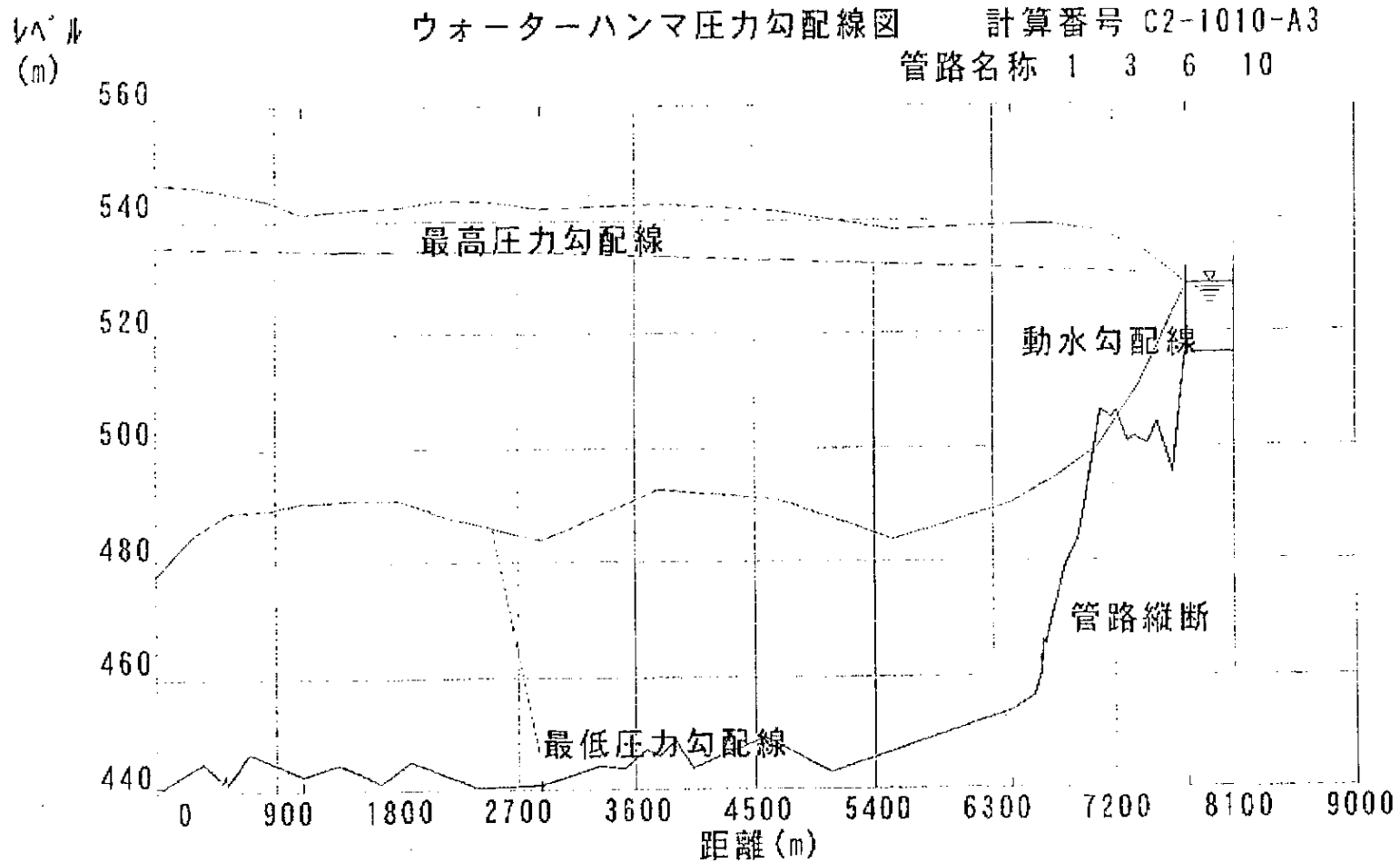


基準ハ'ル 442.61 A3 Pump:

To Calanajala Reservoir

材質: Flywheel 50mm² 取付

5-67



基準ℳℳ 442.61

A3 Pump:

To Banfalawatta Reservoir

材質: Flywheel 50 ϕ m 鋼管

ウォーターハンマ計算条件

計算番号 C2-1010-B

PAGE 1

Transmission Pump (B)

基準レベル 566.000 m
 計算時間単位 .05491 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	327.0	FCD3	200	6.0	1.600		1 0 0	0	0	0	1.900	2.600	.000	.5491	32.2567	10
2	564.0	FCD3	200	6.0	1.600	1	0 0 0	0	0	0	1.900	4.400	.000	.9470	32.2567	18
3	201.0	VP 1	225	12.7	.027	2	0 0 0	0	0	0	1.900	.800	.000	1.0773	7.9846	20
4	250.0	VP 1	225	12.7	.027	3	0 0 0	0	0	1	1.900	1.000	5.200	1.3399	7.9846	24

【 ポンプ仕様 】

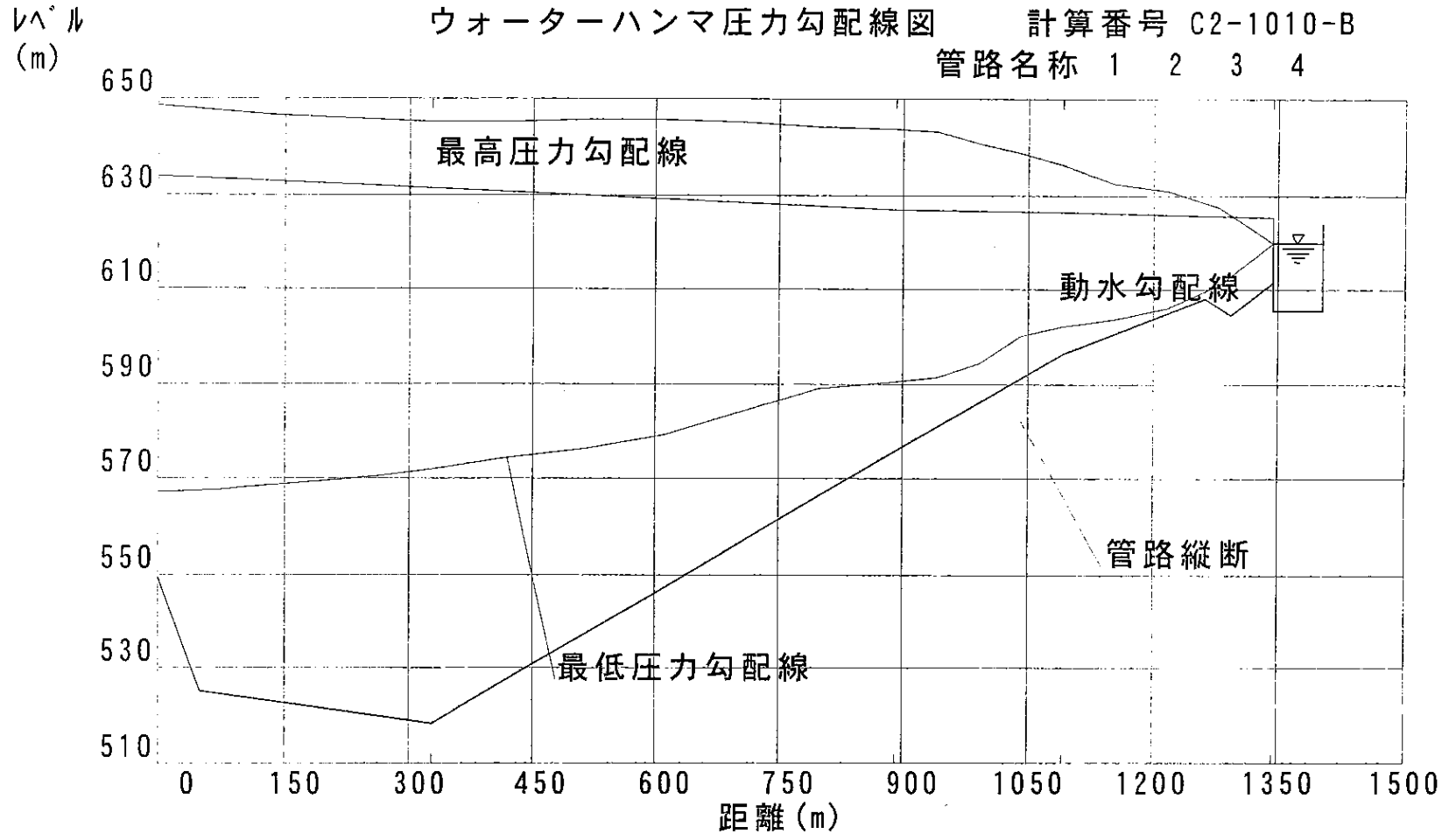
番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライール kg-m2	回転数 min-1	効率 %	減衰 定数 k	----- 初期状態 ----- 揚程 m	吐出量 m3/m	回転数	トルク
1	1	1	1	0	68.000	1.900	37.0	2	1	.850	.000	2900	69	1.5607	68.000	1.900	1.000	1.000

【 圧力線図仕様 】

管路名称	1	2	3	4

【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	549.50	50.0	525.32	327.0	518.49		
2	327.0	518.49	891.0	575.88				
3	891.0	575.88	1092.0	596.33				
4	1092.0	596.33	1261.0	608.33	1292.0	604.62	1342.0	611.50



基準レベル 566

TRANSMISSION Pump (B):

Heerasafala Low SR → Heerasafala Middle SR.

1-70

ウォーターハンマ計算条件

計算番号 C2-1010-C

PAGE 1

Transmission Pump (C)

基準レベル 613.000 m
 計算時間単位 .08880 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	110.0	FCD3	150	6.0	1.600		1 0 0	0	0	0	.490	.300	.000	.1776	59.6353	2
2	200.0	FCD3	150	6.0	1.600	1	0 0 0	0	0	0	.490	.600	.000	.3229	59.6353	4
3	350.0	VP 1	160	12.7	.027	2	0 0 0	0	0	1	.490	.600	7.500	1.6038	18.4690	18

【 ポンプ仕様 】

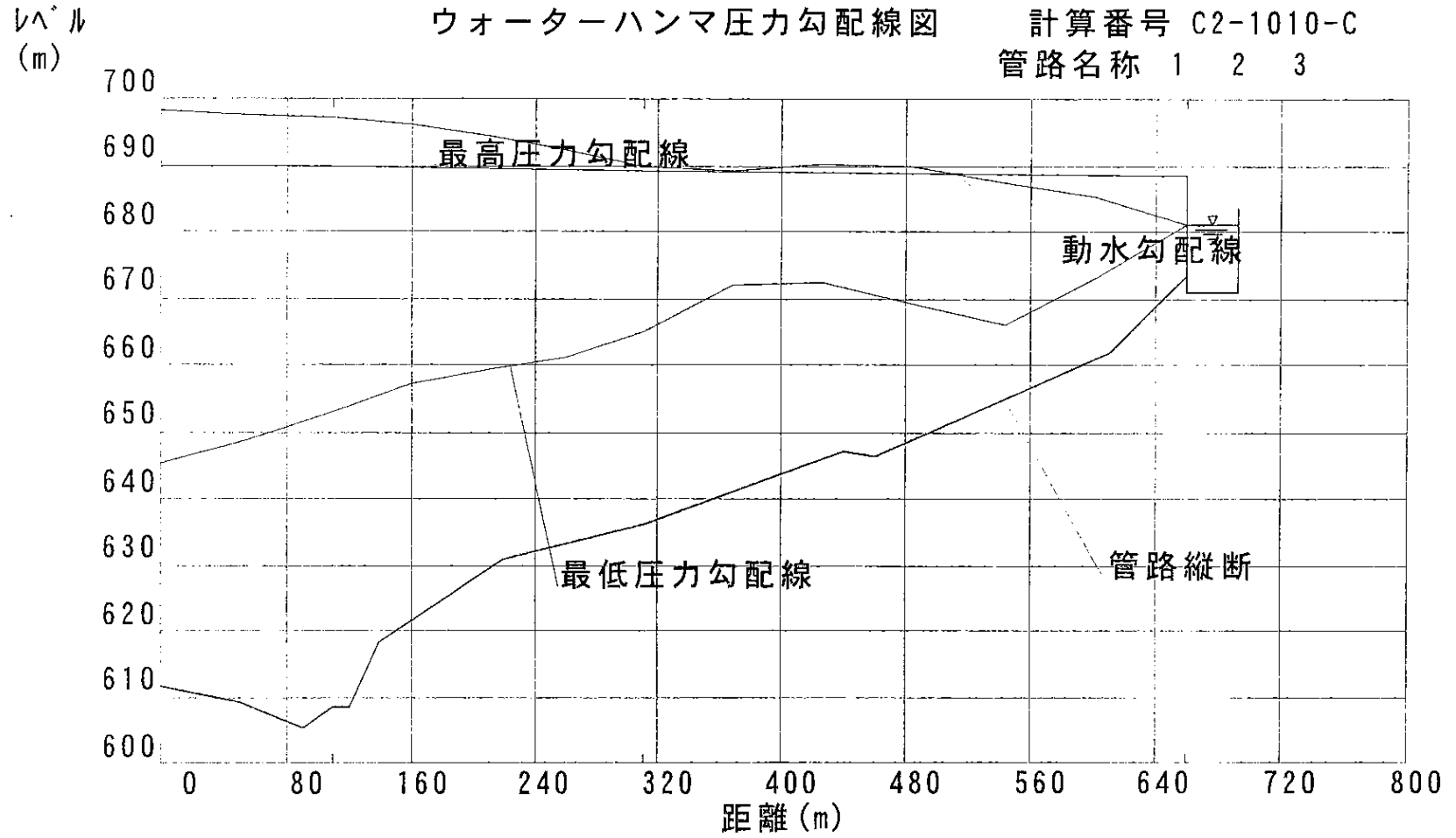
番号	台数	形式	弁 閉鎖	弁 番号	全揚程 m	吐出量 m3/m	出力 kw	極 数	型 式	ポンプ・モータ kg-m2	フライール kg-m2	回転数 min-1	効 率 %	減衰 定数 k	----- 初期状態 ----- 揚程 m	吐出量 m3/m	回転数	トルク
1	1	1	1	0	77.000	.490	18.5	2	1	.460	.000	2900	47	1.2364	77.000	.490	1.000	1.000

【 圧力線図仕様 】

管路名称	1	2	3
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【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	611.50	50.0	609.00	90.0	605.28	110.0	608.47
2	110.0	608.47	120.0	608.37	140.0	618.19	220.0	630.85
3	310.0	636.10	440.0	646.97	460.0	646.20	610.0	661.64
	660.0	673.50						



基準レベル 613

Transmission Pump (C):

Heerasafala Middle SR → Heerasafala High SR.

Transmission Pump (D1)

基準レベル 582.500 m
 計算時間単位 .05248 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タカ 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	235.0	VP 1	225	12.7	.027		1 0 0	0	0	0	.830	.200	.000	1.2595	7.9846	24
2	2774.0	FCD3	200	6.0	1.600	1	0 0 0	0	0	0	.830	4.700	.000	4.6578	32.2567	88
3	958.0	VP 1	225	12.7	.027	2	0 0 0	0	0	1	.830	.800	3.800	5.1345	7.9846	98

【 ポンプ仕様 】

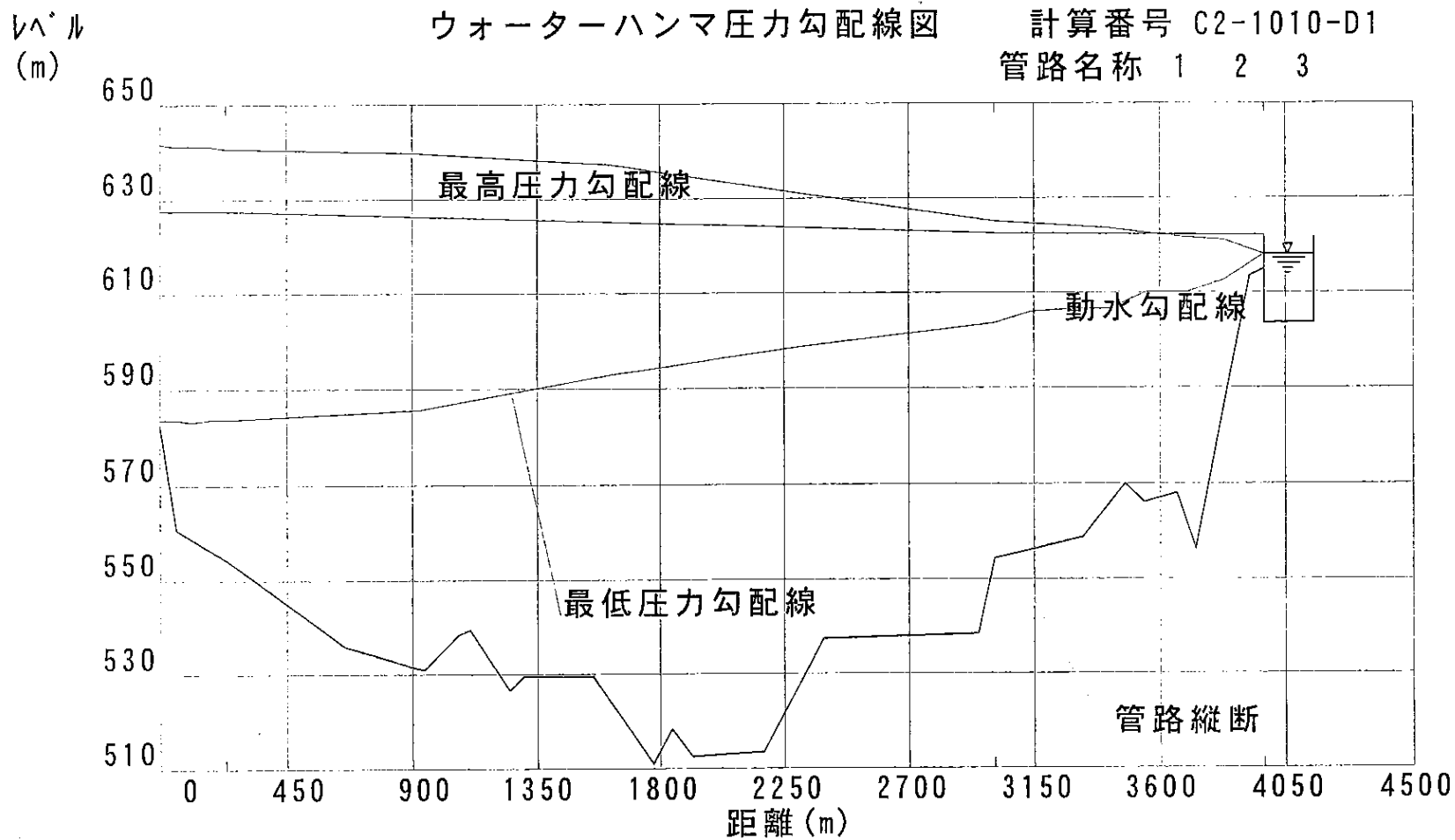
番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライール kg-m2	回転数 min-1	効率 %	減衰 定数 k	初期状態 揚程 m	吐出量 m3/m	回転数	トルク
1	1	1	1	0	45.000	.830	11.0	2	1	.270	.000	2900	66	1.4850	45.000	.830	1.000	1.000

【 圧力線図仕様 】

管路名称 1 2 3

【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	582.08	58.0	560.55	235.0	554.00		
2	235.0	554.00	662.0	536.23	940.0	531.00	1068.0	538.59
	1108.0	539.48	1250.0	526.64	1306.0	529.73	1551.0	529.79
	1767.0	510.75	1840.0	518.40	1915.0	512.30	2169.0	513.27
	2389.0	537.46	2949.0	538.39	3009.0	554.00		
3	3009.0	554.00	3330.0	558.58	3479.0	569.84	3547.0	565.77
	3657.0	568.00	3727.0	556.25	3917.0	613.50	3967.0	615.00



基準レベル 582.5

TRANSMISSION Pump (D-1) :

Ampitiya SR → Othona SR

カ-74

ウォーターハンマ計算条件

計算番号 1010D2PC

PAGE 1

Trans. P(D2) Muller Ph3

基準レベル 582.500 m
 計算時間単位 .18784 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング率	上流の管路	ポンプ番号	サージタンク番号	弁番号	終点条件	管路流量 m3/m	配管損失 m	弁絞損失 m	圧力波往復時間 sec	管路定数	分割
1	930.7	FCD3	150	6.0	1.600		1 0 0	0	0	0	.680	4.415	.000	1.5027	59.6353	8
2	961.8	FCD3	150	6.0	1.600	1	0 0 0	0	0	1	.680	4.563	3.922	1.5529	59.6353	8

【 ポンプ仕様 】

番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライホイール kg-m2	回転数 min-1	効率 %	減衰定数 k	----- 初期状態 ----- 揚程 m	吐出量 m3/m	回転数	トルク
1	1	1	1	0	146.000	.680	30.0	2	1	.541	2.000	2900	60	.4614	146.000	.680	1.000	1.000

【 圧力線図仕様 】

管路名称 1 2

【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	588.83	127.0	567.07	930.7	619.30	1108.9	629.14
	1450.0	647.84	1818.2	663.13	1892.5	705.80	1892.5	713.00

D2

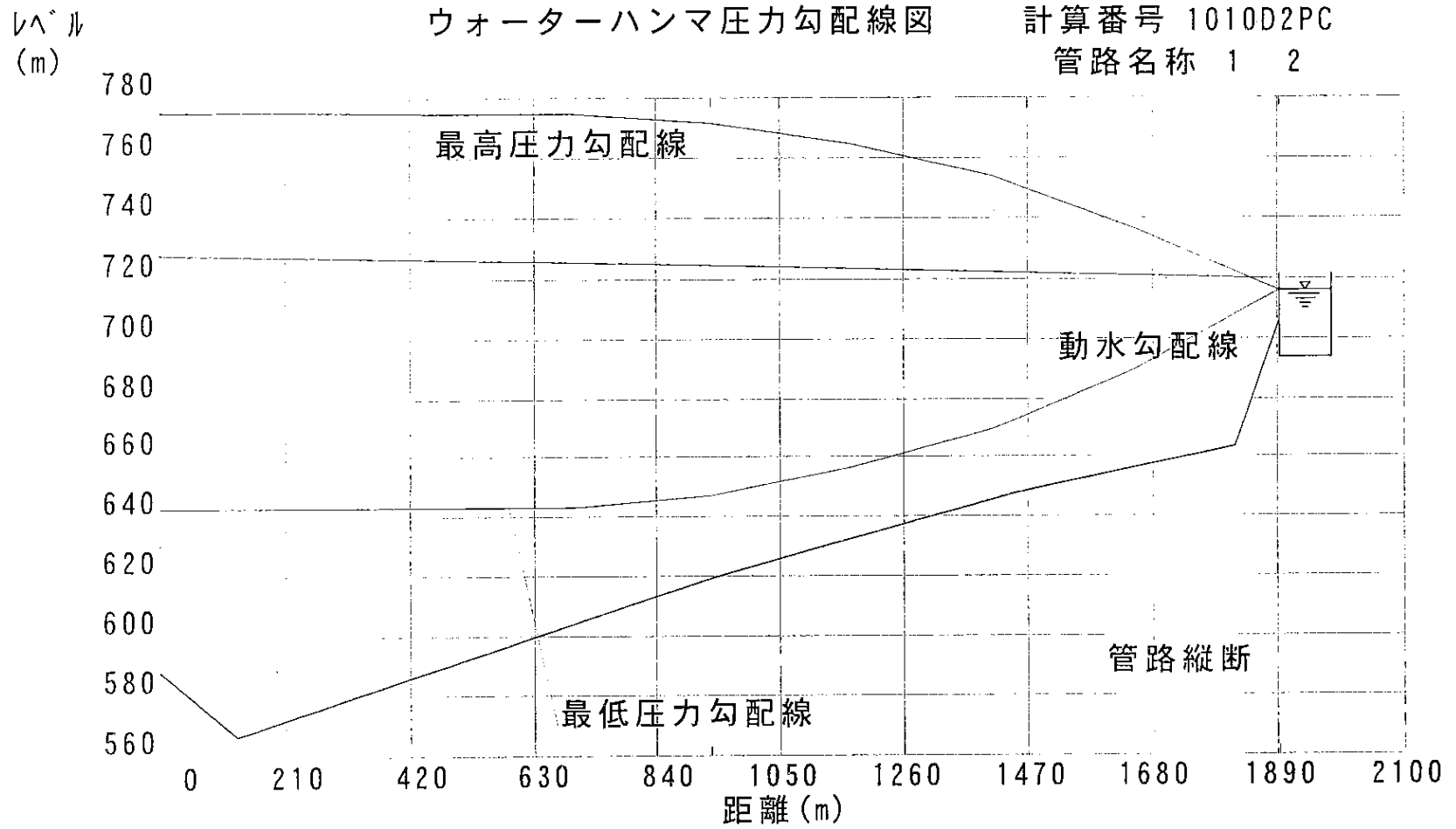
Phase 3

Flywheel : 2 kgf-m²

1. 計算インターバル 8

3. 管路の圧力変化

管路 番号	追加 距離 m	----- 最高圧力 -----				----- 最低圧力 -----			
		経過時間 sec	流量 m3/m	圧力 (水頭) m	圧力 (\sqrt{h} 表示) m	経過時間 sec	流量 m3/m	圧力 (水頭) m	圧力 (\sqrt{h} 表示) m
1	.0	5.447	.000	192.627	775.127	3.005	.000	60.492	642.992
1	232.7	5.447	.000	192.578	775.078	2.818	.000	60.549	643.049
1	465.4	5.635	.001	192.452	774.952	2.630	.002	60.733	643.233
1	698.0	5.447	-.002	192.026	774.526	2.442	.006	61.243	643.743
2	.0	5.260	-.028	188.973	771.473	2.254	.035	64.608	647.108
2	240.4	5.072	-.086	182.057	764.557	2.066	.114	74.038	656.538
2	480.9	4.884	-.179	171.169	753.669	1.878	.227	87.313	669.813
2	721.3	4.884	-.166	153.400	735.900	1.691	.398	106.798	689.298



基準レベル 582.5

D2 Phase 3 Flywheel : 2kgf-m²

4-77

ウォーターハンマ計算条件

計算番号 1010D3PA

PAGE 1

Trans. P(D3) to Meeka. R

基準レベル 582.500 m
計算時間単位 .00807 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	10.0	FCD3	150	6.0	1.600		1 0 0	0	0	0	.868	.062	.000	.0161	59.6353	2
2	465.0	FCD3	150	6.0	1.600	1	0 0 0	0	0	0	.868	2.865	.000	.7508	59.6353	92
5	1625.0	VP 1	160	12.7	.027	2	0 0 0	0	0	0	.868	7.312	.000	7.4460	18.4690	924
8	10.0	VP 1	160	12.7	.027	5	0 0 0	0	0	1	.868	.045	.000	.0458	18.4690	6

【 ポンプ仕様 】

番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライール kg-m2	回転数 min-1	効率 %	減衰 定数 k	揚程 m	初期状態 吐出量 m3/m	回転数	トルク
1	1	1	1	0	73.000	.868	37.0	2	1	.860	.000	2900	67	.7791	73.000	.868	1.000	1.000

【 圧力線図仕様 】

管路名称	1	2	5	8
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【 縦断仕様 】

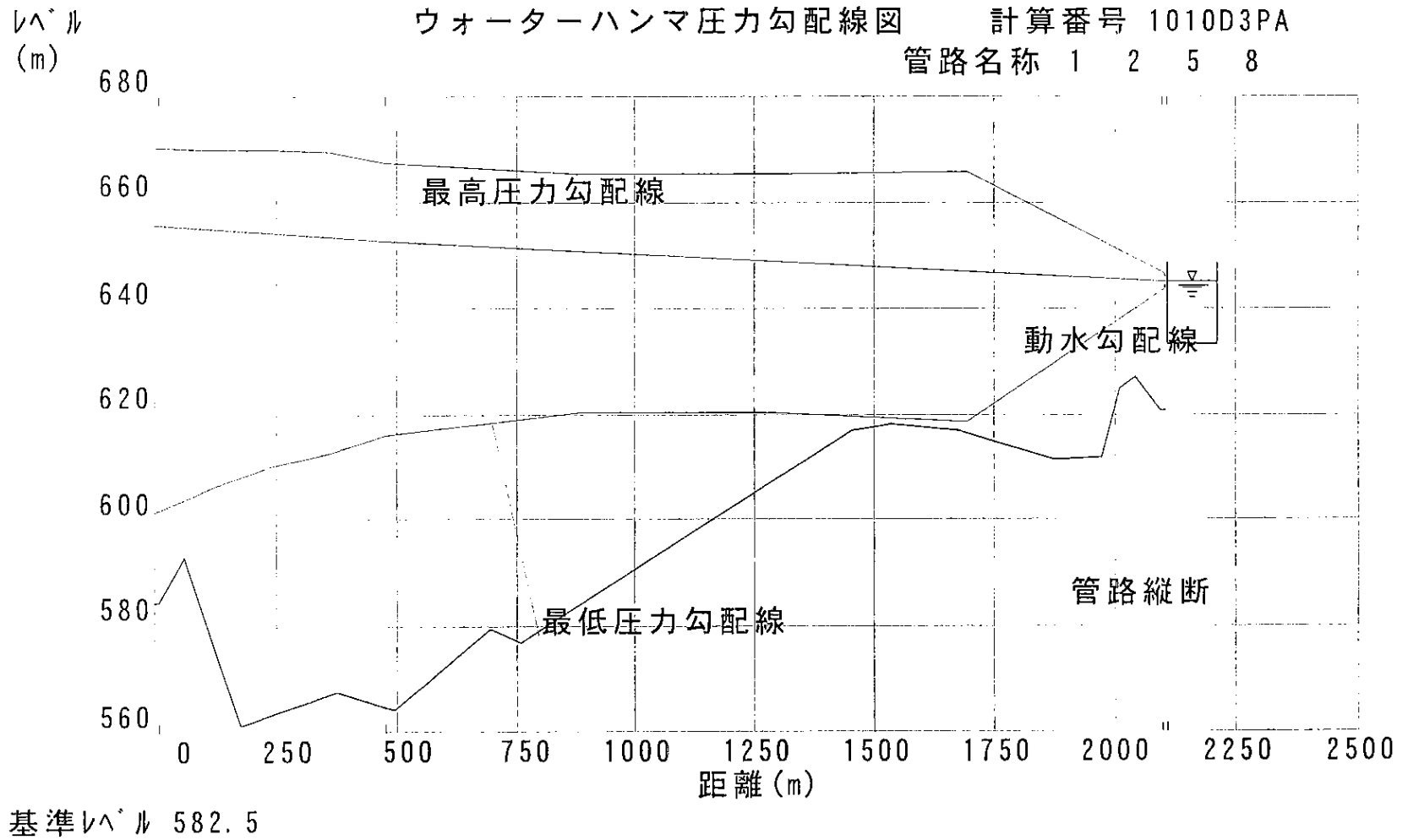
管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	584.26	10.0	584.26	60.0	592.69	175.0	561.12
	375.0	567.73	475.0	564.70	495.0	564.12	695.0	579.34
	762.0	576.85	1455.0	616.85	1535.0	618.03	1675.0	616.86
	1875.0	611.23	1975.0	611.70	2010.0	624.69	2045.0	626.86
	2095.0	620.50	2105.0	620.50				

D3 Phase 1

1. 計算インターバル 1638

3. 管路の圧力変化

管路 番号	追加 距離 m	-----最高圧力-----				-----最低圧力-----			
		経過時間 sec	流量 m3/m	圧力 (水頭) m	圧力 (バル表示) m	経過時間 sec	流量 m3/m	圧力 (水頭) m	圧力 (バル表示) m
1	.0	9.550	.000	87.700	670.200	1.631	.004	18.855	601.355
1	5.0	9.546	.000	87.700	670.200	1.643	-.002	19.095	601.595
2	.0	9.550	.000	87.699	670.199	1.647	-.004	19.330	601.830
2	116.3	9.570	.000	87.529	670.029	1.740	-.043	23.972	606.472
2	232.5	9.712	.002	87.449	669.949	1.833	-.072	27.469	609.969
2	348.8	9.619	-.003	86.903	669.403	1.925	-.095	30.217	612.717
5	.0	9.526	-.021	84.741	667.241	2.018	-.122	33.495	615.995
5	406.3	10.604	.054	82.754	665.254	6.955	.013	37.684	620.184
5	812.5	11.609	.055	82.756	665.256	6.022	.019	37.911	620.411
5	1218.8	12.598	.046	82.992	665.492	5.042	-.051	36.162	618.662
8	.0	12.424	-.264	64.209	646.709	4.158	.818	60.920	643.420
8	1.7	12.420	-.271	63.967	646.467	4.154	.826	61.208	643.708
8	3.3	12.416	-.277	63.723	646.223	4.150	.834	61.501	644.001
8	5.0	12.412	-.284	63.475	645.975	4.146	.842	61.797	644.297
8	6.7	12.408	-.291	63.225	645.725	4.141	.851	62.099	644.599
8	8.3	12.404	-.298	62.972	645.472	4.137	.859	62.404	644.904



D3 Phase 1.

ウォーターハンマ計算条件

計算番号 C2-1010-D2

PAGE 1

Transmission Pump (D2)

基準レベル 582.500 m
 計算時間単位 .03202 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	119.0	FCD3	150	6.0	1.600		1 0 0	0	0	0	.680	.600	.000	.1921	59.6353	6
2	2031.0	FCD3	150	6.0	1.600	1	0 0 0	0	0	1	.680	9.600	2.300	3.2793	59.6353	104

【 ポンプ仕様 】

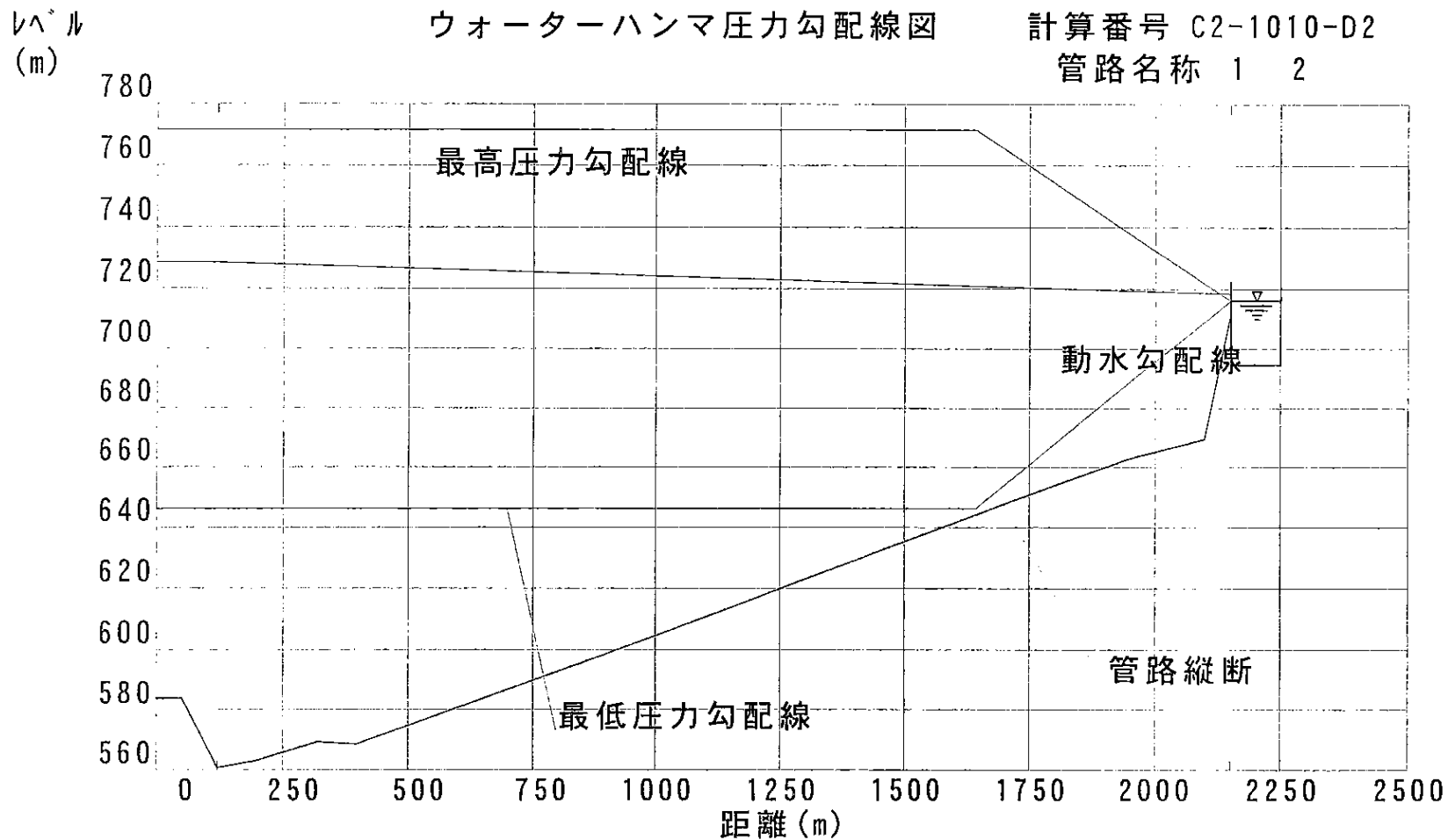
番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライホイール kg-m2	回転数 min-1	効率 %	減衰 定数 k	初期状態 揚程 m	吐出量 m3/m	回転数	トルク
1	1	1	1	0	146.000	.680	30.0	2	1	.541	.000	2900	60	2.1669	146.000	.680	1.000	1.000

【 圧力線図仕様 】

管路名称 1 2

【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	584.26	50.0	584.26	119.0	561.12		
2	119.0	561.12	200.0	562.97	320.0	568.88	398.0	568.25
	1150.0	614.37	1450.0	632.78	1940.0	662.83	2100.0	669.41
	2150.0	711.50						



基準レベル 582.5

Transmission Pump (D-2):

Amstiya SR → Muloipihalla SR

1-22

ウォーターハンマ計算条件

計算番号 C2-1010-D3

PAGE 1

Transmission Pump (D3)

基準レベル 582.500 m
 計算時間単位 .00807 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	10.0	FCD3	150	6.0	1.600		1 0 0	0	0	0	1.490	.100	.000	.0161	59.6353	2
2	355.0	FCD3	150	6.0	1.600	1	0 0 0	0	0	0	1.490	.900	.000	.5732	59.6353	72
3	355.0	FCD3	150	6.0	1.600	1	0 0 0	0	0	0	1.490	.900	.000	.5732	59.6353	72
4	355.0	FCD3	150	6.0	1.600	1	0 0 0	0	0	0	1.490	.900	.000	.5732	59.6353	72
5	1710.0	VP 1	160	12.7	.027	2	0 0 0	0	0	0	1.490	2.900	.000	7.8355	18.4690	972
6	1710.0	VP 1	160	12.7	.027	3	0 0 0	0	0	0	1.490	2.900	.000	7.8355	18.4690	972
7	1710.0	VP 1	160	12.7	.027	4	0 0 0	0	0	0	1.490	2.900	.000	7.8355	18.4690	972
8	10.0	VP 1	160	12.7	.027	5 6 7	0 0 0	0	0	1	1.490	.100	.000	.0458	18.4690	6

【 ポンプ仕様 】

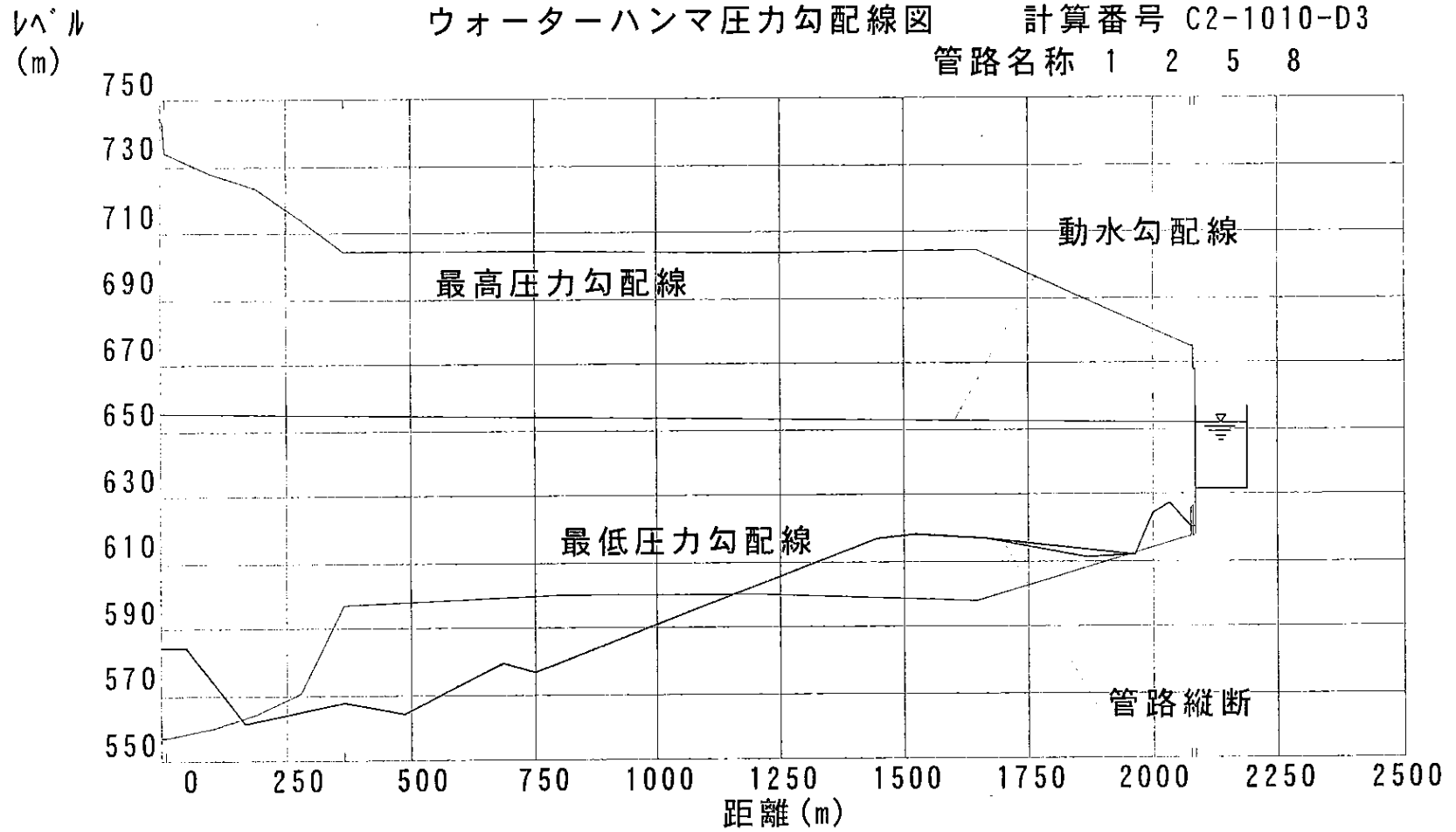
番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライール kg-m2	回転数 min-1	効率 %	減衰 定数 k	初期状態 揚程 m	吐出量 m3/m	回転数	トルク
1	1	1	1	0	73.000	1.490	37.0	2	1	.860	.000	2900	67	1.3374	73.000	1.490	1.000	1.000

【 圧力線図仕様 】

管路名称	1	2	5	8
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【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	584.26	10.0	584.26				
2	10.0	584.26	50.0	584.26	165.0	561.12	365.0	567.73
5	365.0	567.73	465.0	564.70	485.0	564.12	685.0	579.34
	752.0	576.85	1445.0	616.85	1525.0	618.03	1665.0	616.86
	1865.0	611.23	1965.0	611.70	1665.0	616.86	1965.0	611.70
	2000.0	624.69	2035.0	626.86	2075.0	620.50		
8	2075.0	620.50	2085.0	620.50				



基準レベル 582.5

Transmission Pump (D-3):

Amputiya SR → Nakamura SR

管径: 200mm

785

ウォーターハンマ計算条件

計算番号 C2-1010-D3

PAGE 1

Transmission Pump (D3)

基準レベル 582.500 m
計算時間単位 .00807 sec

Ely ashari: 15/10/02

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	10.0	FCD3	150	6.0	1.600		1 0 0	0	0	0	1.490	.100	.000	.0161	59.6353	2
2	355.0	FCD3	150	6.0	1.600	1	0 0 0	0	0	0	1.490	.900	.000	.5732	59.6353	72
3	355.0	FCD3	150	6.0	1.600	1	0 0 0	0	0	0	1.490	.900	.000	.5732	59.6353	72
4	355.0	FCD3	150	6.0	1.600	1	0 0 0	0	0	0	1.490	.900	.000	.5732	59.6353	72
5	1710.0	VP 1	160	12.7	.027	2	0 0 0	0	0	0	1.490	2.900	.000	7.8355	18.4690	972
6	1710.0	VP 1	160	12.7	.027	3	0 0 0	0	0	0	1.490	2.900	.000	7.8355	18.4690	972
7	1710.0	VP 1	160	12.7	.027	4	0 0 0	0	0	0	1.490	2.900	.000	7.8355	18.4690	972
8	10.0	VP 1	160	12.7	.027	5 6 7	0 0 0	0	0	1	1.490	.100	.000	.0458	18.4690	6

【 ポンプ仕様 】

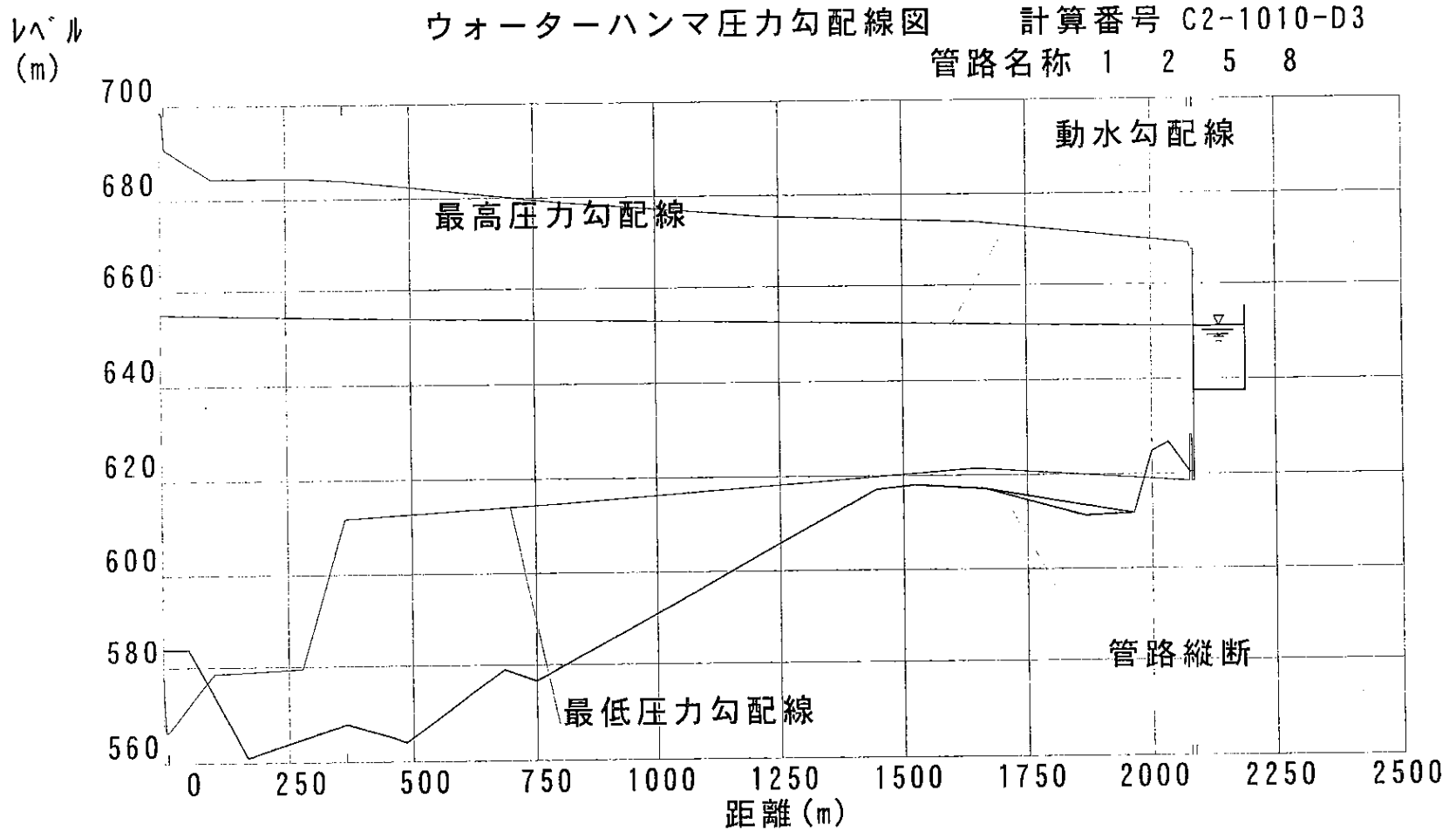
番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライール kg-m2	回転数 min-1	効率 %	減衰 定数 k	初期状態 揚程 m	吐出量 m3/m	回転数	トルク
1	1	1	1	0	73.000	1.490	37.0	2	1	.860	15.000	2900	67	.0725	73.000	1.490	1.000	1.000

【 圧力線図仕様 】

管路名称	1	2	5	8
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【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	584.26	10.0	584.26				
2	10.0	584.26	50.0	584.26	165.0	561.12	365.0	567.73
5	365.0	567.73	465.0	564.70	485.0	564.12	685.0	579.34
	752.0	576.85	1445.0	616.85	1525.0	618.03	1665.0	616.86
	1865.0	611.23	1965.0	611.70	1665.0	616.86	1965.0	611.70
	2000.0	624.69	2035.0	626.86	2075.0	620.50		
8	2075.0	620.50	2085.0	620.50				



基準レベル 582.5

Transmission Pump (D-3):

Arpitija SR → Mekanawe SR

管径 150^{mm} Flywheel 付

ウォーターハンマ計算条件

計算番号 C2-1010-E

PAGE 1

Transmission Pump (E)

基準レベル 516.000 m
計算時間単位 .04570 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	50.0	FCD3	350	6.5	1.600		1 0 0	0	0	0	5.080	.100	.000	.0914	9.6740	2
2	836.0	FCD3	350	6.5	1.600	1	0 0 0	0	0	0	5.080	2.600	.000	1.5283	9.6740	34
3	1624.0	FCD3	350	6.5	1.600	2	0 0 0	0	0	0	5.080	5.100	.000	2.9689	9.6740	64
4	1396.0	FCD3	350	6.5	1.600	3	0 0 0	0	0	1	3.750	2.500	5.700	2.5521	9.6740	56
5	949.0	FCD3	200	6.0	1.600	3	0 0 0	0	0	1	1.330	3.900	11.800	1.5935	32.2567	34

【 ポンプ仕様 】

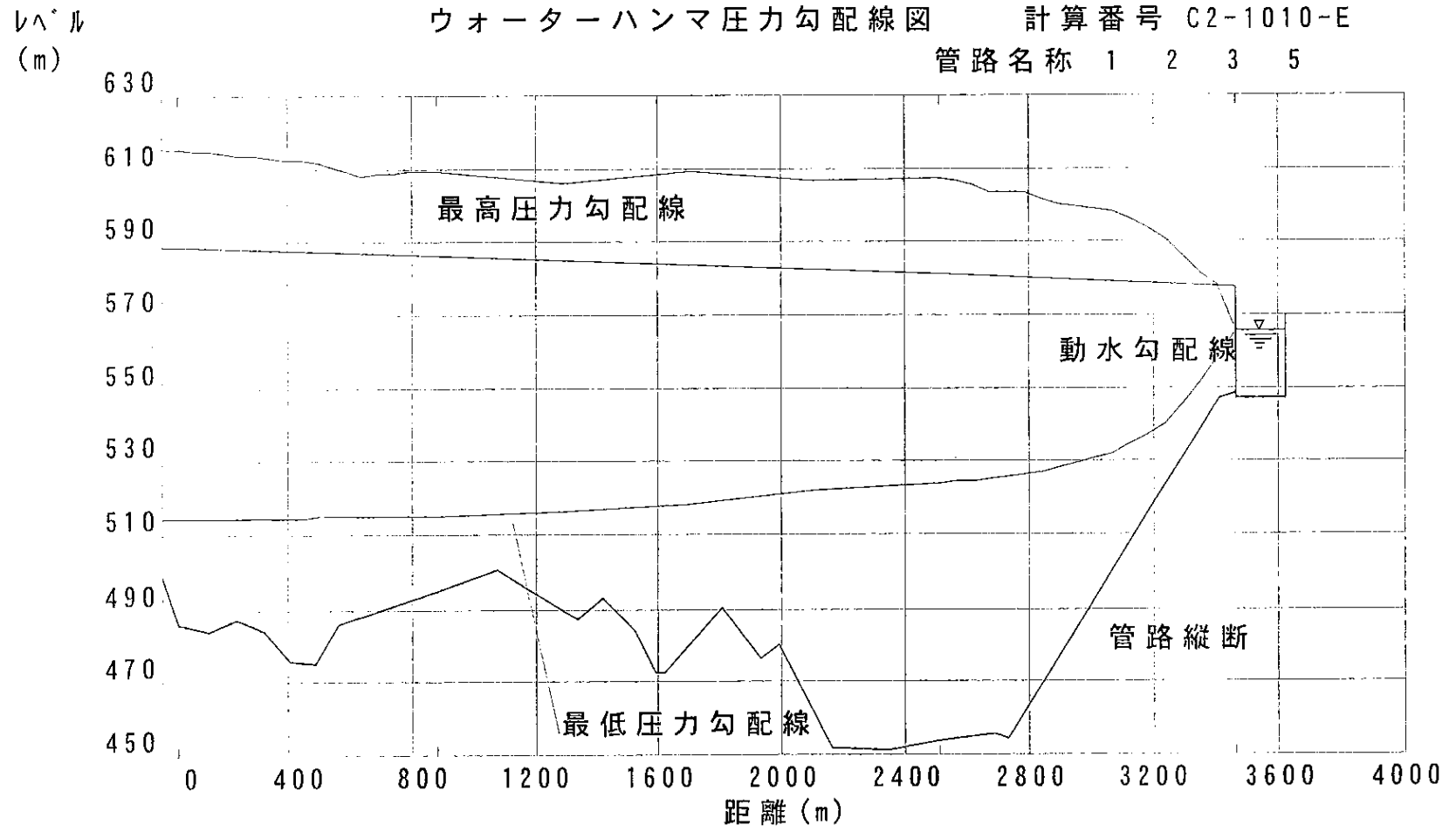
番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライール kg-m2	回転数 min-1	効率 %	減衰 定数 k	揚程 m	初期状態 吐出量 m3/m	回転数	トルク
1	2	1	1	0	73.000	2.540	55.0	2	1	.960	.000	2900	68	2.0124	73.000	2.540	1.000	1.000

【 圧力線図仕様 】

管路名称	1	2	3	4
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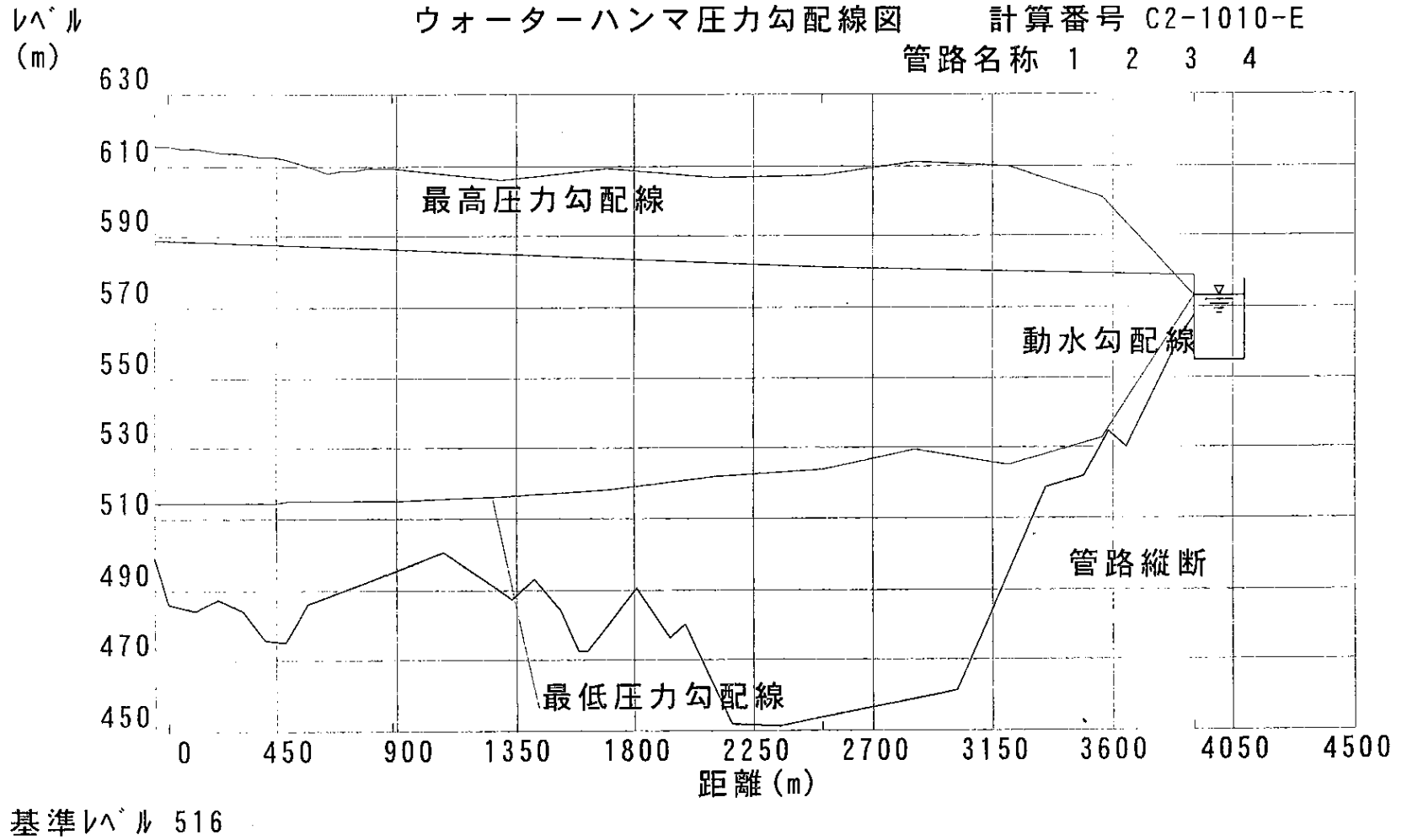
【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	498.50	50.0	486.14				
2	50.0	486.14	147.0	484.10	235.0	487.52	323.0	484.14
3	410.0	476.10	486.0	475.32	564.0	485.85	886.0	495.12
	886.0	495.12	1078.0	500.46	1333.0	487.24	1418.0	493.21
	1523.0	483.87	1586.0	473.01	1622.0	472.93	1807.0	490.55
	1932.0	476.41	1990.0	480.34	2160.0	451.89	2349.0	451.01
	2510.0	453.53						
4	2510.0	453.53	3013.0	461.30	3354.0	518.97	3492.0	522.09
	3586.0	534.91	3650.0	530.52	3856.0	561.75	3906.0	567.50
5	2510.0	453.53	2690.0	455.90	2732.0	454.58	3409.0	547.02
	3459.0	548.50						



基準レベル 516

FOR Tolambafakawatta Reservoir



For Kurufoda Reservoir

ウォーターハンマ計算条件

計算番号 C2-1010-E1

PAGE 1

Transmission Pump (E)

基準レベル 516.000 m
 計算時間単位 .04570 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	50.0	FCD3	350	6.5	1.600		1 0 0	0	0	0	5.250	.100	.000	.0914	9.6740	2
2	836.0	FCD3	350	6.5	1.600	1	0 0 0	0	0	0	5.250	2.800	.000	1.5283	9.6740	34
3	1624.0	FCD3	350	6.5	1.600	2	0 0 0	0	0	0	5.250	5.400	.000	2.9689	9.6740	64
4	1396.0	FCD3	350	6.5	1.600	3	0 0 0	0	0	1	5.250	4.700	.000	2.5521	9.6740	56

【 ポンプ仕様 】

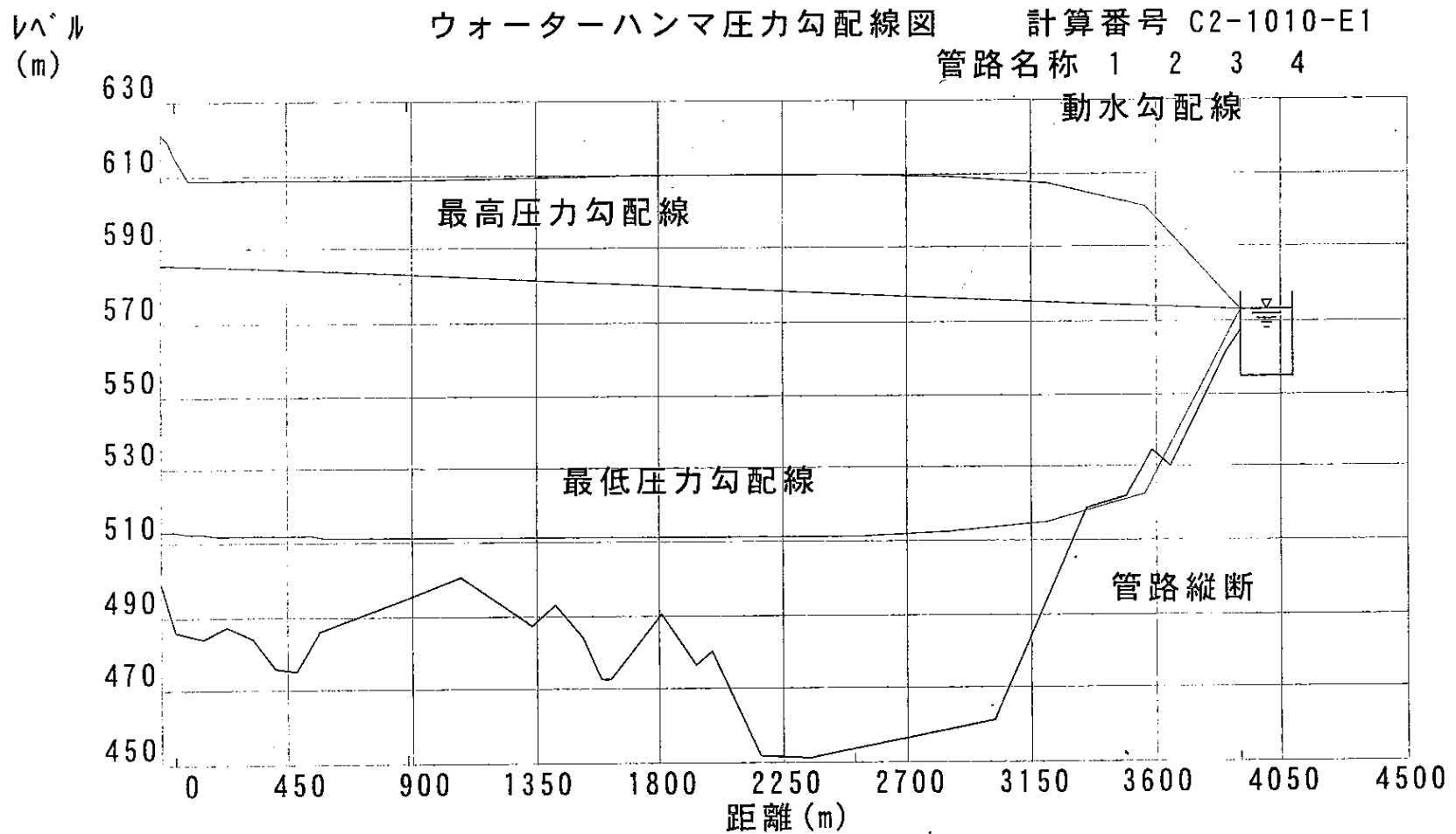
番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライール kg-m2	回転数 min-1	効率 %	減衰 定数 k	初期状態 揚程 m	吐出量 m3/m	回転数	トルク
1	2	1	1	0	70.000	2.625	55.0	2	1	.960	.000	2900	67	2.0240	70.000	2.625	1.000	1.000

【 圧力線図仕様 】

管路名称	1	2	3	4
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【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	498.50	50.0	486.14				
2	50.0	486.14	147.0	484.10	235.0	487.52	323.0	484.14
	410.0	476.10	486.0	475.32	564.0	485.85	886.0	495.12
3	886.0	495.12	1078.0	500.46	1333.0	487.24	1418.0	493.21
	1523.0	483.87	1586.0	473.01	1622.0	472.93	1807.0	490.55
	1932.0	476.41	1990.0	480.34	2160.0	451.89	2349.0	451.01
	2510.0	453.53						
4	2510.0	453.53	3013.0	461.30	3354.0	518.97	3492.0	522.09
	3586.0	534.91	3650.0	530.52	3856.0	561.75	3906.0	567.50
5	2510.0	453.53	2690.0	455.90	2732.0	454.58	3409.0	547.02
	3459.0	548.50						



基準レベル 516

For Kubota Reservoir of 10/12

5-91

ウォーターハンマ計算条件

計算番号 C2-1010-F

PAGE 1

Transmission Pump (F)

基準レベル 549.490 m
 計算時間単位 .06786 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	970.0	FCD3	200	6.0	1.600		1 0 0	0	0	1	4.100	3.400	.000	1.6287	32.2567	24

【 ポンプ仕様 】

番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライール kg-m2	回転数 min-1	効率 %	減衰 定数 k	揚程 m	吐出量 m3/m	初期状態 回転数	トルク
1	1	1	1	0	102.000	1.360	55.0	2	1	1.440	.000	2900	58	1.1767	102.000	1.360	1.000	1.000

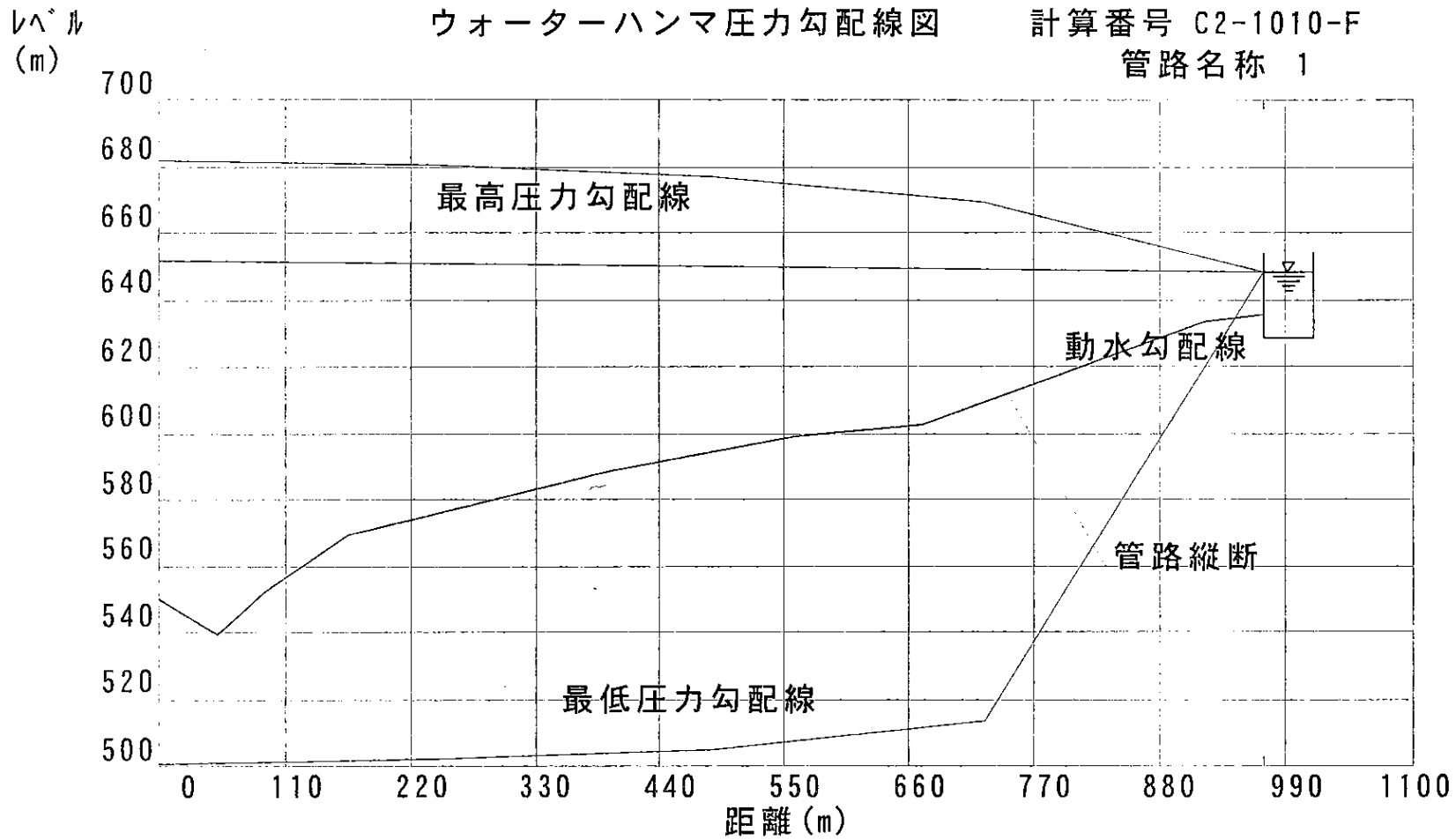
【 圧力線図仕様 】

管路名称 1

【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	549.50	50.0	539.49	91.0	552.24	164.0	569.40
	397.0	588.57	559.0	599.15	672.0	602.37	920.0	633.36
	970.0	635.30						

5-92

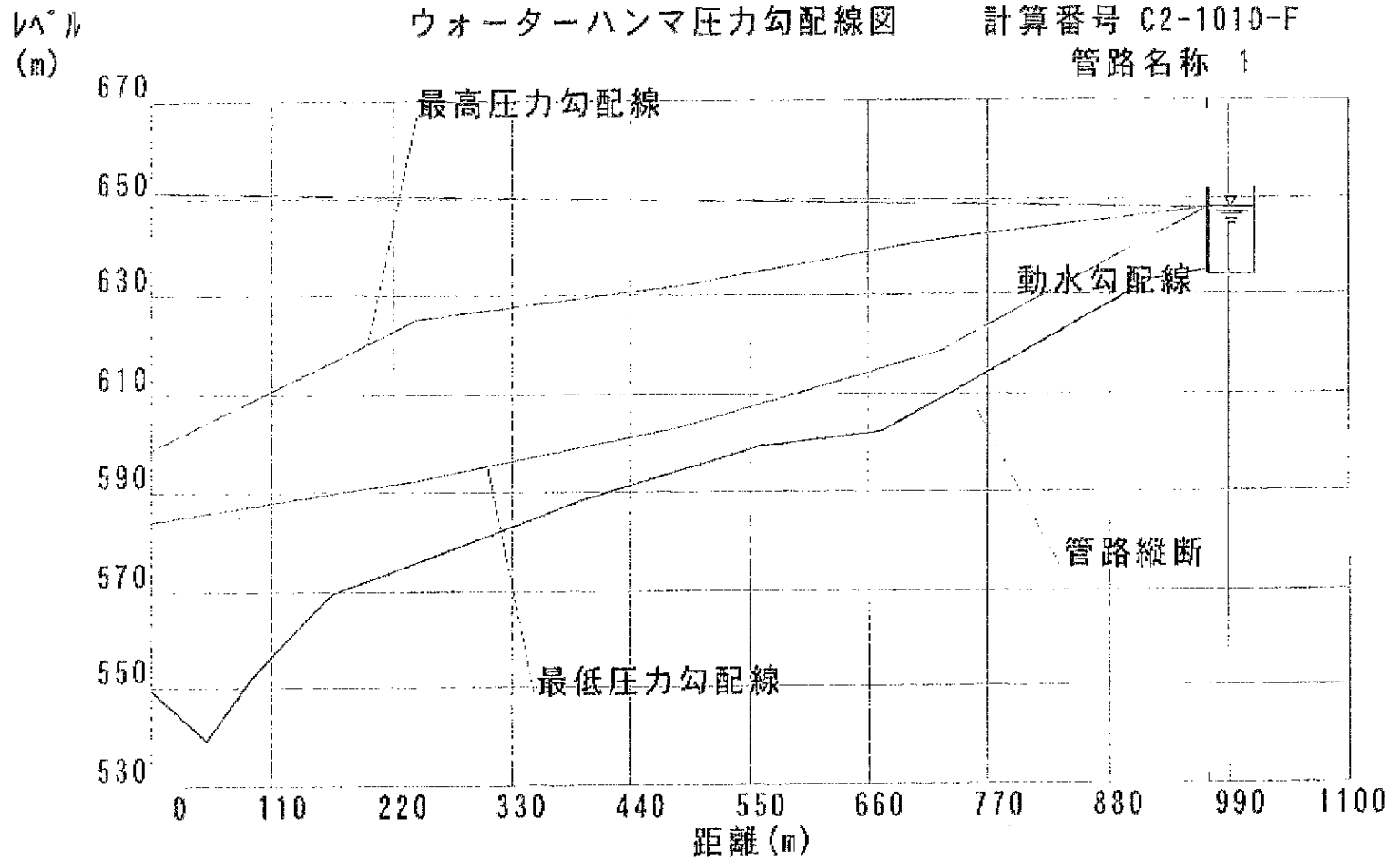


基準レベル 549.49

Transmission Pump (F):

R2 SR → Hantana place SR.

無対策: 負圧発生.



基準バール 549.49

Transmission Pump (F) :

R2 SR → Hantana Maue SR

対称(中分) (m pit) → 既設

ウォーターハンマ計算条件

計算番号 C2-1010-F

PAGE 1

Transmission Pump (F)

基準レベル 549.490 m
 計算時間単位 .06786 sec

【管路仕様】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m ³ /m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	970.0	FCD3	200	6.0	1.600		1 0 0	1	0	1	4.100	3.400	.000	1.6287	32.2567	24

【ポンプ仕様】

番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m ³ /m	出力 kw	極数	型式	ポンプ・モータ kg-m ²	フライール kg-m ²	回転数 min-1	効率 %	減衰 定数 k	揚程 m	初期状態 吐出量 m ³ /m	回転数	トルク
1	1	1	1	0	102.000	1.360	55.0	2	1	1.440	.000	2900	58	1.1767	102.000	1.360	1.000	1.000

【サージタンク仕様】

番号	形式	弁番号	水位 高さ m	断面積 m ²	連絡管 損失 m	空気弁 個数	連絡管 長さ m	管種	管径 mm	管厚 mm	ヤング 率	圧力波 往復時間 sec	管路 定数	分割 数	初期 空気量 m ³	戻り管 損失 m
1	3	0	.100	.000	7.347	0	.0	0	0	.0	.000	.0000	.000	0	.1	5.000

【圧力線図仕様】

管路名称 1

【縦断仕様】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	549.50	50.0	539.49	91.0	552.24	164.0	569.40
	397.0	588.57	559.0	599.15	672.0	602.37	920.0	633.36
	970.0	635.30						

Transmission Pump (H)

基準レベル 531.250 m
 計算時間単位 .04811 sec

【 管路仕様 】

管路名称	管長 m	管種	管径 mm	管厚 mm	ヤング 率	上流の管路	ポンプ 番号	サージ タンク 番号	弁 番号	終点 条件	管路流量 m3/m	配管 損失 m	弁絞 損失 m	圧力波 往復時間 sec	管路定数	分割
1	42.0	VP 1	160	12.7	.027		1 0 0	0	0	0	1.110	.310	.000	.1925	18.4690	4
2	1483.0	VP 1	160	12.7	.027	1	0 0 0	0	0	0	1.110	10.900	.000	6.7953	18.4690	140
3	160.0	VP 1	225	12.7	.027	2	0 0 0	0	0	0	1.110	.220	.000	.8575	7.9846	18
4	296.0	FCD3	200	6.0	1.600	3	0 0 0	0	0	1	1.110	.850	.000	.4970	32.2567	10

【 ポンプ仕様 】

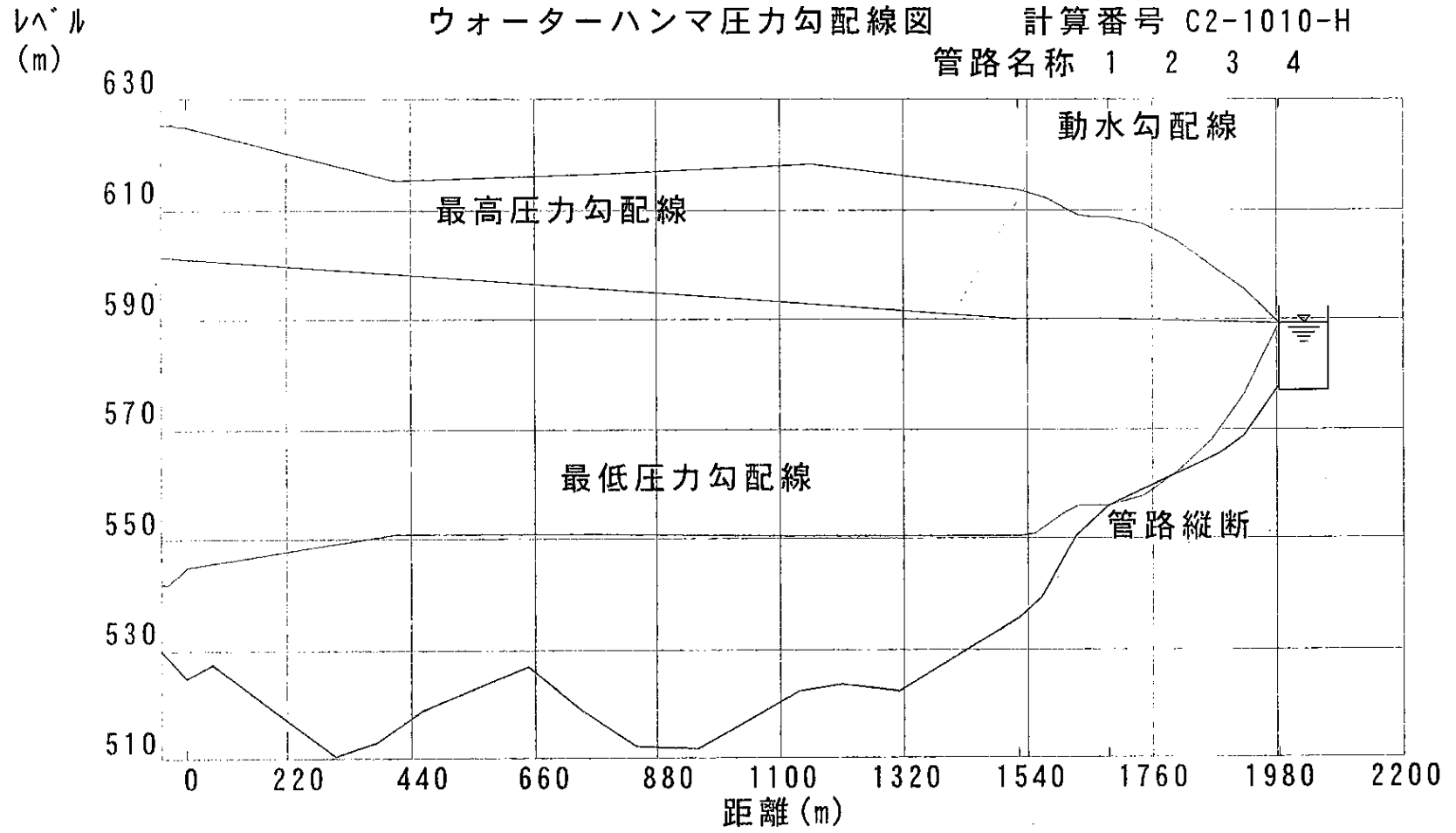
番号	台数	形式	弁閉鎖	弁番号	全揚程 m	吐出量 m3/m	出力 kw	極数	型式	ポンプ・モータ kg-m2	フライール kg-m2	回転数 min-1	効率 %	減衰 定数 k	初期状態 揚程 m	吐出量 m3/m	回転数	トルク
1	1	1	1	0	70.000	1.110	30.0	2	1	.555	.000	2900	53	1.8715	70.000	1.110	1.000	1.000

【 圧力線図仕様 】

管路名称	1	2	3	4
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【 縦断仕様 】

管路名称	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m	追加距離 m	レベル m
1	.0	529.75	42.0	524.66				
2	42.0	524.66	90.0	527.14	304.0	510.40	380.0	512.86
	460.0	518.88	650.0	526.76	738.0	519.25	840.0	512.14
	950.0	511.53	1130.0	522.13	1210.0	523.54	1310.0	522.40
	1525.0	535.84						
3	1525.0	535.84	1563.0	539.32	1625.0	550.31	1685.0	555.94
4	1685.0	555.94	1875.0	565.00	1921.0	568.42	1981.0	577.94



基準レベル 531.25

Transmission Pump (H) :

Kondadeniya SR. → Kulyamana SR.

06 Electrical Design Calculations

A. INTAKE [Phase 1]

3-1. Capacity Calculation Sheet for Transformer

Calculation Condition	Duty Transformer Name	Three Phase Load Capacity ($\Sigma P1$)	kVA Load Equipment ($\Sigma P2$)		Single Phase Load Equipment ($\Sigma P3$)		
		(kW)	(kVA)		(kVA)		
	NO.1 Power Transformer	333.30	4.70				
	NO.2 Power Transformer						

Capacity Calculation Formula	[Calculation Formula for Power Transformer]																																																																																																																																																																											
	$TR = \left(\frac{\Sigma P1}{\eta \times \phi} + \Sigma P2 + \sqrt{3} \times \Sigma P3 \right) \times \alpha \times \beta$																																																																																																																																																																											
	R : Required Transformer Capacity in kVA																																																																																																																																																																											
	$\Sigma P1 \sim 3$: Total Capacity for each facility in kW/kVA																																																																																																																																																																											
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	ϕ : General Power Factor	0.85																																																																																																																																																																										
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	<table border="1" style="width:100%; border-collapse: collapse;"> <tr> <td rowspan="2" style="text-align:center; vertical-align:middle;">Calculation Result</td> <td style="text-align:center;">Transformer Name</td> <td colspan="8" style="text-align:center;">Required Transformer Capacity in kVA</td> <td style="text-align:center;">Remarks</td> </tr> <tr> <td>NO.1-1 Power Transformer</td> <td colspan="8" style="text-align:center;">466.01</td> <td></td> </tr> <tr> <td></td> <td>NO.1-2 Power Transformer</td> <td colspan="8"></td> <td></td> </tr> <tr> <td></td> <td></td> <td colspan="8"></td> <td></td> </tr> <tr> <td></td> <td></td> <td colspan="8"></td> <td></td> </tr> <tr> <td colspan="2" style="text-align:center;">Rated capacity of transformer in kVA</td> <td style="text-align:center;">10</td> <td style="text-align:center;">15</td> <td style="text-align:center;">20</td> <td style="text-align:center;">30</td> <td style="text-align:center;">50</td> <td style="text-align:center;">75</td> <td style="text-align:center;">100</td> <td style="text-align:center;">150</td> <td style="text-align:center;">200</td> <td style="text-align:center;">300</td> </tr> <tr> <td colspan="2"></td> <td colspan="2" style="text-align:center;">500</td> <td colspan="2" style="text-align:center;">750</td> <td colspan="2" style="text-align:center;">1000</td> <td colspan="2" style="text-align:center;">1500</td> <td colspan="2" style="text-align:center;">2000</td> </tr> <tr> <td colspan="12" style="text-align:center;">Proposed Transformer</td> </tr> <tr> <td></td> <td style="text-align:center;">kVA</td> <td colspan="2" style="text-align:center;">Number</td> <td colspan="8" style="text-align:center;">Rated Voltage</td> </tr> <tr> <td></td> <td></td> <td colspan="2"></td> <td colspan="4" style="text-align:center;">Primary</td> <td colspan="4" style="text-align:center;">Secondary</td> </tr> <tr> <td>NO.1 Transformer</td> <td style="text-align:center;">500</td> <td colspan="2"></td> <td colspan="4"></td> <td colspan="4"></td> </tr> <tr> <td>NO.2 Transformer</td> <td></td> <td colspan="2"></td> <td colspan="4"></td> <td colspan="4"></td> </tr> <tr> <td></td> <td></td> <td colspan="2"></td> <td colspan="4"></td> <td colspan="4"></td> </tr> <tr> <td></td> <td></td> <td colspan="2"></td> <td colspan="4"></td> <td colspan="4"></td> </tr> </table>										Calculation Result	Transformer Name	Required Transformer Capacity in kVA								Remarks	NO.1-1 Power Transformer	466.01										NO.1-2 Power Transformer																																Rated capacity of transformer in kVA		10	15	20	30	50	75	100	150	200	300			500		750		1000		1500		2000		Proposed Transformer													kVA	Number		Rated Voltage												Primary				Secondary				NO.1 Transformer	500											NO.2 Transformer																																			
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A. INTAKE [Phase 1]

5. Capacity Calculation of Alternator

Calculation Condition	Description		Value	Calculation Result	Value	Remarks	Rated Alternator Capacity					
	Σ P0	Load Capacity Covered by Alt. (kW)	336.33				PG 1	494.60		20	37.5	50
Calculation Condition	Pm	Max. Motor	Load Name	Raw Water Pump	PG 2	378.00		100	150	200	250	300
			Starting Method	SOFT STERTER	PG 3	368.58		375	500	625	750	875
		kW		280.00	PG 4	13.33		1000	1250	1500	2000	2500
	R	Harmonic wave generating load		0.00	PG max	494.60		3125				
	Unbalanced load capacity	A	(kW)		0.00	Selected (kVA)	750	Diesel-engine , Radiator type	JEM-1354			
B		(kW)		0.00	×1set							
C		(kW)		0.00								

Calculation Formula	The rated alternator capacity is to be proposed on the basis of the maximum value among the following calculation.	
	a. Required for all load operation PG1 [kVA]	
	$PG1 = \frac{\Sigma P0}{\eta L \times \phi L} \times \alpha \times Sf$	β : Starting kVA for max. motor per kW 7.20 C : Motor starter factor 0.25 KG4 : Factor due to allowable negative phase current 0.15 R : Total harmonic wave generating load in kW Δ P : Total single phase unbalance capacity in kW 0.00 Where A ≥ B ≥ C , Δ P = A+B-2C U : Single phase unbalance factor $U = \frac{A-C}{\Delta P}$ 0.00 fv1 : Decrease factor of load starting 0.95
	b. Required from allowable voltage drop PG2 [kVA]	
	$PG2 = Pm \times \beta \times C \times Xd' \frac{1-\Delta E}{\Delta E}$	
	c. Required for starting the max. motor lastly PG3 [kVA]	
	$PG3 = \frac{fv1}{\gamma G} \{ (\Sigma P0 - Pm) \times \frac{\alpha}{\eta L \times \phi m} + Pm \times \beta \times C \}$	Value of decrease factor of load starting (fv)
	d. Required from allowable negative phase current PG4 [kVA]	
	$PG4 = \frac{1}{KG4} \sqrt{ \{ (0.432R)^2 + (1.23 \Delta P)^2 \times (1-3U+3U^2) \}}$	
	Where	
η L : General Efficiency 0.85		
φ L : General Power Factor 0.80		
α : Demand Factor 1.00		
Xd' : Alternator Factor 0.25		
Σ P0 : Total load capacity covered by generator in kW (Excluding Stand-by) Note 1		
Sf : Current increasing factor due to unbalanced load (= 1+0.6×(Δ P ÷ Σ P0)) 1.00		
Δ E : Allowable voltage drop factor 0.25		
γ G : Tolerant capacity for momentary overload of Alternator 1.5		
φ m :Max. motor power factor 0.85		

Note1: To exchange kVA load into kW , single phase load to be multiplied by 0.8 , rectifier to be calculated as multiplying of rated Dc voltage and DC current, UPS to be calculated as multiplying of rated output in kVA and 0.9 , and these exchanged value to be added to three phase load capacity in kW.

A. INTAKE [Phase 1]

6. Capacity Calculation of Engine

Calculation Condition	Description		Value	Calculation Result	Value	Remarks	Generator efficiency		
	PG	Generator Output in kVA	750				PE 1	887.92	
Pm	Maximum Motor	Load name	Raw Water Pump	PE 2-1	175.59		kVA	2~8P	10~18P
		Starting Method	SOFT STERTER	PE 2-2	132.35		20	79.0	-
		kW	280				37.5	82.5	-
Σ P0	Load Capacity Covered by Alt. (kW)		168.165	PE max	887.92		50	84.3	-
							62.5	85.2	-
				Selected (PS)	900	Diesel-engine generator , Radiator type	75	85.7	-
							100	86.7	-
							125	87.6	-
							150	88.1	-
							200	88.9	-
							250	89.5	-
							300	90.0	-
							375	90.6	-
							500	91.3	-
							625	91.9	-
							750	92.3	91.7
							875	92.5	92.0
							1000	92.8	92.3
							1250	93.2	92.8
							1500	93.4	93.1
							2000	93.8	93.5
							2500	93.9	93.7
							3125	94.0	93.8

Calculation Formula	Value
Maximum value or over among the following calculation is to be proposed as engine capacity.	
a. PE1 in PS is to be derived from requirement for full load running	
$PE1 = \frac{PG \times \phi G}{\eta G} \times 1.36 \times \Delta H$	
b. PE2 in PS is to be derived from requirement of max. motor starting lastly	
① PE2-1 is to be derived from based on allowable load starting factor	
$PE2-1 = fv2 \left\{ 0.75 \times \frac{1}{\eta'G} \times (\Sigma P0 - Pm) \times \frac{\alpha}{\eta L} + \frac{1}{\epsilon \times \eta'G} \times Pm \times \beta \times C \times \phi s \right\} \times 1.36 \times \Delta H$	
② PE2-2 is to be derived from tolerant capacity for momentary overload	
$PE2-2 = \frac{fv3}{\eta'G \times \gamma E} \times \left\{ (\Sigma P0 - Pm) \times \frac{\alpha}{\eta L} + Pm \times \beta \times C \times \phi s \right\} \times 1.36 \times \Delta H$	
Where	
Σ P0 : Total load capacity covered by generator in kW	0.85
η L : General Efficiency	0.8
φ L : General Power factor	0.8
α : Demand Factor	0.8
φ G : Generator Power factor	0.8
γ E : Tolerant capacity for momentary overload of Engine	1.1
β : Starting kVA for max. motor of per kW	7.2
C : Motor starter factor	0.25
φ s : Motor starting Power Factor for max. motor starting kVA , Squirrel cage	0.4
η G : Generator efficiency	0.919
η 'G : Generator overload efficiency	0.855
fv2 : Decreased factor due to motor starting	0.9
fv3 : Decreased factor due to motor starting	1.0
ε : Tolerant capacity due to non-motor starting of Engine	1.0
Δ H : Altitude compensation	1.0

Starting method	Starter Name
β × C	
7.2×1	Direct on-line
7.2×2 / 3	Star - delta
7.2×1 / 3	Star - delta with resistor
1.2	VVVF
1.2	Wound - rotor type
7.2×0.5	Reactor 50%
7.2×0.65	Reactor 65%
7.2×0.8	Reactor 80%
7.2×0.25	Auto - transformer 50%
7.2×0.42	Auto - transformer 65%
7.2×0.64	Auto - transformer 80%

A. INTAKE [Phase 1]

7. Fuel Calculation

Calculation Condition	Description		Value , Type	Calculation Result	Description		Value	Remarks
	PG	Generator output in kVA			750	Fuel tank	5677.6 → 6000 L × 1 set	
P	Engineoutput in PS		900					
	Engine Type		Diesel-engine , Radiator type					
	Fuel Type		Light oil					

Fuel Tank Volume is to be derived from the following calculation.

a. Q [m3] Fuel Tank Volume

$$Q = \frac{P \times be \times H}{d} \times \alpha$$

be : Fuel consumption factor [unit : kg/PS·h]

Output (PS)	Diesel	Gas turbine
30 or less	0.23	-
over 30 and 250 or less	0.22	0.5
over 250 and 450 or less	0.2	0.48
over 450 and 750 or less	0.18	0.43
over 750	0.17	0.38

be : Fuel consumption factor kg/PS·h

H : Running hour hours

d : Fuel density kg/m3
 (A heavy oil 850kg/m3)
 (Light oil 830kg/m3)
 (Kerosine 790kg/m3)

α : Surplus Factor

Calculation Formula

B. INTAKE [Phase 3]

3-1. Capacity Calculation Sheet for Transformer

Calculation Condition	Duty Transformer Name	Three Phase Load Capacity (Σ P1)	kVA Load Equipment (Σ P2)	Single Phase Load Equipment (Σ P3)
		(kW)	(kVA)	(kVA)
	NO.1 Power Transformer	903.70	4.70	
	NO.2 Power Transformer			

Capacity Calculation Formula	[Calculation Formula for Power Transformer]															
	$TR = \left(\frac{\sum P1}{\eta \times \phi} + \sum P2 + \sqrt{3} \times \sum P3 \right) \times \alpha \times \beta$															
	R : Required Transformer Capacity in kVA Σ P1~3 : Total Capacity for each facility in kW/kVA η : General Efficiency <table border="1" style="display: inline-table; vertical-align: middle;"><tr><td style="padding: 2px;">0.85</td></tr></table> φ : General Power Factor <table border="1" style="display: inline-table; vertical-align: middle;"><tr><td style="padding: 2px;">0.85</td></tr></table> α : Surplus Factor <table border="1" style="display: inline-table; vertical-align: middle;"><tr><td style="padding: 2px;">1</td></tr></table> β : Demand Factor <table border="1" style="display: inline-table; vertical-align: middle;"><tr><td style="padding: 2px;">1</td></tr></table>												0.85	0.85	1	1
	0.85															
	0.85															
	1															
	1															
	Calculation Result	Transformer Name	Required Transformer Capacity in kVA								Remarks					
		NO.1-1 Power Transformer	1255.50													
		NO.1-2 Power Transformer														
	Rated capacity of transformer in kVA	10	15	20	30	50	75	100	150	200	300					
		500		750		1000		1500		2000						
Proposed Transformer																
		kVA	Number		Rated Voltage											
					Primary				Secondary							
	NO.1 Transformer	1500	× 1		33000				415							
	NO.2 Transformer															

The upper rated transformer capacity is to be proposed through the capacity calculation.

B. INTAKE [Phase 3]

5. Capacity Calculation of Alternator

Calculation Condition	Description		Value	Calculation Result	Value	Remarks	Rated Alternator Capacity					
	Σ P0	Load Capacity Covered by Alt. (kW)	906.73				PG 1	1333.43		20	37.5	50
Pm	Max. Motor	Load Name	Raw Water Pump	280.00	PG 2	378.00		100	150	200	250	300
		Starting Method	SOFT STERTER		PG 3	868.58		375	500	625	750	875
		kW			PG 4	13.33		1000	1250	1500	2000	2500
R	Harmonic wave generating load		0.00	PG max	1333.43		3125					
Unbalanced load capacity	A	(kW)		Selected (kVA)	750	× 2set	Diesel-engine , Radiator type					
	B	(kW)										
	C	(kW)										

Calculation Formula	The rated alternator capacity is to be proposed on the basis of the maximum value among the following calculation.																																											
	a. Required for all load operation PG1 [kVA]																																											
	$PG1 = \frac{\Sigma P0}{\eta L \times \phi L} \times \alpha \times Sf$					β : Starting kVA for max. motor per kW 7.20 C : Motor starter factor 0.25 KG4 : Factor due to allowable negative phase current 0.15 R : Total harmonic wave generating load in kW Δ P : Total single phase unbalance capacity in kW 0.00 Where A ≥ B ≥ C , Δ P = A+B-2C U : Single phase unbalance factor $U = \frac{A-C}{\Delta P}$ 0.00 fv1 : Decrease factor of load starting 0.95																																						
	b. Required from allowable voltage drop PG2 [kVA]																																											
	$PG2 = Pm \times \beta \times C \times Xd' \frac{1-\Delta E}{\Delta E}$					Value of decrease factor of load starting (fv) <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th rowspan="2">Number of Poles</th> <th colspan="4">Pm / Σ P0</th> <th rowspan="2">Remarks</th> </tr> <tr> <th>0~</th> <th>0.8</th> <th>0.9</th> <th>1</th> </tr> </thead> <tbody> <tr> <td>2P</td> <td>1</td> <td>0.9</td> <td>0.85</td> <td>0.8</td> <td>PG3 , fv1</td> </tr> <tr> <td>Over 4P</td> <td>1</td> <td>0.95</td> <td>0.95</td> <td>0.9</td> <td>PE2-2 , fv3</td> </tr> <tr> <td>2P</td> <td>0.9</td> <td>0.85</td> <td>0.85</td> <td>0.8</td> <td>PE2-1 , fv2</td> </tr> <tr> <td>Over 4P</td> <td>0.9</td> <td>0.9</td> <td>0.9</td> <td>0.9</td> <td></td> </tr> </tbody> </table>					Number of Poles	Pm / Σ P0				Remarks	0~	0.8	0.9	1	2P	1	0.9	0.85	0.8	PG3 , fv1	Over 4P	1	0.95	0.95	0.9	PE2-2 , fv3	2P	0.9	0.85	0.85	0.8	PE2-1 , fv2	Over 4P	0.9	0.9	0.9	0.9	
	Number of Poles	Pm / Σ P0				Remarks																																						
		0~	0.8	0.9	1																																							
	2P	1	0.9	0.85	0.8	PG3 , fv1																																						
	Over 4P	1	0.95	0.95	0.9	PE2-2 , fv3																																						
	2P	0.9	0.85	0.85	0.8	PE2-1 , fv2																																						
Over 4P	0.9	0.9	0.9	0.9																																								
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γ G : Tolerant capacity for momentary overload of Alternator		1.5																																										
φ m : Max. motor power factor		0.85																																										

Note1: To exchange kVA load into kW , single phase load to be multiplied by 0.8 , rectifier to be calculated as multiplying of rated Dc voltage and DC current, UPS to be calculated as multiplying of rated output in kVA and 0.9 , and these exchanged value to be added to three phase load capacity in kW.

B. INTAKE [Phase 3]

6. Capacity Calculation of Engine

Calculation Condition	Description		Value	Calculation Result	Value	Remarks	Generator efficiency			
	PG	Generator Output in kVA	750				PE 1	887.92	Rate	η G effi. (%)
Calculation Condition	Pm	Maximum Motor	Load name	Raw Water Pump	PE 2-1	463.80	20 37.5 50 62.5 75 100	2~8P	79.0	-
		Starting Method	SOFT STERTER	PE 2-2	501.09	82.5		-		
			kW	280	PE max	887.92		84.3	-	
	Σ P0	Load Capacity Covered by Alt. (kW)	453.365	Selected (PS)	900	Diesel-engine generator , Radiator type		85.7	-	
Calculation Formula	Maximum value or over among the following calculation is to be proposed as engine capacity.						125	87.6	-	
	a. PE1 in PS is to be derived from requirement for full load running						150	88.1	-	
	$PE1 = \frac{PG \times \phi G}{\eta G} \times 1.36 \times \Delta H$						200	88.9	-	
	b. PE2 in PS is to be derived from requirement of max. motor starting lastly						250	89.5	-	
	① PE2-1 is to be derived from based on allowable load starting factor						300	90.0	-	
	$PE2-1 = fv2 \left\{ 0.75 \times \frac{1}{\eta 'G} \times (\Sigma P0 - Pm) \times \frac{\alpha}{\eta L} + \frac{1}{\epsilon \times \eta 'G} \times Pm \times \beta \times C \times \phi s \right\} \times 1.36 \times \Delta H$						375	90.6	-	
	② PE2-2 is to be derived from tolerant capacity for momentary overload						500	91.3	-	
	$PE2-2 = \frac{fv3}{\eta 'G \times \gamma E} \times \left\{ (\Sigma P0 - Pm) \times \frac{\alpha}{\eta L} + Pm \times \beta \times C \times \phi s \right\} \times 1.36 \times \Delta H$						625	91.9	-	
	Where						750	92.3	91.7	
	Σ P0 : Total load capacity covered by generator in kW						875	92.5	92.0	
	η L : General Efficiency						1000	92.8	92.3	
	φ L : General Power factor						1250	93.2	92.8	
	α : Demand Factor						1500	93.4	93.1	
φ G : Generator Power factor						2000	93.8	93.5		
γ E : Tolerant capacity for momentary overload of Engine						2500	93.9	93.7		
β : Starting kVA for max. motor of per kW						3125	94.0	93.8		
C : Motor starter factor										
φ s : Motor starting Power Factor for max. motor starting kVA , Squirrel cage										
η G : Generator efficiency										
η 'G : Generator overload efficiency										
fv2 : Decreased factor due to motor starting										
fv3 : Decreased factor due to motor starting										
ε : Tolerant capacity due to non-motor starting of Engine										
Δ H : Altitude compensation										

Starting method	
β × C	Starter Name
7.2×1	Direct on-line
7.2×2 / 3	Star - delta
7.2×1 / 3	Star - delta with resistor
1.2	VVVF
1.2	Wound - rotor type
7.2×0.5	Reactor 50%
7.2×0.65	Reactor 65%
7.2×0.8	Reactor 80%
7.2×0.25	Auto - transformer 50%
7.2×0.42	Auto - transformer 65%
7.2×0.64	Auto - transformer 80%

B. INTAKE [Phase 3]

7. Fuel Calculation

Calculation Condition	Description		Value, Type		Calculation Result	Description		Value		Remarks
	PG	Generator output in kVA		750		Fuel tank	5677.6 → 6000 L × 2 sets			
P	Engine output in PS		900			or 12000 L × 1 set				
	Engine Type		Diesel-engine, Radiator type							
	Fuel Type		Light oil							

Fuel Tank Volume is to be derived from the following calculation.

a. Q [m3] Fuel Tank Volume

$$Q = \frac{P \times be \times H}{d} \times \alpha$$

be : Fuel consumption factor [unit : kg/PS·h]

Output (PS)	Diesel	Gas turbine
30 or less	0.23	-
over 30 and 250 or less	0.22	0.5
over 250 and 450 or less	0.2	0.48
over 450 and 750 or less	0.18	0.43
over 750	0.17	0.38

be : Fuel consumption factor kg/PS·h

H : Running hour hours

d : Fuel density kg/m³
 (A heavy oil 850kg/m³)
 (Light oil 830kg/m³)
 (Kerosine 790kg/m³)

α : Surplus Factor

Calculation Formula

C. WTP [Phase 1]

1. LOAD LIST FOR ELECTRICAL WORKS

SUMMARY SHEET

Facility name	Equipment name	Numbers (Duty)	Numbers (Stand-by)	Numbers (Total)	Commer. Power (kW)	Generator (Nummbers)	Generator (kW)	Remarks
	1. Flocculation & Sedimentation Basins	13	0	13	5.00	13	5.00	
					5.00			NO.1Tr
					0.00			NO.2Tr
	2.Filter Units	26	4	30	99.90	27	154.90	
					154.90			NO.1Tr
					0.00			NO.2Tr
	3.Clear Water Pump Station	9	8	17	805.10	9	805.10	
					805.10			NO.1Tr
					0.00			NO.2Tr
	4.Chemical Building	10	3	13	17.45	10	17.45	
					17.45			NO.1Tr
								NO.2Tr
	5.Backwash Recovery Facility	1	1	2	30.00	1	30.00	
					30.00			NO.1Tr
								NO.2Tr
	8. Architectural and others							
	Architectural (1)	kW	1	1	80.00	1	80.00	NO.1Tr
	Architectural (2)	kW	1	1	30.00	1	30.00	NO.1Tr
	Architectural (3)	kW						NO.2Tr
	Generator-1	kW	1	1	20.00	1	20.00	NO.1Tr
	Generator-1	kW						NO.2Tr
	UPS	kVA	1	1	33.00	1	33.00	NO.1Tr
	Total (NO.1 Transformer)	kW			1142.45		1142.45	Σ 1 , Three Phase
		kVA			33.00		33.00	Σ 2 , Three Phase
		kVA						Σ 3 , Single Phase
	Total (NO.2 Transformer)	kW						Σ 1 , Three Phase
		kVA						Σ 2 , Three Phase
		kVA						Σ 3 , Single Phase
	Total				1172.15		1172.15	

Total(kW)= Σ 1+ Σ 2×0.9+ Σ 3×0.8

C. WTP [Phase 1]

3-1. Capacity Calculation Sheet for Transformer

Calculation Condition	Duty Transformer Name	Three Phase Load Capacity (Σ P1)	kVA Load Equipment (Σ P2)	Single Phase Load Equipment (Σ P3)
		(kW)	(kVA)	(kVA)
	NO.1 Power Transformer	1142.45	33.00	0.00
NO.2 Power Transformer	0.00	0.00	0.00	

[Calculation Formula for Power Transformer]			
$TR = \left(\frac{\Sigma P1}{\eta \times \phi} + \Sigma P2 + \sqrt{3} \times \Sigma P3 \right) \times \alpha \times \beta$			
<p>R : Required Transformer Capacity in kVA Σ P1~3 : Total Capacity for each facility in kW/kVA</p>			
η : General Efficiency	0.85		
φ : General Power Factor	0.85		
α : Surplus Factor	1		
β : Demand Factor	1		

Calculation Result	Transformer Name	Required Transformer Capacity in kVA	Remarks
	NO.1-1 Power Transformer	1614.25	
	NO.1-2 Power Transformer	0.00	

Rated capacity of transformer in kVA	10	15	20	30	50	75	100	150	200	300
		500		750		1000		1500		2000

Proposed Transformer				
	kVA	Number	Rated Voltage	
			Primary	Secondary
NO.1 Transformer	2000	× 1	33000	415
NO.2 Transformer				

The upper rated transformer capacity is to be proposed through the capacity calculation.

C. WTP [Phase 1]

5. Capacity Calculation of Alternator

Description		Value	Calculation Result	Value	Remarks	Rated Alternator Capacity						
Calculation Condition												
Calculation Condition	Σ P0	Load Capacity Covered by Alt. (kW)	1172.15	PG 1	1551.38		20	37.5	50	62.5	75	
	Pm	Max. Motor	Load Name	Raw Water Pump	PG 2	607.50		100	150	200	250	300
			Starting Method	SOFT STERTER	PG 3	1082.72		375	500	625	750	875
			kW	450.00	PG 4	13.33		1000	1250	1500	2000	2500
	R	Harmonic wave generating load		0.00	PG max	1551.38		3125				
	Unbalanced load capacity			0.00	Selected (kVA)	2000	Diesel-engine , Radiator type	JEM-1354				
A		(kW)	4.00	× 1set								
B		(kW)	4.00									
	C	(kW)	4.00									
Calculation Formula	The rated alternator capacity is to be proposed on the basis of the maximum value among the following calculation.											
	a. Required for all load operation PG1 [kVA]											
	$PG1 = \frac{\Sigma P0}{\eta L \times \phi L} \times \alpha \times Sf$			β : Starting kVA for max. motor per kW		7.20						
				C : Motor starter factor		0.25						
				KG4 : Factor due to allowable negative phase current		0.15						
				R : Total harmonic wave generating load in kW								
				Δ P : Total single phase unbalance capacity in kW		0.00						
				Where A ≥ B ≥ C , Δ P = A+B-2C								
				U : Single phase unbalance factor U= $\frac{A-C}{\Delta P}$		0.00						
				fv1 : Decrease factor of load starting		0.95						
c. Required for starting the max. motor lastly PG3 [kVA]												
$PG3 = \frac{fv1}{\gamma G} \{ (\Sigma P0 - Pm) \times \frac{\alpha}{\eta L \times \phi m} + Pm \times \beta \times C \}$			Value of decrease factor of load starting (fv)									
			Number of Poles		Pm / Σ P0				Remarks			
					0~	0.8	0.9	1				
			2P		1	0.9	0.85	0.8	PG3 , fv1			
			Over 4P		1	0.95	0.95	0.9	PE2-2 , fv3			
			2P		0.9	0.85	0.85	0.8	PE2-1 ,fv2			
			Over 4P		0.9	0.9	0.9	0.9				
d. Required from allowable negative phase current PG4 [kVA]												
$PG4 = \frac{1}{KG4} \sqrt{ \{ (0.432R)^2 + (1.23 \Delta P)^2 \times (1-3U+3U^2) \} }$			1.00									
Where												
η L : General Efficiency		0.85										
φ L : General Power Factor		0.80										
α : Demand Factor		0.90										
Xd' : Alternator Factor		0.25										
Σ P0 : Total load capacity covered by generator in kW (Excluding Stand-by) Note 1												
Sf : Current increasing factor due to unbalanced load (= 1+0.6× (Δ P ÷ Σ P0)												
Δ E : Allowable voltage drop factor		0.25										
γ G : Tolerant capacity for momentary overload of Alternator		1.5										
φ m :Max. motor power factor		0.85										

Note1: To exchange kVA load into kW , single phase load to be multiplied by 0.8 , rectifier to be calculated as multiplying of rated Dc voltage and DC current, UPS to be calculated as multiplying of rated output in kVA and 0.9 , and these exchanged value to be added to three phase load capacity in kW.

C. WTP [Phase 1]
6. Capacity Calculation of Engine

Calculation Condition	Description		Value	Calculation Result	Value	Remarks	Generator efficiency			
	PG	Generator Output in kVA	2000				PE 1	2367.79	Rate	η G eff. (%)
Calculation Condition	Pm	Maximum Motor	Load name	Raw Water Pump	PE 2-1	601.34	20	kVA	2~8P	10~18P
		Starting Method	SOFT STERTER	PE 2-2	621.03					
	kW	450								
	Σ P0	Load Capacity Covered by Alt. (kW)	586.075							
				PE max	2367.79					
Calculation Formula				Selected (PS)	2400	Diesel-engine generator , Radiator type	75	85.7	-	
	Maximum value or over among the following calculation is to be proposed as engine capacity.							100	86.7	-
	a. PE1 in PS is to be derived from requirement for full load running							125	87.6	-
	$PE1 = \frac{PG \times \phi G}{\eta G} \times 1.36 \times \Delta H$							150	88.1	-
	b. PE2 in PS is to be derived from requirement of max. motor starting lastly							200	88.9	-
	① PE2-1 is to be derived from based on allowable load starting factor							250	89.5	-
	$PE2-1 = fv2 \left\{ 0.75 \times \frac{1}{\eta G} \times (\Sigma P0 - Pm) \times \frac{\alpha}{\eta L} + \frac{1}{\epsilon \times \eta G} \times Pm \times \beta \times C \times \phi s \right\} \times 1.36 \times \Delta H$							300	90.0	-
	② PE2-2 is to be derived from tolerant capacity for momentary overload							375	90.6	-
	$PE2-2 = \frac{fv3}{\eta G \times \gamma E} \times \left\{ (\Sigma P0 - Pm) \times \frac{\alpha}{\eta L} + Pm \times \beta \times C \times \phi s \right\} \times 1.36 \times \Delta H$							500	91.3	-
	Where							625	91.9	-
	Σ P0 : Total load capacity covered by generator in kW							750	92.3	91.7
	η L : General Efficiency							875	92.5	92.0
	φ L : General Power factor							1000	92.8	92.3
	α : Demand Factor							1250	93.2	92.8
	φ G : Generator Power factor							1500	93.4	93.1
γ E : Tolerant capacity for momentary overload of Engine							2000	93.8	93.5	
β : Starting kVA for max. motor of per kW							2500	93.9	93.7	
C : Motor starter factor							3125	94.0	93.8	
φ s : Motor starting Power Factor for max. motor starting kVA , Squirrel cage										
η G : Generator efficiency										
η 'G : Generator overload efficiency										
fv2 : Decreased factor due to motor starting										
fv3 : Decreased factor due to motor starting										
ε : Tolerant capacity due to non-motor starting of Engine										
Δ H : Altitude compensation										

Starting method	
β × C	Starter Name
0.85	7.2×1 Direct on-line
0.8	7.2×2 / 3 Star - delta
0.8	7.2×1 / 3 Star - delta with resistor
0.8	1.2 VVVF
1.1	1.2 Wound - rotor type
0.25	7.2×0.5 Reactor 50%
0.4	7.2×0.65 Reactor 65%
0.919	7.2×0.8 Reactor 80%
0.855	7.2×0.25 Auto - transformer 50%
0.9	7.2×0.42 Auto - transformer 65%
1.0	7.2×0.64 Auto - transformer 80%
1.0	
1.0	

C. WTP [Phase 1]
7. Fuel Calculation

Calculation Condition	Description		Value, Type	Calculation Result	Description		Value	Remarks
	PG	Generator output in kVA			2000	Fuel tank	15140.2 → 16000 L × 1 sets	
P	Engine output in PS		2400					
	Engine Type		Diesel-engine, Radiator type					
	Fuel Type		Light oil					

Fuel Tank Volume is to be derived from the following calculation.

a. Q [m3] Fuel Tank Volume

$$Q = \frac{P \times be \times H}{d} \times \alpha$$

be : Fuel consumption factor [unit : kg/PS·h]

Output (PS)	Diesel	Gas turbine
30 or less	0.23	-
over 30 and 250 or less	0.22	0.5
over 250 and 450 or less	0.2	0.48
over 450 and 750 or less	0.18	0.43
over 750	0.17	0.38

be : Fuel consumption factor kg/PS·h

H : Running hour hours

d : Fuel density kg/m³
(A heavy oil 850kg/m³)
(Light oil 830kg/m³)
(Kerosine 790kg/m³)

α : Surplus Factor

Calculation Formula

D. WTP [Phase 3]

1. LOAD LIST FOR ELECTRICAL WORKS

SUMMARY SHEET

Facility name	Equipment name	Numbers (Duty)	Numbers (Stand-by)	Numbers (Total)	Commer. Power (kW)	Generator (Nummbers)	Generator (kW)	Remarks
	1. Flocculation & Sedimentation Basins	37	0	37	14.20	40	14.20	
					5.00			NO.1Tr
					9.20			NO.2Tr
	2.Filter Units	67	5	72	112.60	68	167.60	
					154.90			NO.1Tr
					12.70			NO.2Tr
	3.Clear Water Pump Station	19	10	29	2456.10	19	2456.10	
					1055.30			NO.1Tr
					1400.80			NO.2Tr
	4.Chemical Building	20	3	23	37.45	20	37.45	
					37.45			NO.1Tr
								NO.2Tr
	5.Backwash Recovery Facility	1	1	2	30.00	1	30.00	
					30.00			NO.1Tr
								NO.2Tr
	8. Architectural and others							
	Architectural (1)	kW	1	1	80.00	1	80.00	NO.1Tr
	Architectural (2)	kW	1	1	30.00	1	30.00	NO.1Tr
	Architectural (3)	kW	1	1	30.00	1	30.00	NO.2Tr
	Generator-1	kW	1	1	20.00	1	20.00	NO.1Tr
	Generator-1	kW	1	1	20.00	1	20.00	NO.2Tr
	UPS	kVA	1	1	33.00	1	33.00	NO.1Tr
	Total (NO.1 Transformer)	kW			1412.65		2885.35	Σ 1 , Three Phase
		kVA			33.00		33.00	Σ 2 , Three Phase
		kVA						Σ 3 , Single Phase
	Total (NO.2 Transformer)	kW			1472.70			Σ 1 , Three Phase
		kVA						Σ 2 , Three Phase
		kVA						Σ 3 , Single Phase
	Total				2915.05		2915.05	

Total(kW)=Σ 1+ Σ 2×0.9+ Σ 3×0.8

D. WTP [Phase 3]

3-1. Capacity Calculation Sheet for Transformer

Calculation Condition	Duty Transformer Name	Three Phase Load Capacity (Σ P1)	kVA Load Equipment (Σ P2)	Single Phase Load Equipment (Σ P3)
		(kW)	(kVA)	(kVA)
	NO.1 Power Transformer	1412.65	33.00	0.00
NO.2 Power Transformer	1472.70	0.00	0.00	

Capacity Calculation Formula	[Calculation Formula for Power Transformer]																																																																						
	$TR = \left(\frac{\Sigma P1}{\eta \times \phi} + \Sigma P2 + \sqrt{3} \times \Sigma P3 \right) \times \alpha \times \beta$ <p> R : Required Transformer Capacity in kVA Σ P1~3 : Total Capacity for each facility in kW/kVA η : General Efficiency 0.85 φ : General Power Factor 0.85 α : Surplus Factor 1 β : Demand Factor 0.9 </p>	<table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th rowspan="2" style="writing-mode: vertical-rl; transform: rotate(180deg);">Calculation Result</th> <th>Transformer Name</th> <th>Required Transformer Capacity in kVA</th> <th>Remarks</th> </tr> </thead> <tbody> <tr> <td>NO.1-1 Power Transformer</td> <td style="text-align: center;">1789.40</td> <td></td> </tr> <tr> <td>NO.1-2 Power Transformer</td> <td style="text-align: center;">1834.51</td> <td></td> </tr> <tr> <td> </td> <td> </td> <td> </td> </tr> <tr> <td> </td> <td> </td> <td> </td> </tr> </tbody> </table> <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th rowspan="2">Rated capacity of transformer in kVA</th> <th>10</th> <th>15</th> <th>20</th> <th>30</th> <th>50</th> <th>75</th> <th>100</th> <th>150</th> <th>200</th> <th>300</th> </tr> </thead> <tbody> <tr> <td> </td> <td colspan="2" style="text-align: center;">500</td> <td colspan="2" style="text-align: center;">750</td> <td colspan="2" style="text-align: center;">1000</td> <td colspan="2" style="text-align: center;">1500</td> <td colspan="2" style="text-align: center;">2000</td> </tr> </tbody> </table> <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th colspan="5">Proposed Transformer</th> </tr> <tr> <th rowspan="2"> </th> <th rowspan="2">kVA</th> <th rowspan="2">Number</th> <th colspan="2">Rated Voltage</th> </tr> <tr> <th>Primary</th> <th>Secondary</th> </tr> </thead> <tbody> <tr> <td>NO.1 Transformer</td> <td style="text-align: center;">2000</td> <td style="text-align: center;">1 set</td> <td style="text-align: center;">33000</td> <td style="text-align: center;">415</td> </tr> <tr> <td>NO.2 Transformer</td> <td style="text-align: center;">2000</td> <td style="text-align: center;">1 set</td> <td> </td> <td> </td> </tr> <tr> <td> </td> <td> </td> <td> </td> <td> </td> <td> </td> </tr> <tr> <td> </td> <td> </td> <td> </td> <td> </td> <td> </td> </tr> </tbody> </table>	Calculation Result	Transformer Name	Required Transformer Capacity in kVA	Remarks	NO.1-1 Power Transformer	1789.40		NO.1-2 Power Transformer	1834.51								Rated capacity of transformer in kVA	10	15	20	30	50	75	100	150	200	300		500		750		1000		1500		2000		Proposed Transformer						kVA	Number	Rated Voltage		Primary	Secondary	NO.1 Transformer	2000	1 set	33000	415	NO.2 Transformer	2000	1 set											
Calculation Result	Transformer Name	Required Transformer Capacity in kVA		Remarks																																																																			
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The upper rated transformer capacity is to be proposed through the capacity calculation.

D. WTP [Phase 3]

5. Capacity Calculation of Alternator

Calculation Condition	Description		Value	Calculation Result	Value	Remarks	Rated Alternator Capacity				
	Σ P0	Load Capacity Covered by Alt. (kW)			2915.05	PG 1	3858.15		20	37.5	50
Pm	Max. Motor	Load Name	Raw Water Pump	PG 2	607.50		100	150	200	250	300
		Starting Method	SOFT STERTER	PG 3	2457.75		375	500	625	750	875
R	Harmonic wave generating load		0.00	PG 4	13.33		1000	1250	1500	2000	2500
	Unbalanced load capacity			PG max	3858.15		JEM-1354				
		A (kW)		Selected (kVA)	2000	Diesel-engine , Radiator type					
		B (kW)		× 2set							
		C (kW)									

Calculation Formula	The rated alternator capacity is to be proposed on the basis of the maximum value among the following calculation.																																			
a. Required for all load operation PG1 [kVA]	$PG1 = \frac{\Sigma P0}{\eta L \times \phi L} \times \alpha \times Sf$	β : Starting kVA for max. motor per kW 7.20 C : Motor starter factor 0.25 KG4 : Factor due to allowable negative phase current 0.15																																		
b. Required from allowable voltage drop PG2 [kVA]	$PG2 = Pm \times \beta \times C \times Xd' \frac{1-\Delta E}{\Delta E}$	R : Total harmonic wave generating load in kW Δ P : Total single phase unbalance capacity in kW 0.00 Where $A \geq B \geq C, \Delta P = A+B-2C$																																		
c. Required for starting the max. motor lastly PG3 [kVA]	$PG3 = \frac{fv1}{\gamma G} \{ (\Sigma P0 - Pm) \times \frac{\alpha}{\eta L \times \phi m} + Pm \times \beta \times C \}$	U : Single phase unbalance factor $U = \frac{A-C}{\Delta P}$ 0.00 fv1 : Decrease factor of load starting 0.95																																		
d. Required from allowable negative phase current PG4 [kVA]	$PG4 = \frac{1}{KG4} \sqrt{ \{ (0.432R)^2 + (1.23 \Delta P)^2 \} \times (1-3U+3U^2) }$	Value of decrease factor of load starting (fv) <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th rowspan="2">Number of Poles</th> <th colspan="4">Pm / Σ P0</th> <th rowspan="2">Remarks</th> </tr> <tr> <th>0~</th> <th>0.8</th> <th>0.9</th> <th>1</th> </tr> </thead> <tbody> <tr> <td>2P</td> <td>1</td> <td>0.9</td> <td>0.85</td> <td>0.8</td> <td>PG3 , fv1</td> </tr> <tr> <td>Over 4P</td> <td>1</td> <td>0.95</td> <td>0.95</td> <td>0.9</td> <td>PE2-2 , fv3</td> </tr> <tr> <td>2P</td> <td>0.9</td> <td>0.85</td> <td>0.85</td> <td>0.8</td> <td>PE2-1 ,fv2</td> </tr> <tr> <td>Over 4P</td> <td>0.9</td> <td>0.9</td> <td>0.9</td> <td>0.9</td> <td></td> </tr> </tbody> </table>	Number of Poles	Pm / Σ P0				Remarks	0~	0.8	0.9	1	2P	1	0.9	0.85	0.8	PG3 , fv1	Over 4P	1	0.95	0.95	0.9	PE2-2 , fv3	2P	0.9	0.85	0.85	0.8	PE2-1 ,fv2	Over 4P	0.9	0.9	0.9	0.9	
Number of Poles	Pm / Σ P0				Remarks																															
	0~	0.8	0.9	1																																
2P	1	0.9	0.85	0.8	PG3 , fv1																															
Over 4P	1	0.95	0.95	0.9	PE2-2 , fv3																															
2P	0.9	0.85	0.85	0.8	PE2-1 ,fv2																															
Over 4P	0.9	0.9	0.9	0.9																																
Where		η L : General Efficiency 0.85 φ L : General Power Factor 0.80 α : Demand Factor 0.90 Xd' : Alternator Factor 0.25 Σ P0 : Total load capacity covered by generator in kW (Excluding Stand-by) Note 1 Sf : Current increasing factor due to unbalanced load (= 1+0.6×(Δ P ÷ Σ P0)) 1.00 Δ E : Allowable voltage drop factor 0.25 γ G : Tolerant capacity for momentary overload of Alternator 1.5 φ m :Max. motor power factor 0.85																																		

Note1: To exchange kVA load into kW , single phase load to be multiplied by 0.8 , rectifier to be calculated as multiplying of rated Dc voltage and DC current, UPS to be calculated as multiplying of rated output in kVA and 0.9 , and these exchanged value to be added to three phase load capacity in kW.

D. WTP [Phase 3]

6. Capacity Calculation of Engine

Calculation Condition	Description		Value	Calculation Result	Value	Remarks	Generator efficiency		
	PG	Generator Output in kVA	2000				PE 1	2367.79	Rate
Pm	Maximum Motor	Load name	Raw Water Pump	PE 2-1	1481.96		kVA	2~8P	10~18P
		Starting Method	SOFT STERTER	PE 2-2	1747.75		20	79.0	-
		kW	450				37.5	82.5	-
Σ P0	Load Capacity Covered by Alt. (kW)		1457.525	PE max	2367.79		50	84.3	-
				Selected (PS)	2400	Diesel-engine generator , Radiator type	62.5	85.2	-
							75	85.7	-
							100	86.7	-
							125	87.6	-
							150	88.1	-
							200	88.9	-
							250	89.5	-
							300	90.0	-
							375	90.6	-
							500	91.3	-
							625	91.9	-
							750	92.3	91.7
							875	92.5	92.0
							1000	92.8	92.3
							1250	93.2	92.8
							1500	93.4	93.1
							2000	93.8	93.5
							2500	93.9	93.7
							3125	94.0	93.8

Calculation Formula	Calculation Result																								
<p>Maximum value or over among the following calculation is to be proposed as engine capacity.</p> <p>a. PE1 in PS is to be derived from requirement for full load running</p> $PE1 = \frac{PG \times \phi G}{\eta G} \times 1.36 \times \Delta H$ <p>b. PE2 in PS is to be derived from requirement of max. motor starting lastly</p> <p>① PE2-1 is to be derived from based on allowable load starting factor</p> $PE2-1 = fv2 \left\{ 0.75 \times \frac{1}{\eta 'G} \times (\Sigma P0 - Pm) \times \frac{\alpha}{\eta L} + \frac{1}{\epsilon \times \eta 'G} \times Pm \times \beta \times C \times \phi s \right\} \times 1.36 \times \Delta H$ <p>② PE2-2 is to be derived from tolerant capacity for momentary overload</p> $PE2-2 = \frac{fv3}{\eta G \times \gamma E} \times \left\{ (\Sigma P0 - Pm) \times \frac{\alpha}{\eta L} + Pm \times \beta \times C \times \phi s \right\} \times 1.36 \times \Delta H$																									
<p>Where</p> <p>Σ P0 : Total load capacity covered by generator in kW</p> <p>η L : General Efficiency</p> <p>φ L : General Power factor</p> <p>α : Demand Factor</p> <p>φ G : Generator Power factor</p> <p>γ E : Tolerant capacity for momentary overload of Engine</p> <p>β : Starting kVA for max. motor of per kW</p> <p>C : Motor starter factor</p> <p>φ s : Motor starting Power Factor for max. motor starting kVA , Squirrel cage</p> <p>η G : Generator efficiency</p> <p>η 'G : Generator overload efficiency</p> <p>fv2 : Decreased factor due to motor starting</p> <p>fv3 : Decreased factor due to motor starting</p> <p>ε : Tolerant capacity due to non-motor starting of Engine</p> <p>Δ H : Altitude compensation</p>	<table border="1"> <tbody> <tr><td>0.85</td></tr> <tr><td>0.8</td></tr> <tr><td>0.8</td></tr> <tr><td>0.8</td></tr> <tr><td>1.1</td></tr> <tr><td>7.2</td></tr> <tr><td>0.25</td></tr> <tr><td>0.4</td></tr> <tr><td>0.919</td></tr> <tr><td>0.855</td></tr> <tr><td>0.9</td></tr> <tr><td>1.0</td></tr> <tr><td>1.0</td></tr> <tr><td>1.0</td></tr> </tbody> </table>	0.85	0.8	0.8	0.8	1.1	7.2	0.25	0.4	0.919	0.855	0.9	1.0	1.0	1.0										
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D. WTP [Phase 3]
7. Fuel Calculation

Calculation Condition	Description		Value, Type	Calculation Result	Description		Value	Remarks
	PG	Generator output in kVA			2000	Fuel tank	15140.2 → 16000 L × 2 sets	
P	Engine output in PS		2400					
	Engine Type		Diesel-engine, Radiator type					
	Fuel Type		Light oil					

Fuel Tank Volume is to be derived from the following calculation.

a. Q [m3] Fuel Tank Volume

$$Q = \frac{P \times be \times H}{d} \times \alpha$$

be : Fuel consumption factor [unit : kg/PS·h]

Output (PS)	Diesel	Gas turbine
30 or less	0.23	-
over 30 and 250 or less	0.22	0.5
over 250 and 450 or less	0.2	0.48
over 450 and 750 or less	0.18	0.43
over 750	0.17	0.38

be : Fuel consumption factor kg/PS·h

H : Running hour hours

d : Fuel density kg/m3
(A heavy oil 850kg/m3)
(Light oil 830kg/m3)
(Kerosine 790kg/m3)

α : Surplus Factor

Calculation Formula