

7.3

Mechanical Equipment



1 Mechanical Calculation of Master plan

This chapter does a calculation about the capacity of the machine.

1.1 Lift pump

1.1.1 Necessary condition

Design maximum daily wastewater flow

- 512,000 m³/day

1.1.2 Necessary pumps units and capacity

It as same as sewage pumping station

1.2 Raw sludge pump

1.2.1 Necessary condition

Design maximum daily wastewater flow

- 512,000 m³/day

Design raw sludge generation volume

- Solids volume 53.76 t/day
- Moisture content 98 %
- Sludge volume 2,688 m³/day

1.2.2 Necessary pump units

Facilitate 2(1) pumps per train. 8 trains are total. Therefore,

8trains * 2(1) unit/1train = 16(8) units

1.2.3 Necessary pump capacity (Q)

Operation time is 12 hours per day.

$$Q = V_o / (\text{units} * 12 * 60)$$

$$= 2,688 / (8 * 12 * 60)$$

$$= 0.46 \rightarrow 0.5 \text{ m}^3/\text{min}$$

- Q : Necessary pump capacity (m³/min)
- V_o : Sludge volume = 2,688 m³/day

1.2.4 Pump diameter (D)

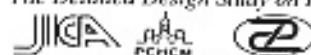
$$D = 146\sqrt{Q / V_e}$$

$$= 146\sqrt{0.5 / 2.5}$$

$$= 65.29 \rightarrow 80 \text{ mm}$$

- D : Pump diameter (mm)
- Q : Pump capacity = 0.5 m³/min
- V_e : Suction flow velocity = 2.5 m/s

1.2.5 Pump head (H)



$$H = h_1 + h_2 + h_3$$

$$= 2 + 11 + 1$$

$$= 14 \text{ m}$$

- H : Pump head (m)
- h₁ : Static head, = 2 m
- h₂ : Pipe loss head, = 11 m
- h₃ : Residual velocity head, = 1 m

1.2.6 Pump input power (P)

$$P = (0.163 * Q * \gamma * H * \alpha) / \rho$$

$$= (0.163 * 1.0 * 1.05 * 14 * 1.2) / 0.65$$

$$= 4.4 \rightarrow 5.5 \text{ kw}$$

- Q : Pump capacity = 0.5 m³/min * 2units
- γ : Fluid density = 1.05
- H : Pump head = 14 m
- α : Allowance = 1.2
- ρ : Pump efficiency = 0.65

1.2.7 Spec

- ϕ 80 mm * 0.5 m³/min * 14 m * 5.5 kw

1.3 Return sludge pump

1.3.1 Necessary condition

Design maximum daily wastewater flow

- 512,000 m³/day

Design return sludge volume

- return sludge ratio 50~100 %
- 512,000 m³/day * 50~100 % = 256,000 ~ 512,000 m³/day
- 64,000 m³/day * 50~100 % = 32,000 ~ 64,000 m³/day

1.3.2 Necessary pump units

$$\begin{array}{l} \text{Facilitate } \left\{ \begin{array}{l} 25 \% * 4 \text{ units} \\ 50 \% * 2 \text{ units} \end{array} \right\} \text{ pumps per train.} \\ 32,000 \sim 64,000 \text{ m}^3/\text{day} \\ 25 \% * 4 \text{ units} = 32,000 \text{ m}^3/\text{day} \\ 50 \% * 2 \text{ units} = 32,000 \text{ m}^3/\text{day} \\ \hline = 64,000 \text{ m}^3/\text{day} \end{array}$$

1.3.3 Necessary pump capacity (Q)

$$(25\%)Q = V_0 / (\text{units} * 24 * 60)$$

$$= 32,000 / (4 * 24 * 60)$$

$$= 5.55 \rightarrow 5.6 \text{ m}^3/\text{min}$$

- Q : Necessary pump capacity (m³/min)



- V_o : Sludge volume = 32,000 m³/day

$$\begin{aligned}(50\%)Q &= V_o / (\text{units} \times 24 \times 60) \\ &= 32,000 / (2 \times 24 \times 60) \\ &= 11.11 \rightarrow 11.2 \text{ m}^3/\text{min}\end{aligned}$$

- Q : Necessary pump capacity (m³/min)
- V_o : Sludge volume = 32,000 m³/day

1.3.4 Pump diameter (D)

$$\begin{aligned}(25\%)D &= 146\sqrt{Q / V_e} \\ &= 146\sqrt{5.6 / 2.5} \\ &= 218 \rightarrow 250 \text{ mm}\end{aligned}$$

- D : Pump diameter (mm)
- Q : Pump capacity = 5.6 m³/min
- V_e : Suction flow velocity = 2.5 m/s

$$\begin{aligned}(50\%)D &= 146\sqrt{Q / V_e} \\ &= 146\sqrt{11.2 / 2.5} \\ &= 309 \rightarrow 300 \text{ mm}\end{aligned}$$

- D : Pump diameter (mm)
- Q : Pump capacity = 11.2 m³/min
- V_e : Suction flow velocity = 2.5 m/s

1.3.5 Pump head (H)

$$\begin{aligned}(25\%)H &= h_1 + h_2 + h_3 \\ &= 1.5 + 3.5 + 1 \\ &= 6 \text{ m}\end{aligned}$$

- H : Pump head (m)
- h_1 : Static head = 1.5 m
- h_2 : Pipe loss head = 3.5 m
- h_3 : Residual velocity head = 1 m

$$\begin{aligned}(50\%)H &= h_1 + h_2 + h_3 \\ &= 1.5 + 4.5 + 1 \\ &= 7 \text{ m}\end{aligned}$$

- H : Pump head (m)
- h_1 : Static head = 1.5 m
- h_2 : Pipe loss head = 4.5 m
- h_3 : residual velocity head = 1 m

1.3.6 Pump input power (P)

$$\begin{aligned}(25\%)P &= (0.163 \times Q \times \gamma \times H \times \alpha) / \rho \\ &= (0.163 \times 5.6 \times 1.05 \times 6 \times 1.2) / 0.65 \\ &= 10.61 \rightarrow 11 \text{ kw}\end{aligned}$$

- Q : Pump capacity = 5.6 m³/min
- γ : Fluid density = 1.05
- H : Pump head = 6 m
- α : Allowance = 1.2
- ρ : Pump efficiency = 0.65

$$\begin{aligned} (50\%)P &= (0.163 * Q * \gamma * H * \alpha) / \rho \\ &= (0.163 * 11.2 * 1.05 * 7 * 1.2) / 0.65 \\ &= 24.77 \rightarrow 30\text{kw} \end{aligned}$$

- Q : Pump capacity = 11.2 m³/min
- γ : Fluid density = 1.05
- H : Pump head = 7m
- α : Allowance = 1.2
- ρ : Pump efficiency = 0.65

1.3.7 Spec

- (25%) ϕ 200 mm * 5.6 m³/min * 6 m * 11 kw
- (50%) ϕ 300 mm * 11.2 m³/min * 7 m * 30 kw

1.4 Excess sludge pump

1.4.1 Necessary condition

Design maximum daily wastewater flow

- 512,000 m³/day

Design excess sludge generation volume

- Solids volume 38.39 t/day
- Moisture content 99.4 %
- Sludge volume 6,397.5 m³/day

1.4.2 Necessary pump units

Facilitate 2(1) pumps per train, 8 trains are total. Therefore

$$8\text{train} * 2(1) \text{ unit} / 1\text{train} = 16(8)\text{units}$$

1.4.3 Necessary pump capacity (Q)

Operation time is 12hours per day.

$$\begin{aligned} Q &= V_o / (\text{units} * 12 * 60) \\ &= 6,397.5 / (8 * 12 * 60) \\ &= 1.11 \rightarrow 1.2 \text{ m}^3/\text{min} \end{aligned}$$

- Q : Necessary pump capacity (m³/min)
- V_o : Sludge volume = 6,397.5 m³/day

1.4.4 Pump diameter (D)

$$\begin{aligned} D &= 146\sqrt{(Q / V_e)} \\ &= 146\sqrt{(1.2 / 2.5)} \end{aligned}$$



$$= 101.15 \rightarrow 100 \text{ mm}$$

- D : Pump diameter (mm)
- Q : Pump capacity = 1.2 m³/min
- V_e : Suction flow velocity = 2.5 m/s

1.4.5 Pump head (H)

$$H = h_1 + h_2 + h_3$$

$$= 2 + 10 + 1$$

$$= 13 \text{ m}$$

- H : Pump head (m)
- h₁ : Static head = 2 m
- h₂ : Pipe loss head = 10 m
- h₃ : Residual velocity head = 1 m

1.4.6 Pump input power (P)

$$P = (0.163 * Q * \gamma * H * \alpha) / \rho$$

$$= (0.163 * 2.4 * 1.05 * 13 * 1.2) / 0.65$$

$$= 9.8 \rightarrow 11 \text{ kw}$$

- Q : Pump capacity = 1.2 m³/min * 2units
- γ : Fluid density = 1.05
- H : Pump head = 13 (m)
- α : Allowance = 1.2
- ρ : Pump efficiency = 0.65

1.4.7 Spec

- ϕ 100mm * 1.2 m³/min * 13 m * 11 kw

1.5 Blower equipment

1.5.1 Necessary condition

Design maximum daily wastewater flow

- 512,000 m³/day

Influx water quality

- BOD : 120 mg
- S-BOD : 80 mg
- SS : 105 mg
- kj - N : 30 mg

Water temp 33 °C (River average Water temp 30°C)

Temp 26 °C

MLSS 2,000 mg/l

HRT 6 hr

E-S-C 38,385 kgSS/day

Nitrogen content. 0.08 kgN/kgSS



1.5.2 Actual oxygen requirements (AOR)

$$\text{AOR} = \text{Od1} + \text{Od2} + \text{Od3} + \text{Od4}$$

$$= 36,864 + 17,386 + 56,160 + 0$$

$$= 110,410 \text{ (kgO}_2\text{/day)}$$

- Od1 : Amount of oxygen. That oxidizes BOD (kgO₂/day)
- Od2 : Amount of oxygen. That endogenous respiration (kgO₂/day)
- Od3 : Amount of oxygen. That nitrification (kgO₂/day)
- Od4 : Oxygen in A/T outflow.(kgO₂/day)

$$\begin{aligned} \textcircled{1} \text{ Od1} &= A * (\text{Removal BOD} - \text{nitrification} * K) \\ &= 0.6 * (512,000 * 120 * 10^{-3}) \\ &= 36,864 \text{ (kgO}_2\text{/day)} \end{aligned}$$

- A: Amount of oxygen. That removal BOD = 0.6
- K: BOD consumption by nitrifications = 2.86
- ※ This plan is not nitrification. Therefore

$$\begin{aligned} \textcircled{2} \text{ Od2} &= B * V_A * \text{MLVSS} \\ &= 0.1 * 129,360 * (0.84 * 2,000) * 0.8 * 10^{-3} \\ &= 17,386 \text{ (kgO}_2\text{/day)} \end{aligned}$$

- B : Amount of oxygen. That endogenous respiration per An MLVSS = 0.1
- V_A : aerobics volume part of aeration tank = (1,617m³ * 80 = 129,360 m³)
- MLVSS / MLSS : 0.8

$$\begin{aligned} \textcircled{3} \text{ Od3} &= C * (\text{kj} - \text{N volume nitrified}) \\ &= 4.57 * (512,000 * 30 * 10^{-3} - 0 - 3,071) \\ &= 56,160 \text{ (kgO}_2\text{/day)} \end{aligned}$$

- C : Amount of oxygen. That nitrification = 4.57
- kj-N volume nitrified : (kj-N inflow volume) - (kj-N outflow volume) - (kj-N removal volume at excess sludge)
- kj-N inflow volume = 30mg
- kj-N outflow volume = 0mg
- kj-N removal volume at excess sludge

$$= \text{Excess sludge volume} * \text{nitrogen content}$$

$$= 38,385 \text{ kgSS/day} * 0.08 \text{ kgN/kgSS}$$

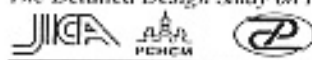
$$= 3,071 \text{ kgN/day}$$

$$\textcircled{4} \text{ Od4} = 0 \text{ (※As it miss out, it extremely little)}$$

1.5.3 Standard oxygen requirements (SOR)

$$\begin{aligned} \text{SOR} &= ((\text{AOR} * C_{sw} * \gamma) / (1.024^{(T-20)} * \alpha (\beta * C_s * \gamma - C_A))) * 760 / P \\ &= ((110,410 * 8.84 * 1.27) / (1.024^{(33-20)} * 0.83(0.95 * 7.23 * 1.27 - 2))) * 760 / 760 \\ &= 163,339 \text{ (kgO}_2\text{/day)} \end{aligned}$$

- C_{sw} : Density saturated oxygen at 20°C = 8.84
- γ : Aeration depth by correction of C_s.



$$\begin{aligned}
 &= 1 + (H / 2) / 10.24 \\
 &= 1 + (5.5 / 2) / 10.24 \\
 &= 1.27
 \end{aligned}$$

- H : Aeration depth = 5.5 m
 - T : Mixed sewage (Waste water and Activated sludge) temp = 33°C
 - α : Correction of K_{la} = 0.83
 - β : Correction of Density saturated oxygen. = 0.95
 - C_s : Density saturated oxygen at T°C = 7.23
 - C_A : Average DO of mixed sewage. = 2 mg/l
 - P : Atmospheric pressure. = 760 mmHg
- $$\begin{aligned}
 &= ((110,410 * 8.84 * 1.27) / (1.024^{(33-20)} \\
 &\quad * 0.83(0.95 * 7.23 * 1.27 - 2))) * 760 / 760 \\
 &= 163,339 \text{ (kgO}_2\text{/day)}
 \end{aligned}$$

1.5.4 Arithmetic of necessary air content

$$\begin{aligned}
 Q &= \text{SOR} / E_A * 10^{-2} * \rho * O_w \\
 &= 163,339 / 10 * 10^{-2} * 1.293 * 0.233 \\
 &= 5,421,699 \text{ (Nm}^3\text{/day)}
 \end{aligned}$$

- SOR : Standard oxygen requirements. = 163,339(kgO₂/day)
- E_A : Oxygen transfer efficiency at mixed sewage. = 7.5 % ~ 15 %
- ρ : Atmospheric density. = 1.293 (kgAir/Nm³)
- O_w : Oxygen weight per atmospheric. = 0.233 (kgO₂/kgAir)

$$\text{Air content / 1train} = 5,421,699 / 8 = 677,712 \text{ (Nm}^3\text{/day)}$$

1.5.5 1-Blower capacity = Air content / 1 train

$$\begin{aligned}
 Q1 &= 677,712 \text{ (Nm}^3\text{/day)} \\
 &= 470.3 \rightarrow 470 \text{ (Nm}^3\text{/min)} \\
 Q2 &= Q1 * (273 + T) / 273 * \alpha \\
 &= 470 * (273 + 33) / 273 * 1.15 \\
 &= 605 \rightarrow 600 \text{ (m}^3\text{/min)} \\
 T &: 33^\circ\text{C} \\
 \alpha &: \text{Allowance} = 15\%
 \end{aligned}$$

1.5.6 Spec

- $\phi 700 * \phi 600 * 600 \text{ (m}^3\text{/min)} * 6,800 \text{ mmAq} * 810 \text{ kw} * 9(1) \text{ units}$

1.6 Diffuser

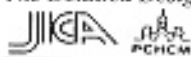
1.6.1 Necessary condition

$$\text{1-Blower capacity} = \text{Air content} / \text{1train}$$

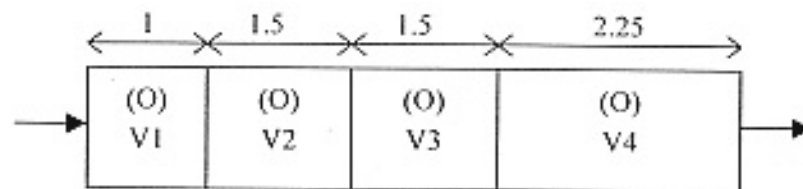
- $Q1 = 600 \text{ m}^3\text{/min}$

$$\text{Air content / 1units}$$

- $Q2 = 600 / 10$
 $= 60 \text{ m}^3\text{/min}$



Aeration tank volume



- $V1 = W10.5m * L(28m / 6.25) * 1 * H5.5m = 258.72 m^3$
- $V2 = W10.5m * L(28m / 6.25) * 1.5 * H5.5m = 388.08 m^3$
- $V3 = W10.5m * L(28m / 6.25) * 1.5 * H5.5m = 388.08 m^3$
- $V4 = W10.5m * L(28m / 6.25) * 2.25 * H5.5m = 582.12 m^3$
- $V_{all} = V1 + V2 + V3 + V4 = 1617 m^3$

1.6.2 Air content / V_x

- Air content / $V1 = 60 m^3/min * 258.72 m^3 / 1617 m^3 = 9.6 m^3/min$
- Air content / $V2 = 60 m^3/min * 388.08 m^3 / 1617 m^3 = 14.4 m^3/min$
- Air content / $V3 = 60 m^3/min * 388.08 m^3 / 1617 m^3 = 14.4 m^3/min$
- Air content / $V4 = 60 m^3/min * 582.12 m^3 / 1617 m^3 = 21.6 m^3/min$

1.6.3 Diffuser air content

- Diffuser = 120 l/min/unit

1.6.4 Necessary Diffuser units

- $V1 = 9.6 / 0.12 = 80$ units
- $V2 = 14.4 / 0.12 = 120$ units
- $V3 = 14.4 / 0.12 = 120$ units
- $V4 = 21.6 / 0.12 = 180$ units
- Sum = $80 + 120 + 120 + 180 = 500$ units
- Total = $500 \text{ units} * 10 \text{ units} * 8 \text{ strains} = 40,000$ units

1.6.5 Spec

- $120 (l/min) * 40,000$ units

1.7 Chlorination

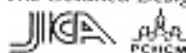
1.7.1 Necessary condition

Design maximum daily wastewater flow

- $512,000 m^3/day$

Chemical infuse rate.

- $2 \sim 4 \text{ ppm}$ (Usually 3 ppm)



1.7.2 Necessary chemical volume (Q1) and tank capacity (Q2)

$$\begin{aligned} Q1 &= Q * R * 10^{-6} * (100 / \alpha) * (1 / \beta) \\ &= 512,000 * 3\text{ppm} * 10^{-6} * (100 / 10) * (1 / 1.1) \\ &= 13.9 \text{ m}^3/\text{day} \end{aligned}$$

- Q : 512,000 m³/day
- R : Chemical infuse rate. = 3 ppm
- α : Effective chlorine density. = 10 %
- β : Density = 1.1 (at 10%)

Storage days of chemical are a one-week.

Units are 8 units

$$\begin{aligned} Q2 &= 13.9 \text{ m}^3/\text{day} * 7 \text{ days} * (1 / 8) \\ &= 12.16 \rightarrow 13 \text{ m}^3 \end{aligned}$$

1.7.3 Necessary pump capacity (Q3)

$$\begin{aligned} Q3 &= Q * R * 10^{-6} * (1 / 24) * (100 / \alpha) * (1 / \beta) * (1 / \text{unit}) \\ &= 512,000 * 2 \sim 4 \text{ ppm} * 10^{-6} * (1 / 24) * (100 / 10) * (1 / 1.1) * (1 / 8) \\ &= 0.049 \sim 0.097 \text{ m}^3/\text{h} \rightarrow 0.81 \sim 1.62 \text{ l/min} \end{aligned}$$

- Q : 512,000 m³/day
- R : Chemical infuse rate. = 2 ~ 4 ppm (Usually 3 ppm)
- α : Effective chlorine density. = 10 %
- β : Density = 1.1 (at 10 %)
- Unit : 8units

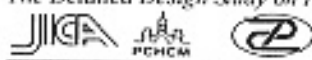
1.7.4 Spec

- Sodium Hypochlorite tank : 13 m³
- Sodium hypo chlorite pump : $\phi 25 * 0.81 \sim 1.62 \text{ l/min}$

1.8 Sand filtration

1.8.1 Necessary condition

Secondary effluent.



Name	Use pressure (Mpa)	Use volume (L/min)
Sprinkling nozzle	1.96	1,000
Antifoaming nozzle: (Gravity type thickened)	1.96	320
Antifoaming nozzle (Aeration tank)	0.98	26,320
Cyclone separator: 6units (Washing) 1units	1.47	500
Centrifugal: 6units (Washing) 1units	1.47	500
Total		28,640

Sand filtration effluent

Name	Use pressure (Mpa)	Use volume (L/min)
Sprinkling nozzle	1.96	(1,000)
Main pump: 6units	1.96	105
Blower: 9units (Coolant): 8units	0.98	774
Cyclone separator: 6units (Coolant) 4units	0.98	400
Centrifugal: 6units (Coolant) 4units	0.98	400
Chemical dissolution water	0.98	670
Total		2,349 (3,349)

Design of sand filtration effluent volume

$$Q = 2.4 \text{ m}^3/\text{min} (2,349 \text{ l/min}) * 24 * 60$$

$$= 3,456 \text{ m}^3/\text{day}$$

Filtration rate

$$V = 200 \text{ m}^3/\text{day}$$

Filtration area.

$$D = Q / V$$

$$= 3,456 / 200$$

$$= 17.28 \rightarrow 20 \text{ m}^2$$

1.8.2 Necessary sand filtration units

A one unit is Maximum filtration area of 5 m^2 .

$$20 \text{ m}^2 / 5 \text{ m}^2 = 4 \text{ units}$$

- 4 units

1.8.3 Sand filtration charges pump capacity.

$$5 \text{ m}^2 * 200 \text{ m}^3/\text{day} = 1,000 \text{ m}^3/\text{day}$$



- $0.7 \text{ m}^3/\text{min}$

1.8.4 Spec

- Sand filtration : $5 \text{ m}^2 \times 4 \text{ units}$
- Charge pump : $\phi 80 \times 0.7 \text{ m}^3/\text{min} \times 4 \text{ units}$

1.9 Thickened sludge pump

1.9.1 Necessary condition

Design maximum daily wastewater flow

- $512,000 \text{ m}^3/\text{day}$

Design thickened sludge generation volume

- Solids volume 53.76 t/day
- Moisture content 97%
- Sludge volume $1,792 \text{ m}^3/\text{day}$

1.9.2 Necessary pump units

Facilitate 2(1) pumps per a thickened tank.

4 Thickened tank are total. Therefore

- $4 \text{ tank} \times 2(1) \text{ pumps} = 8(4) \text{ units}$

1.9.3 Necessary pump capacity (Q)

Operation time is 12 hours per day.

$$Q = V_o / (\text{units} \times 12 \times 60)$$

$$= 1,792 / (4 \times 12 \times 60)$$

$$= 0.62 \rightarrow 0.7 \text{ m}^3/\text{min}$$

- Q : Necessary pump capacity (m^3/min)
- V_o : Sludge volume = $1,792 \text{ m}^3/\text{day}$

1.9.4 Pump diameter (D)

$$D = 146 \sqrt{Q / V_e}$$

$$= 146 \sqrt{0.7 / 2.5}$$

$$= 77.2 \rightarrow 80 \text{ mm}$$

- D : Pump diameter mm
- Q : Pump capacity = $0.7 \text{ m}^3/\text{min}$
- V_e : Suction flow velocity = 2.5 m/s

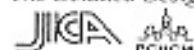
1.9.5 Pump head (H)

$$H = h_1 + h_2 + h_3$$

$$= 1 + 8 + 1$$

$$= 10 \text{ m}$$

- H : Pump head (m)
- h_1 : Static head = 1 m
- h_2 : Pipe loss head = 8 m
- h_3 : Residual velocity head = 1 m

**1.9.6 Pump input power (P)**

$$P = (0.163 * Q * \gamma * H * \alpha) / \rho$$

$$= (0.163 * 1.4 * 1.05 * 10 * 1.2) / 0.65$$

$$= 4.4 \rightarrow 5.5 \text{ kw}$$

- Q : Pump capacity = $0.7 \text{ m}^3/\text{min} * 2 \text{ units}$
- γ : Fluid density = 1.05
- H : Pump head = 10 m
- α : Allowance = 1.2
- ρ : Pump efficiency = 0.65

1.9.7 Spec

- $\phi 80 \text{ mm} * 0.7 \text{ m}^3/\text{min} * 10 \text{ m} * 5.5 \text{ kw}$

1.10 Centrifugal thickener**1.10.1 Necessary condition**

Design maximum daily wastewater flow

- $512,000 \text{ m}^3/\text{day}$

Design excess sludge generation volume

- Solids volume 38.39 t/day
- Moisture content 99.4%
- Sludge volume $6,397.5 \text{ m}^3/\text{day}$

1.10.2 Necessary Centrifugal thickener units

Facilitate (2trains of WWTP = 1trains of STP)

$8 \text{ trains} / 2 \text{ trains} = 4 \text{ trains}$

$1 \text{ train} = 1 \text{ unit}, + 2 \text{ unit stand-by}$

$4 \text{ trains} * 1 \text{ unit} = 4 \text{ units} + 2 \text{ units stand-by.}$

1.10.3 Necessary Centrifugal thickener capacity (Q)

Operation time is 24hours per day.

$$Q = V_o / (\text{units} * 24)$$

$$= 6,397.5 / (4 * 24)$$

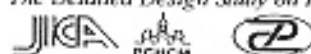
$$= 66.6 \rightarrow 70 \text{ m}^3/\text{h}$$

- Q : Necessary Centrifugal thickener capacity (m^3/h)
- V_o : Sludge volume = $6,397.5 \text{ m}^3/\text{day}$

1.10.4 spec

- $70 \text{ m}^3/\text{h} * 112.75 \text{ kw}$

1.11 Centrifugal thickener charge pump**1.11.1 Necessary condition**



Design maximum daily wastewater flow

- 512,000 m³/day

Design thickened sludge generation volume

- Solids volume 38.39 t/day
- Moisture content 99.4 %
- Sludge volume 6,387.5 m³/day

1.11.2 Necessary pump units

Take into consideration centrifugal thickener 1unit = charge pump 1unit

- Centrifugal thickener 6(2) units = Charge pump 6(2) units

1.11.3 Necessary pump capacity (Q)

Centrifugal thickener 70m³/h

Facilitate pump capacity is 0.5~1.5 times as Centrifugal thickener capacity.

$$Q = V_o * 0.5 \sim 1.5$$

$$= 70 * 0.5 \sim 1.5$$

$$= 35 \sim 105 \text{ m}^3/\text{min} \text{ (70 m}^3/\text{h)}$$

- Q : Necessary pump capacity (m³/min)
- V_o : Centrifugal thickener capacity = 70 m³/h

1.11.4 Spec

- ϕ 250 mm * 35 ~ 105 m³/min * 10 m * 30 kw

1.12 Centrifugal dehydrator

1.12.1 Necessary condition

Design maximum daily wastewater flow

- 512,000 m³/day

Design thickened sludge generation volume

- Solids volume 92.16 t/day
- Moisture content 96.65 %
- Sludge volume 2,752 m³/day

Operation days / week

- 7days / 1week

Operation hours / day

- 24hours / 1day

1.12.2 Necessary centrifugal dehydrator units

- 4 units

1.12.3 Necessary centrifugal dehydrator capacity (Q)

Operation days are 7days / week.

Operation hours are 24h / day.

$$Q = (V_o * 7 / 7) / (U * T)$$



$$= (2,752 \times 7 / 7) / (4 \times 24)$$

$$= 28.6 \rightarrow 30 \text{ m}^3/\text{h}$$

- Q : Necessary centrifugal dehydrator (m^3/h)
- V_o : Sludge volume = $2,752 \text{ m}^3/\text{day}$
- T : Operation hours = 24h
- U : units = 4

1.12.4 spec

- $30 \text{ m}^3/\text{h} \times 147.4 \text{ kw}$

1.13 Centrifugal dehydrator charge pump

1.13.1 Necessary condition

Design maximum daily wastewater flow

- $512,000 \text{ m}^3/\text{day}$

Design thickened sludge generation volume

- Solids volume 92.16 t/day
- Moisture content 96.65%
- Sludge volume $2,752 \text{ m}^3/\text{day}$

1.13.2 Necessary pump units

Take into consideration centrifugal dehydrator 1 unit = charge pump 1 unit

- Centrifugal dehydrator 6(2)units = Charge pump 6(2) units

1.13.3 Necessary pump capacity (Q)

Centrifugal dehydrator $30 \text{ m}^3/\text{h}$

Facilitate pump capacity is 0.5~1.5 times as centrifugal dehydrator capacity.

$$Q = V_o \times 0.5 \sim 1.5$$

$$= 30 \times 0.5 \sim 1.5$$

$$= 15 \sim 45 \text{ m}^3/\text{h} \text{ (10 m}^3/\text{h)}$$

- Q : Necessary pump capacity (m^3/h)
- V_o : Centrifugal dehydrator capacity = $30 \text{ m}^3/\text{h}$

1.13.4 Spec

- $\phi 125 \text{ mm} \times 15 \sim 45 \text{ m}^3/\text{min} \times 10 \text{ m} \times 11 \text{ kw}$

1.14 Drainage pump

1.14.1 Necessary condition

Design maximum daily wastewater flow

- $512,000 \text{ m}^3/\text{day}$

Flow rate of extracted

- From Cyclone Separators : about $5,200 \text{ m}^3/\text{day}$
- From Centrifugal Separators : about $2,100 \text{ m}^3/\text{day}$



- Grand total : 7,300 m³/day

1.14.2 Necessary pump units

Facilitate 2(1) pumps for 1 Drainage Tank; there are 2 Tanks in total, therefore:

$$2 \text{ tanks} * 2(1) \text{ unit/1 tanks} = 4(2) \text{ units}$$

1.14.3 Necessary pump capacity (Q)

Operation time is 24 hours per day.

$$Q = V_o / (24 * 60)$$

$$= 7,300 / (24 * 60)$$

$$= 5.06 \rightarrow 5.1 \text{ m}^3/\text{min}$$

- Q : Necessary pump capacity (m³/min)
- V_o : Total amount of Drainage Water = 7,300 m³/day

1.14.4 Pump diameter (D)

$$D = 146 \sqrt{(Q / V_e)}$$

$$= 146 \sqrt{(5.1 / 2.5)}$$

$$= 208 \rightarrow 200 \text{ mm}$$

- D : Pump diameter (mm)
- Q : Pump capacity = 5.1 m³/min
- V_e : Suction flow velocity = 2.5 m/s

1.14.5 Pump head (H)

$$H = h_1 + h_2 + h_3$$

$$= 1 + 13 + 1$$

$$= 15 \text{ m}$$

- H : Pump head (m)
- h₁ : Static head, = 1 m
- h₂ : Pipe loss head, = 13 m
- h₃ : Residual velocity head, = 1 m

1.14.6 Pump input power (P)

$$P = (0.163 * Q * H * \alpha) / \rho$$

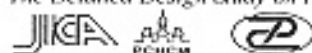
$$= (0.163 * 5.1 * 1.05 * 15 * 1.2) / 0.65$$

$$= 24.17 \rightarrow 30 \text{ kw}$$

- Q : Pump capacity = 5.1 m³/min
- γ : Fluid density = 1.05
- H : Pump head = 15 m
- α : Allowance = 1.2
- ρ : Pump efficiency = 0.65

1.14.7 Spec

- φ200 mm * 5.1 m³/min * 15 m * 30 kw



2 Mechanical calculation of Phase 1

This chapter does a calculation about the capacity of the machine.

2.1 Lift pump

2.1.1 Necessary condition

Design maximum daily wastewater flow of Phase 1.

- 141,000 m³/day

2.1.2 Necessary pumps units and capacity

This pump equipment is as same as intermediate pumping station.

2.2 Raw sludge pump

2.2.1 Necessary condition

Design maximum daily wastewater flow

- 141,000 m³/day

Design raw sludge generation volume

- Solids volume 10.36 t/day
- Moisture content 98 %
- Sludge volume 518.2 m³/day

2.2.2 Necessary pump units

Facilitate 2 pumps per train. Phase 1 are 1 train. Therefore,

1trains * 2 unit / 1train = 2 units+1stand-by

2.2.3 Necessary pump capacity (Q)

Operation time is 12 hours per day.

$$Q = V_o / (\text{units} * 12 * 60)$$

$$= 518.2 / (2 * 12 * 60)$$

$$= 0.36 \rightarrow 0.5 \text{ m}^3/\text{min}$$

- Q : Necessary pump capacity (m³/min)
- V_o : Sludge volume = 518.2 m³/day

2.2.4 Pump diameter (D)

$$D = 146 \sqrt{Q / V_e}$$

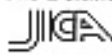
$$= 146 \sqrt{0.5 / 2.5}$$

$$= 65.29 \rightarrow 80 \text{ mm}$$

- D : Pump diameter (mm)
- Q : Pump capacity = 0.5 m³/min
- V_e : Suction flow velocity = 2.5 m/s

2.2.5 Pump head (H)

h_l : Static head. = 2m



h_2 : Pipe loss head. = 11m

h_3 : Residual velocity head = 1m

$H = h_1 + h_2 + h_3$

= 2 + 11 + 1

= 14 → 14 m

2.2.6 Pump input power (P)

$$P = (0.163 * Q * \gamma * H * \alpha) / \rho$$

$$= (0.163 * 0.5 * 1.05 * 14 * 1.2) / 0.3$$

$$= 4.79 \rightarrow 5.5 \text{ kw}$$

- Q : Pump capacity = 0.5 m³/min
- γ : Fluid density = 1.05
- H : Pump head = 14 m
- α : Allowance = 1.2
- ρ : Pump efficiency = 0.3

2.2.7 Spec

- ϕ 80 mm * 0.5 m³/min * 14 m * 5.5 kw
- 2units+1stand-by

2.3 Return sludge pump

2.3.1 Necessary condition

Design maximum daily wastewater flow

- 141,000 m³/day

Design return sludge volume

- return sludge ratio 5~10 %
- 141,000 m³/day * 5~10 % = 7,050 ~ 14,100 m³/day

2.3.2 Necessary pump units

Facilitate 10 % * 2 units pumps per train.

$$7,050 \text{ m}^3 * 2\text{units} = 14,100 \text{ m}^3$$

2.3.3 Necessary pump capacity (Q)

$$Q = V_0 / (\text{units} * 24 * 60)$$

$$= 7,050 / (1 * 24 * 60)$$

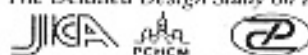
$$= 4.89 \rightarrow 5.6 \text{ m}^3/\text{min}$$

∴ It is made the thing of the capacity which is the same as the pump for the future so that it can use it in the future.

- Q : Necessary pump capacity (m³/min)
- V_0 : Sludge volume = 7,050 m³/day

2.3.4 Pump diameter (D)

$$D = 146\sqrt{Q / V_e}$$



$$= 146 \sqrt{(5.6 / 2.5)}$$

$$= 218 \rightarrow 250 \text{ mm}$$

- D : Pump diameter (mm)
- Q : Pump capacity = 5.6 m³/min
- Ve : Suction flow velocity = 2.5 m/s

2.3.5 Pump head (H)

h1 : Static head. = 1.5m

h2 : Pipe loss head. = 3.5m

h3 : Residual velocity head = 1m

$$H = h1 + h2 + h3$$

$$= 1.5 + 3.5 + 1$$

$$= 6 \text{ m}$$

2.3.6 Pump input power (P)

$$P = (0.163 * Q * \gamma * H * \alpha) / \rho$$

$$= (0.163 * 5.6 * 1.05 * 6 * 1.2) / 0.65$$

$$= 10.61 \rightarrow 11 \text{ kw}$$

- Q : Pump capacity = 5.6 m³/min
- γ : Fluid density = 1.5
- H : Pump head = 6 m
- α : Allowance = 1.2
- ρ : Pump efficiency = 0.65

2.3.7 Spec

- ϕ 200 mm * 5.6 m³/min * 6 m * 11 kw
- 2units+2stand-by

2.4 Excess sludge pump

2.4.1 Necessary condition

Design maximum daily wastewater flow

- 141,000 m³/day

Design excess sludge generation volume

- Solids volume 10.778 t/day
- Moisture content 99.4 %
- Sludge volume 1,796.3 m³/day

2.4.2 Necessary pump units

Facilitate 2 pumps per train. Phase I are 1 train. Therefore

$$1 \text{ train} * 2 \text{ unit} / 1 \text{ train} = 2 \text{ units}$$

2.4.3 Necessary pump capacity (Q)

Operation time is 12hours per day.



$$\begin{aligned}
 Q &= V_o / (\text{units} * 12 * 60) \\
 &= 1,796.3 / (2 * 12 * 60) \\
 &= 1.24 \rightarrow 1.2 \text{ m}^3/\text{min} \\
 &\bullet \quad Q : \text{Necessary pump capacity (m}^3/\text{min)} \\
 &\bullet \quad V_o : \text{Sludge volume} = 1,796.3 \text{ m}^3/\text{day}
 \end{aligned}$$

2.4.4 Pump diameter (D)

$$\begin{aligned}
 D &= 146 \sqrt{Q / V_e} \\
 &= 146 \sqrt{1.2 / 2.5} \\
 &= 101.15 \rightarrow 100 \text{ mm} \\
 &\bullet \quad D : \text{Pump diameter (mm)} \\
 &\bullet \quad Q : \text{Pump capacity} = 1.2 \text{ m}^3/\text{min} \\
 &\bullet \quad V_e : \text{Suction flow velocity} = 2.5 \text{ m/s}
 \end{aligned}$$

2.4.5 Pump head (H)

$$\begin{aligned}
 h_1 &: \text{Static head.} = 2\text{m} \\
 h_2 &: \text{Pipe loss head.} = 10\text{m} \\
 h_3 &: \text{Residual velocity head} = 1\text{m} \\
 H &= h_1 + h_2 + h_3 \\
 &= 2 + 10 + 1 \\
 &= 13 \text{ m}
 \end{aligned}$$

2.4.6 Pump input power (P)

$$\begin{aligned}
 P &= (0.163 * Q * \gamma * H * \alpha) / \rho \\
 &= (0.163 * 2.4 * 1.05 * 13 * 1.2) / 0.65 \\
 &= 9.8 \rightarrow 11 \text{ kw} \\
 &\bullet \quad Q : \text{Pump capacity} = 1.2 \text{ m}^3/\text{min} * 2\text{units} \\
 &\bullet \quad \gamma : \text{Fluid density} = 1.05 \\
 &\bullet \quad H : \text{Pump head} = 13 \text{ (m)} \\
 &\bullet \quad \alpha : \text{Allowance} = 1.2 \\
 &\bullet \quad \rho : \text{Pump efficiency} = 0.65
 \end{aligned}$$

2.4.7 Spec

- $\phi 100\text{mm} * 1.2 \text{ m}^3/\text{min} * 13 \text{ m} * 11 \text{ kw}$
- 2units+1 stand-by

2.5 Blower equipment

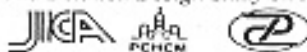
2.5.1 Necessary condition

Design maximum daily wastewater flow

- 141,000 m³/day

Air Feeding rate

- 2 ~ 4 times of wastewater volume



2.5.2 1-Blower capacity = Air content / 1 train

$$Q1 = 141,000 * 2 \sim 4 \text{ times}$$

$$= 282,000 \sim 564,000$$

$$= 195.8 \sim 391.6 \rightarrow 360 \text{ m}^3/\text{min}$$

2.5.3 Spec

- $\phi 600 * 360(\text{m}^3/\text{min}) * 6,800\text{mmAq} * 480\text{kw}$
- 1 units + 1 stand-by

2.6 Diffuser

2.6.1 Necessary condition

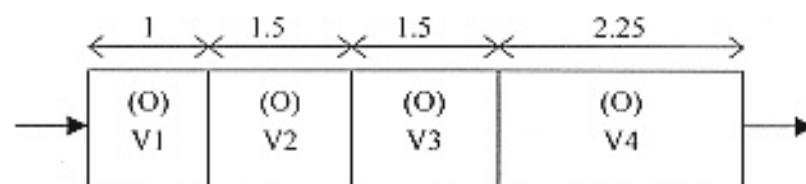
$$1\text{-Blower capacity} = \text{Air content} / 1 \text{ train}$$

- $Q1 = 360 \text{ m}^3/\text{min}$

$$\text{Air content} / 1 \text{ units}$$

- $Q2 = 360 / 10$
 $= 36 \text{ m}^3/\text{min}$

$$\text{Aeration tank volume}$$



- $V1 = W10.5\text{m} * L(28\text{m} / 6.25) * 1 * H5.5\text{m} = 258.72 \text{ m}^3$
- $V2 = W10.5\text{m} * L(28\text{m} / 6.25) * 1.5 * H5.5\text{m} = 388.08 \text{ m}^3$
- $V3 = W10.5\text{m} * L(28\text{m} / 6.25) * 1.5 * H5.5\text{m} = 388.08 \text{ m}^3$
- $V4 = W10.5\text{m} * L(28\text{m} / 6.25) * 2.25 * H5.5\text{m} = 582.12 \text{ m}^3$
- $V_{\text{all}} = V1 + V2 + V3 + V4 = 1617 \text{ m}^3$

2.6.2 Air content / Vx

- $\text{Air content} / V1 = 36 \text{ m}^3/\text{min} * 258.72 \text{ m}^3 / 1617 \text{ m}^3 = 5.76 \text{ m}^3/\text{min}$
- $\text{Air content} / V2 = 36 \text{ m}^3/\text{min} * 388.08 \text{ m}^3 / 1617 \text{ m}^3 = 8.64 \text{ m}^3/\text{min}$
- $\text{Air content} / V3 = 36 \text{ m}^3/\text{min} * 388.08 \text{ m}^3 / 1617 \text{ m}^3 = 8.64 \text{ m}^3/\text{min}$
- $\text{Air content} / V4 = 36 \text{ m}^3/\text{min} * 582.12 \text{ m}^3 / 1617 \text{ m}^3 = 12.96 \text{ m}^3/\text{min}$

2.6.3 Diffuser air content

- Diffuser = 120 l/min/unit

2.6.4 Necessary Diffuser units

- $V1 = 5.76 / 0.12 = 48 \text{ units}$
- $V2 = 8.64 / 0.12 = 72 \text{ units}$
- $V3 = 8.64 / 0.12 = 72 \text{ units}$



- $V4 = 12.96 / 0.12 = 108$ units
- $\text{Sum} = 48 + 72 + 72 + 108$
= 300 units
- $\text{Total} = 300\text{units} * 10\text{units} * 1\text{trains}$
= 3,000 units

2.6.5 Spec

- $120 (\text{l/min}) * 3,000$ units

2.7 Chlorination

2.7.1 Necessary condition

Design maximum daily wastewater flow

- $141,000 \text{ m}^3/\text{day}$

Chemical infuse rate.

- $2 \sim 4 \text{ ppm}$ (Usually 3 ppm)

2.7.2 Necessary chemical volume (Q1) and tank capacity (Q2)

$$\begin{aligned} Q1 &= Q * R * 10^{-6} * (100 / \alpha) * (1 / \beta) \\ &= 141,000 * 3\text{ppm} * 10^{-6} * (100 / 10) * (1 / 1.1) \\ &= 3.85 \text{ m}^3/\text{day} \end{aligned}$$

- $Q : 141,000 \text{ m}^3/\text{day}$
- $R : \text{Chemical infuse rate.} = 3 \text{ ppm}$
- $\alpha : \text{Effective chlorine density.} = 10 \%$
- $\beta : \text{Density} = 1.1 \text{ (at } 10\%)$

Storage days of chemical are a one-week.

Units are 8 units

$$\begin{aligned} Q2 &= 3.85 \text{ m}^3/\text{day} * 7 \text{ days} \\ &= 26.9 \rightarrow 13 \text{ m}^3 * 2\text{units} \end{aligned}$$

2.7.3 Necessary pump capacity (Q3)

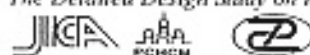
$$\begin{aligned} Q3 &= Q * R * 10^{-6} * (1 / 24) * (100 / \alpha) * (1 / \beta) * (1 / \text{unit}) \\ &= 141,000 * 2 \sim 4 \text{ ppm} * 10^{-6} * (1 / 24) * (100 / 10) * (1 / 1.1) * (1 / 2) \\ &= 0.054 \sim 0.107 \text{ m}^3/\text{h} \rightarrow 0.92 \sim 1.78 \text{ l/min} \end{aligned}$$

∴ It is made the thing of the capacity which is the same as the pump for the future so that it can use it in the future. Therefore, $0.82 \sim 1.62 \text{ l/min}$

- $Q : 141,000 \text{ m}^3/\text{day}$
- $R : \text{Chemical infuse rate.} = 2 \sim 4 \text{ ppm}$ (Usually 3 ppm)
- $\alpha : \text{Effective chlorine density.} = 10 \%$
- $\beta : \text{Density} = 1.1 \text{ (at } 10\%)$
- Unit : 2 units

2.7.4 Spec

- Sodium hypochlorite tank: $13 \text{ m}^3 * 2\text{units}$



- Sodium hypochlorite pump
: $\phi 25 \times 0.82 \sim 1.62 \text{ l/min} \times 2 \text{ units} + 2 \text{ stand-by}$

2.8 Sand filtration

2.8.1 Necessary condition

Secondary effluent.

Name	Use pressure (Mpa)	Use volume (L/min)
Sprinkling nozzle	1.96	(1,000)
Antifoaming nozzle: (Gravity type thickened)	1.96	440
Antifoaming nozzle (Aeration tank)	0.98	1,600
Centrifugal type thickener: 2 units (Washing) 1 units	1.47	850
Centrifugal type dehydrator: 2 units (Washing) 1 units	1.47	460
Total		3,350(4,350)

Sand filtration effluent

Name	Use pressure (Mpa)	Use volume (L/min)
Sprinkling nozzle	1.96	(1,000)
Blower: 2 units (Coolant): 1 units	0.98	230
Chemical dissolution water	0.98	230
Total		460 (1,460)

Design of sand filtration effluent volume

$$Q = 0.46 \text{ m}^3/\text{min} (460 \text{ l/min}) \times 24 \times 60 \\ = 662 \text{ m}^3/\text{day}$$

Filtration rate

$$V = 200 \text{ m/day}$$

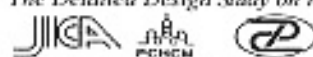
Filtration area.

$$D = Q / V \\ = 662 / 200 \\ = 3.31 \rightarrow 4 \text{ m}^2$$

2.8.2 Necessary sand filtration units

Though this necessary treatment area is 4m², it is made 5m² based on the plan in the future.

- 2 units (include 1 stand-by)

**2.8.3 Sand filtration charges pump capacity.**

$$5\text{ m}^2 * 200 \text{ m}^3/\text{day} = 1,000 \text{ m}^3/\text{day}$$

- $0.7 \text{ m}^3/\text{min}$

2.8.4 Spec

- Sand filtration: 5 m^2 *
: 1 units+1 stand-by
- Charge pump : $\phi 80 * 0.7 \text{ m}^3/\text{min} * 10\text{m}$
: 1 units+1 stand-by

2.9 Thickened sludge pump**2.9.1 Necessary condition**

Design maximum daily wastewater flow

- $141,000 \text{ m}^3/\text{day}$

Design thickened sludge generation volume

- Solids volume 10.364 t/day
- Moisture content 97%
- Sludge volume $345.5 \text{ m}^3/\text{day}$

2.9.2 Necessary pump units

Facilitate 2(1) pumps per a thickened tank.

1 Thickened tank are this time.

- $1 \text{ tank} * 2(1) \text{ pumps} = 2(1) \text{ units}$

2.9.3 Necessary pump capacity (Q)

Operation time is 12 hours per day.

$$Q = V_o / (\text{units} * 12 * 60)$$

$$= 345.5 / (1 * 12 * 60)$$

$$= 0.48 \rightarrow 0.7 \text{ m}^3/\text{min}$$

∴ It is made the thing of the capacity which is the same as the pump for the future so that it can use it in the future. Therefore, $0.7 \text{ m}^3/\text{min}$

- Q : Necessary pump capacity (m^3/min)
- V_o : Sludge volume = $345.5 \text{ m}^3/\text{day}$

2.9.4 Pump diameter (D)

$$D = 146 \sqrt{Q / V_e}$$

$$= 146 \sqrt{0.2 / 2.5}$$

$$= 77.2 \rightarrow 80 \text{ mm}$$

- D : Pump diameter mm
- Q : Pump capacity = $0.7 \text{ m}^3/\text{min}$
- V_e : Suction flow velocity = 2.5 m/s

2.9.5 Pump head (H)

h_1 : Static head.



$$h1 = (+8,000) - (+3,200)$$

$$= 4.8 \text{ m}$$

$h2$: Pipe loss head.

$$h2' = (10.666 * Q^{1.85}) * L / (110^{1.85} * D^{4.87})$$

$$= (10.666 * 0.011^{1.85}) * 60 / (110^{1.85} * 0.10^{4.87})$$

$$= 1.88 \text{ m}$$

- $h2'$: Pipe loss in the clear water
- Q : The amount of total flow = $0.7 \text{ m}^3/\text{min} * 1 \text{ units}$
 $= 0.7 \text{ m}^3/\text{min} \rightarrow 0.011 \text{ m}^3/\text{sec}$
- L : length of pipe = 60 m
- D : Diameter of pipe = 100 mm

$$h2 = \alpha * h2'$$

$$= 1.9 * 1.88$$

$$= 3.58 \rightarrow 4 \text{ m}$$

- α : Sludge factor = 1.9

$h3$: Residual velocity head

$$h3 = 1 \text{ m}$$

$$H = h1 + h2 + h3$$

$$= 4.8 + 4 + 1$$

$$= 9.8 \rightarrow 10 \text{ m}$$

2.9.6 Pump input power (P)

$$P = (0.163 * Q * \gamma * H * \alpha) / \rho$$

$$= (0.163 * 1.4 * 1.05 * 10 * 1.2) / 0.65$$

$$= 4.4 \rightarrow 5.5 \text{ kw}$$

- Q : Pump capacity = $0.7 \text{ m}^3/\text{min} * 2 \text{ units}$
- γ : Fluid density = 1.05
- H : Pump head = 10 m
- α : Allowance = 1.2
- ρ : Pump efficiency = 0.65

2.9.7 Spec

- $\phi 80 \text{ mm} * 0.7 \text{ m}^3/\text{min} * 10 \text{ m} * 5.5 \text{ kw}$

2.10 Centrifugal thickener

2.10.1 Necessary condition

Design maximum daily wastewater flow

- $141,000 \text{ m}^3/\text{day}$

Design excess sludge generation volume

- Solids volume 10.778 t/day
- Moisture content 99.4%
- Sludge volume $1,796.3 \text{ m}^3/\text{day}$



2.10.2 Necessary centrifugal thickener units

Facilitate (2trains of WWTP = 1trains of STP)

8 trains / 2 trains = 4 trains

2 trains = 3 units, (include 1 stand-by) Therefore,

4 trains = 6 units, (Include 2 stand-by)

2.10.3 Necessary centrifugal thickener capacity (Q)

Operation time is 24hours per day.

$$Q = V_o / (\text{units} * 24)$$

$$= 1,796.3 / (1 * 24)$$

$$= 74.8 \rightarrow 70 \text{ m}^3/\text{h}$$

- Q : Necessary centrifugal thickener capacity (m³/h)
- V_o : Sludge volume = 1,796.3 m³/day

2.10.4 spec

- 70 m³/h * 112.75 kw * 2units (Include 1 stand-by)

2.11 centrifugal thickener charge pump

2.11.1 Necessary condition

Design maximum daily wastewater flow

- 141,000 m³/day

Design thickened sludge generation volume

- Solids volume 10.778 t/day
- Moisture content 99.4 %
- Sludge volume 1,796.3 m³/day

2.11.2 Necessary pump units

Take into consideration centrifugal thickener 1unit = charge pump 1unit

- Centrifugal thickener 6(2) units = Charge pump 6(2) units

2.11.3 Necessary pump capacity (Q)

Centrifugal thickener 70m³/h

Facilitate pump capacity is 0.5~1.5 times as cyclone separator capacity.

$$Q = V_o * 0.5 \sim 1.5$$

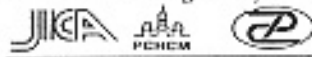
$$= 70 * 0.5 \sim 1.5$$

$$= 35 \sim 105 \text{ m}^3/\text{h}$$

- Q : Necessary pump capacity (m³/min)
- V_o : Cyclone separator capacity = 70 m³/h

2.11.4 Pump spec

Spec of Progress cavity pump is no calculation. So had to refer to Product catalog.
Therefore,



- $\phi 250 \text{ mm} \times 35 \sim 105 \text{ m}^3/\text{h} \times 10\text{mAq} \times 30 \text{ kw}$

2.12 Centrifugal dehydrator

2.12.1 Necessary condition

Design maximum daily wastewater flow

- $141,000 \text{ m}^3/\text{day}$

Design thickened sludge generation volume

- Solids volume 21.142 t/day
- Moisture content 96.56%
- Sludge volume $615 \text{ m}^3/\text{day}$

Operation days / week

- 7 days / 1week

Operation hours / day

- 24 hours / 1day

2.12.2 Necessary Centrifugal dehydrator units

- 1 unit

2.12.3 Necessary centrifugal separator capacity (Q)

Operation days are 7 days / week.

Operation hours are 24 h / day.

$$Q = (V_o \times 7 / 7) / (U \times T)$$

$$= (615 \times 7 / 7) / (1 \times 24)$$

$$= 25.6 \rightarrow 30 \text{ m}^3/\text{h}$$

- Q : Necessary Centrifugal dehydrator capacity (m^3/h)
- V_o : Sludge volume = $615 \text{ m}^3/\text{day}$
- T : Operation hours = 24 h
- U : units = 1

2.12.4 spec

- $30 \text{ m}^3/\text{h} \times 147.4 \text{ kw} \times 2 \text{ units (Include 1 stand-by)}$

2.13 Centrifugal dehydrator charge pump

2.13.1 Necessary condition

Design maximum daily wastewater flow

- $141,000 \text{ m}^3/\text{day}$

Design thickened sludge generation volume

- Solids volume 21.142 t/day
- Moisture content 96.56%
- Sludge volume $615 \text{ m}^3/\text{day}$

2.13.2 Necessary pump units



Take into consideration centrifugal separator 1 unit = charge pumps 1 unit

- Centrifugal dehydrator 6(2) units = Charge pump 6(2) units

2.13.3 Necessary pump capacity (Q)

Centrifugal dehydrator 30 m³/h

Facilitate pump capacity is 0.5~1.5 times as Centrifugal dehydrator capacity.

$$Q = V_o \times 0.5 \sim 1.5$$

$$= 30 \times 0.5 \sim 1.5$$

$$= 15 \sim 45 \text{ m}^3/\text{h}$$

- Q : Necessary pump capacity (m³/min)
- V_o : Centrifugal dehydrator capacity = 30 m³/h

2.13.4 Pump spec

Spec of Progress cavity pump is not calculation. So had to refer to Product catalog.
Therefore,

- φ 125 mm * 15 ~ 45 m³/h * 10mAq * 11 kw

2.14 Drainage pump

2.14.1 Necessary condition

Design maximum daily wastewater flow

- 141,000 m³/day

Flow rate of extracted

- From Centrifugal thickener 5,200 m³/day
- From Centrifugal dehydrator 2,100 m³/day
- Grand total : 7,300 m³/day

2.14.2 Necessary pump units

Facilitate 2(1) pumps for 1 Drainage Tank; there are 2 Tanks in total, therefore:

$$2 \text{ tanks} \times 2(1) \text{ unit/tanks} = 4(2) \text{ units}$$

2.14.3 Necessary pump capacity (Q)

Operation time is 24 hours per day.

$$Q = V_o / (24 \times 60)$$

$$= 7,300 / (24 \times 60)$$

$$= 5.06 \rightarrow 5.1 \text{ m}^3/\text{min}$$

- Q : Necessary pump capacity (m³/min)
- V_o : Total amount of Drainage Water = 7,300 m³/day

2.14.4 Pump diameter (D)

$$D = 146 \sqrt{Q / V_c}$$

$$= 146 \sqrt{5.1 / 2.5}$$

$$= 208 \rightarrow 200 \text{ mm}$$



- D : Pump diameter (mm)
- Q : Pump capacity = 5.1 m³/min
- Ve : Suction flow velocity = 2.5 m/s

2.14.5 Pump head (H)

$$H = h_1 + h_2 + h_3$$

$$= 1 + 13 + 1$$

$$= 15 \text{ m}$$

- H : Pump head (m)
- h₁ : Static head. = 1 m
- h₂ : Pipe loss head. = 13 m
- h₃ : Residual velocity head. = 1 m

2.14.6 Pump input power (P)

$$P = (0.163 * Q * H * \alpha) / \rho$$

$$= (0.163 * 5.1 * 1.05 * 15 * 1.2) / 0.65$$

$$= 24.17 \rightarrow 30 \text{ kw}$$

- Q : Pump capacity = 5.1 m³/min
- γ : Fluid density = 1.05
- H : Pump head = 15 m
- α : Allowance = 1.2
- ρ : Pump efficiency = 0.65

2.14.7 Spec

- $\phi 200\text{mm} * 5.1 \text{ m}^3/\text{min} * 15 \text{ m} * 30 \text{ kw}$

7.4

Electrical Equipment

HO CHI MINH CITY, VIETNAM
WATER ENVIRONMENT IMPROVEMENT PROJECT

Calculation Sheet

for

MCCB Capacity

Package : E

Plant : Wastewater Treatment Plant

WWTP MCCB SIZE

100	Lift Pump
200	Blower D Direct start
300	Sedimenta C Aux. Auto TR start
400-500	Chlorinatio SR Secondary Resistor
600	Dewatering SD Star-Delta
700	Compost
800	Ventilation

E - 99H0067

CUSTOMER VIETNAM/HCMC

MOTORS AND AUXILIARIES LIST																			
No.	EQUIPMENT NAME	QTY				POWER (kW)	VOLTAGE (V)	Reversible Operation	STARTING METHOD	POLE	GENERATOR REQ. LOAD	Current Calc. Ratio							
		Phase-1		Phase-2								TOTAL	Rated Current	MCCB Size	Control Center	Ph-1 CC Unit (unit)	Ph-2 CC Unit (unit)		
		DUTY	STAND BY	DUTY	STAND BY														
	LIFT PUMP EQUIPMENT																		
121	LIFT PUMP (1)	2	1			3 220	380	-	C	1		440.00	220.00						
122	LIFT PUMP (2)			3		3 460	380	-	C	1		1,380.00							
124	HOIST	1				1 655	380	B	D			655			65	100	350	1	
125	FLOOR DRAINAGE PUMP	6	6	1	1	14 22	380	-	D			39.30	39.30	6.55	6.55	45.85	180	12	2
	LIFT PUMP EQUIPMENT TOTAL											405.85	259.30	1,386.55	6.55	1,872.40	265.85	13	2
	CELOWER EQUIPMENT																		
211	BLOWER (1)	1	1			2 480	3300	-	SR			480.00	480.00			600			
211A	BLOWER (1) Aux Equipment	1	1			2 415	380	-	D			415	415		41	50	240	2	
212	BLOWER (2)			2		2 310	3300	-	SR			1,620.00			920	1000	180		2

WWTP MCCB SIZE

100	Lift Pump
200	Blower D Direct start
300	Sedimenta C Aux. Auto TR start
400-500	Chlorinatio SR Secondary Resistor
600	Dewatering SD Star-Delta
700	Compost
800	Ventilation

E - 95HC067

CUSTOMER VIETNAM/HCMC

MOTORS AND AUXILIARIES LIST												
No.	EQUIPMENT NAME	QTY	TOTAL				POWER (kW)	VOLTAGE (V)	Reversible Operation	STARTING METHOD	POLE	GENERATOR REQ. LOAD
			Phase-1	Phase-2	TOTAL							
					DUTY	STAND BY						
212A	BLOWER (2)Aux Equipment											
213	DISCHARGE VALVE (1)	1	1			2	0.75	380	R	D		
214	DISCHARGE VALVE (2)					2	0.75	380	R	D		
215	AIR FILTER	1	1	2			4	0.2	380	-	D	
216	FLOOR DRAINAGE PUMP	1	1				2	2.2	380	-	D	
217	CRANE	1					1	8.05	380	R	D	
	BLOWER EQUIPMENT TOTAL											
	<WATER TREATMENT FACILITY> PRIMARY SEDIMENTATION TANK											
312	SLUDGE SCRAPER	10		30			40	1.5	380	R	D	
314	SCUM PUMP	1		1	3		5	5.5	380	-	D	

Required Capacity				Current Calc. Ratio		Rated Current	MCCB Size	Control	Pl-1	Pl-2
Phase-1	Phase-2		TOTAL							
Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	(A)	(AT)	Unit Size (mm)	CC Unit (mm)	CC Unit (mm)
		12.00		12.00		59	100	360		2
0.75	0.75			0.75	0.75	7	30	240	2	
		1.50		1.50		7	30	240		2
0.20	0.20	0.40		0.60	0.20	2	30	150	2	2
2.20	2.20			2.20	2.20	22	30	180	2	
6.05				6.05		79	100	360	1	
495.55	487.50	1,633.00		2,129.25	487.50				9	8
15.00		45.00		60.00		15	30	240	10	30
5.50	5.50	16.50	16.50	33.00	43.00	54	100	360	2	6

WWTP MCCB SIZE

100	Lift Pump
200	Blower
300	Sedimenta
400-500	Chlorinatio
600	Dewatering
300	Compost
800	Ventilation

E - 99H0057

CUSTOMER VIETNAM/HCMC

MOTORS AND AUXILIARIES LIST									
No.	EQUIPMENT NAME	QTY		TOTAL		POWER (kW)	VOLTAGE (V)	Reversible Operation	STARTING METHOD
		Phase-1	Phase-2	Phase-1	Phase-2				
		DUTY	DUTY	DUTY	DUTY				
337	RETURN SLUDGE VALVE	10	30	40	0.4	380	R	D	
338	EXCESS SLUDGE PUMP	2	1	3	12	380	-	D	
339	EXCESS SLUDGE VALVE	10	30	40	0.2	380	R	D	
340	COMMUNITER	1	1	2	3.7	380	R	D	
351	FLOOR DRAINAGE PUMP	14	30	44	2.2	380	-	D	
WATER TREATMENT FACILITY TOTAL									
COINFECTION FACILITY>									
414	SODIUM HYPOCHLORITE PUMP	2	1	3	12	0.4	380	-	D
CWATER SUPPLY FACILITY>									
512	TREATED WATER SUPPLY PUMP(1)	1	1	2	5	30	380	-	SD

Current Calc. Ratio										3
Required Capacity						Rated Current	MCCB Size	Control Center	Ph-1	Ph-2
Phase-1		Phase-2		TOTAL						
Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	(A)	(kAT)	Unit Size (mm)	CC Unit (unit)	CC Unit (unit)
4.00		12.00		16.00		4	30	240	10	30
22.00	11.00	55.00	33.00	88.00	44.00	109	150	480	3	9
2.00		6.00		8.00		2	30	240	10	30
3.70		3.70		7.40		33	50	240	1	1
30.80		66.00		96.80		22	30	180	14	30
172.25	27.50	481.45	83.50	653.70	110.00			180	90	254
0.60	0.40	2.40	1.20	3.20	1.60	4	30	180	3	9
30.00	30.00	90.00		120.00	30.00	69	100	600	2	3

WWTP MCCB SIZE

100	Lift Pump
200	Blower D Direct start
300	Sedimenta C Aux Auto TR start
400-500	Chlorinatio SR Secondary Resistor
600	Demister SD Star-Delta
700	Compost
800	Ventilation

E - 99H00267

CUSTOMER VIETNAM/HCMC

MOTORS AND AUXILIARIES LIST											
No.	EQUIPMENT NAME	Q-TY	POWER				VOLTAGE	Reversible Operation	STARTING METHOD	POLE	GENERATOR REQ. LOAD
			TOTAL								
			Phase-1	Phase-2	STAND BY						
					DUTY	DUTY					
513	TREATED WATER STRAINER(1)	1	1	2	0.4	380	-	D			
514	FLOOR DRAINAGE PUMP	4	4	8	2.2	380	-	D			
516	TREATED WATER SUPPLY PUMP(2)	1	1	2	22	380	-	D			
517	TREATED WATER STRAINER(2)	1		1	0.4	380	-	D			
521	FILTRATION SUPPLY PUMP	1	1	2	3.7	380	-	D			
522	FILTRATION SUPPLY STRAINER	1	1	2	0.4	380	-	D			
523	SAND FILTER	1	1	2		220	-	-			
524	FILTERED WATER SUPPLY PUMP	1	1	3	11	380	-	D			
525	BACKWASH PUMP	1	1	2	7.5	380	-	D			
526	AIR WASH BLOWER	1	1	2	7.5	380	-	D			
527	BACKWASH WASTEWATER PUMP	1	1	2	3.7	380	-	D			

Current Calc. Ratio					3	Required Capacity				Rated Current	MCCB Size	Control Center	PI-1	PI-2
Phase-1		Phase-2		TOTAL	TOTAL									
Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	IA	(AT)	Unit Size (mm)	CC Unit (unit)	CC Unit (unit)
0.40		0.40		0.80				0.80		4	30	180	1	1
8.60	8.60			8.80	8.80					22	30	180	8	
22.00	22.00	44.00		66.00	22.00					217	225	600	2	2
0.40				0.40						4	30	180	1	
3.70	3.70			3.70	3.70					37	50	240	2	
0.40	0.40			0.40	0.40					4	30	180	2	
										-	30	180	2	
11.00	11.00	11.00		22.00	11.00					109	150	480	2	1
7.50	7.50			7.50	7.50					74	100	360	2	
7.50	7.50			7.50	7.50					74	100	360	2	
3.70	3.70			3.70	3.70					37	50	240	2	

WWTP MCCB SIZE

100	Lift Pump
200	Blower
300	Sediment
400-500	Chlorinator
500	Denitrifier
700	Compost
800	Ventilation

E - 9910057

CUSTOMER VIETNAM/HCMC

MOTORS AND AUXILIARIES LIST														
No	EQUIPMENT NAME	QTY	Phase-1			Phase-2		TOTAL	POWER (kW)	VOLTAGE (V)	Reversible Operation	STARTING METHOD	POLE	GENERATOR REQ. LOAD
			DUTY	STAND BY	DUTY	STAND BY								
528	AIR COMPRESSOR	1	1				2	3.7	380	-	D			
529	DEHUMIDIFIER	1					1	0.25	220	-	-			
530	SOLENOID VALVE BOX	1	1				2	2	220	-	-			
DISINFECTION FACILITY TOTAL														
<SLUDGE TREATMENT FACILITY>														
611	GRAVITY THICKENER	1			3		4	1.5	380	R	D			
613	THICKENED SLUDGE PUMP	1	1		3		4	5.5	380	-	D			
614	THICKENER EFFLUENT PUMP	1	1		3		4	5.5	380	-	D			
615	FLOOR DRAINAGE PUMP	1	1		3		4	2.2	380	-	D			
621	EXCESS SLUDGE MIXER	1			1		2	1.1	380	-	D			

Current Calc. Ratio									
3									
Required Capacity									
Phase-1		Phase-2		TOTAL		MCCB Size		Pl-1	
Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Unit Size (mm)	CC Unit (mm)	Unit Size (mm)	CC Unit (mm)
3.70	3.70			3.70	3.70	50	240	2	
0.25				0.25		30	180	1	
2.00	2.00			2.00	2.00	50	180	2	
102.15	100.70	147.80	1.20	249.95	101.90			30	16
1.50		4.50		6.00		30	240	1	3
5.50	5.50	16.50	16.50	22.00	22.00	100	360	2	6
5.50	5.50	16.50	16.50	22.00	22.00	100	360	2	6
2.20	2.20	5.60	5.60	8.80	8.80	20	150	2	6
11.00		11.00		22.00		150	450	1	1

WWTP MCCB SIZE

100 Lift Pump
 200 Blower D Direct start
 300 Sedimenta C Aux Auto TR start
 400-500 Chlorinatio SR Secondary Resistor
 600 Dewatering SD Star-Delta
 300 Compost
 800 Ventilation

E - 89HC067

CUSTOMER VIETNAM/HCMC

MOTORS AND AUXILIARIES LIST											
No	EQUIPMENT NAME	QTY				POWER (kW)	VOLTAGE (V)	Reversible Operation	STARTING METHOD	POLE	GENERATOR REQ. LOAD
		Phase-1	Phase-2	TOTAL							
				DUTY	STAND BY						
622	EXCESS SLUDGE FEED PUMP	1	3	1	6	30	360	-	SD		
623A	CENTRIFUGAL THICKENER DRIVE MOTOR	1	3	1	6	90	360	R	SD		
623B	CENTRIFUGAL THICKENER BACKDRIVE MOTOR	1	3	1	6	22	300	R	D		
623C	CENTRIFUGAL THICKENER LUBRICATION PUMP	1	3	1	6	0.75	300	-	D		
624	CRANE (20t)	1			1	15.25	380	-	D		
631	MIXED SLUDGE MIXER	2	6		8	11	300	-	D		
632	MIXED SLUDGE FEED PUMP	1	3	1	6	11	360	-	D		
633A	CENTRIFUGAL DEHYDRATOR DRIVE MOTOR	1	3	1	6	110	340	R	SD		
633B	CENTRIFUGAL DEHYDRATOR BACK DRIVE MOTOR	1	3	1	6	37	360	R	SD		
633C	CENTRIFUGAL DEHYDRATOR LUBRICATION PUMP	1	3	1	6	0.4	360	-	D		
634A	CAKE HOPPER	1	3	1	6	1.5	380	R	D		

				Current Calc. Ratio		3				
Required Capacity						Rated Current	MCCB Size	Control Center	Ph-1 DC Unit (unit)	Ph-2 DC Unit (unit)
Phase-1		Phase-2		TOTAL						
Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	(A)	(AT)	Unit Size (mm)	DC Unit (unit)	DC Unit (unit)
30.00	30.00	90.00	30.00	120.00	60.00	55	100	600	2	4
90.00	90.00	270.00	90.00	360.00	180.00	255	400	1200	2	4
22.00	22.00	66.00	22.00	88.00	44.00	217	225	840	2	4
0.75	0.75	2.25	0.75	3.00	1.50	7	30	180	2	4
15.25				15.25		150	200	600	1	
22.00		55.00		66.00		109	150	450	2	5
11.00	11.00	33.00	11.00	44.00	22.00	109	150	450	2	4
110.00	110.00	330.00	110.00	440.00	220.00	362	400	1200	2	4
37.00	37.00	111.00	37.00	148.00	74.00	122	150	450	2	4
0.40	0.40	1.20	0.40	1.60	0.80	4	30	180	2	4
1.50	1.50	4.50	1.50	6.00	3.00	15	30	240	2	4

WWTP MCCB SIZE

100	Lift Pump
200	Blower D Direct start
300	Sedimenta C Aux. Auto TR start
400-500	Chlorinator SR Secondary Resistor
600	Dewatering SD Star-Delta
700	Compost
800	Ventilation

E - 99HC087

CUSTOMER VIETNAM/HCMC

No.	EQUIPMENT NAME	MOTORS AND AUXILIARIES LIST						GENERATOR REQ. LOAD	
		QTY		TOTAL		POWER (kW)	VOLTAGE (V)	Reversible Operation	STARTING METHOD
		Phase-1	Phase-2	Phase-1	Phase-2				
		OUT	STAND BY	OUT	STAND BY				
6340	CAKE HOPPER	1	1	3	1	6	1.5	380	R D
635	POLYMER FEEDER	1	1	3	1	6	0.4	380	- D
636	POLYMER DISSOLUTION TANK	1	1	3	1	6	5.5	380	- D
637	POLYMER FEED PUMP	1	1	3	1	6	3.7	380	- D
638A	WATER SUPPLY PUMP UNIT	1	1	1	1	2	18.5	380	- D
638B	WATER SUPPLY PUMP UNIT	1	1	1	1	2	18.5	380	- D
639	AIR COMPRESSOR	1	1	1	1	3	5.5	380	- D
640	DEHUMIDIFIER	1	1	1	1	2	0.25	220	-
641	CRANE (20t)	1	1	1	1	1	15.25	380	R D
643	TREATED WATER INFLOW VALVE	1	1	1	1	1	0.1	380	R D
651	RECYCLE FLOW MIXER	1	1	1	1	2	11	380	- D

No.	EQUIPMENT NAME	MOTORS AND AUXILIARIES LIST						GENERATOR REQ. LOAD	
		QTY		TOTAL		POWER (kW)	VOLTAGE (V)	Reversible Operation	STARTING METHOD
		Phase-1	Phase-2	Phase-1	Phase-2				
		OUT	STAND BY	OUT	STAND BY				
6340	CAKE HOPPER	1	1	3	1	6	1.5	380	R D
635	POLYMER FEEDER	1	1	3	1	6	0.4	380	- D
636	POLYMER DISSOLUTION TANK	1	1	3	1	6	5.5	380	- D
637	POLYMER FEED PUMP	1	1	3	1	6	3.7	380	- D
638A	WATER SUPPLY PUMP UNIT	1	1	1	1	2	18.5	380	- D
638B	WATER SUPPLY PUMP UNIT	1	1	1	1	2	18.5	380	- D
639	AIR COMPRESSOR	1	1	1	1	3	5.5	380	- D
640	DEHUMIDIFIER	1	1	1	1	2	0.25	220	-
641	CRANE (20t)	1	1	1	1	1	15.25	380	R D
643	TREATED WATER INFLOW VALVE	1	1	1	1	1	0.1	380	R D
651	RECYCLE FLOW MIXER	1	1	1	1	2	11	380	- D

WWTP MCCB SIZE

100	Lift Pump
200	Blower D Direct start
300	Sedimenta C Aux. Auto TR start
400-500	Chlorinatio SR Secondary Resistor
600	Dewatering SD Star-Delta
700	Compost
800	Ventilation

E - 99H006

CUSTOMER VIETNAM/HCMC

MOTORS AND AUXILIARIES LIST															
No.	EQUIPMENT NAME	Q'TY	Phase-1				Phase-2		TOTAL	POWER (kW)	VOLTAGE (V)	Reversible Operation	STARTING METHOD	POLE	GENERATOR REQ. LOAD
			DUTY	STAND BY	DUTY	STAND BY	TOTAL								
652	RECYCLE FLOW PUMP	1	1	1	1	4	30	380	-	SD					
662	DEODORIZATION FAN			1		1	7.5	380							
	<u>SLUDGE TREATMENT FACILITY TOTAL</u>														
	<COMPOST FACILITY>														
711	MIXING MACHINE	2					2	80	380	-	SD				
712	SUCKING FAN	4					4	5.5	380	-	D				
713	HUMIDIFYING PUMP	2					2	1.5	350	-	D				
732	DEODORIZATION FAN	2					2	30	380	-	SD				
733	SPRAY WATER PUMP	1					1	3.7	380	-	D				

Current Calc. Ratio					3					
Required Capacity					Rated Current	MCCB Size	Control Center	Pl-1 CC Unit (unit)	Pl-2 CC Unit (unit)	
Phase-1	Phase-2		TOTAL							
Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)		Unit Size (mm)			
30.00	30.00	30.00	30.00	60.00	60.00	296	400	1200	2	2
		7.50		7.50		74	100	350		1
475.80	352.45	1,153.80	302.35	1,029.40	345.50			180	47	88
180.00				180.00		296	400	1200	2	
22.00				22.00		54	100	360	4	
3.00				3.00		15	30	160	2	
60.00				60.00		99	100	500	2	
3.70				3.70		32	50	240	1	

WWTP MCCB

WWTP MCCB SIZE

100	Lift Pump
200	Blower D Direct start
300	Sedimenta C Aux. Auto TR start
400-500	Chlorinatio SR Secondary Resistor
600	Dewatering SD Star-Delta
700	Compost
800	Ventilation

E - 9910067

CUSTOMER_VIETNAM/HCMC

MOTORS AND AUXILIARIES LIST														
No.	EQUIPMENT NAME	Q'TY	Phase-1				Phase-2		POWER (kW)	VOLTAGE (V)	Reversible Operation	STARTING METHOD	POLE	GENERATOR REQ. LOAD
			DUTY	STAND BY	DUTY	STAND BY	TOTAL							
808	AIR EXHAUST FAN	1		3		4	0.3	380	-	D				
809	AIR INTAKE FAN	2		2		4	7.5	380	-	D				
810	AIR INTAKE FAN	1		1		2	15	380	-	D				
811	AIR EXHAUST FAN	1				1	0.75	380	-	D				
812	AIR INTAKE FAN	1		-1			0.75	380	-	D				
812	AIR INTAKE FAN			1		1	1.5	380	-	D				
813	AIR INTAKE FAN	4				4	0.9	380	-	D				
814	AIR EXHAUST FAN	5				5	0.3	380	-	D				
815	AIR EXHAUST FAN	1				1	11	380	-	D				
816	AIR INTAKE FAN	1				1	1.5	380	-	D				
817	AIR EXHAUST FAN	1				1	2.2	380	-	D				

7-4-12

Current Calc. Ratio										3	Rated Current	MCCB Size	Control Center	Ph-1 DC Unit (unit)	Ph-2 DC Unit (unit)
Required Capacity						TOTAL									
Phase-1		Phase-2													
Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)										
0.30		0.90		1.20		3	30	180	1	3					
15.00		15.00		30.00		74	100	360	2	2					
15.00		15.00		30.00		148	150	480	1	1					
0.75				0.75		7	30	180	1						
0.75		-0.75				7	30	180	1	-1					
		0.75		0.75		15	30	180		1					
3.60				3.60		9	30	180	4						
1.50				1.50		3	30	180	5						
11.00				11.00		109	150	480	1						
1.50				1.50		15	30	180	1						
2.20				2.20		22	30	180	1						

WWTP MCCB SIZE

100	Lift Pump
200	Blower D Direct start
300	Sediments C Aux. Auto TR start
400-500	Chlorinator SR Secondary Resistor
500	Dewatering SD Star-Delta
700	Compost
800	Ventilation

E - 99H0057

CUSTOMER VIETNAM/HCMC

MOTORS AND AUXILIARIES LIST														
No.	EQUIPMENT NAME	Q'TY	Phase-1			Phase-2			POWER (kW)	VOLTAGE (V)	Reversible Operation	STARTING METHOD	POLE	GENERATOR REQ. LOAD
			DUTY	STAND BY	DUTY	STAND BY	TOTAL							
818	AIR INTAKE FAN	1						1	0.75	380	-	D		
819	AIR INTAKE FAN	1						1	3.75	380	-	D		
820	AIR EXHAUST FAN	1			1			2	5.5	380	-	D		
821	AIR EXHAUST FAN	1						1	0.4	380	-	D		
822	AIR EXHAUST FAN	2						2	0.75	380	-	D		
823	AIR EXHAUST FAN	1						1	0.3	380	-	D		
824	AIR INTAKE FAN	1						1	3.7	380	-	D		
825	AIR INTAKE FAN	2						2	0.28	380	-	D		
826	AIR EXHAUST FAN	2						2	0.75	380	-	D		
827	AIR INTAKE FAN	1						1	0.25	380	-	D		
828	AIR EXHAUST FAN	2						2	0.4	380	-	D		

No.		EQUIPMENT NAME		Current Calc Ratio				3	Required Capacity					Rated Current	MCCB Size	Control Center	Ph-1	Ph-2
				TOTAL														
				Phase-1		Phase-2			TOTAL									
Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)	Duty (kW)	Stand-by (kW)											
0.75						0.75						7	30	180		1		
3.75						3.75						37	50	240		1		
5.50				5.50		11.00						54	100	250		1	1	
5.50						5.50						4	30	150		1		
11.00						11.00						7	20	180		2		
5.50						5.50						3	30	180		1		
5.50						5.50						37	50	150		1		
11.00						11.00						3	30	150		2		
11.00						11.00						7	30	180		2		
5.50						5.50						3	30	180		1		
11.00						11.00						4	30	180		2		

HO CHI MINH CITY, VIETNAM
WATER ENVIRONMENT IMPROVEMENT PROJECT

Calculation Sheet
for
Power Cable Capacity

Package : E

Plant : Wastewater Treatment Plant

Vietnam / Ho Chi Minh City Water Environment Improvement Project										
[Package E]		Wastewater Treatment Plant Phase-1								
区分	Motor No.	機器名称	数量	容量	電圧	起動方式	起動電流	Pf	電圧降下	起動電流
Location	Motor No.	Name of Equipment	Q'ty	kW	V	Starting Method	Starting Current		V/drop	S/Current
<LIFT PUMP EQUIPMENT>										
	121-1	LIFT PUMP (1-1)	1	220	380	C	4342.10	0.8		800.0
	121-2	LIFT PUMP (1-2)	1	220	380	C	4342.10	0.8		800.0
	121-3	LIFT PUMP (1-3)	1	220	380	C	4342.10	0.8		800.0
	124-1	HOIST	1	6.55	380	D	21.50	0.8	1.5	3.5
	125-1	FLOOR DRAINAGE PUMP(D-1)	1	2.2	380	D	43.40	0.8	8.0	5.5
	125-2	FLOOR DRAINAGE PUMP(D-2)	1	2.2	380	D	43.40	0.8	14.0	5.5
	125-3	FLOOR DRAINAGE PUMP(D-3)	1	2.2	380	D	43.40	0.8	22.0	5.5
	125-4	FLOOR DRAINAGE PUMP(D-4)	1	2.2	380	D	43.40	0.8	38.0	5.5
	125-5	FLOOR DRAINAGE PUMP(D-5)	1	2.2	380	D	43.40	0.8	38.0	5.5
	125-6	FLOOR DRAINAGE PUMP(D-6)	1	2.2	380	D	43.40	0.8	38.0	5.5
	125-7	FLOOR DRAINAGE PUMP(S-1)	1	2.2	380	D	43.40	0.8	8.0	5.5
	125-8	FLOOR DRAINAGE PUMP(S-2)	1	2.2	380	D	43.40	0.8	14.0	5.5
	125-9	FLOOR DRAINAGE PUMP(S-3)	1	2.2	380	D	43.40	0.8	22.0	5.5
	125-10	FLOOR DRAINAGE PUMP(S-4)	1	2.2	380	D	43.40	0.8	38.0	5.5
	125-11	FLOOR DRAINAGE PUMP(S-5)	1	2.2	380	D	43.40	0.8	38.0	5.5
	125-12	FLOOR DRAINAGE PUMP(S-6)	1	2.2	380	D	43.40	0.8	38.0	5.5
<BLOWER EQUIPMENT>										
	211-1	BLOWER (1-1)	1	480	3300	SR	150.00	0.8	22.0	60.0
	211-2	BLOWER (1-2)	1	480	3300	SR	150.00	0.8	22.0	60.0
	211A-1	BLOWER (1-1) Aux. Equipment	1	4.15	380	D	81.90	0.8	100.0	100.0
	211A-2	BLOWER (1-2) Aux. Equipment	1	4.15	380	D	81.90	0.8	100.0	100.0
	213-1	DISCHARGE VALVE (1-1)	1	0.75	380	D	14.80	0.8	14.0	3.5
	213-2	DISCHARGE VALVE (1-2)	1	0.75	380	D	14.80	0.8	14.0	3.5
	215-1	AIR FILTER	1	0.2	380	D	3.90	0.8	5.5	5.5
	215-2	AIR FILTER	1	0.2	380	D	3.90	0.8	3.5	3.5
	216-1	FLOOR DRAINAGE PUMP	1	2.2	380	D	43.40	0.8	60.0	5.5
	216-2	FLOOR DRAINAGE PUMP	1	2.2	380	D	43.40	0.8	60.0	5.5
	217-1	CRANE	1	8.05	380	D	26.50	0.8	38.0	3.5
<WATER TREATMENT FACILITY>										
PRIMARY SEDIMENTATION TANK										
	312-1	SLUDGE SCRAPER	1	1.5	380	D	29.60	0.8	38.0	3.5
	312-2	SLUDGE SCRAPER	1	1.5	380	D	29.60	0.8	38.0	3.5
	312-3	SLUDGE SCRAPER	1	1.5	380	D	29.60	0.8	38.0	3.5
	312-4	SLUDGE SCRAPER	1	1.5	380	D	29.60	0.8	38.0	3.5

Vietnam / Ho Chi Minh City Water Environment Improvement Project													
[Package E]													
Wastewater Treatment Plant Phase-1													
区分	Motor No.	機器名称	数量	容量	電圧	起動方式	起動電流	Pf	電圧降下	起動電流	Final		
Location	Motor No.	Name of Equipment	Q'ty	kW	V	Starting Method	Starting Current		Cable Size	S/Current	Cable Size		
	312-5	SLUDGE SCRAPER	1	1.5	380	D	29.60	0.8	38.0	3.5	38.0		
	312-6	SLUDGE SCRAPER	1	1.5	380	D	29.60	0.8	38.0	3.5	38.0		
	312-7	SLUDGE SCRAPER	1	1.5	380	D	29.60	0.8	38.0	3.5	38.0		
	312-8	SLUDGE SCRAPER	1	1.5	380	D	29.60	0.8	38.0	3.5	38.0		
	312-9	SLUDGE SCRAPER	1	1.5	380	D	29.60	0.8	22.0	3.5	22.0		
	312-10	SLUDGE SCRAPER	1	1.5	380	D	29.60	0.8	22.0	3.5	22.0		
	314-1	SCUM PUMP	1	5.5	380	D	108.60	0.8	150.0	38.0	150.0		
	314-2	SCUM PUMP	1	5.5	380	D	108.60	0.8	150.0	38.0	150.0		
	315-1	RAW SLUDGE PUMP	1	5.5	380	D	108.60	0.8	150.0	38.0	150.0		
	315-2	RAW SLUDGE PUMP	1	5.5	380	D	108.60	0.8	150.0	38.0	150.0		
	315-3	RAW SLUDGE PUMP	1	5.5	380	D	108.60	0.8	150.0	38.0	150.0		
	316-1	RAW SLUDGE VALVE	1	0.2	380	D	3.90	0.8	5.5	3.5	5.5		
	316-2	RAW SLUDGE VALVE	1	0.2	380	D	3.90	0.8	5.5	3.5	5.5		
	316-3	RAW SLUDGE VALVE	1	0.2	380	D	3.90	0.8	5.5	3.5	5.5		
	316-4	RAW SLUDGE VALVE	1	0.2	380	D	3.90	0.8	5.5	3.5	5.5		
	316-5	RAW SLUDGE VALVE	1	0.2	380	D	3.90	0.8	5.5	3.5	5.5		
	316-6	RAW SLUDGE VALVE	1	0.2	380	D	3.90	0.8	5.5	3.5	5.5		
	316-7	RAW SLUDGE VALVE	1	0.2	380	D	3.90	0.8	5.5	3.5	5.5		
	316-8	RAW SLUDGE VALVE	1	0.2	380	D	3.90	0.8	5.5	3.5	5.5		
	316-9	RAW SLUDGE VALVE	1	0.2	380	D	3.90	0.8	5.5	3.5	5.5		
	316-10	RAW SLUDGE VALVE	1	0.2	380	D	3.90	0.8	5.5	3.5	5.5		
	317-1	COMMINUTER	1	0.4	380	D	7.90	0.8	5.5	3.5	5.5		
AERATION TANK													
	324-1	AIR FLOW CONTROL VALVE	1	0.4	380	D	7.90	0.8	14.0	3.5	14.0		
	324-2	AIR FLOW CONTROL VALVE	1	0.4	380	D	7.90	0.8	8.0	3.5	8.0		
	324-3	AIR FLOW CONTROL VALVE	1	0.4	380	D	7.90	0.8	8.0	3.5	8.0		
	324-4	AIR FLOW CONTROL VALVE	1	0.4	380	D	7.90	0.8	8.0	3.5	8.0		
	324-5	AIR FLOW CONTROL VALVE	1	0.4	380	D	7.90	0.8	8.0	3.5	8.0		
	324-6	AIR FLOW CONTROL VALVE	1	0.4	380	D	7.90	0.8	8.0	3.5	8.0		
	324-7	AIR FLOW CONTROL VALVE	1	0.4	380	D	7.90	0.8	8.0	3.5	8.0		
	324-8	AIR FLOW CONTROL VALVE	1	0.4	380	D	7.90	0.8	8.0	3.5	8.0		
	324-9	AIR FLOW CONTROL VALVE	1	0.4	380	D	7.90	0.8	8.0	3.5	8.0		
	324-10	AIR FLOW CONTROL VALVE	1	0.4	380	D	7.90	0.8	5.5	3.5	5.5		
FINAL SEDIMENTATION TANK													
	332-1	SLUDGE SCRAPER	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0		

Vietnam / Ho Chi Minh City Water Environment Improvement Project									
[Package E]									
Wastewater Treatment Plant Phase-I									
区分	Motor No.	数量	容量	电压	启动方式	启动电流	Pf	电压降下	启动电流
Location	Motor No.	Qty	kW	V	Starting Method	Starting Current		V/drop Cable Size	S/cable Size
Name of Equipment									
Final Cable Size									
	332-2	1	2.2	380	D	43.40	0.8	38.0	5.5
	332-3	1	2.2	380	D	43.40	0.8	38.0	5.5
	332-4	1	2.2	380	D	43.40	0.8	38.0	5.5
	332-5	1	2.2	380	D	43.40	0.8	38.0	5.5
	332-6	1	2.2	380	D	43.40	0.8	38.0	5.5
	332-7	1	2.2	380	D	43.40	0.8	38.0	5.5
	332-8	1	2.2	380	D	43.40	0.8	38.0	5.5
	332-9	1	2.2	380	D	43.40	0.8	38.0	5.5
	332-10	1	2.2	380	D	43.40	0.8	38.0	5.5
	334-1	1	2.2	380	D	43.40	0.8	22.0	5.5
	334-2	1	5.5	380	D	108.60	0.8	100.0	39.0
	335-1	1	5.5	380	D	108.60	0.8	100.0	39.0
	335-2	1	11	380	D	217.10	0.8	400.0	100.0
	335-3	1	11	380	D	217.10	0.8	400.0	100.0
	335-4	1	11	380	D	217.10	0.8	200.0	100.0
	337-1	1	11	380	D	217.10	0.8	200.0	100.0
	337-2	1	0.4	380	D	7.90	0.8	8.0	3.5
	337-3	1	0.4	380	D	7.90	0.8	8.0	3.5
	337-4	1	0.4	380	D	7.90	0.8	8.0	3.5
	337-5	1	0.4	380	D	7.90	0.8	8.0	3.5
	337-6	1	0.4	380	D	7.90	0.8	8.0	3.5
	337-7	1	0.4	380	D	7.90	0.8	5.5	5.5
	337-8	1	0.4	380	D	7.90	0.8	5.5	5.5
	337-9	1	0.4	380	D	7.90	0.8	5.5	5.5
	337-10	1	0.4	380	D	7.90	0.8	5.5	5.5
	338-1	1	11	380	D	217.10	0.8	250.0	100.0
	338-2	1	11	380	D	217.10	0.8	250.0	100.0
	338-3	1	11	380	D	217.10	0.8	250.0	100.0
	339-1	1	0.2	380	D	3.90	0.8	3.5	3.5
	339-2	1	0.2	380	D	3.90	0.8	3.5	3.5
	339-3	1	0.2	380	D	3.90	0.8	3.5	3.5
	339-4	1	0.2	380	D	3.90	0.8	3.5	3.5
	339-5	1	0.2	380	D	3.90	0.8	3.5	3.5
	339-6	1	0.2	380	D	3.90	0.8	3.5	3.5
	339-7	1	0.2	380	D	3.90	0.8	3.5	3.5
	339-8	1	0.2	380	D	3.90	0.8	3.5	3.5
	339-9	1	0.2	380	D	3.90	0.8	3.5	3.5

WWTP (Ph-1)

Vietnam / Ho Chi Minh City Water Environment Improvement Project											
[Package E]											
Wastewater Treatment Plant Phase-1											
区分	Motor No.	機器名称	数量	容量	電圧	起動方式	起動電流	Pf	電圧降下	起動電流	
Location	Motor No.	Name of Equipment	Qty	kW	V	Starting Method	Starting Current		Cable Size V/drop	Cable Size S/current	Cable Size Final
	339-10	EXCESS SLUDGE VALVE	1	0.2	380	D	3.90	0.8	3.5	3.5	3.5
	340-1	COMMINUTER	1	3.7	380	D	73.00	0.8	38.0	14.0	38.0
	351-1	FLOOR DRAINAGE PUMP(D-1)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-2	FLOOR DRAINAGE PUMP(D-2)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-3	FLOOR DRAINAGE PUMP(D-3)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-4	FLOOR DRAINAGE PUMP(D-4)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-5	FLOOR DRAINAGE PUMP(D-5)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-6	FLOOR DRAINAGE PUMP(D-6)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-7	FLOOR DRAINAGE PUMP(D-7)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-8	FLOOR DRAINAGE PUMP(D-8)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-9	FLOOR DRAINAGE PUMP(D-9)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-10	FLOOR DRAINAGE PUMP(D-10)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-11	FLOOR DRAINAGE PUMP(D-11)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-12	FLOOR DRAINAGE PUMP(D-12)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-13	FLOOR DRAINAGE PUMP(D-13)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
	351-14	FLOOR DRAINAGE PUMP(D-14)	1	2.2	380	D	43.40	0.8	60.0	5.5	60.0
<DISINFECTION FACILITY>											
	414-1	SODIUM HYPOCHLORITE PUMP	1	0.4	380	D	7.90	0.8	3.5	3.5	3.5
	414-2	SODIUM HYPOCHLORITE PUMP	1	0.4	380	D	7.90	0.8	3.5	3.5	3.5
	414-3	SODIUM HYPOCHLORITE PUMP	1	0.4	380	D	7.90	0.8	3.5	3.5	3.5
<WATER SUPPLY FACILITY>											
	512-1	TREATED WATER SUPPLY PUMP (1)	1	30	380	SD	197.40	0.8	38.0	100.0	100.0
	512-2	TREATED WATER SUPPLY PUMP (1)	1	30	380	SD	197.40	0.8	38.0	100.0	100.0
	513-1	TREATED WATER STRAINER (1)	1	0.4	380	D	7.90	0.8	3.5	3.5	3.5
	514-1	FLOOR DRAINAGE PUMP(D-1)	1	2.2	380	D	43.40	0.8	5.5	5.5	5.5
	514-2	FLOOR DRAINAGE PUMP(D-2)	1	2.2	380	D	43.40	0.8	5.5	5.5	5.5
	514-3	FLOOR DRAINAGE PUMP(D-3)	1	2.2	380	D	43.40	0.8	5.5	5.5	5.5
	514-4	FLOOR DRAINAGE PUMP(D-4)	1	2.2	380	D	43.40	0.8	5.5	5.5	5.5
	514-5	FLOOR DRAINAGE PUMP(S-1)	1	2.2	380	D	43.40	0.8	5.5	5.5	5.5
	514-6	FLOOR DRAINAGE PUMP(S-2)	1	2.2	380	D	43.40	0.8	5.5	5.5	5.5
	514-7	FLOOR DRAINAGE PUMP(S-3)	1	2.2	380	D	43.40	0.8	5.5	5.5	5.5
	514-8	FLOOR DRAINAGE PUMP(S-4)	1	2.2	380	D	43.40	0.8	5.5	5.5	5.5
	515-1	TREATED WATER SUPPLY PUMP (2)	1	22	380	D	434.20	0.8	100.0	250.0	250.0
	515-2	TREATED WATER SUPPLY PUMP (2)	1	22	380	D	434.20	0.8	100.0	250.0	250.0
	517-1	TREATED WATER STRAINER (2)	1	0.4	380	D	7.90	0.8	3.5	3.5	3.5

Vietnam / Ho Chi Minh City Water Environment Improvement Project

Wastewater Treatment Plant Phase-1											
区分	Motor No. Location	设备名称 Name of Equipment	数量 Qty	容量 kW	电压 V	启动方式 Starting Method	启动电流 Starting Current	Pf	电压降下 V/drop Cable Size	启动电流 S/current Cable Size	Final Cable Size
	521-1	FILTRATION SUPPLY PUMP	1	3.7	380	D	73.00	0.8	8.0	14.0	14.0
	521-2	FILTRATION SUPPLY PUMP	1	3.7	380	D	73.00	0.8	8.0	14.0	14.0
	522-1	FILTRATION SUPPLY STRAINER	1	0.4	380	D	7.90	0.8	3.5	3.5	3.5
	522-2	FILTRATION SUPPLY STRAINER	1	0.4	380	D	7.90	0.8	3.5	3.5	3.5
	523-1	SAND FILTER	1	2	220	-	11.40	0.8	3.5	3.5	3.5
	523-2	SAND FILTER	1	2	220	-	11.40	0.8	3.5	3.5	3.5
	524-1	FILTERED WATER SUPPLY PUMP	1	11	380	D	217.10	0.8	22.0	100.0	100.0
	524-2	FILTERED WATER SUPPLY PUMP	1	11	380	D	217.10	0.8	22.0	100.0	100.0
	525-1	BACKWASH PUMP	1	7.5	380	D	148.00	0.8	22.0	60.0	60.0
	525-2	BACKWASH PUMP	1	7.5	380	D	148.00	0.8	22.0	60.0	60.0
	526-1	AIR WASH BLOWER	1	7.5	380	D	148.00	0.8	22.0	60.0	60.0
	526-2	AIR WASH BLOWER	1	7.5	380	D	148.00	0.8	22.0	60.0	60.0
	527-1	BACKWASH WASTEWATER PUMP	1	3.7	380	D	73.00	0.8	14.0	14.0	14.0
	527-2	BACKWASH WASTEWATER PUMP	1	3.7	380	D	73.00	0.8	14.0	14.0	14.0
	528-1	AIR COMPRESSOR	1	3.7	380	D	73.00	0.8	14.0	14.0	14.0
	528-2	AIR COMPRESSOR	1	3.7	380	D	73.00	0.8	14.0	14.0	14.0
	529-1	DEHUMIDIFIER	1	0.25	220	-	6.50	0.8	3.5	3.5	3.5
	530-1	SOLENOID VALVE BOX	1	2	220	-	11.40	0.8	3.5	3.5	3.5
	530-2	SOLENOID VALVE BOX	1	2	220	-	11.40	0.8	3.5	3.5	3.5
<<SLUDGE TREATMENT FACILITY>>											
	611-1	GRAVITY THICKENER	1	1.5	380	D	29.60	0.8	14.0	3.5	14.0
	613-1	THICKENED SLUDGE PUMP	1	5.5	380	D	108.60	0.8	60.0	38.0	60.0
	613-2	THICKENED SLUDGE PUMP	1	5.5	380	D	108.60	0.8	60.0	38.0	60.0
	614-1	THICKENER EFFLUENT PUMP	1	5.5	380	D	108.60	0.8	60.0	38.0	60.0
	614-2	THICKENER EFFLUENT PUMP	1	5.5	380	D	108.60	0.8	60.0	38.0	60.0
	615-1	FLOOR DRAINAGE PUMP(D-1)	1	2.2	380	D	43.40	0.8	22.0	5.5	22.0
	615-2	FLOOR DRAINAGE PUMP(S-1)	1	2.2	380	D	43.40	0.8	22.0	5.5	22.0
	621-1	EXCESS SLUDGE MIXER	1	11	380	D	217.10	0.8	38.0	100.0	100.0
	622-1	EXCESS SLUDGE FEED PUMP	1	30	380	SD	197.40	0.8	38.0	100.0	100.0
	622-2	EXCESS SLUDGE FEED PUMP	1	30	380	SD	197.40	0.8	38.0	100.0	100.0
	623A-1	CENTRIFUGAL THICKENER- DRIVE MOTOR	1	90	380	SD	592.10	0.8	325.0	325.0	325.0
	623A-2	CENTRIFUGAL THICKENER- DRIVE MOTOR	1	90	380	SD	592.10	0.8	400.0	325.0	400.0
	623B-1	CENTRIFUGAL THICKENER- BACKDRIVE MOTOR	1	22	380	D	434.20	0.8	200.0	250.0	250.0
	623B-2	CENTRIFUGAL THICKENER- BACKDRIVE MOTOR	1	22	380	D	434.20	0.8	250.0	250.0	250.0
	623C-1	CENTRIFUGAL THICKENER- LUBRICATION PUMP	1	0.75	380	D	14.80	0.8	5.5	3.5	5.5
	623C-2	CENTRIFUGAL THICKENER- LUBRICATION PUMP	1	0.75	380	D	14.80	0.8	5.5	3.5	5.5

WWTP (Ph-1)

Vietnam / Ho Chi Minh City Water Environment Improvement Project										
[Package E]										
Wastewater Treatment Plant Phase-I										
区分 Location	Motor No. Motor No.	機器名称 Name of Equipment	数量 Qty	容量 kW	電圧 V	起動方式 Starting Method	起動電流 Starting Current	電圧降下 V/drop	起動電流 S/current	Final Cable Size
	712-3	SUCKING FAN	1	5.5	380	D	108.60	38.0	38.0	38.0
	712-4	SUCKING FAN	1	5.5	380	D	108.60	38.0	38.0	38.0
	713-1	HUMIDIFYING PUMP	1	1.5	380	D	29.60	8.0	3.5	8.0
	713-2	HUMIDIFYING PUMP	1	1.5	380	D	29.60	8.0	3.5	8.0
	732-1	DEODORIZATION FAN	1	3.0	380	D	592.10	400.0	325.0	400.0
	732-2	DEODORIZATION FAN	1	3.0	380	D	592.10	400.0	325.0	400.0
	733-1	SPRAY WATER PUMP	1	3.7	380	D	73.00	38.0	14.0	38.0
	734-1	FLOOR DRAINAGE PUMP	1	3.7	380	D	73.00	38.0	14.0	38.0
<VENTILATION FACILITY>										
	801-1	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	14.0	3.5	14.0
	801-2	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	801-3	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	801-4	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	802-1	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	802-2	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	802-3	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	802-4	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	803-1	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	803-2	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	803-3	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	804-1	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	804-2	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	804-3	AIR EXHAUST FAN (B E/R)	1	0.4	380	D	7.90	8.0	3.5	8.0
	805-1	AIR EXHAUST FAN (B E/R)	1	0.3	380	D	5.90	5.5	3.5	5.5
	805-2	AIR EXHAUST FAN (B E/R)	1	0.3	380	D	5.90	5.5	3.5	5.5
	805-3	AIR EXHAUST FAN (B E/R)	1	0.3	380	D	5.90	5.5	3.5	5.5
	805-4	AIR EXHAUST FAN (B E/R)	1	0.3	380	D	5.90	5.5	3.5	5.5
	806-1	AIR EXHAUST FAN (C E/R)	1	0.3	380	D	5.90	5.5	3.5	5.5
	806-2	AIR EXHAUST FAN (C E/R)	1	0.3	380	D	5.90	5.5	3.5	5.5
	806-3	AIR EXHAUST FAN (C E/R)	1	0.3	380	D	5.90	5.5	3.5	5.5
	806-4	AIR EXHAUST FAN (C E/R)	1	0.3	380	D	5.90	5.5	3.5	5.5
	807-1	AIR EXHAUST FAN (C E/R)	1	0.3	380	D	5.90	5.5	3.5	5.5
	808-1	AIR EXHAUST FAN (C E/R)	1	0.3	380	D	5.90	5.5	3.5	5.5
	809-1	AIR INTAKE FAN (B E/R)	1	7.5	380	D	148.00	38.0	60.0	60.0
	809-2	AIR INTAKE FAN (B E/R)	1	7.5	380	D	148.00	38.0	60.0	60.0
	810-1	AIR INTAKE FAN (C E/R)	1	1.5	380	D	295.10	100.0	150.0	150.0

Vietnam / Ho Chi Minh City Water Environment Improvement Project											
[Package E]											
Wastewater Treatment Plant Phase-1											
区分 Location	Motor No. Motor No.	機器名称 Name of Equipment	数量 Qty	容量 kW	電圧 V	起動方式 Starting Method	起動電流 Starting Current	Pf	電圧降下 V/drop	起動電流 S/Current	ケーブルサイズ Cable Size
	B11-1	AIR INTAKE FAN (C E/R)	1	0.75	380	D	14.80	0.8	5.5	3.5	5.5
	B12-1	AIR INTAKE FAN (A E/R)	1	0.75	380	D	14.80	0.8	14.0	3.5	14.0
	B13-1	AIR INTAKE FAN (A E/R)	1	0.9	380	D	17.80	0.8	22.0	3.5	22.0
	B13-2	AIR INTAKE FAN (A E/R)	1	0.9	380	D	17.80	0.8	14.0	3.5	14.0
	B13-3	AIR INTAKE FAN (A E/R)	1	0.9	380	D	17.80	0.8	14.0	3.5	14.0
	B13-4	AIR INTAKE FAN (A E/R)	1	0.9	380	D	17.80	0.8	14.0	3.5	14.0
	B14-1	AIR EXHAUST FAN (C E/R)	1	0.3	380	D	5.90	0.8	3.5	3.5	3.5
	B14-2	AIR EXHAUST FAN (C E/R)	1	0.3	380	D	5.90	0.8	3.5	3.5	3.5
	B14-3	AIR EXHAUST FAN (C E/R)	1	0.3	380	D	5.90	0.8	3.5	3.5	3.5
	B14-4	AIR EXHAUST FAN (C E/R)	1	0.3	380	D	5.90	0.8	3.5	3.5	3.5
	B14-5	AIR EXHAUST FAN (C E/R)	1	0.3	380	D	5.90	0.8	3.5	3.5	3.5
	B15-1	AIR EXHAUST FAN (A E/R)	1	1.1	380	D	217.10	0.8	150.0	100.0	150.0
	B16-1	AIR INTAKE FAN (A E/R)	1	1.5	380	D	29.60	0.8	22.0	3.5	22.0
	B17-1	AIR EXHAUST FAN (A E/R)	1	2.2	380	D	43.40	0.8	22.0	3.5	22.0
	B18-1	AIR INTAKE FAN (D E/R)	1	0.75	380	D	14.80	0.8	5.5	3.5	5.5
	B19-1	AIR INTAKE FAN (E E/R)	1	3.75	380	D	74.00	0.8	36.0	14.0	38.0
	B20-1	AIR EXHAUST FAN (D E/R)	1	5.5	380	D	109.60	0.8	60.0	38.0	60.0
	B21-1	AIR EXHAUST FAN (D E/R)	1	0.4	380	D	7.90	0.8	5.5	3.5	5.5
	B22-1	AIR EXHAUST FAN (D E/R)	1	0.75	380	D	14.80	0.8	8.0	3.5	8.0
	B22-2	AIR EXHAUST FAN (D E/R)	1	0.75	380	D	14.80	0.8	14.0	3.5	14.0
	B23-1	AIR EXHAUST FAN (E E/R)	1	0.3	380	D	5.90	0.8	5.5	3.5	5.5
	B24-1	AIR EXHAUST FAN (E E/R)	1	3.7	380	D	73.00	0.8	100.0	14.0	100.0
	B25-1	AIR EXHAUST FAN (E E/R)	1	0.28	380	D	5.50	0.8	8.0	3.5	8.0
	B25-2	AIR EXHAUST FAN (E E/R)	1	0.28	380	D	5.50	0.8	5.5	3.5	5.5
	B26-1	AIR EXHAUST FAN (E E/R)	1	0.75	380	D	14.80	0.8	22.0	3.5	22.0
	B26-2	AIR EXHAUST FAN (E E/R)	1	0.75	380	D	14.80	0.8	22.0	3.5	22.0
	B27-1	AIR EXHAUST FAN (A E/R)	1	0.28	380	D	5.50	0.8	5.5	3.5	5.5
	B28-1	AIR EXHAUST FAN (A E/R)	1	0.4	380	D	7.90	0.8	8.0	3.5	8.0
	B28-2	AIR EXHAUST FAN (A E/R)	1	0.4	380	D	7.90	0.8	8.0	3.5	8.0
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WATER ENVIRONMENT IMPROVEMENT PROJECT

Issue date Rev.1 : 13-Jan-01

Calculation Sheet

for

Receiving Power Capacity for WWTP

1. Introduction ;

The receiving power capacity of the plant is decided from the result of the following study.

- 1) The classification of all electrical equipments and a character are examined.
- 2) Total electrical capacity is computed in search of rated capacity of every item.
- 3) Maximum demand power is calculated by using demand factor of each electrical equipments.

2. Calculation ;

- 1) The result of the above item 1) and 2) is shown in the Table: WWTP Ph-1 & 2.
- 2) Total maximum demand power can be looked for by using rated capacity and demand factor from the following formula;

$$(\text{Receiving power capacity} = (\text{Maximum demand power}) / (\text{Efficiency} \times \text{Power factor}))$$

[Unit : kW]

	Rated capacity	Demand factor	Max. demand power
Phase-1	2,301.3	0.8	1,841.0
Phase-2	5,964.7	0.8	4,771.8
Total	8,266.0	0.8	6,612.8

3. Selection ;

Receiving power capacity was decided from the above result from the following reason.

- 1) When the operation which become stable is done, paralell operation of receiving transformer is necessary.
- 2) Future expansion shall be cosidered.

4. Attachment ;

- 1) Electrical Equipment List for WWTP Phase-1
- 2) Electrical Equipment List for WWTP Phase-2

ELECTRICAL EQUIPMENT LIST

Name of electric consumer : Wastewater Treatment Plant (WWTP) - Phase 1

Address :

Working table-time :

Schedule of electric consumer:

Issue date

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No.	Electrical equipment name	Q'ty	Capacity		Total	Remarks
			(HB)	(kW)	(kW)	(Demand Factor)
	LIFT PUMP EQUIPMENT					
121	Lift pump (1)	2	-	220.00	440.00	0.6
123	Floor drainage pump	1	-	2.20	2.20	0.6
124	Crane	1	-	16.00	16.00	0.3
	BLOWER EQUIPMENT					
211	Blower (1)	1	-	480.00	480.00	1.0
211A	Aux. Equipment for Blower (1)	1	-	4.15	4.15	1.0
213	Discharge valve (1)	1	-	0.75	0.75	0.6
215	Air filter	1	-	3.70	3.70	0.6
216	Floor drainage pump	1	-	2.20	2.20	0.6
217	Crane	1	-	8.25	8.25	0.3
	WATER TREATMENT FACILITY					
	(Primary sedimentation tank)					
312	Sludge scraper	10	-	1.50	15.00	1.0
314	Scum pump	1	-	5.50	5.50	0.6
315	Raw sludge pump	2	-	5.50	11.00	0.6
316	Raw sludge valve	10	-	0.20	2.00	0.6
317	Comminuter	1	-	0.75	0.75	1.0
	(Aeration tank)					
324	Air flow control valve	10	-	0.40	4.00	0.6
	(Final sedimentation tank)					
332	Sludge scraper	10	-	2.20	22.00	1.0
334	Scum pump	1	-	5.50	5.50	0.6
335	Return sludge pump (25%)	4	-	11.00	44.00	1.0
337	Return sludge valve	10	-	0.40	4.00	0.6
338	Excess sludge pump	2	-	11.00	22.00	0.6
339	Excess sludge valve	10	-	0.20	2.00	0.6
340	Comminuter	1	-	3.70	3.70	1.0
351	Floor drainage pump	10	-	2.20	22.00	0.6
	DISINFECTION FACILITY					
411	Sodium hypochlorite pump	2	-	0.40	0.80	1.0
	WATER SUPPLY FACILITY					
512	Treated water supply pump (1)	1	-	30.00	30.00	1.0
513	Treated water strainer	1	-	0.40	0.40	0.6

ELECTRICAL EQUIPMENT LIST

Name of electric consumer : Wastewater Treatment Plant (WWTP) - Phase 1

Address :

Working table-time :

Schedule of electric consumer:

Issue date

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No.	Electrical equipment name	Q'ty	Capacity		Total (kW)	Remarks (Demand Factor)
			(HB)	(kW)		
514	Floor drainage pump	1	-	2.20	2.20	0.6
516	Treated water supply pump (2)	1	-	22.00	22.00	0.8
517	Treated water strainer (2)	1	-	0.40	0.40	0.6
521	Filtration supply pump	1	-	3.70	3.70	0.6
522	Filtration supply strainer	1	-	0.40	0.40	0.6
523	Sand filter	1	-	2.20	2.20	0.4
524	Filtered water supply pump	1	-	11.00	11.00	1.0
525	Backwash pump	1	-	7.50	7.50	0.4
526	Air wash blower	1	-	7.50	7.50	0.4
527	Backwash wastewater pump	1	-	3.70	3.70	0.4
528	Air compressor	1	-	3.70	3.70	0.5
529	Dehumidifier	1	-	0.25	0.25	0.5
530	Solenoid valve box	1	-	1.50	1.50	0.5
SLUDGE TREATMENT FACILITY						
611	Gravity thickener	1	-	1.50	1.50	1.0
613	Thickened sludge pump	1	-	5.50	5.50	0.6
614	Thickened effluent pump	1	-	5.50	5.50	0.6
615	Floor drainage pump	1	-	2.20	2.20	0.6
621	Excess sludge mixer	1	-	11.00	11.00	1.0
622	Excess sludge feed pump	1	-	30.00	30.00	1.0
623A	Centrifugal thickener drive motor	1	-	90.00	90.00	1.0
623B	Centrifugal thickener backdrive motor	1	-	22.00	22.00	1.0
623C	Centrifugal thickener lubrication pump	1	-	0.75	0.75	1.0
624	Crane (20t)	1	-	16.00	16.00	0.3
631	Mixed sludge mixer	2	-	11.00	22.00	1.0
632	Mixed sludge feed pump	1	-	11.00	11.00	1.0
633A	Centrifugal thickener drive motor	1	-	110.00	110.00	1.0
633B	Centrifugal thickener backdrive motor	1	-	37.00	37.00	1.0
633C	Centrifugal thickener lubrication pump	1	-	0.40	0.40	1.0
634A	Cake hopper	1	-	1.50	1.50	0.3
634B	Cake hopper	1	-	1.50	1.50	0.3
635	Polymer feeder	1	-	0.40	0.40	1.0
636	Polymer dissolution tank	1	-	5.50	5.50	1.0
637	Polymer feed pump	1	-	3.70	3.70	1.0

ELECTRICAL EQUIPMENT LIST

Name of electric consumer : Wastewater Treatment Plant (WWTP) - Phase 1

Address :

Working table-time :

Schedule of electric consumer: Issue date Rev.1 13-Jan-01

No.	Electrical equipment name	Q'ty	Capacity		Total (kW)	Remarks (Demand Factor)
			(HB)	(kW)		
638A	Water supply pump unit	1	-	18.50	18.50	0.6
638B	Water supply pump unit	1	-	18.50	18.50	0.6
639	Air compressor	1	-	5.50	5.50	0.5
640	Dehumidifier	1	-	0.25	0.25	0.5
641	Crane (20t)	1	-	16.00	16.00	0.3
643	Treatment water inflow valve	1	-	0.10	0.10	0.6
651	Recycle flow mixer	1	-	11.00	11.00	1.0
652	Recycle flow pump	1	-	30.00	30.00	0.6
671	Floor drainage pump	3	-	2.20	6.60	0.6
	COMPOST FACILITY					
721	Mixing machine	2	-	90.00	180.00	1.0
722	Sucking fan	2	-	5.50	11.00	1.0
723	Mumidifing pump	2	-	1.50	3.00	1.0
742	Deodorization fan	5	-	22.00	110.00	1.0
744	Spray water pump	1	-	2.20	2.20	0.5
745	Floor drainage pump	2	-	2.20	4.40	0.5
	VENTILATION FACILITY					
801	Air exhaust fan	8	-	0.40	3.20	1.0
802	Air exhaust fan	6	-	0.40	2.40	1.0
803	Air exhaust fan	8	-	0.30	2.40	1.0
804	Air exhaust fan	1	-	0.30	0.30	1.0
805	Air exhaust fan	1	-	0.30	0.30	1.0
806	Air exhaust fan	2	-	15.00	30.00	1.0
807	Air exhaust fan	2	-	7.50	15.00	1.0
808	Air exhaust fan	2	-	2.20	4.40	1.0
809	Air exhaust fan	3	-	0.40	1.20	1.0
810	Air exhaust fan	2	-	0.75	1.50	1.0
811	Air exhaust fan	1	-	7.50	7.50	1.0
812	Air exhaust fan	3	-	0.75	2.25	1.0
813	Air exhaust fan	1	-	0.25	0.25	1.0
814	Air exhaust fan	1	-	7.50	7.50	1.0
815	Air exhaust fan	1	-	2.20	2.20	1.0
816	Air exhaust fan	2	-	0.60	1.20	1.0

Sheet : 4 of 4

ELECTRICAL EQUIPMENT LIST

Name of electric consumer : Wastewater Treatment Plant (WWTP) - Phase 2

Address :

Working table-time :

Schedule of electric consumer:

Issue date

Rev.1

13-Jan-01

No.	Electrical equipment name	Q'ty	Capacity		Total (kW)	Remarks (Demand Factor)
			(HB)	(kW)		
	LIFT PUMP EQUIPMENT					
122	Lift pump (2)	3	-	460.00	1,380.00	0.6
	BLOWER EQUIPMENT					
212	Blower (1)	2	-	810.00	1,620.00	1.0
212A	Aux. Equipment for Blower (1)	2	-	6.00	12.00	1.0
214	Discharge valve (1)	2	-	0.75	1.50	0.6
215	Air filter	2	-	3.70	7.40	0.6
216	Floor drainage pump	3	-	2.20	6.60	0.6
	WATER TREATMENT FACILITY					
	(Primary sedimentation tank)					
312	Sludge scraper	30	-	1.50	45.00	1.0
314	Scum pump	3	-	5.50	16.50	0.6
315	Raw sludge pump	6	-	5.50	33.00	0.6
316	Raw sludge valve	30	-	0.20	6.00	0.6
317	Comminuter	1	-	0.75	0.75	1.0
	(Aeration tank)					
324	Air flow control valve	30	-	0.40	12.00	0.6
	(Final sedimentation tank)					
332	Sludge scraper	30	-	2.20	66.00	1.0
334	Scum pump	3	-	5.50	16.50	0.6
335	Return sludge pump (25%)	12	-	11.00	132.00	1.0
337	Return sludge valve	30	-	0.40	12.00	0.6
338	Excess sludge pump	6	-	11.00	66.00	0.6
339	Excess sludge valve	30	-	0.20	6.00	0.6
340	Comminuter	1	-	3.70	3.70	1.0
351	Floor drainage pump	30	-	2.20	66.00	0.6
	DISINFECTION FACILITY					
414	Sodium hypochlorite pump	6	-	0.40	2.40	1.0
	WATER SUPPLY FACILITY					
512	Treated water supply pump (1)	3	-	30.00	90.00	1.0
513	Treated water strainer (1)	1	-	0.40	0.40	0.6
516	Treated water strainer (2)	2	-	22.00	44.00	0.8
524	Fitered water supply pump	1	-	11.00	11.00	0.6

ELECTRICAL EQUIPMENT LIST

Name of electric consumer : Wastewater Treatment Plant (WWTP) - Phase 2
Address :
Working table-time :
Schedule of electric consumer: Issue date Rev.1 13-Jan-01

No.	Electrical equipment name	Q'ty	Capacity		Total (kW)	Remarks (Demand Factor)
			(HB)	(kW)		
	SLUDGE TREATMENT FACILITY					
611	Gravity thickener	3	-	1.50	4.50	1.0
613	Thickened sludge pump	3	-	5.50	16.50	0.6
614	Thickened effluent pump	3	-	5.50	16.50	0.6
615	Floor drainage pump	3	-	2.20	6.60	0.6
621	Excess sludge mixer	1	-	11.00	11.00	1.0
622	Excess sludge feed pump	3	-	30.00	90.00	1.0
623A	Centrifugal thickener drive motor	3	-	90.00	270.00	1.0
623B	Centrifugal thickener backdrive motor	3	-	22.00	66.00	1.0
623C	Centrifugal thickener lubrication pump	3	-	0.75	2.25	1.0
631	Mixed sludge mixer	6	-	11.00	66.00	1.0
632	Mixed sludge feed pump	3	-	11.00	33.00	1.0
633A	Centrifugal thickener drive motor	3	-	110.00	330.00	1.0
633B	Centrifugal thickener backdrive motor	3	-	37.00	111.00	1.0
633C	Centrifugal thickener lubrication pump	3	-	0.40	1.20	1.0
634A	Cake hopper	3	-	1.50	4.50	0.3
634B	Cake hopper	3	-	1.50	4.50	0.3
635	Polymer feeder	3	-	0.40	1.20	1.0
636	Polymer dissolution tank	3	-	5.50	16.50	1.0
637	Polymer feed pump	3	-	3.70	11.10	1.0
638A	Water supply pump unit	1	-	18.50	18.50	0.6
638B	Water supply pump unit	1	-	18.50	18.50	0.6
639	Air compressor	1	-	5.50	5.50	0.5
640	Dehumidifier	1	-	0.25	0.25	0.5
651	Recycle flow mixer	1	-	11.00	11.00	1.0
652	Recycle flow pump	1	-	30.00	30.00	0.6
662	Deodorization fan	1	-	7.50	7.50	1.0
671	Floor drainage pump	2	-	2.20	4.40	0.6
	COMPOST FACILITY					
721	Mixing machine	6	-	90.00	540.00	1.0
722	Sucking fan	6	-	5.50	33.00	1.0
723	Humidifying pump	6	-	1.50	9.00	0.5
742	Deodorization fan	15	-	22.00	330.00	1.0
744	Spray water fan	3	-	2.20	6.60	0.5
745	Floor drainage pump	6	-	2.20	13.20	0.5

