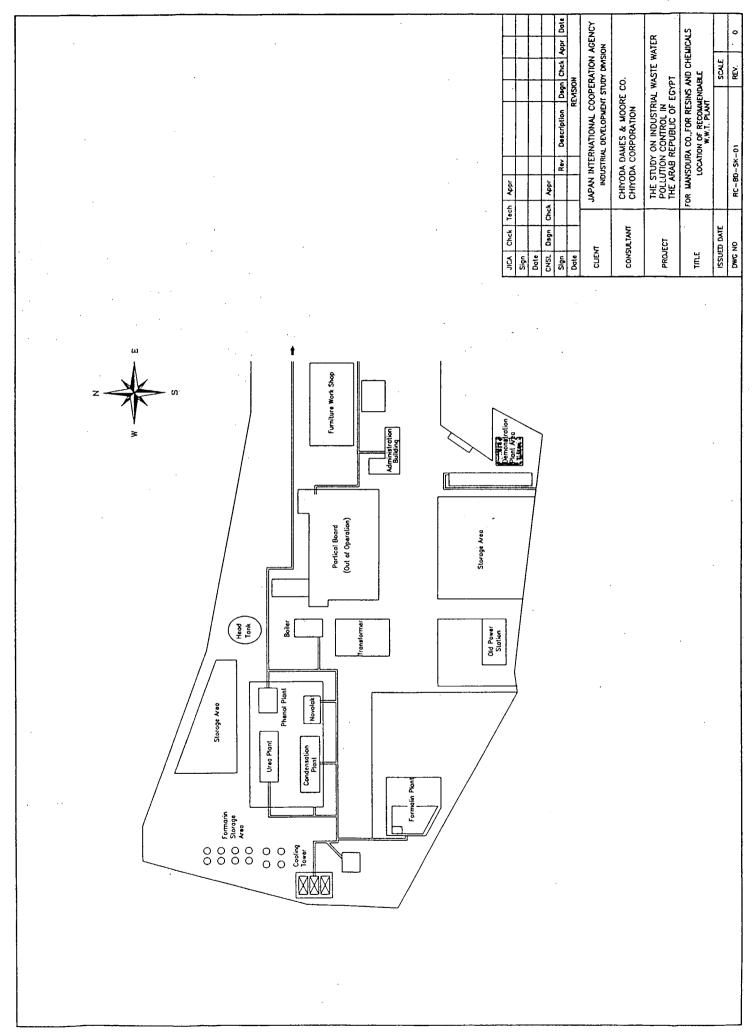
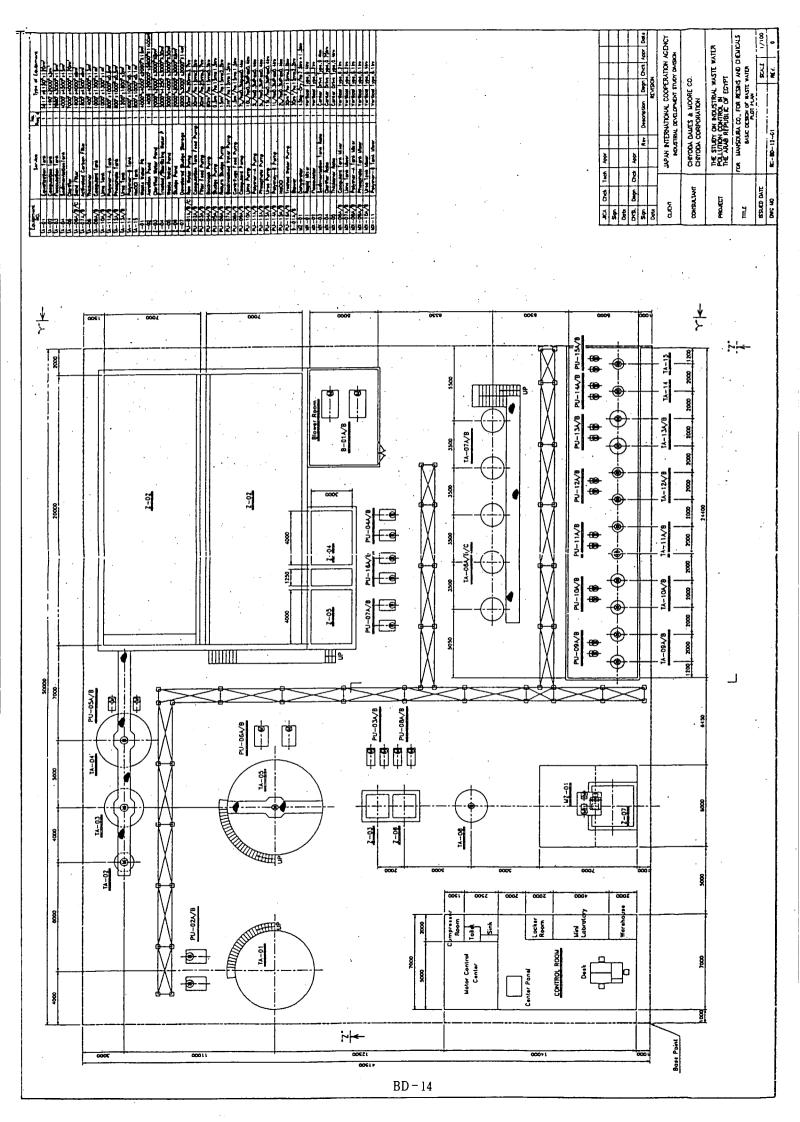
N INTERNATIONAL COOPERATION AGENCY	RECOMMENDABLE WASTEWATER TREATMENT PLANT	FOR	MANSOURA CO. FOR RESINS AND CHEMICALS	February 2000
		ENDABLE WASTEWATER	ENDABLE WASTEWATER FOR	ENDABLE WASTEWATER FOR NSOURA CO. FOR RESINS

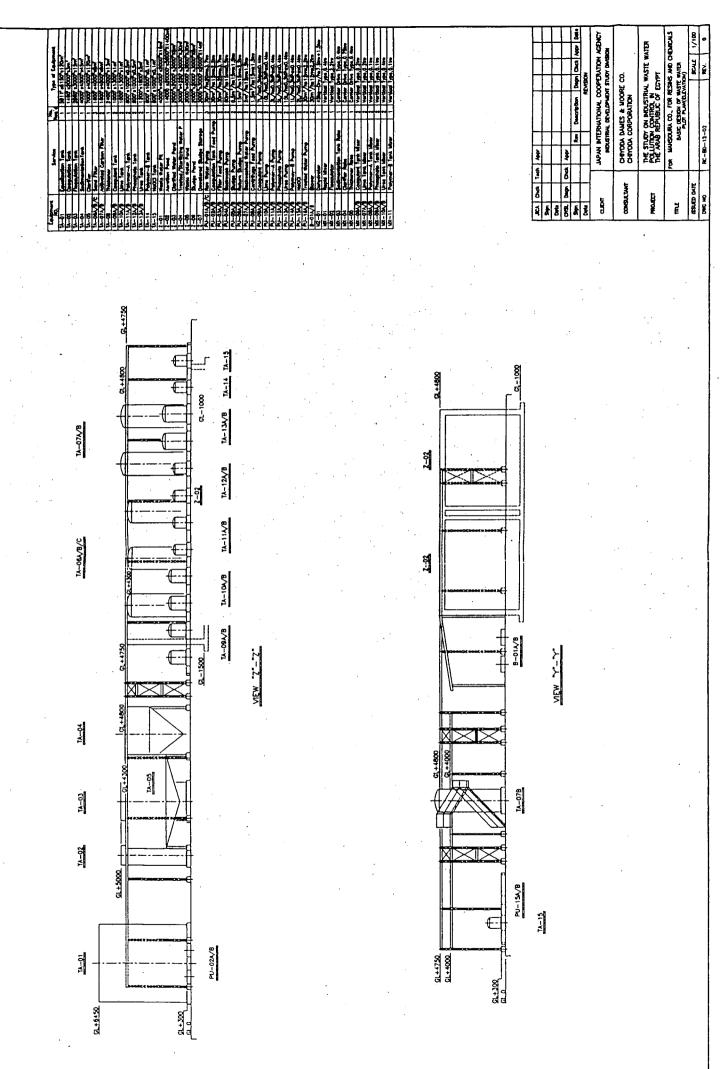
CHIYODA DAMES AND MOORE CO.

CHIYODA CORPORATION

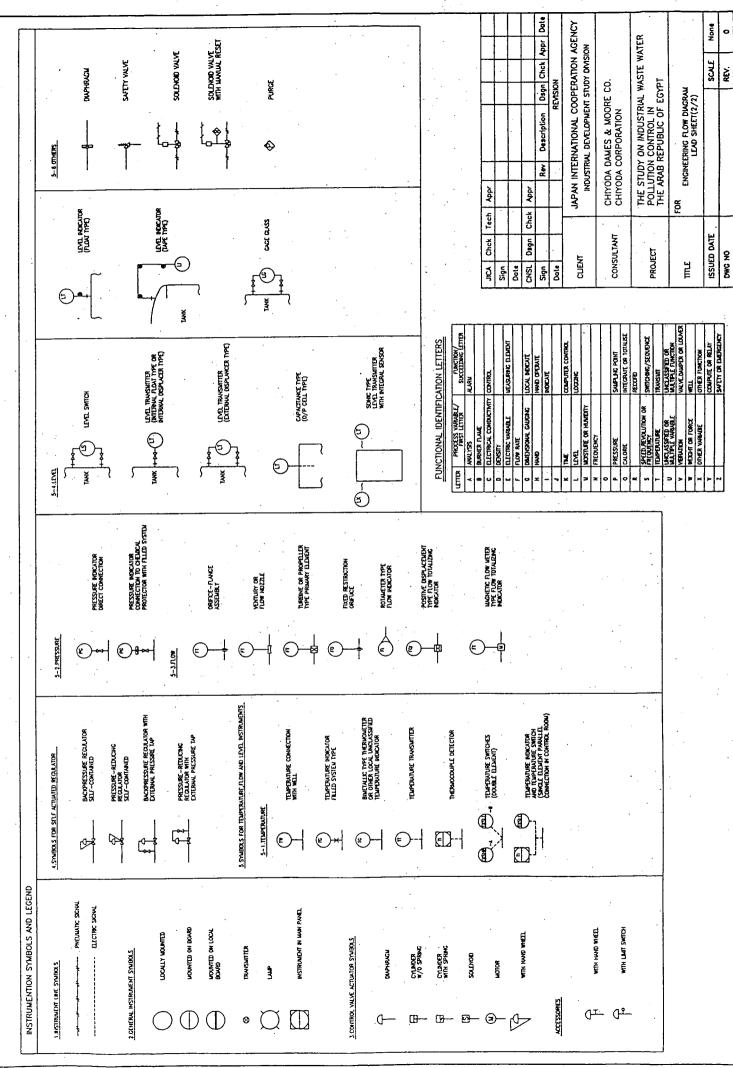
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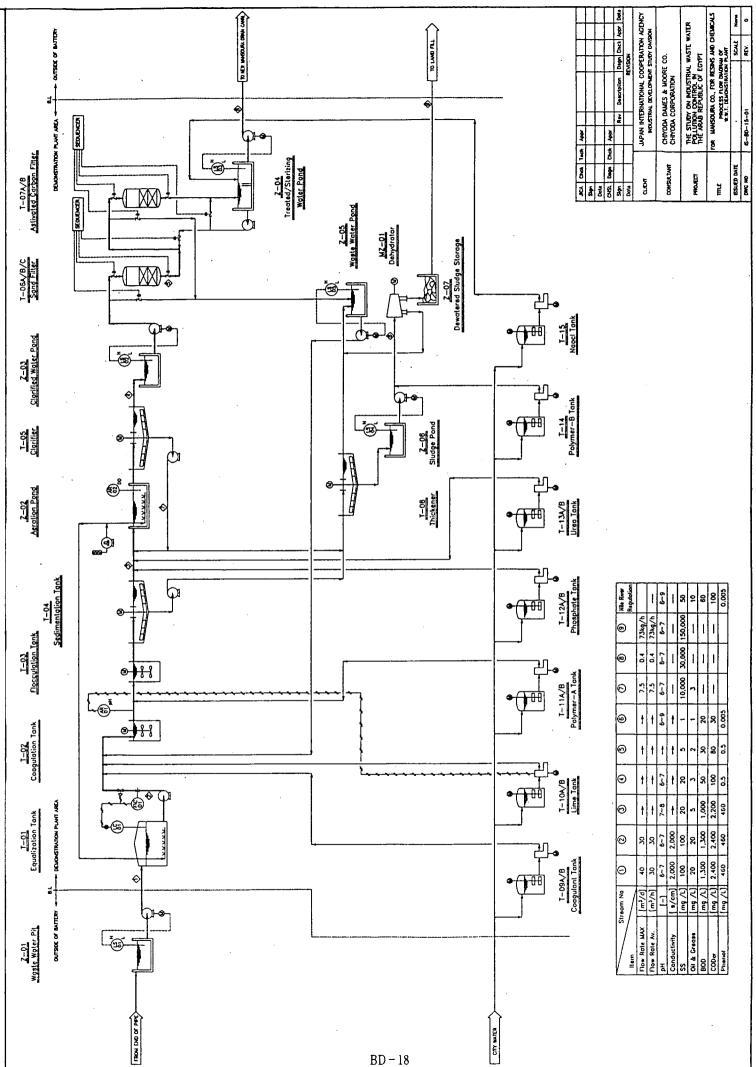


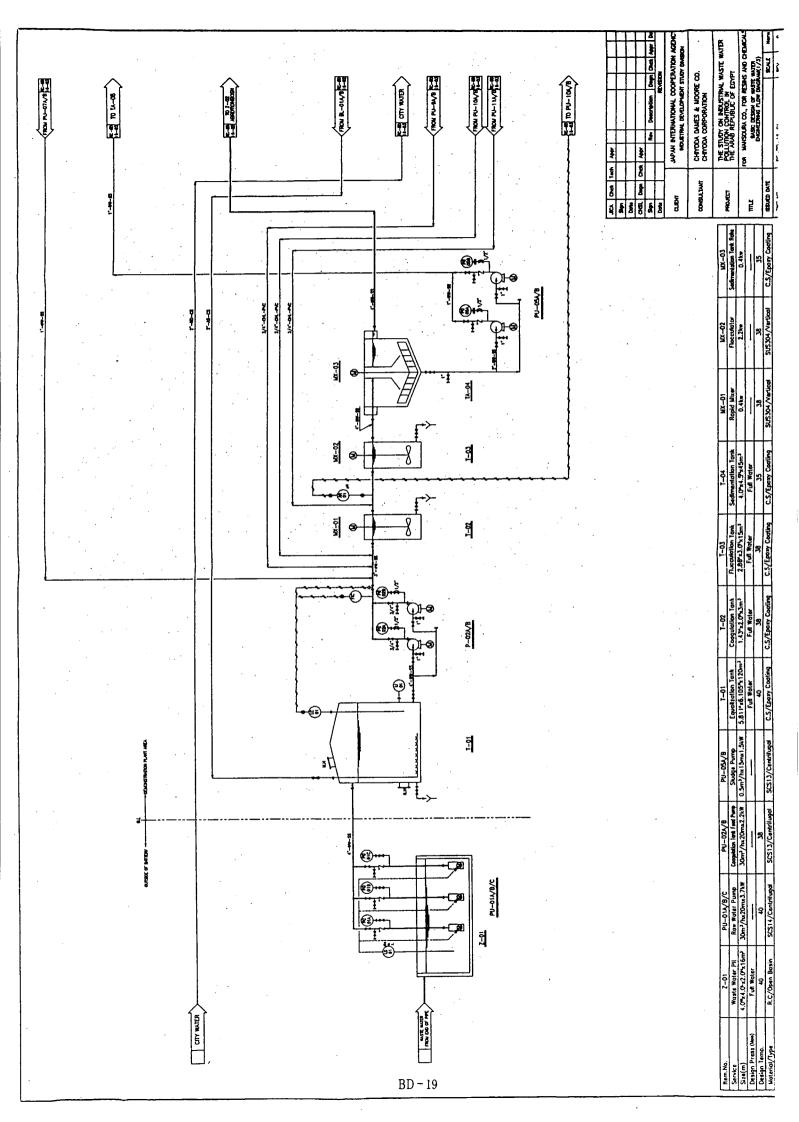
JAPAN INTERNATIONAL COOPERATION AGENCY None Rev Description | Dsgn | Chck | Appr | Dat ٥ THE STUDY ON INDUSTRIAL WASTE WATER POLLUTION CONTROL IN THE ARAB REPUBLIC OF EGYPT INDUSTRIAL DEVELOPMENT STUDY DMSION COOLING WATER SUPPLY COOLING WATER RETURN SCALE REV. TEUPORURY STRUNER RECONTRED WATER NOUSTRUL WATER DRINKING WATER NISCELLANEOUS INSTRUMENT AR UNNEACTURER FULURE CLOSE BATTERY LINE NONAL CLOSE FALURE OPEN SYMBOLS OF FLUID SWEETY VALVE NONAL OPEN CHIYODA DAMES & MOORE CO. CHIYODA CORPORATION WASTE WATER ATHOSPHERE REVISION SERMCE AR OLITY WELD ENGINEERING FLOW DIAGRAU LEAD SHEET(1/2) cuustic CHEMICAL SERMCE ABBREVIATION . ਸ SMBOL ଛ ٦, B ₹ ŝ 뛄 ರ Ē 2 e J ų £ **.**2 Appr JICA Chek Tech Appr <u>S</u> Chek ISSUED DATE CONSULTANT Dagn TO RUINY SEWER to oily sener PROJECT DWG NO SIGHT GLASS CLENT SYMBOLS OF EQUIPMENT EVE SHOWER LINE LIXER 빌 WND HOLE CNSL Sign JOH NUL Date Sig Dote SILENCER SHOWER ន ب<del>د</del> ᢞ THIOL NOTINATA 2 WOLL IN THE SLEEVE EXPANTION JOINT CONCENTRIC REDUCER TEMPORARY STRAINER ECCENTRIC REDUCER FLANCE CONNECTION RESTRICTION ORIFICE SYMBOLS OF EQUIPMENT HOSE CONNECTION SPECTACLE BUND I-TYPE STRAINER DIMPHRACK VALVE r-Tipe Strainer BUTTERFLY VALVE FLOW DETECTOR 3801 3181X314 NEEDLE VALVE COCK VALVE SWETY VILVE CHECK VALVE SEWER DRAW SIGHT CLASS SPOOL, PIECE GLOBE VALVE BALL VALVE FOOT VALVE SWAY VALVE CATE VALVE BLIND SYMBOLS OF LINE 3 ţ ٩ 84 2  $\oslash$ 8 Ż ¢ IN EACH SYSTEM ETD DESIGNATES PIPING CLASS CHANCES OR APPLICABLE LOW. WAGINARY LINE, BURIED LINE SAMPLING CONNECTION FOR WATER FROM PIPE LINE FACTORY-JICA UNIT-UNIT PROCESS LINE ( & UTILITY LINE etc.) UTILITY LINE SUPPLEMENTIARY LINE 6-63 SAMPLING CONNECTION JUN PROCESS UNE BOUNDARY LINE LINE IDENTIFICATION CENTER LINE CONTRACTOR SYMBOLS OF LINE INCLUED ETD SHEET NO. NUN NEN BREAK DOWN OF EFD-EFD PROCESS LINE FROM FLUID NAME FLUID NAME FROM of TO NON NON  $\langle$ GENERAL VERTICAL TYPE(OPEN) RECIPROCATING PUMP CENTRIFUCAL PUMP. HORIZONTAL TYPE CONE ROOF TANK BELT CONVEYOR BELT CONNEYOR ELECTRIC HOIST PUMP, BLOWER, ETC MOTOR DRIVEN VERTICAL TYPE ROOT BLOWER DUMP TRUCK OPEN TANK TANK CAR EJECTOR DRUMS NOCR TANK ⊚\_\_{ Ţ ЧŢ Ø ¶¶• ģ М ¢  $\bowtie$ 

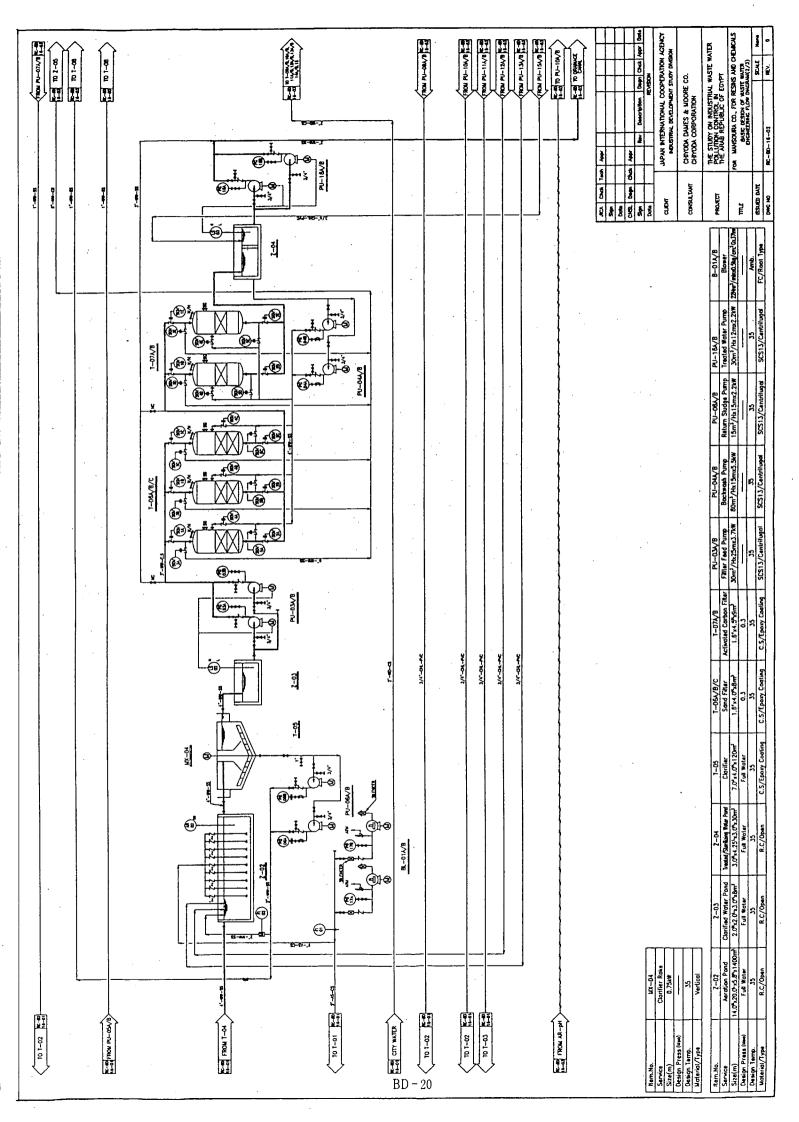


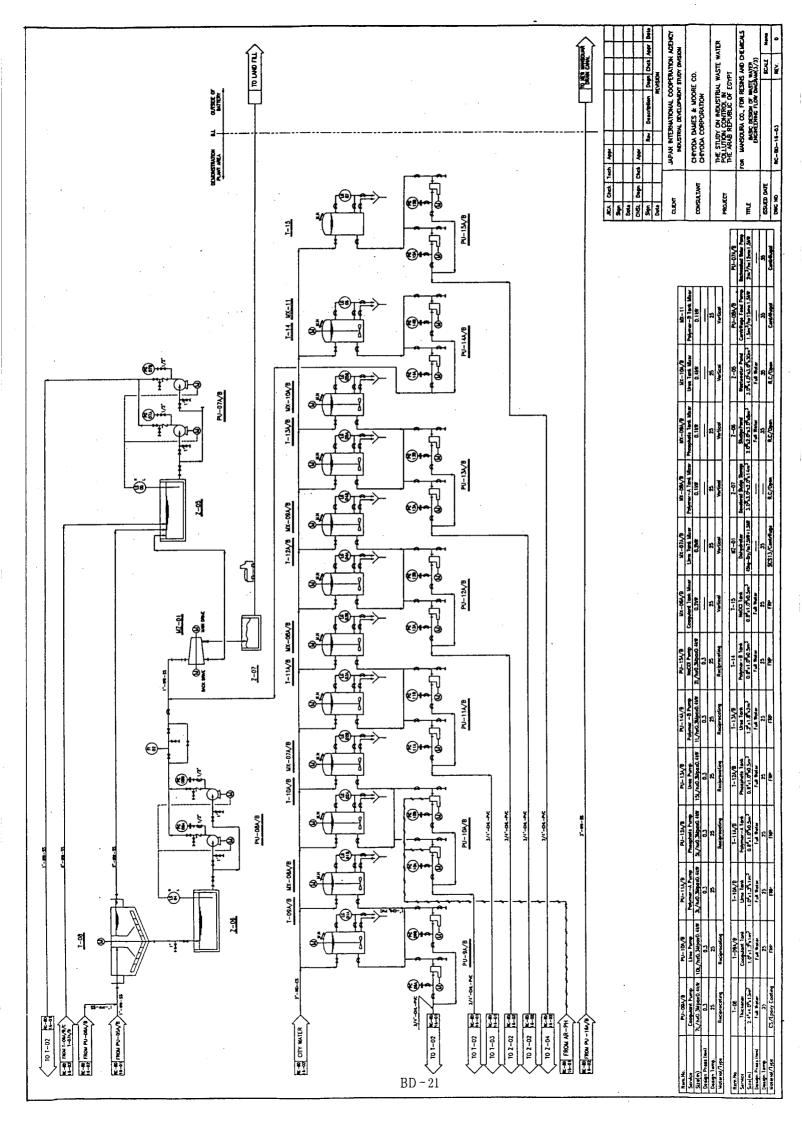
BD - 17

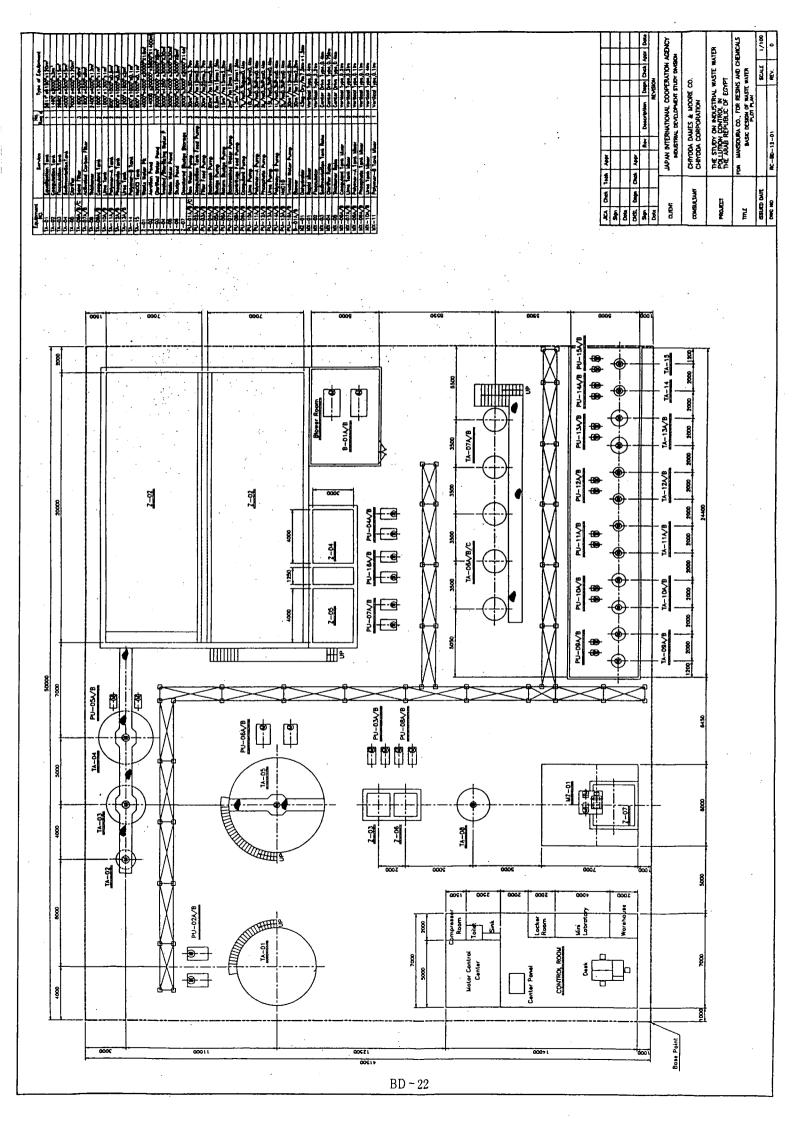
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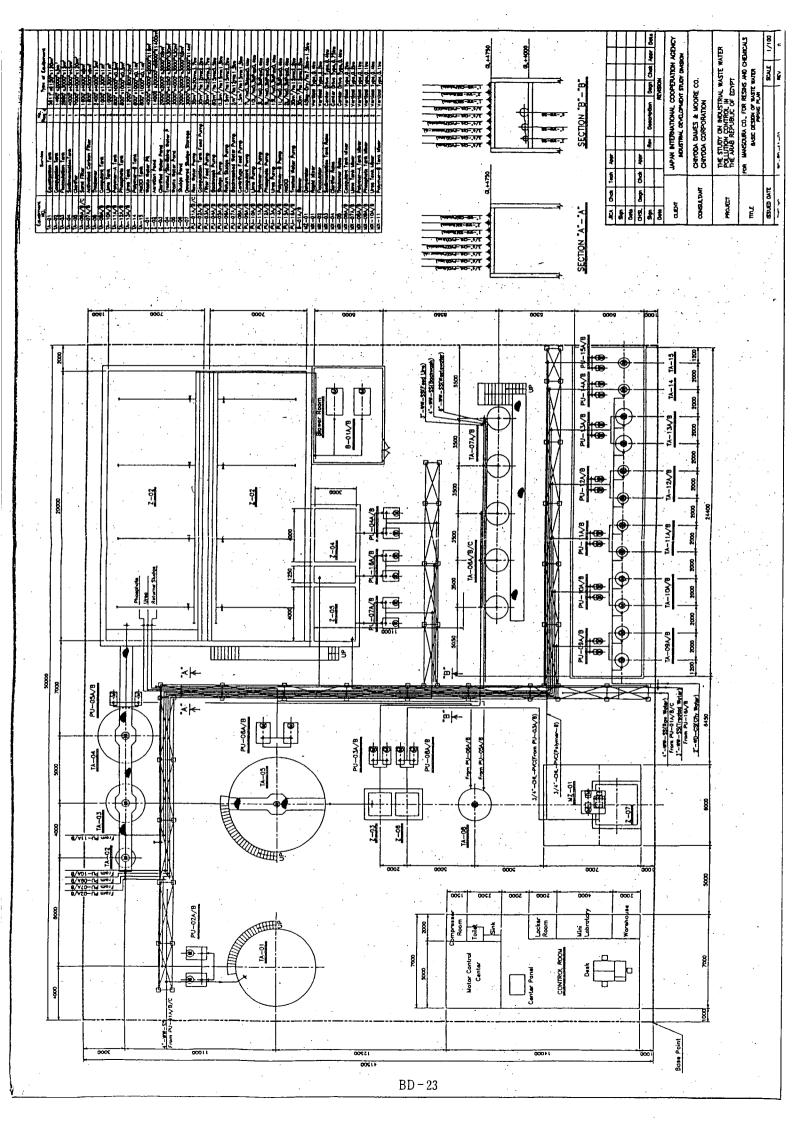






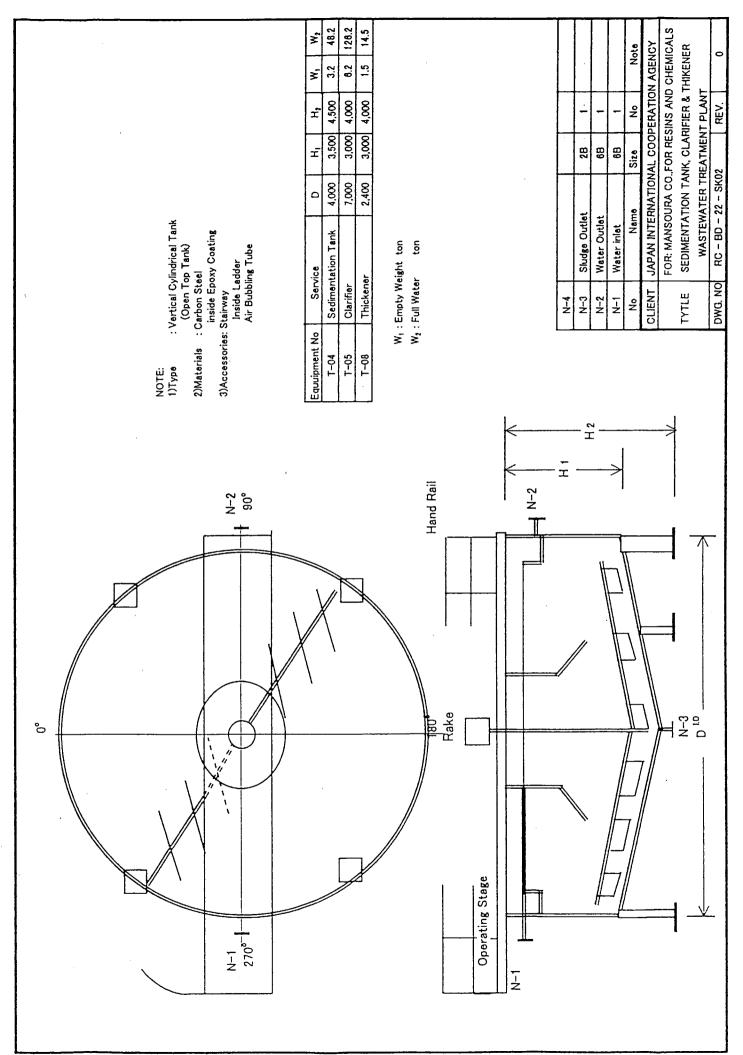






FOR: MANSOURA CO., FOR RESINS AND CHEMICALS JAPAN INTERNATIONAL COOPERATION AGENCY Note 0 120 m<sup>3</sup> EQUALIZATION TANK (T - 01) WASTEWATER TREATMENT PLANT REV. ° 500 ¢ Size 500 ¢ ... 7 . ~ , ~ ۴, , T 4 RC - BD - 22 - SK01 Raw Water Outlet **Bubbling Air Inlet** Level Instrument Raw Water inlet Name 9.7 ton 130 ton : Vertical Cylindrical Tank (Open Top Tank) : Carbon Steel inside Epoxy Coating **Over Flow** Manhole Manhole 3)Accessories: Stairway Inside Ladder Air Bubbling Tube Drain : Empty Weight : Full Water DWG. NO CLIENT TYTLE M-2 8--N N-3 M-1 2-2 N-2 N-4 N-2 ł ŕ Loading Data : 2)Materials NOTE: 1)Type Top Angle L65x65x5t N-2, N-4 9-N N-3 90°-3 135° N-7 7-7 ₩-7 Foundation (RC) Air Bubbling Pipe N-2 -1 180° 5,811<sup>10</sup> ဝိ <del>1</del>9 ĕ 4.5t N-8 225° Π 个 270° N-1 N-1 M-1 <sup>H</sup>201.9

BD-24

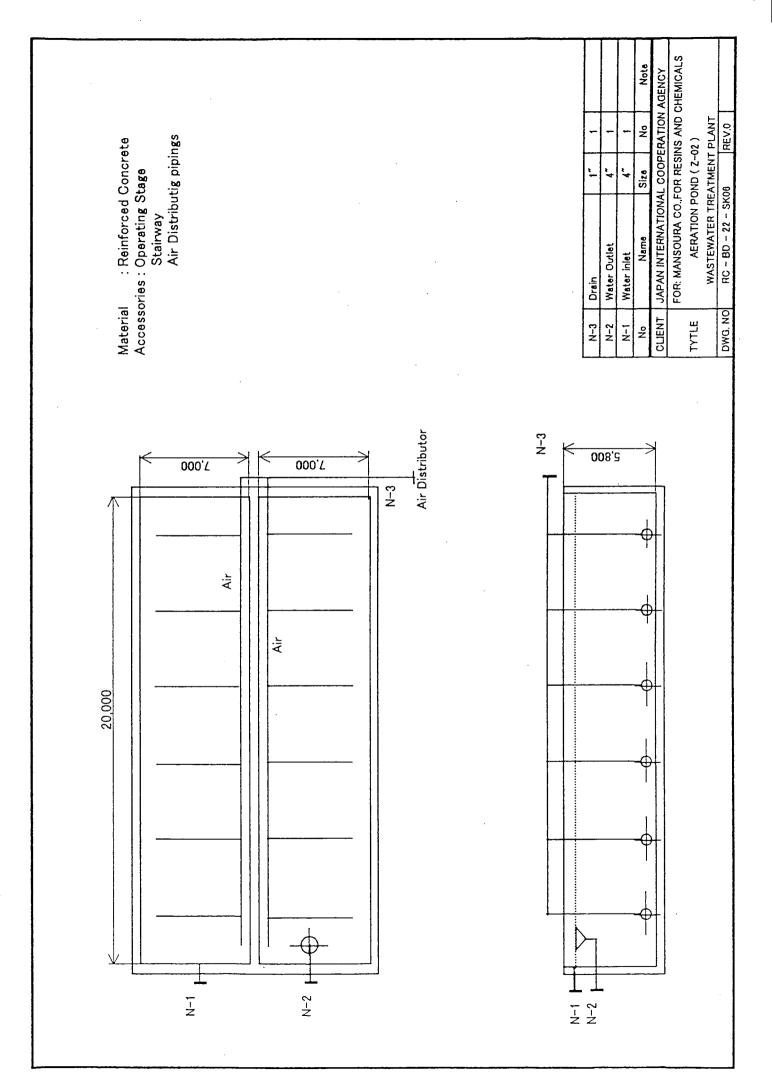


NOTE: 1)Type : Vertical Cylindrical Tank (Open Top Tank) 2)Materials : Cerbon Steel inside Epoxy Coating 3)Accessories: Stairway Inside Ladder Air Bubbling Tube	o Service D H, H <sub>2</sub> W,	Sand Filter 1.600 4,000 6,000 8.9	1-03A/B Activated Carbon Filter 1,600 4,500 8,500 6.8 17.8	W <sub>1</sub> : Empty Weight ton W <sub>2</sub> : Full Water ton		M-3 Manhole 500Φ 1	Manhole		N-3 Surface Wash water 2" 1	N-2 Filtered Water Outlet / 4" 1	Backwash Water Inlet	N-1 Clarified W.ater inlet/ 8" 1	Backwash Waste Outlet	No Name Size No Note	CLIENT JAPAN INTERNATIONAL COOPERATION AGENCY	FOR: MANSOURA CO., FOR RESINS AND CHEMICALS	TYTLE SAND FILTER & ACTIVATED CARBON FILTER	WASTEWATER TREATMENT F	DWG. NO  RC - BD - 22 - SK03   REV.   0
	180°	N1 M-1	1		H-3	H	Anthracite	Activated	Carbon	Gravel		N-2				N-2 M-2			

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NOTE: NOTE: 1)Type : Vertical Cylindrical Tank (Open Top Tank) 2)Materials : Carbon Steel inside Epoxy Coating 3)Accessories: Stairway	Equuipment NoServiceDHW_1W_2 $T-02$ Coagulant Tank $1,430$ $2,000$ $3$ $18$ $T-03$ Flocculation Tank $2,800$ $3,000$ $3$ $18$ W <sub>1</sub> : Empty Weight tonW <sub>2</sub> : Full Waterton	N-3     Drain     1"     1       N-2     Water Outlet     4"     1       N-1     Water Inter     4"     1	Name Si	CLIENT JAPAN INTERNATIONAL COOPERATION AGENCY	FOR: MANSOURA CO.FOR RESINS AND CHEMICALS TYTLE COAGULATION/FLOCCULATION TANK (T-02/03)	WASTEWATER TREATMENT PLANT       DWQ. NO     RC - BD - 22 - SK05
N-1 0 0 10,0 10,0 10,0 10,0 10,0 10,0 10,	H			E-1	V V I V	

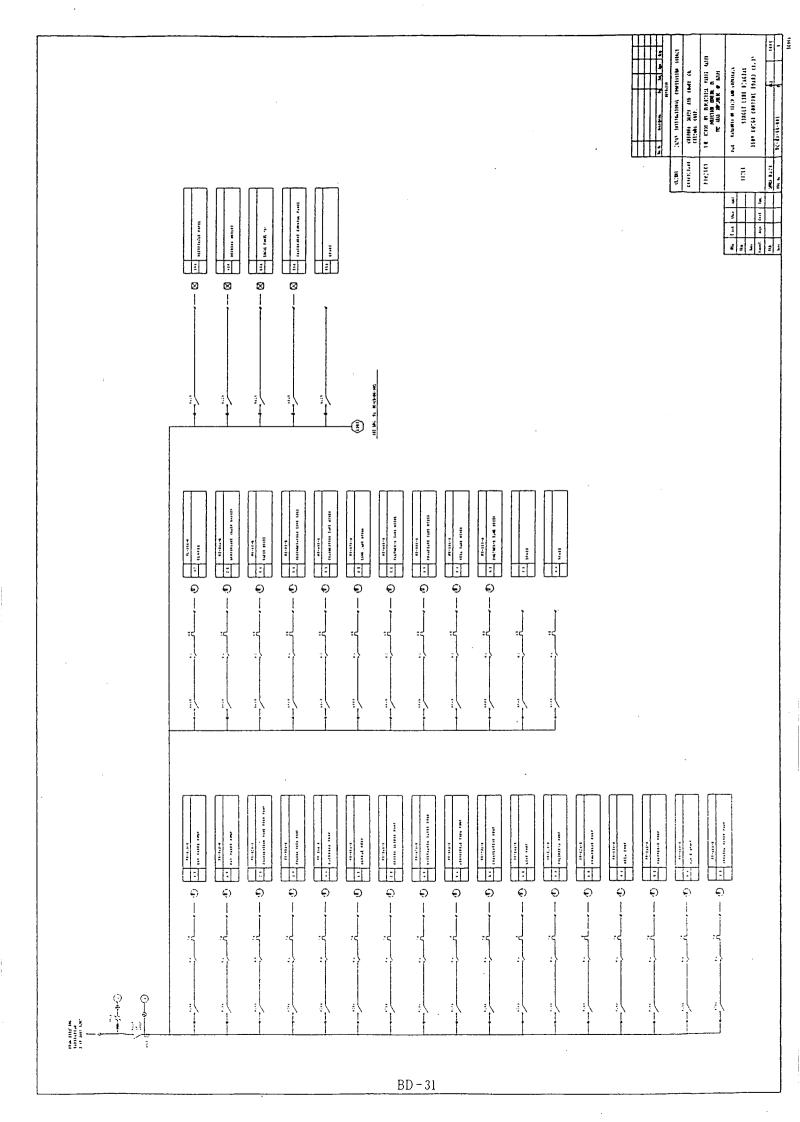
idrical Tank	D         H <sub>1</sub> H <sub>2</sub> W <sub>1</sub> W <sub>1</sub> W <sub>1</sub> 1,000         1,300         6,000         0.06         1           1,000         1,300         6,000         0.06         1           800         1,000         6,000         0.04         0.5           800         1,000         6,000         0.04         0.5           800         1,000         6,000         0.04         0.5           800         1,000         6,000         0.04         0.5           800         1,000         6,000         0.04         0.5	4000 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	Name     Size     No     Note       JAPAN INTERNATIONAL COOPERATION AGENCY     FOR: MANSOURA CO.FOR RESINS AND CHEMICALS     CHEMICAL TANK       CHEMICAL TANK     WASTEWATER TREATMENT PLANT     RC - BD - 22 - SK04     REV.     0
NOTE: 1)Type : Vertical Cylindrical Tank 2)Materials : FRP 3)Accessories: Level Gage	Equuipment No Service T-09A/B Coagulation Tank T-10A/B Lime Tank T-11A/B Polymer-A Tank T-13A/B Urea Tank T-13A/B Polymer-B Tank T-15A/B NaOCI Tank Y, : Empty Weight ton W <sub>2</sub> : Full Water ton	M-1ManholeN-5VentN-4DrainN-3Level GageN-2Level GageN-1Water Inlet	⊢ <u></u> 9
270° N-2 N-3 0°	N-1 N-1 N-1 N-1 N-1 N-2 N-2 N-1 N-2 N-1 N-1 N-1 N-1 N-1 N-1 N-1 N-1	 	N-3

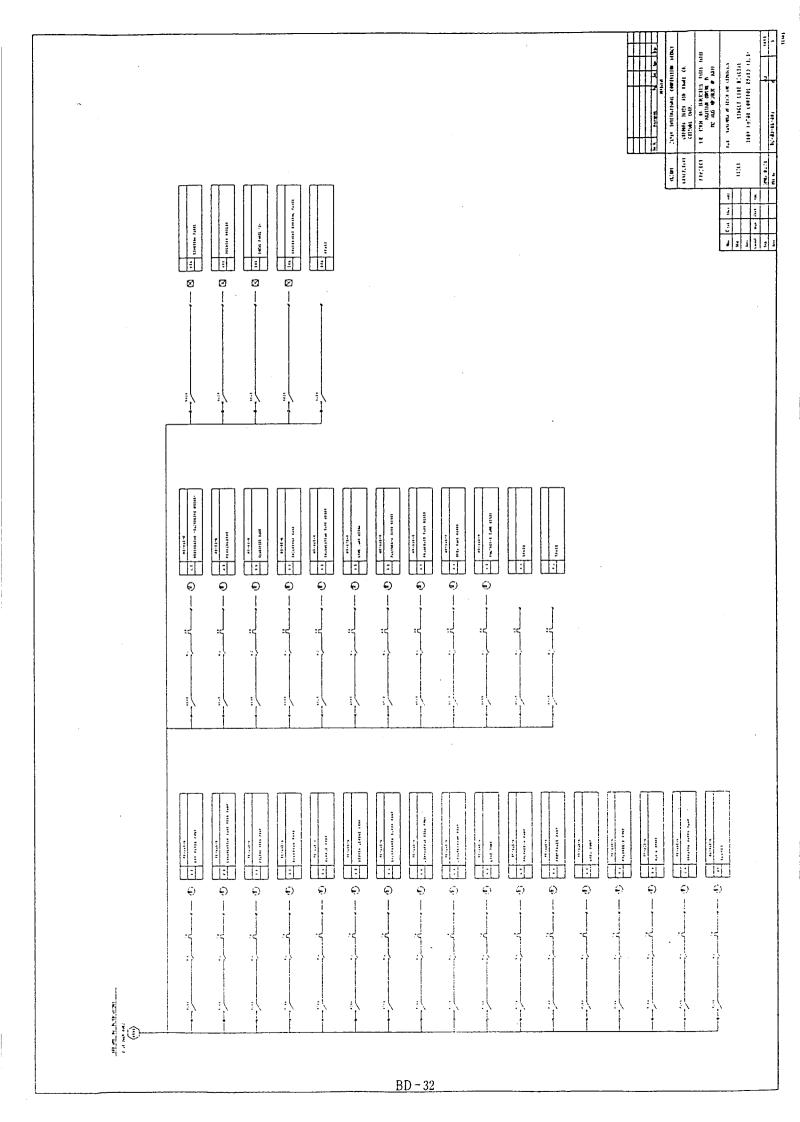


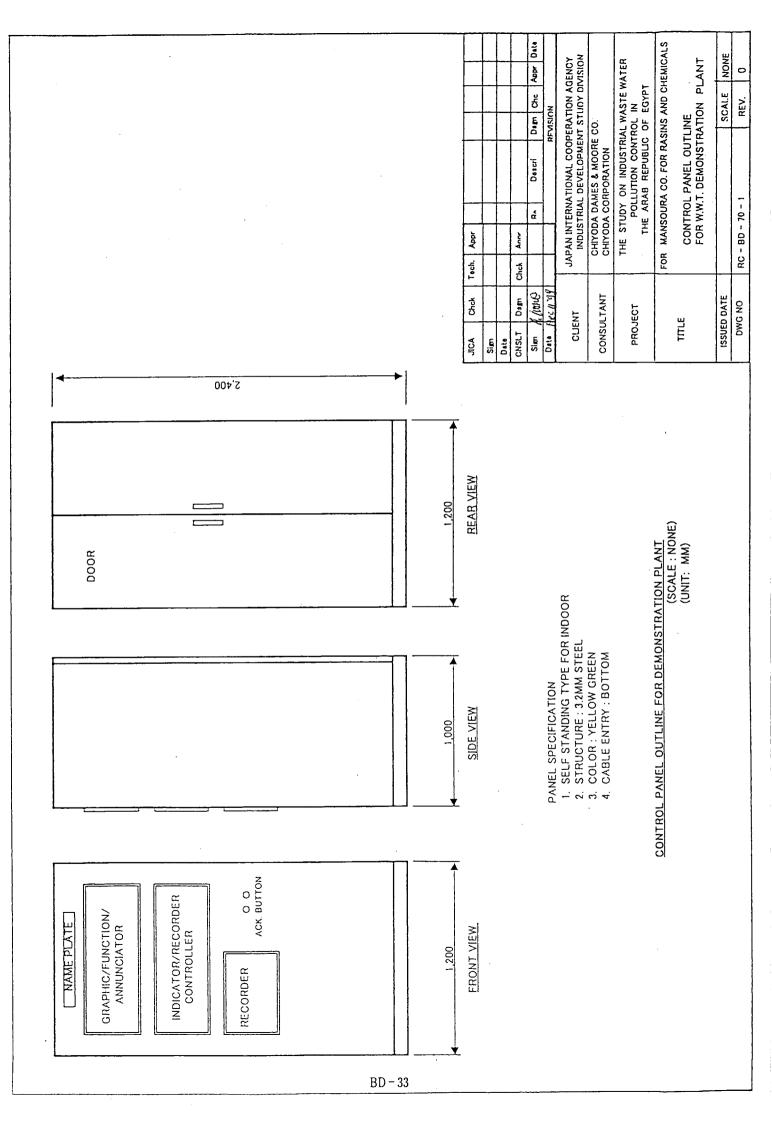
\*2; SHIELD EARTH \*1; PLANT EARTH ·LIGHTING ·EQUIPMENT ·LOCAL PANEL ·LOCAL PANEL \* \* \* ·INSTRUMENT \*3; LIGHTNING MOTOR 220VAC,24VDC 220VAC **380VAC** 220VAC \*1\*2 ¥ CONTROL PANEL INSTRUMENT POWER DISTRIBUTION PANEL TRANSFORMER WWT DEMONSTRATION PLANT (NEW) CONTROL ROOM (NEW) ø MOTOR CONTROL ¥ CENTER 380VAC/50HZ SUB-STATION (EXISTING) SWITCH GEAR (EXISTING)

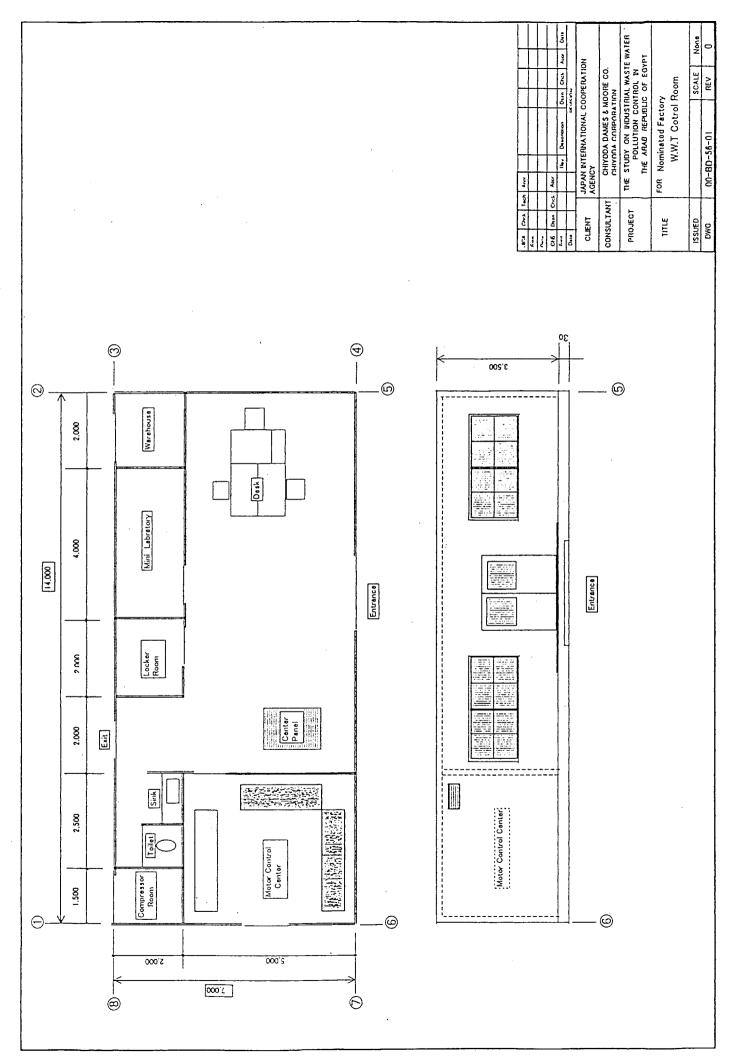
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CONFIGURATION OF ELECTRICAL & INSTRUMENTATION SYSTEM FOR DEMONSTRATION PLANT









CLIENT :Japan International Cooperation Agency	REV	1	2	3	MADE	- Dan
PROJECT : The Study on Industrial Waste Water Plant	BY				CKD	U
PLANT : Monsoura Co. for Resins and Chemicals	APVE				APVE	
WASTE W. :End of Pipe(Sanitary Waste W.+ Waste Water)	DATE				DATE	05616.99

(1/5)

	No. Type of Equipment No. Reg'd		Remarks	
T-01 E	Equalization Tank	1	Vertical Cylindrical Type	Carbon Steel/Epoxy
	:		5,811 $^{\circ}$ × 6,105 <sup>H</sup> × 120 m <sup>3</sup>	Coating
T-02 0	Coagulation Tank	1	Vertical Cylindrical Type	Carbon Steel/Epoxy
			1, $430^{\circ} \times 2$ , $000^{H} \times 3 \text{ m}^{3}$	Coating
T-03 F	Flocculation Tank	1	Vertical Cylindrical Type	Carbon Steel/Epoxy
	·		2,860 $^{\bullet}$ × 3,000 $^{H}$ × 15 m <sup>3</sup>	Coating
T-04 S	Sedimentation Tank	1	Vertical Cylindrical Type	Carbon Steel/Epoxy
			4, $000^{\circ} \times 4$ , $500^{H} \times 45 \text{ m}^{3}$	Coating
T-05 C	Clarifier	1	Vertical Cylindrical Type	Carbon Steel/Epoxy
			7,000 $^{\diamond} \times 4$ ,000 $^{\rm H} \times 120 {\rm m}^3$	Coating
-06A/B/CS	Sand Filter	3	Vertical Cylindrical Type	Carbon Steel/Epoxy
			$1,600^{\diamond} \times 4,000^{H} \times 8 m^{3}$	Coating
T-07A/B	Activated Carbon Filter	2	Vertical Cylindrical Type	Carbon Steel/Epoxy
			1,600 $^{\diamond}$ × 4,500 <sup>H</sup> × 9 m <sup>3</sup>	Coating
T-08 1	Thickener	1	Vertical Cylindrical Type	Carbon Steel/Epoxy
			2, $400^{\circ} \times 4$ , $000^{H} \times 13 m^{3}$	Coating
T-09A/B	Coagulant Tank	2	Vertical Cylindrical Type	FRP
			$1,000^{\circ} \times 1,300^{H} \times 1 m^{3}$	
T-10A/B	Lime Tank	2	Vertical Cylindrical Type	FRP
			$1,000^{\circ} \times 1,300^{H} \times 1 m^{3}$	
T-11A/B	Polymer-A Tank	2	Vertical Cylindrical Type	FRP
			$800^{\circ} \times 1,000^{H} \times 0.5 m^{3}$	
T-12A/B	Phosphate Tank	2	Vertical Cylindrical Type	FRP
			$800^{\circ} \times 1,000^{H} \times 0.5 m^{3}$	

CLIENT : Japan International Cooperation Agency		1	2	3	MADE	
PROJECT : The Study on Industrial Waste Water Plant	BY				CKD	
PLANT :Monsoura Co. for Resins and Chemicals	APVE				APVE	
WASTE W. <u>:End of Pipe(Sanitary Waste W.+ Waste Water)</u>	DATE				DATE	

(2/5)

Equipment NO.			Type of Equipment	Remarks
T-13A/B	Urea Tank	2	Vertical Cylindrical Type	FRP
			$1,200^{\circ} \times 1,800^{H} \times 2 m^{3}$	
T-14	Polymer-B	1	Vertical Cylindrical Type	FRP
			$800^{\circ} \times 1,000^{H} \times 0.1 \text{ m}^{3}$	
T-15	NaOCl Tank	1	Vertical Cylindrical Type	FRP
			$800^{\bullet} \times 1,000^{H} \times 0.1 \text{ m}^{3}$	
Z-01	Waste Water Pit	1	Vertical Square Type	Reinforced Concrete
			4,000 $^{\texttt{W}}$ × 4,000 <sup>L</sup> × 2,000 <sup>H</sup> × 16 m <sup>3</sup>	
Z-02	Aeration Pond	1	Vertical Rectangular Type	Reinf: Coating
			$14,000^{\texttt{W}} \times 20,000^{\texttt{L}} \times 5,800^{\texttt{H}} \times 1,4$	00 m <sup>3</sup>
Z-03	Clarified Water Pond	1	Vertical Square Type	Reinforced Concrete
			2,000 <sup>#</sup> ×2,000 <sup>L</sup> ×3,000 <sup>H</sup> ×8 m <sup>3</sup>	
Z-04	Treated/Sterilizing Water P.	1	Vertical Rectangular Type	Reinforced Concrete
			$3,000^{\text{W}} \times 5,250^{\text{L}} \times 3,000^{\text{H}} \times 30 \text{ m}^{3}$	
Z-05	Waste Water Pond	1	Vertical Rectangular Type	Reinforced Concrete
			$3,000^{\text{W}} \times 4,000^{\text{L}} \times 3,000^{\text{H}} \times 30 \text{ m}^3$	
Z-06	Sludge Pond	1	Vertical Square Type	Reinforced Concrete
			2,000 <sup><math>\text{W} \times 2</math>,000<sup><math>\text{L} \times 3</math>,000<sup><math>\text{H} \times 8 m3</math></sup></sup></sup>	
Z-07	Dewatered Sludge Storage	1	Vertical Square Type	Reinforced Concrete
, 			$3,000^{\text{W}} \times 3,000^{\text{L}} \times 2,000^{\text{H}} \times 14 \text{ m}^3$	
			· · · · · · · · · · · · · · · · · · ·	
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Note:

CLIENT : Japan International Cooperation Agency	REV	1	2	3	MADE	
PROJECT :The Study on Industrial Waste Water Plant	BY				CKD	
PLANT : Monsoura Co. for Resins and Chemicals	APVE				APVE	
WASTE W. :End of Pipe(Sanitary Waste W. + Waste Water)	DATE				DATE	

(3/5)

Equipment NO.	Service	No. Req'd	Type of Equipment	Remarks
PU-01	Raw Water Pump	3	Submergible Type	SCS14/SCS14
A/B/C			30 m <sup>3</sup> /h×20 m×3.7 k₩	
PU-02A/B	Coagulation Tank Feed Pump	2	Horizontal Centrifugal Type	SCS13/SCS13
			30 m³/h×12 m×2.2 k₩	
PU-03A/B	Filter Feed Pump	2	Horizontal Centrifugal Type	SCS13/SCS13
			30 m³/h×25 m×3.7 k₩	
PU-04A/B	Backwash Pump	2	Horizontal Centrifugal Type	SCS13/SCS13
	· ·		80 m³/h×15 m×5.5 k₩	
PU-05A/B	Sludge Pump	2	Horizontal Centrifugal Type	SCS13/SCS13
			0.5 m³/h×15 m×1.5 k₩	
PU-06A/B	Return Sludge Pump	2	Horizontal Centrifugal Type	SCS13/SCS13
			15 m <sup>3</sup> /h×15 m×2.2 kW	
PU-07A/B	Backwashed Water Pump	2	Horizontal Centrifugal Type	SCS13/SCS13
			2 m <sup>3</sup> /h×12 m×1.5 kW	
PU-08A/B	Centrifuge Feed Pump	2	Horizontal Centrifugal Type	SCS13/SCS13
			1.5 m³/h×15 m×1.5 k₩	
PU-09A/B	Coagulant Pump	2	Reciprocating Type	SCS14/SCS14
			7 L/h×0.3 Mpa×0.4 k₩	
PU-10A/B	Lime Pump	2	Reciprocating Type	SCS13/SCS13
			10 L/h×0.3 MPa×0.4 k₩	
PU-11A/B	Polymer-A Pump	2	Reciprocating Type	SCS13/SCS13
			3 L/h×0.3 MPa×0.4 k₩	
PU-12A/B	Phosphate Pump	2	Reciprocating Type	SCS13/SCS13
			5 L/h×0.3 MPa×0.4 k₩	
			· · · · · · · · · · · · · · · · · · ·	

Note:

CLIENT : Japan International Cooperation Agency	REV	1	2	3	MADE	
PROJECT : The Study on Industrial Waste Water Plant	BY				CKD	
PLANT :Monsoura Co. for Resins and Chemicals	APVE				APVE	
WASTE W. :End of Pipe(Sanitary Waste W. + Waste Water)	DATE				DATE	

(4/5)

Equipment NO.	Service	No. Reg'd	Type of Equipment	Remarks
PU-13A/B	Urea Pump	2	Reciprocating Type	SCS13/SCS13
			15 L/h×0.3 MPa×0.4 k₩	
PU-14A/B	Polymer-B Pump	2	Reciprocating Type	SCS13/SCS13
			1 L/h×0.3 MPa×0.4 k₩	
PU-15A/B	NaCl0	2	Reciprocating Type	PVC/PVC
			2 L/h×0.3 MP×0.4 k₩	
2U−16A/B	Treated Water Pump	2	Horizontal Centrifugal Type	SCS13/SCS13
			30 m <sup>3</sup> /h×12 m×2.2 k₩	
B-01A/B	Blower	2	Root Type	FC/FC
	,		22 Nm³/min×0.05 MPa×37 k₩	
MZ-01	Dehydrator	1	Centrifuge Type	SCS13/SCS13
			45 kg-Dry/h×7.5 k₩+1.5 k₩	
			Sharples/Super-D-Canter	· ·
MX-01	Rapid Mixer	1	Vertical Type, 0.4 kW	SUS304
MX-02	Flocculator	1	Vertical Type,2.2 k₩	SUS304
MX-03	Sedimentation Tank Rake	1	Center Drive Type, 0.4 k₩	Carbon Steel
				/Epoxy Coating
MX-04	Clarifier Rake	1	Center Drive Type, 0.75 k₩	Carbon Steel
				/Epoxy Coating
MX-05	Thickener Rake	1	Center Drive Type, 0.4 k₩	Carbon Steel
				/Epoxy Coating
MX-06A/B	Coagulant Tank Mixer	2	Vertical Type, 0.2 kW	SUS304
	Lime Tank Mixer	2	Vertical Type, 0.2 kW	SUS304
	Polymer-A Tank Mixer	2	Vertical Type, 0.1 kW	SUS304
	Phosphate Tank Mixer	2	Vertical Type, O.1 kW	SUS304

Note:

CLIENT : Japan International Cooperation Agency	REV	1	2	3	MADE	
PROJECT :The Study on Industrial Waste Water Plant	BY				CKD	
PLANT : Monsoura Co. for Resins and Chemicals	APVE				APVE	
WASTE W. End of Pipe(Sanitary Waste W.+ Waste Water)	DATE				DATE	

(5/5)

Equipment NO.		Service	No. Req'd	Type of Equipment	Remarks
MX-10A/B	Urea Tank	Mixer	2	Vertical Type, 0.4 kW	SUS304
MX-11A/B	Polymer-B	Tank Mixer	2	Vertical Type, 0.1 kW	SUS304
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Note:					

## INSTRUMENT LIST for Mansoura Co. for Resins and Chemicals

DOC. NO.	:RC-BD-L2-(1/3)
CLIENT	:Japan International Cooperation Agency

PROJECT : The Study on Industrial W. W. Pollution Control

TROJECT The order on Indescriter .....

 REV
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 3
 MADE

 BY
 CKD

 APVE
 APVE

 DATE
 DATE
 DEC. 16.59

 PLANT
 :Monsoura Co. for Resins and Chemicals

 WASTE W.
 :End of Pipe(Sanitary Waste W. + Waste Water)

Equipment NO.	Service	No. Reg'd	Type of Equipment	Remarks
AR-01	WW, T-02 Coagulation T. Out	1	pH 4~10	
			pH Analyzer	С. Р.
AR-02	WW, Z-02 Aeration Pond	1	0~10 mg/L	
			Disolved Oxygen Analyzer	С. Р.
FIC-01	Sedimentation line	1	10 m <sup>3</sup> /h~50 m <sup>3</sup> /h	
			Flow Indicating Controller	
FI-01	AS, BL-01A/B Blower Outlet	1	15 Nm <sup>3</sup> /min~30 Nm <sup>3</sup> /min	
			Flow Meter	
FI-02	WW, Z-02 Aeration Pond Inlet	1	5 m <sup>3</sup> /h~30 m <sup>3</sup> /h	
			Magnetic Flow Meter	
F1-03	WW, PU-08A/B Feed Pump Out.	1	0.5 m³/h~3 m³/h	
			Flow Meter	
LS-01	WW, Z-01 Waste Water Pit	1	500 mm~1,000 mm	
			Level Switch HH, H, L	
LC-01	WW, T-01 Equalization Tank	1	1,000 mm~4,500 mm	
			Level Controller	•
LI-01	WW, T-01 Equalization Tank	1	500 mm~5,500 mm	
			Level Indicator	
LS-02	WW, Z-03 Clarified Water Pond	1	1,000 mm~1,500 mm	
			Level Switch H, L	
LS-03	CHL, Z-04 Treated Water Pond	1	1,000 mm~2,000 mm	
			Level Switch H, L	
LS-04	WW, Z-06 Sludge Pond	1	500 mm~2,000 mm	
			Level Switch II, L	
LS-05	WW, Z-05 Wastewater Pond	1	500 mm~2,500 mm	
			Level Switch H.L	
				1

L.P. = Local Panel Mount

## INSTRUMENT LIST for Mansoura Co. for Resins and Chemicals

DOC. NO.	:RC-BD-L2-(2/3)	<b></b>					(2/3)
CLIENT	:Japan International Cooperation Agency	REV	1	2	3	MADE	
PROJECT	:The Study on Industrial W. W. Pollution Control	BY				СКД	
PLANT	Monsoura Co. for Resins and Chemicals	APVE	_			APVE	
WASTE W.	End of Pipe(Sanitary Waste W.+ Waste Water)	DATE				DATE	

Equipment NO.	Service	No. Req'd	Type of Equipment	Remarks
	T-09A/B Coagulant Tank	2	Tubular	
			Level Gage	<u> </u>
LG-02A/B	T-10A/B Lime Tank	2	Tubular	<u> </u>
			Level Gage	
LG-03A/B	T-11A/B Polymer-A Tank	2	Tubular	
			Level Gage	
LG-04A/B	T-12A/B Phosphate Tank	2	Tubular	· · · ·
			Level Gage	
LG-05A/B	T-13A/B Urea Tank	2	Tubular	
			Level Gage	
LG-06	T-14 Polymer-B Tank	1	Tubular	
			Level Gage	
LG-07	T-15 NaOC1 Tank	1	Tubular	
<u> </u>			Level Gage	
PI-01A/B/C	WW,PU-01A/B/C Outlet	3	Buldon Tube	
•			Pressure Indicator	
PI-02A/B	WW,PU-02A/B Outlet	2	Buldon Tube	
			Pressure Indicator	
PI-05A/B	WW, PU-05A/B Outlet	2	Diaphragm	
			Pressure Indicator	
PI-06A/B	WW, PU-06A/B Outlet	2	Diaphragm	
			Pressure Indicator	
PI-17A/B	AS, BL-OIA/B Outlet	2	Buldon Tube	

Note: C.P. = Center Panel Mount

L.P. = Local Panel Mount

INSTRUMENT LIST for Mansoura Co. for Resins and Chemicals

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DATE

CLIENT : Japan International Cooperation Agency

DOC. NO. :RC-BD-L2-(3/3)

PROJECT : The Study on Industrial W. W. Pollution Control

PLANT :Monsoura Co. for Resins and Chemicals

WASTE W. :End of Pipe(Sanitary Waste W. + Waste Water)

Equipment NO.	Service	No. Req'd	Type of Equipment	Remarks
PI-03A/B	WW,PU-03A/B Outlet	2	Buldon Tube	
			Pressure Indicattor	
PI-04A/B	WW, PU-04A/B Outlet	2	Buldon Tube	
			Pressure Indicattor	
PI-16A/B	WW,PU-16A/B Outlet	2	Buldon Tube	·
			Pressure Indicattor	·
PI-08A/B	WW, PU-08A/B Outlet	2	Diaphragm	· · · · · · · · · · · · · · · · · · ·
			Pressure Indicattor	
PI-07A/B	WW, PU-07A/B Outlet	2	Buldon Tube	
			Pressure Indicattor	•
PI-09A/B	Coagulant, PU-09A/B Outlet	2	Diaphragm	
			Pressure Indicattor	
PI-10A/B	Lime, PU-10A/B Outlet	2	Diaphragm	
			Pressure Indicattor	
PI-11A/B	Polymer, PU-11A/B Outlet	2	Diaphragm	
			Pressure Indicattor	
PI-12A/B	Phosphate, PU-12A/B Outlet	2	Diaphragm	
			Pressure Indicattor	
PI-13A/B	Urea, PU-13A/B Outlet	2	Diaphragm	
			Pressure Indicattor	
PI-14A/B	Polymer, PU-14A/B Outlet	2	Diaphragm	
			Pressure Indicattor	
PI-15A/B	NaOC1, PU-15A/B Outlet	2	Diaphragm	
			Pressure Indicattor	

L.P. = Local Panel Mount

DOC.NO.: RC-BD-LI

INDUCTION MOTOR LIST

The Study on Industrial Waste Water Plant Jupun International Cooperation Agency Monsourn Co. for Resins and Chemicals PROJECT CLIENT PI.ANT

MADG 379A CKD 3 c, APVE REV BY

	2					111	Γ												
End of Pipe (Sanitary Maste K. + Maste Mater)	USLO N. + N	US LC NOT		EIVA		u vi						Ī	ł	ŀ					
Service	No.	Type	10	Output	Speed	Revolu P	Pole	×-Φ-H2	-		lnsi	Enclose.	Cable .	Mounding	Drive	Bearing	Acc. Location		Remarks
	Required	_	Estimato	Final	Chrst	tion	r.p.m		Rating	Currrent Torque	tion							finit	
Raw Water Pump	<b>6</b>	sc	3.7		o	CW 4	1200	380-3-50	v			TEFC	-	Ŧ	-		8		-
Cosgulation Tank Food Pump	2	sc	2.2		0	CW	4-7500	380-3-50	o			TEFC		т	٥		8	_	
Filter Feed Pump	2	sc	3.7		o	CW J	1500	380-3-50	υ			TEFC		Ŧ	٥		8	_	_
Backwash Pump	2	sc	5.5		o	CW	4-7500	380-3-50	υ			TEFC		Ŧ	٥		8	_	
Siudge Pump	2	sc	1.5		v	CW 0	4-1500 3	380-3-50	v			TEFC		r	٥	-	8	_	
Return Sludge Primp	2	sc	2.2		υ	CW 6	-1500	380-3-50	c			TEFC		т	۵		8		
Backwashed Water Pump	2	sc	5.1		v	CW A	1500	380-3-50	c			TEFC		Ŧ	٥		8		
Centrifure Feed Pump	2	sc	1.5		0			380-3-50	0			TEFC		н	٥		OD		
Coasulation Pump	2	sc	0.4		υ			380-3-50	υ			TEFC		н	D		8		
Lime Pump	2	sc	0.4		υ	CW 6	4-1500 380-3-50	180-3-50	o			TEFC		Ŧ	0		8		
Polymer-A Pump	2	sc	0.4		υ	cw 4	4-1500	380-3-50	υ			TEFC		н	0		0		
Phosphete Pump	2	sc	0.4		υ		1500	380-3-50	o			TEFC		т	0		8	_	_
Ures Pump	2	sc	0.4		v	cw L	12/00	380-3-50	c			TEFC		т	σ		8		
Polymer-B Pump	2	sc	0.4		С	CW	4-1500	380-3-50	o			TEFC		x	σ		8		
NaOCI Pump	2	sc	0.4		ပ		4-1500	380-3-50	v			TEFC		Ξ	0	_	8		
Treated Water Pump	2	sc	2.2		ပ	cw L	4-1500	380-3-50	υ			TEFC		Ŧ	σ		8	0	
Blower	2	sc	37		o		4-1500	380-3-50	υ			TEFC		т	>		8		
Dehydrator (Main Motor)	-	sc	7.5		υ		1500	380-3-50	υ			TEFC		Ŧ	>		8		
Dehvdrator (Backdrive Motor)	-	sc	1.5		o	r no	1500	380-3-50	o			TEFC		н	^		00		_
Repid Mixer	-	sc	0.4		0	cw L	1500	380-3-50	0			TEFC		>	0		8		
Flocculator		sc	2.2		o	CW	4-7500	380-3-50	υ			TEFC		>	0		8	0	
Sedimentation Tank Rake	-	sc	0.4		ပ	CW	1200	380-3-50	υ			TEFC		>	U		8		
Clarifier Reke	-	sc	0.8		υ	cw	4-1500	380-3-50	υ			TEFC		>	0		8		
Thickener Reke	-	Sc	0.4		o	CW	4-1500	380-3-50	υ			TEFC		>	σ		8		
Coagulation Tank Mixor	2	sc	0.2		o	CW	4 1500	380-3-50	o			TEFC		>	σ		8		
Lime Tank Mixer	~	SC	0.2		o	CW 1	4-1500	380-3-50	c			TEFC.	-	^	0		oo	0	
Polymer-A Tank Mixer	2	sc	0.1		v	cw L	4-1500	380-3-50	υ			TEFC		>	0		8		
Phosphate Tank Mixor	2	sc	0.1		o	CW	1500	380-3-50	υ			TEFC		>	U		8		
Urea Tank Mixer	2	sc	0.4		υ	CW	/200	380-3-50	υ			TEFC		>	0	_	8		
Polymer-B Tank Mixer	2	sc	0.1		v	Ś	4-1500	380-3-50	U			TEFC		>	0	_	go		
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							•			-	-				•				-

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Notes:

: SC = Squirrel Cage. W = Wound Rotor. 1. Type

: C = Constant. M = Multi. A = Adjustable. V = Varying.

2. Speed

3. Revolution Direction : Direction when viewed from coupling side.

5. Time Rating : C = Continuouse. ST = Short Time. P = Periodic.

4. Voltage : Rated Voltage

CW = Clockwise. CCW = Counter-Clockwise.

Cable( or Wire ): T = Top. B = Bottom. S = Side. H = Hub for conduit tube or flexible tube.
 Mounting : H = Horizontal. V = Vertica!
 Drive : D = Direct. B = Belt. C = Chein. G = Geer.

: TEFC = Totally-Enclosed Fan-Cooled.

6. Enclosure

DR = Drip-Proof.

: ID = Indoor. OD = Outdoor.

10. Location

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Å		Major Activities for Implementation	y Ac on of	Selection of Demonstration Factory Commitation of Datailard Dataian Package including	- List of Materials and Equipment	- List of Construction works	Short Listing of Suppliers who can supply the Plant as a whole	Short Listing of Construction Contractors in Egypt to	be qualified by JICA	Agreement for Implementation of Phase 2 Study	between JICA and Egyptian Side Contract between JICA and Phase 2 Study Team	he P	Selection of the Plant Supplier by Competitive Bid	Design Verification and Development by Supplier	Procurement of Materials and Equipment by Supplier Monifesticies and Decembring on proceeded	Insuration and Test before Shipment		o uo	Selection of Construction Contractor by Qualification	by JICA and Study Team	Site Preparation and Temporary Facilities Installation	CIVII & DUIIDING YORKS, INCOURTING FOUNDAUOUS, CONCIENCE Define Contact Deemo 11-4-200000 - 01-2000	Basins, Control Koom, Underground Piping, etc. Shon fahrication and installation of 1 ocally procired	Tanka, Structures, Pipes, etc.	Unloading, Customa Clearance, Inland Transportation of	Imported Met'l & Eq	Roceiving, Stonng Eauismest Installation			Instrumentation		Precommissioning	Mechanical Completion Commissioning		peration of the Plar Performance Test	<b>Operation and Demonstration</b>	
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ITEM	11			BL	Demarcation	
	Yen Portion (¥1000)	LE Portion (LE)	Yen Portion (¥1000)	LE Portion (LE)	Japanese Side	Egyptian Side
1. Equipment & Materials						
(1) Machinery	50, 290					
(2) Piping Materials	10, 207					
(3) Instrument'n Eq. & Htl's	16, 950	:				
(4) Electrical Eq. & Mtl's	12, 600					
(5) Testing Eq., Etc.	3, 854	:				
1. Subtotal	93, 901	. 0	0	0	93, 901	0 ***
2. Field Construction						
(1) Steel Tanks & Vessels		481,837				
(2) Acid-Proof Lining		0				
(3) Equipment Installation		60, 500				
(4) Piping		128, 980		17, 600		- 600
(5) Foundations		75, 000				
(6) RC-made Reservoir/Structu	re	843, 750				0
(7) Road/Pavement		30, 000				
(8) Building		361, 760		2 Parameter		0
(9) Platform, Piperack		30, 000		-		0
(10) Painting		50, 000				s
(11) Electrical Works		62, 840		11, 760		- 400
(12) Instrumentation		300, 000				0.02
(13) Commissioning/Test		30, 000				0
2. Subtotal	0	2, 454, 667	0	29, 360	83, 500	1,000
Direct Cost: 1 + 2 (Eq. ¥1000)	177,	360	9	98		
3. Indirect Cost						
(1) Export Packing, Ocean Tra	13, 500				13, 500	0
(2) Import Duty, Inland Trans	portation*1	790, 000		0		26, 900
(3) Temporary Facilities*2		147,000			5,000	
(4) Subcontractor Expenses*3		613, 667			20, 900	
(5) Insurance, Social Tax*4		152,000		1,000	5, 200	0
(6) Supervisor Expenses	10,000				10,000	
3. Subtotal	23, 500	1, 702, 667	0	1,000	54, 500	
All Total: 1 + 2 + 3	117, 401	4, 157, 334	0	30, 360	231, 901	27,90
All Total (Eq. ¥1000)	117, 401	141, 400	0	1,000		
IBL/OBL Total (Eq. ¥1000)	258	,801	1,	000		
Total Cost		259	801		231,901	27,900

## Demo-Plant in Mansoula Co., Resins & Chemicals: ESTIMATE SUMMARY & DEMARCATION

\*1: (日本調達資材費+輸出梱包·海上輸送費) x25% IBL=264,500千円x25%=66,125千円=1,945,000LE OBL=9,500千円x25%=2,375千円=69,900LE

\*2 : 現地工事費x6%=6,560,000LEx0.06=393,600LE

\*3: 現地工事我x25%=6,560,000LEx0.25=1,640,000LE

\*4 : 1+2(Superviser Feeを除く) x2.7% IBL=7, 142千円(210, 000LE)+177, 000LE=3S7, 000LE OBL=257千円(7,600LE)+30,500LE=38,100LE

Costs are Demarcated to Egyptian Side.

## Unit Cost for Estimation of W.W.T. Demonstration Plant (Reference)

Factory Name:	Mansoura Co. for Resins and Chemicals.
Design Case:	Basic Design

1. Major Equipment

Equipment Name	<u>Unit Cost [x10<sup>3</sup>Yen]</u>	<u>Note</u>
(1) Acid water pumps	600	Material: SCS
(2) Clarifier Rake	10,000	1 set
(3) Sedimentation Tank rake	8,000	1 set
(4) Thickener Rake	6,000	1 set
(5) Dehydrator	6,000	3 sets
(6) Motor Control Center	13,500	
(7) Center Control Panel	3,000	1 set

2. Field Work

Work Item	<u>unit</u>	unit Cost[LE]	Note
(1) Site Preparation	$[m^2]$	8	
(2) Civil (Earth Work)	) [m <sup>3</sup> ]	34	
(3) RC Work	[m <sup>3</sup> ]	1,500	Foundation, Water Basin
(3) Storage Tank	[ton]	3,430	Equalization Tank, Chemical tank
			Neutralization Tanks
(4) Structural Steel	[ton]	2,000	Pipe rack, Operating Stage
(5) Equipment Install	ation [ton]	400	Pumps, Clarifier rakes, Dehydrator
(6) Piping	[ton]	3,970	Except valves
	[in-m]	30	Except valves
(7) Painting	[m <sup>2</sup> ]	50	
(8) Local Building	$[m^2]$	2,600	W.W.T Control Room
(9) Electrical	[cable-m]	3	

Running Cost-Mansoura Co., Resins and chemicals	o., Resin	s and che	amicals		ĥ	* Unit cost is not fixed yet	s not fixed ye		1999.11.23 T.Yasukawa
	Treating	Feeding	Consump.	Unit	Cost-1	Cost-2	Cost-3	Unit Cost	Remarks
Itoms	Capacity	Ratio		Cost					
	(m <sup>3</sup> /h)	(mg/L)	(kg/h)	(LE/kg)	(H/J)	(LE/day)	LE/year)	(LE/m <sup>3</sup> )	
1 Chemical Cost					1				
1) Alum ( Al <sub>2</sub> (SO <sub>4</sub> ) <sub>2</sub> ·18H <sub>2</sub> O )	30	30	0.9	0.3	0.27	<u>o</u>	2,138		
* 2) Lime ( Ca(OH) <sub>2</sub> )	30	20	0.6	0.1	0.06		475	0.002	
3) Polymer-A (Anionic or Cationic)	30	0.3	0.01	27	0.24	9	1,925	. 0.008	
4) Polymer-B (Anionic or Cationic)	11 kg/h	1%	0.11	27	2.97	71	23,522		
	30	110	3.3	0.6	1.98	48	15,682		
* 6) H <sub>3</sub> PO4	30	30	0.9	0.6	0.54	13	4.277	0.018	
7) NaOCI	30	4	0.9	0.385	0.35	8	2,744	0.012	
Sub-Total	-	ļ	1		6.41	154	50,763	0.214	
2 Filter Media	Loading	Loss	Loss/h						
* 1) Anthracite (3 Sets)	4.2 m <sup>3</sup>	20 %/year	0.2		0.20	5	1,584	0.007	
* 2) Sand (3 Sets)	1.8 m <sup>3</sup>	10 %/year	0.1	0.3	0.03	-	238	0.001	
* 3) Activated Carbon (1 Set)	5.0 m <sup>3</sup>	14 days	7.4	14.7	108.78	2,611	861,538	3.626	
Sub-Total	]	1	1	1	109.01	2,616	863,359	3.634	
			kWh/d	LE/kWh					
3 Power Consumption			1,244	0.12	6.22	149.23	49,248	0.207	
			m³/day	ີຍ					
4 Industrial Water or Potable Water			5	0.528	0.11	2.64	871	0.004	
		-	Person/d	LE/P/year					
5 Operator	I Person*3	Shift+1P	4	10,000	5.05	121.21	40,000	0.168	
6 Maintenance Fee	8,984,706				34.03	816.79	269,541	1.134	
(Plant Cost * 3 %/year)								,	
305,480,000/34=8,984,706 LE	-								
Total Operation Cost	1	-	1		160.83	3,859.95	1,273,782	5.36	

																															ž
	Consump.	88.80	52.80	88.80	2.75	36.00	52.80	36.00	12.00	9.60	9.60	9.60	9.60	9.60	9.60	9.60	52.80	888.00	72.00	9.60	52.80	9.60	18.00	9.60	0.04	4.80	0.02	0.02	0.08	0.02	1,554.53
	Operation	24	24	24	0.5	24	24	24	ω	24	24	24	24	24	24	24	24	24	8	24	24	24	24	24	0.2	24	0.2	0.2	0.2	0.2	1
onsumption	kW	3.7	2.2	3.7	5.5	1.5	2.2	1.5	1.5	0.4	0.4	0.4	0.4	0.4	0.4	0.4	2.2	37	6	0.4	2.2	0.4	0.75	0.4	0.2	0.2	0.1	0.1	0.4	0.1	1
ower Consul	Tag No.	PU-01	PU-02	PU-03	PU-04	PU-05	PU-06	PU-07	PU-08	PU-09	PU-10	PU-11	PU-12	PU-13	PU-14	PU-15	PU-16	B-01	MZ-01	MX-01	MX-02	MX-03	MX-04	MX-05	90-XM	MX-07	MX-08	MX-09	MX-10	MX-11	Total

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### Client: JAPAN INTERNATIONAL COOPERATION AGENCY (JICA)

Project Name: THE STUDY ON INDUSTRIAL WASTE WATER POLLUTION CONTROL IN THE ARAB REPUBLIC OF EGYPT

Factory Name:

## MANSOURA CO. FOR RESINS AND CHEMICALS

## BASIC DESIGN

Document Title:

# CALCULATION SHEET

### FOR

# W.W.T. RECOMMENDABLE PLANT

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#### 1. Object

This design calculation sheet is applied to the study of W.W.T. Recommendation Plant planning for 「Mansoura Co.for Resins and Chemicals」.

#### 2. Wastewater to be treated

- (1) Process Waste Water except Formalin Plant Regeneration Waste and Novolak Resin Solid Resin of Phenol Formaldehyde The Formalin Plant regeneration Waste and Novolak Resin Solid Resin of Phenol Formaldehyde shall be treated by boiler or incinerator.
- (2) Sanitary Waste Water
- 3. Design Conditions
  - (1) Waste management system in the Factory should be organized, and operated adequatly under the responsible managers.
  - (2) Suitable routine works, periodical maintainances should be conducted in the whole company.

#### 4. Contents of Wastewater Treating Facility

(1) Pre-treatment
(2) Primary Treatment
(3) Secondary Treatment
(4) Advanced Treatment
(5) Secondary Treatment
(6) Secondary Treatment
(7) Secondary Treatment
(8) Secondary Treatment
(9) Secondary Treatment
(1) Equalization Tank
(2) Equalization Tank
(3) Secondary Treatment
(4) Advanced Treatment
(5) Secondary Treatment
(6) Secondary Treatment
(7) Secondary Treatment
(8) Secondary Treatment
(9) Secondary Treatment
(1) Secondary Treatment
(2) Secondary Treatment
(3) Secondary Treatment
(4) Advanced Treatment
(5) Secondary Treatment

### 5. Design Basis

- 5.1 Quality and Quantity of Influent Wastewater Shown on Table-1.
- 5.2 Quality and Quantity of Treated Water

The Law 48/82 Non potable Surface Water ( Industrial) is to Basic Design. Treated water qualities are shown on Table-1.

Table - 1	Design_	Basis of Maste	ewaler Quality	and Quantity
Items		Raw Water	Treated Water	Law48/82
Flow Rate	$[m^3/h]$	$20 \sim 40$	30	
рН	[ - ]	$6 \sim 7$	6~9	6~9
SS	[mg/L]	100	< 1	< 50
BOD	[mg/L]	1,300	< 20	< 60
COD	[mg/L]	2,400	< 30	< 100
Oil&Grease	[mg/L]	20	< 1	< 10
Phenol	[mg/L]	460	< 0.005	< 0.005
TDS	[mg/L]	700	< 750	< 2,000
Water Temp.	[°C]	35~40	30~32	< 35

Table - 1 Design Basis of Wastewater Quality and Quantity

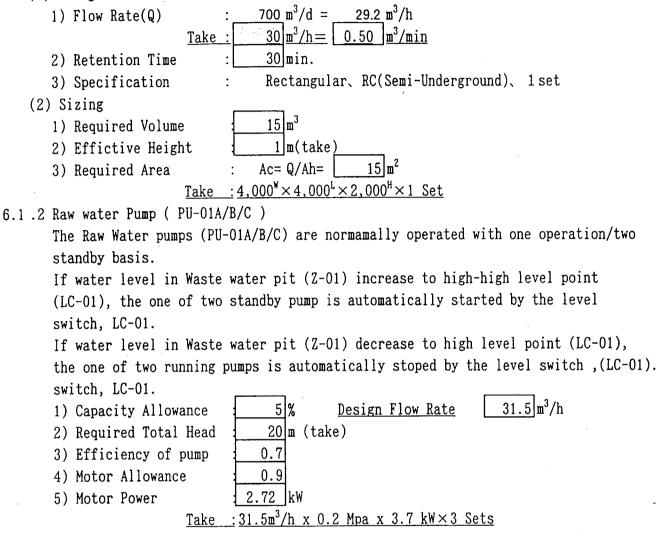
6. Unit Design

6.1 Wastewater Collection (Out of Battery)

The waste water of end of pipe is pumped to Equalization Tank.

6.1.1 Waste Water Pit ( Z-01 )

(1) Design Condition



6.2 Equalization Tank

Waste water from end of pipe is storaged in the Equalization Tank (TK-01) for equalization of waste water quantity and quality for further treatment.

6.21. Equalization Tank ( T-01 )

- (1) Design Conditions
  - 1) Quality of Wastewater: Shown on Table-2

:

:

- 2) Retention Time : 4h
- 3) Specification

Vertical cylindrical、1set

4) Others

Air bubbling device

<u>Table-</u>	<u>2 Qua</u>	<u>ntity</u> and Qua	<u>lity of Wastewater</u>
Items		Raw Water	Equalized W.
Flow Rate	$[m^3/h]$	<u>20</u> ~40	30
рH	[ - ]	$6 \sim 7$	6~7
SS	[mg/L]	100	100
BOD	[mg/L]	1,300	1,300
COD	[mg/L]	2,400	2,400
Oil&Grease	[mg/L]	20	20
Phenol	[mg/L]	460	460
TDS	[mg/L]	700	700
Water Temp.	[°C]	35~40	35 ~40

(2) Sizing

 $120 | m^3$ 1) Required Volume 2) Effictive Height 5 m(take)  $24 | m^2$ 5.53 Ac = Q/Ah =Diameter = 3) Required Area . : <u>Take : 5,811 $^{\phi} \times 6,105^{H}$ </u> ( Chiyada Standard Tank ) 4) Air Bubbling Device  $3 \text{ Nm}^3/\text{m}^2/\text{h}$ a) Required Air (design base):  $72 |Nm^3/h=|$ 1.2 Nm<sup>3</sup>/min(take) b) Required Air Quantity: 6.2 .2 Coagulation Tank Feed Pump ( PU-02A/B ) Two pumps are provided as Coagulation Tank Feed Pumps(PU-2A/B). One pump is normally in operation and the other pump is standby.  $31.5 \text{ m}^3/\text{h}$ 1) Capacity Allowance 5 % Design Flow Rate 2) Required Total Head 12 m (take) 0.7 3) Efficiency of pump 4) Motor Allowance 0.9 1.63 kW 5) Motor Power :31.5m<sup>3</sup>/h x 0.2 Mpa x 2.2 kW×2 Sets Take

#### 6.3 Chemical Clarifier

#### (1) Purpose

The function of Chemical Clarifier is to reduce Suspended Solid (SS), free oil and color of the wastewater.

(2) Design Conditions

1) Wastewater

- W.W. after equalized in T-01.
- 2) Capacity :  $30 \text{ m}^3/\text{h}$

3) Quality of In & outlet of Clarifier: Shown on Table-3.

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4) Chemicals

a) Coagulant= Al<sub>2</sub>(SO4)<sub>3</sub>

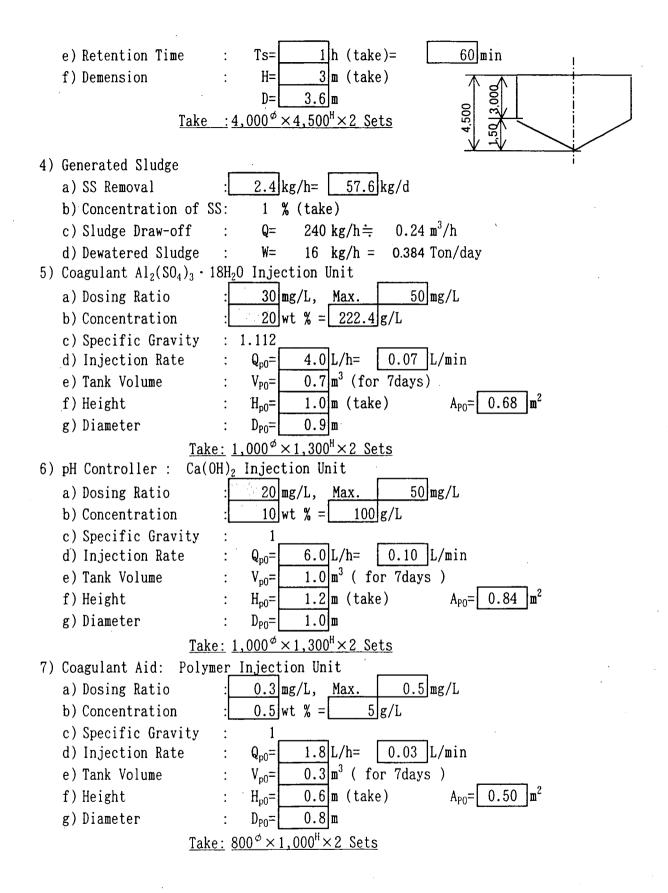
- b) pH Controller=Ca(OH)<sub>2</sub>
- c) Coagulant Aid=Polymer

Table-3 Quantity and Quality of Wastewater

Items		Equalized W.	Clarified W.
Flow Rate	[m <sup>3</sup> /h]	30	 30
рH	[ - ]	6 ~7	7.~8
SS	[mg/L]	100	 20 -
BOD	[mg/L]	1,300	1,000
COD	[mg/L]	2,400	 2,200
Oil&Grease	[mg/L]	20	 5
Phenol	[mg/L]	460	460
TDS	[mg/L]	700	750
Water Temp.	[°C]	35~40	35~40

(3) Sizing

1) Coagulation Tank (T-02) 5 min (take) a) Rapid Mixing Time  $2.5 \,\mathrm{m}^3$ V = 1b) Reruired Volume : Vertical Cylindrical, Carbon Steel with Epoxy Coating c) Specification d) Number of Required : 1 set  $1.56 \text{ m}^2$ Req'd Area= e) Demension H= 1.6 m (take) D= 1.41 m <u>Take :1,430 $^{\phi} \times 2,000^{H} \times 1$  Set</u> 2) Flocculation Tank ( T-03 ) 30 min (take) a) Slow Mixing Time  $15 \, {\rm m}^3$ V= b) Reruired Volume : Vertical Cylindrical, Carbon Steel with Epoxy Coating c) Specification d) Number of Required : 1 set  $6 | m^2$ Req'd Area = H=2.5 m (take) Demension D=| 2.76 m  $:2,860^{\phi} \times 3,000^{H} \times 1$  Set Take 3) Sedimentation Tank  $3 m^3/m^2/h$  (take) a) Surface Load Ls=  $10 \, \text{m}^2$ b) Required Area As= : Vertical Cylindrical, Carbon Steel with Epoxy Coating c) Specification d) Number of Required : 1 set



### 6.4 Biological Treating Unit (Activated Sludge Treatment)

(1) Purpose

To remove Organic Substances (BOD,COD,Phenol etc.) by aerobic micro bacterias. (2)Design Conditions

:Activated Sludge Treatment

1) Wastewater

3) Capacity

:Treated water from Chemical Clarifier

2) Treating Method

30 m<sup>3</sup>/h Shown on table-4

4) Water Quality

Table-4 Water Quality

		Table 4 Hate	
<u>Items</u>		Clarified W.	Clarified W.
Flow Rate	$[m^3/h]$	30	30
рН	[ - ]	7~8	 6~7
SS	[mg/L]	20	 20
BOD	[mg/L]	1,000	 50
СОД	[mg/L]	2,200	100
Oil&Grease	[mg/L]	5	 3
Phenol	[mg/L]	460	0.5
TDS	[mg/L]	750	750
Water Temp.	[°C]	35~40	32~35

5) Specification

a) Aeration Basin : Rectangular/Above ground, RC, 1 set

- b) Clarifier : Circular/Above ground, CS+Epoxy coating, 1 set
- 6) Chemicals

N and P are injected in case of lack of nutrient.

:

(3) Sizing

1) Aeration Basin			
a) BOD Loading	:[	0.5	<u>kg-BOD</u> /m <sup>3</sup> /day (take)
b) Volume of Basin	:	Vas=	<u>1368</u> m <sup>3</sup>
c)Height of Basin	:	Has=	5  m(take) Aas= 273.6 m <sup>2</sup>
		W=	14 W(take) L= <u>19.54</u> m
<u>Take</u>	: 1	4,000	$\times 20,000^{L} \times 5,800^{H} \times 1$ Set
d) BOD Removal	:	R <sub>bod</sub> =	684 kg/day
e) MLSS	:	Ca=	2,000 mg/L
2) Clarifier			
a) Surface Loading	:	Las=	$1 m^{3/m^2/h}(take) = 24 m^{3/m^2/day}$
b) Surface Area	:	Ass=	30 m <sup>2</sup>
c)Height of Basin	:	Hss=	<u>3</u> m (take)
d) Volume of Basin	:	Vss=	<u>90</u> m <sup>3</sup>
e) Retention Time	:	Tss=	3 h
f) Sludge Concentrati.	:	C <sub>R</sub> =	10,000 mg/L
g)Diameter	:	Dss=	<u>6.18</u> m
<u>Take</u>	<u>: 7</u>	,000¢	$\times 4,000^{H} \times 1$ Set

3) Surplus Sludge a) BOD $\rightarrow$ SS Conversin Rate 0.3 (take) b) Sludge from Act. Sludge T.:  $Ws_1 =$ 8.55 kg/h from BOD c) Sludge from Chemical Clar.: Ws<sub>2</sub>= 2.40 kg/h from SS d) Total Generated Sludge  $W_{TS} = |10.95| kg/h = |10.95|$ 262.8 kg/day f) Generated 85 % Water Cont. 73 kg/h= 1,752 kg/day W<sub>85</sub>= g) Centrifuge Feed Flow Q=  $1.5 \text{ m}^3/\text{h}$ 4) Air Requirement for Aeration  $= 519.84 \, \text{kg/day}$  $W_{02} = a * R_{BOD} + b * Sa$ a) Oxygen Demand : a= BOD Factor =  $0.55 \text{ kg} - 0_2/\text{kg} - 0_2$ b= MLVSS Factor= 0.07 Sa= 0.75\*MLSS\*Vol.of Basin/1,000= 2,052  $R_{BOD}$  = BOD Removal = 684 kg/daykg : Qair=  $(W_{02}*3.57m^3/kg-0_2*1.2)/(0.08*24*60)$ ь) Required Air  $= 19.33 \text{ Nm}^3/\text{min}$ Qta= 24.638 Nm<sup>3</sup>/min c) Blower capacity <u>Take: 25 Nm<sup>3</sup>/minx6 mHx37 kW</u> Rs = Ca/(Cr-Ca)5) Return Sludge Ratio : = 25 % 6) Nutrient as N :CO(NH<sub>2</sub>)<sub>2</sub> Injection Unit :BOD : N = 100 : 5a) Dosing Ratio BOD :  $CO(NH_2)_2 = 100 : 11$ 25 wt % b) Concentration c) Specific Gravity : 1.069 12.3 L/h d) Injection Rate  $Q_{C0} =$ :  $2.1 \,\mathrm{m^3}$  (7 days) e) Tank Volume  $V_{c0} =$ 1.8 m (take)  $A_{P0} = | 1.15 | m^2$ f) Height  $H_{n0} =$ 1.2 m g) Diameter  $D_{P0}=$ Take:  $1,200^{\phi} \times 1,800^{H} \times 2$  Sets :H<sub>3</sub>PO<sub>4</sub> Injection Unit 7) Nutrient as P :BOD : P = 100 : 1a) Dosing Ratio  $BOD : H_3PO_4 = 100 : 3$ b) Concentration 25 wt % : c) Specific Gravity 1.189 : 3.0|L/h d) Injection Rate  $Q_{\rm ph} =$  $0.5 \text{ m}^3$  ( 7days ) e) Tank Volume : V<sub>ph</sub>= 0.9 m (take)  $A_{P0} = | 0.57$ f) Height  $H_{\nu 0} =$ 0.8m  $D_{P0}=$ g) Diameter Take:  $800^{\phi} \times 1,000^{H} \times 2$  Sets

BD - 56

8) Polymer-B

- /			
	a) Dosing Ratio	:	1 % as dry SS
	b) Concentration	:	0.5 wt %
	c) Specific Gravity	:	1
	d) Injection Rate	:	$Q_{\rm ph} = 0.13  {\rm L/h}$
	e) Tank Volume	:	$V_{\rm ph} = 0.02  {\rm m}^3$ ( 7days )
	f)Height	:	$H_{p0} = 0.5 \text{ m} \text{ (take)}$
	g)Diameter	:	$D_{PO} = 0.2 m$
	Tal	<u>ke: 8</u>	$00^{\phi} \times \overline{1,000^{H} \times 1}$ Set
9)	Sludge Thickener		•
	a) Solids Loading		Lss= 60 kg/m²/d
	b) Total Solids		Lto= 262.8 kg/d
	c) Required Area	`	$Ath = 4.38 \text{ m}^2$
	d) Diameter		D <sub>P0</sub> = 2.36 m
	Tal	<u>ke: 2</u>	$400^{\phi} \times 4,000^{H} \times 1$ Set

6.5 Sand Filter Unit

(1) Purpose

To remove overflow floc(SS) from Activated Sludge Treatment

- (2) Design Conditions
  - 1) Wastewater 2) Capacity

:<u>Treated</u> Water from Biological Treatment Unit 30 m<sup>3</sup>/h

 $A_{P0} = 0.04 \text{ m}^2$ 

3) Water Quality

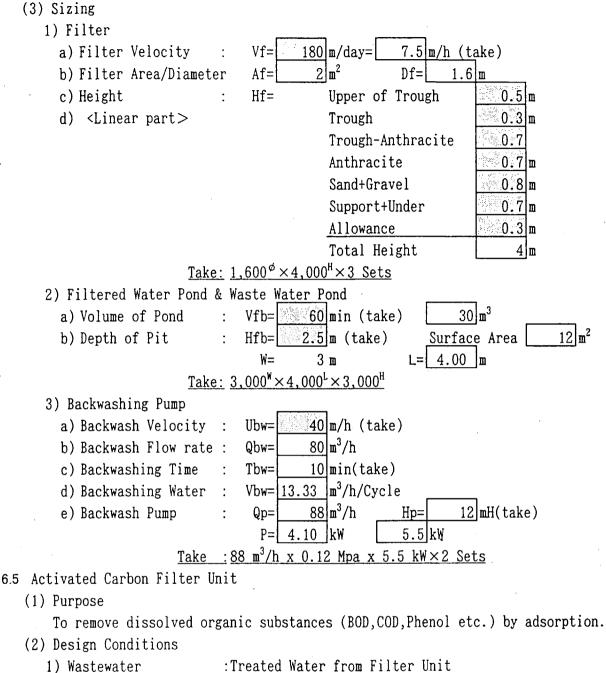
:Show on Table-5

	<u> </u>	Table-5	<u>6 Water Quali</u>	ty
Items		Biological T.		Filtered W.
Flow Rate	[m <sup>3</sup> /h]	30		30
рH	[ - ]	7~8		6~7
SS	[mg/L]	20	,	5
BOD	[mg/L]	1,000		30
COD	[mg/L]	2,200		80
Oil&Grease	[mg/L]	5		2
Phenol	[mg/L]	0.5		0.5
TDS	[mg/L]	750		750
Water Temp.	[°C]	35~40		32~35

4) Specification

:Vertical Cylindrical, Carbon Steel with Epoxy Coating, Pressure Type

- 5) No. of Filter :3 Sets (2 Operatio + 1 Stand-by)
- 6) Filter Media :Anthracite + Sand/Gravel 7) Backwashing
  - : Water (Pump)



- $30 \text{ m}^3/\text{h}$ 2) Capacity
- 3) Water Quality

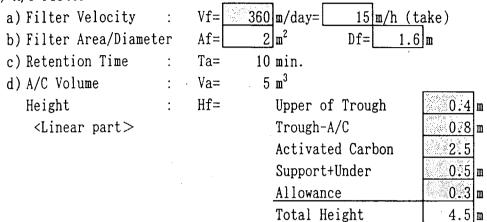
:Show on Table-6

		Table-6	<u>6 Water Quali</u>	ity
<u>Items</u>		Filtered W.		Treated Water
Flow Rate	[m <sup>3</sup> /h]	30		30
рH	[ - ]	$6 \sim 7$		6~9
SS	[mg/L]	5	<u></u>	1
BOD	[mg/L]	30		20
COD	[mg/L]	80		30
Oil&Grease	[mg/L]	2		1
Phenol	[mg/L]	0.5		0.005
TDS	[mg/L]	750		750
Water Temp.	[°C]	32~35		$32 \sim 35$

4) specification

5) No. of Filter

- :Vertical Cylindrical,Carbon Steel with Epoxy Coating, Pressure Type
- :2 Sets (1 Operatio + 1 Stand-by)
- 6) Filter Media :Activated Carbon
- 7) Backwashing : Water (Pump)
- (3) Sizing
  - 1) A/C Filter



Take:  $1,600^{\phi} \times 4,500^{H} \times 2$  Sets

#### 6.6 Sterilization

(1) Purpose

To sterilize treated water including sanitary wastewater

(2) Design Condition

