Appendix 12.3 Pumping Station - Capacity Calculation

1. Pumping Facility

Alternative	1	Alternative 1				Alternative 2		
Area	·····	Kandy			Ka	Katugastota		
Pump Station		P/S 1	P/S 2-1	P/S 2-2	STP	P/S 1	STP	P/S 1
	m3/sec	0.01220	0.02900	0.02900	0.30000	0.00700	0.27333	0.02900
P/S Flow	m3/min	0.732	1.740	1.740	18.000	0.420	16.400	1,740
P/S Type		Circular	Circular	Circular	Rectangular	Circular	Rectangular	Circular
Number (+1)-standby		1(+1)	1(+1)	1(+1)	2(+1)	1(+1)	2(+1)	1(+1)
Capacity	m3/min	0.74	1.74	1.74	9.00	0.42	8.20	1.74
Head	m	9	48	48	12	14	14	
h1 =	m	7.00	40.00	40.00	10.00	7.00	10.00	15.00
h2 =	m	0.2	26.99	26.99	0.25	6,51	0.29	and the second s
D ==	mm	250	150	150	600	100	450	
L=	m	630	1,400	1,400	150	650	50	and the second s
V =	m/sec	0.249	1.641	1.641	1.061	0.891	1.719	0.923
h3 =	m	1.50	1.50	1.50	1.50	1.50	1.50	1.50
Diameter	mm	79	122	122	392	- 60	374	
Diameter	mm	150	125	125	400	150	400	125
Motor Output	kW	2.1	26.1	26.1	33.7	1.8		the second se
Motor Output	kW	2.2	30	30	37	2.2	37	11

2. Pump Pit (Circular)

Alternative		Alternative 1	Alternative 2			
Area		Kandy	Katugastota	Kandy		
Pump Station		P/S 1-1	P/S 1-2	P/S 2	P/S 1	P/S 2
	m3/sec	0.02900	0.02900	0.01220	0.02900	0.01220
P/S Flow	m3/min	1.740	1.740	0.732	1.740	0.732
P/S Type		Circular	Circular	Circular	Circular	Circular
Number (+1)-standby		1(+1)	1(+1)	1(+1)	1(+1)	1(+1)
Capacity	m3/min	1.74	1.74	0,74	1.74	0.74
Pump Minimum Starting Period	min	15	15	8	8	8
Pump Pit Capacity	cu.m	6,53	6.53	1.48	3.48	1.48
Therefore	cu.m	7.00	7.00	2.00	4.00	2.00
Ground Level	m	0.00	0.00	0.00	0.00	0.00
Inlet Pipe Level	m	-4.00	-4.00	-4,00	-4.00	-4.00
Effective Depth	m.	1.00	1.00	1.00	1.00	1.00
Тор	m	0.50	0.50	0.50	0.50	0.50
Bottom	m	0.50	0.50	0.50	0.50	0.50
Required Area	sq.m	7.00	7.00	2.00	4.00	2.00
Diameter	m	2.99	2.99	1.60	2.26	1.60
Therefore	m	3.00	3.00	1.60	2.50	1.60
Dimension (DIA)	m	3.00	3.00	1.60	2.50	1.60
(D)	m	6.00	6.00	6.00	6.00	6.00
Retention Time	min	4,06	4.06	2.75	2.82	2.75

3. Pump Pit (Rectangular)

Alternative	Alter 1	Alter 2	
Area	Kandy	Kandy	
Pump Station	STP	STP	
P/S Flow	m3/sec	0.29570	0.26670
1/3 Flow	m3/min	17.742	16.002
P/S Type		Rectangular	Rectangular
Number (+1)-standby		3(+1)	3(+1)
Capacity	m3/min	5.92	5.34
Pump Minimum Starting Period	min	15	15
Pump Pit Capacity	cu.m	22.20	20.03
Therefore	cu.m	24.00	22.00
Ground Level	m	0.00	0.00
Inlet Pipe Level	m	-4.00	-4.00
Effective Depth	m	0.80	0.80
Тор	m	0.50	0.50
Bottom	m	0.70	0.70
Required Area	sq.m	30.00	27.50
Width	m	7.00	7.00
Length	m	4.29	3.93
Therefore	m	4.90	4.90
Dimension (W	m	7.00	7.00
(L)	m	4.90	4.90
(D)	m	6.00	6,00
Retention Time	min	9.47	10.50

Sewage Treatment Plant – Capacity Calculation

Appendix 12.4.1 Alternative 1 – Kandy (Oxidation Ditch)

Appendix 12.4.2 Alternative 2 – Kandy (Oxidation Ditch)

Appendix 12.4.3

Alternative 2 – Katugastota (Dual Power Aerated Lagoon)

Appendix 12.4.1 Sewage Treatment Plant - Capacity Calculation

CAPACITY CALCULATION OF FACILITIES Alternative 1 - Kandy (Oxidation Ditch)

1 BASIC CONDITIONS

1-1 BASIC ITEMS

(1) Name : Kandy Sewage Treatment Plant

(2) Land Area :	Approximately		3.00	ha
(3) Elevation :	474.000	m		
(4) Inlet Pipe Level :	465.883	m	·	
(5) Pipe Diameter :	600	m		
(6) Land Use :	-			
(7) Collection System :	Seperate Type			
(8) Treatment Method :	Sewage Treatm Sludge Treatme			itch Method kener, Drying Bed
(9) Effluent Point :	Mada Ela River	r		
(10) Effluent Point Water I	evel :	. 4	70.64	0 m
(11) Target Year :	Year 2005 (Pha	se 1), Year	2015	(Phase 2)

(12) Lowest Monthly Average Temperature 23.6 °C (January)

1-2 Design Population

Design Population : 55,000 Persons (Total)

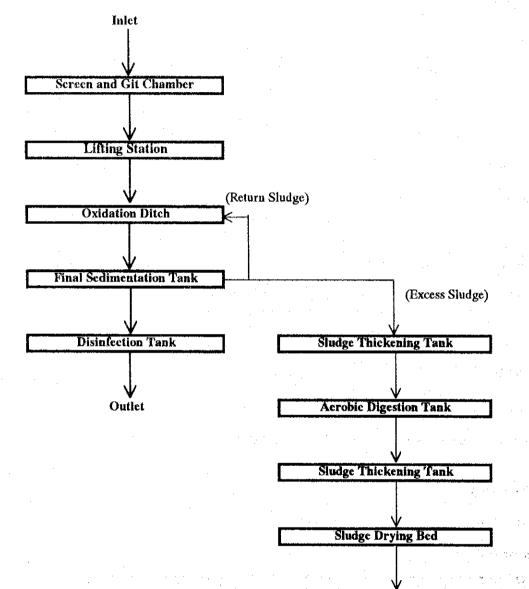
1-3 Design Sewage Flow

ITEM	m3/day	m3/hr	m3/min	m3/sec
Daily Average	15,220	634.2	10.57	0.176
Daily Maximum	18,000	750.0	12.50	0.208
Hourly Maximum	25,540	1064.2	17.74	0.296

1-4 Design Sewage Quality

I	ITEM	INFLUENT	EFFLUENT	REMOVAL	REMARKS
		(mg/L)	(mg/L)	RATIO (%)	
	BOD	240	30	88	
	SS	250	50	80	

1-5 Flow Chart (Oxidation Ditch)



Composting/Disposal

1-6 Design Criteria for Oxidation Ditch

ITEMS	UNIT	Formula or Value	Application
1-6-1 Grit Chamber			
 Water Surface Load Average Velocity 	m3/m2/sec	< 1800	1,800
	m/sec	< 0.3	0.3
1-6-2 Oxidation Ditch			
 BOD-SS Load MLSS Concentration Return Sludge Ratio Water Depth Width Retention Time Oxygen Requirement Sludge Age 	kg/kg/day mg/l % m m hour kgO2/kgBOD day	$\begin{array}{c} 0.03 - 0.05 \\ 3,000 - 4,000 \\ 100 - 200 \\ 1.0 - 3.0 \\ 2.0 - 6.0 \\ 24 - 48 \\ 1.4 - 2.2 \\ 8 - 50 \end{array}$	0.05 4,000 150 Same as Left Same as Left Same as Left 2.0 Same as Left
 1-6-3 Final Sedimentation Tank (1) Water Surface Load (2) Retention Time (3) Water Depth 	m3/m2/day	8 - 12	8 - 12
	hour	6.0 - 12.0	Same as Left
	m	3.0 - 4.0	3.0
1-6-4 Disinfection Tank(1) Retention Time(2) Dosage	min.	> 15	15
	mg/l	2.0 - 4.0	3.0
 1-6-5 Sludge Thickening Tank (1) Solid Matter Load (2) Water Depth 	kg/m2/day	60 - 90	70
	m	Approximately 4.0	4.0
 1-6-6 Aerobic Digestion Tank (1) Retention Time (2) Solid Matter Load 	day	10.0 - 15.0	Same as Left
	kg/m2/day	1.60 - 4.81	Same as Left
1-6-7 Sludge Drying Bed(1) Drying Period(2) Depth of Bed	day	15 - 30	20
	m	0.3 - 1.0	0.3

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2 CAPACITY CALCULATION

2-1 Grit Chamber and Screen (Hourly Maximum)

ITEM		SIGN	UNIT	CALCULATION	RESULT
Туре		-		Parallel Flow Type	
Design Flow		Q1	m3/day		25,540
		Q2	m3/sec	-	0.30
Water Surface Load		WSL	m3/m2/day	-	1,800
Required Surface Area	a	RSA	m2	Q1/WSL	14.189
Basin Number (Total)		BN	basin	-	6
Basin Number (Stand-	-By)	BNS	basin	. —	2
Average Velocity		V	m/sec	~	0.30
Depth		H	m		0.80
Width		W1	m	Q2/(V*H)	1.232
	Therefore	W2	m		1:20
Length		L1	m	RSA/W2/(BN-BNS)	2.956
· ·	Therefore	L2	m		2.70
Dimension	(W)	W V	m	W2	1.20
	(L)	L	m	L2	2.70
	(Basin)		basin	BN	4
	(Stand-By)	-	stand-by	BNS	2
Screen Type	/	_ · · ·		Fine Bar Screen	
Screen Set Number		SSN	set	BN	6
Check			UNIT	APPLICATION	RESULT
Water Surface Load			m3/m2/day	< 1800	1,971
Average Velocity			m/sec	< 0.3	0.08

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2-2 Oxidation Ditch (Daily Maximum)

ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре	-	-	Re-circulation Flow Type	****
Design Flow	Q1	m3/day		18,000
	Q2	m3/hr		750.0
Basin Number	BN	Basin	-	6
Inlet BOD Quality	С	mg/L	-	240
Inlet SS Quality	S	mg/L		250
Inlet BOD Matter	М	kg/day	Q1*C*10^-3	4,320
BOD-SS Load	BS	kg/kg/day	· -	0.05
MLSS Concentration	SS	mg/L	-	4,000
Required Volume	V 1	m3	M/(SS*BS*10^-3)	21,600
Therefore	V2	m3	-	21,600
Retention Time	Т	br	(V2/Q1)*24	28.8
Return Sludge Ratio	R1	%		150
	R2	-	R1/100	1.5
Return Sludge Quality	RS1	mg/L	(SS*(1+R2)-C)/R2	6,507
Therefore	RS2	mg/L	-	6,510
Sludge Åge	SA	day	SS*V2/(Q1*S)	19.2
Width	W	m	-	6.0
Water Depth	Н	m	-	3.0
Length	L1	m	(V2/BN)/(W*H)	200.0
Therefore	L2	m	-	200.0
Dimension (Width)	W	m	W	6.0
(Depth)	H	m	Н	3.0
(Length)	L	m	L2	200.0
(Basin Number)		basin	BN	6
Required Oxygen	O2-day	kgO2/day	Q1*C*10^-3*2.0	8,640.0
	O2-hr	kgO2/br	(O2-day)/24	360,0
Aerator Motor Output	~	kW	O2-hr/1.9	189.5
	-	kW		180.0
Aerator Type		-	Slanting Shaft Screw Aerator	
Check		UNIT	APPLICATION	RESULT
Retention Time		hour	24 - 48	28.8
Oxygen Supply		kgO2/kg	1.4 - 2.2	2.0
Sludge Age		day	8 - 50	19.2

(0)

ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре		-	Radial Flow Circular Type	
Design Flow	Q1	m3/day		18,000
Ŭ	Q2	m3/sec	_	750.00
Basin Number	BN	Basin	-	6
Water Surface Load	L	m3/m2/day	4.14*10^4*T^0.95*SS^-1.35	11.4
Therefore	L	m3/m2/day		
Required Surface Area	A1	m2	Q1/L	1500.0
-	A2	m2/Basin	A1/BN	250.0
Water Depth	Н	m	-	3.0
Diameter	D1	m	(A2/3.14)^0.5*2	17.8
Therefore	D2	. m		18.0
Dimension (Dian	D	m	D2	18.0
(Depth)	H	m	Н	3.0
(Basin Number)	-	Basin	BN	6
Sludge Collector Type	۰.	-	Central Drive Type	
Check		UNIT	APPLICATION	RESULT
Water Surface Load		m3/m2/day	8 - 12	11.8
Retention Time		hour	6.0 - 12.0	5.1

2-3 Final Sedimentation Tank (Daily Maximum)

2-4 Disinfection Tank (Daily Maximum)

ITEM		SIGN	UNIT	CALCULATION	RESULT
Chemical Type		-	-	Chlorination Type	
Design Flow		Q1	m3/day	-	18,000
		Q2	m3/min	-	12.50
Retention Time		T	min.		15.0
Basin Number	T	BN	basin	-	2
Required Volume		v	m3	Q2*T	94
Width		W	m		3.00
Water Depth		Н	m	-	1.50
Length		L1	m	V/(W*H)	20.833
	therefore	L2	m	-	21:00
Dosage	,	D	mg/L		3.0
Required Chemical		RC1	kg/day	Q1*D*10^-3/C	54.00
_	Therefore	RC2	kg/hr	RC1/24	2.25
Dimension	(W)	W	m	W	3.0
	(Length)	L	m	1.2	21.0
	(Depth)	H	m	H	1.5
· .	(Basin)	BN	basin		2
Chlorine Feeder		_	unit	including 1 for stand-by	
Check			UNIT	APPLICATION	RESULT
Retention Time			min.	15	15.1

Т

2-5 Sludge Thickening Tank (Daily Maximum)

ITEM		SIGN	UNIT	CALCULATION	RESULT
Туре	T	-	-	Radial Flow Circular Type	
Design Flow		Q1	m3/day	-	18,000
	Г	Q2	m3/hr		634.2
Basin Number		BN	Basin	-	2
Inlet SS Quality		С	mg/L `		250
Removal Ratio		R1	%	_ .	80
		R2	- 1	R1/100	0.80
Sludge Generation Ratio		SG1	%	-	75
(Oxidation Ditch)	Γ	SG2	-	SG1/100	0.75
Inlet SS Matter		М	kg/day	Q1*C*R2*SG2*10^-3	2,700
Solid Matter Load		L	kg/m2/day	-	70.0
Required Surface Area		Al	m2	M/L	38.6
		A2	m2/Basin	A1/BN	19.3
Water Depth		H	m	-	4.0
Diameter		D1	m	(A2/3.14)^0.5*2	5.0
T	herefore	D2	m	-	5.0
Dimension		D	m	D2	5.0
	(Depth)	Н	m	Н	4.0
	(Basin)	Basin	Basin	BN	2
Check			UNIT	APPLICATION	RESULT
Solid Matter Load	T		kg/m2/day	70	68.8

2-6 Aerobic Sludge Digestion Tank (Daily Maximum)

ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре	· · ·	-	Circular Type	
Basin Number	BN	Basin		2
Design Flow	Q1	m3/day		18,000
Inlet SS Matter	M	kg/day		2,700
Moisture Content	G	%	-	97.5
Sludge Volume	V1	m3/day	M*100/(100-G)	108.0
Temperature - Summer	TS	°C	-	26.5
- Winter	TW	°C	-	23.6
Temperature - Sludge Age	TSA	day-°C	VolatileSolidReduction=40%	470
Sludge Age	SA	day	TSA/TS	19.9
Total Mass of VSS	VSS	kg/day	0.8*M	2,160
VSS Reduction - Summer (41%)	VRS	kg/day	VSS*0.4	864.0
- Winter (40%)	VRW	kg/day	VSS*0.41	885.6
Required Volume	V	m3	V1/0.7/(0.125*0.8+1/SA)	514
Water Depth	Н	m		4.0
Diameter	D1	m	(A2/3.14)^0.5*2	12.8
Therefore	D2	: m	-	13.0
Dimension	• D	m	D2	13.0
(Depth)	Н	m	Н	4.0
(Basin)	Basin	Basin	BN	2
Required Oxygen	RO	kgO2/day	2.3*VRS	1987.2
Required Air	RA	kg-Air/br	RO/(0.1*0.233*1.293)/1440	2,748.4
Check		UNIT	APPLICATION	RESULT
Retention Time		day	10.0 - 15.0	4.9
Solid Matter Load	• • • • • •	kg/m3/day	1.60 - 4.81	10.2

ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре	-	-	Radial Flow Circular Type	
Basin Number	BN	Basin	-	2
Inlet SS Matter to Digestion	M1	kg/day		2,700
Removal Ratio at Digestion	R1	%	-	40%
Inlet SS Matter	M2	kg/day	M1*(1-R1)	1620
Moisture Content	G	%	-	
Sludge Volume	V1	m3/day	M2*100/(100-G)	162.0
Solid Matter Load	L	kg/m2/day	_	70,0
Required Surface Area	A1	m2	M/L	23.1
· · ·	A2	m2/Basin	A1/BN	11.6
Water Depth	H	m		4.0
Diameter	D1	m	(A2/3.14)^0.5*2	3.8
Therefore	D2	m	• 1	5.0
Dimension	D	m	D2	5.0
(Depth)	Н	m	H	4.0
(Basin)	Basin	Basin	BN	2
Check		UNIT	APPLICATION	RESULT
Solid Matter Load		kg/m2/day	70	41.3

2-7 Sludge Thickening Tank (Daily Maximum)

2-8 Sludge Drying Bed (Daily Maxmum)

ITEM		SIGN	UNIT	CALCULATION	RESULT
				CALCULATION	
Design Flow		Q1	m3/day	-	18,000
Inlet SS Matter	1	M1	kg/day	Q1*C*R2*10^-3	1,620
	· f	M2	t/day	M1/1000	1.62
Moisture Content		G	%	-	97.0
Sludge Volume		V1	m3/day	M2*100/(100-G)	54.0
Drying Period		P.	day		10
Required Volume		V2	m3/day	V1*P	540.0
Depth of Bed		Η	m	-	0.3
Required Area		A	m2	V2/H	1,800
Unit Number		UN	Unit		20
Width per Unit		W	m		6.0
Length per Unit		L1	m.	A/(UN*W)	15.0
	Therefore	L2	m		15.0
Dimension	(Width	W	m	W	6.0
	(Length)	L	m	L2	15.0
· · · ·	(Depth)	H	• m	H	0.3
	(Basin)	Basin	Basin	BN	20.0
Check	· · · · · · · · · · · · · · · · · · ·		UNIT	APPLICATION	RESULT
Drying Period			day	20	10.0

Appendix 12.4.2 Sewage Treatment Plant - Capacity Calculation

CAPACITY CALCULATION OF FACILITIES Alternative 2 - Kandy (Oxidation Ditch)

3.00 ha

BASIC CONDITIONS 1

BASIC ITEMS 1-1

þ

Kandy Sewage Treatment Plant (1) Name :

(2) Land Area	:	Approximately	
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(3) Elevation 474.000 m :

(4) Inlet Pipe Level : 465.883 m

(5) Pipe Diameter : 600

(6) Land Use :

- Seperate Type (7) Collection System :
- Sewage Treatment : Oxidation Ditch Method (8) Treatment Method : Sludge Treatment : Sludge Thickener, Drying Bed

m

- Mada Ela River (9) Effluent Point :
- 470.640 m (10) Effluent Point Water Level :
- Year 2005 (Phase 1), Year 2015 (Phase 2) (11) Target Year
- 23.6 °C (January) (12) Lowest Monthly Average Temperature

1-2 Design Population

49,700 Persons (Total) **Design Population** :

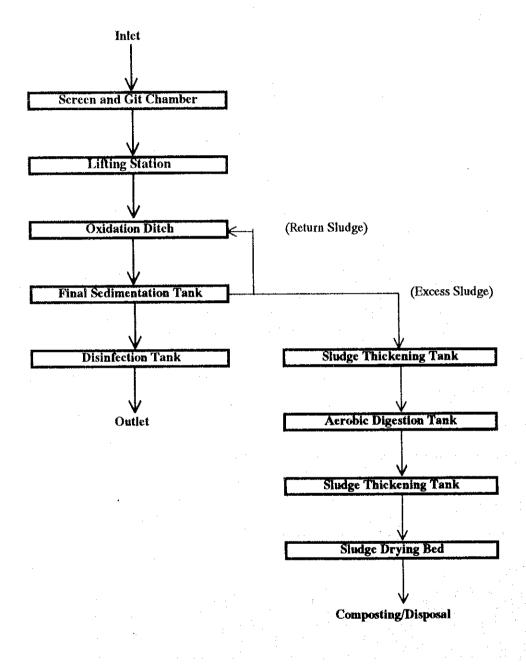
Design Sewage Flow 1-3

ITEM	m3/day	m3/hr	m3/min	m3/sec
Daily Average	13,700	570.8	9.51	0.159
Daily Maximum	17,000	708.3	11.81	0.197
Hourly Maximum	23,030	959.6	15.99	0.267

Design Sewage Quality 1-4

ITEM	INFLUENT	EFFLUENT	REMOVAL	REMARKS
	(mg/L)	(mg/L)	RATIO (%)	
BOD	240	30	88	
SS	250	50	80	

1-5 Flow Chart (Oxidation Ditch)



A-12.4-10

1-6 Design Criteria for Oxidation Ditch

ITEMS	UNIT	Formula or Value	Application
1-6-1 Grit Chamber			
(1) Water Surface Load	m3/m2/sec	< 1800	1,800
(2) Average Velocity	m/sec	< 0.3	0.3
1-6-2 Oxidation Ditch			
(1) BOD-SS Load	kg/kg/day	0.03 - 0.05	0.05
(2) MLSS Concentration	mg/l	3,000 - 4,000	4,000
(3) Return Sludge Ratio	%	100 - 200	150
(4) Water Depth	m	1.0 - 3.0	Same as Left
(5) Width	m	2.0 - 6.0	Same as Left
(6) Retention Time	hour	24 -48	Same as Left
(6) Oxygen Requirement	kgO2/kgBOD	1.4 - 2.2	2.0
(7) Shudge Age	day	8 - 50	Same as Left
1-6-3 Final Sedimentation Tank			
			•
(1) Water Surface Load	m3/m2/day	8 - 12	8 - 12
(2) Retention Time	hour	6.0 - 12.0	Same as Left
(3) Water Depth	m	3.0 - 4.0	3.0
1-6-4 Disinfection Tank			
(1) Retention Time	min.	> 15	15
(2) Dosage	mg/l	2.0 - 4.0	3.0
1-6-5 Sludge Thickening Tank			
(1) Solid Matter Load	kg/m2/day	60 - 90	70
(2) Water Depth	m	Approximately 4.0	4.0
1-6-6 Aerobic Digestion Tank			
1			
(1) Retention Time	day	10.0 - 15.0	Same as Left
(2) Solid Matter Load	kg/m2/day	1.60 - 4.81	Same as Left
			L
1-6-7 Sludge Drying Bed			· ·
			ļ
(1) Drying Period	day	15 - 30	20
(2) Depth of Bed	m	0.3 - 1.0	0.3

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2 CAPACITY CALCULATION

UNIT CALCULATION RESULT **ITEM** SIGN Parallel Flow Type: Туре Q1 23,030 Design Flow m3/day _ 0.27 Q2 m3/sec _ 1,800 Water Surface Load WSL m3/m2/day _ Q1/WSL 12.794 RSA **Required Surface Area** m^2 Basin Number (Total) BN basin -6 BNS Basin Number (Stand-By) basin 1 0.30 Average Velocity V m/sec -Н 0.80 Depth m -Q2/(V*H) 1.111 Width W1 m :1.20 Therefore W2 m RSA/W2/(BN-BNS) 2.666 Length L1 m 2:70 Therefore L2 נח . $\overline{W2}$ 1.20 Dimension (W Ŵ m L L2 2.70 (L) m BN (Basin) basin 4 (Stand-By) stand-by BNS 2 -Screen Type Fine Bar Screen -SSN Screen Set Number BN 6 set APPLICATION RESULT UNIT Check 1,777 Water Surface Load m3/m2/day < 1800 < 0.3 0.07 Average Velocity m/sec

2-1 Grit Chamber and Screen (Hourly Maximum)

2-2 Oxidation Ditch (Daily Maximum)

ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре	- ·	~	Re-circulation Flow Type	
Design Flow	Q1	m3/day		17,000
Ç	Q2	m3/hr	· · · · · · · · · · · · · · · · · · ·	708.3
Basin Number	BN	Basin	_	6
Inlet BOD Quality	С	mg/L		240
Inlet SS Quality	S	mg/L	-	250
Inlet BOD Matter	M	kg/day	Q1*C*10^-3	4,080
BOD-SS Load	BS	kg/kg/day	-	0.05
MLSS Concentration	SS	mg/L	-	4,000
Required Volume	V1	m3	M/(SS*BS*10^-3)	20,400
Therefore	V2	m3 .	-	20,400
Retention Time	Т	hr	(V2/Q1)*24	28.8
Return Sludge Ratio	R1	%		150
	R2	~	R1/100	1.5
Return Sludge Quality	RS1	mg/L	(SS*(1+R2)-C)/R2	6,507
Therefore	RS2	mg/L	-	6,510
Sludge Age	SA	day	SS*V2/(Q1*S)	19.2
Width	W	m	~	6.0
Water Depth	Н	m	-	3.0
Length	L1	m	(V2/BN)/(W*H)	188.9
Therefore	L2	m	*	190.0
Dimension (Width)	W	m	W	6.0
(Depth)	Н	m	H	3.0
(Length)	L	m	L2	190.0
(Basin Number)	_	basin	BN	6
Required Oxygen	O2-day	kgO2/day	Q1*C*10^-3*2.0	8,160.0
	O2-hr	kgO2/hr	(O2-day)/24	340.0
Aerator Motor Output	- .	kW	O2-hr/1.9	178.9
	-	kW	-	180.0
Aerator Type	-	-	Slanting Shaft Screw Aerator	
Check	<u> </u>	UNIT	APPLICATION	RESULT
Retention Time		hour	24 -48	29.0
Oxygen Supply		kgO2/kg	1.4 - 2.2	2.0
Sludge Age		day	8 - 50	19.2

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ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре	-	-	Radial Flow Circular Type	
Design Flow	Q1	m3/day		17,000
	Q2	m3/sec	-	708.33
Basin Number	BN	Basin		6
Water Surface Load	L	m3/m2/day	4.14*10^4*'I^0.95*SS^-1.35	11.4
Therefore	L	m3/m2/day		12:0
Required Surface Area	A1	m2	Q1/L	1416.7
	A2	m2/Basin	A1/BN	236.1
Water Depth	H	m	-	3.0
Diameter	D1	m	(A2/3.14)^0.5*2	17.3
Therefore	D2	m	-	16.0
Dimension (Diar	D	m	D2	16.0
(Depth)	Н	m	Н	3.0
(Basin Number)		Basin	BN	6
Sludge Collector Type	-		Central Drive Type	
Check		UNIT	APPLICATION	RESULT
Water Surface Load		m3/m2/day	8 - 12	14.1
Retention Time		hour	6.0 - 12.0	4.3

2-3 Final Sedimentation Tank (Daily Maximum)

2-4 Disinfection Tank (Daily Maximum)

ITEM		SIGN	UNIT	CALCULATION	RESULT
Chemical Type		-		Chlorination Type	
Design Flow		Q1	m3/day		17,000
		Q2	m3/min	-	11.81
Retention Time		Т	min.	-	15.0
Basin Number		BN	basin		2
Required Volume		V	m3	Q2*T	89
Width		W	m	-	3.00
Water Depth		Н	m	-	1.50
Length		Li	m	V/(W*H)	19.676
	therefore	L2	m		20.00
Dosage		D	mg/L	-	3.0
Required Chemical		RC1	kg/day	Q1*D*10^-3/C	51.00
	Therefore	RC2	kg/hr	RC1/24	2.13
Dimension	(W	W	m	W	3.0
	(Length)	L	m	1.2	20.0
	(Depth)	Н	m	Н	1.5
	(Basin)	BN	basin	-	2
Chlorine Feeder		-	unit	including 1 for stand-by	3
Check	N		UNIT	APPLICATION	RESULT
Retention Time			min.	15	15.2

2-5 Sludge Thickening Tank (Daily Maximum)

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ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре		**	Radial Flow Circular Type	
Design Flow	Q1	m3/day	-	17,000
-	Q2	m3/hr	-	570.8
Basin Number	BN	Basin	-	2
Inlet SS Quality	С	mg/L	~	250
Removal Ratio	R1	%	-	80
	R2	· _	R1/100	0.80
Sludge Generation Ratio	SG1	%	-	75
(Oxidation Ditch)	SG2		SG1/100	0.75
Inlet SS Matter	М	kg/day	Q1*C*R2*SG2*10^-3	2,550
Solid Matter Load	L	kg/m2/day	· -	70.0
Required Surface Area	A1	m2	M/L	36.4
	A2	m2/Basin	A1/BN	18.2
Water Depth	H	m		4.0
Diameter	D1	m	(A2/3.14)*0.5*2	4.8
Therefore	D2	m	-	5.0
Dimension	D	m	D2	5.0
(Depth)	Н	m	Н	4.0
(Basin)	Basin	Basin	BN	2
Check		UNIT	APPLICATION	RESULT
Solid Matter Load		kg/m2/day	70	65.0

2-6 Aerobic Sludge Digestion Tank (Daily Maximum)

ITEM	SIGN	UNIT	CALCULATION	RESULT
Гуре	· ·	-	Circular Type	
Basin Number	BN	Basin	-	2
Design Flow	Q1	m3/day	-	17,000
Inlet SS Matter	M	kg/day	-	2,550
Moisture Content	G	%	-	97.5
Sludge Volume	V 1	m3/day	M*100/(100-G)	102.0
Temperature - Summer	TS	°C	-	26.5
- Winter	TW	°C	•	23.6
Temperature - Sludge Age	TSA	day- C	VolatileSolidReduction=40%	470
Sludge Age	SA	day	TSA/TS	19.9
Total Mass of VSS	VSS	kg/day	0.8*M	2,040
VSS Reduction - Summer (41%)	VRS	kg/day	VSS*0.4	816.0
- Winter (40%)	VRW	kg/day	VSS*0.41	836.4
Required Volume	V	m3	V1/0.7/(0.125*0.8+1/SA)	485
Water Depth	H	. m		4.(
Diameter	D1	m	(A2/3.14)^0.5*2	12:4
Therefore	D2	m	-	13.0
Dimension	D	m	D2	13.0
(Depth)	Н	m	Н	4.0
(Basin)	Basin	Basin	BN	
	RO	kgO2/day	2.3*VRS	1876.8
Required Oxygen Required Air	RA	kg-Air/hr	RO/(0.1*0.233*1.293)/1440	2,595.7
Check		UNIT	APPLICATION	RESULT
Retention Time		day	10.0 - 15.0	5.
Solid Matter Load		kg/m3/day	1.60 - 4.81	9.

A-12.4-15

ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре	-	-	Radial Flow Circular Type	
Basin Number	BN	Basin		2
Inlet SS Matter to Digestion	M 1	kg/day		2,550
Removal Ratio at Digestion	R1	%		40%
Inlet SS Matter	M2	kg/day	M1*(1-R1)	1530
Moisture Content	G	%		99.0
Sludge Volume	Vi	m3/day	M2*100/(100-G)	153.0
Solid Matter Load	L	kg/m2/day	-	70.0
Required Surface Area	Al	m2	M/L	21.9
	A2 -	m2/Basin	A1/BN	10.9
Water Depth	Н	m ·		4.0
Diameter	D1 .	m	(A2/3.14)^0.5*2	3.7
Therefore	D2	m	-	5.0
Dimension	D	m	D2	5.0
(Depth)	Н	m	H	4.0
(Basin)	Basin	Basin	BN	2
Check		UNIT	APPLICATION	RESULT
Solid Matter Load		kg/m2/day	70	39.0

2-7 Sludge Thickening Tank (Daily Maximum)

2-8 Sludge Drying Bcd (Daily Maxmum)

ITEM		SIGN	UNIT	CALCULATION	RESULT
Design Flow		Q1	m3/day	-	17,000
Inlet SS Matter		M 1	kg/day	Q1*C*R2*10^-3	1,530
	Г	M2	t/day	M1/1000	1.53
Moisture Content		G	%		97.0
Sludge Volume		V 1	m3/day	M2*100/(100-G)	51.0
Drying Period	T	Р	day		10
Required Volume		V2	m3/day	V1*P	510.0
Depth of Bed		Н	m	-	0.3
Required Area		Α	m2	V2/H	1,700
Unit Number		UN	Unit	1	20
Width per Unit	Î.	. W -	m		6.0
Length per Unit	ļ	L1	m	A/(UN*W)	14.2
	Therefore	L2	m	-	14.5
Dimension	(Width)	W	m	W	6.0
	(Length)	L	m	1.2	14.5
	(Depth)	H	· m ·	H	0.3
	(Basin)	Basin	Basin	BN	20.0
Check			UNIT	APPLICATION	RESULT
Drying Period	· · · · ·		day	20	10.2

A-12.4-16

Appendix 12.4.3 Sewage Treatment Plant - Capacity Calculation CAPACITY CALCULATION OF FACILITIES Alternative 2 - Katugasutota (Dual Power Aerated Lagoon)

1 BASIC CONDITIONS

1-1 BASIC ITEMS

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(1) Name : Katugastota Scwage Treatment Plant

(2) Land Area :	Approximately	1.2	0 ha
(3) Elevation :	475.950	m	
(4) Inlet Pipe Level :	472.447	m	
(5) Pipe Diameter :	300	m	
(6) Land Use :	n, a. ⊷		
(7) Collection System :	Seperate Type		
(8) Treatment Method :	Sewage Treatme Sludge Treatme		
(9) Effluent Point :	Mahaweli Gang	a	
(10) Effluent Point Water Le	vel :	446.4	m
(11) Target Year :	Year 2005 (Pha	se 1), Year 2015	5 (Phase 2)
(12) Lowest Monthly Average	e Temperature	23	.6 °C (January)

1-2 Design Population

Design Population : 5,260 Persons

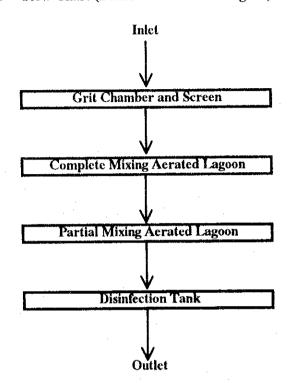
1-3 Design Sewage Flow

ITEM	m3/day	m3/hr	m3/min	m3/sec
Daily Average	1,500	62.5	1.04	0.017
Daily Maximum	1,700	70.8	1.18	0.020
Hourly Maximum	2,500	104.2	1.74	0.029

1-4 Design Sewage Quality

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ITEM	INFLUENT	EFFLUENT	REMOVAL	REMARKS
	(mg/L)	(mg/L)	RATIO (%)	·
BOD	240	30	88	
SS	250	50	80	



1-5 Flow Chart (Dual Power Aerated Lagoon)

	ITEMS	UNIT	Formula or Value	Application
1-6-1 G	rit Chamber			
(1) W	ater Surface Load	m3/m2/day	> 1800	1,800
(2) Av	verage Velocity	m/sec	> 0.3	0.3
1-6-2 Co	omplete Mixing Aerated Lagoon			
(1) Re	etention Time	day	1.5 - 2.5	1.50
(2) W	ater Depth	m	3.0 - 4.0	3.0
	ower Requirement for Mixing	W/m3	> 6.0	6.0
1-6-3 Pa	artial Mixing Aerated Lagoon			
(1) R e	etention Time	day	2.0	2.0
(2) W	ater Depth	m	2.0 - 4.0	3.0
	ower Requirement for Mixing	W/m3	> 1.0	1.0
(4) N	umber of Cell	Cell/Basin	1 - 3	3
1-6-4 St	torm Water Settling Tank			
(1) W	Vater Depth	m	1.5 - 3.0	1.5
	etention Time (Hourly Max Rain)	hour	> 0.5	0.5
(3) W	Vater Surface Load (Hourly Max Rain)	m3/m2/day	75 - 150	150.0
1-6-5 D	isinfection Tank			· · · · · · · · · · · · · · · · · · ·
(1) R	etention Time	min.	> 15	15.0
. ,	losage	mg/i	2.0 - 4.0	3.0

1-6 Design Criteria for Dual Power Aerated Lagoon

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2 CAPACITY CALCULATION

2-1 Grit Chamber and Screen (Hourly Maximum)

ITEM		SIGN	UNIT	CALCULATION	RESULT
Туре		-	-	Parallel Flow Type	
Design Flow		Q1	m3/day		2,500
C.		Q2	m3/sec	•	0.029
Water Surface Load		WSL	m3/m2/day	-	1,800
Required Surface Area	L .	RSA	m2	Q1/WSL	1.389
Basin Number (Total)		BN	basin		2
Basin Number (Stand-	By)	BNS	basin	-	1
Average Velocity		V	m/sec	· · ·	0.30
Depth		Н	m	-	0.20
Width		W1	m	Q2/(V*H)	0.482
	Therefore	W2	m	-	0.50
Length		L1	m	RSA/W2/(BN-BNS)	2.778
0	Therefore	L2	m	-	3.00
Dimension	(W)	W	m	W2	0.50
	(Ľ)	L	m	1.2	3.00
-	(Basin)	_	basin	BN	1
·	(Stand-By)		stand-by	BNS	1
Screen Type		· -		Fine Bar Screen	
Screen Set Number		SSN	set	BN	2
Check			UNIT	APPLICATION	RESULT
Water Surface Load			m3/m2/day		1,667
Average Velocity			m/sec	> 0.3	0.29

ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре		-	Rectangular Type	
Design Flow	Q1	m3/day	-	1,700
	Q2	m3/hr	-	70.83
Retention Time	T1	day	-	1.50
Inlet BOD Quality	So	mg/L	-	240
Required Volume	V1	m3/basin	Q1*T	2,550
Basin Number	BN	basin	-	
Required Volume per Basin	VBN	m3/basin	Q1*T/BN	1,275
Water Depth	H	m	-	3.00
Required Surface Area	A	m2	V/H	42
Width	W	m	-	30.0
Length	L1	m	A/W	14.16
Therefore	L2	m	-	15.00
Oxygen Demand Rate	PR1	kg/h	(4.16*10^-5)*r*Q1*So	2:
-max. oxygen uptake	ſ_	W/m3	-	1.
Aeration Unit Power Rate	PRO	kg/h	1000*PR1/(N*Q1*T1)	5.2
Therefore	PRO	W/m3	-	5.
-aeration performance	N	W/m3	-	
Power Requirement	P1	kW	-	16.
1) Oxygen Requirement	P10	kW .	PR1/N	13.4
2) Mixing Power	P1M	kW	V1*P0*10^-3	15.
Dimension (Width)	W	m	W	30.0
(Length)	L	m	1.2	15.0
(Depth)	Н	m	Н	3.0
(Basin)	-	basin	BN	
Aerator Type		-	Slanting Shaft Screw Aerator	
Check		UNIT	APPLICATION	RESULT
Retention Time		day	1.5 - 2.5	1.5

2-2 Complete Mixing Aerated Lagoon (Daily Maximum)

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ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре	-		Rectangular Type	
Design Flow	Q1	m3/day	-	1,700
	Q2	m3/hr		70.83
Retention Time	T2	day	-	2.00
Required Volume	V2	m3/basin	Q2*T	3,400
Basin Number	BN	basin	-	
Cells Number	CN	cell/basin	-	
Stand-by Cell Number	CNS	basin	-	
Sludge Accumulation	SA	m3/year	365*Q1*Xi/(x*10^6)	853
-inert solid concentration	Xi	mg/l	-	5'
-weight fraction of solids	x	-	-	0.04
No. of Cells Cleaned per Year	CNC	basin	-	
Total Sludge Accumulation	TSA	m3	-	1,280
Required Volume	V	m3/cell	(Q1*T+TSA)/(BN*CN-CNS)	930
Water Depth	D	m	-	4:00
Required Surface Area	A	m2/cell	V/H	234
Width	W	m	-	30.00
Length	L1	m	A/W	7.800
Therefore	L1	m	-	8.00
Power Requirement	P2	kW	-	4.0
1) Mixing Power	P2M	kW	Q1*T2*CN*10^-3	3.4
Dimension (Width)	W	m	W	30.00
(Length)	L	m	L1	8.00
(Depth)	H	m	Н	4.00
(Basin)	-	basin	BN	
(Cell)	- -	cell/basin	CN	
(Stand-by Cell)	-	cell	•	1
Aerator Type		-	Slanting Shaft Screw Aerator	
Check		UNIT	APPLICATION	RESULT
Surface Area		m2	•	1,440
Retention Time		day	2.0	2.0

2-3 Partial Mixing Acrated Lagoon (Daily Maximum)

2-6 Disinfection Tank (Daily Maximum)

ITEM	SIGN	UNIT	CALCULATION	RESULT
Chemical Type	-	-	Chlorination Type	
Design Flow	Q1	m3/day	-	1,700
	Q2	m3/min	-	1.18
Retention Time	Т	min.		15.0
Basin Number	BN	basin		1
Required Volume	V	m3	'Q2*T	18
Width	W	m	-	1.00
Water Depth	H	m	-	1.00
Length	L1	m	V/(W*H)	17.708
there	fore L2	m	-	18.00
Dosage	D	mg/L	-	3.0
Required Chemical	RC1	kg/day	Q1*D*10^-3/C	5.10
There	fore RC2	kg/hr	RC1/24	0.21
Dimension (Wi	dth) W	m	W	1.00
(Len		m	L2	18.00
(De	pth) H	m	H	1.00
	pth) BN	basin	-	1
Chlorine Feeder	-	unit	including 1 for stand-by	3
Check		UNIT	APPLICATION	RESULT
Retention Time		min.	> 15	15.2

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Appendix 12.5 Summary of Construction Cost Exchange Rate =

1.8 Yen/Rs

Construction Cost - Master Plan : Alternatives

	E356		Alternative 1	ve 1			Alternative 2	ve 2	
	racijines	Specifications	Civil	M&E	Total	Specifications	Civil	M&E	Total
S.	. Sewer								
	Sub-Totai		777,683		777,683		747,251		747,251
	2. Pumping Station	uc							
	Kandy								
	P/S 1	0.74*27*2	918	2,185		0.74*27*2	918	2,185	
1	P/S 2-1	1.74*48*2	1,383	4,211					
	P/S 2-2	1.74*48*2	1,383	4,211					
	STP-1	9.0*14*4	7,211	12,050		8.2*14*4	7,211	11,275	
	STP-2	4.5*14*4	0	3,661		4.1*14*4	0	3,454	
	Katugastota								
	STP					1.74*24*2	1,210	2,438	
	Sub-Total		10,895	26,317	37,212		9,339	19,351	28,690
S.	3. Sewage Treatment Plant	nent Plant						_	
	Kandy	18,000m3/day	358,896	666,558		17,000m3/day	344,809	636,899	
	Katugastota					1,700m3/day	45,428	35,242	
	Sub-Total		358,896	666,558	1,025,454		390,237	672,141	1,062,378
1	Total		1,147,474 692,875		1,840,349		1,146,827	691,492	1,838,319

Construction Cost - Feasibility Study

		M/P (Alter	tternative 2)			F/S (Phase 1)	e 1)			Phase 2	: 2	
Facilities	es Specifications	Ö	M&E	Total	Specifications	Civil	M&E	Total	Specifications	Civil	M&E	Total
1. Sewer												
Sub-Total	otal	747,253		747,251		463,191		463,191		284,060		284,060
2. Pumping Station	Station											
Kandy												
L/S 1	1 0.74*27*2	918	2,185		0.74*27*2	918	2,185					
I-dLS	-1 8.2*14*2	7,211	11,275		8.2*14*2	7,211	8,137		8.2*14*2	0	3,137	
TTS	STP-2 4.1*14*2	0	3,454		4.1*14*2	0	1,727		4.1*14*2	0	1,727	
Katugastota	ustota											
STP	1.74+24*2	1,210	2,438			0	0		1.74*24*2	1,210	2,438	
Sub-Total	leio	9,339	19,351	28,690		8,129	12,049	20,178		1,210	7,302	8,512
3. Sewage	1. Sewage Treatment Plant						•					
Kandy	17,000m3/day	/day 344,809	636,899		8,500m3/day	190,707	320.246		8,500m3/day 154,102	154,102	316,654	
Katugastota	istota 1,700m3/day	/day 45,428	35,242			0	0	1	1.700m3/day	45,428	35,242	
Sub-Total	otal	390,237	672,141	1,062,378		190,707	320,246	510,953		199,530	351,896	551,426
Total		1,146,827	691,492	1,838,319		662,027	332,294	994,321		484,800	484,800 359,197	843,997

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Alternative 2 (A					Master Plan		Feasibility Study			
ITEM	DESCRIPTION	Depth	UNIT	RATE	QUANTITY	COST	QUANTITY	COST		
Clay Pipe Laying	150 mm (Lateral)	1.5	m	5,498	9,300	51,131,400	4,500	24,741,000		
	150 mm	1.5	m	5,498	4,651	25,571,198	4,651	25,571,198		
	150 mm	2,5	m	7,871	793	6,241,703	793	6,241,703		
	225 mm	1.5	m	7,142	1,527	10,905,834	1,527	10,905,834		
	225 mm	2.5	m	9,603	1,859	17,851,977	1,509	14,490,927		
	225 mm	3.5	m	12,459	691	8,609,169	691	8,609,169		
	225 mm	7.5	m	27,832	100	2,783,200	0	C		
	300 mm	1.5	m	10,593	1,942	20,571,606	1,942	20,571,606		
	300 mm	2.5	m	13,173	680	8,957,640	680	8,957,640		
	300 mm	3.5	m	16,147	80	1,291,760	80	1,291,760		
	300 mm	7.5	m	31,994	80	2,559,520	80	2,559,520		
	400 mm	1.5	m	15,652	2,590	40,538,680	840	13,147,680		
	400 mm	2.5	m	18,373	548	10,068,404	348	6,393,804		
	400 mm	4.5	m	25,001	200	5,000,200	0	C		
· · · · · ·	450 mm	1.5	m	17,475	75	1,310,625	- 75	1,310,625		
	500 mm	1.5	m	20,461	288	5,892,768	288	5,892,768		
	500 mm	2.5	m	23,318	70	1,632,260	70	1,632,260		
	600 mm	1.5	m	33,513	312	10,456,056	312	10,456,056		
	600 mm	2.5	m	36,508	55	2,007,940	55	2,007,940		
HP Pipe Laying	675 mm	1.5	m	16,046	500	8,023,000	500	8,023,000		
	675 mm	2.5	m	19,178	180	3,452,040	180	3,452,040		
	675 mm	3.5	m	22,704	120	2,724,480	120	2,724,480		
	675 mm	4.5	m	26,626	190	5,058,940	190	5,058,940		
· · · · · · · · · · · · · · · · · · ·	675 mm	5.5	m	30,942	100	3,094,200	100	3,094,200		
<u> </u>	750 mm	2.5	m	21,242	150	3,186,300	150	3,186,300		
	825 mm	1.5	m	20,005	400	8,002,000	400	8,002,000		
	825 mm	2.5	m	23,413	480	11,238,240	480	11,238,240		
	825 mm	4.5	m	31,416	.700	21,991,200	700	21,991,200		
·	825 mm	7.5	m	46,382	50	2,319,100	50	2,319,100		
DI Pipe Laying	100 mm	1.5	m	6,242	650	4,057,300	650	4,057,300		
	150 mm		m	7,358				-		
Manhole	Type 1		Nr	80,181	517	41,453,577	369	29,586,789		
	Туре 2		Nr	93,941	57	5,354,637	57	5,354,637		
	Туре 3	· .	Nr	109,418	-	-	-			
Connection Pipe	100mmPVC,L=4m		Nr	25,712	12,402	318,880,224	5,794	148,975,328		
Inspection Pit	RC,300×300	·	Nr	5,098	12,402	63,225,396	5,794	29,537,812		
Siphon		4.5	Nr	868,712	1	868,712	1	868,712		
Siphon Pipe	450mm×2	4.5	m	27,024	40	1,080,960	40	1,080,960		
Siphon		7.5	Nr	1,053,558		1,053,558	1	1,053,558		
Siphon Pipe	450mm×2	7.5	m	40,127	40	1,605,080	40	1,605,080		
Road Crossing	Jacking(675mm)		m	240,000	30	7,200,000	30	7,200,000		
TOTAL	Sewer Main + Later	al			29,361	747,250,884	21,961	463,191,160		
	Sewer Main			1. J. A.	20,061		17,461			

Appendix 12.6 Cost of Sewer

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A-12.6-1

ITEM	DESCRIPTION	Depth	UNIT	RATE	COST	Feasibility Study			
lay Pipe Laying	and a start of the second defendence on the start of the second se	1.5		5,498	QUANTITY 9,300	51,131,400	Quantini	0001	
lay Pipe Laying		<u>1.5</u> 1.5	m	<u> </u>	4,651	25,571,198		······	
			m						
		2.5	m	7,871	793	6,241,703			
	the second se	1.5	m	7,142	1,527	10,905,834			
		2.5	m	9,603	1,859	17,851,977			
		3.5	m	12,459	691	8,609,169			
		7.5	m	27,832	100	2,783,200			
		1.5	m	10,593	1,268	13,431,924			
		2.5	m	13,173	320	4,215,360	-		
	300 mm	7.5	m	31,994	80	2,559,520			
	400 mm	1.5	m	15,652	2,590	40,538,680			
**************************************	400 mm	2.5	m	18,373	548	10,068,404			
		4,5	m	25,001	200	5,000,200		6 <i>#</i> _6	
		1.5	m	17,475	674	11,778,150	· · · · · ·		
		2.5	m	20,263	360	7,294,680			
		3.5	m	23,446	80	1,875,680			
		1.5	m	33,513	363	12,165,219	· · · · ·	······	
		2.5	<u>+</u> +	36,508	70	2,555,560			
7D D' 7			m					· · · · · ·	
IP Pipe Laying		1.5	m	16,046	632	10,141,072			
		2.5	m	19,178	55	1,054,790			
		3.5	m	22,704	120	2,724,480			
	675 mm	4.5	m	26,626	100	2,662,600			
	675 mm	5.5	m	30,942	100	3,094,200		1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 -	
	750 mm	1.5	m	17,972	180	3,234,960	and the second second		
	750 mm	2.5	m	21,242	330	7,009,860			
	750 mm	4.5	m	28,964	90	2,606,760			
	825 mm	1.5	m	20,005	400	8,002,000	1		
	825 mm	2.5	m	23,413	480	11,238,240			
1	825 mm	4.5	m	31,416	700	21,991,200			
·····	825 mm	7.5	m	46,382	50	2,319,100			
DI Pipe Laying	100 mm	1.5	m	6,242	650	4,057,300		· · ·	
	200 mm	1.5	m	8,514	2,600	22,136,400			
Manhole	Type 1	11.5	Nr	80,181	509	40,812,129			
	Type 2		Nr	93,941	65	6,106,165		<u> </u>	
	Type 2 Type 3		Nr	109,418	05	0,100,105			
Connection Pipe	100mmPVC,L=4m	ļ	Nr	25,712	12,402	318,880,224		·	
		<u> </u>	-						
Inspection Pit	RC,300×300	4.5	Nr	5,098	12,402	63,225,396			
Siphon	450 0	4.5	Nr	868,712			ļ		
Siphon Pipe	450mm×2	4.5	m	27,024		1,080,960	ļ	and the second s	
Siphon	+	7.5	Nr	1,053,558		1,053,558	· · · · · · · · · · · · · · · · · · ·		
Siphon Pipe	450mm×2	7.5	m	40,127		1,605,080			
Road Crossing	Jacking(675mm)		m	240,000	30	7,200,000			
TOTAL	Sewer Main + Later Sewer Main	al			31,961 22,661	777,683,044			

Manhole Span	50	m
Manhole Type	150 to 600 mm	Type 1
	700 to 900 mm	Type 2
	900 to 1200 mm	Туре 3

Numbers of Service Connections

	Kandy	Reference
Size of Family (people/house)	6.65	
M/P Population (2015)	54,985	
Domestic (No. of Houses)	8,268	
Total (No. of houses)	12,402	Domestic × 1.5
F/S Population (2005)	19,262	
Domestic (No. of Houses)	2,897	
Total (No. of Connections)	5,794	Domestic × 2

A-12.6-2

Appendix 12.7 Unit Cost Appendix 12.7.1 Unit Cost of Civil Works

are used for cost estimate.

	ltem		NWSD	B Rate 97		outh - Ground			outh - Pumpin		Applied	Adjusted
				Overhead 20%	Local (Rs)	Forign(Yen)	Total (Rs)	Local (Rs)	Forign(Ycn)	Total (Rs)		
1.1	Excavation											
	Bulldozer (incl. Backfilling	<u>;)</u>	(Basement)	(Basement)								490.00
	Backfoe (incl. Backfilling)		(Pit/Irench)	(Pit/Trench)	(150 mm)			(225 nm)				790.00
	Rock excavation	m³	1,469.00	1,763.00	69.00	544.38	371.43	1,716.00	195.27	1,824,48	1,808,99	1,990.00
2.1	Earth Filling											430,00
	earth available at site	m ³	141.00	169,00							169.00	190.00
	earth to be borrowed	m²	324.00	389.00							389.00	430.00
3.	Soil Disposal											310,00
	On site	m ³	68.00	82.00							68.00	80,00
	Off site	m	232.00	278.00						L	278.00	310.00
4.	Piling	Ī										
	On site 600 mm dia.	m			1,824.81	14,399.00	9,824.25				9,824.25	10,810.00
5.	Concrete Work	Γ										
—	Orade 10	Ι.					· · · · · · · · · · · · · · · · · · ·	<u></u>				7,840.00
Г	Foundations	m	3,743.00	4,492.00	76,07	600.18	409.50	514.80	58.58	547.34	7,123.19	
F-	Orade 20/30		(Grade 20)		(Grade 30)			(Orade 30)	L		8,658.97	9,530.00
Γ	Columns	m ³	4,868.00	5,842.00	1,820.50	14,362.89	9,799.88	6,864.00	781.07	7,297.93	8,659.97	9,530.00
6.	Form Work	Ī		T							960.43	1,060.00
7.	Reinforcement	1								L	66,328.41	72,970.00
	Tor steel		50,220.00	60,264.00	13,510.53	106,591.98	72,728.30	62,920.00	7,159.76	66,897.64	66,329.41	72,970.00
L	Mild steel	tor	46,920.00	56,304.00	11,312.83	89,253.07	60,897.87	62,920.00	7,159.76	66,897.64	66,329,41	72,970.00
8,	Building				L	·				·	l	
	Offices 2F, 126 m ²	m	9,600.00	11,520.00	13,494.97	1,535.61	14,348.09			ļ	14,226.22	15,700.00
Г	Operating houses	m ¹	8,600.00	10,320.00	I					· ·		20,000.00
r	Pumping Station BF, 181n	n ²			·	1		31,855.72	3,624.91	33,869.56	33,581.87	37,000.00
F	Chlorine House 1F, 24m ²	m			17,014.23	1,973.50	18,110.62	<u> </u>	· · ·	L	17,953.99	19,800.00
F	Store houses 1F, 24m ²	m	8,200.00	9,840.00	18,950.98	2,156.46	20,149.01				19,977,86	22,000.00
F	Quarters 1F, 100m ²	m			17,496.47	1,971.32	18,591.64			L	18,435.19	20,300.60
9.	Pavement	1			r	1						
F	Reinstatement	m	-		206.58	1,629.82	1,112.04	Actual pay	ment to RDA	Rs. 2000.00)	2,000.00	2,000.00
10). Miscellaneous	T		1	1							
F	Miscellancous	%	-	-	Γ			I			L	5 to 20 %

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Appendix 12.7.2 Unit Cost of Piping Materials

are used for cost estimate.

					L										
T	1	Diameter (n	nni)	NWSD	B Rate 97	Beire Lake	Manufacturer		Towns	South		Applied	Adjusted		
				Rs/m	Overhead 20%	Rs/m	Rs/m	Local (Rs)	Forign(Yen)	C. D. (Rs)	Total (Rs)				
. W	ater	Supply													
	DIP			(CIF+C.D.)											
	1	200	mm	2,647.48	3,177.00								3,500.00		
	~	250	mm	2,981.44	3,578.00			65.58	6,467.59	661.72	3,807.10	3,807.10	4,190.00		
		300	ກາກາ	3,794.56	4,553.00			82.79	8,165.06	835,39	4,806.30	4,806.30	5,290.00		
		350	mm	4,537.50	5,445.00			103.27	10,234.03	1,041.95	6,018.57	6,018.57	6,630.00		
		400	mm	5,324.00	6,389.00			137.05	13,515.35	1,382.79	7,955.72	7,955.72	8,760.00		
		450	mm	6,352.50	7,623.00			144.09	14,210.53	1,453.92	8,364.93	8,364.93	9,210.00		
		500	nun	7,292.67	8,751.00			193.08	19,041.13	1,948.15	11,208.43	11,208.43	12,330.00		
-1	-1	600	mm	9,075.00	10,890.00			223,43	22,034.08	2,254.36	12,970.21	12,970.21	14,270.00		
		700	mm	11,918.50	14,302.00								20,000.00		
		800	mm	14,762.00	17,714.00			462.19	45,580.63	4,663.47	26,830.72	26,830.72	29,520.00		
		900	mm	15,851.00	19,021.00								35,000.00		
	PVC	C (type 600)			1								(type 600)		
	1	63	mm	50,00	60.00			55.95	55.18		82.23	82.23	100.00		
	_	75	ກນາ	78.00	94,00							114.78	130.00		
		90	ກາກາ	118.00	142.00			109.75	108.23		161.29	161.29	180.00		
		110	nım	173.00	208.00			161.15	158.93		236.83	236,83	270.00		
		160	ញា	340.00	408.00			340.35	335.65		500.18	500.18	560.00		
		225	mm	655.00	786.00	l		667.15	657.94		980.45	980.45	1,080.00		
2. S	ewei	rage													
		C (type 600)				(type 400)	(type 600)	[(type 600)		
		110	mm	173.00	208.00		1.1.1	161.15	158.93		236.83	236.83	270.00		
		160	mm	340.00	408.00		786.95	340.35	335.65		500.18	500.18	510.00		
		225	mm	655.00	786.00		1,496.80	667.15	657.94	T	980.45	980.45	990.00		
		280	nim		1,216.00		2,294,65					2,294.65	2,300.00		
		315	nım	1,010.00	1,22010	·····	2,888.02		1			2,888.02	2,890.00		
	Hu	ne Pipe			+	<u> </u>	1								
	1	150	mm	352.00	422.00	1	198.39		1	· · ·					
		225	าหา	- c	596.00	 	273.13		1				1. A.		
		250	mm		1	t	1	1	1		1.1		· · ·		
		300	mm		792.00	t	355.25		1			792.00	800.00		
		375	nm			<u> </u>	516.73	<u> </u>	1	·		1,080.00	1,080.00		
		400	nım		1	<u> </u>	1					1.0			
		450	mm		1,194.00		611.31	2,577.99	1,307.04		3,200.39	1,194.00	1,200.00		
	— —	500	mm			1			1						
	1	544	mm			1	1	4,124.78	2,091.26		5,120.62	(with inner			
	†	600	mm		1,663.00	1	847.07	T				1,663.00	1,670.00		
	<u>†</u>	675	mn		1	5,960.00	1	1	1	1		5,960.00	5,960.00		
	†	750	<u>+</u>		2,242.00	6,790.00	1,092.52	T				6,790.00	6,790.00		
-	+	825	mm		+	7,630.00	1,093.52	1		1	1	7,630.00	7,630.00		
-	+	900	mm	-	3,050.00	1	1,495.76	1		1	1	3,660.00	3,660.00		
	╉╼┈	1050				<u>†</u>	3,820.13	t			1	4,752.00	4,760.00		
⊢	C1	d	1			1	1	1		1	1	1	1		
<u> </u>	LC18	y Pipe	+	410.00	403.00	710.0			+	+	+	730.88	740.00		
—			mm					╂────			+	730.88	740.00		
		225	mn	648.00	778.00	1,789.8	ŧ	1	1		 -	1,789.84	1,790.00		
		250	mn	1		L		L					L		
		300	mn	1,235.00	1,482.00	4,464.6	6			1 ·	1.	4,464.66	4,470.00		
	+-	400	-	·····	1	8,578.3		1	1	T	1	8,578.39	8,580.00		
<u> </u>	1	450		-		9,959.2			1	1	1	9,959.28	9,960.00		
	+		-	-				1		1	+				
	1	500	ար առ	11	1	12,457.1	0				1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	12,457.10 24,476.30			

Note: 1. For transmission mains of water supply, 20 % of the cost of pipes shall be add to compensate the cost of specials, valves etc. 2. For diatribution mains of water supply, 35 % of the cost of pipes shall be add to compensate the cost of specials, valves etc.



Appendix 12.7.3 Unit Cost of Pipe Laying

						are used for o	ost estimate.				
			NRUAD			1 70	<u></u>	Toman	Cul Leules	Analised	Adjusted
	Diamete	r		B Rate 97		Towns South	(D) + 1 (D) >	Japan	Sri Lanka	лфриса	Adjusted
	(nun)		Rs/m	Overhead 20%	Local (Rs)	Forign(Yen)	Total (Rs)	Man-Day	Rs/m		
. Layin					L					(only Pi	e Laying
DIF					excavation, bac	kfilling etc.)					104.0
	200	mm	559.00	671.00				0.18	124.60	124.60	125.0
	250	mm	580.00	696.00	100.06	789.40	475.96	0.22	154.00	154.00	154.0
	300	mm	698.00	838.00	105.58	832.96	502.23	0.26	182.70	182.70	183.0
	350	mm	740.00	888.00	123.73	976.16	588.57	0.32	222.60	222.60	223.0
	400	nım	795.00	954.00	129.25	1,019.72	614.83	0.38	269.03	269.03	270.0
_	450	mm	852.00	1,022.00	149.53	1,180.10	711.48	0.45	316.87	316.87	317.0
	500	nun	942.00	1,130.00	258.50	2,039.45	1,229.67	0.52	365.40	365.40	366.0
	600	mm	1,077.00	1,292.00				0.66	463.87	463.87	464.0
	700	nun	1,234.00	1,481.00			,	0,80	562.33	562.33	563.0
	800	mm	1,395.00	1,674.00	385.00	3,037.48	1,831.42	0,96	672.00	672.00	672.0
	900 m		1,578.00	1,894.00				1.09	765.10	765.10	766.0
PV	Ċ		(only P	pe Laving)	(with 1 to 2m	excavation, ba	ckfilling etc.))			
-1	63	mm	11.76	14.00	29.04	229.11	138.14	0.04	30.10	30.10	31,0
	75	mm	11.76	14.00	29.04	229.11	138.14	0.04	30.10	30.10	31.0
	90	mm	13.94	17.00	29.04	229.11	138.14	0.06	39.90	39.90	40.0
	110	mm	15.00	18.00	34.98	275.98	166.40	0.06	39.90	39.90	40.0
1	160	mm	15.00	18.00	38.94	307.22	185.24	0.07	51.80	51.80	52.0
	225	ញាញ	18.15	22.00	40.04	315.90	190.47	0.10	72.80	72.80	73.0
	280	mm	18.74	22.00				0.14	98.00	98.00	98.0
<u> </u>	315	mm	10/1/1		†	t		0.17	119.00	119.00	119.0
-+-					<u>†</u>	<u> </u>					
u .,	1 me Pipe/Clay	l Pina	(with excava	tion, backfilling	(denth is unk	[]					·
	150		134.00	161.00	(depin is diki	1		0.32	224.00	112.00	112.0
	the second s	mm	164.00	197.00	 	<u> </u>		0.40	277.20	138.60	139.0
	225	mm	104.00	197.00	 		····	0.46	319.20	159.60	160.0
	300	mm	227.00	272.00	ł			0.53	369.60	184.80	185.0
	300	mm	270.00		.	l		0.60	420.00	210.00	210.0
		mm	270.00	324.00	_	} -		0.61	428.40	214.20	215.0
	400	mm	220 00	206.00		1 001 10	3,406.71	0.84	588.00	294.00	294.0
<u> </u>	450	mm	330.00	396.00	2,033.77	2,883.18	5,400.71	0.84	604.80	302.40	303.0
	500	mm		<u> </u>	2 012 72	2,883.18	3,406,71	0.96	672.00	336.00	336.0
	544	mm	410.00	102.00	2,033.77	2,003.10	5,400,71	1.06	744.80	372.40	373.0
	600	mm	410.00	492.00	<u> </u>		 		784.00	392.00	392.0
	675	mm	500.00		 			1.12 1.15	803.60	401.80	402.0
	750	mm	500.00	600.00			<u> </u>	1.13	840.00	401.00	402.0
	825	mm		780.00	·			1.20	862.40	420.00	420.0
	900	mm	650.00	780.00	_	 			L	470.40	471.0
	1050	mm	680.00	816.00				1.34	940.80	470.40	4/1.0
	vation		.		L	ļ					
	ckfoe	1				L	L	ļ			790.0
	cl. Backfillin	g)	L	L	1		L	1		 	
3. Soil	Disposal			L		<u> </u>	L	_			<u> </u>
Of	f site	m ³						[i	I	310.0
	cfilling with s		 	t	1	1	1	1	1	1	
		1 4	 	<u> </u>		t	+	1	1	1	1,000.
	th sand suppl	<u>y m</u> ³			<u> </u>	<u> </u>	ļ	<u> </u>	+	{	1,000.
5. Pave		<u> </u>	Į	 	.	·}	<u> </u>	_	·	+	
l n	instatement	m ²	l I	1	1	1	1	4	1	1	2,000.0

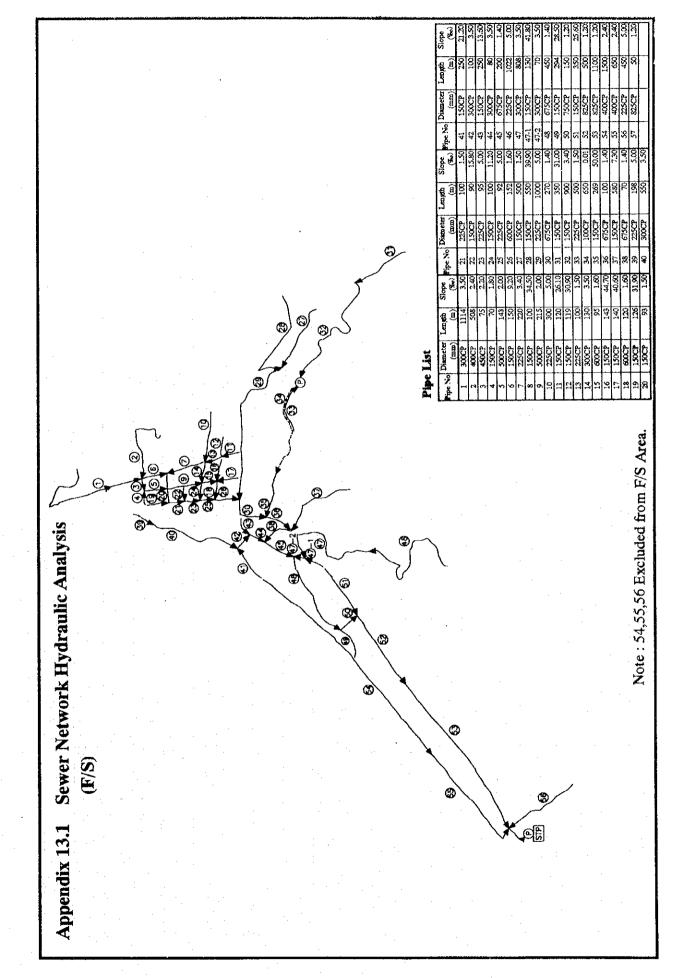
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Chapter 13

Appendix 13.1	Sewer Network Hydraulic Analysis
	(F/S)
Appendix 13.2	Trunk Sewer Profile
Appendix 13.3	Pumping Equipment
	- Capacity Calculation
Appendix 13.4	Sewage Treatment Plant

- Capacity Calculation Appendix 13.5 Hydraulic Calculation Appendix 13.6 Drawings Appendix 13.7 Storage Capacity of Sewer (Kandy)



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μ																			
0.324m3/capita-day		Remarks									-								
324m3/	<u>i</u>		E	100		126	175		100	<u>372</u> 100		00 00		134	100	100		167	i
				I			1 1							1 1	1 1	1		1 1	
Flow		Level		533314 506804		535567 - 506694	505890 505725		506215 506089	502980 501414		506252 505502	L C S	506631	505172 501722	501414 500284		506252	• • 1 · 1 1
ewage	er	G.L.	×	53550		54357	50814		50739	50726 50297		50750		50814	50975	50297 50184		51100	+
WUnit Sewage	gn Sever	Flow	щ3/S	00572		01020	01337		d0065	d1689		00262		d0146	00834	01689	• • • • • • •	00318	ŀ
n×	Design	λ	s/m	d809		0812	0841		d365	0860		0658		1821	\$008	0860		0799	
		Slope	98	350						200		8		83	3450				
		Dia.	Ë	300		400	450		150	500		225		150	225	200		225	
		Accum.	na3/s	d0254 ¢		00392			¢.	\$ 92.900	•	, 00045 ø		00015 Ø	00078 ¢	00769 Ø		00118 Ø	
	2			001143 00		003796			00086	005240 00					1				
	Other Flow	Accus.	: m3/s							50 002		53 000453		51 000151	71 000777	51 006168		1001035	
	0th	Sec.	m3/s	001143		96.796			000086	00123		000453		000151	000173	000151		001035	
		Flow	m3/s	00140	~	00012			• • • • • •	00152			 			00152			+
	ge Flow	Population Sec. Accum.	a.	3742		307	4			4049						4049		385	
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Sewage Flow Calculation Table (Kandy)

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Sewage Flow Calculation Table (Kandy)

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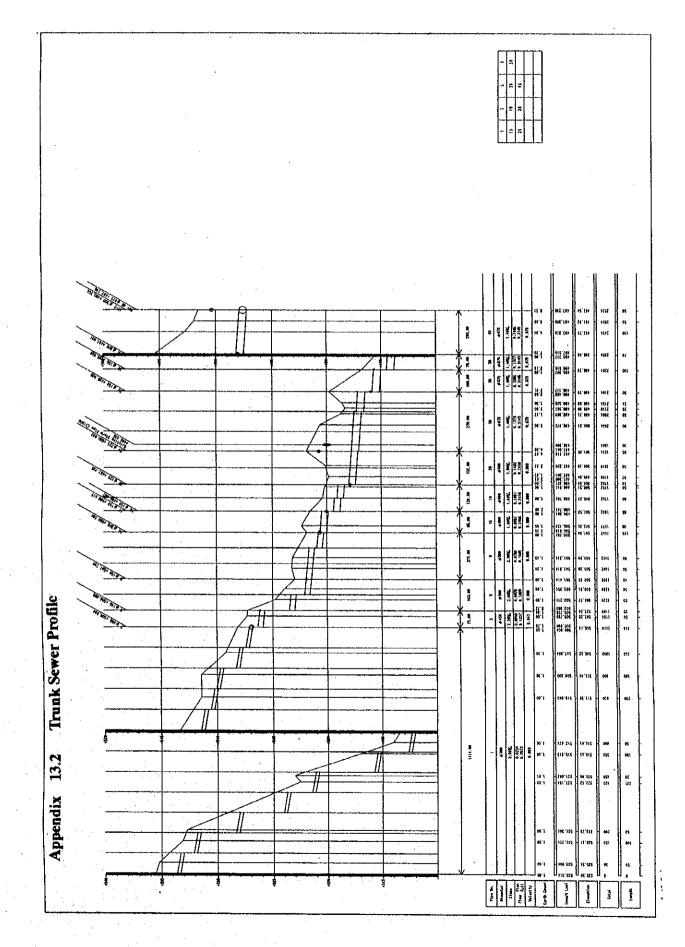
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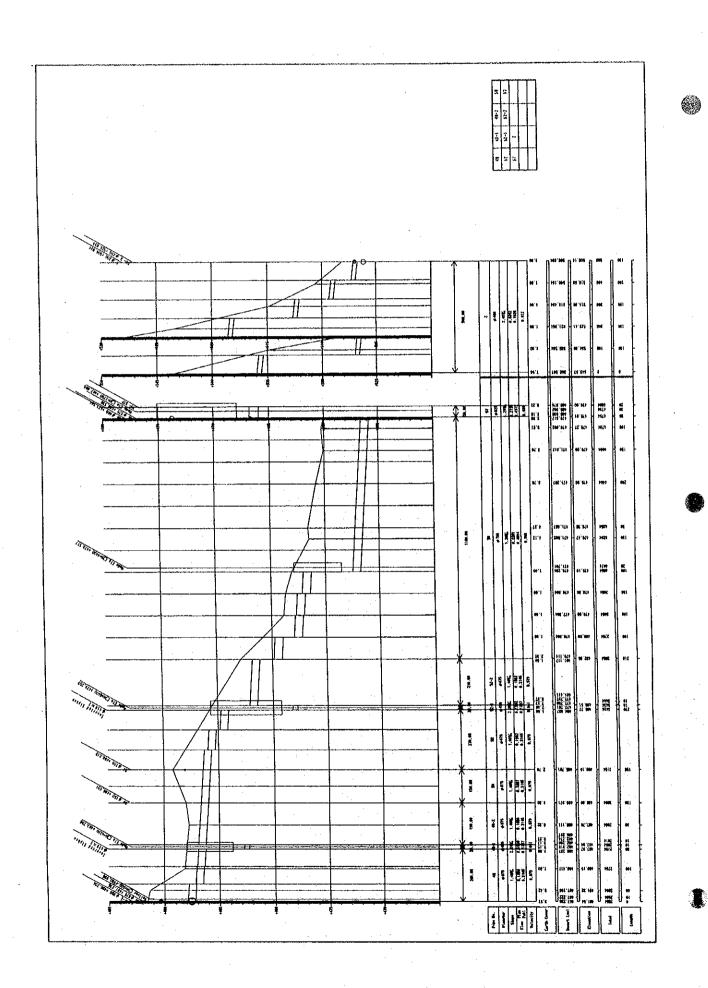
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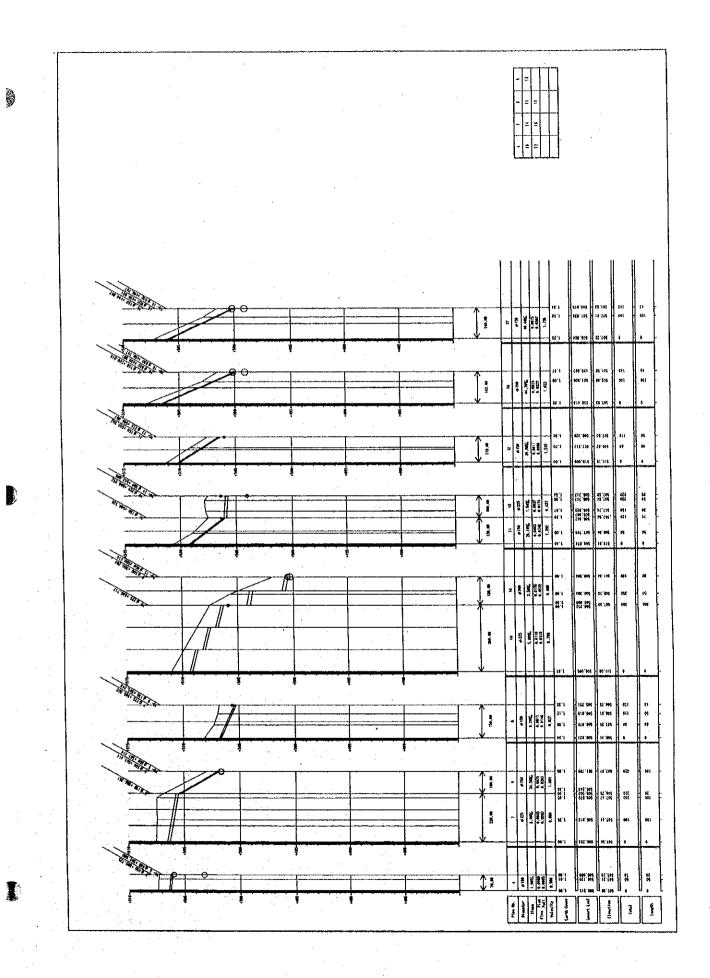
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2	Service Area	Length		<u>م</u> ۲	ainfall	1	Storm Run-off Service	Run-off Service Area			Sewag	Sewage Flow		oth	Other Flow			ļ		Design Sewer	wer.			
ŶĊ	Accum. S	Sec. Accum	cum.		ia a	<u>ں</u>	Sec.	Accum.	R.O.	rop/t	Sec	Accu.	FLOW	Sec.	Accur.		Dia.	Slope	>	Flow	e.L.	Level	ß	Remarks
<u>م</u>	्रम्			nim	m3/s-ha		ha	μ	a/S∎	P/ha		ď	m 3/s	s/6at	m 3/s	m3/s	ä	3 48	篇/S	m3/s	×	×	6	
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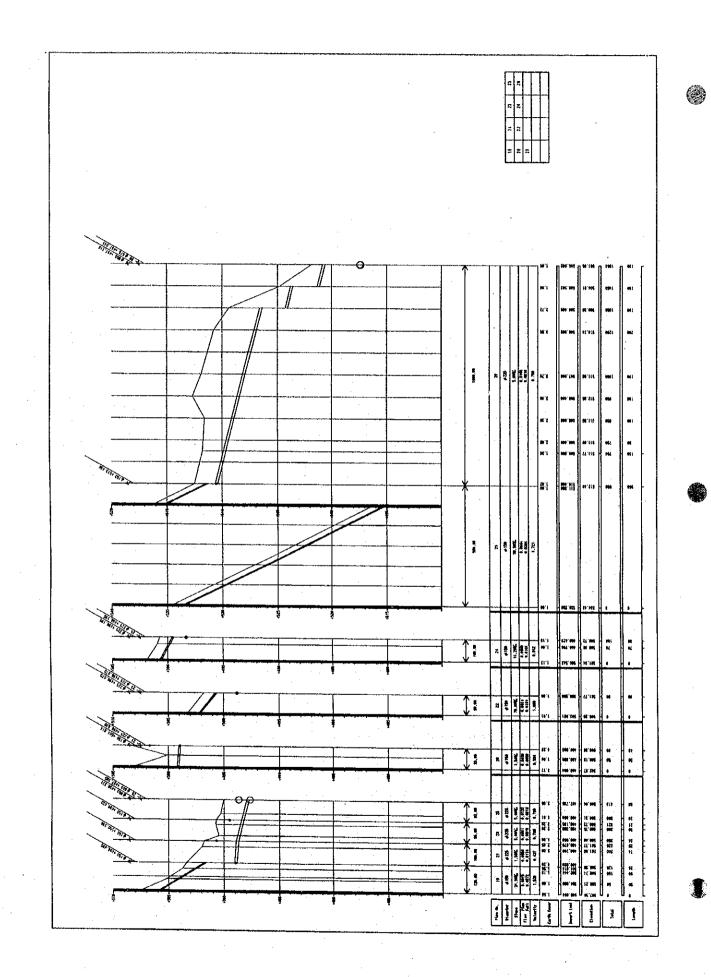


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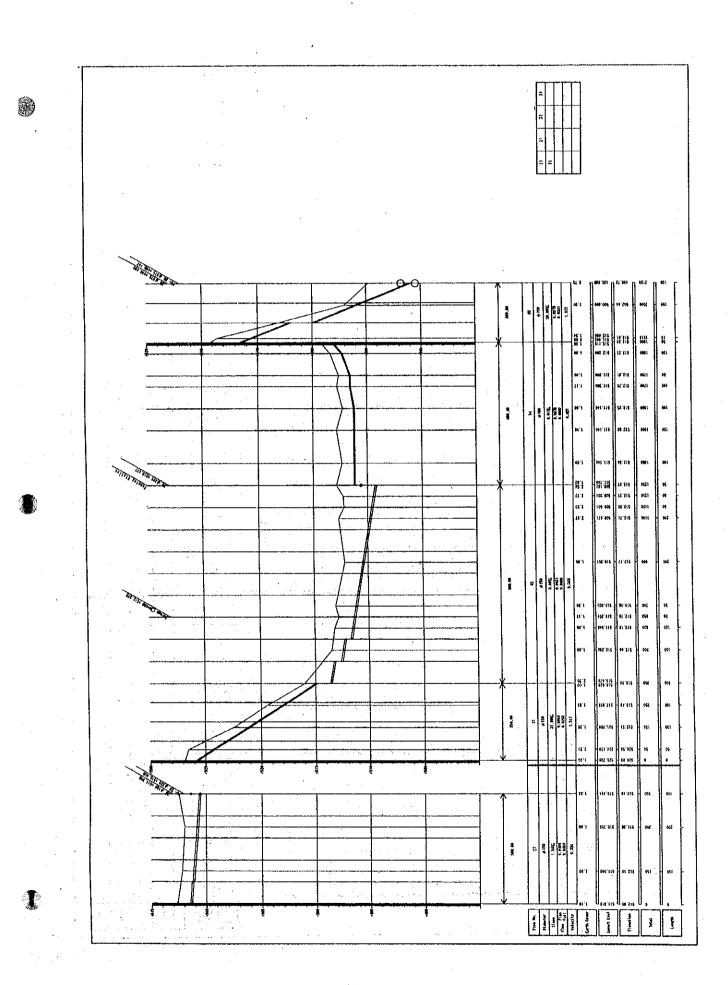


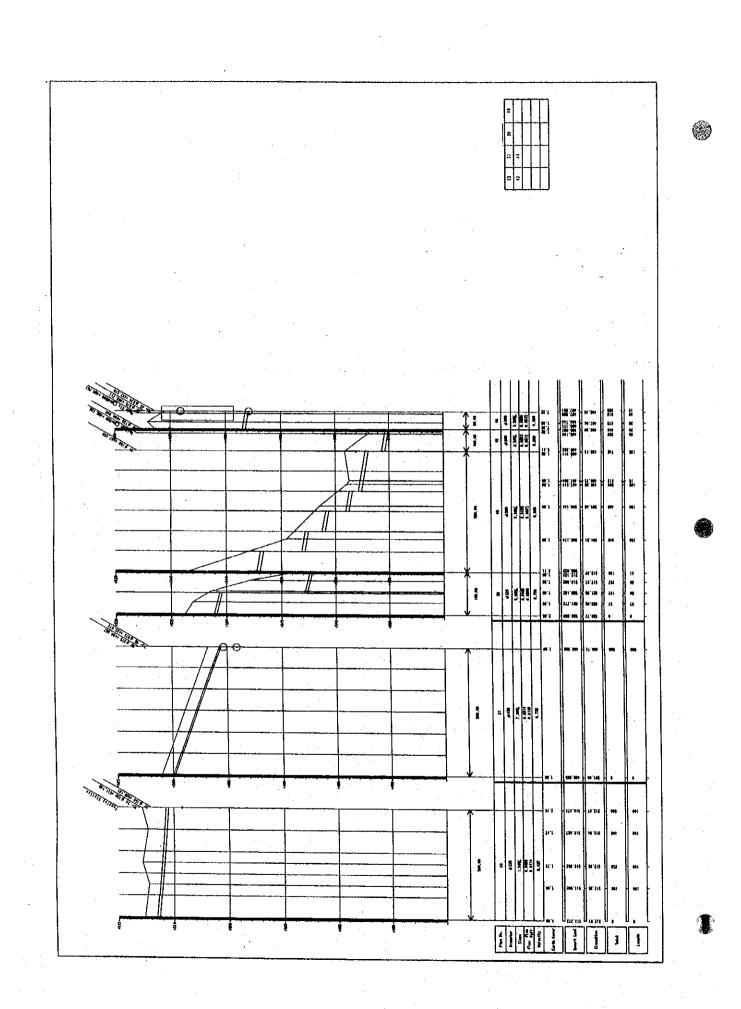


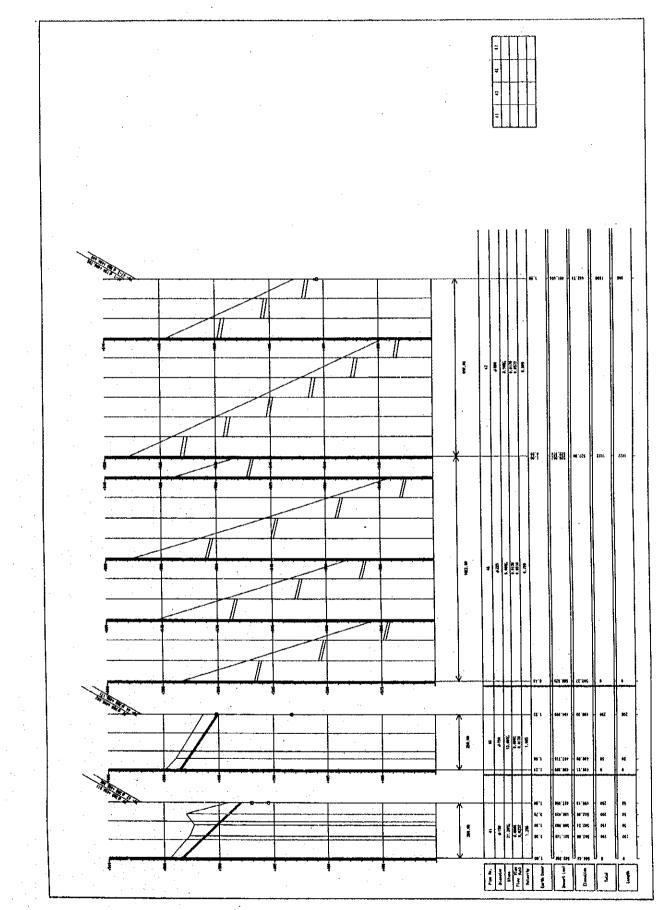
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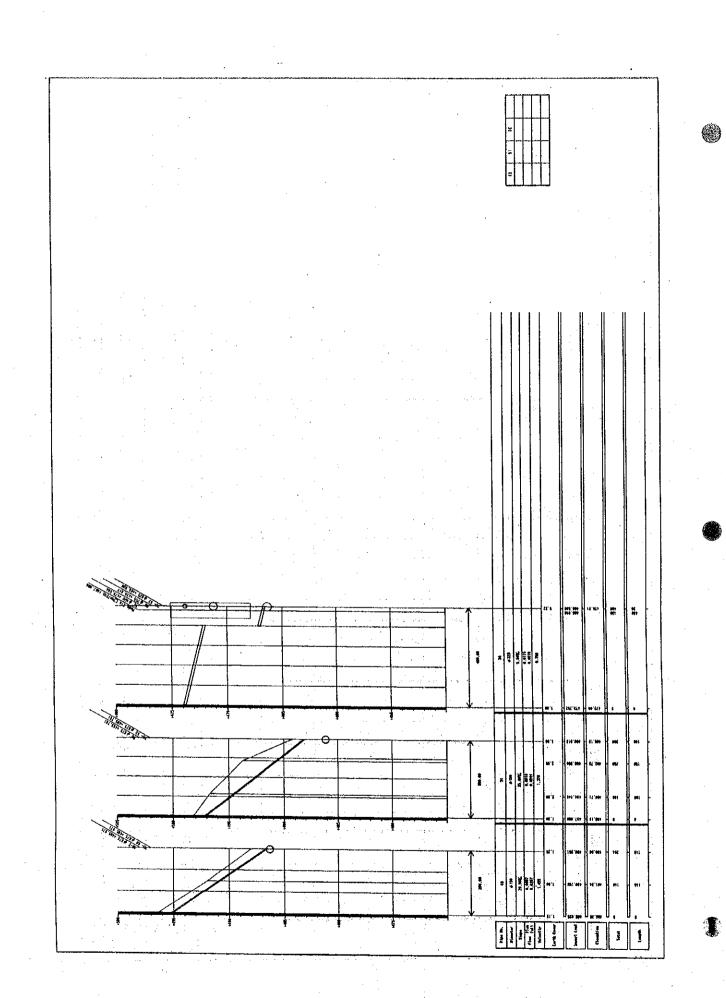


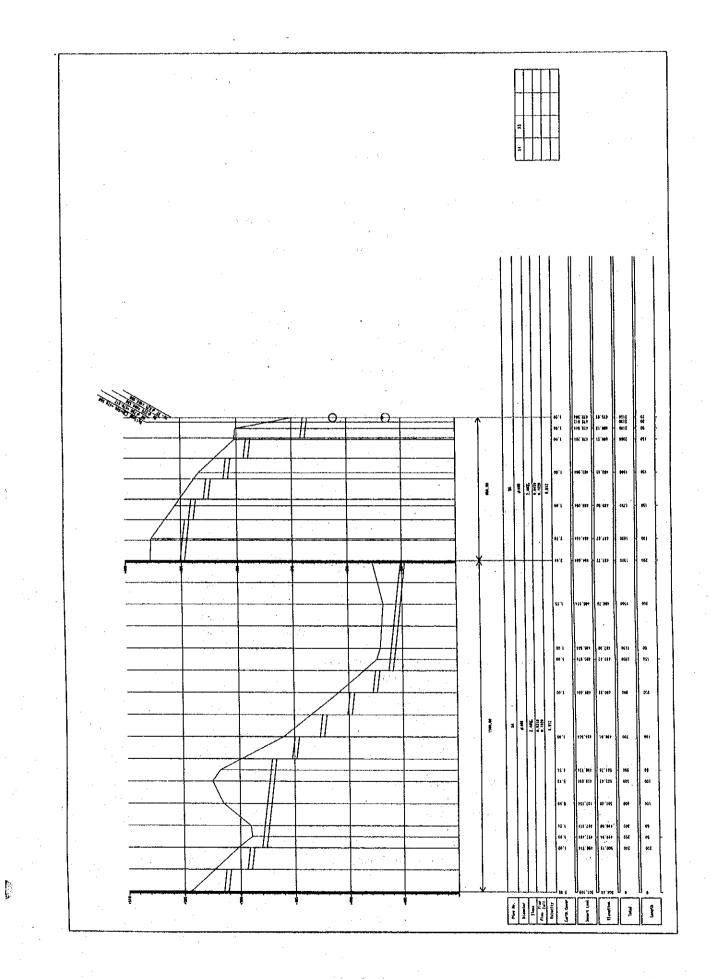




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Appendix 13.3 Pumping Equipment-Capacity Caluculation Kandy

Total Capacity	.2 (Kandy Lake)	605 m3	8/day=		0.42	m3/n	nin
Quantity of pump	1			t for s	tand-by		
Pump Capacity		605 m3			una oj		
rump capaeny	Q =	0.420 m3					
		0.0070 m3					
	q =	0.0070 III.	<i>Jscc</i>				
Diameter	Diameter = 146*	*(Q/v)^(1/2)					
		77 m			55	mm	
	=	65 m	n				
	where,v=	1.50	to		3.00		
Total Head	Total Head H=h	1.1.67.1.62			12.3	F (1)	
1 otal meau	Total Head H-B	17127110-	14	0 m	1.4.1.2	511	
			14.	o m	4.45	***	
	actual head h1 =				508.66		
		tion level hs					
		ivery level h			513.11	m	
	friction loss (Ha				pe		
	$h2 = 10.666 * c^{-1}$	-1.85*D^-4.8	37*q^1.3	85*L			
	=	6.51 m					
	where, c=	130					
	D=		m dia /1	000			
	L =	650 m					
		0.892 m					
			(acc)				
	friction loss : fit						
	$h3 = f * (v^2)$						
· ·	. =	1.34 m					
	where, $v =$	2.11 m					c
	where,		Q'ty		f/pc		f
	check valve			1	1.50		1.5
	sluice valve			2	0.10		0.2
	increase			0	0.15		0.0
	90deg			5	0.18		0.9
	tee			2	1.15		2.3
	outlet			1	1.00		1.0
		1			total		5.9
· · · ·		•					
Motor Output	Motor Output =			1+a)			
	—	1.8 k					
	=	2.2 k	W 💠				
	where,r=	1.00					
	e≖	0.60					
	a=	0.15			5. S		
Specification					·		
Туре	Submersible Se						
	65 m						
Diameter							
Capacity	0.42 m					•	
Head	14.0 m						
Motor Outpu							
Quantity	1 se	ts + 1 set for	standby	y			

A-13.3-1

2. Sewage Treatment P	lant (Large)							
Total Capacity		23,613	m3/d	lay≕		16.40	m3/m	in
Quantity of pump		2	sets -	+ 1 set 1	for sta	and-by		
Pump Capacity		11,807	m3/d	lay				
	Q =	8,199						
	q ≕	0.1366						
	1							
Diameter	Diameter = 14					~ ~ ~	н., с.	
	=			to		241	mm	
			mm					
	where,v=	1.50		to		3.00		
Total Head	Total Head H	=h1+h2+h3	=			12.2	m	
Totut Hous				14.0	m			
	actual head hi	l = hd - hs	=			9.62	m	
		uction leve				465.38	m	
		lelivery lev		:		475.00		
	friction loss (I				ht viv			
,	h2 = 10.666*c					-		
		0.29		ų 1.0-				
	=							
	where, c=	130		1. 110	^^			
	D =			dia /10	00			
· ·	L =) m					
	(v=		m/se	ec)				
	friction loss :							
	$h3 = f * (v ^{)}$					1		
	=	2.33						
	where, $v =$	2.78	m/se					c
	where,			Q'ty		f/pc		f
	check valve				1.	1.50		1.50
	sluice valve				2	0.10		0.20
	increase				0	0.15		0.00
	90deg				5	0.18		0.90
	tee				2	1.15		2.30
	outlet				1.	1.00		1.00
						total		5.90
Motor Output	Motor Output	ı – ∕0 163*	•**I	J/e*/1.	(هـ			
Motor Output			9 kW	.40) (I)			
	· · · · · ·		kW					
	where,r=	1.00						
		0.60						
	e=	0.00						
•	a=	0.15	,					
Specification								
Туре	Submersible	Sewage Pu	mp					
Diameter	250		-			÷ .		
Capacity	8.2	m3/min						· .
Head	14.0							
Motor Output		kW						
Quantity		sets + 1 set	for st	andby				

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3. Sewage Treatment P	lant (Small)						
Total Capacity		23 613	m3/day≈		16 Å0	m3/min	
Quantity of pump						нэ/шн	
			sets $+1$ set		stand-by		
Pump Capacity	0		m3/day				
	Q =		m3/min				
	q =	0,0683	m3/sec				
Diameter	Diameter = 14	6*(Q/v)^(1	/2)				. .
	=		mm to		171	mm	
	=		mm				
	where,v=	1.50	to		3.00		
70 4 1 77. 1		11.10.10					
Total Head	Total Head H=	n1+n2+n3		~	11.3	m	
		=		.0 m			
	actual head h1				9.62		
		ection level			465.38		
		elivery leve			475.00	m	
	friction loss (H	lazen Willi	ams) :strai	ght pi	pe		•
	h2 = 10.666*c						
	=	0.29	-				
	where, c=	130					
	D =		mm dia /1	1000			
	L=		m				
	(v=		m/sec)		1.1.1		
	friction loss : f		m/sec}		s.		. •
		-					
	$h3 = f * (v^2)$				•.		
		1.42		. ,			
	where, $v =$	2.17	m/sec			_	
	where,		Q'ty	· .	f/pc	f	
	check valve			1	1.50		50
	sluice valve			2	0.10		20
	increase			0	0.15	0.	00
	90deg			5 -	0.18	0.	90
	tee			2	1.15	2.	30 🦾
	outlet			1	1.00	1.	00
					total	5.	90
Matur Output	Martin Ordenad	(0.1/0.*	*****				ta ta a
Motor Output	Motor Output	•		т+а)			. *
		17.9					
	=	18.5	K₩ .				
	where,r=	1.00			· · ·		8 - M.S.A.
	e=	0.60					
	a=	0.15			÷		-
Specification							
Туре	Submersible S	awa ao Du-			the state	t i s	1.1.1 I.
Diameter			ıh			e i seco	
	200 n						•
Capacity		13/min					·
Head	14.0 n						
Motor Output	18.5 k			-			
Quantity	4 s	ets + 1 set :	for standby	7	· · · ·		

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Appendix 13.4 Sewage Treatment Plant - Capacity Calculation CAPACITY CALCULATION OF FACILITIES (Uxidation Ditcn)

1 BASIC CONDITIONS

1-1 BASIC ITEMS

- (1) Name : Kandy Sewage Treatment Plant
- (2) Land Area: Approximately1.00 ha(3) Elevation: 474.000 m
- (4) Inlet Pipe Level : 465.883 m
- (5) Pipe Diameter : 600 m
- (6) Land Use : Paddy Field
- (7) Collection System : Seperate Type
- (8) Treatment Method : Sewage Treatment : Oxidation Ditch Method Sludge Treatment : Sludge Digestion and Drying Bed
- (9) Effluent Point : Mada Ela River
- (10) Effluent Point Water Level : 470.640 m
 (11) Target Year : Year 2005 (Phase 1)
- (12) Lowest Monthly Average Temperature 23.6 °C (January)
 - کر ان ہے کہ ڈی جانوع کر ڈیل ہوں۔ ایک ان میں میں ان میں ان میں ان ہوتا ہے کہ ان میں ان میں ان ان ان ان ان میں ا

1-2 Design Population

Design Population : 19,260 Persons (Total)

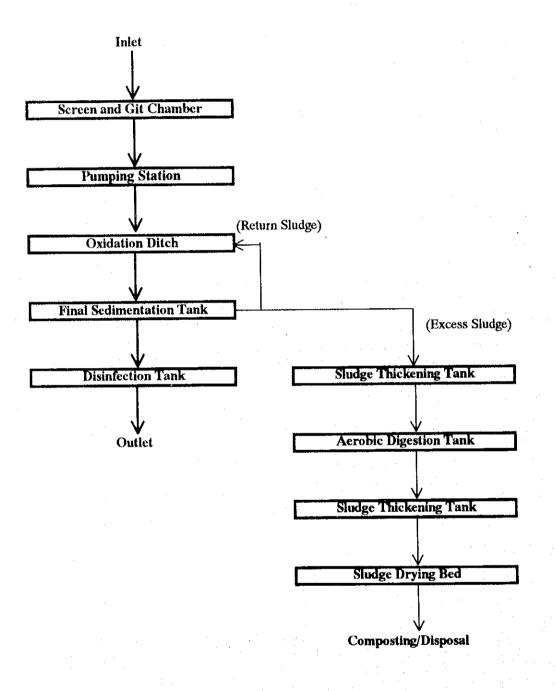
1-3 Design Sewage Flow

ITEM	m3/day	m3/hr	m3/min	m3/sec
Daily Average	6,950	289.6	4.83	0.080
Daily Maximum	8,500	354.2	5.90	0.098
Hourly Maximum	11,550	481.3	8.02	0.134

1-4 Design Sewage Quality

	ITEM	INFLUENT (mg/L)	EFFLUENT (mg/L)	REMOVAL RATIO (%)	REMARKS
Γ	BOD	240	30	88	
Γ	SS	250	50	80	

1-5 Flow Chart (Oxidation Ditch)



A-13.4-2

1-6 Design Criteria for Oxidation Ditch

Г	TTEMS	UNIT	Formula or Value	Application
1-6-1 Oxidatio	n Ditch			
 (3) Return S (4) Water D (5) Width (6) Retention 	oncentration ludge Ratio epth n Time Requirement	kg/kg/day mg/i % m m hour kgO2/kgBOD day	$\begin{array}{c} 0.03 - 0.05 \\ 3,000 - 4,000 \\ 100 - 200 \\ 1.0 - 3.0 \\ 2.0 - 6.0 \\ 24 - 48 \\ 1.4 - 2.2 \\ 8 - 50 \end{array}$	0.05 4,000 150 Same as Left Same as Left Same as Left 2.0 Same as Left
1-6-2 Final Se	dimentation Tank			
 Water S Retentio Water D 		m3/m2/day hour m	8 - 12 6.0 - 12.0 3.0 - 4.0	8 - 12 Same as Left 3.0
1-6-3 Disinfec	tion Tank			
 (1) Retention (2) Dosage 	n Time	min. mg/l	> 15 2.0 - 4.0	15 3.0
1-6-4 Sludge	Thickening Tank			
(1) Solid M(2) Water I	atter Load Depth	kg/m2/day m	60 - 90 Approximately 4.0	70 4.0
1-6-5 Aerobic	Digestion Tank		· · · · · · · · · · · · · · · · · · ·	
(1) Retention(2) Solid M	on Time atter Load	day kg/m2/day	10.0 - 15.0 1.60 - 4.81	Same as Left Same as Left
1-6-6 Sludge	Drying Bed		1	
(1) Drying(2) Depth of		day m	15 - 30 0.3 - 1.0	20 0.3

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2 CAPACITY CALCULATION 2-1 Oxidation Ditch (Daily Maximum)

ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре		-	Re-circulation Flow Type	
Design Flow	Q1	m3/day	-	8,500
	Q2	m3/hr	1	354.2
Basin Number	BN	Basin	-	3
Inlet BOD Quality	С	mg/L	-	240
Inlet SS Quality	- S	mg/L		250
Inlet BOD Matter	М	kg/day	Q1*C*10^-3	2,040
BOD-SS Load	BS	kg/kg/day	• · · · · · · · · · · · · · · · · · · ·	0.05
MLSS Concentration	SS	mg/L		4,000
Required Volume	V1	m3	M/(SS*BS*10^-3)	10,200
Therefore	V2	m3	and the second	10,200
Retention Time	T	hr	(V2/Q1)*24	28.8
Return Sludge Ratio	R1	%	_	150
	R2	- -	R1/100	1.5
Return Sludge Quality	RS1	mg/L	(SS*(1+R2)-C)/R2	6,507
Therefore	RS2	mg/L	-	6,510
Sludge Age	SA	day	SS*V2/(Q1*S)	19.2
Width	W	m	-	6.0
Water Depth	H	m	n 🕳 ser en	3.0
Length	L1	m	(V2/BN)/(W*H)	188.9
Therefore		m	••	190.0
Dimension (Width)	W	m	W	6.0
(Depth) H	m	Н	3.0
(Length) <u>L</u>	m	L2	190.0
(Basin Number) -	basin	BN	3
Required Oxygen	O2-day	kgO2/day	Q1*C*10^-3*2.0	4,080.0
	O2-hr	kgO2/hr	(O2-day)/24	170.0
Aerator Motor Output		kW	O2-hr/1.9	89.5
		kW		90.0
Aerator Type		-	Slanting Shaft Screw Aerator	
Check		UNIT	APPLICATION	RESULT
Retention Time		hour	24 -48	29.0
Oxygen Supply		kgO2/kg	1.4 - 2.2	2.0
Sludge Age		day	8 - 50	19.2

A-13.4-4

2-2 Final Scdimentation Tank (Daily Maximum)

THEM		SIGN	UNIT	CALCULATION	RESULT
Туре		· _	-	Radial Flow Circular Type	
Design Flow		Q1	m3/day	_	8,500
0	ľ	Q2	m3/sec		354.17
Basin Number	Ì	BN	Basin	~	3
Water Surface Load	-	L.	m3/m2/day	4.14*10^4*T^0.95*SS^-1.35	11.4
T	erefore	L	m3/m2/day		12.0
Required Surface Area	1	A1	m2	Q1/L	708.3
1	[A2	m2/Basin	A1/BN	236.1
Water Depth		H	m		3.0
Diameter		D1	m	(A2/3.14)^0.5*2	17.3
T	nerefore	D2	m		16.0
Dimension	(Diam	D	m	D2	16.0
	(Depth)	H	m	Н	3.0
(Basin N	lumber)	- .	Basin	BN	
Sludge Collector Type		-	~	Central Drive Type	
Check	الأغنية منطقي بهديها		UNIT	APPLICATION	RESULT
Water Surface Load			m3/m2/day		14.1
Retention Time			hour	6.0 - 12.0	3.4

2-3 Disinfection Tank (Daily Maximum)

ITEM		SIGN	UNIT	CALCULATION	RESULT
Chemical Type		.	-	Chlorination Type	
Design Flow		Q1	m3/day	-	8,500
•	F	Q2	m3/min	-	5.90
Retention Time		T	min.	-	15.0
Basin Number		BN	basin	-	1
Required Volume		V	m3	Q2*T	89
Width		W	m	-	3.00
Water Depth		Н	m		1.50
Length		L1	m	V/(W*H)	19.676
Ŭ	therefore	L2	m	-	20.00
Dosage		D	mg/L		2.0
Required Chemical		RC1	kg/day	Q1*D*10^-3/C	17.00
	Therefore	RC2	kg/hr	RC1/24	0.71
Dimension	(Wi	W	m	W	3.(
	(Length)	L	m	L2	20.0
	(Depth)	Н	m	Н	1.5
	(Basin)	BN	basin		
Chlorine Feeder		-	unit	including 1 for stand-by	
Check	****		UNIT	APPLICATION	RESULT
Retention Time	T		min.	15	15.

ПЕМ	SIGN	UNIT	CALCULATION	RESULT
Турс	- '	-	Radial Flow Circular Type	
Design Flow	Q1	m3/day	-	8,500
	Q2	m3/hr	-	289.6
Basin Number	BN	Basin	-	
Inlet SS Quality	С	mg/L	-	250
Removal Ratio	R 1	%		80
	R2	**	R1/100	0.80
Sludge Generation Ratio	SG1	%	-	75
(Oxidation Ditch)	SG2		SG1/100	0.75
Inlet SS Matter	М	kg/day	Q1*C*R2*SG2*10^-3	1,275
Solid Matter Load	L	kg/m2/day	-	70.0
Required Surface Area	A1	m2	M/L	18.2
	A2	m2/Basin	A1/BN	18.2
Water Depth	H .	m	-	4.0
Diameter	D1	m	(A2/3.14)^0.5*2	4.8
Therefore	D2	m	-	5.0
Dimension (D	m	D2	5.0
(Depth)	H	m	Н	4.(
(Basin)	Basin	Basin	BN	1
Check		UNIT	APPLICATION	RESULT
Solid Matter Load		kg/m2/day	70	65.0

2-4 Sludge Thickening Tank (Daily Maximum)

2-5 Aerobic Sludge Digestion Tank (Daily Maximum)

ITEM	SIGN	UNIT	CALCULATION	RESULT
Туре	- [-	Circular Type	
Basin Number	BN	Basin	-	1
Design Flow	Q1	m3/day	-	8,500
Inlet SS Matter	М	kg/day		1,275
Moisture Content	G	%	-	97,5
Sludge Volume	V1	m3/day	M*100/(100-G)	. 51.0
Temperature - Summer	TS	°C	-	26.5
- Winter	TW	°C	-	23.6
Temperature - Sludge Age	TSA	day-°C	VolatileSolidReduction=40%	470
Sludge Age	SA	day	TSA/TS	19.9
Total Mass of VSS	VSS	kg/day	0.8*M	1,020
VSS Reduction - Summer (41%)	VRS	kg/day	VSS*0.4	408.0
- Winter (40%)	VRW	kg/day	VSS*0.41	418.2
Required Volume	V	m3	V1/0.7/(0.125*0.8+1/SA)	485
Water Depth	H -	m		4.0
Diameter	D1	m	(A2/3.14)^0.5*2	12.4
Therefore	D2	m	-	13.0
Dimension (D	m	D2	13.0
(Depth)	H	m	H	4.0
(Basin)	Basin	Basin	BN	1
Required Oxygen	RO	kgO2/day	2.3*VRS	938.4
Required Air	RA	kg-Air/hr	RO/(0.1*0.233*1.293)/1440	1,297.8
Check		UNIT	APPLICATION	RESULT
Retention Time		day	10.0 - 15.0	10.4
Solid Matter Load		kg/m3/day	1.60 - 4.81	2.4

A-13.4-6

2-6 Sludge Thickening Tank (Daily Maximum)

TEM	SIGN	UNIT	CALCULATION	RESULT
Туре	*	-	Radial Flow Circular Type	
Basin Number	BN	Basin		1
Inlet SS Matter to Digestion	M1	kg/day	-	1,275
Removal Ratio at Digestion	R 1	%	-	40%
Inlet SS Matter	M2	kg/day	M1*(1-R1)	765
Moisture Content	G	%	-	99.0
Sludge Volume	V1	m3/day	M2*100/(100-G)	76.5
Solid Matter Load	L	kg/m2/day	-	70.0
Required Surface Area	A1	m2	M/L	10.9
1	A2	m2/Basin	A1/BN	10.9
Water Depth	Н	m	-	4.0
Diameter	D1	m	(A2/3.14)^0.5*2	3.7
Therefore	D2	m	-	5.0
Dimension (D	m	D2	5.0
(Depth)	Н	m	Н	4.0
(Basin)	Basin	Basin	BN	1
Check		UNIT	APPLICATION	RESULT
Solid Matter Load	i .	kg/m2/day	70	39.0

2-7 Sludge Drying Bed (Daily Maxmum)

ITEM		SIGN	UNIT	CALCULATION	RESULT
Design Flow		Q1	m3/day		8,500
Inlet SS Matter		M1	kg/day	Q1*C*R2*10^-3	765
		M2	t/day	M1/1000	0.765
Moisture Content		G	%	-	97.0
Sludge Volume		V1	m3/day	M2*100/(100-G)	25.5
Drying Period		P	day	-	10
Required Volume		V2	m3/day	V1*P	255.0
Depth of Bed		H	m		0.3
Required Area		A	m2	V2/H	850
Unit Number		UN	Unit	-	10
Width per Unit		W	m	-	6.0
Length per Unit		L1	m	A/(UN*W)	14.2
· · ·	Therefore	L2	m	-	14,5
Dimension	(Width)	W	m	W	6.0
	(Length)	L	m	1.2	14.5
	(Depth)	Н	m	Н	0.3
	(Basin)	Basin	Basin	BN	10.0
Check			UNIT	APPLICATION	RESULT
Drying Period			day	20	10.2

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Appendix 13.5 Hydraulic Calculation

1. Design Condition

1.1 Design Wastewater Quantity

Flow		m ³ /day	m ³ /hour	m ³ /min	m ³ /sec
Daily Average	Qd-ave	6,950	289.6	4.826	0.080
Daily Maxmum	Qd-max	8,500	354.2	5.903	0.098
Hourly Maximum	Qh-max	11,550	481.3	8.021	0.134

1.2 Unit and Capacity of Treatment Facilities

Facilities	Total	Duty	Stand-by	Capacity
Grit Chamber/Screen	2	2	1	Qhw-max
Oxydation Ditch	3	3	0	Qd-ave
Sedimentation Tank	3	. 3	0	Qd-ave
Disinfection Tank	1	1	0	Qd-ave

1.3 Discharge

Discharge Point	Meda Ela
HWL	470.64 m

1.4 Formula for Hydraulic Calculation

a. Friction loss for streight pipe

Head Loss

Darcy-Weisbach

Head Loss
$$h = f * V^2 / (2 * g)$$

where, f1 = (0.02 + 1 / (2000 * D)) * (L / D)

b. Friction loss for fittings

 $h = f * V^{2} / (2 * g)$ where, f2 = 1.00 (Inlet)

f3 = 0.50 (Outet)

2. Hydraulic Calculation

2.1 Water Level of Disinfection Tank Effluent Cha	amber (WL1)
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Det	•					
n. ·			Qd-ave	Qd-max	Qh-max	(Unit)
Design l	Flow	Q	6,950	8,500	11,550	m ³ /day
		q	0.080	0,098	0,134	m ³ /sec
Pipe Dia	ameter		300	mm		
Pipe Lei	ngth		50.0	m		
No. of P	Pipe		1	set		
Velocity	1	V =	1.14	1.39	1.89	m/sec
Hydraul	lic Loss	h =	f * V ^ 2 / (2	ι*g)		
		where,	f1 =	(0.02 + 1/(2000 * D)) *	(L/D)
				3.6111E-06	(Straight Pipe))
			f2 =	1.00	(Inlet)	
			f3 =	0.50	(Outet)	
Hydrau	lic Loss	h1 =	0.099	0.148	0.274 r	n
	WL1 =	470.640	+ h1 =	470.788	470.914 r	n
			say,	470.79	470.92 r	n
			· · · · ·	(Qd-max)	(Qh-max)	
				``		
iter Level	of Disinf	ection Tank (V	WL2)			
Weir W		W =	,	m		
No. of V	Weir	- -	. 1	set		
Weir lev	1 A A A A A	hw =	473.10	m		
	w height	h=	(Q/(1.84 *	W))^(2/3)		
		h2 =	0.124	0.142	0.174 r	n
			hw + h2 =	473.242	473.274 r	n
	WL2 =					
	WL2 =		say,	473.25	473.28 r	
	WL2 =				1	
	WL2 =			473.25 (Qd-max)	1	
iter Level		l Water Efflue	say,	(Qd-max)	1	
1	of Settlec	l Water Efflue	say, ent Chamber ((Qd-max) WL3)	1	
Pipe Di	of Settlec ameter	l Water Efflue	say, ent Chamber (200	(Qd-max) WL3) mm	1	
Pipe Di Pipe Le	of Settlec ameter ngth	l Water Efflue	say, ent Chamber (200 50.0	(Qd-max) WL3) mm m	1	
Pipe Di Pipe Le No. of I	of Settlec ameter ngth Pipe	l Water Efflue V =	say, ent Chamber (200 50.0 3	(Qd-max) WL3) mm m sets	(Qh-max)	n
Pipe Di Pipe Le No. of I Velocity	of Settlec ameter ngth Pipe	V =	say, ent Chamber (200 50.0 3 0.85	(Qd-max) WL3) mm m sets 1.04	(Qh-max)	
Pipe Di Pipe Le No. of I Velocity	of Settlec ameter ngth Pipe	<u>V =</u> h =	say, ent Chamber (200 50.0 3 0.85 f * V ^ 2 / (2	(Qd-max) WL3) mm sets 1.04 2 * g)	(Qh-max)	n m/sec
Pipe Di Pipe Le No. of I Velocity	of Settlec ameter ngth Pipe	V =	say, ent Chamber (200 50.0 3 0.85 f * V ^ 2 / (2 f1 =	(Qd-max) WL3) mm m sets 1.04 2 * g) (0.02 + 1 / ((Qh-max) 1.42 2000 * D)) *	n <u>m/sec</u> (L/D)
Pipe Di Pipe Le No. of I Velocity	of Settlec ameter ngth Pipe	<u>V =</u> h =	say, ent Chamber (200 50.0 3 0.85 f * V ^ 2 / (2 f1 = =	(Qd-max) WL3) mm m sets 1.04 2*g) (0.02 + 1 / (5.625E-06	(Qh-max) 1.42 2000 * D)) * (Straight Pipe	n <u>m/sec</u> (L/D)
Pipe Di Pipe Le No. of I Velocity	of Settlec ameter ngth Pipe	<u>V =</u> h =	say, ent Chamber (200 50.0 3 0.85 $f * V ^ 2 / (2)$ f1 = f2 =	(Qd-max) WL3) mm sets 2 * g) (0.02 + 1 / (5.625E-06 1.00	(Qh-max) <u>1.42</u> 2000 * D)) * (Straight Pipe (Inlet)	n <u>m/sec</u> (L/D)
Pipe Di Pipe Le No. of I Velocity	of Settlec ameter ngth Pipe Jic Loss	<u>V =</u> h =	say, ent Chamber (200 50.0 3 0.85 f * V ^ 2 / (2 f1 = =	(Qd-max) WL3) mm m sets 1.04 2*g) (0.02 + 1 / (5.625E-06 1.00 0.50	(Qh-max) 1.42 2000 * D)) * (Straight Pipe (Inlet) (Outet)	n <u>m/sec</u> (L/D)

(Qd-max) (Qh-max)

473.34

473.44 m

A-13.5-2

say,

2.4 Water Level of Scalimentation Tank Trough (W	L4)
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No. of Sedimentation	Tank	3 ta	inks		
Tank Diameter	D =	16.0 n	1		
Trough Length	L =	25.1 n	1		
Trough Width	B =	0.3 m	1 1	free fall	
Trough Level	hw =	473.50 n	n		
Critical Water Level	hcl = ((Q^2)/(g	*B^2))^	(1/3)	
· · ·	hcl =	0.093	0.107	0.131	m
Hydraulic Loss	h4 = (3	3)^(1/2)*1	ncl		
	h =	0.162	0.185	0.227	m
WL4 =	hw +	h4 =	473.685	473.727	m
		say,	473.69	473.73	m
			(Od-max)	(Oh-max)	

2.5 Water Level of Sedimentation Tank (WL5)

No. of Sedimenta	ation Tank	3	tanks				
Tank Diameter	a ta	16.0	m				
No. of Notches	(8 nos/m)	402	nos				
Weir level	hw =	473.98	m	,			1.1
Hydraulic Loss	h5 =	((Q/n)/1	.42) ^	(2/5)			1
[<u>h =</u>	0.019		0.020	0.023	m :	
WL5 =	•	hw + h5 =	4	74.000	474.003	m	
		say,		474.00	474.01	m [·] ··	
	:		(Q	d-max)	(Qh-max)		

2.6 Water Level of Oxidation Ditch Effluent Chamber (WL6)

Pipe Diameter		200 mi	n		•
Pipe Length		50.0 m			
No. of Pipe		3 set	is .		1.1.1
Velocity	V =	0.85	1.04	1.42	m/sec
Hydraulic Loss	h = f * T	V^2/(2*	g)		
	where,	f1 = (0	0.02 + 1/(2	2000 * D))	*(L/D)
· · · ·	· ·	=	5.625E-06 (Straight Pip	e)
		f2 =	1.00 (Inlet)	
· · · · ·		<u>f3 =</u>	0.50 (Outet)	* • •
Hydraulic Loss	h6 =	0.056	0.083	0.154	m
WL6 =	WL5 + +	h6 =	474.083	474.164	m
		say,	474.09	474.17	m
	· · · · ·	· .	(Qd-max)	(Qh-max)	

2.7 Water Level of Oxidation Ditch (WL7)						
No. of Sedimentation Tan	k	3 tank	S			
Weir Width	W =	1.0 m				
No. of Weir		1 set				
Weir level	hw = 4	74.33 m				
Overflow height	h = (Q/(1))	.84 * W))	^(2/3)			
	h2 =	0.060	0.068	0.084	m	
WL7 =	hw +	h7 =	174.398	474.414	m	
		say,	474.40	474.42	m	
		(Qd-max)	(Qh-max)		

2.8 Water Level of Distribution Chamber - Effluent (WL8)

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Pipe Diameter		200	mm			
Pipe Length	50.0 m					
No. of Pipe		3	sets			
Velocity	• V =	0.85	1.04	1.42	m/sec	
Hydraulic Loss	h = f '	* V ^ 2 / (2	*g)			
	where,	f1 =	(0.02 + 1)/(2000 * D))*	*(L/D)	
		=	5.625E-06	(Straight Pipe	*)	
		f2 =	1.00	(Inlet)		
· .		f3 =	0.50	(Outet)		
Hydraulic Loss	h6 =	0.056	0.083	0.154	m	
WL8 =	WL7 +	+ h8 =	474.483	474.574	m	
		say,	474.49	474.58	m	
			(Qd-max)	(Qh-max)		

2.9 Water Level of Distribution Influent (WL9)

No. of Sedimentation	Tank	3	sets		
Weir Width	W =	1.0	m		
No. of Weir		1	set		
Weir level	hw =	474.70	m .		
Overflow height	<u>h= (</u>	Q / (1.84 *	W))^(2/3)		
	h2 =	0.060	0.068	0.084	m
WL9 =	ł	1w + h9 =	474.768	474.784	m
		say,	474.77	474.79	m
			(Qd-max)	(Qh-max)	

2.10 Water Level of Grit Chamber Effluent Chamber (WL10)

Pipe Diameter	· ·	400 mm	l		
Pipe Length		50.0 m			
No. of Pipe		1 set	· · · · · · · · · · · · · · · · · · ·		
Velocity	V =	0.64	0.78	1.06	m/sec
Hydraulie Loss	h = f *	V^2/(2*g	;)		

	where, $fi = (0.02 + 1 / (2000 * D)) * (L / D)$					
		= 2.6563E-06 (Straight Pipe)				
		f2 =	1.00	(Inlet)		
		f3 =	0.50	(Outet)		
Hydraulic Loss	h6 =	0.031	0.047	0.087	m	
WL10 =	WL9 + +	h10 =	474.817	474.877	m	
		say,	474.82	474.88	m	
	1		(Qd-max)	(Qh-max)		

2.11 Water Level of Grit Chamber Influent Chamber (WL15)

	3 sets including 1 for standby				
h11 =	0.10 m	·			
WL10 +	h11 =	474.920	474.980 m		
	say,	474.92	474.98 m		
		(Od-max)	(Qh-max)		
		h11 = 0.10 m WL10 + $h11 =$	h11 = 0.10 m $WL10 + h11 = 474.920$		

Appendix 13.6 DRAWING

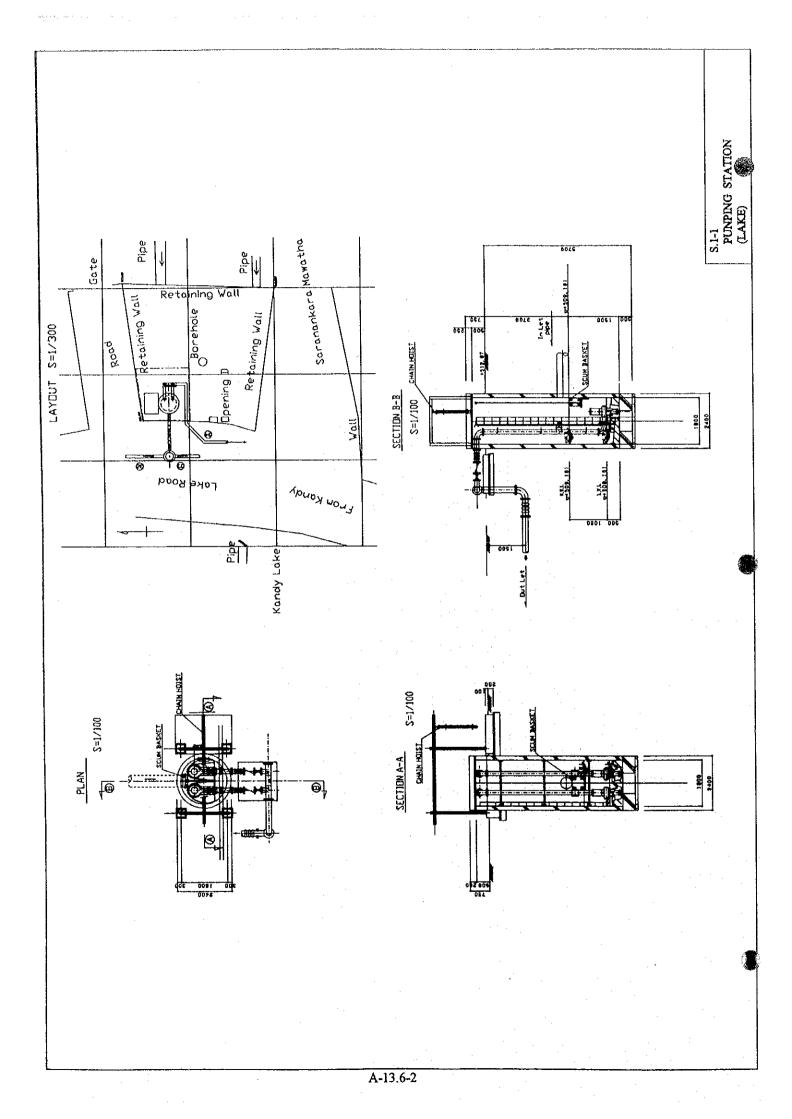
No.	DRAWING NAME
S.1-1	PUMP STATION (LAKE)
S.2-1	SEWAGE TREATMENT PLANT LAYOUT
S.2-2	HYDRAULIC PROFILE
S.2-3	FLOW DIAGRAM (1)
S.2-4	FLOW DIAGRAM (2)
S.2-5	PUMPING STATION (1)
S.2-6	PUMPING STATION (2)
S.2-7	OXIDATION DITCH
S.2-8	SEDIMENTATION BASIN
S.2-9	DISINFECTION TANK
S.2-10	RETURN SLUDGE PUMP ROOM
S.2-11	SLUDGE THICKENING TANK
S.2-12	AEROBIC SLUDGE DIGESTION TANK
S.2-13	SLUDGE DRYING BED LAYOUT
S.2-14	SLUDGE DRYING BED

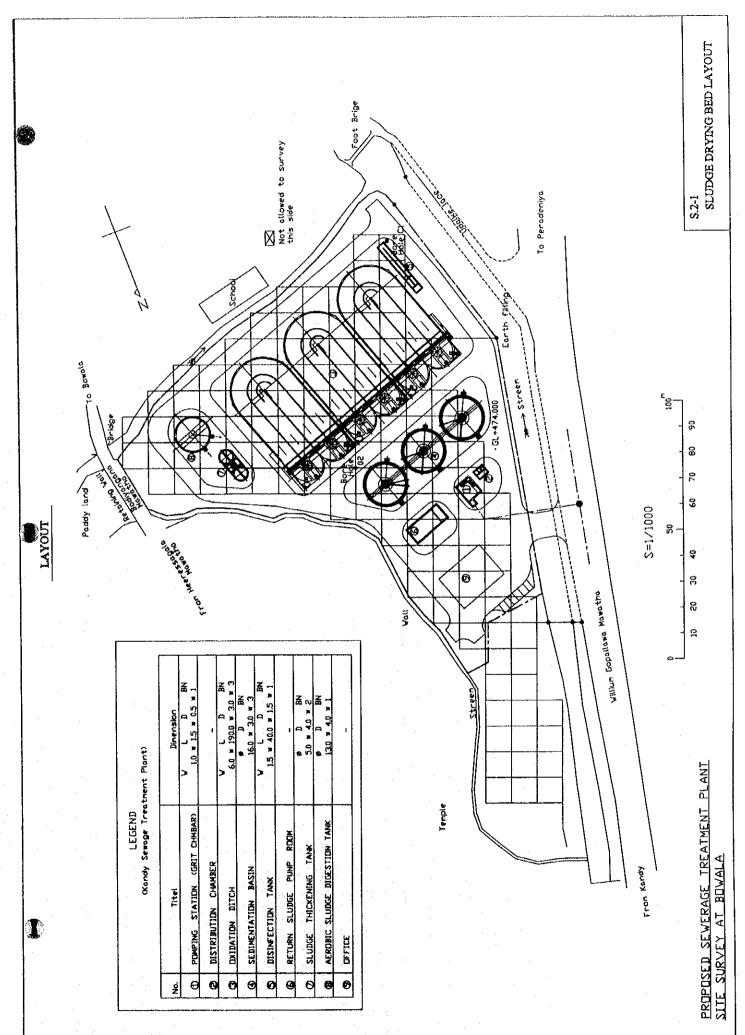
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Asia

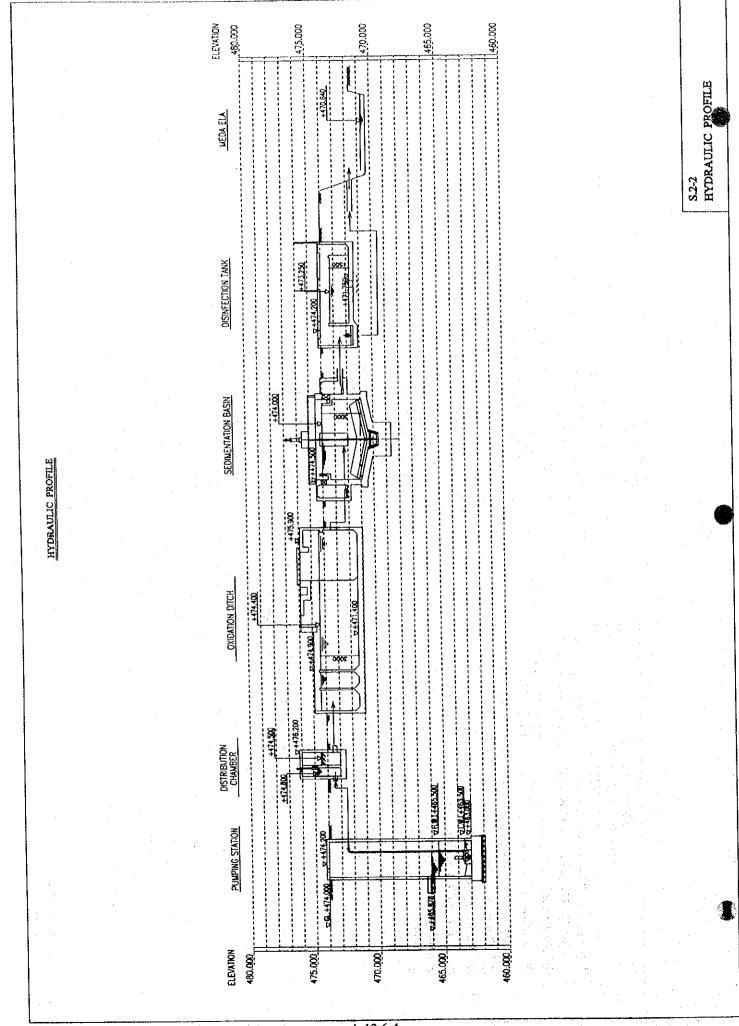
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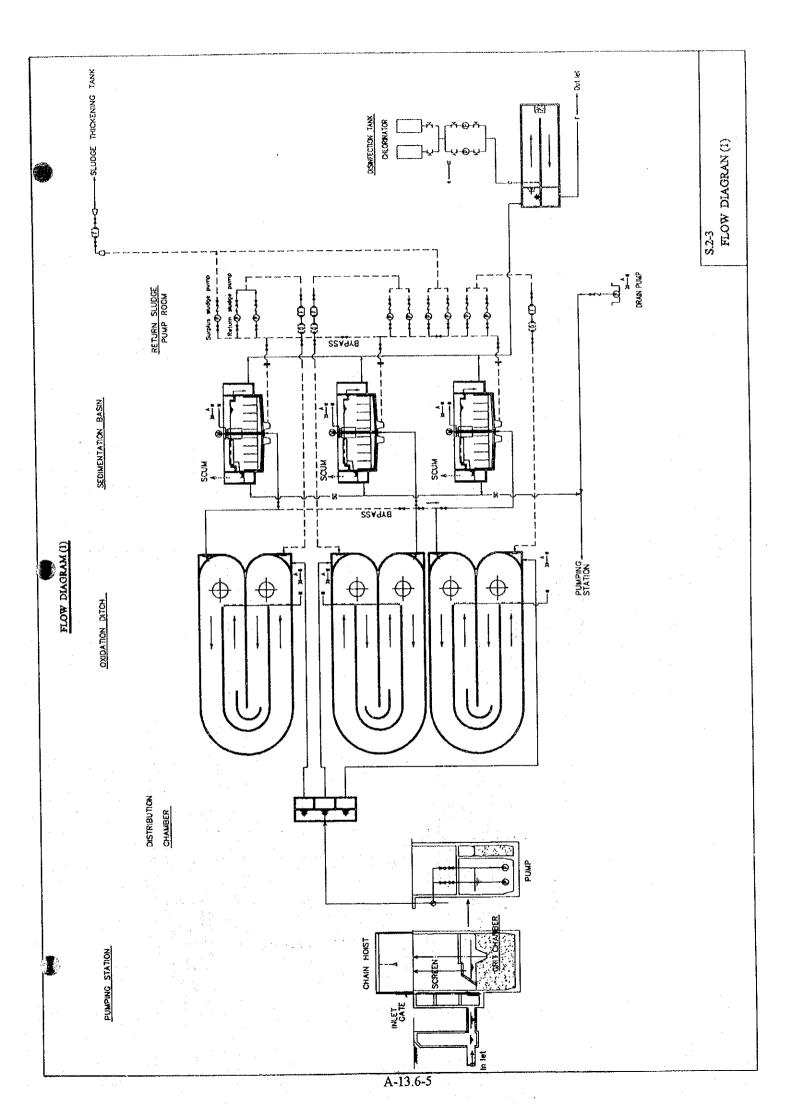
A-13.6-1

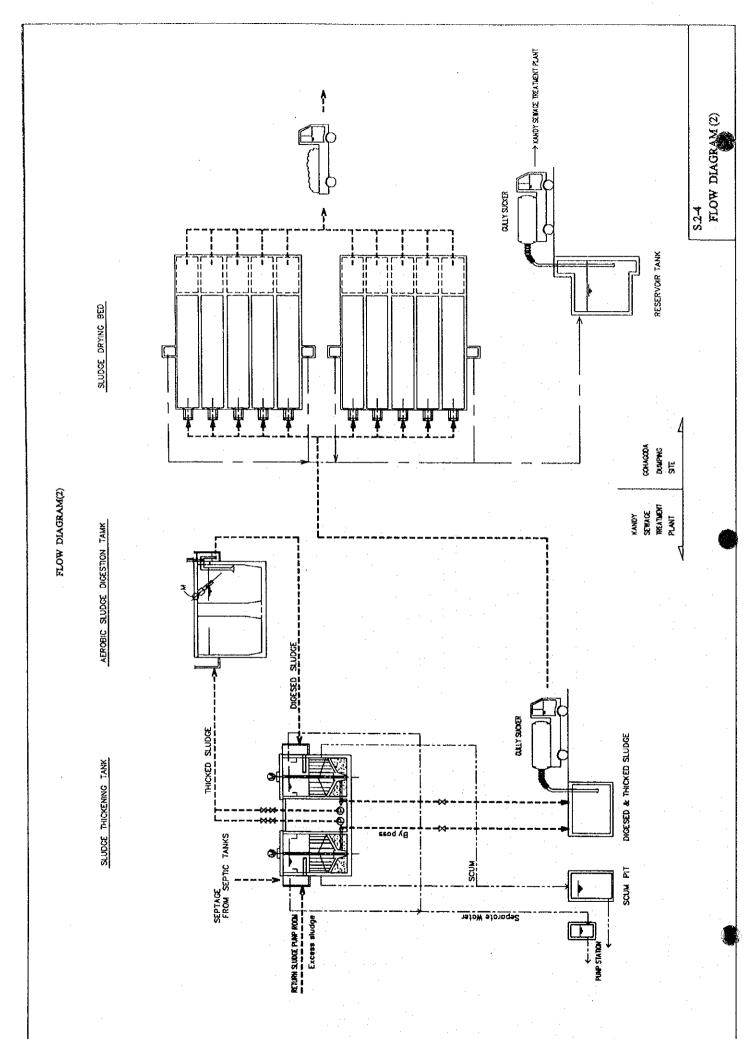


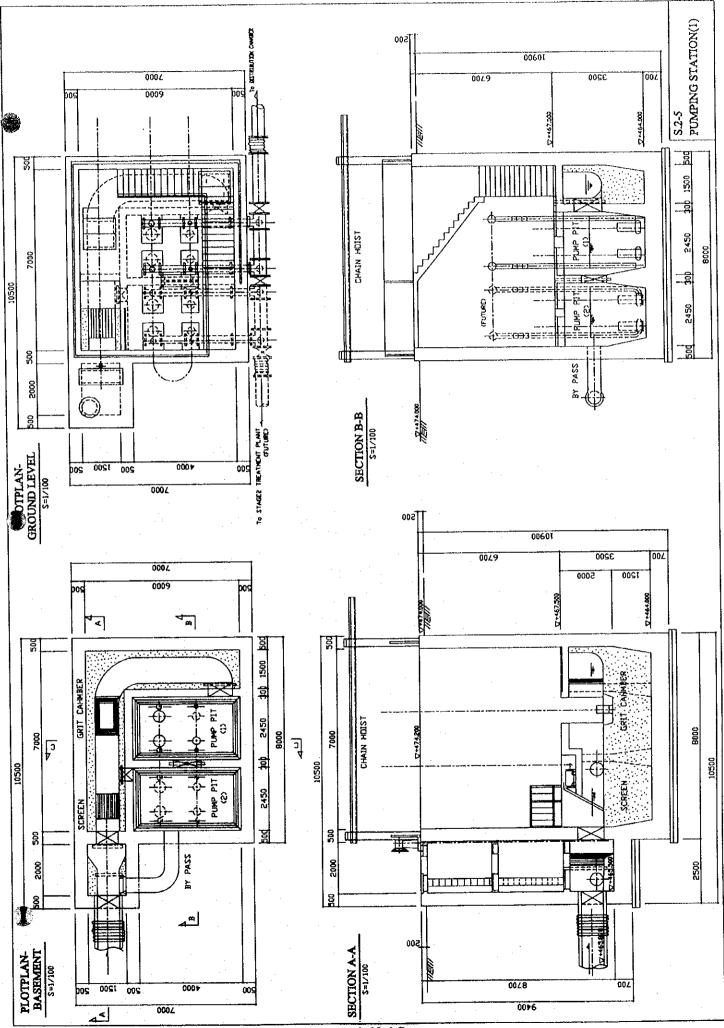


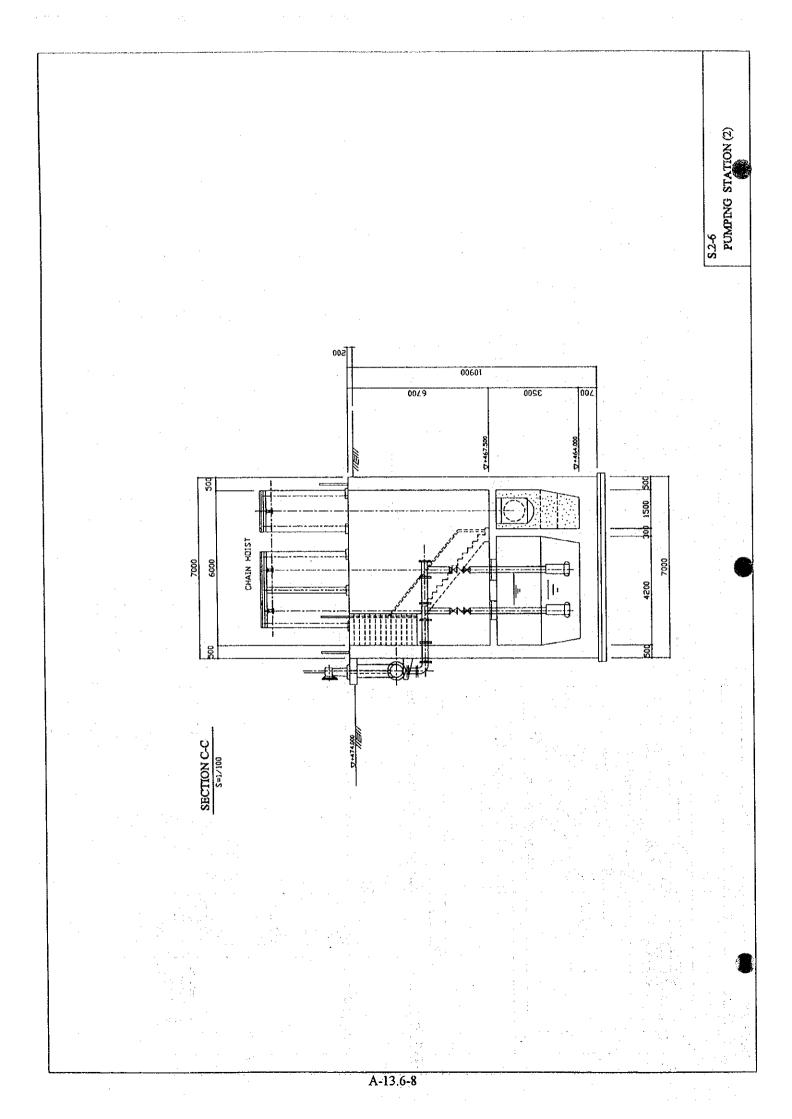
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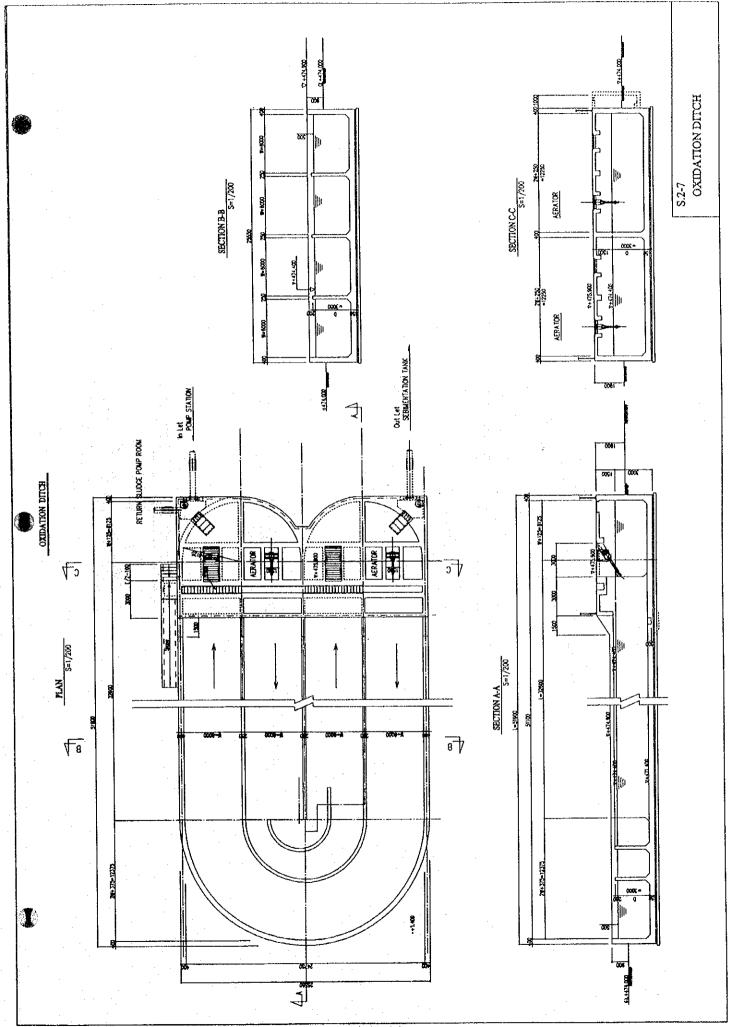


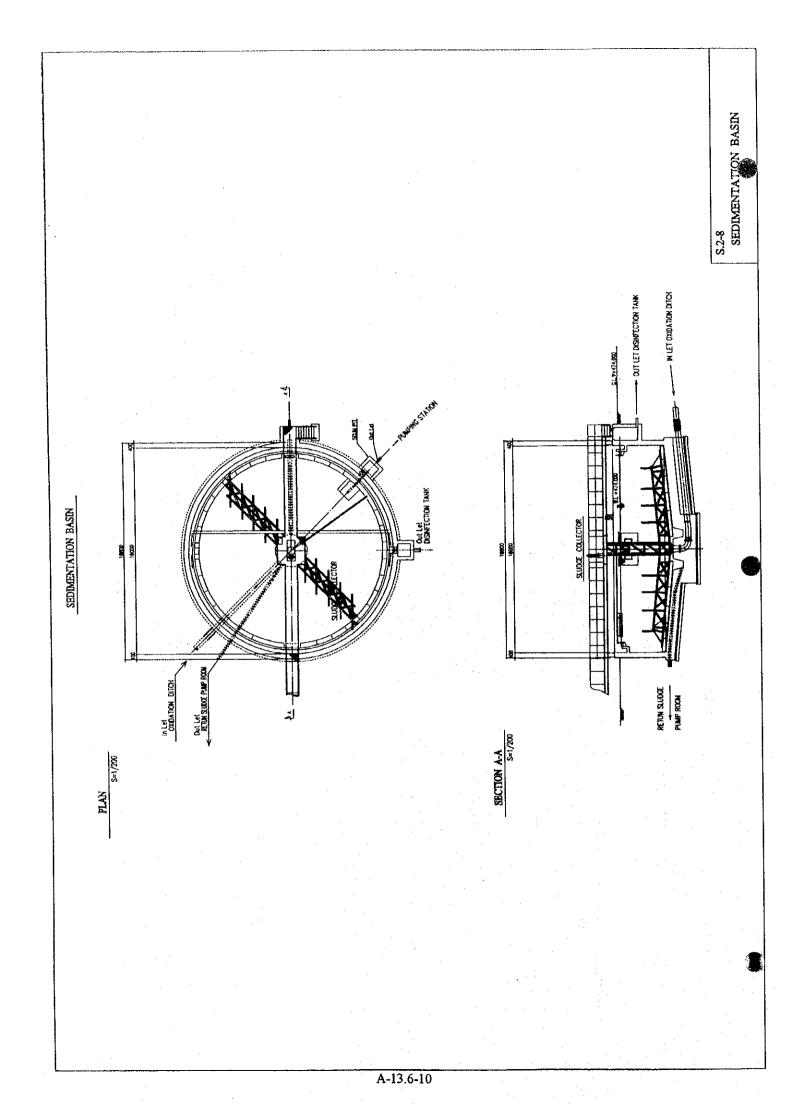


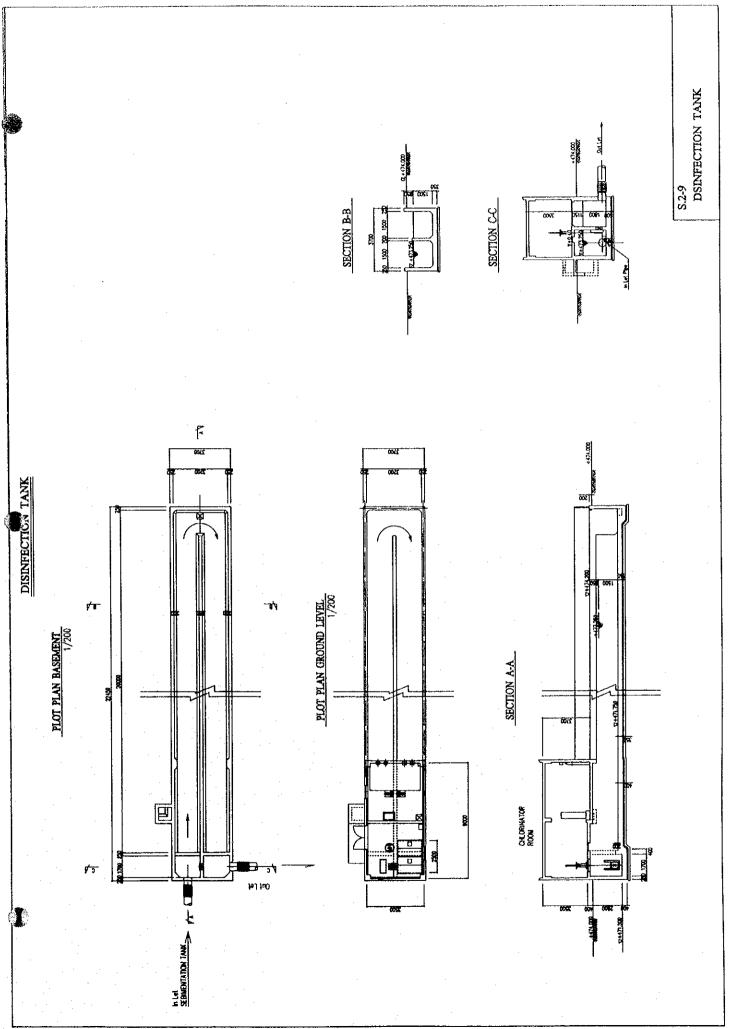








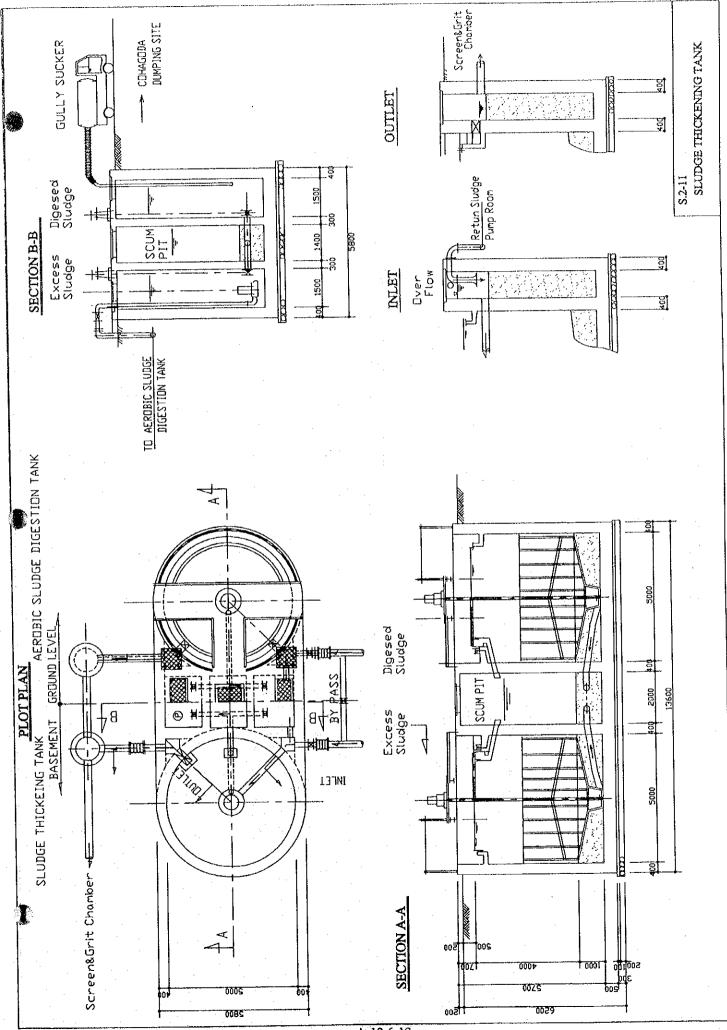




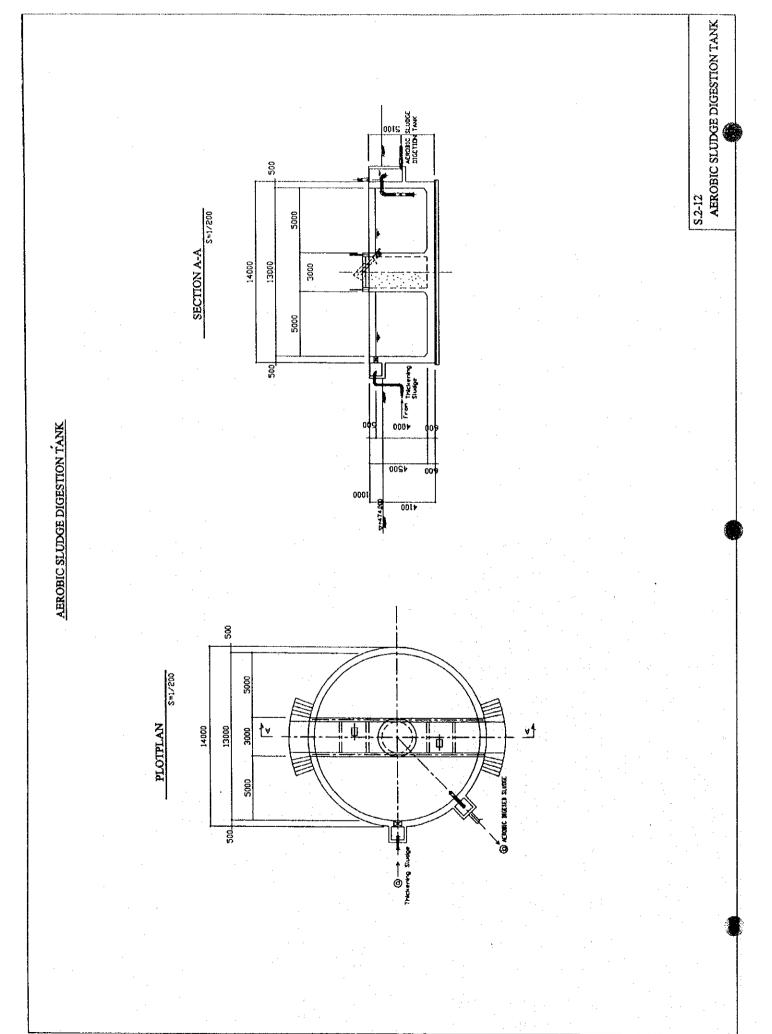
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S.2-10 RETURN SLUDGE PUNP ROOM 0005 0005 53 PLOT PLAN GROUND LEVEL SECTION B-B Æ 101121 00 88 | RETURN SLUDGE PUMP ROOM Surptus Sudge Pump telura Sudge Pump Relum Sudge Pump Surplus Sudge Pump 9 00 SEDMENTATION BASIN ¢C PLOT PLAN BASEMENT S=1/200 ____ SECTION A-A S=1/200 30 Э 71 8 0 3 8 mm CKIDATION DITCH ł

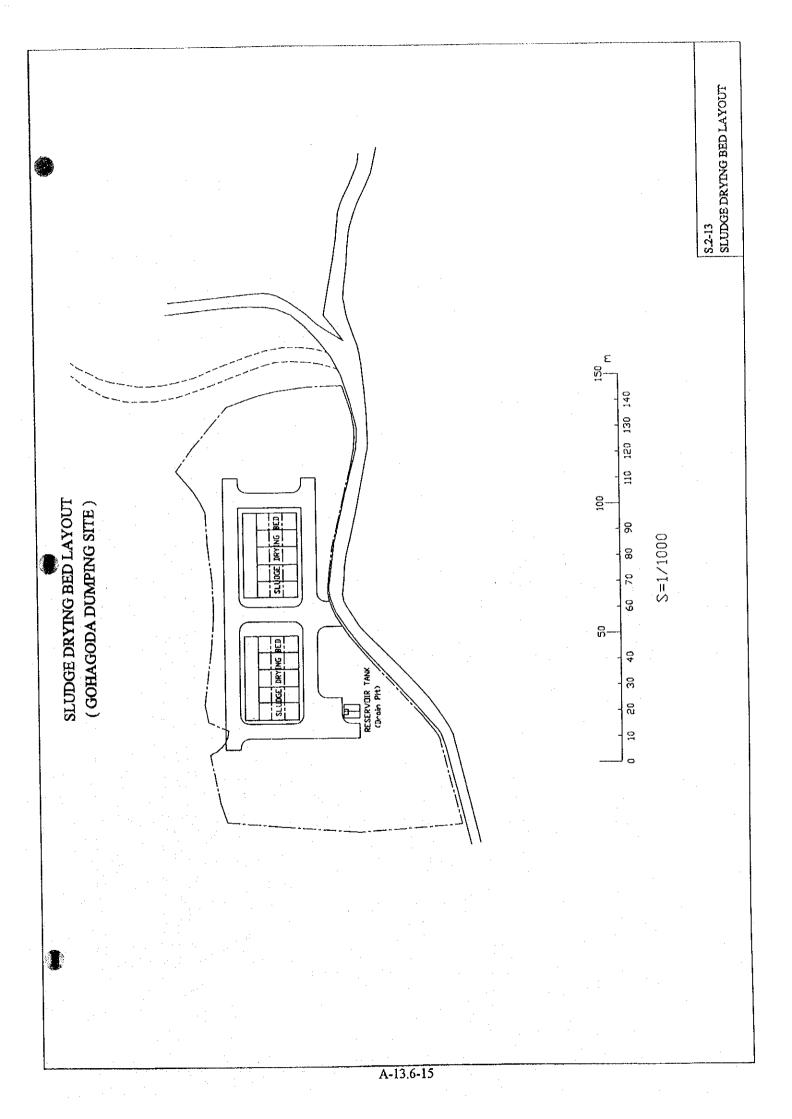
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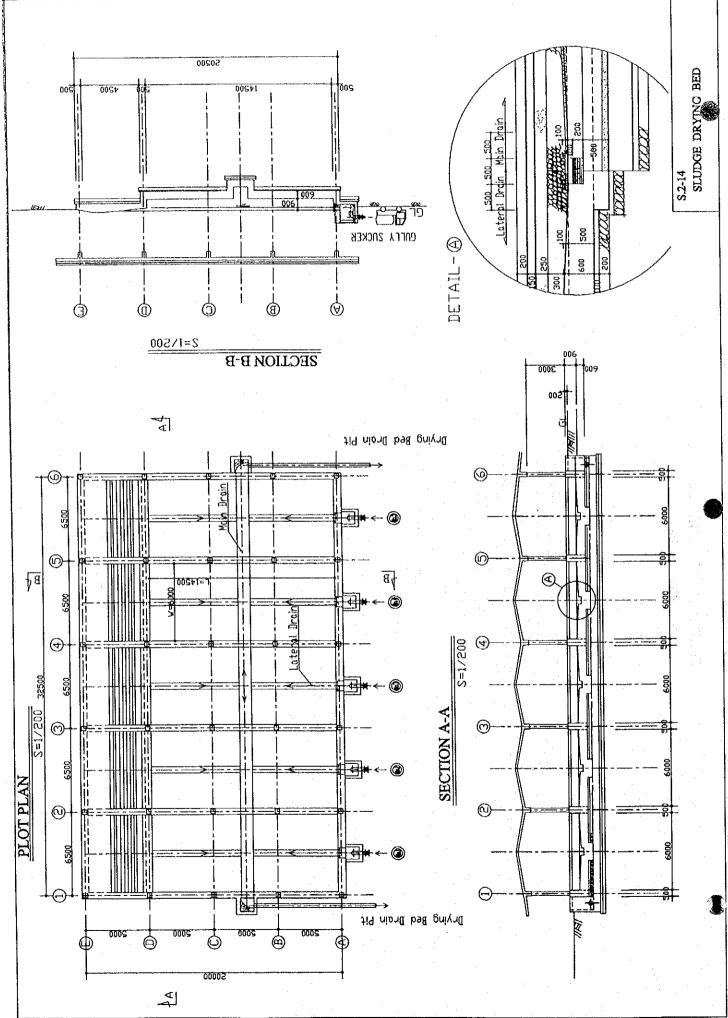


A-13.6-13



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Appendix 13.7 Storage Capacity of Sewer (Kandy)

Phase 1 (2005)

1 Pumping Station in Kandy STP

(1) Sewage Flow

 $Q_{HM} = 12,200 \text{ m}^3/\text{day} = 508 \text{ m}^3/\text{hour}$ (Hourly Maximum Sewage Flow to STP)

(2) Sewer to be used for Sewage

Since Pumping Station is located at GL+474m, sewers with invert level of +473m is considered to use for sewer storage. Length and Pipe Nos. of these sewers are as follows;

No. 57 ϕ 825. L= 50m (Allowance 50%)

No. 53 ϕ 750. L= 750m (Allowance 50%)

(3) Manhole

Nos. of Manhole $\frac{50+750}{50} = 16$ (50m pitch) Manhole Depth 475.01-470.817 = 4.2m (up to No.53)

- (4) Calculation of Storage Capacity
 - a) Sewer

$$\left[\frac{0.825^2 \times 3.14}{4} \times 50 + \frac{0.75^2 \times 3.14}{4} \times 750\right] \times (1 - \frac{1}{1.5}) = 119.3 \text{ m}^3$$

b) Manhole

$$\frac{1.2^2 \times 3.14}{4} \times (4.2 - 0.825) \times 16 \qquad \qquad \frac{= 61.0 \text{m}^3}{\text{Total} \quad 180.3 \text{m}^3}$$

(5) Storage Time

 $\frac{180.3\text{m}^3}{508\text{m}^3/\text{hour}} = 0.35 \text{ hour } = 20.9 \text{ min}$

2. Kandy Lake Pumping Station

(1) Sewage Flow

 $Q_{HM} = 0.0031 \text{ m}^3/\text{sec} = 11.16 \text{ m}^3/\text{hour}$

(Hourly Maximum Sewage Flow to Kandy Lake PS)

(2) Sewer to be used for Sewage

Since Pumping Station is located at GL+512.87m, sewers with invert level of +512.5m is considered to use for sewer storage. Length and Pipe Nos. of these sewers are as follows;

No.32. ϕ 150 L = 750m (Allowance 50%)

(3) Manhole

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Nos. of Manhole $\frac{750}{50} = 15$ (50m pitch) Manhole Depth 512.17-510.351 = 1.8 (Center of No. 32)

- (4) Calculation of Storage Capacity
 - a) Sewer

$$\frac{0.15^2 \times 3.14}{4} \times 750 \times (1 - \frac{1}{2.0}) = 6.6 \text{m}^3$$

b) Manhole

$$\frac{0.9^2 \times 3.14}{4} \times (1.8 \times 0.15) \times 15 = 15.7 \text{m}^3$$

Total 22.3m³

(5) Storage Time

 $\frac{22.3 \text{ m}^3}{11.16 \text{ m}^3/\text{hour}} = 2.0 \text{ hour } = \underline{120.0 \text{ min}}$