2.3.5 Final Flotation Test

(1) Bulk differential flotation

Under the best conditions obtained in the basic test of BDF, the final flotation test was carried out, with two-stage cleaning respectively in the bulk flotation section and the lead differential flotation section. The test comprised two parts, one without sulfidizer and the other using 100g/t of the same. The test flow sheet and the test results are shown in Fig.34 in Table 25, respectively.

The test findings are summarized as follows:

- 1) The two-stage cleaning in the bulk flotation section generally produced favorable results as far as the lead and zinc grades are concerned. However, pyrite in free particles were abundant in the zinc concentrate, indicating insufficient depression of pyrite in the bulk flotation. Further study on quantity of added lime in the bulk flotation cleaners is considered necessary.
- 2) Almost 85% of lead grading nearly 70% was recovered in concentrate of the first stage of the two-stage cleaning in the differential flotation. Under the microscope, however, sphalerite-chalcocite middling was abundantly distributed; therefore, two-stage cleaning is considered necessary for stabilizing flotation performance.
- 3) Sulfidizer was added to recover cerussite, non-sulfide lead component, which lowered the tailing grade but only insufficiently. Intentional recovery of non-sulfide component appears to be unfeasible.

(2) Straight-differential flotation

Under the best conditions obtained in the basic test of SDF, the final flotation test with two-stage cleaning in the lead flotation and in the zinc flotation sections was carried out. The test consisted of two parts: one without sufidizer and the other using 100g/t of it. The test flow sheet appears in Fig.35 and the test results in Table 26.

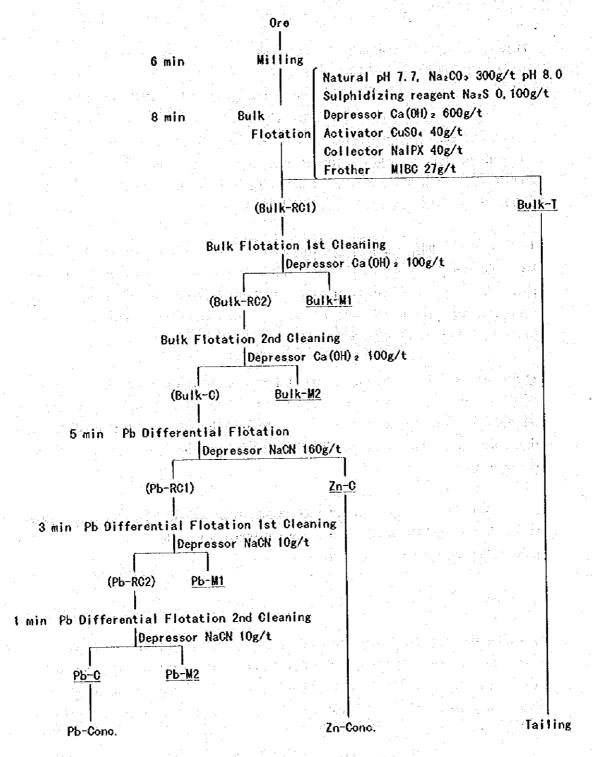


Fig. 34 Final Flotation Test Flowsheet (Bulk Differential Flotation)

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Table 25 Results of Final Flotation Test(Bulk Diffrential Flotation)

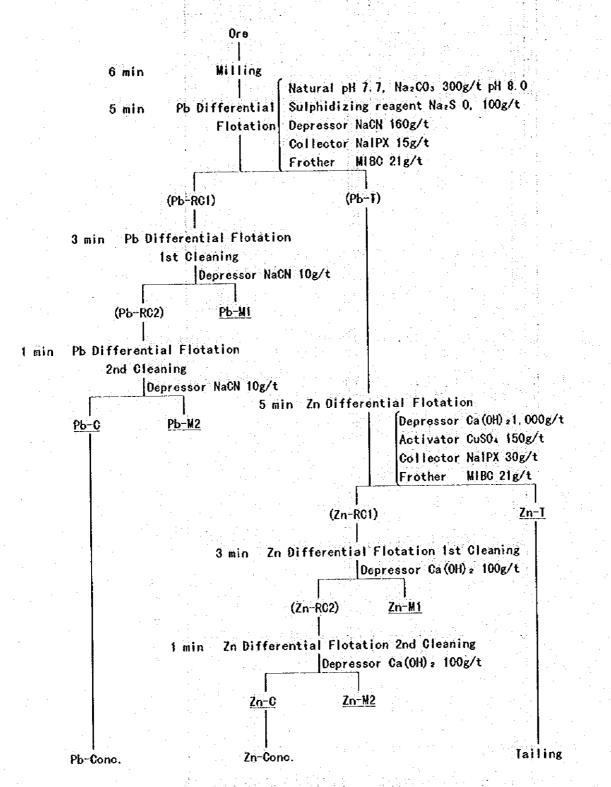


Fig. 35 Final Flotation Test Flowsheet (Straight Differential Flotation)

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Table 26 Results of Final Flotation Test(Straight Differential Flotation)

The test findings are summarized as follows:

- 1) In the second stage concentrate of the lead flotation(SDF), the lead grade reached 71% and the recovery 76%, indicating the zinc depression effect in the cleaners. In the lead concentrate, however, sphalerite grains in free particles were abundantly observed, while 40% of zinc was circulating in the cleaners. There still remains a question as to whether the two-stage cleaning can sufficiently depress and separate zinc.
- 2) 30% of zinc grading 50% was recovered in the concentrate of the two-stage cleaning in the zinc flotation. Under the microscope, galena in free particles was abundantly distributed in the zinc concentrate, which indicates insufficient separation in the lead flotation section. Compared to BDF, higher grade zinc in zinc concentrate was more easily recoverable, whereas the question of recovery still remains.
- 3) In relation to the sulfidizing effect, the tailing grade tended to decrease but only insufficiently; therefore, intentional recovery of non-sulfide component appears unfeasible.
- 4) In order to determine the number of stages of SDF and quantity of reagents added, locked tests or continuous tests have to be conducted, thereby clarifying zinc behavior in the lead flotation.

As compared to the performance of SDF, BDF demonstrated higher stability in the lead and zinc recovery, as the latter process recovers floatable zinc together with lead.

2.3.6 Settling test of concentrates and tailing

The Tsav area being situated in an arid land, there is no large water source in the vicinity. If the mine is put into development, mineral dressing water supply would be insufficient; therefore, water recycling must be contemplated. For this purpose, the settling rates of the concentrates and tailing were measured, which constitute the basic items for planning the mineral dressing water recycling.

For the settling test samples, the undersize(-200 mesh) of sieved bulk flotation tailing was prepared, which is assumed to substitute for the tailing slime fed to the tailing thickener, whereas, in substitution for the lead and zinc cencentrates fed to each concentrate thickeners, the concentrates produced from the flotation test were used without sieving because the quantity of the test products was small. The initial pulp density of respective samples, as the settling test condition, was determined at 10%. Flocculant was not used in the test.

The settling rate measurement is shown in Table 27, while Fig.36 \sim 38 indicate the relationship between the height of interface and the density of sediment by product and by measurement time.

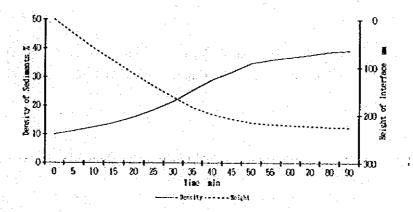


Fig. 36 Height of Interface and Density of Sediments (Tailing)

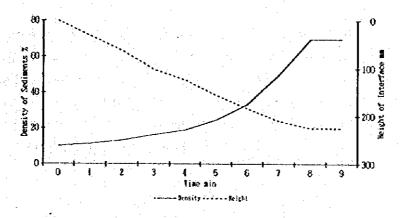


Fig. 37 Height of Interface and Density of Sediments(Pb-Conc.)

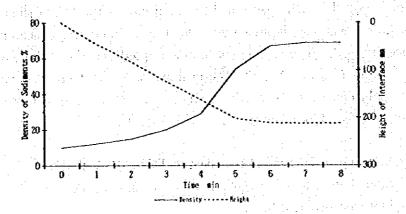


Fig. 38 Height of Interface and Density of Sediments (Zn-Conc.)

From the measurement in Fig.36 \sim 38, the settling rates for each sample to be thickened to certain densities of sediment are calculated as follows:

Tai	ling	Pb	Conc	Zn	Conc
Sediment density(%)	Settling rate(mm/min)	Sediment density(%)	Settling rate(mm/mln)	Sediment density(%)	
20	5.50	20	31.07	20	41.33
30	4.85	30	30.87	30	40.49
35	4. 26	40	30.38	40	40.45
		50	29.98	50	40.41

All the three types of the samples showed certain turbidity in the decanted water (the top water) influenced by clay minerals and fine slime contained but their settling characteristics appeared relatively good in view of the settling rates. Since the turbidity of the tailing slime was higher than that of the concentrates, it would probably be necessary, in the actual operation, to add high-molecular flocculant in the tailing thickener thereby lowering the turbidity of the decanted water.

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Table 27 Settling Rates

In turn, water quality analysis was made on the waters that are assumed to correspond to the decanted waters in the tailing thickener and the concentrates thickeners, which would be recycled in the actual operation, to judge if the water recycled from the thickeners would have any quality problems. The results of analysis are shown in Table 28.

	Overflow of	Overflow of	Overflow of
	Tailing	Pb Conc.	Zn Conc.
	Thickener	Thickener	Thickener
ρΗ	9.9	8. 2	9.6
Cu (ppm)	2. 7	0.15	1.6
Pb (ppm)	<0.02	<0.1	<0.04
Zn (ppm)	<0.02	<0.1	<0.04
T - F e (ppm)	<0.05	<0. 2	<0.1
Cd (ppm)	<0.01	<0.05	<0.02
As (ppm)	<0.02	<0.1	<0.05
CN (ppm)	<0.1	0.5	1.4
S O 4 (ppm)	582	25	121

Table 28 Water Quality Analysis of Decanted Water in the Assumed Thickeners

The analysis revealed that the decanted water in the assumed zinc concentrate thickener was high in cyanide concentration; therefore, the water would desirably be returned to the differential flotation circuit.

Decanted water from the other thickeners have no problem whatever if recycled within the beneficiation plant.

As water quality of the tailing pond overflow can be improved by neutralization treatment, there would be no problem either, if the tailing pond overflow is returned to the beneficiation plant.

Since an excessive portion of the beneficiation effluent would finally be drained off only from the tailing pond, it would cause no problem whatsoever to the environment.

2.4 Final Selection of the Process Flow

(1) Comparison between SDF and BDF

Based on the results of the series of beneficiation tests, a comparative study of the BDF and SDF processes as applied to the Tsav ore has been made, which is summed up in the following paragraphs.

Straight-Differential Flotation

Advantages :

1) As iron is easily depressed by lime in the zinc flotation, it is easy to elevate grade of zinc in zinc concentrate.

· Disadvantages:

1) Due to the existence of copper which is apt to activate zinc, a large amount of NaCN has to be used to depress zinc in the lead flotation.

Nevertheless, a greater part of zinc mixes into lead floats, circulating between the cleaners. Therefore, zinc grade and distribution in lead concentrate are apt to rise. It requires NaCN of a quantity almost similar to that for bulk flotation.

- 2) For depressing zinc in lead floats, the number of cleaning stages and cells have to be increased while, for decreasing returned zinc, certain measures such as additional treatment processes for zinc in middling in the lead floation have to be taken.
- 3) The increase in NaCN addition causes to elevate NaCN concentration in effluent sent to the tailing pond.
- 4) The beneficiation process flow becomes complicated, which makes operation performance less stable.

Bulk-differential flotation

· Advantage:

- 1) Thanks to the existence of copper which is apt to activate zinc, zinc depressor(CuSO 4) requirement in the bulk flotation is small.
- 2) In the bulk flotation, iron and waste alone have to be depressed; therefore, quantity of return ore is small which can be met by fewer stages of cleaning.
- 3) Bulk concentrate fed to the differential flotation is in a decreased quantity, requiring fewer differential flotation cells than those of the zinc flotation in SDF.
- 4) Mineral dressing effluent containing NaCN is returned to the differential flotation circuit, thereby reducing NaCN requirement and, accordingly, the NaCN content in the mineral dressing effluent.
- 5) The mineral dressing process flow is simpler, which makes operation performance more stable.

· Disadvantages:

- 1) Lime used for depression of iron in the bulk flotation may cause to lower lead recovery if added in excess.
- 2) If depression of iron in the bulk flotation is incomplete, iron depressed by NaCN may mix into zinc concentrate in the differential flotation, lowering zinc grade.

The comparison of the advantages and disadvatages of the two processes leads to a conclusion that the BDF process is superior to the SDF process, when applied to the Tsav ore, in that BDF takes advantage of copper being apt to activate zinc, has a simpler flotation process, requires smaller plant equipment and has stabler operation performance than SDF.

(2) Comparison between production of bulk concentrate alone and separate production of lead and zinc concentrates

It is a conceivable alternative to produce bulk concentrate(of lead and zinc) alone, without separation into lead concentrate and zinc concentrate.

Operation performance in this case is estimated in the table below. In this case, metal grades turn out to be inferior to those in case of separate production of lead and zinc concentrates.

*1 * 1			Gi	ade		1 :7	Di	stribut	tion (Quanti	ty
	2 1 1 2	, Au	Ag	РЬ	Zn	Cu,	Au	Ag	РЬ	Zn	Cu
	(t)	g/t	g/t	% .	%	*	g/t	g/t	%	- %	* %
Milt-F	30,000	1. 22	161	6.4	2.9	0.22	100. 0	100.0	100.0	100.0	100.0
Bulk-C	3, 722	7. 77	1,717	45.6	21.7	0.81	79.0	82.6	88.3	92.8	68. 1
Tail.	26, 278	0. 29	32	0.9	0.2	0.08	21.0	17.4	11.7	7. 2	31.9

Remarks: Mill-F;Mill feed Bulk-C;Bulk concentrate Tail.;Tailing

The project revenues and expenses in case of production of bulk concentrate are roughly estimated as follows:

Annual sales revenue of bulk concentrate:

Zinc: $3,722 \times 0.995 \times (0.217 - 0.08) =$	\$558,100
Lead: 3,722x0.995x(0.456-0.03)x650=	1,025,468
Gold: 3,722x0.995x(7.77-1)x0.9x390/31.1024=	283,237
Silver: 3,722x0.995x(1071-100)x0.9x390/31.1024=	582,135
$(-)\Gamma/C: (-)3,722x0.995x(190+10+(13/100x(1,100-1,000)))=$	(-)788,822
Total	\$1,660,118

The total annual sales revenue in case of production of bulk concentrate alone is \$168,000 less than that in case of separate production of lead and zinc concentrates.

Expenses:

In case of bulk concentrate production, one series of differential flotation system and concentrate dewatering system are dispensed with; therefore, the annual depreciation expenses will decrease accordingly.

$$$12,250 + $8,250 = $20,500$$

Likewise, the variable expense items such as the flotation reagents used in the omitted process sections, as well as repair expenses, etc., will become unnecessary, which represents \$35,000 of reduction in expenses.

Altogether, the reduction in annual expenses will be \$56,000.

The calculations reveals that, in case of production of bulk concentratealone, the decline in sales revenue is far greater than the reduction in expenses, which leads to a conclusion that separate production of lead and zinc concentrates is more favorable.

(3) Optimum mineral dressing process flow

The optimum mineral dressing process flow worked out on the basis of all the results of tests and studies so far undertaken is shown in Fig.39.

2.5 Esimated Mineral dressing Performance

The grades of run-of-mine ore of the Tsav deposits are estimated at Au 1.22g/t, Ag 161g/t, Pb 6.37%, Zn 2.94% and Cu 0.22% performance estimated on the basis of the grades of run-of-mine ore and the BDF test results is shown in Table 29.

	Weight		Gra	nde			Dist	ributi	on Qu	antity	<u> </u>
		Au	Ag	Pb	Zn	ปัน	Au	Ag	РЬ	Zn	Cu :
٠.	(t)	g/t	g/t	%	%	%		g/t		*	*
Crude	30,000	1. 22	161	6.4	2. 9	0.22	100.0	100.0	100.0	100.0	100.0
Pb-0	2, 371	11.01	1, 507	69.0	5.0	0.32	71.3	74.0	85. 2	13.6	11.5
Zn-C	1, 351	2.09	307	4.4	51.0	2. 77	7.7	8.6	3.1	79.2	56.6
Tail.	26, 278	0. 29	32	0.9	0.2	0.08	21.0	17.4	11.7	7.2	31.9

Remarks: Crude; Crude ore Pb-C; Pb Concentrate Zn-C; Zn Concentrate Tail; Tailing

Table 29 Estimated operation performance

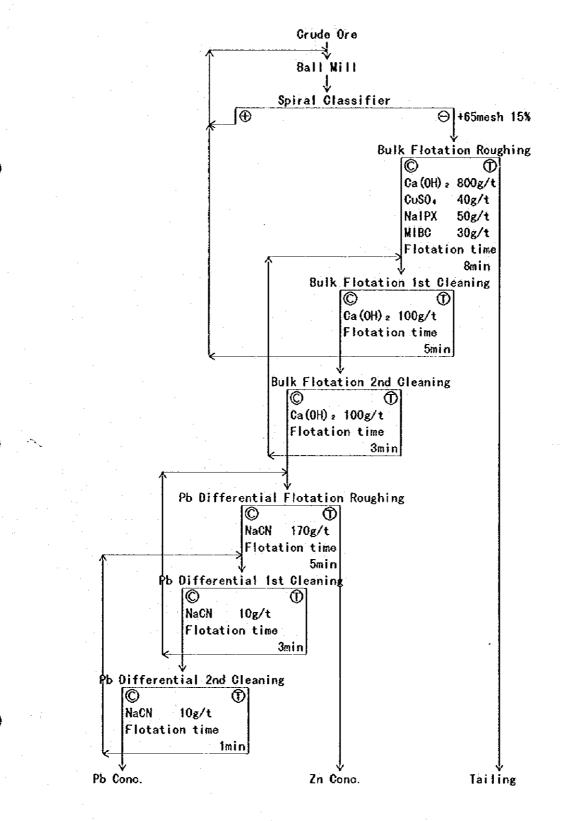


Fig. 39 Optimum Flotation Process Flow sheet

IV . Mine Development Plan







Part N. Mine Development Plan

Chapter 1. Mining Plan

1.1 General

1.1.1 Selection of mining method

The Tsav deposits have the following characteristics:

- (1) The deposits consist of high-grade, fine veins with an average width (in terms of the minable crude ore) of 1.03m.
- (2) The deposits are poor in continuity.
- (3) The deposits dip rather steeply; the No.4 vein dips 65° to 70° .
- (4) The hanging and foot walls are in poor rock conditions as long as it was confirmed at the -60m level.

In mining deposits of this type, the dilution constitutes a serious question. The exploration since 1992 has been carried out by the truckless mining method, and the machinery used for the work still remain at the site and are operable by the Mongolian operators.

Considering the small population of Mongolia (2.2 million), the mechanized cut and fill method combined with the truckless mining is most appropriate for the deposits, even though machinery costs are expensive in relation to labor costs in Mongolia.

1.1.2 Numerical basis for planning

The following base figures are applied for the mining plan:

Minable crude ore to be extracted (t)	332,464
Annual extraction of crude ore (t)	30,000
Number of operating days per year (days)	300
Daily extraction of crude ore (t)	100
Number of shift per day (shifts)	2

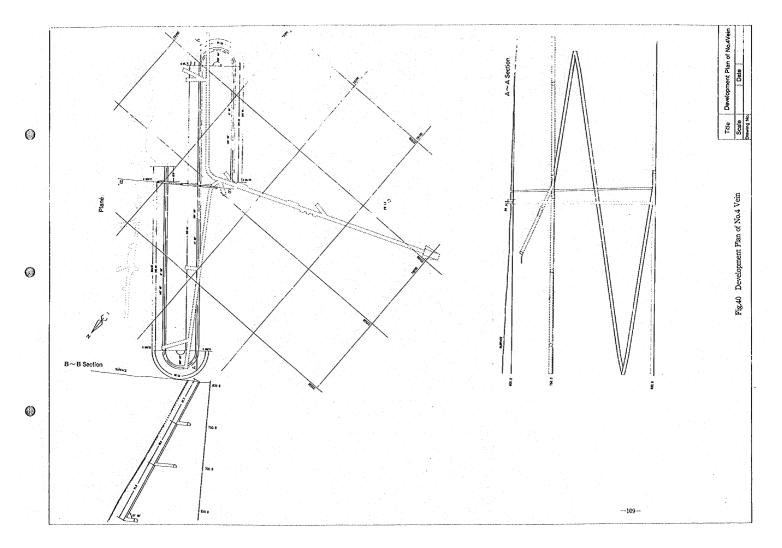
1,1.3 Underground structure (Ref. Fig. 40 Development Plan of No.4 Vein)

At the No.4 vein, already existing are a vertical shaft from the surface to 630m level(PW-14) which was driven during the ex-Soviet-Mongolian joint exploration, a drift at 630m level, an inclined shaft from the surface to 750m level and a 750m level drift at foot wall, the latter two being truckless and driven by MMAI since 1992.

A truckless inclined shaft system is considered appropriate for the deposits for the following reasons:

- (1) Compared with a vertical shaft, an inclined shaft can more flexibly accommodate changes in orebodies, allowing a wider range of options for planning and its revisions. A truckless inclined shaft can be driven from a free level with a free dip and in a free direction, which represents a great advantage in terms of the time required for reaching an orebody and of the stope preparation.
- (2) In case of a vertical shaft, mining cannot be commenced until all the excavation and installation are completed, whereas an inclined shaft permits mining to start as soon as an orebody is reached. At the No.4 vein, the lowest level of the object area of development is 630m, or 220m deep from the surface, while the daily rate of crude ore extraction is as small as 100t. The operation can be done with trucks(for underground use) or load haul dumps(LHDs) on hand, without an additional investment. In contrast, a vertical shaft system requires expensive equipment.
- (3) The orebodies being small in size and separately located, excavation has to be carried out at each of them, for which the vertical shaft system is too costly.

It is therefore envisaged that, starting from the No.2 waste dump at the bottom of the inclined shaft driven at the No.4 vein up to 750m level in 1993, a declining shaft (hereafter called "ramp") with a dip of 6° 30′ be driven at the foot wall of the orebody so that the ramp may bore through the existing drift at 630m level. The prospecting, development and stope preparation are to be done from this ramp.



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1.1.4 Ventilation raise and filling raise(Ref. Fig.40 Development Plan No.4 Vein)

A ventilation shaft will be driven in the central part of the mentioned ramp at the foot wall side, which will be extended downward as the ramp advances. A fan for the shaft sinking will be shifted downward, accordingly. When the shaft reaches 630m level, a ventilation system is established, which comprises the ramp for intake air and the vertical shaft(PW-14) for return air.

After completion of the ventilation system, the ventilation shaft drive as the ramp advances will no longer be used for ventilation but serves as a filling raise. To bore this raise, mechanical boring with a raise borer may be considered as an alternative; in view of the investment effect, however, a stage blasting method(Ref. Fig.41 Stage Blasting Method) is preferable since this is performable with the machinery on hand.

1.2 Operation Plan

1.2.1 Prospecting and Development

Starting from the mentioned ramp, excavation of accesses to the ore deposits, drifting along the veins and prospecting northward(-60m level) are to be conducted in sequence.

1.2.2 Mining methods

(1) In principle, the mechanized cut and fill method will be employed. In practice, however, 1) Ramp in Stoping and 2) Filled Rill Stoping will desirably be applied depending on local conditions. The mechanized cut and fill method in Tsav is shown in Fig.42.

1) Ramp in stoping

Under the mechanized(truckless) cut and fill method, it will become necessary to provide new accesses from the ramp as excavation advances, which increases the quantity of excavation in relation to the quantity of ore. This is a weak point of the method when applied to a deposit like Tsav.

A solution for the problem is the ramp in stoping method, whereby mining is

done diagonally in a stope and changeovers of accesses are minimized. (Ref. Fig. 43 Ramp in Stoping) In the ramp in stoping method, a mining block is diagonally divided in two, and the lower half is excavated from an access which rises in the stope each time a slice is extracted. When the access reaches the upper drift, extraction of the upper half is carried out from the upper drift.

In case of Tsav, however, the average width of veins of minable ore is as narrow as 1.03m whilst an LHD's bucket is 1.6m in width; thus, the dilution comes into a question. To cope with the question, extraction and blasting are to be conducted at two stages(ore and waste). Whether waste or ore should first be blasted is determined depending on vein width, dip, rock conditions, etc.

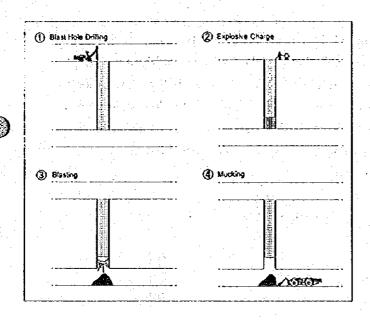
Drilling directions may be upward or horizontal. However, rock conditions on the hanging wall is so poor that the full filling is required; consequently, horizontal drilling is opted for. Height of the ceiling and width of stoping at the time of completion of stoping are assumed to be 3.0m and 2.5m, respectively.

2) Filled rill stoping

This mining method is fit to narrow, steep veins like those of the Tsav deposits. In case the hanging and foot walls are of poor rock conditions, however, the method is not appropriate because it increases the dilution.

As shown in Fig.44 Filled Rill Stoping, the lower drift is first driven, from where blasting holes are drilled either upward or downward. After charging explosives, blasting and mucking at a face, the opened space is filled from the upper drift and, at the face of the filled portion, charging, blasting and mucking are again done. This cycle is repeated later on. The interval between drifts are tentatively set at 6m but, for final determination, vein width, dip and rock conditions must be taken into account.

In order to minimize the dilution, the drifting has to be done with two-staged blasting(for separation of waste and ore), whilst drilling and blasting between drifts should be limited to ore portions as long as it is feasible.



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Fig.41 Stage Blasting Method

Fig.42 Mechanized Cut & Fill Method

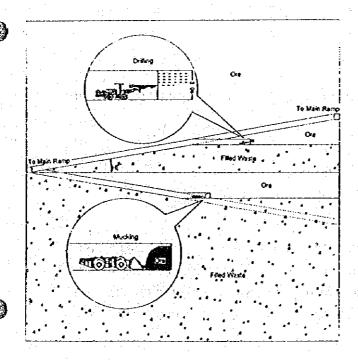


Fig.43 Ramp in Stoping

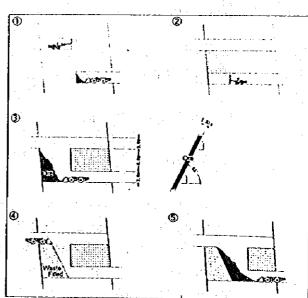


Fig.44 Filled Rill Stoping

(2) Mining Recovery and dilution

The mining recovery is determined by economic viability, vein width and continuity and reliability of ore reserve calculation, whereas vein width and mining method determine the percentage of dilution. The figures below have been empirically worked out on the basis of these considerations. The No.4 vein above 630m level and the other veins up to 100m under the surface are chosen as the mining target. At the No.4 vein, exploration has advanced considerably and the tunnels have been driven up to 750m level.

Vein width)	lining	recovery	Dilution
0.7m or more	Proved ore		90%	20%
	Probable ore		80%	20%
	Possible ore		70%	20%
Less than 0.7m	Proved ore		80%	30%
•	Probable ore		70%	30%
	Possible ore		60%	30%

(3) Minable crude ore

Quantity of minable crude ore calculated on the assumptions in (2) above are shown in Table. 30-1 and 30-2.

1.2.3 Drilling and blasting

(1) Drilling

For drilling operations for tunneling and drifting, the existing diesel-driven, 2-boom, hydraulic jumbo loaded with a 150kg hydraulic drifter is used. For excavation, the single boom, hydraulic jumbo loaded with a 120kg hydraulic drifter is used because of narrow drifts. Their guide cells are of the telescopic type so that they may drive rockbolts.

(2) Blasting

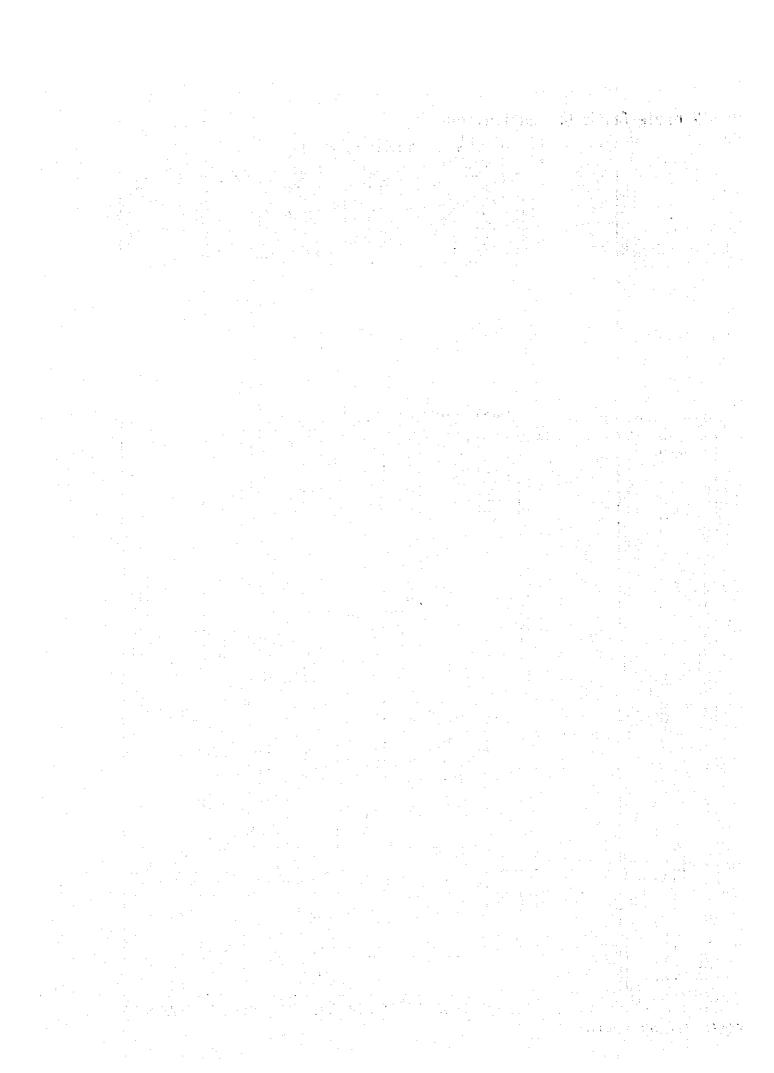
For blasting, AN-FO, desirable in view of easy handling and safety, is

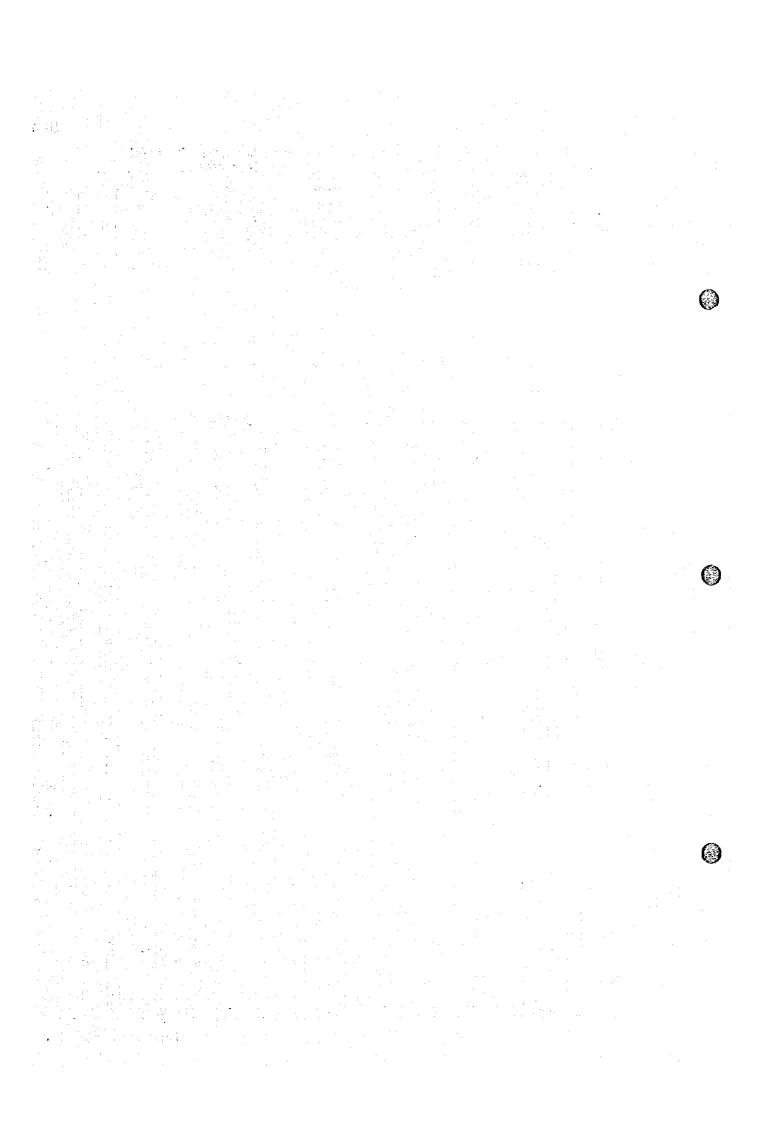
Ore Reserves & Minable Crude Ore Estimation

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10.4		16 188	- 11	32 31	1.435.0		7 13	1 - 12 -	111 65	144		3.107.34		11.32	16.67	9.53	83	31 1,006	1 . 1 0	3,90	0.50	1.33	0.05	3, 486, 35		3.06	. 13.31	0.46
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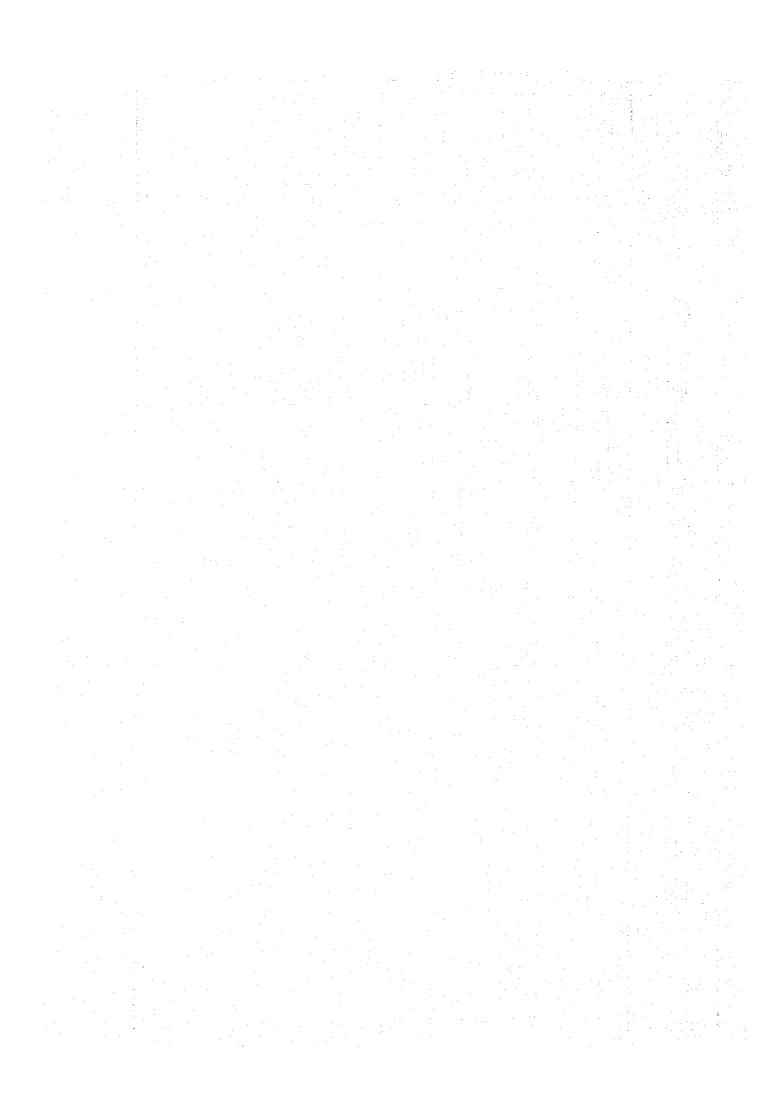
Table 30-1 Ore Reserves & Minable Crude Ore Estimation





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Table 30-2 Ore Reserves & Minable Crude Ore Estimation



unavailable in Mongolia; instead, "Ammonita," a kind of ammonia explosive currently used in Mongolia, will be used. For ignition, detonators are used.

1.2.4 Haulage

Waste and ore extracted at faces and drifts are transported by the existing load haul dumps(LHDs) with 3.8m³ and 2.0m³ cap. buckets. Ores conveyed from faces are transported by the LHD with a 3.8m³ cap. bucket to the surface via the inclined shaft. In case haulage distance exceeds 500m, ores are temporarily placed at the waste dumps driven in the inclined shaft during the exploration and, in turn, transported to the surface, thereby avoiding excessive load on the LHD engines. Compared to another alternative of utilizing 15 or 20-ton underground dump trucks, haulage by LHDs is more advantageous in respect of the investment effect.

Waste coming out of faces and drifts is stored at unused tunnels to the maximum possible extent for future use as filler, and only excess waste is hauled to the surface.

(2) Personnel, Machinery and supplies

For underground transportation of personnel, machinery and supplies, the existing light truck is used. For heavy machinery, the LHDs may be used.

1.2.5 Filling and timbering

(1) Filling

Wastes built up on the surface during the development phase and extracted during the operation phase are utilized as filling material.

Waste on the surface is cast into the vertical ventilation shaft sunk to the central part of the foot wall of No.4 vein when driving the ramp. The cast waste is extracted by an LHD at a level needing waste and transported via the ramp to fill stopes.

(2) Timbering

In principle, timbering is done by rock bolts alone. When rocks are

self-supported, concrete spray is applied in thickness of 3 to 5cm to cracks even though such cracks are abundant. In case rocks are not self-supported(faults, etc.), steel supports such as H-type steel frames are put into use.

The spray concrete is prepared at a batch plant(0.5m³/batch) to be installed either on surface or underground, transported to stopes by a 1.8m³ truck mixer and sprayed to wall rocks with a spraying machine. Considering temperature control of sand and water, the batch plant will preferably be built underground.

(1)

1.3 Equipment Plan

1.3.1 Compressed air

The concrete spray machine (and AN-FO chargers in case AN-FO is available) being the only machinery using compressed air, the existing portable compressor(discharge 21m³/min) can cater for the requirement. Another alternative is to mount a baby compressor on the spraying machine(or the AN-FO charger).

1.3.2 Ventilation

(1) Ventilation system

Since truckless mining method is applied, the ventilation system has to be capable of treating exhaust gas of diesel engines and noxious gases including blasting fume and dust particles.

During the ramp sinking phase, a ventilation system comprising fans fixed at the chute under the foot wall of ore deposits, which serves for intake air, air ducts through which air is sent to stopes and the ramp itself for return air.

At the operating phase(after completion of the ramp), the ramp will serve for intake air, whilst return air is exhausted through the vertical shaft(PW-14) by a fan to be installed at the shaft mouth. Ventilation at stopes is done by local fans and air ducts. When the drifts along veins are completed, a chute will be sunk from the upper drift near to the face(by the stage blasting method), thereby securing the ventilation and improving the work environment without using local fans.

(2) Fans

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One of the existing equipment uses two fans(gas volume 1,000m³/min, wind pressure 150mmAq, 37.5kW) in series and the other uses two fans(gas volume 500m³/min, wind pressure 100mmAq, 18.5kW) in series.

If underground airflow requirement is assumed to be 3m³/min per 1kW of engine power, and in case two LHDs(with diesel engines 185ps and 87ps, respectively) are in use, the required gas volume comes to 600m³ per minute.

(185+87)ps x 0.7355kW/ps x 3m³/kW = 600m³/min

Therefore, a fan of gas volume of 1,000m ³/min or two fans of 500m ³/min installed in parallel will be sufficient. Local ventilation will be done by a local fan of 500m ³/min.

1.3.3 Water supply and drainage

(1) Water supply

Water requirement for drilling is 65 ℓ /min per rock drill. On the assumption that three rock drills are used, the total requirement comes to 195 ℓ /min, which can be met by estimated underground drainage of 200 ℓ /min. Underground drainage is distributed to each stope via 2 'pipes laid through the ramp.

(2) Underground drainage

While the ramp is being driven, drainage is done by a pump station to be installed in the ramp near the ventilation chute and by 4° pipes laid in the chute. After completion of the ramp, a pump station will be installed at 630m level, and underground water will be drained through the pipes laid in the vertical shaft(PW-14). Drained water is sent to a thickener at the mineral dressing plant and utilized for mineral dressing.

1.3.4 Ancillary facilities

(1) Explosives storage and handling station

The existing magazine and handling station are utilized.

(2) Oil and lubricant storage

For gas oil, the tank (25,000 l cap.) buried near the shaft mouth will be utilized, while a lubricant storage will be newly built in the vicinity of the workshop.

(3) Office and accommodations

An office building and staff accommodations will be built at the site of ex-lodging house for the Japanese team. For workers' accommodations, the existing facilities for the Mongolian personnel will be utilized.

1.4 Main Machinery and Equipment

Type	Quantity	Specifications
Drill Jumbo (Drift)	1	Hydraulic 2 Boom, 150Kg.
		Telscopic boom Type
Drill Jumbo (Mining)	1	Hydraulic 1 Boom, 120Kg.
	. •	Telscopic boom Type
Concrete spray Equ.	1	10m³/Hrs class
Mixer Truck	1	1.8m³ class
Mortar Charger	1	It truck, Squeeze type charger
Concrete Batch Plant	: 1	0.5m³/batch
Load Haul Dump	2	3.8m³ class
Load Haul Dump	1	2.0m³ class
Compressor	. [21m³/min
Truck	1	2t attached with crane
Truck	2	Underground Service (For Man,
11008	_	Materials)
Wagon Car	2	Underground Patrol
Turbine Pump	2	1.0m³/min, 50Kw
Water Pump	3	5. 2Kw
Water Pump	2	2. 2Kw
Ventilation Fan	1	1,000mmø, 300mmAq, 75Kw
Ventilation Fan	1	900mm¢, 100mmAq, 18.5Kw
·	1	150m class (For Underground)
Boring Machine	1	565m class (For Surface)
Boring Machine	•	OAOM OLDOO /LOL OBLIGORY

Chapter 2. Mineral Dressing Plan

2.1 Mineral Dressing Plant

2.1.1 General

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The mineral dressing plant is assumed to treat crude ore at a rate of 100t/d and operate for 300 days a year; therefore, annual treatment of crude ore comes to 30,000t.

For mineral dressing, the bulk differential flotation process is employed to produce Pb and Zn concentrates.

To receive crude ore, a 600t stockyard will be provided near a crushing section, thereby avoiding troubles with ore quantities which may take place when receiving ore, due to the difference between the mining and mineral dressing divisions in respect to numbers of operating hours and days.

Crushing operation is carried out in two shifts a day while grinding, flotation and dewatering of concentrates are in three shifts.

As regards location of the mineral dressing plant, a site 500m up from the shaft mouth is selected, considering the locations of the shaft mouth and the ore deposits, topography, ground condition and location of the tailing dam. As the plant site is an almost level ground with slight inclination, the plant will be a flat type.

2.1.2. Design criteria

The mineral dressing tests have revealed that zinc ore from Tsav deposits is partially accompanied by oxidized copper ore. Therefore, zinc is apt to be activated and is hard to depress when separating lead from zinc. To depress zinc, sodium cyanide consumption increases. Lead and zinc contained in Tsav ore are easily liberated by the conventional flotation process, without any special treatment. However, a problem lies in the separation of lead and zinc because zinc tends to float. Consequently, the bulk flotation process is more favorable than the straight flotation process, which is the reason for the bulk differential flotation process being selected.

With a view to minimizing the capital cost and the operating cost, and also to make the mineral dressing plant operable, the plant is designed on the following principles:

- (1) A simple process is to be pursued.
- (2) Instrumentation is to remain at a conventional level; high-tech instrumentation involving automation will not be considered.
- (3) A washing plant is installed since there are argillized portions near the veins.
- (4) All the plant equipment are to be installed indoors. For equipment layout, due consideration is to be paid to maintenance and control.
- (5) For selection of machinery and equipment, due consideration is to be paid to their operability and maintainability.

The mineral dressing plant layout is exhibited in Fig.45. The design basis follows:

(1) Operating conditions	
Operating Days per year	300
Amount of treatment ore per day	
Shifts per day Crus	shing 2
Millir	$ng \sim Concentrate$ 3
Tailir	ng treatment 3
Working Hours per shift	8
(2) Mill feed	
Crude ore's average grade Pb(%) 6.4
Zn(%)	
Absolute Specific gravity	3.1
Apparent Specific gravity	1.9
Moisture(%)	5.0
Grinding work index Wi(kWh/t)	11.65

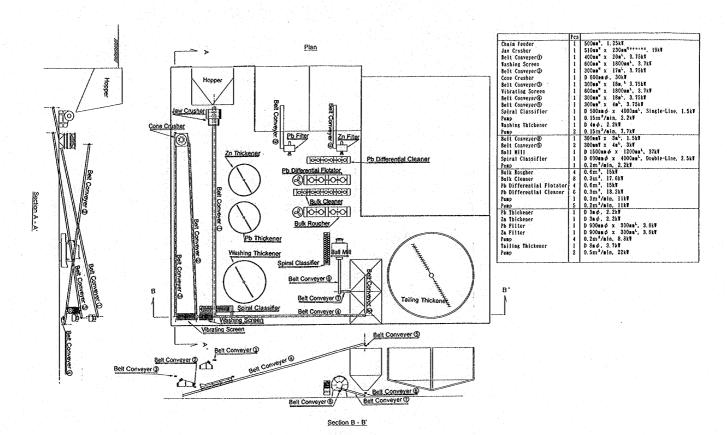
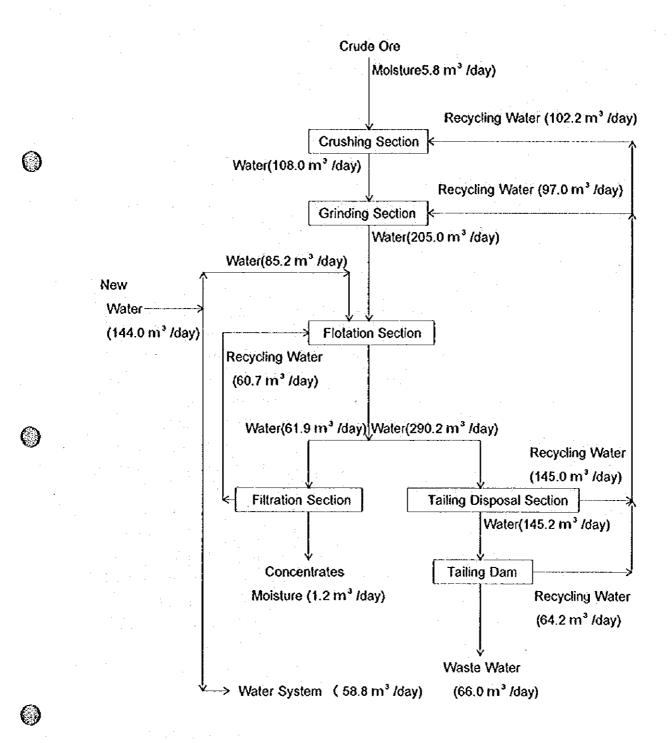


Fig.45 Layout of Mineral Dressing Plant

Crushing method		and the second s		i Scroliu)
	Primary	Jaw Crush		
· · · · · · · · · · · · · · · · · · ·	Secondary	Cone Crus	ner	(4
Treatment ore per 11				(Average)7.2 180
Max feed ore size (mr	n)			
Stockyard Volume (t)		• • •		600
Hopper Volume (t)				10
(4) Grinding section				
Grinding method	Single Ball n	nill (Closed cir	cuit)	
Treatment ore per 11		•		(Average)4.2
Feed size at 80% (mm				3.5
Final grinding size at				185
Classifier recycle load				300
Mill stock yard volum	and the second s			100
	i de la companya de			
(5) Flotation section				*
Title testing manathroad	m(a n 4			
Flotation method	Pb·Zn Bulk	differential flot	ation	
(5)-1 Pb·Zn bulk flotati		differential flot	ation	
and the second s	on		ation	
(5)-1 Pb·Zn bulk flotati	on I Two s ation time	stage		
(5)-1 Pb·Zn bulk flotati Cleaning method	on I Two s ation time		Time	(min)
(5)-1 Pb·Zn bulk flotati Cleaning method	on I Two s ation time	stage	Time 3	(min)
(5)-1 Pb·Zn bulk flotati Cleaning method Density and flota	on I Two s ation time	stage Density (%)	Time	(min)
(5)-1 Pb·Zn bulk flotati Cleaning method Density and flota Conditions	on I Two s ation time I	stage Density (%) 35	Time 3	(min)
(5)-1 Pb·Zn bulk flotati Cleaning method Density and flota Conditions Roughing	on I Two s ation time I	stage Density (%) 35	Time 3 10	(min)
(5)-1 Pb·Zn bulk flotati Cleaning method Density and flota Conditions Roughing Primary clean	on I Two s ation time I ning leaning	stage Density (%) 35	Time 3 10 4	(min)
(5)-1 Pb·Zn bulk flotatic Cleaning method Density and flotal Conditions Roughing Primary clean Secondary Cleaning Water	on I Two s ation time I ning leaning (pH)	stage Density (%) 35	Time 3 10 4 4	(min)
(5)-1 Pb·Zn bulk flotatic Cleaning method Density and flota Conditions Roughing Primary clean Secondary Clean Roughing water (5)-2 Pb Differential flota Cleaning Clean Roughing water (5)-2 Pb Differential flota Cleaning Roughing water (5)-2 Pb Differential flota Cleaning Roughing water (5)-2 Pb Differential flota Cleaning Roughing Rou	on I Two solution time I ning leaning (pH) otation	stage Density (%) 35 35	Time 3 10 4 4	(min)
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(5)-1 Pb·Zn bulk flotatic Cleaning method Density and flotal Conditions Roughing Primary clean Secondary Cleaning water (5)-2 Pb Differential flocal Cleaning method Density and flotal	on I Two solution time I ning I leaning (pH) otation I Two sation time	stage Density (%) 35 35 stage Density (%)	Time 3 10 4 4 10	
(5)-1 Pb·Zn bulk flotatic Cleaning method Density and flota Conditions Roughing Primary clean Secondary Cleaning water (5)-2 Pb Differential flot Cleaning method Density and flota Conditions	on I Two solution time I ning I leaning (pH) otation I Two sation time	stage Density (%) 35 35 stage Density (%) 20	Time 3 10 4 4 10	
(5)-1 Pb·Zn bulk flotatic Cleaning method Density and flotal Conditions Roughing Primary clean Secondary Cleaning water (5)-2 Pb Differential flotal Cleaning method Density and flotal Conditions Roughing	on I Two solution time I ming I leaning (pH) otation I Two solution time	stage Density (%) 35 35 stage Density (%)	Time 3 10 4 4 10 Time 3 10	
(5)-1 Pb·Zn bulk flotatic Cleaning method Density and flota Conditions Roughing Primary clean Secondary Cleaning water (5)-2 Pb Differential flot Cleaning method Density and flota Conditions	on I Two solution time I ning leaning (pH) otation I Two lation time	stage Density (%) 35 35 stage Density (%) 20	Time 3 10 4 4 10	

Pb concent	rate Zn	concentrate
Concentrate grade (%) 69.0		51.0
Recovery (%) 85.2		79.2
Toology (17)		
(6) Concentrate section	***	• •
Dewatering method vaccumed filteration dev	vater	
(6)-1 Pb concentrate	•	
Thickener underflow density (%)	40	
Concentrate size (%) -100 mesh	85	
Concentrate moisture (%)	7	*
Concentrate specific gravity	6.9	
(6)-2 Zn concentrate	. 40	
Thickener underflow density (%)	40	
Concentrate size (%) -100mesh	70	
Concentrate moisture (%)	9	
Concentrate specific gravity	4.1	
(7) Tailings section		$\mathbf{x}^{(t)} = \mathbf{x}^{(t)}$
Concentration method Cyclone and Thickene	r	
Density of flotation tailing (%)	20	
Transportation tailing density (%)	40	
Cyclone overflow's sedimentation velocity (cm/hr)		•
(8) Water consumption		
Water consumption volume (m ³ /day)	404	
New water supply volume (m 3 /day)	144	
Recycle rate (%)	64	

The water balance of the mineral dressing is shown in Fig.46.



*) Crusing Section 2 Shifts / day, After Grinding Section 3 Shifts / day

Fig.46 Water Balance of Mineral Dressing Plant

2.1.3 Mineral dressing process

The process flow sheet of mineral dressing plant is shown in Fig.47.

(1) Receiving of crude ore

Crude ore is hauled from underground to the surface by LHDs. A 600t stockyard is constructed near the crushing section of the mineral dressing plant for buffering ore feed and also for blending purpose. From the stockyard, ore is conveyed and fed by payloader into a receiving hopper of the crushing section.

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(2) Crushing

The crushing process comprises a single series of two-stage crushing; the first stage forms an open circuit while the closed circuit is formed at the second stage. Main equipment are one each of primary and secondary crusher, a vibrating screen which, together with the secondary crusher, forms the closed circuit, another vibrating screen for washing purpose and a spiral classifier.

A chain feeder(500mmW) extracts ore from the receiving hopper and feed it to a jaw crusher(510mm x 230mm). Crushed ore is fed by a conveyer to a washing screen(600mmW x 1,800mmL, single deck, opening size 10mm) for slime removal.

The oversize of the washing screen is fed by a conveyer to a cone crusher (600mmW) while the undersize enters in a spiral classifier. Ore crushed by the cone crusher is, in turn, fed by another conveyer to a vibrating screen (600mmW x 1,800mL, single deck, opening size 10mm). The oversize of this screen is returned to the cone crusher while the undersize is the final crushed product. On the other hand, the undersize of the washing screen fed to the spiral classifier is separated into slime and raking sand. The classifier slime is stored in a washing thickener (4m dia) while the raking sand joins the undersize of the vibrating screen and these are transported to a mill bin as the final crushed product.

Overflow of the washing thickener is recycled to the washing screen while underflow is fed to a ball mill.

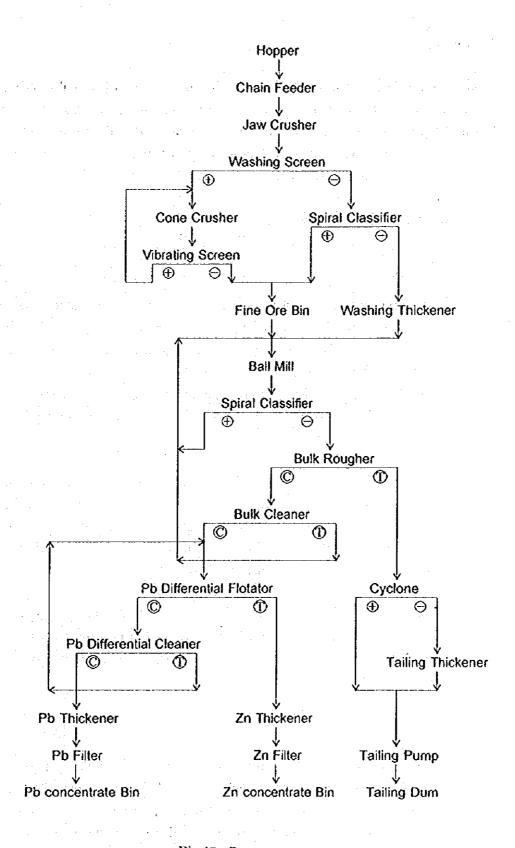


Fig.47 Process Flowsheet

(3) Grinding

Ore from the grinding section's bin is fed by conveyor to a ball mill (1500mm ϕ x 1200mmL) for grinding. Ground ore, in turn, enters the spiral classifier (600mm ϕ) and is separated into flotation feed and return sand. The return sand from the classifier is returned to the ball mill. The flotation feed is sent to the flotation section by a pump.

The grinding mill bin has a storage capacity of 100t.

(4) Flotation

The flotation process is composed of a single series of bulk flotation circuit(4 roughers of 0.6m³ and 8 cleaners of 0.28m³) and a single series of Pb differential flotation(4 roughers of 0.6m³ and 6 cleaners of 0.28m³). Flotation feed is subjected to bulk flotation roughing so that lead and zinc may be recovered as float, whilst the roughing tailing becomes the final tailing. The roughing float is further upgraded through two—stage cleaners and sent to the differential flotation. Cleaner tailings is returned to the grinding circuit.

Float in the bulk flotation is subjected to differential flotation whereby lead may be recovered as float while zinc becomes tailing. Differential flotation roughing float is upgraded to lead concentrate by the two-stage cleaners. Differential flotation cleaner tailing is returned to differential flotation feed. Zinc as differential flotation tailing is stored in the zinc concentrate thickener.

In the bulk flotation roughing and differential flotation, neither regrinding of cleaner tailing, etc. nor intermediate thickening within the flotation circuit is done because of easy liberation. Details of the flotation circuit has to be determined on a basis of pilot test results.

(5) Dewatering of concentrates

Lead concentrate and zinc concentrate, which are the final flotation products, enter their respective concentrate thickeners. Thickened concentrates are dewatered by the drum filters (900mm ϕ x 300mmL), respectively. Overflow of the both thickeners of concentrate are recycled to the flotation section.

Dewatered concentrates are sent directly to the concentrate stockyard by conveyors and stored there. When necessary during wintertime, they are dried by drum-type dryers before storage.

Concentrates at the stockyard are loaded on to trucks by a payloader and weighed by a truck scale before shipment.

2.1.4 Ancillary facilities

(1) Instrumentation

The instrumentation is limited to a minimum necessary level and installation of automation equipment is not considered. For instrumentation, pH meters are installed at the places where bulk flotation feed and differential flotation feed enter. A control center is not envisaged.

(2) Flotation reagents, etc.

Flotation reagents to be used are sodium cyanide, copper sulfate, sodium sulfide, calcium hydroxide, isopropyl xanthate and MIBC.

Reagents are dissolved at the reagent preparation room, sent to storage tanks at the flotation section and added by constant feeders where necessary.

Following are the assumed requirements of reagents, etc. per ton of crude ore:

Sodium cyanide (g)	200
Copper sulfate (g)	70
Sodium sulfide (g)	50
Calcium hydroxide (g)	600
Isopropyl xanthate (g)	50
MIBC (g)	35
Balls for the ball mill (g)	675
Electric power (kWh)	43.2

(3) Dust collection

Dust covers are installed on the cone crushers and the vibrating screens of the crushing section, to draft dust particles, which are treated by a wet-type dust collector.

(4) Sampling

To check operation performance of the mineral dressing plant, one each of samplers is installed at the four points for sampling of the bulk flotation feed, bulk flotation tailing, final concentrate of differential flotation(Pb conc.) and differential flotation tailing(Zn conc.).

(5) Others

Power: Power for the mineral processing plant equipment are distributed at each of the three blocks, ie., 1) crushing block, 2) grinding—flotation—tailing pipage block, and 3) concentrate dewatering block.

Electric hoist: One each of 5t electric hoists is installed at the crushing and grinding sections while a 2t hoist at the flotation section, as these sections have heavy equipment.

Storage space for supplies: Appropriate spaces are provided at the crushing section, flotation section and workshop for storing supplies.

Workshop: The workshop built by the Japanese team near the shaft mouth is utilized.

Assay and laboratory: Rooms for assay, testing and sample preparation are built adjacent to the mineral dressing plant, to conduct the minimum necessary testing for the purpose of process control.

Office: A site office is provided within the mineral dressing plant.

2.2 Facilities for Tailing Disposal

2.2.1 Thickening

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Flotation tailing with a concentration of around 25% is thickened by cyclones to around 45%. Cyclone overflow is sent to a tailing thickener (8m ϕ).

Thickened cyclone underflow and thickener underflow are sent together to the tailing dam by two sand pumps. Waste thickener overflow and tailing dam overflow are recycled to the crushing, grinding and flotation processes.

2.2.2 Tailing disposal

The tailing disposal has a capacity of 11—year service and is designed to allow further expansion. The dam site is selected at a location nearest possible to the mineral dressing plant and out of the area of ore deposits.

As the site is too gently inclined for tailing to be transported by the natural gradient, tailing will be transported by pipage pressurized by Wahman pumps. However, a steep gradient is unnecessary for transportation of tailing dam overflow, which will be sent back by the natural gradient to the mineral dressing plant from the tailing dam to be sited in the upper side of the plant.

The tailing dam is an earth dam of a pond type with an embankment at the lower part to be made from soil excavated in the upper part of the site, taking advantage of the gentle gradient.

With a view to minimize the initial investment, the dam will be partitioned so it may be constructed in four separate phases, balancing the cutting volume with the banking volume.

In the upper side of the dam, an unlined channel is cut along the dam, whereby rain water is drained into a dry stream bed in the lower part.

For intake of the overflow water, a particular portion of the embankment is used for height adjustment, so that overflow can be controlled in relation to the ups and downs of the dam water level. A plan, a location map, and a longitudinal section and a hydrographic map of the tailing dam are exhibited in Fig.48, and Apx.7, 8 and 9, respectively.

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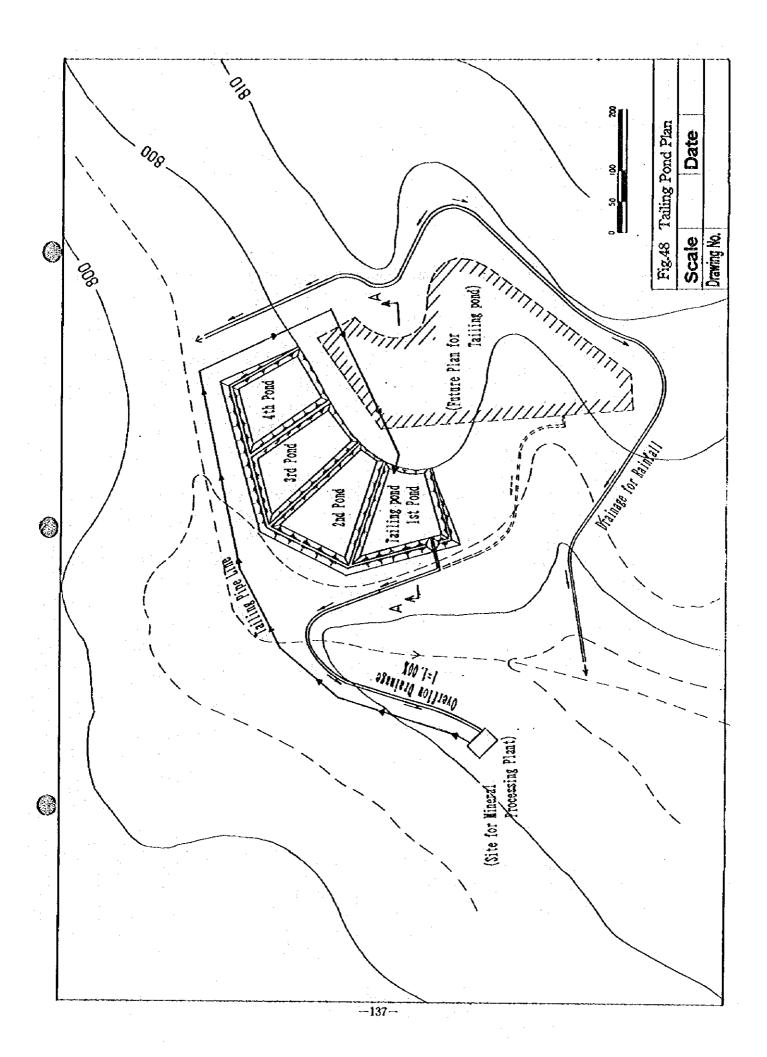
Design of various channels is based on the following assumptions:

- 60 minute rainfall depth probability: 7mm/hour
- Tailing transport volume: 300m³/8 hours
- Overflow water transport volume: 0.01m 3/second

Main specifications of the tailing dam are shown in the following Table:

Descriptions	Quantity	Remarks
Volume	170,000m³	
Area	43,000m²	
Earth dam height	max. 5m	
Crest total length	1,300m	
Crest width	5m	
Slope gradient		
Inside wall	1 : 1.8	
Outside wall	1:2.0	
Cutting face of slope	1 : 1.5	
Tailing pipeline	1,350m	
Channel of overflow		
drainage cycle	640m	
Drainage for rainfall	1,560m	

Table 31 Main Specifications of the Tailing Dam



Chapter 3. Auxiliary Facilities Plan

3.1 Power Receiving and Distribution

3.1.1 General

For electric power supply, two alternatives were considered: (1) in-house power generation using the existing 750KVA generator which was used by the Japanese survey team; and (2) receiving power from a thermal power station in Choybalsan.

In case of the in-house power generation, light oil supply is uncertain and the price is expensive. The state-run power station in Choybalsan, cap. 36,000kW, is operated with lignite mined from Adun Choulung open-pit colliery and is supplying power to the city of Choybalsan and also to the three nearby villages of Helren, Baitomung and Toblagan.

Power is transmitted at 35KV from Choybalsan to Helren(approx. 50km) and at 10KV from Helren to Habilka(approx. 70km). From Habilka to Tsav, no transmission line has been laid. The Choibalsan power station is said to have a surplus supply capacity of 2,000 to 3,000kW in summertime and about 1,000kW in wintertime.

In order for the Tsav mine to receive power supply from the Choybalsan station, a 35KV transmission line would have to be laid by the power station from the village of Habilka to Tsav(approx. 80km). 50% of the cost is to be borne by the user.

In this project, the alternative of receiving power from Choybalsan is chosen, since the long-term stable power supply at low cost is essential. The alternative would be beneficial to the future development of the surrounding area, as well.

3.1.2 Power demand

The maximum power demand of the Tsav mine's production units and other facilities is estimated at about 600KW, whilst the annual power demand is about 2,300MWh, which is broken up as follows:

Section	Maximum Power Demand(KWh)	Annual Power Demand(MWh)
and the second		And the second second
Mining	400	960
Mineral Dressing	200	1,296
Total .	600	2,256

3.1.3 Power receiving and distribution facilities

In order for the Tsav mine to receive power from Choybalsan, to be added to the existing facilities are: (1) an outdoor cubicle for receiving power at 35KV, (2) a 750KVA transformer, and (3)a 3.3KV outdoor cubicle.

(1) Outdoor cubicle for power receiving at 35KV

The cubicle contains a disconnecting switch(DS) board and a vacuum circuit breaker(VCS) panel, to which a protective relay for power receiving has to be added.

(2) 750KVA transformer

The transformer is to step down from the receiving tension of 35KV to 3.3KV, the distribution tension within the mine. The required capacity is put at 750KV, considering the mentioned power demand.

(3) 3.3KV outdoor cubicle

This cubicle is to send the power stepped down by the transformer from 35KV to 3.3KV to the electric systems existing at the mine. It has no synchronizing device as parallel feed with the diesel generator is not considered.

3.1.4 Power cost comparison

Estimated power cost in case power is supplied by Choybalsan

Transmission line laying cost	US\$ 267,000
Power receiving facilities	335,000
Power charges (for mine life)	*1 1,985,000.—
Total	US\$ 2,587,000

Estimated power cost in case of in-house generation

Light oil and lubricant

*2 US\$4,417,000.-

Remarks: * 1 (2,256,000kWh x 11 years x 0.08\$/kWh)

*2 (\$1,100/day x 365days x 11 years)

The cost per day is based on the actual cost at Tsav.

In case of the in-house generation, labor cost for generator operators and generator repair costs have to be considered, in addition to the oil and lubricant costs. This indicates that receiving power from Choybalsan is far more economical than in-house generation.

3.2 Communication equipment

At present, communication to and from the mine site is done by wireless equipment provided respectively in Ulaan Baartar, Choybalsan and Tsav. No additional investment for communication such as telephone/facsimile via INMARSAT is contemplated in this project.

3.3 Water Supply Facilities

Currently, the drinking water is brought to Tsav by a water wagon from a well dug by an ex-USSR team 6km away from Tsav, stored in a 50m³ tank, and distributed to each section. This project follows the current system and contemplates no extra investment.

As for industrial water, 100 & /min out of some 200 & /min of the estimated total underground drainage will be sent to a water storage tank of the mineral

dressing plant. The fresh water will be used mainly for the cleaning process whilst, for the other processes, overflow of the tailing dam and thickeners will be recycled, in an effort to minimize water consumption.

3.4 Workshop

Repair of the underground heavy machinery and mineral dressing equipment is of great importance. In this project, utilization of the existing workshop(24m x 13m) built by the Japanese survey team near the shaft mouth of the No.4 vein is contemplated so that an additional investment may be done without.

3.5 Ancillary Facilities and Vehicles in Common Use

3.5.1 Office and Stuff accommodations

A 660m² building which houses an office and staff accommodations is planned to be built at the site where accommodation for the Japanese survey team was located. The site is conveniently located in respect of water supply and drainage, sewage systems and electric power facilities.

For workers' accommodation, the existing building which was used as the Mongolians' accommodation during the survey period is utilized.

3.5.2 Vehicles in common use

A microbus for transporting personnel between Choybalsan and Tsav and a 11t dump truck for transporting concentrates to Habilka station is included in this project, as vehicles in common use. Facilities such as the ambulance and hospital are not considered in this project.

3.6 Transportation of Concentrates

3.6.1 Stockyard

Lead concentrate and zinc concentrate are stored at a stockyard near the mineral dressing plant until shipment. Storage capacity of the yard is planned to meet the monthly output, ie., 200t of lead concentrate and 110t of zinc concentrate.

3.6.2 Concentrate transportation route

Feasibility of concentrate shipment to Russia has been studied. Under the current economic conditions of the nation, however, the Russian smelters—refineries at Zabaykarsk and Sherlovaya Cora have curtailed or suspended operation and their future trends are hardly predictable. Therefore, it is assumed in this project that the concentrates are to be shipped to coastal smelters—refineries in Japan despite the problems of shipping lot and shipping cost.

For this alternative, the following two routes are considered:

- (1) Tsav → Borzya → Karymskoe → (the Siberian Railways) → Vladivostok → (ocean transportation) → Japan
- (2) Tsav → Borzya → Zabaykarsk → (the Chinese Railways) → Dalian → (ocean transportation) → Japan

The transportation costs come to US\$ 80/t and \$ 70/t, respectively. Apparently, the second alternative route via China is less expensive. However, in case of shipment via China, bulk shipment of concentrates is not allowed, which involves extra bagging costs; furthermore, troubles may arise from the difference between the rail gauge of China and that of Mongolia and Russia.

Taking all these factors into consideration, the first alternative route via Russia is chosen for this project. For the transportation of concentrates to the nearby Habilka station, an 11t dump truck will be used.

Chapter 4. Production Plan and Personnel

4.1 Production Plan

The production plan is based on the following assumptions:

Ore reserves and grade: 1,544,627t

Cu Pb Zn Au Ag 0.24%* 6.84% 4.01% 1.3g/t* 263g/t

Average mining recovery: 18%

Average dilution: 21%

Minable crude ore and grade: 332,464t

C u Pb Zn Au Ag 0.22%* 6.37% 2.94% 1.22g/t* 161g/t

Annual production of crude ore: 30,000t

Arithmetical mine life: 11 years

Mineral dressing recovery:

Pb Zn Au Ag

88.3% 92.8% 79.0% 82.6%

Annual production of concentrates: Pb conc 2,731t

Zn conc 1,351t

Grade of concentrates:

	Cu(%)	Pb(%)	Zn(%)	Au(g/t)	Ag(g/t)
Pb conc		69.0	5.0	11.10	1,507
Zn conc	2.77	4.4	51.0	2.09	307

Remarks: * indicates an average grade of the proved and probable ore reserves.

(For the possible ore reserve, no assay has been done of Cu and Au.)

The mineral dressing performance shown in Table below is used for projection of mine revenues.

	Quan-	<u> </u>	Grade			Grade Distr			ribution		
	tity	Au	Ag	Pb	Zn	Cu	Au	Ag	Pb	Zn	Gu
	(t)	g/t	g/t	%	%	. %	%	%	%	l %	%
Crude											
ore	30,000	1. 22	161	6.4	2.9	0.22	100.0	100.0	100.0	100. 0	100.0
Pb con	2,371	11.01	1,507	69.0	5.0	0.32	71.3				11.5
Zn con	1,351	2.09	307	4.4	51.0	2.77	7. 7	8.6	3.1	79. 2	56.6
Tail.	26, 278	0. 29	32	0.9	0. 2	0.08	21.0	17.4	11.7	7.2	31.9

Table 32 Mineral dressing performance

4.2 Personnel Plan

The organization for operation and personnel arrangement by section and class are shown in Fig. 49.

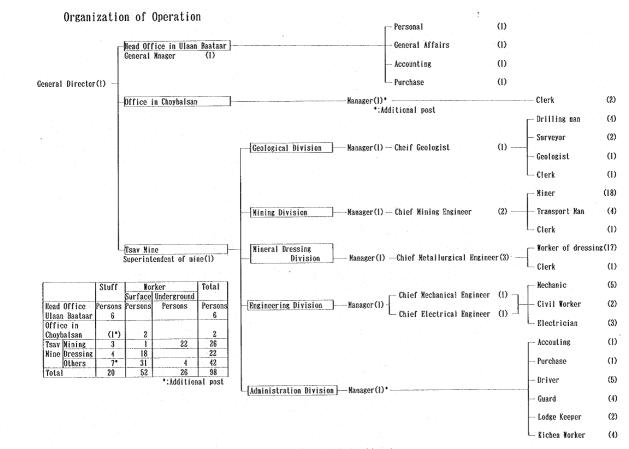


Fig.49 Organization of Operation

(

Chapter 5. Environmental Survey

5.1 General

The Tsav area is situated at a gentle hill in the steppe without trees. There is no streams with constant water flow. Only during a limited period of a year, rain water occasionally form puddles at hollows on the surface but such surface water evaporates due to the region's dry climate and puddles gradually disappear. In some cases, the underground water table appears on the surface at sunken places, forming springs, which rarely last through a year, though. The local nomads draw up and use the ground water for their living.

In August when a survey was conducted, some puddles with rain water were seen here and there in the area; however, there was no ponds or swamps where surface water stays permanently, in the downstream side of the water systems near the planned sites for the mineral dressing plant and the tailing dam and near the water system, into which the underground mine water is currently drained. The drained water, while flowing a short distance, say 1km, on the surface, sinks into the ground.

In the light of these observations, it is considered that, after the mine has been developed, water pollution by the drainage from mine and mineral dressing plant is unlikely to widely spread over the downstream side of the local water system but likely to be confined within a limited area around the mine and plant. For this reason, the survey on soil and ground water was limited only to this area.

5.2 Soil

In the vicinity of Tsav deposits, surface soil samples were collected at four points at a dry stream into which the mine and plant drainage is expected to flow. The four points are: the upper side of the drainage point, near the drainage point and two points in the lower side of the drainage point. For comparison purpose, another soil sample was taken at a place away and independent from the mentioned dry stream. These samples were brought back to Japan for assay of the five heavy metal contents(Cu, Pb, Zn, Fe and Cd) as well as arsenic content.

The assay results in Table 33 indicate a certain difference in Pb and Zn concentration between the upper sampling point and the lower sampling points while no difference in

concentration of the other elements is indicated. Cu, Ad and As are in low grades whilst Fe is considered to be abundant over an extensive area, independently of the ore deposits. The area, in which the difference in Pb and Zn concentration is recognized, is not so wide. It is anticipated, therefore, that water pollution possibly caused by the mine development would be confined to a limited area in the lower side of the mineral dressing plant.

Assay of sample soil taken from the point chosen for comparison purpose indicated Cu 50ppm, Pb 340ppm, Zn 260ppm, Fe 2.5%, Cd <2.5ppm and As 31ppm, which serve as the background values before the mine development is commenced. The assay also indicates the arsenic content being somewhat high, which characterizes this area.

Sampling points	Upper side of shaft mouth	Near shaft mouth immediately	Lower side of shaft mouth	Lower side of shaft mouth	Comparative point (unin-fluenced by ore deposits	
	upstream	downstream	mid-stream	n downstream		
Samples to	aken on : 11	August			T	
Cu (ppm)	60	40	48	45	52	
Pb (ppm)	1000	470	420	260	340	
Zn (ppm)	480	290	320	190	250	
T-Fe(%)	2.6	2. 3	2.5	2. 7	2.5	
Cd (ppm)	⟨2.5	<2.5	⟨2.5	<2.5	<2.5	
As (ppm)	53	35	31	29	30	

Table 33 Environmental Survey around Tsav Deposits(Assay of soil)

5.3 Underground Water

In order to check the present state of pollution of the underground mine water and well water in Tsav area and also to obtain background values, water quality measurement was conducted three times on different days of sample water collected at two points underground (water used for drilling and underground spring water at a separate location) and also of sample water taken from a well that is used for drinking, the latter serving for comparison with the former.

Three samples collected on the final day of measurement and one sample taken from another well(different from the abovementioned well) were brought back to Japan for assay of the five heavy metal contents and arsenic content, similarly to the case of soil. The results of the assay and water quality measurement are shown in Table 34 and 35, respectively.

Based upon these results, suitability of the Tsav underground water for mineral dressing use was also studied.

The items of water quality measurement are pH, electric conductivity, turbidity, dissolved oxygen, water temperature, Cu, Fe²⁺, total Fe, Zn, Ni, Mn, Cr⁶⁺, COD, NO₃ –N and NH ⁴⁺ –N, of which pH, electric conductivity, turbidity, dissolved oxygen and water temperature were measured by instruments while the other items were checked by summary measurement with test papers. Underground water and well water were measured once every week over three weeks, but no significant difference was found.

Underground water taken at two points showed high Zn and total Fe among the metal contents while, among the organic components, COD, NH ⁴⁺ -N and NO ³ -N were high. In the underground water, a minute amount of zinc was detected, which indicates that zinc contained in the ore deposits dissolves into underground water. The total Fe contained in the drilling water suggests influence of the iron piping. The recognized COD, NO ³ -N and NH ⁴⁺ -N are presumed to derive from the pastured animals' droppings which flowed with rain water into the vertical shaft and decomposed, and/or to be influenced by components of the explosives used underground.

In the water samples taken from two different wells outside Tsav area, organic pollutants such as COD and NO₃ -N of minute quantities were detected, which are also presumed to derive from the feces of pastured horses and cows. Except this, no other questions were encountered.

On the basis of the survey findings, suitability of the underground water for the mineral dressing process water was studied, as well. Although all the water surveyed is hard water with somewhat high electric conductivity, it may be concluded that there would be no problem whatsoever if the underground water is used for the mineral dressing of ore.

As for drinking water, it is desirable to use well water located in an area where Zn and Fe contents, as well as organic pollutant contents, are low, although it is not impossible to use the underground water after certain treatment.

Sampling points	. I have a second and a second and a second as a s		Well water near magazine	
Samples ta	ken on : 14 A	ugust	1 .	
Cu (ppm)	<0.01	<0.01	<0.01	<0.01
Pb (ppm)	<0.05	<0.05	<0.05	<0.05
Zn (ppm)	0.07	0.31	1.5	0.01
T-Fe (ppm)	0.55	0. 22	1.5	0.07
Cd (ppm)	<0.005	<0.005	<0.005	<0.005
As (ppm)	<0.01	<0.01	<0.01	<0.01

Table 34 Environmental Survey around Tsav Deposits (Water Quality Analysis)

ا دمین	Well	lii. Jan	na.a	lw.ii	10.1	111 1	Tiir	T	1.,	7			
	!		Under-	Well		Under-	Well		Under-	Well			
ing	water	1	ground	water	1	ground			ground	water			
Points	-	water	water		water	water		water	water	near			
			drill-		•	drill-			drill-	Maga-			
<u> </u>			ing		l	water		<u> </u>	ing	zine			
Date	taken	on 2 Au	igust	taken	on 8 Au	gust	taken on 14 August						
рН	ا مما	ا مما								l .			
F 1 4	8. 2		- 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1	8.5	8.2	7. 2	8. 4	8.1	7.3	7.7			
Electri			(mS/cm)										
÷	1. 3	1.1	1.3	1.3	1.0	1.3	1. 3	1.0	1.3	1.1			
Turbidi	•				1 .								
	0	10	100	2	6	240	2	12	111	4			
DISSOLV		en (ppm)	12.5	<u> </u>			į ·						
	7. 3	11.2	6. 5	8. 7	10.8	7.5	9. 9	10.6	8. 5	11.2			
Nater t		ure (°C)											
		8.9		13. 4	13.0	18. 8	10.4	10.6	15. 2	11.5			
		h test	paper			<u> </u>							
Cu (pp		1											
l	<0.5	<0.5	<0.5	<0.5	<0.5	0. 5	<0.5	<0.5	<0.5	<0.5			
Fe ²⁺ (p										Ì			
	<0.2	<0.2	<0.2	<0. 2	<0.2	2	<0. 2	<0.2	≦ 0. 2	<0.2			
T-Fe(p						+ ,							
	1	<0.2	0.4	≦0.2	<0.2	7	<0. 2	≦0.2	1	≦0.2			
Zn (pp	i												
	0	0	1	0	0	2	0	0	2	0			
Ni (pp	1.00												
		<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5			
Mn (pp													
	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	0.5	<0.5			
Cr ⁶⁺ (:		•							
		<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05			
COD (p		1							· · · - •				
	2	15	18	10	20	40	3	8	20	5			
NO3-N(p													
	<0.006	0.03	<0,006	<0.006	0.04	<0.006	<0.006	0.03	<0.006	<0.006			
NH**-N(
	0.6	0.6	0.8	0.4	0.4	0.6	0.4	0.6	1. 2	0.4			

Table 35 Environmental Survey around Tsav deposits (Water Quality Mesurement)

Chapter 6. Revenue Plan

6.1 Concentrate Prices

6.1.1 Assumptions

- (1) Quotation of metals: Pb \$650/t, Zn \$1,100/t, Au \$390/tr oz, Ag \$5.30/tr oz.
- (2) Payable metals: Pb concentrate Pb: 95% (Minimum deduction 3%)

Au: 1g less; recovery 90%

Ag: 95% (Minimum deduction 100g)

()

Zn concentrate – Zn: 85% (Minimum deduction 8%)

Au: 1g less; recovery 65%

Ag: 4 tr oz less; recovery 60%

(3) Treatment charges(T/C) and refining charges(R/C):

Pb concentrate - Pb: T/C \$160/DMT; scale + 14 ¢ /\$ (Base=\$600)

Ag: R/C 30 ¢ /tr oz

Zn concentrate - Zn: T/C \$190/DMT

Zinc quotation $$1,250 \sim $1,250 \sim 1,000 \sim $1,000$

T/C scale $+15 \notin /\$ + 13 \notin /\$ -8 \notin /\$$

- (4) Penalty: Not applied as impurities are yet to be assayed.
- (5) Concentrate transportation to Japan via Siberian route: \$80/WMT, incl. transportation toss(0.5%) and moisture(8%)
- (6) Transportation insurance: 0.077% x (concentrate price T/C R/C)

6.2 Revenues

Revenues calculated on these assumptions are shown in Table 36.

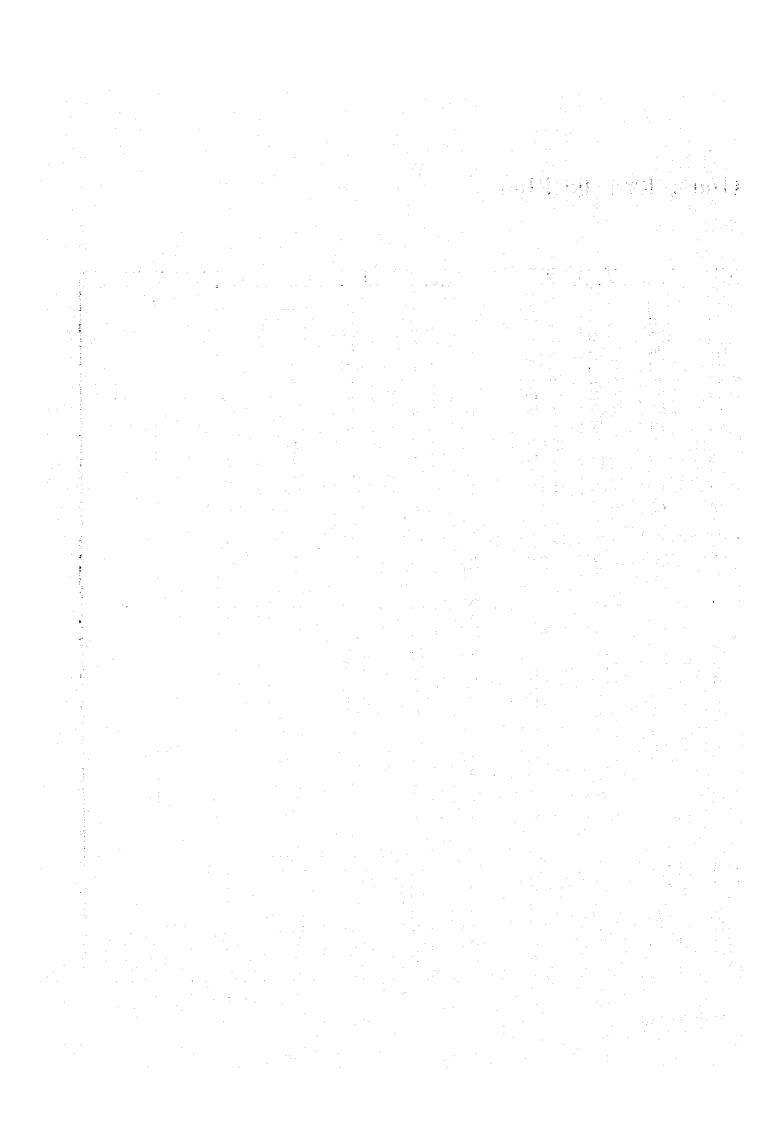
Production , Revenue Plan

Quantity of mining crude ore:100t/day x 300days/year=30,000t/year Quantity of treated ore:100t/day x 300days/year = 30,000t/year

Pb.Zn-Concentrate→Export to Japan

		unit	<u>-1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 </u>	2	3	4	5	6	7.	8	9	10	11	12	Total
Crude ore production	30 '000t/y	'000t/y	30		30	30	30	30	30	30	30	30	30		33
Grade of Pb	6.40 %	%	6, 40		6.40	6.40	6.40	6.40	6.40	6.40	6.40	6.40	6, 40	7	6.4
Minable Zn	2.90 %	×	2.90		2.90	2.90	2.90	2.90	2.90	2.90	2.90	2.90	2.90		2.9
<u> </u>	1.22 g/t	g/t	1.22		1.22	1.22	1. 22	1.22	1.22	1. 22	1.22	1.22	1. 22		1.2
Ag	161 g/t	g/t	161	161	161	161	161	161	161	161	161	161	161		16
Pb- Quantity		DMT/y	2, 371	2,371	2, 371	2, 371	2,371	2, 371	2,371	2, 371	2,371	2,371	2, 371		26, 07
	Recovery 85, 20%	%	69.00		69.00	69.00	69.00	69.00	69.00	69.00	69, 00	69.00	69.00		69.0
Grade of Au	Recovery 71.30%	g/t	11.00	11.00	11.00	11.00	11.00	11.00	11.00	11.00	11.00	11.00	11.00		11.0
	Recovery 74.00%	g/t	1,365		1,365	1,365	1, 365	1, 365	1, 365	1, 365	1, 365	1, 365	1, 365		1.36
Zn- Quantity	de la companya de la	DMT/y	1,351	1,351	1, 351	1, 351	1,351	1,351	1,351	1, 351	1, 351	1, 351	1, 351		14, 86
	Recovery 79, 20%	%	51.00	51.00	51.00	51.00	51.00	51.00	51.00	51.00	51.00	51.00	51.00		51, 0
Grade of Au	Recovery 7.70%	g/t	2.10	2.10	2, 10	2.10	2, 10	2, 10	2, 10	2. 10	2.10	2.10	2.10		2.1
Grade of Ag	Recovery 8.60%	g/t	579		579	579	579	579	579	579	579	579	579		57
Payable Metal Pb-C Pb Transportation	95 %	t	1,546		1,546	1,546	1,546	1,546	1,546	1,546	1,546	1, 546	1,546	WW. 4444 To 4 - 4-4-4	17, 00
Au loss 0.5%	90 %	toz	683		683	683	683	683	683	683	683	683	683		
Unit Discount	-1 g					on a market paragraph		083	083	683	683	683	683		7, 50
Ag	95.0 %	toz	98, 347	98, 347	98, 347	98, 347	98, 347	98, 347	98, 347	98, 347	98, 347	98, 347	98, 347		1,081,81
2n-C Zn Transportation	85 %	t l	583	583	583	583	583	583	583	583	583	583	583		6, 41
Au loss 0.5%	65.0 %	toz	31	31	31	31	31	31	31	31	31	31	31		34
Unit Discount	-1 g			ļ			31	31	31	31	31	31	31	***************************************	34
Ag	60.0 %	toz	11, 788	11, 788	11, 788	11, 788	11, 788	11, 788	11, 788	11, 788	11, 788	11, 788	11,788		129, 67
Unit Discount	-4 toz		1	11, 100	11,100	11, 100	11,100	11, 700	11, 100	11,100	11, 100	11, 100	11,700	·	129, 01
Conc Price Pb-C Pb Price	650 \$/t	'000US\$	1,005	1,005	1,005	1,005	1,005	1,005	1, 005	1,005	1,005	1,005	1,005		11, 05
Au Price	390 \$/toz	'000US\$	266	266	266	266	266	266	266	266	266		266		
Ag Price	5.3 \$/toz	'000US\$	521	521	521	521	521	521	521	521	521	266			2, 92
Zn-C Zn Price	1,100 \$/t	'000US\$	641	641	641	641	641	641	641	641		521	521		5, 73
Au Price	390 \$/toz	'000US\$	12	12	12	12	12	12			641	641	641		7, 05
Ag Price	5.3 \$/toz	'000US\$	62	62	62	62	62	62	12	12	12 62	12	12		13
Pb T/C	160 \$/DMT								62	62		62	62		68
Scale at 600\$ +14c/\$	100 \$/1911	'000US\$	394	394	394	394	394	394	394	394	394	394	394		4, 33
Ag R/C	30 c/toz	'000US\$	30						30				angelanen gebas.		
ns No	ou c/toz	00005\$	30	30	30	30	30	30	30	30	30	30	30		32
n T/C	190 \$/DMT	'000US\$	255	255	255	255	255	255	255	255	255	255	255		0.01
Scale at 1,250\$< +15c/\$,1,260\$> >1,000			200	200	- 200	200	400	203	200	200	200	200	299		2, 81
Penalty	\$/DMT/%	00005\$													
WATER Mary 10 to the common day of the common of the commo	\$/DMT/%	'000US\$		e o do agranto se a											
Insurance															
(Pb-C Price-T/C-R/C)x0.077%	0.077 %	'000US\$	1.054	1.054	1.054	1.054	1.054	1.054	1,054	1, 054	1.054	1.054	1. 054		
(Zn-C Price-T/C-R/C)x0.077%	0.077 %	'000US\$	0.354	0.354	0.354	0.354	0.354	0.354	0.354	0.354	0, 354		0.354		1
Preight			0, 334	0.034	0.004	0. 354	0. 334	0.334	U. 334	0. 334	0.334	0.354	0, 354		
Pb-C Moisuture 8%	80.0 \$/WHT	'000US\$	204	204	204	204	204	204	204	204	204	204	204		
Zn-C Moisuture 8%	80.0 \$/WMT	,000023	116	116	116	116	116	116	116	116	204 116	116	204 116		2, 24
Revenue Pb-C Price-T/C, R/C-i		'000US\$	1, 164	1, 164	1, 164	1, 164	1, 164	1,164	1, 164	1, 164	1, 164	1,164			1, 27
Zn-C Price-T/C, R/C-		00005\$	344	344	344	344	344	344	344	344	344		1, 164		12, 80
Total Revenue		000033	1,508	1,508	1, 508	1,508	1, 508	1, 508	1,508	1,508	1,508	344 1,508	1, 508	553	3, 78

Table 36 Production , Revenue Plan



Chapter 7. Initial, Additional and Replacement Investments and Operating Expenses

7.1 Estimated Initial Investment

7.1.1 Basis for assumption

As regards applicable Mongolian laws and regulations, and for estimation of salaries and wages, machinery prices, construction costs and general price level, the data and information as of September 1995 when the survey was conducted are used as the basis for assumption.

- (1) Development and construction period: One year
- (2) Infrastructure: The power transmission line from Helren to Tsav(80km) is laid by the state—run Choybalsan Electric Power Company. 50% of construction cost is to be borne by the Tsav mine.
- (3) Procurement of equipment and supplies: Those which are available in Mongolia are reinforcing steel bars and cement. All the other equipment, machinery and supplies have to be imported from Russia, China or Japan.
- (4) Customs duty: 7.5% of the FOR prices of imported equipment and supplies is included in the operating expenses.
- (5) Exchange rates:Mongolian Togrog(Tg) per US Dollar 450Tg/\$Japanese Yen(¥) per US Dollar ¥100/\$
- (6) Escalation: Not considered.
- (7) Rate of interest during construction: 6% p.a.

7.1.2 Initial Investment Summary

An annual projection of estimated divisional initial investment (up to project start-up) is indicated in Table.37, which may be summarized as follows:

	US\$'000	
(1) Mining division Excavation machinery, batch plant, trucks for mining operation	1,142	
(2) Mineral dressing division Construction of mineral dressing plant and equipment	1,386	0
(3) Auxiliary(common cost) division Power receiving facilities, transmission line cost sharing, office and accommodation construction	937	
(4) Tailing disposal (Initial—phase construction expenses are included in the operating cost)	341	
(5) Development preparation Head office overheads, customs duties	138	
(6) Interest during construction	240	0
(7) Working capital(10% of divisional initial investment)	347	
Initial Investment -	Total 4,531	

7.2 Additional and Replacement Investments

US\$530,000 is appropriated for the replacement of two LHDs in the sixth year after start—up. In reality, the amount is insufficient for proper replacement capital since the other mining machinery and vehicles including the jumbo should also be replaced, which is burdensome to the project cash flow, though. Therefore, replacement investment has to be limited to the minimum necessary.

Additional investment in phased construction of the tailing dam is included in the repair expense under the mineral dressing division's operating expenses, as in the case of the initial investment, for the second, fifth and eighth years, respectively, after start—up of operation.

7.3 Estimated Operating Expenses

7.3.1 Basis for Estimation

- (1) Exchange rate: Same as the initial investment
- (2) Salary and wage: For estimation, personnel are classified into three categories: staff, surface and underground. (Further classification by type of job is not made.) To the estimated salaries and wages, social insurance premiums of 3% and 1.5%, and labor accident insurance premium of 1.0% are added.
- (3) Consumables and machine parts: All the consumable items and machine parts, excepting cement and reinforcing steel bars, are assumed to be imports, which include explosives, detonators, mineral dressing reagents and fuels. The surveyed local prices in Mongolia of these goods are supposed to include customs duties.

{Customs duties: 15% on general goods and 7.5%(reduced rate) on mining machinery }

- (4) Electric power rate:

 At Choybalsan, the rate is 8 ¢ /kWh (= 36Tg/450Tg/US\$)

 Ref. 3.5 ¢ /kWh in Ulaan Baartaar
- (5) Royalty: 10% of the revenues
- (6) Agent's commission: US\$5.00 per ton of concentrate
- (7) Corporate income tax:

Profit before tax (PBT)	Tax rate
\$1 ~ 1,000	0%
\$1,001 ~ 33,300	15%
\$33,301 ~ 66,600	\$500 + (PBT - \$33,300) x 25%
\$66,601 ~ 100,000	$$1,300 + (PBT - 66,600) \times 35\%$
\$100,001 ~	$2,500 + (PBT - 100,000) \times 40\%$

7.3.2 Operating Expenses Summary

Annual projection of the direct (divisional) operating expenses (from mining to

concentrate production) and the indirect operating expenses are shown in Table 38 and 39, which may be summarized on an annual average basis, as follows:

	Annual average	per ton of
And the second	the second second second	crude ore
	(US\$'000)	(US\$/t)
Mining	699	23.3
Mineral dressing	348	11.6
Head office	35	1.2
Direct operating exp - Total	1,082	36.1
Depreciation exp	317	10.6
Royalty	151	5.0
Agent's commission	19	0.6
Operating Expenses - Total	1,569	52.3

Chapter 8. Financial Valuation

8.1 Internal Financial Rate of Return

To estimate internal financial rate of return(IFRR), a leading index in the financial valuation, it is vital to make a financial projection based on a well-defined fund sources and application. In turn, cash inflow and outflow items are sorted out and a cash flow chart is drawn up, wherein the net inflow, or difference between cash inflow and outflow, is calculated so that a rate of return may be determined.

8.1.1 Sources and application of funds

Funds required for realization of the project are composed of the initial investment, additional investment, interest during construction and working capital. Raising of the funds is planned as follows:

- (1) The project capital structure at the project start—up is assumed to comprize equity capital(30%) and borrowings(70%), which meets a normal equity—borrowings ratio in international projects. Funds required at the project start—up are those for the initial investment(in construction and equipment) and working capital. The working capital is estimated at 10% of the initial investment.
- (2) For the borrowing, low interest loans from an international financing agency such as the World Bank is contemplated, as the interest rates in Mongolia is very high in terms of international standards. The borrowing at the project start-up is a long-term loan while shortages of funds during operation is to be funded by short-term loans. Interest rate for these borrowings is assumed to be 6% p.a.
- (3) The 6% interest is to be paid against the outstanding loan balance as of the preceding year's end. The long-term loan principal is to be repaid in equal annual installments from the fourth to the eleventh year. The short-term loan principals are to be repaid whenever surplus cash flow is available.
- (4) Based on the assumptions in (1) thru (3) above, the total project capital consisting of equity capital and borrowings is assumed to be \$3,811,000, equal to the invested funds plus the working capital required for the operation phase. Therefore, the equity capital comes to \$1,143,000 while the borrowings to \$2,668,000.

8.1.2 Cash flow chart and IFRR

The project cash flow chart(profit and loss projection and fund sources and application) and IFRR are exhibited in Table 39.

The cash inflow side of the chart includes revenue from product sale and salvage value of equipment whilst investment expenditure, operating expenses, taxes and other expenses are included in the cash outflow side.

The corporate income tax is calculated in the following formula:

Corporate income tax = (Revenue - operating expenses - royalty - agent's commission - depreciation expense - interest) x applicable tax rate(ref. 5.3.1)

The straight-line depreciation which is generally used in Mongolia is applied to the project.

In the case of this project, the IFRR, a discount rate at which the present value of the total net cash inflow comes to zero, turns out to be (-)3.0%.

In this study, the income tax is calculated of the difference obtained by deducting all the expense (including interest) from the cash inflow (revenue) and, in turn, the tax is entered in the cash outflow; therefore, it is significant to evaluate the project's financial feasibility by comparing the IFRR and the interest rate for borrowing. The financial analysis for the project is considered unfavorable since the IFRR is far below the assumed interest rate of 6%.

investment			

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Irtici	le	, ,	levesteent	tiee	Book Tales	ta:	- 11	rear E Regrecia	Book Yalve		2 sd Book Tales			Rorecia	1th Sook Tales	tor	S th	Description	6 th	year Dececia-	7 th	Desceria:	Sta Pork Value	Dorrects:	9th	ter	1 Oth	Pear Descripts	1 1 th	Normal Section	Sale
Ing division					in			tio		tion		tion		Line	17	tios		tice		tion		lies		tice		tion		tion	Pa.Gax	lie	
to for Tielog	1 set	h	310,000	Н	5 31.	000 0.3	81		310,000	55,810	254, 260	55,800	159, 400	55, 630	142,630	\$5,800	86,600	55,800	31, 600		\$1,000		31,600		31,601	1	21, 169		31,400	į	
	ì set	l,	350,000			602 0.10			350,000	63,010	287,040	63. B(0	\$24,400	63,603	161,000	63,000	98,600	63,000	85,000		35,000		35,600		35,600		15, 000		35, KQ		
posed of Statereting	l sel	H	350,000		35.	100 0 11	10		350,000	63,010	287,000	65,000	224,000	61,001	261,600	\$3,000	58,100	63,600	35,000		35,000		35,500		35,000		35.400		15, KO		
r Treck (). EstD	1 set	П	43,060		s ((KO 0 11	50		40,00	7,200	32, 600	1, 200	25,500	7, 200	10,400	7, 206	11,200	7, 240	£ 000		4,000	- "	4,600		(.100		4,000		4.00		
Fauld Dusp(8.863)	I set		350,000		5 35.	260 0.11	10				1.17					17.	40		358,900	\$3,000	287,000	63,000	224,000	63.601	161,000	63,000	98,000	£3,000	15,000		
	l set l set	H	130,000 32,000			00 0 E		1	32,020	5, 763	26, 249	5,750	29, 430	5,760	[4,720	5,760	8,950	5,760	188,000 8,200	32, (10	\$47,608 3,208	32, 400	115,200	32,400	\$2,800 1,260	32,410	58,410 3,216	32,400	18, 000 3, 200		
Distript a 2 places	1 set		68,000		s .	0.10	10		69,000	10,800	49, 200	10,800	38, (00	16, 950	27,506	10,800	16,810	18,800	1,010		6,000		6,000		6,000		6,000		6,000		
ge Paup	Lat		40.000		0	100 6.11	13	100			49, 900	4. S00	35,500	4,500	\$1,000	4,500	26,500	4,501	22,030	4,590	17,500	1,500	13,000	4,560	8.500	4,500	1,000		6, 656		
Total of Minio al Dressing division	d dirisios	П	1,112,500	T	_UL.	106			1,112,900	205.569	\$26,400	218,460	766, 288	210,000	554,320	210,060	345,263	218,060	668, 298	59,501	\$68.340	. 59,5%	454, 490	99,910	256,500	19,900	265,690	95,410	171,200		
ing Gacitities fale	Anter Gra Cirara)	١,١	324,000			to 0.50			324,000	13,410	500,500	33,400	267,200	33, 609	223,836	33,400	208, (03	13,400	167, 600	13, (0)		33,400	100 200	33,400	44.44						
ė i			260,000			00 0.10			260,000	26,000	234,000	26,000	218,500	26,000	182,000	26,000	156,000	26.000	130,000	16,000	133,840	26,000	28, 600	26,010	66,800 52,000	25,406	33,400 26,600		33,400 26,600		
lite.	Car and	13	\$45,000			0.10		1 4	245,000	24,500	121,510	24,510	156,600	24,500	177,500	24,500	147,000	24,500	122,500	\$4,500	58,000	24,500	73,500	24,500	19,000	24,500	21,500	1	24,500		
irale Ob Zalbichnu Chicker, Faciliti		1 2	165, 600			10 0 10		1 . (165,010	10,550	148,510	14,510	132,000	14,500	115,500	16,500	15,000	18,500	81,500	16,500	66,046	16,500	43,501	16,500	33,500	66,500	16,500		16,500	- 1	
facility Gecycle		1:	110,000	-11:		90 8.10		1	110,610	11,000	83,010	11,010	88,000	11.000	77,000	11,000	\$6,000	11,000	15,000	11,000	(4, 90	11,000	33, 601	11,000	22,000	11,000	11,600		11,000		
trate terdine Place	: oraginity)	1 :	18,000	11:		20 4 10		1 1	12,000	1,200	14, 890	1,290	9,600 14,400	1, 200	12,660	1,200	7,200 16,800	1,800	6,000	1,200	4,620	1,200	1,605	1,200	2,400	1.200	1,200		1, 200		
lera.		,	61,000	.143		90 4 10		1 1	61,000	6,100	58,900	6,100	48,800	6,100	42,700	6,100	36.160	4,160	30,500	6,100	7,200 24,400	1,800 6,100	5, (0) 19, 300	3,828 6,106	\$,600 12,200	1,800 6,100	1,800		1, 810	- 1	
e-Office (021 m))	Iset	,	181,000	11		00 0 10			181.000	18,106	162,938	19,100	144,810	18,100	126,700	18,100	106,600	18,140	\$0,560	18.100	12,400	18.100	54,300	18,100	36 200	18,100	18,160		18, 100	- 1	
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				11		1				1																					
lotel of Rincral	d Dressing	Н	1,386,569	#	138.0	*	-		1, 355, 500	118,600	T10.00	_134,600	1, 200, 830	198,570	150,510	134,690	B11,664	135,600	\$53,000	138,860	554,400	139, 600	. (15,10)	138,500	277,200		138,800		111,00		
	L Wieclyle Pour Lie	ľ	267,000	11.					251,560	16,020	250,980	16,020	234,969	16,020	216, 545	16,828	202, 920	16,020	186,960	16,020	179, 692	16,620	151,800								
Borestory (650 ml)		ľ	165,000	113		62 6 10			165,060	16,550	149,500	18,500	132,000	16,591	115,590	16,500	35,600	16,500	12,500	16,520	56,600	16,500	49,560	16,625	128,840 33,000	16,020 16,530	182,820	16,020	166,830	16,020	
		ы	60,000	11		60 0.18			50,060	18,810	49, 280	10,100	38, 100	10,830	27,690	10,800	16,800	10,800	6,000		6,000		6,060	19.900	6.000	14.580	6,000		6,090	- 1	
or Transportation of	f Corcestrate(IIt)	,	50,000	11,		00 6 18	0		90,000	16,200	13,800	18.200	57, 600	16, 200	41,490	16, 200	25, 200	16,206	9,000		9,600		8,060	1	9,000		5,000		5,091		
ne facility of Elect	ttic Force	.	355,000	1	15.5	60 6 66	4		355,000	21,310	333,760	21,360	312,400	21,300	291,100	21, 300	269, 800	21,300	241,500	21,310	227,200	21,360	295, 940	21,100	154,690	21,500	163,300	21,300	142,001	29, 303	
Total of Coupon	a dizialea		337,006	#	224.0	60	-		537,600	80,870	66,114	£0,320	123, 160	81,634	694,549	. 10.131	.01.200		\$32,500	51,820	479,090	53.820	.01.30	52, 820	10.10	19,19	117.619	37,320	250, 303	37, 321	
	****	, ,	4.035.000		319,8		-		3, 465, 000	-	3,086,820		2,655,540	429, 195	2.221.000	429, 483		479, 480	1,892,100		1,599,780	292, 320			1.015,145	292,320	122,420			-	

Table 37 Investment & Depreciation of each division

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rsoral Expense	.		1				1.0	1			100				45.00							- 4	1 1	100	- 1		
	5/a-a	1,200.00			10	12,000	10	12.000	10	12,900	10	12,000	19	12,000	10	12,000	10	12,003	10	12,000	10	12,000	10	12,000	10	12,000	
	5/2-2	933.83		i	34	31,733	34	31,733	34	31, 733	34	31,733	34	31,733	34	31, 133	34	31,733	1 1	31,133	34	31, 133		31, 733	31	31,733	
	\$/0.0	1,125.00			26	29,120	26	29,120	26	29,129	26	29,120		29,126	26	29,129	26	23,120		29,120	26	29.120		25, 120	26	29,120	
fatel					79	72,853		72,853		72,453		72,853	79	12,853		72,853	79	72.453					26				
lation Expense						25,892				19,707		Laiden				76,001		(6.934				72.453		18-61		12,451	
	\$/1	3.37			30,600	101,100	33,000	101,100	30,000	101,100	30,000	191,100	30,000	101,100		101,100					44.44					122.	
	1/1	0.53			50,000	15, 500	33,000	15,500	30,000	15,900	30,600	15,500	30,000	15,900	30,000	15, 500	38,000	101,100	10,000	101,100	30,002	101,100	30,010	101,103	30,000	101,100	
	1/1	0.09			30,000	2,700	\$3,000	2,700		2,700	30,000								30,000	15,900	38,600	15,900	50,000	15,900	38, 990	15,900	
									38,000			2,700	30.000	2,700	30,600	2, 700	38,800	2,700	30,000	2,700	30,000	2,700	30.030	1,700	39, 800	2,700	
	\$/1	0.15			30,600	4,500	10,000	4,500	39,000	4,500	30,000	4,500	30,010	4,500	36,000	1,500	38,000	4,500	30,000	4,500	30,000	4,500	30,000	1,500	39,000	4,500	
	S/L	9.00	1 - 1		30,000	210,000	50,000	270,000	59,000	270,000	30,000	270,000	30,010	270,000	39,600	210,000	33,000	210,000	30,009	270,000	30,000	279.000	30,010	279,000	30,000	210,000	
		29				24,810		24.849		24,810		24,849		24,840	نند	24,840		24,840		24,840		24,849		24,640		24,840	
fetal						419,040		418.849		418,040		419,049		419,040		(13,900		419,010		(19,040		419,040		413,040		419,040	
poort Expense					100	1.9%		1.15	10.0	1	1.50	4 20				1000		1.0		3.00	1	4. 2		1.0	- 1	100	
	5/4	138.30		. 1	240	33, 192	240	33, 192	740	33,192	241	33, 192	240	13,192	240	33,192	249	33,192	240	33, 192	240	33, 192	240	33, 192	249	33,192	
sives	1/4	21.60	- 1		210	5,184	240	5.164	240	5,184	240	5,184	240	5, 184	240	5, 184	210	5.184	240	5,184	240	5, 184	240	5, 184	243	5,184	
aters	\$/4	3.70		- 1	240	888	240	888	240	888	2(0	888	240	888	240	858	240	638	249	888	240	888	210	858	249	858	
	\$/0	6.30		- 1	240	1,512	240	1.512	240	1.512	210	1,512	240	1,512	240	1,512	210	1,512	249	1,512	240	1.512	240	1,512	210	1,512	
nary · Electric Parts	\$/6	838.00		- 1	240	81,120	210	81,120	240	81,126	240	81, 125	240	81,120	249	\$1,120	210	81,130	242	81,120	249	81,120	240	81,120	240	81, 120	
		20	. [- 1	3.1	8,155		8,155		8.155	100	8,155		8, 155	""	8.155		E, 155		8,155		8.155		8,155	****	8, 155	
Total .	3					136.051		130,051		130,051	- 1111	130,051		130,051		130,051		133,651		130,051							
	(An	9.88			960,000	76, 800	968, 800	76,800	959,000	76,800	960,000	76,800	960,000		0.00 000		NA MA		A/0.000		A42 400	130,051	200 200	130,051		_130.05t	
direct Express Total					302,309	658,745				638,745	200,000		_ 499,599	26,800	960,000	76,850	960,000	76,400	960,000	76, 899	960,000	76,800	999,600	76,800	364,900	75,830	
	in	1					PROFES TO SERVICE SERVICES	691.165				638,745		698,745		_638,7(5		898,745		698,745		698.765		638,745		698,745	
	30					23, 21		23.29		23.24		23.23		23 23		23 29		23 29		23,25		23,29		23.29		23.29	
Expense		- 1	- 1		- 1				1.1	- 1			1.0			- 1						1			· 1		
1 Dressing Division		i	j	- 1	- 1	1		1			- 1			-	1.0												
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	/4-4	1,200.00			- 1	4, 830	- 4	4,800	. (4,800	- 4	1,810	4	4, 800	- 1	4,800	- 4	4,800	1.0	4,800	- 0	4,100	[4]	4,800	+	4,800	
rior 4	Vara	933.33				16,800	18	16,800		16,800	18	16,870	18	16,800	0	16,800	18	18,800	18	16,535	0	16,800	18	16.630	18	16,800	
Total						21,600		21,600		21,600		21,600	2000	21,600		21,600		21,690		21,500		21, 600		21,500		21,600	
I Expense and others	- 1							. 1	. 14.	3.5			4.11	1 13.				4.00					-				
ical Rosgest : 1	1/1	.1.52	1		30,000	45,640	30,090	45,600	39,660	45,600	30,000	45,600	30,000	(5, 600	30,000	45, 600	30,000	45,610	30,000	45,600	30,000	45, 500	30,000	45,500	39,000	45,600	
s-Mill Liners 1	1/1	0.14	.	.	30,000	4,280	30,000	1,209	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	35,600	4,200	30,000	4,200	30,000	4,200	30,000	6,200	30,000	4,200	
forB.C. and Filters 1	1/1	0.12			30,000	8,600	30,000	3,600	39,910	3,600	30,000	3,500	30,000	3,600	31,000	3,600	30,000	3,600	30,000	3,600	38,000	3,600	30,000	3,600	36,000	3,500	
	1/1	0.51			33,000	15,500	30,000	15,900	30,000	15,910	30,000	15,900	30,000	15,900	30,000	15,500	38,000	15,990	30,000	15,900	30.009	15,900	30,000	15,900	30,000	15,900	
	1/4	1.56	.		33,000	46, 810	30,000	46,830	30,000	45,830	30,000	45,800	30,000	45,800	31,000	46, 830	30,000	46,810	30,000	46,830	28,000	46,830	30,000	45,800	30,000	45,800	
	\$/1	0.34	1	. 1	30,000	16,200	30.000	10,200	30,000	10,200	30,000	10,200	30,000	10.200	30,000	10,200	38,000	10.200	30.000	10,240	30,000	10,200	30,000	10,200	30,000	10.200	
	Dan		. 4	341,000	30.000	10.000	30.000	206,000	~	10,200	30,000	10.200	30,000	206,000	. 20.004	10,240	30,000	10.000	30.000	206.000	30.00	10, 200	30,000	10, 200	30, 900	10,200	
	1/1	0.11	- 1	341,000	30,000	1 600	30,000	4.200	30,000	4,200	100		- 44 44		4.00		20.00					10.00	1				
	311	0.68]	1	1,295,000	103,580	1,296,000			103,580	30,000	1,200	30,000	4,200	33,000	4,200	30,000	6,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	
			- 1					103,650	1,236,000		1,296,000	103,689	1,295,000	183,680	1,256,000	103,680	1,295,000	103,680	1,295,000	193,680	1.296,000	143,685	1,296,000	103,680	1,295,000	103,680	
	#/C	0.18			30,990	5, 698	30,000	5.400	30,000	5,400	39,090	S, 400	32,091	5.100	20,000	5,400	30,000	5, 400	30,000	5.400	30,030	5, (09	30,000	5,490	39,600	5, 600	
fotal				\$41,000		239,580		445,550		239,580		233,583		415,580		239,590		139,500		145,580		239,588		239,560		239,580	
	*			211.500		261,183	!	467,155		261, 163		261,189	1	457, 180		261, (60)		261,183		467,130		251,182		261, 180	1	261, 180	
	\$4.			11.31		8.71		15.57		8, 71		121		15.57				8.71		15.57		3,11		8.71		2.11	
Expense	. 1	- 1		- 1	ı	- 1	- 1	- 1	- 1	10.00			-		1.5	. 1	. "	.]		i		- 1				i	
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al Expense	- 1	. 1		- 1	1		- 1	- 1		- 1			- 1	- 1		- 1	- 1			- 1		1	į	- 1	- 1		
	4.1	1,200.00	ان ا	7,200		7, 200	ا ،	7,200		1,200		7,200	أد	7,200	1 1	7, 201		7,203	أر	7, 200		1,200				2 200	
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portation Expense	- 1.	. 1		3,000		1,000		3,000		3,000	- 1	3,000	į	3,000	1	1,000	- · · · •	1,000		1,000	1	1,010	. i	1,600	1	1,000	
			. i			43,000	- 1	3,000		3,000		3.000		3,000	. 1	43, 600	- 1	3,000		3.003		3,000	. [3,009	1	3,000	
ers on Fachinary forly feve	astacit)			125,950												4.95		4									
								11,200 1		11,202	5 7 7 1	11,200		11, 200		\$4,175		13,220		11,201		(1,200)					
Total Grand Total				138, 150 419, 150		51.250 1.011.125		1.117.125		971,125		\$71.125		1.177.125		1.054,100		971.125		1.171.125		971,125		970,125		171.125	

Table 38 Direct Operating Expense

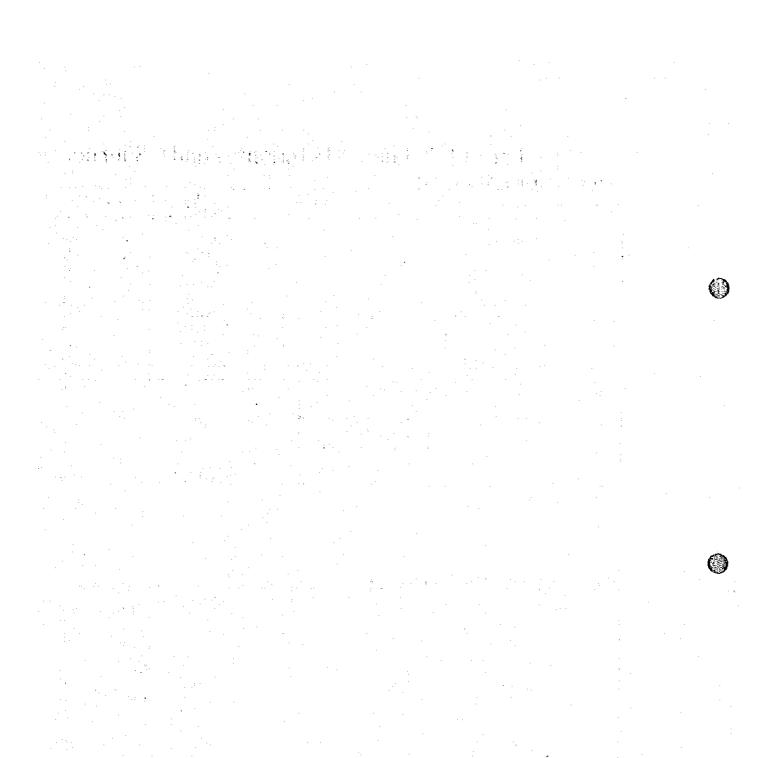
Profit & Loss Statement Funds-Sources and Application Internal Financial Rate of Return

		Unit	-1	1	2	3	4	5	6	7	8	9	10	11		Total
Renenue		'000US\$		1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	553	17.13
Expense																
Direct Operat-Mining		'000US\$	0	699	699	699	699	699	699	699	699	699	699	699		7,68
ting Expense Dressing		'000US\$	341	261	467	261	261	467	261	261	467	261	261	261		3,83
Head Office		'000US\$	138 479	51	- 11	11	11	11	94	11	11	11	11	11		38
Total		'000US\$	479	1,011	1, 177	971	971	1, 177	1,054	971	1, 177	971	971	971		11,90
Royality Revenuex10%	10 %	'000US\$	0	151	151	151	151	151	151	151	151	151	151	151		1,65
Agent Comis.Conc Qualityx5\$	5 \$	'000US\$	0	19	19	19	19	19	19	19	19	19	19	19		21
Depreciation		'000US\$	0	425	429	429	429	429	292	292	292	292	133	37		3, 48
Interest	6 %	'000US\$		178	190	191	181	170	170	195	185	186	176	165	136	2, 12
Total		'000US\$	479	1,784	1,966	1, 762	1,752	1,947	1,687	1,629	1,825	1,620	1, 450	1,344	136	19,38
Profit before Tax		'000US\$	-479	-276	-459	-254	-244	-439	-179	-121	-317	-112	58	164	416	-2, 24
Tax Corporate Profit(0	0%	*000US	0	0	0	0	0	0	0	0	0	0	22	64	165	25
Income Tax Profit(1,500/4							1 110									F
Profit<3,000/4	50*000\$ 25%						1.0					,				
Profit<4, 500/4	50*000\$ 35%															1
Profit>4, 500/4	50*000\$ 40%															
Total			0	. 0	0	0	0	. 0	0	0	0	0	22	64	165	25
Profit after Tax		'000US\$	-479	-276	-459	-254	-244	-439	-179	-121	-317	-112	36	100	251	-2.49

Funds-Sources and Application			100	3.53	de la			<u> </u>								
		Unit		1	2	3	4	5	6	7	8	9	10	11		Total
Renenue Profit after Tax		· '000US\$	-479	-276	-459	-254 429	-244	-439	-179	-121	-317	-112	36	100	251	-2, 492
Depreciation		'000US\$	0	425	429	429	429	429	292	292	292	292	133	37		3,482
Allowance for Reinvestment		'000US\$							la vanima vanima l				I :			0
Equity of Capital		'000US\$	1, 143								- transition of the same	Linical manager.				1, 143
Long-term Borrowings		'000US\$	2,668	اعتفدت								-	1		BOOK 11 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	2,668
Short-term Borrowings		'000US\$	293	198	29		148	343	750	162	358	153	164			2,598
Total		'000US\$	3,625	347	-0	175	334	334	863	333	334	333	333	137	251	7,399
Expence Investment		00008\$	3, 465	and the second				ar simulation	530						l	3,995
Interest during constructi	on	'000US\$	160								nitration was a base					160
Working Capital		'000US\$		347										-347		0
Repayment of long-term Box		'000US\$				المكاملة في المال	334	334	334	334	334	334	334	334		2,668
Repayment of short-term Bo	rrowings	'000US\$		and a state of the	. ma omelian.	175							1	150	2,273	2,598
Total		'000US\$	3,625	347	0	175	334	334	864	334	334	334	334	137	2,273	9, 421
Cash flow surplus		'000US\$	0	. 0	- 0	0	0	0	-0	-0	0	-0	-0	0	-2,022	-2,022
Total Cash flow surplus		'000US\$	0	1	0	1	1	1	1	1	1	0	-0	-0	-2,022	-2,016
Cashflow		'000US\$	-3,944	-20	160	366	366	160	-247	366	160	366	345	649	388	-882

Cashflor-Cash flow surplus-Equity Capital-Borrowings*Repayment*Interest
DCFIRR= -3.0% NPY(-4%)= 358
NPY(-3%)= -15

Table 39 Profit & Loss Statement-Funds-Sources and Application Internal Financial Rate of Return



Chapter 9. Economic Valuation

9.1 Shift from Financial Cost to Economic Cost

The financial analysis attempts to appraise an investment project from the private investor's standpoint. It lays emphasis on whether the project will generate a due reward and seeks for conditions for the profit maximization. On the other hand, the economic analysis is to evaluate project feasibility from the viewpoint of national economy, in search of the most efficient utilization of public resources as the evaluation criterion.

The economic analysis, therefore, requires adjustment of transfer costs employed in the financial analysis, calculation of opportunity cost, modification of exchange rates to be applied, adjustment of cost of public goods, etc., as detailed in the following paragraphs.

9.1.1 Adjustment of transfer cost

For computation of project economic cost, transfer costs such as taxes included in financial cost have to be adjusted or deducted. In this study, the customs duty imposed on imported goods, the commodity tax included in local commodity prices, the corporate income tax imposed on operating profit, and the royalty levied on sales revenue are deducted as transfer items. The other transfer costs are left unadjusted as they are considered negligible.

For the customs duty adjustment, 15% on general goods and 7.5% on mining machinery, etc. are deducted from the financial costs of imports. As for local goods, the 10% commodity tax is deducted from their financial costs.

In the actual calculation, 95% of material cost included in the (financial) operating cost is assumed to be imports while the remaining 5% is assumed to represent local procurement, from which 15% or 10% are deducted as the tax portions, respectively. 10% is also deducted from the local transportation cost.

As regards the initial investment cost, 30% of the cost of those equipment that requires erection work is assumed to be local costs(for erection and local transportation), from which 10%(commodity tax) is deducted, while 7.5%(customs

duty) is deducted from the remaining 70%(imported mining machinery).

9.1.2 Estimation of opportunity cost of labor

This study assumes that, as for demand and supply of skilled labor(staffs) in Mongolia, the market mechanism is relatively well functioning under nearly perfect competition and, therefore, labor cost is determined at a level reflecting the actual situation of the Mongolian economy, free from market distortions. Based on the assumption, opportunity cost of skilled labor is determined by the actual market rate, which is same as the labor cost in the financial analysis.

As for opportunity cost of unskilled labor, the question is not as simple as skilled labor. In Mongolia, as well as in Choybalsan, the unemployment rate is very high. The labor market is in a state of excess labor economy. This implies that opportunity cost of unskilled labor stays at a rate considerably inferior to the actual market rate of wages applied as the financial cost.

According to the public employment security office at Choybalsan, about 3,900 out of the city's total population of 40,000 are unemployed and 70% of the unemployed is youths under 32. In this study, therefore, opportunity cost(economic cost) of unskilled labor(workers other than staffs) is assumed to be a half of the financial labor costs.

9.1.3 Modification of exchange rate

It is a general practice to observe the national trade balance, changes in the wholesale price level, etc. to find out a real(shadow) exchange rate to be applied to the economic valuation of a project. In the relationship between the past Mongolian trade/price data and the official exchange rates, however, regularities are not necessarily recognizable, probably because the nation is still in the process of transition to a market economy since 1989.

Owing to the dear interest policy persued in Mongolia to depress the hyper-inflation, the Togrog seems to have been over-estimated. But inflation rate has declined from 325.5% in 1992 to 66.3% in 1994 and recently, it has settled down to a level of 2% per month. Besides, most of the project equipment and machinery which constitutes a major part of the project costs are imports which

are settled in US Dollars. Considering these factors, no modification is made in this study on the exchange rate used for the financial analysis.

9.1.4 Cost of public goods

Since the cost of laying the power transmission line is the public expenditure, only 50% of the total cost, which must be borne by a user, is included in the financial costs of the project. For economic analysis, however, the full cost must be counted in.

9.2 Internal Economic Rate of Return(IERR)

Unlike the financial analysis, the economic analysis focuses on a difference between cost and benefit in terms of economic price, after eliminating the transfer cost such as tax.

All the goods and services related to the project are divided into the foreign currency portion(traded goods) and the local currency portion(non-traded goods), the former's value being measured with a shadow exchange rate. (In this study, however, the same official exchange rate is applied, as explained.)

In accordance with these procedures, profit and loss projection, fund sources and application and IERR exhibited in Table 40 have been calculated, on the basis of the operating expenses, divisional initial investment cost and depreciation expenses exhibited in Table 41 and 42. The discount rate at which the present value of net benefit(benefit less cost) of this project comes to zero is 8.3%. In order to judge the project desirability from the national viewpoint, IERR is used as a criterion. The World Bank is said to consider an investment project feasible when IERR is not less than 12%, whilst 8% is the lower limit for the USAID and 10% for the Asian Development Bank. Whether or not this project is feasible from the viewpoint of national economy is a delicate question to answer.

Profit & Loss Statement Funds-Sources and Application Internal Economical Rate of Return

		Unit			2	3	4	5	6	7	8	9	10	11		Total
Renenue		'000US\$		1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	622	17, 20
Expense						in the America										
Direct Operat-Mining		'000US\$	0	588	588	588	588	588	588	588	588	588	588	588		6, 47
ting Expense Dressing		'000US\$	310	226	413	226	226	413	226	226	413	226	226	226		3, 35
Head Office		'000US\$	11	51	11	11	11	11	51	11	11	11	11	11		21
Total		00008\$	321	865	1,013	825	825	1,013	865	825	1,013	825	825	825	- 110 17111 2 2 2 2 2	10.0
Royality Revenuex109	0 %	'000US\$	0	0	0	0	0	0	0	0	0	0	0	0		
Agent Comis.Conc Qualityx	5\$ 5 \$	'000US\$	0	19	19	19	19	19	19	19	19	19	19	19		21
Depreciation		000US\$	0	432	437	437	437	437	301	301	301	301	146	50		3, 58
Interest	6 %	'000US\$	11.	175	170	168	168	147	126	105	84	63	42	21	-0	1, 26
Total	5.7	'000US\$	321	1,492	1,639	1, 449	1,449	1,616	1,312	1,251	1,417	1, 209	1,033	916	-0	15, 10
Profit before Tax		'000US\$	-321	16	-131	59	59	-108	196	257	91	299	475	592	622	2,10
Tax Corporate Profit<0	09	'000US\$	0	0	0	0	0	0	0	0	0	0	0	0	0	
Income Tax Profit(1,50																
Profit<3,00	0/450*000\$ 25%															
Profit<4,50	0/450*000\$ 35%	11										incommer sum				
Profit>4,50	0/450*000\$ 40%		1.0		- 100	1.5			*, .							
Total			0	0	0	0	0	. 0	0	0	0	0	0	0	0	
Profit after Tax		00005\$	-321	16	-131	59	59	-108	196	257	91	299	475	592	622	2, 10

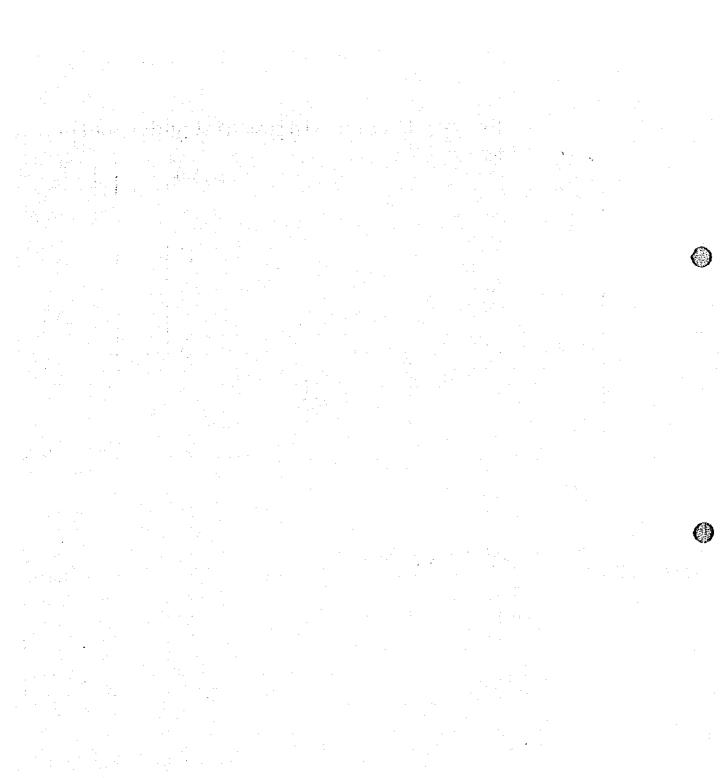
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				-	-											*************
		Unit			2	3	4	1 5	6		8	9	10	- 11		Total
Renenue	Profit after Tax	'000US\$	-321	16	-131	59	59	-108	196	257	91	299	475	592	622	2, 105
	Depreciation	'000US\$	0	432	437	437	437	437	301	301	301	301	146	50		3,580
	Allowance for Reinvestment	'000US\$														0
	Equity of Capital	'000US\$	1, 198			- 15										1, 198
	Long-term Borrowings	'000US\$	2,796													2,796
	Short-term Borrowings	000US\$	125													125
	Total	00005\$	3, 799	448	306	495	495	329	497	558	392	600	621	642	622	9, 804
Expence	Investment	00003\$	3,632			1.00			530							4, 162
	Interest during construction	'000US\$	168												-	168
man and a line realism.	Working Capital	'000US\$		363										-363		0
	Repayment of long-term Borrowings	'000US\$					350	350	350	350	350	350	350	350		2,796
	Repayment of short-term Borrowings	000US\$		85	40									1		125
	Total	'000US\$	3, 799	448	40	0	350	350	880	350	350	350	350	-14	0	7, 251
Cash flow		'000US\$	-0	-0	266	495	146	-21	-382	209	42	251	272	656	622	2, 553
	flow surplus	000US\$	-0	-1	265	760	906	885	503	711	754	1,004	1, 276	1, 932	2,553	11, 547
Cashflow		20001154	-3 952	260	476	663	663	476	93	663	476	663	663	1 028	622	2 701

Cashflow=Cash flow surplus-Equity Capital-Borrowings*Repayment*Interest DCFIRR= 8.3% NPV(8%)= 57 NPV (9%) =

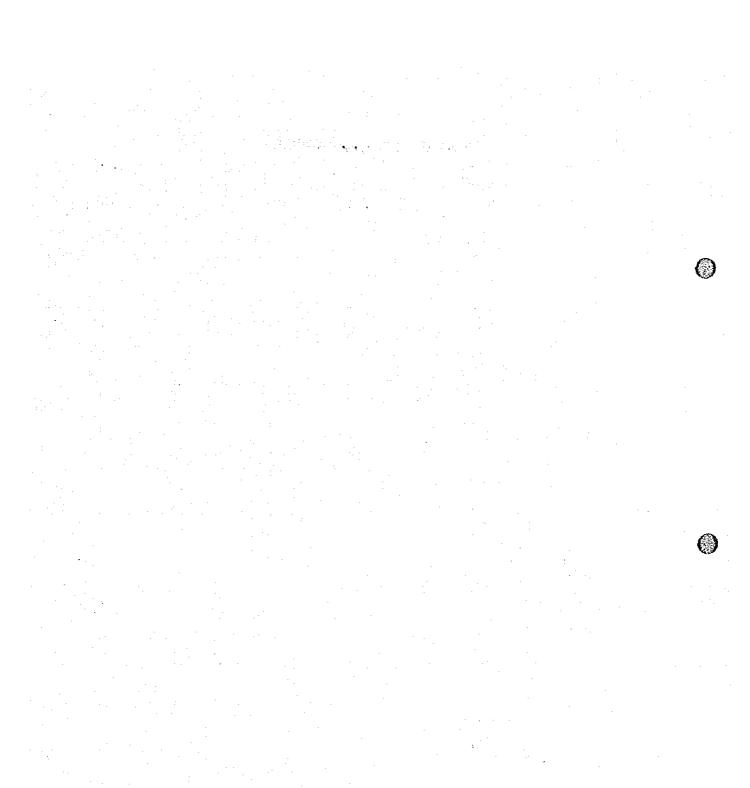
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Table 40 Profit & Loss Statement Punds-Sources and Application Internal Economical Rate of Return



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ding division Personal Expense		1.0		100		1.4		1.74					19.00		1		T	7			Tanada.	- San	- Santa		- Maillo	/4/201		
Staff	\$/4.4	1,200.00	1	1	10	12,020		12,000	10	12,000	10	12,000	10						177									
Exterior	\$/6.1	465.67	1]	34	15,817	34	15,857	31	15,867	14		34	12.000 15.867	10	12,000				12,000	10	18,000		12,000	10	12,000		
Interior	5/6:2	500.00	l_	1	26	14,596	26	14,550	25	14,560	26	14.550				15.867	1			15.857	34		34		34	15,867		
Total					79	12.427		42, 127	20	47, 427		12, 127	26	42,427	36	14,560			26	(4,560	26		26	14,560		14,564		
ploitation Expense	1													10,761		43, 427	2	13,627		12,427		12, 427		42.421		_0,07		
lits - lods	5/L	2.94		1	30,999	88, [13	30,000	88,113	30,000	85,113	30,000	88,113	50,000	83, [13	30,000	85, 113	30,000	88,113	30,000			10.00	100					
iplasives	\$/1	0.46	100		38,000	13,858	30,000	13, 858	50,000	13.858	30,000	13.858	30,020	13,858	30,000	13,858			30,000	88,113 13,858		88,113	30,000	88, 113	38,900	88,113		
otonaters .	\$/1	0.01			30,000	346	30,000	346	\$0,000	346	30,000	145	30,030	346	30,010	345			30,000	73.635	30,000		30,000	13,858	38,000	13,858		
oels	5/t	0.13	1	l	35,000	3,528	30,000	3.922	30,006	3,922	30,000	3,912	30,600	3,922	30.030	3,922			33,600	3,922	30,000	346	39,000	346	30,000	348		
Cachinary · Electric Parts	s/t	7.86		- 1	34,000	235, 316	30,000	235, 316	30,030	235, 316	30,000	235, 316	30,000	235, 316	30,000	235,316	38,000		50,000	235, \$16	30,000		30,000	3,922 235,316	30,006	3,922		
hers(204 of abovementioned)	. X	20				21,248		21,245		21,248		21.248		21, 248		21,248	1	21,248		21,248	30,000	21.248	34,000		30,000	235, 314		
						363.802		363, 302		162.802		\$62,802		362,802		262, 892	1	362,802	1	\$62,802		362, 892		21,248		352,632		
velopacst Expense	1	1. A.A.				2.2		ale di				120			- ,7					12524		200,000	h	363.802				
Bils · Rods	5/a	120.53		- 1	240	28, 928	240	28,928	240	28,928	249	28,928	245	28,92\$	240	26, \$28	240	28,928	240	21,928	210	28,926	240	28,928	243	28, \$28		
Deplosives Deforators	1/a 1/a	18.83			243	4,518	249	6,518	247	4,518	240	1,518	219	4,518	248	4,518	240		240	1.518	240	4,518	210		240	4,518		
Petoratera Tuela	1/4				240	774	210	774	240	174	240	ne	249	174	210	1116	240		240	714	240	174	240		240	ne		
Gels Gehinary · Electric Parts	5/4	5.43 294.58			240	1,318	240	1,316	249	1,318	210	1,318	240	1,318	240	1,318			240	1,318	240	1,318	240	1,318	240	1,318		
ors(20% of aborescutioned)				ļ. :	210	70, 693	240	70,699	240	76, 699	240	70,699	249	70,639	248	70.659	210	70,699	240	10.639	249	70,699	240	70, 695	240	70,695		
Total		50				7,148		7,106		7,108		7,106		7,198	سنديد	7,198		7,108		2,101		7,168		7,165		7.199		
lectric Fee	\$ 403	0.07			205 005	113.345	***	113,345		113.345	100000	113,345		113,365		113, \$45		D1.16		113,245		118,345		113 345		113,345		
ing direct Espense fotal	1				\$60,000	\$9.518	960,000	65.818	960,000	69,818	950,000	62, 614	900.000	69.818	369.000	69, 618	950,600	69, 818	\$68,000	69.818	950,000	69,818	\$50,000	69,818	368,600	63.818		
ton of Vieles direct	\$/\$					\$38,392		588,392		548, 292		588, 392		533,382		568.193		588, 392		588_332		588, 192		538, 392		548, 592		
Expense	-23-1					19.61		.13.51		18.61		13,61		19.61		19.61		19.61		19.61		15,61		13.61		19.61		
eral Dressing Division	- 1				- 1					4.5	11						1.2	1 1				i	1					
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eterior	5/2.2	455.67			18	8,400		8.600		8,400				4, 800	4	4,810		4,830	. 4	4,830		6,800		4,800	4	4,800		
Total						13,200		13, 200		13,200		13,200	18	8,400		8,409	18	8,100	16	1,100		8, 430	18	8,400	18	8.490		
terial figures and others												19.249		13,200		13,200		13,200		13, 200		13,290		13,290		13,200		
Desical Rescet	1/4	1,32		- 1	36,000	39, 1(2	30,000	39, 742	30,000	39 742	30,000	29, 141	30,000	39,742	30,000	39,742	36,000	l	34.33		11.75	100				- 1		
alls - Mill Liters	1/t	0.12			30,000	3,650	30,000	3,660	30,000	3,680	39,600	3,650	30,009	3,650	30,000	3,690	30,000	39,142	30,000	39, 142	30,000	35,742	30,000	39, 742	\$0,600	39, 742		
lets for B. C. and Filters	\$/t	0.10	i	- 1	30,000	3,138	34,000	3,138	30,000	3.138	30,000	3,138	30,000	3, 138	30,000	3,138	30,000	3,138	30,000 30,000	3,650	30,000	3, 661	30,000	3,690	\$9,000	3,660		
uels	\$/t	0.46		- 1	30,000	19.858	20,000	13, 858	30,000	13, 858	30,000	13,656	30,000	13,858	30,000	13,858	30,000	13.858	30,000	3,138	31,600	3, 138	30,000	3,139	30,000	5.138		
lachinary - Electric Parts	\$/L	1.36	1.5		35, 600	10,788	39,000	40, 788	30,000	10,748	30,600	10,758	30,000	49,788	30,400	40,768	30,000	40,788	30,000	13,858 40,788	30,000	13,858	39,000	13,858	30,000	13,858		
opair Expense	\$/1	0.30			30,000	8,890	38,000	8,890	30,000	8,830	38,800	8, 899	30,000	8,835	31,000	8, 890		8,890	30,000	8,890	30,000	8.830	30,600	49, 785	30,000	10,788		
	re Dua	4		310,000	4.14		1.1	187.273			- 1			187,273				*	30.020	187, 273	. 20,000	6.630	30,000	8,890	30,000	8.890		
talysis and others	\$/1	0.12		1	35,000	3.660	39,600	9,669	30,000	3.660	30,000	3,660	30,000	3,650	\$0,000	3,660	30,660	3,665	30,000	3,690	30,000	3,660	20.000					
	S/Aria	0.07			1,295,000	94, 255	1,295,000	94,255	1.255,000	34, 255	1.296.000	\$4,255	1.296.000	34,255	1, 256, 000	\$4,255	1,236,000	\$1,255	1,295,000	84, 255	1, 296, 000	94, 255	30,000 1,256,000	3,660 14,255	30,000	3,660		
	5/3	9,16			39,010	4.901	30,000	1,500	39,620	1,505	30,000	4,909	30,000	4,903	30,000	4.909	30,000	4, 909	20,000	4,909	30,000	1.303	30,000	4, 509		34, 255		
total				210,010		212,900		400,173	.:	212,900		212,900		400,173		212,900		212,900		430, 173		212,300	30,390	2/2,900	29,500	1, 999 212, 900		
ssing Direct Expense Total	1			310,000		226, 160		413,373		225, 100		226,100		412,373		226, 100		226,100	-	413.373		226,100		225, 100		235,100		
	\$/1			10.33		2.51		13.78		2.54		7,54		13.78		7.54		7.54		13.78		7.54		7.54		7.51		
Expense	- 1		- 1	. 1	- 1	- 1		1.0				- 1							-							a5:2**		
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exportation Coperse	i	- 1	- 1	2.127	- 1	12,727	- 1	2, 727		909		909	- 1	909	1	509	- 1- 1	509	- 4	309	-	919	İ	909		505		
10 A 10 A 10 A 10 A 10 A 10 A 10 A 10 A	estech	,			. 1	10,000		6.161	1	2,14		2,727		2.727		42.727		2.727		2.727		2,727		2.727	i	2,727		
Total .				10,336		50.836		10,836		16, 835		1449		18.84									I					
Grant Total				320,836		835, 328		612,601		125, 328		10, 636 825, 328		10.836		\$4,531		19,838		19.835		10.135		10,876		10.836		
	\$/3					28 84		33.75		27.51		27.51		1.012.691		865, 324		825, 328	4.7	1.012.601	1	125, 121	- 1	825, 328	- 7	\$25,328		

Table 41 Direct Operating Expense(Economical)



																						+									W1:US\$
Article		i.	1000	ijer Lier	Besident Book Talas	laves	2000	No.) pl Senk falus	rar Decrecia	2 td y	dar Brendela	3rd y	ear Doorocia	4th s	rar Bescecia	51h	tar Deprecia	6 th	rear Descecia	7.0 P	ear Poprecia- 1	Bib r	ear Bootecla	9 in s		1 O to		i i ii		Jete
ilig division		Ĭ		T	1			T t	ite	tion		tion		\$ ito		tion		tion		tion		tica		lies		tion		tion		ties	
An for Histor 1 s			315,040	11.	31.00	0 0 18			310.600	\$5,810	254,200	55, 898	158,400	55, 809	142,600	\$5,800	ts. 600	55,600	31.010	. ***	31,000		81,000		31,000	- 1	31,000		21,000	l	
TO THE REPORT OF	•	П		Ш				ļ										İ		1.0	- 1		•			[
cher Flant 3 s	et	,	340,455	,		S 8 16			\$40,455	61.282	275, 173	E1, 212	217,891	61,212	156,603	61,232	\$5,\$27	\$1,292	10,46		34,045	.	36,645	.	34, 845		34.045		34,045		
ipocat of Shaterellos 1 s	et ,	1	350,000	5	35,50	0 6.18	9		\$55,000	63,000	287,000	63,600	224,000	63,000	163.000	63,000	\$5,000	63,000	35,401		22,000		35,000		23.000		33,500		,		
er Truck(). 8a3) i s	et)	(8, 60)	1	4,00	0.18	•	1	49,006	1,200	12,102	1,200	25,600	7,200	(8,406	7,230	11,890	7, 200	4,000		£ 900		4.000	-	4,000		4.600	.]	4,000		
		П	100	11														. 4.1	150,000	63,000	287, 109	63,00á	224,600	63,000	161,000	63,000	13,600	\$3,600	15,000		
Build hope (Salt) 1 s	iel	П	350,002	11,	35.0	0 18	1			- 2	1								1977	100	100		1.		1.1	47.1	50,100	12,490	18,000	.	
(d fine) d Bane (1, 762) 1 : (d (1,1) y 2 places 1 :		Ш	180,000 32,000	1	18.0	0 0.18			32, 160	5,750	26, 240	5,766	20, 650	5,162	14,720	5,760	8,550	5, 769	189, 000 3, 200	32, 693	3,200	32,400	115,200 3,200	32, 400	82,600 3,200	\$2.480	3,200	12,410	3.200	1	
	F					0 0 18			60,000	19.630	49, 200	10,500	38,490	19,899	27,600	10,600	16,800	16,830	6,000		6,000	.	6,000		6,600		6,000		6,000		
on (350kg) a 2 pieces 1 s	wt		68,010	,		. *							100		40.4	6,500	25,500	(.590	22,000	4,500	17,500	6,590	13,030	4,500	8,560	4,500	6.900	1	4.000		
sace Puno	wt		40,010		4,00	0 0.21	1				49,000	4,500	35,500	4,500	31,800	6,500										-			170, 245		
Total of Rinics di tral Dressing division	elsion		1,762.65	- -	170.8	5	-		3, 132, 455	293,842	968, 613	208, 342	760, 271	208,312	\$50, 920	205, 342	10.50	209, 242	F15,265	59,900	\$65,145		_455_445	_19,300	365, 545	99,500	265,665	55,400	10,410		
			324,891	11.		8 8.10			324,851	32, 489	252, 102	32, (83	259, 913	32,419	227,424	32, 489	134, \$35	32,689	162, 465	32,413	129, 956	32,03	97,467	32, 481	66,578	32, 485	32, 485		32,489	ļ	
sking Gacilities Brickses ling	r.ore strages	1	252,508			0.10			252,599	25, 291	227,618	25, 291	202, 327	25,291	177,036	25.261	151,765	25,251	124, 455	25,291	101,164	25,251	25, \$13	25,291	59,512	25, 291 23, 832	25, 291 23, 832		25,291 23,832		
atetion		2	238, 318	1		12 0.10		.	236, 318	23, 832	214,486	21, \$32	190,855	23,432		23, \$12	142.991	23, 832	113, 159	23,832	\$5, 527	23,832	71, 456 48, 150	21,832 16,050	47,664 32,100	16,010	16,050		16,060	i	
centrate Gb Zethichner. F		2	160,500	1		50 0.10		i	160,500		100,650	16,050	128, 400	14,456	112,350	10,700	\$5,300	16,850 19,790	80, 250 53, 500	16,650	E4, 200 42, 800	10,790	32,102	10,700	21,400	19.760	19,700		10,700		
lief (falchoet Facilities		14	167,600			0.10		1	107,000	10,100	\$6,330	10,760	85,610	10,700		1.167	1,004	3, 163	5.826	1,167	4,659	1,167	3,502	1,167	2,134	1,167	1,367		1, 161		
plag facility Otecycle De	rteas te)	2	11,673			67 0.10			11,673	1.167	10,505	1,107	9,328	1,167	12, 255	1.751	10,505	1,751	8,755	1,151	7,026	1,751	\$,253	1.751	3,502	1.751	1,751		2,751		
centrate toucies flace] 2]	17,509	11		91 0.10			17,509	1.751	15,758	1,751	34,007	1,751 5,534	41,535	5,534	35, 602	5,934	29,668	5,934	23, 135	5, 934	17, 801	5, 924	11,858	5,534	5,374		5.534		
cratery		1 2	\$9, 836	111		0.10		Ι.	59,316	8.934 17.606	53,403 158,457	5.834	47, 465 140, 151	17,606		17,606	105,638	17,636	88,612	17,606	79, 425	17,606	52.819	17, 506	35, 212	(7,606	17,666		17,606	- 1	
ilding Office (721 m)	1 set	2	176,064	1 13	17.6	0.10	*		176,064	11,816	158, 637	17,606	140.001	. 11.020	123,211	17.000	100,100			,,,,,,,		1		,	,,,,,,,,					. 1	
		LΙ			1	1		1	1			1.1			1		1					- 1	- 1				100				
		ll			1 .	1.3	1.0	1			1		1		1			1				1									
		ΙI		М	1	1			1										- 1					. 1.							
		-		- - - -	154,8			-	1, 143, 200	10.84	1 215 164	124 855	1, 678, 568	124 120	\$43,740	134, 829	626, 923	134, 120	674, 100	124 126	539,293	134,820	404,469	134,828	269,640	124,820	124, 129		125, 820		
Total of Sistrat P	G88.66	1-1	1,348,269	l total	1350						T. KINGSON.		Transie .												1						
pia dirisica		ll		ш	1 1		ŧ	1	1.0	1			i																		
den of Corstraction Cot (I.I	485, 455	Ш,	ء ور	45 0.00			485, 455	25,127	456,327	29, 127	427, 200	29,127	359,013	29,127	358, 545	28,127	339, 818	29,127	310,691	29, 127	281,561	25,127	252,436	29,127	223, 205	29, 127	194,182	29,127	
ice - Decalifory (450 m)	1 set	1:1	160,500	H.		50 0.10			163,530	16,050	144, 650	16,050	128, 410	16,060		16,650	\$6,310	16,052	80,250	16.050	£4,200	16,000	48,158	16,850	32,150	16,850	16,050		18,058		
epes	1 165	131	60,000	Ш		00 0.10			65,660	19,808	49, 200	16,820	38,400	10,800	27,600	16.800	16,860	10,830	8,600		6,000		8,600		6,000		\$,000		6,000		
		П		Ш	1 :	. 11-				1		1	1.5		1			. 32			100						1 000		1.00	- 1	
k for Transportation of C	occetrate(iit)	3	50,000		1.0	60 0.11	10		90,000	16,200	13,866	16,200	57,600	36, 200	43,400	18,200	25,200	16, 210	9,600		5,000	1	1,000		9,000						
elving facility of Closes	e Power .	1	255, 000		35.5	60 0.6	20		355,400	21,390	333,700	21,300	312,400	25,360	291,100	21,300	269, 800	21,300	141.500	21,300	227,260	21,300	205, 900	21,300	184, 690	21,300	143,380	21,303	142,000	21,300	
fotal of Creeve 4	irlaise		1, 150, 955	坩	240.1	73			1, 150, 355	93,417	1,61,471	\$1.477	964,000	13,02	674,513	23,477	111,66	10.00	\$63,568	_54,513	\$17,091	65,07	550,633	6.07	41.136	66,417	417,655	50,427	367, 232	\$0,621	
		Н		ببل	+	-	+		3,631,609	411 110	3, 239, 474	431.214	2, 502, 631	676 679	2,364,191	OS 539	1,929,552	(36,123	2,022,913	361, 197	1,721,716	201.397	1,420,510	301, 417	1.115,321	321, 197	118.124	145,821	472, 237	50,427	Dosceclati
		10	4, 201, 509	1	205.0	03	11:	1	3,431,609	14.40		131,555		14.55		16.55		14.55	1	10.04	1			10.64		18.61			T Depreciat	3,575,740	

Table 42 Investment & Depreciation of each division(Economical)