

2.3.5 Final Flotation Test

(1) Bulk differential flotation

Under the best conditions obtained in the basic test of BDF, the final flotation test was carried out, with two-stage cleaning respectively in the bulk flotation section and the lead differential flotation section. The test comprised two parts, one without sulfidizer and the other using 100g/t of the same. The test flow sheet and the test results are shown in Fig.34 in Table 25, respectively.

The test findings are summarized as follows:

1) The two-stage cleaning in the bulk flotation section generally produced favorable results as far as the lead and zinc grades are concerned. However, pyrite in free particles were abundant in the zinc concentrate, indicating insufficient depression of pyrite in the bulk flotation. Further study on quantity of added lime in the bulk flotation cleaners is considered necessary.

2) Almost 85% of lead grading nearly 70% was recovered in concentrate of the first stage of the two-stage cleaning in the differential flotation. Under the microscope, however, sphalerite-chalcocite middling was abundantly distributed; therefore, two-stage cleaning is considered necessary for stabilizing flotation performance.

3) Sulfidizer was added to recover cerussite, non-sulfide lead component, which lowered the tailing grade but only insufficiently. Intentional recovery of non-sulfide component appears to be unfeasible.

(2) Straight-differential flotation

Under the best conditions obtained in the basic test of SDF, the final flotation test with two-stage cleaning in the lead flotation and in the zinc flotation sections was carried out. The test consisted of two parts: one without sulfidizer and the other using 100g/t of it. The test flow sheet appears in Fig.35 and the test results in Table 26.

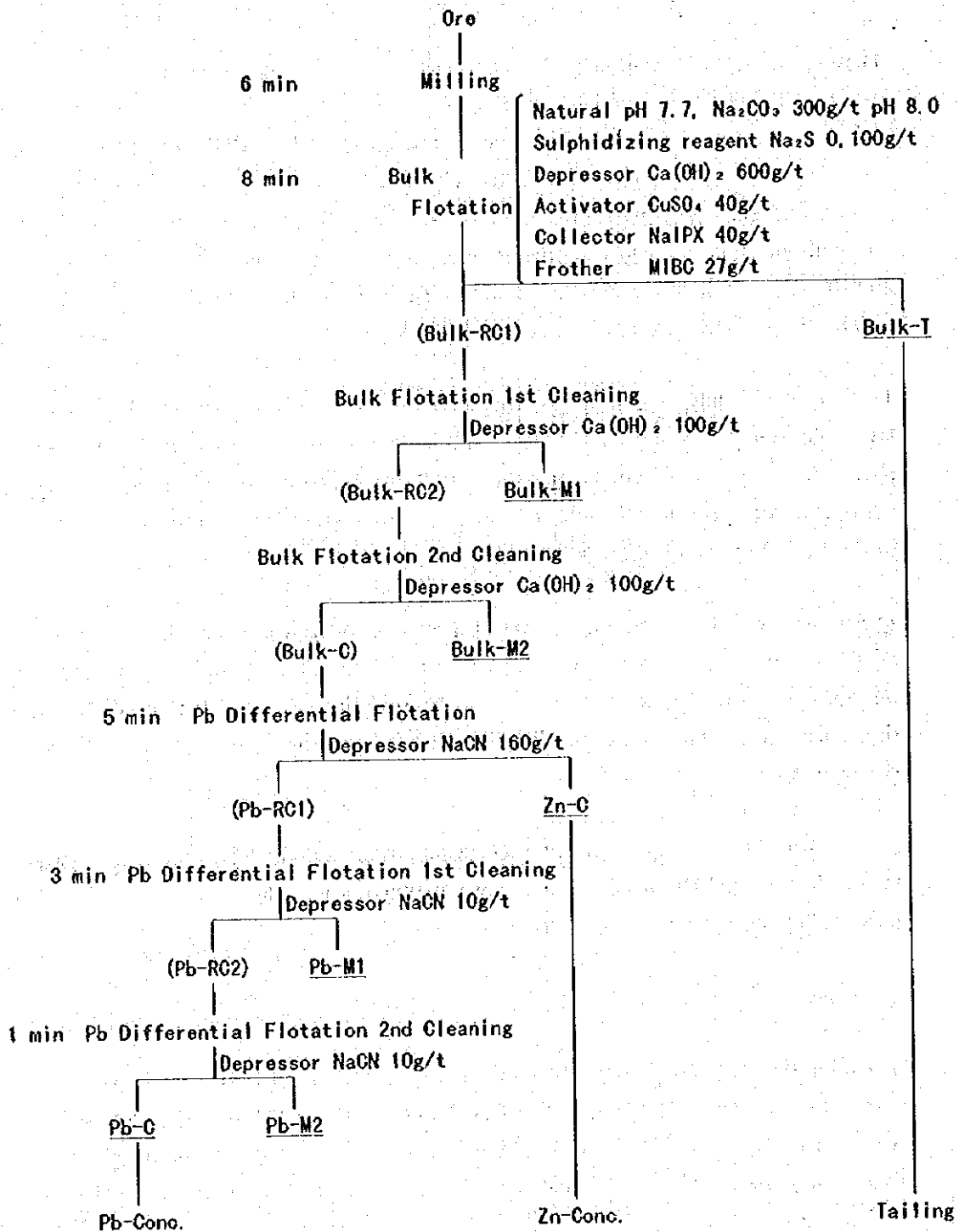


Fig. 34 Final Flotation Test Flowsheet
 (Bulk Differential Flotation)

Test No.	Type	Weight (g)	Weight (%)	Grade										Distribution													
				Cu		Pb		Zn		Fe		Ag		Au		Cu		Pb		Zn		Fe		Ag		Au	
				Weight	Weight (%)	Weight	Weight (%)	Weight	Weight (%)	Weight	Weight (%)	Weight	Weight (%)	Weight	Weight (%)	Weight	Weight (%)	Weight	Weight (%)	Weight	Weight (%)	Weight	Weight (%)	Weight	Weight (%)	Weight	Weight (%)
1	Crude Ore	497.61	100.0	0.09	7.82	3.12	4.66	116	0.7	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	
	Bulk Rough 1	98.89	19.7	0.36	35.90	15.04	8.43	528	3.2	81.6%	91.1%	85.6%	35.8%	88.6%	90.5%	90.5%	90.5%	90.5%	90.5%	90.5%	90.5%	90.5%	90.5%	90.5%	90.5%	90.5%	
	Bulk Tail	398.92	80.3	0.02	0.87	0.17	3.73	14	0.1	18.4%	8.9%	4.4%	64.2%	11.4%	9.7%	9.7%	9.7%	9.7%	9.7%	9.7%	9.7%	9.7%	9.7%	9.7%	9.7%	9.7%	
	Bulk Rough 2	88.65	17.7	0.38	39.54	16.62	7.29	563	3.1	77.4%	90.1%	84.9%	27.8%	77.7%	86.5%	86.5%	86.5%	86.5%	86.5%	86.5%	86.5%	86.5%	86.5%	86.5%	86.5%	86.5%	
	Bulk Mid 1	10.04	2.0	0.18	3.76	1.09	18.50	219	3.8	4.2%	1.0%	0.7%	8.0%	10.9%	3.8%	3.8%	3.8%	3.8%	3.8%	3.8%	3.8%	3.8%	3.8%	3.8%	3.8%	3.8%	
	Bulk Conc	78.64	15.7	0.41	43.94	18.13	7.09	625	3.1	74.2%	88.8%	91.8%	24.0%	69.7%	85.2%	85.2%	85.2%	85.2%	85.2%	85.2%	85.2%	85.2%	85.2%	85.2%	85.2%	85.2%	
	Bulk Mid 2	10.01	2.0	0.14	4.97	4.76	8.86	76	2.8	3.2%	1.3%	3.1%	3.8%	8.0%	1.3%	1.3%	1.3%	1.3%	1.3%	1.3%	1.3%	1.3%	1.3%	1.3%	1.3%	1.3%	
	Pb Rough 1	51.22	10.3	0.12	66.54	5.76	3.30	918	2.8	14.2%	37.6%	19.0%	7.3%	40.1%	81.5%	81.5%	81.5%	81.5%	81.5%	81.5%	81.5%	81.5%	81.5%	81.5%	81.5%	81.5%	
	Zn Conc	27.42	5.4	0.95	1.72	41.24	14.17	78	3.8	60.0%	1.2%	72.8%	16.7%	29.6%	3.7%	3.7%	3.7%	3.7%	3.7%	3.7%	3.7%	3.7%	3.7%	3.7%	3.7%	3.7%	
	Pb Rough 2	48.86	9.8	0.12	69.20	5.40	2.40	925	2.8	13.5%	86.9%	17.0%	5.1%	38.8%	78.3%	78.3%	78.3%	78.3%	78.3%	78.3%	78.3%	78.3%	78.3%	78.3%	78.3%	78.3%	
	Pb Mid 1	2.36	0.5	3.0	0.12	11.47	13.21	21.93	773	2.0	0.7%	0.7%	2.0%	2.2%	1.3%	3.2%	3.2%	3.2%	3.2%	3.2%	3.2%	3.2%	3.2%	3.2%	3.2%	3.2%	
	Pb Conc	36.35	7.3	0.11	72.24	5.00	1.12	954	3.1	9.2%	67.5%	11.7%	1.8%	32.0%	60.1%	60.1%	60.1%	60.1%	60.1%	60.1%	60.1%	60.1%	60.1%	60.1%	60.1%	60.1%	
	Pb Mid 2	12.51	2.5	0.15	60.37	6.56	6.12	841	1.9	4.3%	19.4%	5.3%	3.3%	6.8%	18.2%	18.2%	18.2%	18.2%	18.2%	18.2%	18.2%	18.2%	18.2%	18.2%	18.2%	18.2%	
	2	Crude Ore	496.85	100.0	0.11	7.68	3.14	4.72	115	0.6	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%
Bulk Rough 1		92.89	18.6	0.42	37.60	15.97	7.93	554	2.7	70.7%	91.5%	95.1%	31.4%	86.0%	90.1%	90.1%	90.1%	90.1%	90.1%	90.1%	90.1%	90.1%	90.1%	90.1%	90.1%	90.1%	
Bulk Tail		403.96	81.4	0.04	0.80	0.19	3.98	14	0.1	29.3%	8.5%	4.9%	68.6%	14.0%	9.9%	9.9%	9.9%	9.9%	9.9%	9.9%	9.9%	9.9%	9.9%	9.9%	9.9%		
Bulk Rough 2		88.65	17.7	0.38	38.90	16.60	7.32	561	2.7	61.0%	90.3%	94.3%	27.7%	83.5%	97.1%	97.1%	97.1%	97.1%	97.1%	97.1%	97.1%	97.1%	97.1%	97.1%	97.1%		
Bulk Mid 1		4.24	0.9	1.26	10.42	2.80	20.68	408	1.7	9.7%	1.2%	0.8%	3.7%	2.5%	3.0%	3.0%	3.0%	3.0%	3.0%	3.0%	3.0%	3.0%	3.0%	3.0%	3.0%		
Bulk Conc		72.07	14.4	0.43	45.64	19.50	4.03	643	3.1	58.2%	86.1%	90.1%	12.4%	76.6%	81.2%	81.2%	81.2%	81.2%	81.2%	81.2%	81.2%	81.2%	81.2%	81.2%	81.2%	81.2%	
Bulk Mid 2		16.58	3.3	0.16	9.60	3.99	21.62	205	1.2	4.8%	4.2%	4.2%	15.3%	6.9%	5.9%	5.9%	5.9%	5.9%	5.9%	5.9%	5.9%	5.9%	5.9%	5.9%	5.9%		
Pb Rough 1		49.17	9.9	0.14	65.34	6.50	2.10	870	2.8	12.5%	84.7%	20.5%	4.4%	47.2%	74.9%	74.9%	74.9%	74.9%	74.9%	74.9%	74.9%	74.9%	74.9%	74.9%	74.9%		
Zn Conc		22.90	4.5	31.8	1.05	2.27	47.41	8.17	156	3.7	43.7%	1.4%	69.6%	8.0%	29.4%	6.3%	6.3%	6.3%	6.3%	6.3%	6.3%	6.3%	6.3%	6.3%	6.3%	6.3%	
Pb Rough 2		44.87	9.0	62.2	0.14	70.60	4.60	1.20	940	2.9	11.4%	82.9%	13.2%	2.3%	73.8%	73.8%	73.8%	73.8%	73.8%	73.8%	73.8%	73.8%	73.8%	73.8%	73.8%		
Pb Mid 1		4.30	0.9	6.0	0.14	16.17	26.33	11.49	140	1.1	1.1%	1.8%	7.3%	2.1%	1.1%	1.1%	1.1%	1.1%	1.1%	1.1%	1.1%	1.1%	1.1%	1.1%	1.1%		
Pb Conc		36.35	7.3	50.4	0.13	74.05	3.54	0.70	989	3.2	8.6%	70.4%	8.2%	1.1%	62.9%	62.9%	62.9%	62.9%	62.9%	62.9%	62.9%	62.9%	62.9%	62.9%	62.9%		
Pb Mid 2		8.52	1.7	11.8	0.18	55.88	9.12	3.33	731	1.8	2.8%	12.5%	5.0%	1.2%	10.9%	10.9%	10.9%	10.9%	10.9%	10.9%	10.9%	10.9%	10.9%	10.9%	10.9%		

Table 25 Results of Final Flotation Test(Bulk Differential Flotation)

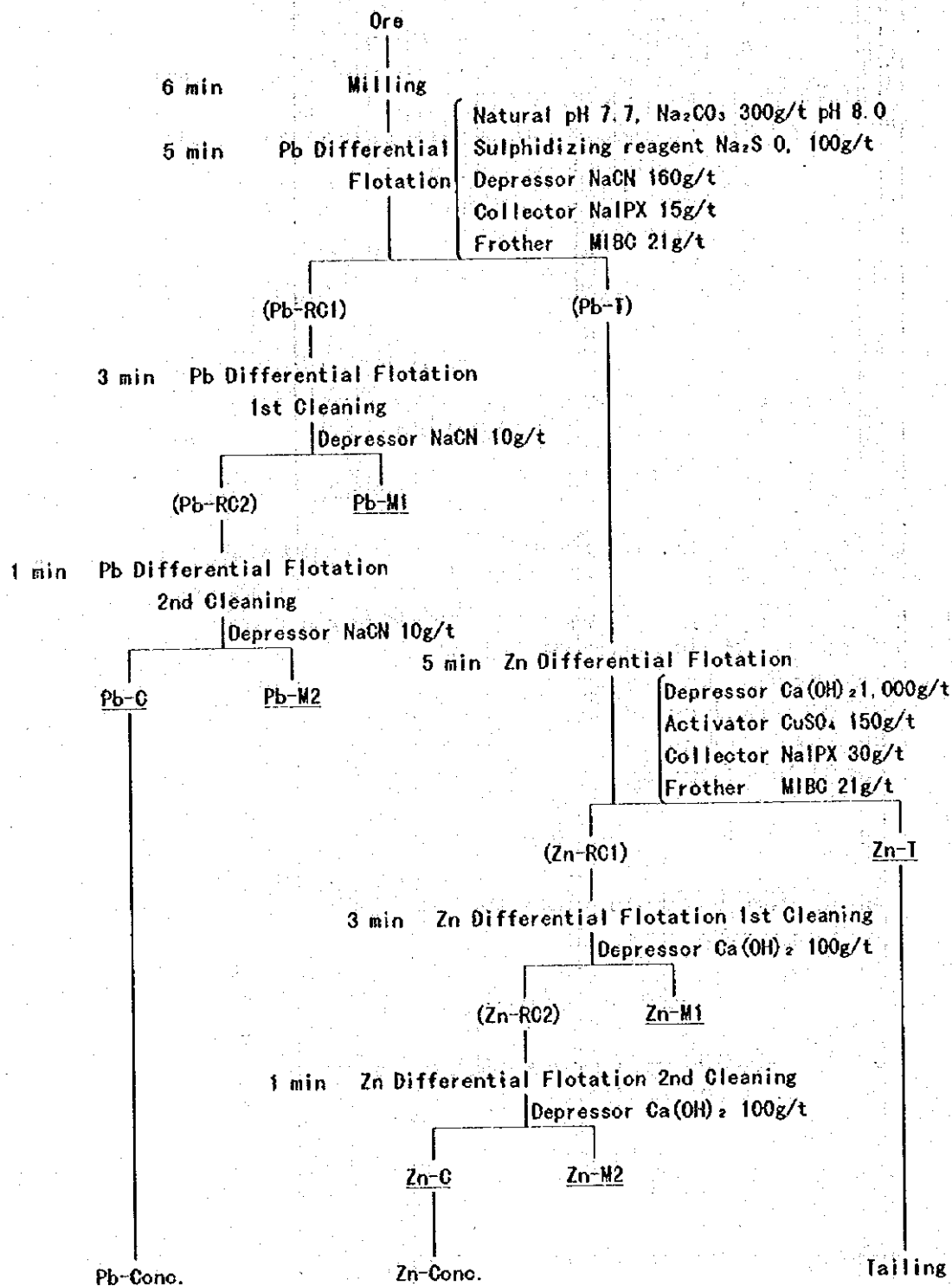


Fig. 35 Final Flotation Test Flowsheet
(Straight Differential Flotation)

Test No.	Type	Weight (g)	Weight (%)	Grade								Distribution																				
				Cu	Pb	Zn	Fe	Ag	Au	Cu	Pb	Zn	Fe	Ag	Au	Cu	Pb	Zn	Fe	Ag	Au											
1	Crude Ore	497.76	100.0	0.13	7.12	3.00	4.70	105	0.6	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%					
	Pb Rough 1	54.91	11.1	0.67	51.96	14.27	2.11	694	3.8	55.5%	80.5%	52.5%	4.9%	73.1%	64.9%																	
	Pb Tail	442.85	88.9	0.07	1.56	1.60	5.02	32	0.3	44.5%	19.5%	47.5%	95.1%	26.9%	35.1%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%										
	Pb Rough 2	41.58	8.4	0.39	65.34	8.10	0.79	797	4.0	24.5%	76.7%	22.6%	1.4%	63.6%	51.7%																	
	Pb Mid 1	13.33	2.7	1.54	10.22	33.52	6.23	373	3.2	31.0%	3.8%	29.9%	3.5%	13.2%	13.2%																	
	Pb Conc	35.64	7.2	0.08	70.65	4.47	0.45	812	4.2	4.3%	71.1%	10.7%	0.7%	55.5%	46.5%																	
	Pb Mid 2	5.94	1.2	2.25	33.48	29.88	2.83	707	2.8	20.2%	5.6%	11.9%	0.7%	8.1%	5.2%																	
	Zn Rough 1	25.71	5.2	0.82	13.52	25.15	7.34	317	2.8	31.9%	9.8%	43.3%	8.0%	15.7%	22.2%												58.3%	63.1%				
	Zn Tail	417.14	83.7	0.02	0.82	0.15	4.88	14	0.1	12.6%	9.7%	4.2%	87.1%	11.2%	12.3%																	
	Zn Rough 2	14.31	2.9	0.77	14.11	37.77	4.02	345	2.9	16.7%	5.7%	36.2%	2.4%	9.5%	13.0%																	
	Zn Mid 1	11.40	2.3	0.88	12.79	9.30	11.52	282	2.6	15.2%	4.1%	7.1%	5.6%	6.2%	9.2%																	
	Zn Conc	9.29	1.9	0.75	12.37	49.21	3.80	352	3.1	10.5%	3.2%	30.6%	1.5%	6.3%	8.9%																	
	Zn Mid 2	5.02	1.0	0.82	17.32	16.60	4.42	332	2.6	6.2%	2.5%	5.6%	0.9%	3.2%	4.1%																	
2	Crude Ore	497.30	100.0	0.13	7.25	3.14	4.66	102	0.5	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%				
	Pb Rough 1	60.46	12.1	0.68	51.60	13.91	2.28	652	2.6	62.0%	86.4%	53.9%	5.9%	77.6%	64.7%																	
	Pb Tail	436.84	87.9	0.06	1.11	1.65	4.99	26	0.2	38.0%	13.6%	46.1%	94.1%	22.4%	35.3%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%									
	Pb Rough 2	46.89	9.4	0.47	64.69	9.64	1.01	754	2.8	33.2%	84.0%	29.0%	2.0%	69.6%	54.1%																	
	Pb Mid 1	13.57	2.7	1.41	6.37	23.66	6.67	300	1.9	28.8%	2.4%	24.9%	3.9%	8.0%	10.6%																	
	Pb Conc	40.86	8.2	0.13	71.16	5.27	0.62	791	2.9	8.0%	80.5%	13.8%	1.1%	63.6%	48.9%																	
	Pb Mid 2	6.03	1.2	2.77	20.85	39.25	3.65	503	2.1	25.2%	3.8%	15.2%	0.9%	6.0%	5.2%																	
	Zn Rough 1	20.85	4.2	0.81	9.35	30.55	11.20	264	2.1	25.5%	5.5%	40.8%	10.2%	10.8%	18.1%																	
	Zn Tail	415.99	83.7	0.02	0.70	0.20	4.68	14	0.1	12.5%	3.1%	5.3%	83.9%	11.5%	17.2%																	
	Zn Rough 2	12.45	2.5	0.73	9.67	44.56	6.93	299	2.3	13.7%	3.4%	35.5%	3.8%	7.4%	11.9%																	
	Zn Mid 1	8.40	1.7	0.93	8.88	9.79	17.53	212	1.8	11.8%	2.1%	5.3%	6.4%	3.5%	6.2%																	
	Zn Conc	8.87	1.8	0.74	9.56	50.98	4.84	324	2.4	9.9%	2.4%	23.9%	1.9%	5.7%	8.8%																	
	Zn Mid 2	3.58	0.7	0.71	9.94	28.65	12.11	237	2.1	3.8%	1.0%	6.6%	1.9%	1.7%	3.1%																	

Table 26 Results of Final Flotation Test(Straight Differential Flotation)

The test findings are summarized as follows:

1) In the second stage concentrate of the lead flotation(SDF), the lead grade reached 71% and the recovery 76%, indicating the zinc depression effect in the cleaners. In the lead concentrate, however, sphalerite grains in free particles were abundantly observed, while 40% of zinc was circulating in the cleaners. There still remains a question as to whether the two-stage cleaning can sufficiently depress and separate zinc.

2) 30% of zinc grading 50% was recovered in the concentrate of the two-stage cleaning in the zinc flotation. Under the microscope, galena in free particles was abundantly distributed in the zinc concentrate, which indicates insufficient separation in the lead flotation section. Compared to BDF, higher grade zinc in zinc concentrate was more easily recoverable, whereas the question of recovery still remains.

3) In relation to the sulfidizing effect, the tailing grade tended to decrease but only insufficiently; therefore, intentional recovery of non-sulfide component appears unfeasible.

4) In order to determine the number of stages of SDF and quantity of reagents added, locked tests or continuous tests have to be conducted, thereby clarifying zinc behavior in the lead flotation.

As compared to the performance of SDF, BDF demonstrated higher stability in the lead and zinc recovery, as the latter process recovers floatable zinc together with lead.

2.3.6 Settling test of concentrates and tailing

The Tsav area being situated in an arid land, there is no large water source in the vicinity. If the mine is put into development, mineral dressing water supply would be insufficient; therefore, water recycling must be contemplated. For this purpose, the settling rates of the concentrates and tailing were measured, which constitute the basic items for planning the mineral dressing water recycling.

For the settling test samples, the undersize(-200 mesh) of sieved bulk flotation tailing was prepared, which is assumed to substitute for the tailing slime fed to the tailing thickener, whereas, in substitution for the lead and zinc concentrates fed to each concentrate thickeners, the concentrates produced from the flotation test were used without sieving because the quantity of the test products was small. The initial pulp density of respective samples, as the settling test condition, was determined at 10%. Flocculant was not used in the test.

The settling rate measurement is shown in Table 27, while Fig.36 ~ 38 indicate the relationship between the height of interface and the density of sediment by product and by measurement time.

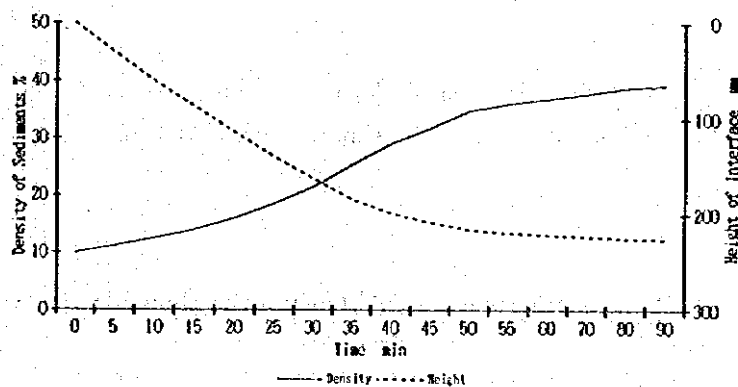


Fig. 36 Height of Interface and Density of Sediments(Tailing)

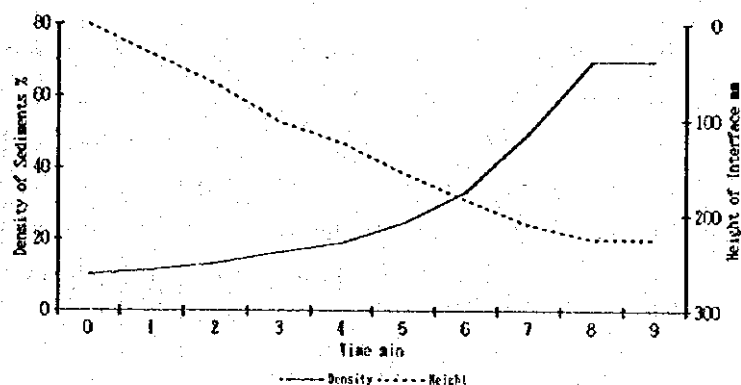


Fig. 37 Height of Interface and Density of Sediments(Pb-Conc.)

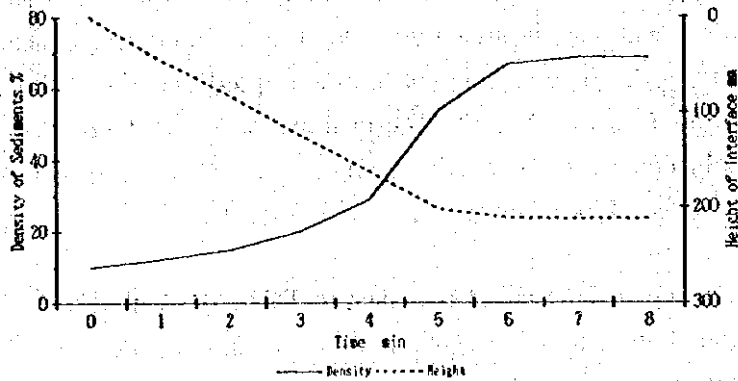


Fig. 38 Height of Interface and Density of Sediments(Zn-Conc.)

From the measurement in Fig.36 ~ 38, the settling rates for each sample to be thickened to certain densities of sediment are calculated as follows:

Tailing		Pb Conc		Zn Conc	
Sediment density(%)	Settling rate(mm/min)	Sediment density(%)	Settling rate(mm/min)	Sediment density(%)	Settling rate(mm/min)
20	5.50	20	31.07	20	41.33
30	4.85	30	30.87	30	40.49
35	4.26	40	30.38	40	40.45
		50	29.98	50	40.41

All the three types of the samples showed certain turbidity in the decanted water(the top water) influenced by clay minerals and fine slime contained but their settling characteristics appeared relatively good in view of the settling rates. Since the turbidity of the tailing slime was higher than that of the concentrates, it would probably be necessary, in the actual operation, to add high-molecular flocculant in the tailing thickener thereby lowering the turbidity of the decanted water.

Tailing			Pb-Conc.			Zn-Conc.		
Time	Height of Interface	Density of Sediments	Time	Height of Interface	Density of Sediments	Time	Height of Interface	Density of Sediments
min	mm	%	min	mm	%	min	mm	%
0	0	10.0	0	0	10.0	0	0	10.0
1	6	10.2	1	32	11.4	1	45	12.2
2	13	10.4	2	63	13.2	2	82	14.9
3	19	10.7	3	103	16.4	3	124	20.0
5	30	11.1	4	124	18.9	4	162	28.8
10	60	12.5	5	156	24.6	5	202	53.8
15	87	14.0	6	184	33.4	6	211	66.8
20	114	16.0	7	210	49.8	7	212	68.7
25	140	18.6	8	225	69.6	8	212	68.7
30	162	21.5	9	225	69.6			
35	184	25.4						
40	199	29.1						
45	208	31.8						
50	216	34.8						
55	219	36.0						
60	221	36.9						
70	223	37.8						
80	225	38.8						
90	226	39.3						
Sample	100g		Sample	50g		Sample	50g	
Water	900cc		Water	450cc		Water	450cc	
pH	9.7		pH	7.5		pH	7.4	

Table 27 Settling Rates

In turn, water quality analysis was made on the waters that are assumed to correspond to the decanted waters in the tailing thickener and the concentrates thickeners, which would be recycled in the actual operation, to judge if the water recycled from the thickeners would have any quality problems. The results of analysis are shown in Table 28.

	Overflow of Tailing Thickener	Overflow of Pb Conc. Thickener	Overflow of Zn Conc. Thickener
p H	9.9	8.2	9.6
C u (ppm)	2.7	0.15	1.6
P b (ppm)	<0.02	<0.1	<0.04
Z n (ppm)	<0.02	<0.1	<0.04
T - F e (ppm)	<0.05	<0.2	<0.1
C d (ppm)	<0.01	<0.05	<0.02
A s (ppm)	<0.02	<0.1	<0.05
C N ⁻ (ppm)	<0.1	0.5	1.4
S O ₄ ⁻² (ppm)	582	25	121

Table 28 Water Quality Analysis of Decanted Water in the Assumed Thickeners

The analysis revealed that the decanted water in the assumed zinc concentrate thickener was high in cyanide concentration; therefore, the water would desirably be returned to the differential flotation circuit.

Decanted water from the other thickeners have no problem whatever if recycled within the beneficiation plant.

As water quality of the tailing pond overflow can be improved by neutralization treatment, there would be no problem either, if the tailing pond overflow is returned to the beneficiation plant.

Since an excessive portion of the beneficiation effluent would finally be drained off only from the tailing pond, it would cause no problem whatsoever to the environment.

2.4 Final Selection of the Process Flow

(1) Comparison between SDF and BDF

Based on the results of the series of beneficiation tests, a comparative study of the BDF and SDF processes as applied to the Tsav ore has been made, which is summed up in the following paragraphs.

Straight-Differential Flotation

• Advantages :

1) As iron is easily depressed by lime in the zinc flotation, it is easy to elevate grade of zinc in zinc concentrate.

• Disadvantages :

1) Due to the existence of copper which is apt to activate zinc, a large amount of NaCN has to be used to depress zinc in the lead flotation.

Nevertheless, a greater part of zinc mixes into lead floats, circulating between the cleaners. Therefore, zinc grade and distribution in lead concentrate are apt to rise. It requires NaCN of a quantity almost similar to that for bulk flotation.

2) For depressing zinc in lead floats, the number of cleaning stages and cells have to be increased while, for decreasing returned zinc, certain measures such as additional treatment processes for zinc in middling in the lead flotation have to be taken.

3) The increase in NaCN addition causes to elevate NaCN concentration in effluent sent to the tailing pond.

4) The beneficiation process flow becomes complicated, which makes operation performance less stable.

Bulk-differential flotation

• Advantage :

- 1) Thanks to the existence of copper which is apt to activate zinc, zinc depressor(CuSO_4) requirement in the bulk flotation is small.
- 2) In the bulk flotation, iron and waste alone have to be depressed ; therefore, quantity of return ore is small which can be met by fewer stages of cleaning.
- 3) Bulk concentrate fed to the differential flotation is in a decreased quantity, requiring fewer differential flotation cells than those of the zinc flotation in SDF.
- 4) Mineral dressing effluent containing NaCN is returned to the differential flotation circuit, thereby reducing NaCN requirement and, accordingly, the NaCN content in the mineral dressing effluent.
- 5) The mineral dressing process flow is simpler, which makes operation performance more stable.

• Disadvantages :

- 1) Lime used for depression of iron in the bulk flotation may cause to lower lead recovery if added in excess.
- 2) If depression of iron in the bulk flotation is incomplete, iron depressed by NaCN may mix into zinc concentrate in the differential flotation, lowering zinc grade.

The comparison of the advantages and disadvantages of the two processes leads to a conclusion that the BDF process is superior to the SDF process, when applied to the Tsav ore, in that BDF takes advantage of copper being apt to activate zinc, has a simpler flotation process, requires smaller plant equipment and has stabler operation performance than SDF.

(2) Comparison between production of bulk concentrate alone and separate production of lead and zinc concentrates

It is a conceivable alternative to produce bulk concentrate(of lead and zinc) alone, without separation into lead concentrate and zinc concentrate.

Operation performance in this case is estimated in the table below. In this case, metal grades turn out to be inferior to those in case of separate production of lead and zinc concentrates.

	(t)	Grade					Distribution Quantity				
		Au g/t	Ag g/t	Pb %	Zn %	Cu %	Au g/t	Ag g/t	Pb %	Zn %	Cu %
Mill-F	30,000	1.22	161	6.4	2.9	0.22	100.0	100.0	100.0	100.0	100.0
Bulk-C	3,722	7.77	1,717	45.6	21.7	0.81	79.0	82.6	88.3	92.8	68.1
Tail.	26,278	0.29	32	0.9	0.2	0.08	21.0	17.4	11.7	7.2	31.9

Remarks: Mill-F; Mill feed Bulk-C; Bulk concentrate Tail.; Tailing

The project revenues and expenses in case of production of bulk concentrate are roughly estimated as follows:

Annual sales revenue of bulk concentrate:

Zinc : $3,722 \times 0.995 \times (0.217 - 0.08) =$	\$558,100
Lead : $3,722 \times 0.995 \times (0.456 - 0.03) \times 650 =$	1,025,468
Gold : $3,722 \times 0.995 \times (7.77 - 1) \times 0.9 \times 390 / 31.1024 =$	283,237
Silver : $3,722 \times 0.995 \times (1071 - 100) \times 0.9 \times 390 / 31.1024 =$	582,135
(-)T/C : $(-)3,722 \times 0.995 \times (190 + 10 + (13/100 \times (1,100 - 1,000))) =$	(-)788,822
Total	\$1,660,118

The total annual sales revenue in case of production of bulk concentrate alone is \$168,000 less than that in case of separate production of lead and zinc concentrates.

Expenses:

In case of bulk concentrate production, one series of differential flotation system and concentrate dewatering system are dispensed with; therefore, the annual depreciation expenses will decrease accordingly.

$$\$12,250 + \$8,250 = \$20,500$$

Likewise, the variable expense items such as the flotation reagents used in the omitted process sections, as well as repair expenses, etc., will become unnecessary, which represents \$35,000 of reduction in expenses.

Altogether, the reduction in annual expenses will be \$56,000.

The calculations reveals that, in case of production of bulk concentrate alone, the decline in sales revenue is far greater than the reduction in expenses, which leads to a conclusion that separate production of lead and zinc concentrates is more favorable.

(3) Optimum mineral dressing process flow

The optimum mineral dressing process flow worked out on the basis of all the results of tests and studies so far undertaken is shown in Fig.39.

2.5 Estimated Mineral dressing Performance

The grades of run-of-mine ore of the Tsav deposits are estimated at Au 1.22g/t, Ag 161g/t, Pb 6.37%, Zn 2.94% and Cu 0.22% performance estimated on the basis of the grades of run-of-mine ore and the BDF test results is shown in Table 29.

	Weight (t)	Grade					Distribution Quantity				
		Au g/t	Ag g/t	Pb %	Zn %	Cu %	Au g/t	Ag g/t	Pb %	Zn %	Cu %
Crude	30,000	1.22	161	6.4	2.9	0.22	100.0	100.0	100.0	100.0	100.0
Pb-C	2,371	11.01	1,507	69.0	5.0	0.32	71.3	74.0	85.2	13.6	11.5
Zn-C	1,351	2.09	307	4.4	51.0	2.77	7.7	8.6	3.1	79.2	56.6
Tail.	26,278	0.29	32	0.9	0.2	0.08	21.0	17.4	11.7	7.2	31.9

Remarks: Crude;Crude ore Pb-C;Pb Concentrate Zn-C;Zn Concentrate
Tail;Tailing

Table 29 Estimated operation performance

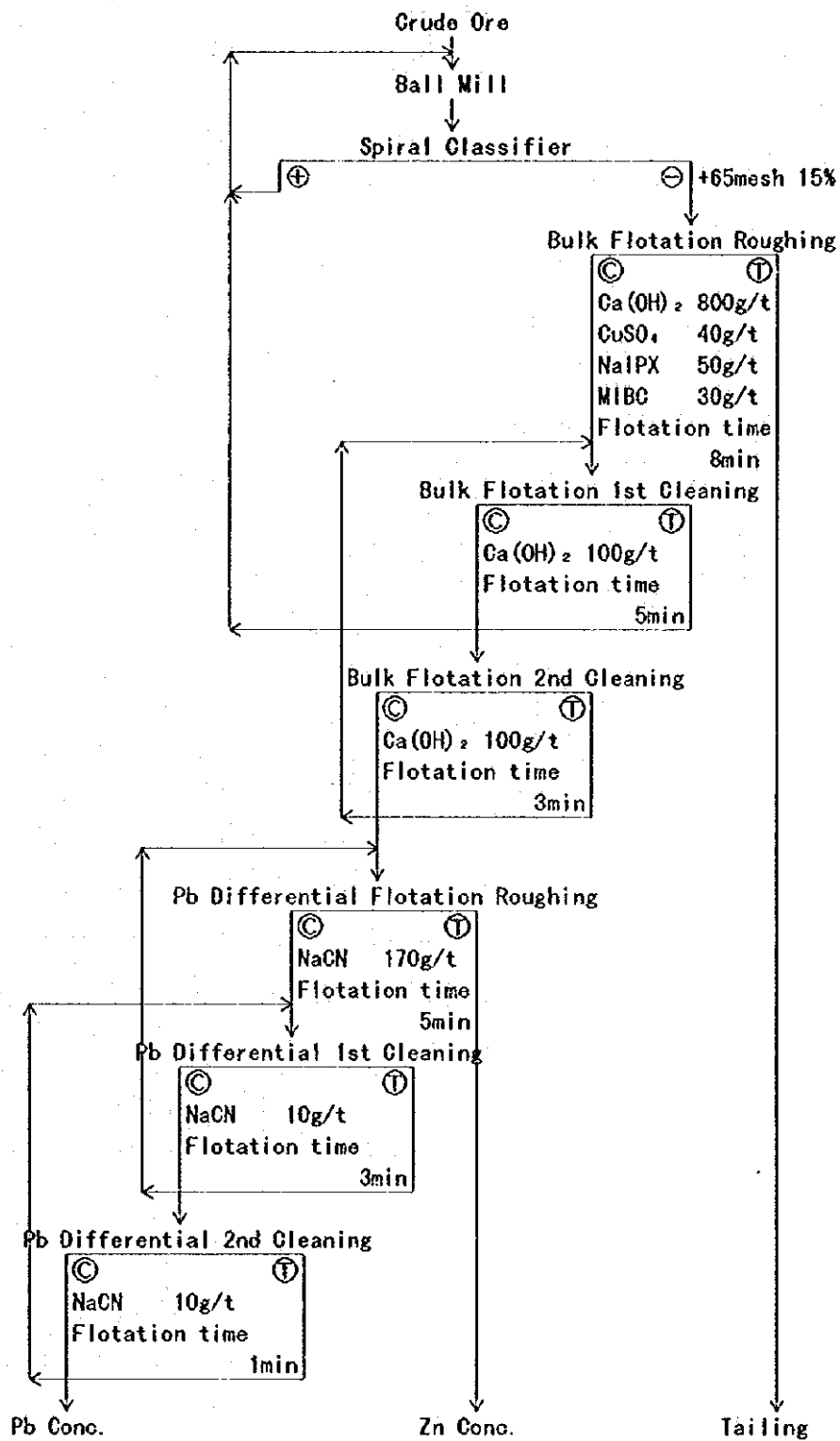


Fig. 39 Optimum Flotation Process Flow sheet



IV. Mine Development Plan



Part IV . Mine Development Plan

Chapter 1. Mining Plan

1.1 General

1.1.1 Selection of mining method

The Tsav deposits have the following characteristics:

- (1) The deposits consist of high-grade, fine veins with an average width (in terms of the minable crude ore) of 1.03m.
- (2) The deposits are poor in continuity.
- (3) The deposits dip rather steeply ; the No.4 vein dips 65 ° to 70 ° .
- (4) The hanging and foot walls are in poor rock conditions as long as it was confirmed at the - 60m level.

In mining deposits of this type, the dilution constitutes a serious question. The exploration since 1992 has been carried out by the truckless mining method, and the machinery used for the work still remain at the site and are operable by the Mongolian operators.

Considering the small population of Mongolia (2.2 million), the mechanized cut and fill method combined with the truckless mining is most appropriate for the deposits, even though machinery costs are expensive in relation to labor costs in Mongolia.

1.1.2 Numerical basis for planning

The following base figures are applied for the mining plan:

Minable crude ore to be extracted (t)	332,464
Annual extraction of crude ore (t)	30,000
Number of operating days per year (days)	300
Daily extraction of crude ore (t)	100
Number of shift per day (shifts)	2

1.1.3 Underground structure (Ref. Fig.40 Development Plan of No.4 Vein)

At the No.4 vein, already existing are a vertical shaft from the surface to 630m level(PW-14) which was driven during the ex-Soviet-Mongolian joint exploration, a drift at 630m level, an inclined shaft from the surface to 750m level and a 750m level drift at foot wall, the latter two being truckless and driven by MMAJ since 1992.

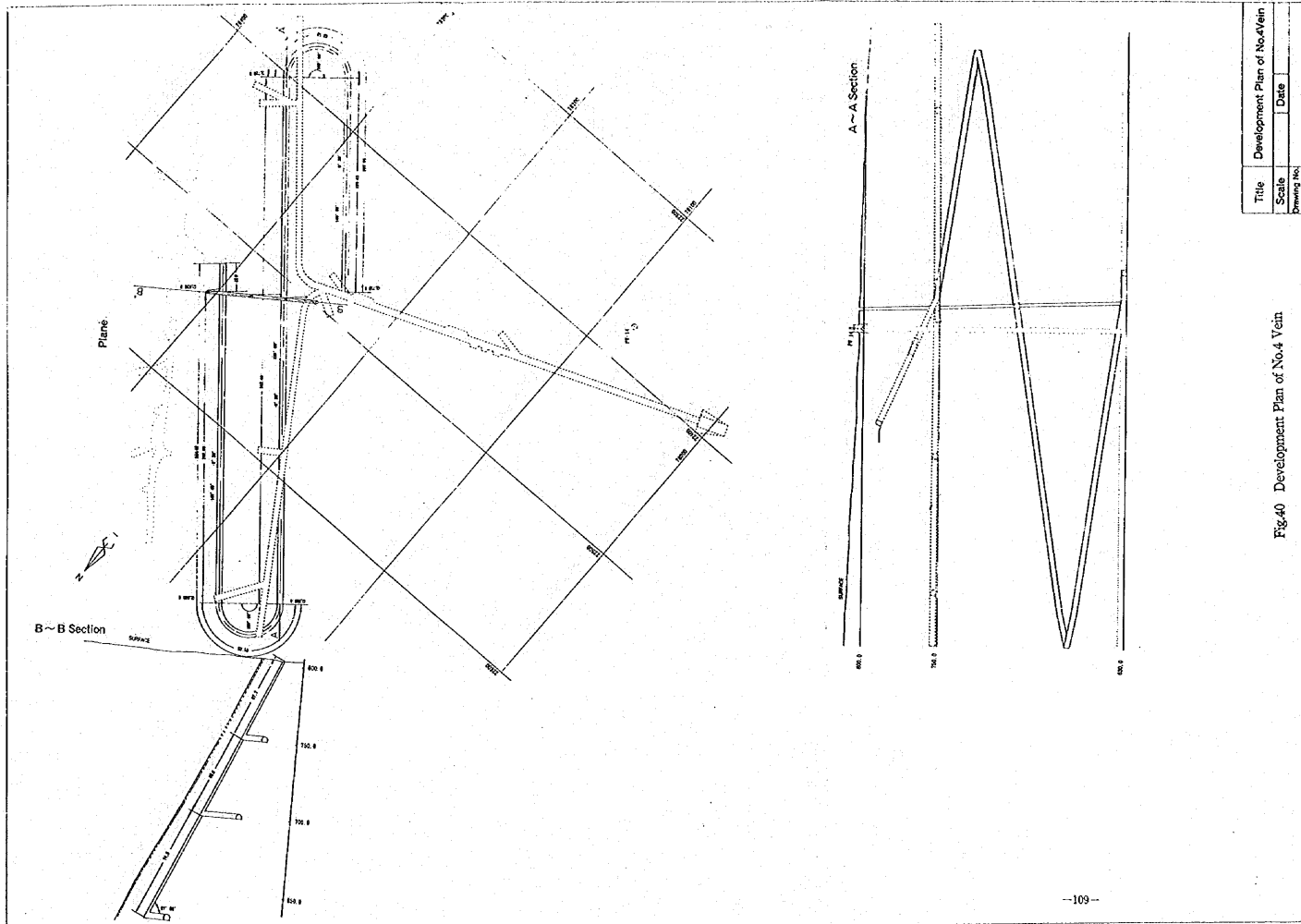
A truckless inclined shaft system is considered appropriate for the deposits for the following reasons:

(1) Compared with a vertical shaft, an inclined shaft can more flexibly accommodate changes in orebodies, allowing a wider range of options for planning and its revisions. A truckless inclined shaft can be driven from a free level with a free dip and in a free direction, which represents a great advantage in terms of the time required for reaching an orebody and of the stope preparation.

(2) In case of a vertical shaft, mining cannot be commenced until all the excavation and installation are completed, whereas an inclined shaft permits mining to start as soon as an orebody is reached. At the No.4 vein, the lowest level of the object area of development is 630m, or 220m deep from the surface, while the daily rate of crude ore extraction is as small as 100t. The operation can be done with trucks(for underground use) or load haul dumps(LHDs) on hand, without an additional investment. In contrast, a vertical shaft system requires expensive equipment.

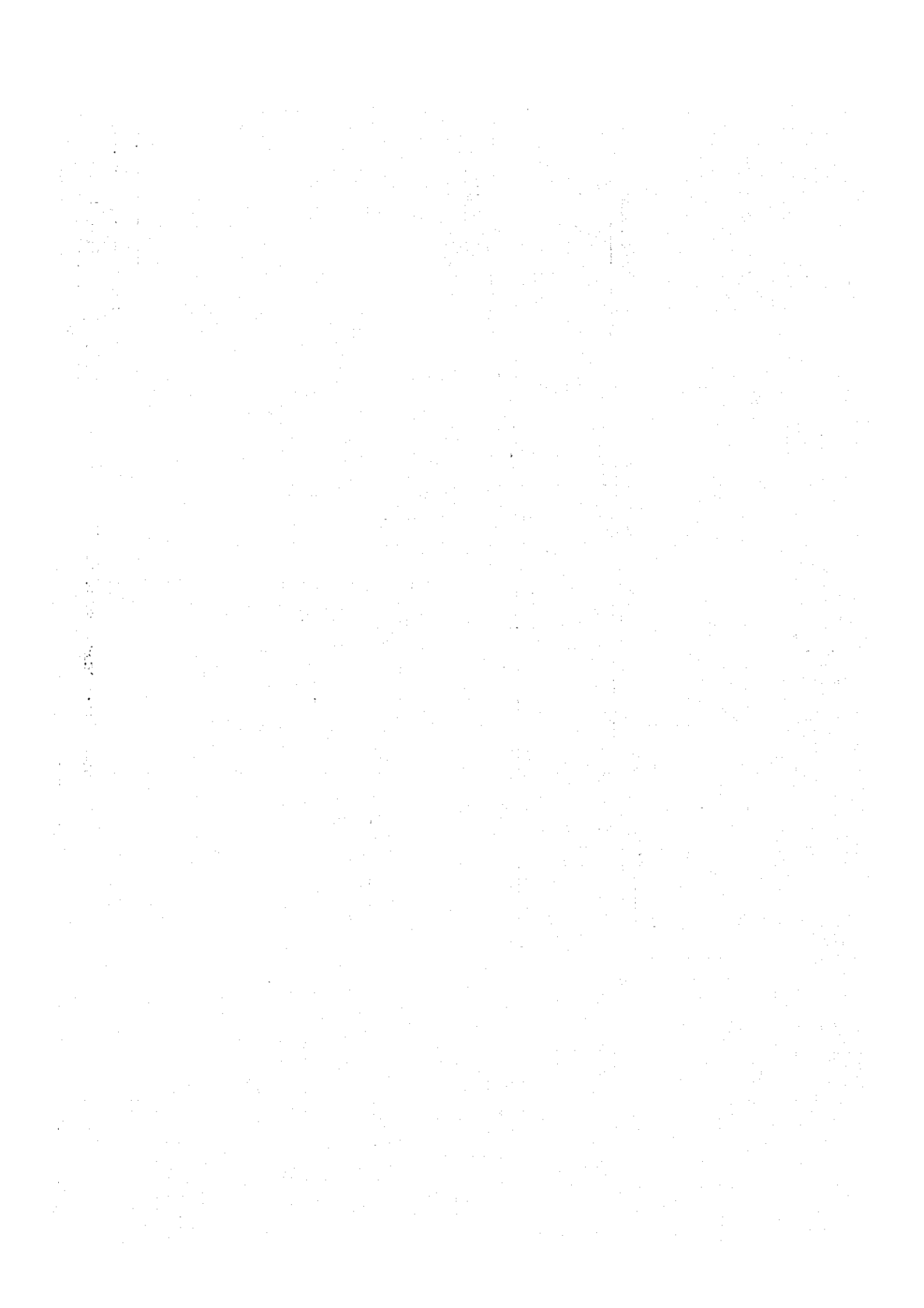
(3) The orebodies being small in size and separately located, excavation has to be carried out at each of them, for which the vertical shaft system is too costly.

It is therefore envisaged that, starting from the No.2 waste dump at the bottom of the inclined shaft driven at the No.4 vein up to 750m level in 1993, a declining shaft (hereafter called "ramp") with a dip of $6^{\circ} 30'$ be driven at the foot wall of the orebody so that the ramp may bore through the existing drift at 630m level. The prospecting, development and stope preparation are to be done from this ramp.



Title	Development Plan of No.4 Vein
Scale	
Drawing No.	
Date	

Fig.40 Development Plan of No.4 Vein





1.1.4 Ventilation raise and filling raise(Ref. Fig.40 Development Plan No.4 Vein)

A ventilation shaft will be driven in the central part of the mentioned ramp at the foot wall side, which will be extended downward as the ramp advances. A fan for the shaft sinking will be shifted downward, accordingly. When the shaft reaches 630m level, a ventilation system is established, which comprises the ramp for intake air and the vertical shaft(PW-14) for return air.

After completion of the ventilation system, the ventilation shaft drive as the ramp advances will no longer be used for ventilation but serves as a filling raise. To bore this raise, mechanical boring with a raise borer may be considered as an alternative; in view of the investment effect, however, a stage blasting method(Ref. Fig.41 Stage Blasting Method) is preferable since this is performable with the machinery on hand.

1.2 Operation Plan

1.2.1 Prospecting and Development

Starting from the mentioned ramp, excavation of accesses to the ore deposits, drifting along the veins and prospecting northward(-60m level) are to be conducted in sequence.

1.2.2 Mining methods

(1) In principle, the mechanized cut and fill method will be employed. In practice, however, 1) Ramp in Stoping and 2) Filled Rill Stoping will desirably be applied depending on local conditions. The mechanized cut and fill method in Tsav is shown in Fig.42.

1) Ramp in stoping

Under the mechanized(truckless) cut and fill method, it will become necessary to provide new accesses from the ramp as excavation advances, which increases the quantity of excavation in relation to the quantity of ore. This is a weak point of the method when applied to a deposit like Tsav.

A solution for the problem is the ramp in stoping method, whereby mining is

done diagonally in a stope and changeovers of accesses are minimized.(Ref. Fig.43 Ramp in Stoping) In the ramp in stoping method, a mining block is diagonally divided in two, and the lower half is excavated from an access which rises in the stope each time a slice is extracted. When the access reaches the upper drift, extraction of the upper half is carried out from the upper drift.

In case of Tsav, however, the average width of veins of minable ore is as narrow as 1.03m whilst an LHD's bucket is 1.6m in width; thus, the dilution comes into a question. To cope with the question, extraction and blasting are to be conducted at two stages(ore and waste). Whether waste or ore should first be blasted is determined depending on vein width, dip, rock conditions, etc.

Drilling directions may be upward or horizontal. However, rock conditions on the hanging wall is so poor that the full filling is required; consequently, horizontal drilling is opted for. Height of the ceiling and width of stoping at the time of completion of stoping are assumed to be 3.0m and 2.5m, respectively.

2) Filled rill stoping

This mining method is fit to narrow, steep veins like those of the Tsav deposits. In case the hanging and foot walls are of poor rock conditions, however, the method is not appropriate because it increases the dilution.

As shown in Fig.44 Filled Rill Stoping, the lower drift is first driven, from where blasting holes are drilled either upward or downward. After charging explosives, blasting and mucking at a face, the opened space is filled from the upper drift and, at the face of the filled portion, charging, blasting and mucking are again done. This cycle is repeated later on. The interval between drifts are tentatively set at 6m but, for final determination, vein width, dip and rock conditions must be taken into account.

In order to minimize the dilution, the drifting has to be done with two-staged blasting(for separation of waste and ore), whilst drilling and blasting between drifts should be limited to ore portions as long as it is feasible.

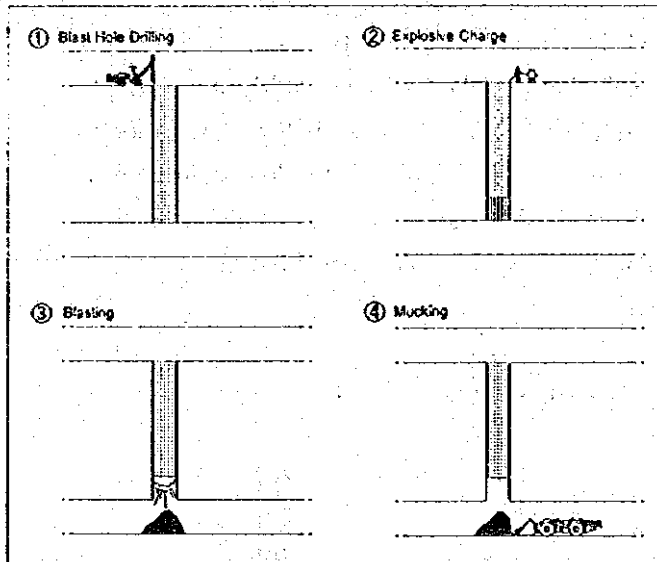


Fig.41 Stage Blasting Method

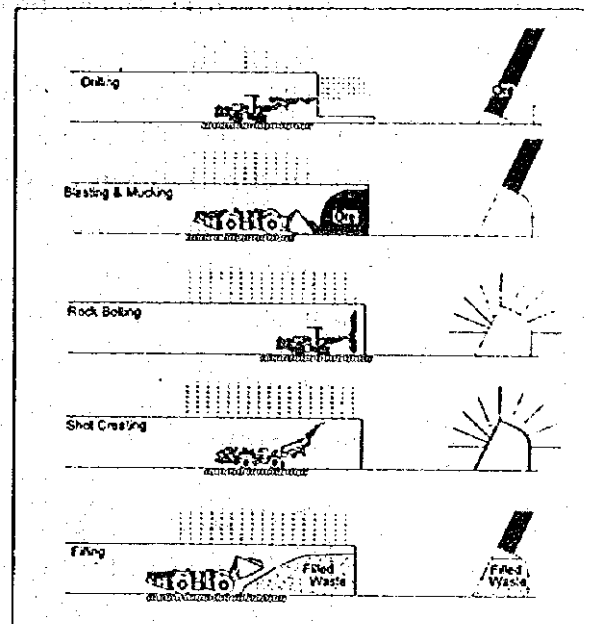


Fig.42 Mechanized Cut & Fill Method

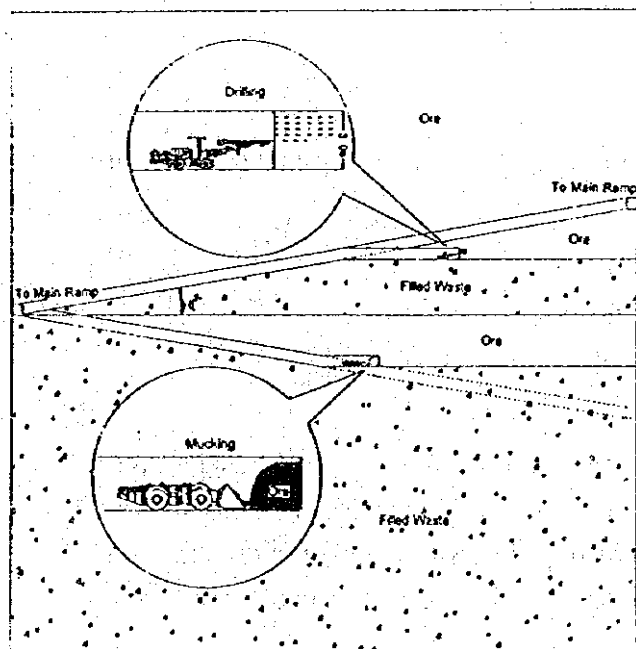


Fig.43 Ramp in Stoping

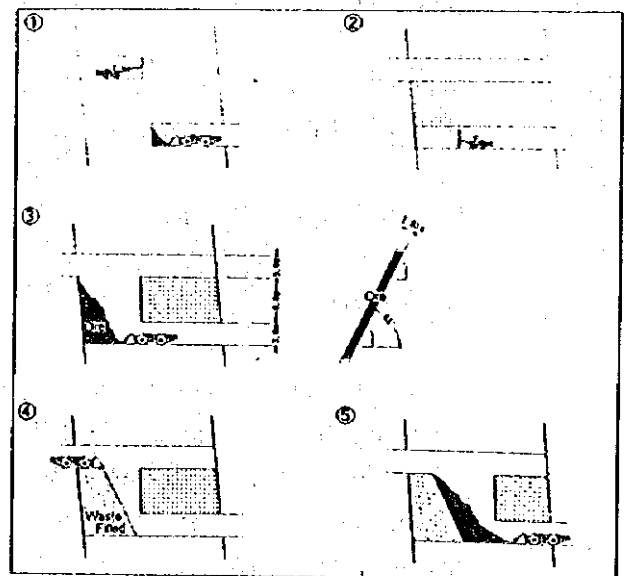


Fig.44 Filled Rill Stoping

(2) Mining Recovery and dilution

The mining recovery is determined by economic viability, vein width and continuity and reliability of ore reserve calculation, whereas vein width and mining method determine the percentage of dilution. The figures below have been empirically worked out on the basis of these considerations. The No.4 vein above 630m level and the other veins up to 100m under the surface are chosen as the mining target. At the No.4 vein, exploration has advanced considerably and the tunnels have been driven up to 750m level.

Vein width		Mining recovery	Dilution
0.7m or more	Proved ore	90%	20%
	Probable ore	80%	20%
	Possible ore	70%	20%
Less than 0.7m	Proved ore	80%	30%
	Probable ore	70%	30%
	Possible ore	60%	30%

(3) Movable crude ore

Quantity of movable crude ore calculated on the assumptions in (2) above are shown in Table. 30-1 and 30-2.

1.2.3 Drilling and blasting

(1) Drilling

For drilling operations for tunneling and drifting, the existing diesel-driven, 2-boom, hydraulic jumbo loaded with a 150kg hydraulic drifter is used. For excavation, the single boom, hydraulic jumbo loaded with a 120kg hydraulic drifter is used because of narrow drifts. Their guide cells are of the telescopic type so that they may drive rockbolts.

(2) Blasting

For blasting, AN-FO, desirable in view of easy handling and safety, is

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unavailable in Mongolia; instead, "Ammonita," a kind of ammonia explosive currently used in Mongolia, will be used. For ignition, detonators are used.

1.2.4 Haulage

Waste and ore extracted at faces and drifts are transported by the existing load haul dumps (LHDs) with 3.8m³ and 2.0m³ cap. buckets. Ores conveyed from faces are transported by the LHD with a 3.8m³ cap. bucket to the surface via the inclined shaft. In case haulage distance exceeds 500m, ores are temporarily placed at the waste dumps driven in the inclined shaft during the exploration and, in turn, transported to the surface, thereby avoiding excessive load on the LHD engines. Compared to another alternative of utilizing 15 or 20-ton underground dump trucks, haulage by LHDs is more advantageous in respect of the investment effect.

Waste coming out of faces and drifts is stored at unused tunnels to the maximum possible extent for future use as filler, and only excess waste is hauled to the surface.

(2) Personnel, Machinery and supplies

For underground transportation of personnel, machinery and supplies, the existing light truck is used. For heavy machinery, the LHDs may be used.

1.2.5 Filling and timbering

(1) Filling

Wastes built up on the surface during the development phase and extracted during the operation phase are utilized as filling material.

Waste on the surface is cast into the vertical ventilation shaft sunk to the central part of the foot wall of No.4 vein when driving the ramp. The cast waste is extracted by an LHD at a level needing waste and transported via the ramp to fill stopes.

(2) Timbering

In principle, timbering is done by rock bolts alone. When rocks are

self-supported, concrete spray is applied in thickness of 3 to 5cm to cracks even though such cracks are abundant. In case rocks are not self-supported (faults, etc.), steel supports such as H-type steel frames are put into use.

The spray concrete is prepared at a batch plant ($0.5\text{m}^3/\text{batch}$) to be installed either on surface or underground, transported to stopes by a 1.8m^3 truck mixer and sprayed to wall rocks with a spraying machine. Considering temperature control of sand and water, the batch plant will preferably be built underground.

1.3 Equipment Plan

1.3.1 Compressed air

The concrete spray machine (and AN-FO chargers in case AN-FO is available) being the only machinery using compressed air, the existing portable compressor (discharge $21\text{m}^3/\text{min}$) can cater for the requirement. Another alternative is to mount a baby compressor on the spraying machine (or the AN-FO charger).

1.3.2 Ventilation

(1) Ventilation system

Since truckless mining method is applied, the ventilation system has to be capable of treating exhaust gas of diesel engines and noxious gases including blasting fume and dust particles.

During the ramp sinking phase, a ventilation system comprising fans fixed at the chute under the foot wall of ore deposits, which serves for intake air, air ducts through which air is sent to stopes and the ramp itself for return air.

At the operating phase (after completion of the ramp), the ramp will serve for intake air, whilst return air is exhausted through the vertical shaft (PW-14) by a fan to be installed at the shaft mouth. Ventilation at stopes is done by local fans and air ducts. When the drifts along veins are completed, a chute will be sunk from the upper drift near to the face (by the stage blasting method), thereby securing the ventilation and improving the work environment without using local fans.

(2) Fans

One of the existing equipment uses two fans(gas volume 1,000m³/min, wind pressure 150mmAq, 37.5kW) in series and the other uses two fans(gas volume 500m³/min, wind pressure 100mmAq, 18.5kW) in series.

If underground airflow requirement is assumed to be 3m³/min per 1kW of engine power, and in case two LHDs(with diesel engines 185ps and 87ps, respectively) are in use, the required gas volume comes to 600m³ per minute.

$$(185+87)\text{ps} \times 0.7355\text{kW/ps} \times 3\text{m}^3/\text{kW} = 600\text{m}^3/\text{min}$$

Therefore, a fan of gas volume of 1,000m³/min or two fans of 500m³/min installed in parallel will be sufficient. Local ventilation will be done by a local fan of 500m³/min.

1.3.3 Water supply and drainage

(1) Water supply

Water requirement for drilling is 65 ℓ /min per rock drill. On the assumption that three rock drills are used, the total requirement comes to 195 ℓ /min, which can be met by estimated underground drainage of 200 ℓ /min. Underground drainage is distributed to each stope via 2" pipes laid through the ramp.

(2) Underground drainage

While the ramp is being driven, drainage is done by a pump station to be installed in the ramp near the ventilation chute and by 4" pipes laid in the chute.

After completion of the ramp, a pump station will be installed at 630m level, and underground water will be drained through the pipes laid in the vertical shaft(PW-14). Drained water is sent to a thickener at the mineral dressing plant and utilized for mineral dressing.

1.3.4 Ancillary facilities

(1) Explosives storage and handling station

The existing magazine and handling station are utilized.

(2) Oil and lubricant storage

For gas oil, the tank(25,000 ℓ cap.) buried near the shaft mouth will be utilized, while a lubricant storage will be newly built in the vicinity of the workshop.

(3) Office and accommodations

An office building and staff accommodations will be built at the site of ex-lodging house for the Japanese team. For workers' accommodations, the existing facilities for the Mongolian personnel will be utilized.

1.4 Main Machinery and Equipment

Type	Quantity	Specifications
Drill Jumbo(Drift)	1	Hydraulic 2 Boom, 150Kg. Telescopic boom Type
Drill Jumbo(Mining)	1	Hydraulic 1 Boom, 120Kg. Telescopic boom Type
Concrete spray Equ.	1	10m ³ /Hrs class
Mixer Truck	1	1.8m ³ class
Mortar Charger	1	1t truck, Squeeze type charger
Concrete Batch Plant	1	0.5m ³ /batch
Load Haul Dump	2	3.8m ³ class
Load Haul Dump	1	2.0m ³ class
Compressor	1	21m ³ /min
Truck	1	2t attached with crane
Truck	2	Underground Service(For Man, Materials)
Wagon Car	2	Underground Patrol
Turbine Pump	2	1.0m ³ /min, 50Kw
Water Pump	3	5.2Kw
Water Pump	2	2.2Kw
Ventilation Fan	1	1,000mmφ, 300mmAq, 75Kw
Ventilation Fan	1	900mmφ, 100mmAq, 18.5Kw
Boring Machine	1	150m class(For Underground)
Boring Machine	1	565m class(For Surface)

Chapter 2. Mineral Dressing Plan

2.1 Mineral Dressing Plant

2.1.1 General

The mineral dressing plant is assumed to treat crude ore at a rate of 100t/d and operate for 300 days a year; therefore, annual treatment of crude ore comes to 30,000t.

For mineral dressing, the bulk differential flotation process is employed to produce Pb and Zn concentrates.

To receive crude ore, a 600t stockyard will be provided near a crushing section, thereby avoiding troubles with ore quantities which may take place when receiving ore, due to the difference between the mining and mineral dressing divisions in respect to numbers of operating hours and days.

Crushing operation is carried out in two shifts a day while grinding, flotation and dewatering of concentrates are in three shifts.

As regards location of the mineral dressing plant, a site 500m up from the shaft mouth is selected, considering the locations of the shaft mouth and the ore deposits, topography, ground condition and location of the tailing dam. As the plant site is an almost level ground with slight inclination, the plant will be a flat type.

2.1.2. Design criteria

The mineral dressing tests have revealed that zinc ore from Tsav deposits is partially accompanied by oxidized copper ore. Therefore, zinc is apt to be activated and is hard to depress when separating lead from zinc. To depress zinc, sodium cyanide consumption increases. Lead and zinc contained in Tsav ore are easily liberated by the conventional flotation process, without any special treatment. However, a problem lies in the separation of lead and zinc because zinc tends to float. Consequently, the bulk flotation process is more favorable than the straight flotation process, which is the reason for the bulk differential flotation process being selected.

With a view to minimizing the capital cost and the operating cost, and also to make the mineral dressing plant operable, the plant is designed on the following principles:

- (1) A simple process is to be pursued.
- (2) Instrumentation is to remain at a conventional level; high-tech instrumentation involving automation will not be considered.
- (3) A washing plant is installed since there are argillized portions near the veins.
- (4) All the plant equipment are to be installed indoors. For equipment layout, due consideration is to be paid to maintenance and control.
- (5) For selection of machinery and equipment, due consideration is to be paid to their operability and maintainability.

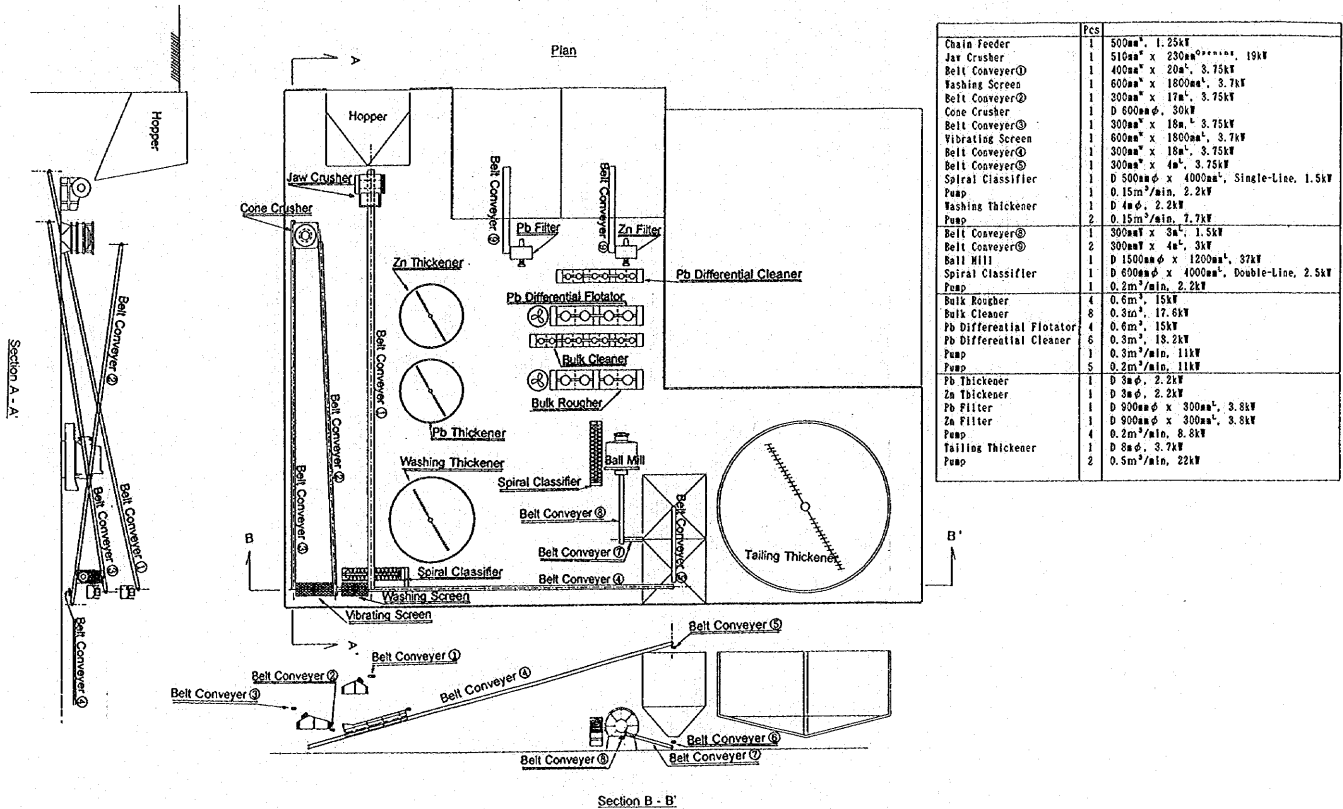
The mineral dressing plant layout is exhibited in Fig.45. The design basis follows:

(1) Operating conditions

Operating Days per year		300
Amount of treatment ore per day (t)		(Average)100
Shifts per day	Crushing	2
	Milling ~ Concentrate	3
	Tailing treatment	3
Working Hours per shift		8

(2) Mill feed

Crude ore's average grade	Pb(%)	6.4
	Zn(%)	2.9
Absolute Specific gravity		3.1
Apparent Specific gravity		1.9
Moisture(%)		5.0
Grinding work index Wi(kWh/t)		11.65



	Pcs	
Chain Feeder	1	500mm ² , 1.25kW
Jaw Crusher	1	510mm ² x 230mm ² *****, 19kW
Belt Conveyor①	1	400mm ² x 20m ² , 3.75kW
Washing Screen	1	600mm ² x 1800mm ² , 3.7kW
Belt Conveyor②	1	300mm ² x 17m ² , 3.75kW
Cone Crusher	1	D 600mm ² , 30kW
Belt Conveyor③	1	300mm ² x 18m ² , 3.75kW
Vibrating Screen	1	600mm ² x 1800mm ² , 3.7kW
Belt Conveyor④	1	300mm ² x 18m ² , 3.75kW
Belt Conveyor⑤	1	300mm ² x 4m ² , 3.75kW
Spiral Classifier	1	D 500mm ² x 4000mm ² , Single-Line, 1.5kW
Pump	1	0.15m ³ /min, 2.2kW
Washings Thickener	1	D 4m ² , 2.2kW
Pump	2	0.15m ³ /min, 7.7kW
Belt Conveyor⑥	1	300mm ² x 3m ² , 1.5kW
Belt Conveyor⑦	2	300mm ² x 4m ² , 3kW
Ball Mill	1	D 1500mm ² x 1200mm ² , 37kW
Spiral Classifier	1	D 600mm ² x 4000mm ² , Double-Line, 2.5kW
Pump	1	0.2m ³ /min, 2.2kW
Bulk Rougher	4	0.6m ² , 15kW
Bulk Cleaner	8	0.3m ² , 17.6kW
Pb Differential Flotator	4	0.6m ² , 15kW
Pb Differential Cleaner	6	0.3m ² , 19.2kW
Pump	1	0.3m ³ /min, 11kW
Pump	5	0.2m ³ /min, 11kW
Pb Thickener	1	D 3m ² , 2.2kW
Zn Thickener	1	D 3m ² , 2.2kW
Pb Filter	1	D 900mm ² x 300mm ² , 3.8kW
Zn Filter	1	D 900mm ² x 300mm ² , 3.8kW
Pump	4	0.2m ³ /min, 8.8kW
Tailing Thickener	1	D 2m ² , 3.7kW
Pump	2	0.5m ³ /min, 22kW

Fig.45 Layout of Mineral Dressing Plant



(3) Crushing section

Crushing method	Two stage grinding(Closed Circuit in Second)	
	Primary	Jaw Crusher
	Secondary	Cone Crusher
Treatment ore per 1 hour (t)		(Average)7.2
Max feed ore size (mm)		180
Stockyard Volume (t)		600
Hopper Volume (t)		10

(4) Grinding section

Grinding method	Single Ball mill (Closed circuit)	
Treatment ore per 1 hour (t)		(Average)4.2
Feed size at 80% (mm)		3.5
Final grinding size at 80% (μ)		185
Classifier recycle load (%)		300
Mill stock yard volume (t)		100

(5) Flotation section

Flotation method Pb-Zn Bulk differential flotation

(5)- 1 Pb-Zn bulk flotation

Cleaning method	Two stage	
Density and flotation time	Density (%)	Time (min)
Conditions	35	3
Roughing	35	10
Primary cleaning		4
Secondary Cleaning		4
Roughing water (pH)		10

(5)-2 Pb Differential flotation

Cleaning method	Two stage	
Density and flotation time	Density (%)	Time (min)
Conditions	20	3
Roughing	20	10
Primary cleaning		3
Secondary Cleaning		6
Roughing water (pH)		9

(5)-3 Mineral dressing test result

	Pb concentrate	Zn concentrate
Concentrate grade (%)	69.0	51.0
Recovery (%)	85.2	79.2

(6) Concentrate section

Dewatering method vacuumed filtration dewater

(6)-1 Pb concentrate

Thickener underflow density (%)	40
Concentrate size (%) - 100mesh	85
Concentrate moisture (%)	7
Concentrate specific gravity	6.9

(6)-2 Zn concentrate

Thickener underflow density (%)	40
Concentrate size (%) - 100mesh	70
Concentrate moisture (%)	9
Concentrate specific gravity	4.1

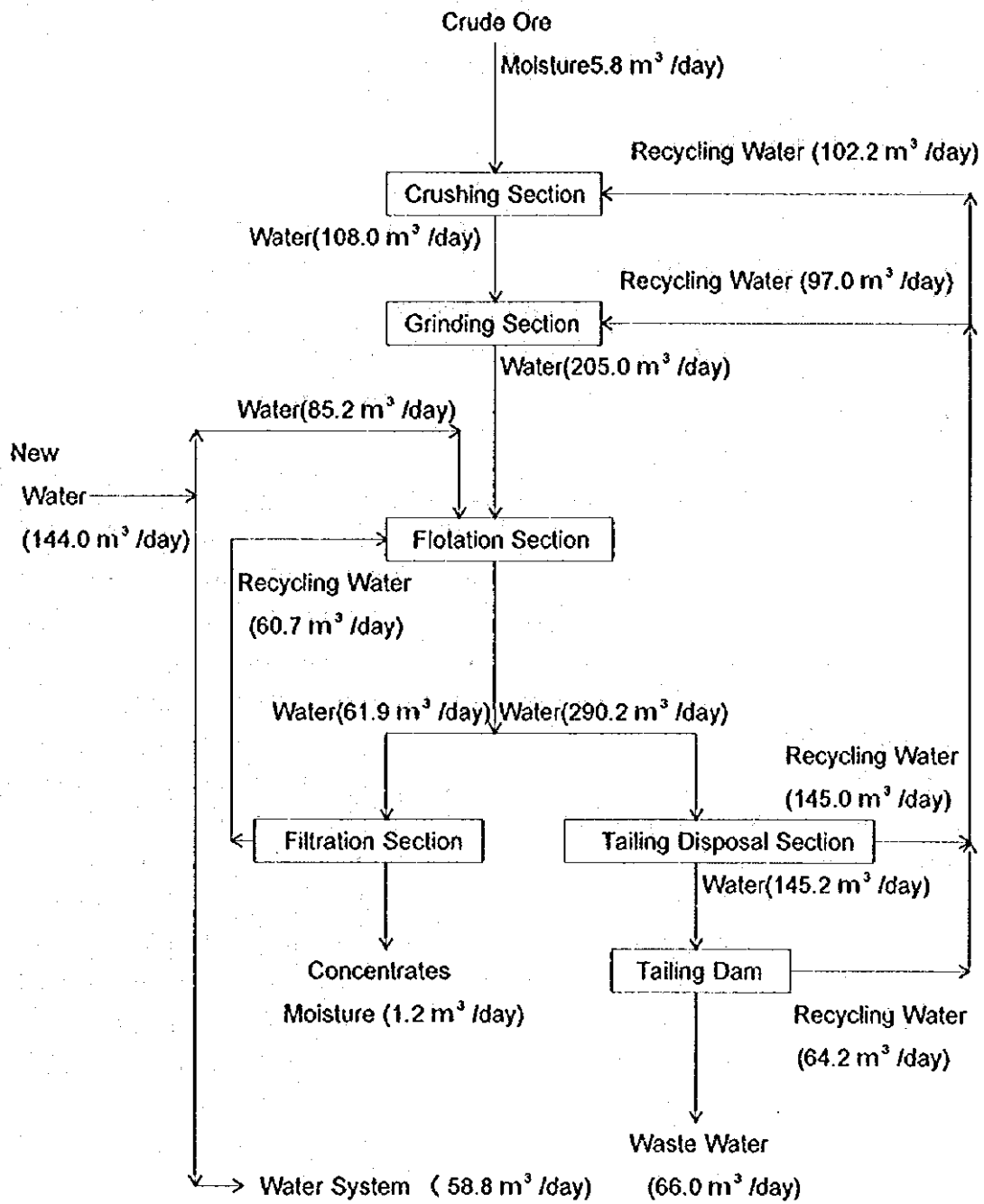
(7) Tailings section

Concentration method	Cyclone and Thickener
Density of flotation tailing (%)	20
Transportation tailing density (%)	40
Cyclone overflow's sedimentation velocity (cm/hr)	25.56

(8) Water consumption

Water consumption volume (m ³ /day)	404
New water supply volume (m ³ /day)	144
Recycle rate (%)	64

The water balance of the mineral dressing is shown in Fig.46.



*) Crusing Section 2 Shifts / day, After Grinding Section 3 Shifts / day

Fig.46 Water Balance of Mineral Dressing Plant

2.1.3 Mineral dressing process

The process flow sheet of mineral dressing plant is shown in Fig.47.

(1) Receiving of crude ore

Crude ore is hauled from underground to the surface by LHDs. A 600t stockyard is constructed near the crushing section of the mineral dressing plant for buffering ore feed and also for blending purpose. From the stockyard, ore is conveyed and fed by payloader into a receiving hopper of the crushing section.

(2) Crushing

The crushing process comprises a single series of two-stage crushing; the first stage forms an open circuit while the closed circuit is formed at the second stage.

Main equipment are one each of primary and secondary crusher, a vibrating screen which, together with the secondary crusher, forms the closed circuit, another vibrating screen for washing purpose and a spiral classifier.

A chain feeder(500mmW) extracts ore from the receiving hopper and feed it to a jaw crusher(510mm x 230mm). Crushed ore is fed by a conveyer to a washing screen(600mmW x 1,800mmL, single deck, opening size 10mm) for slime removal.

The oversize of the washing screen is fed by a conveyer to a cone crusher(600mmW) while the undersize enters in a spiral classifier. Ore crushed by the cone crusher is, in turn, fed by another conveyer to a vibrating screen(600mmW x 1,800mmL, single deck, opening size 10mm). The oversize of this screen is returned to the cone crusher while the undersize is the final crushed product. On the other hand, the undersize of the washing screen fed to the spiral classifier is separated into slime and raking sand. The classifier slime is stored in a washing thickener(4m dia) while the raking sand joins the undersize of the vibrating screen and these are transported to a mill bin as the final crushed product.

Overflow of the washing thickener is recycled to the washing screen while underflow is fed to a ball mill.

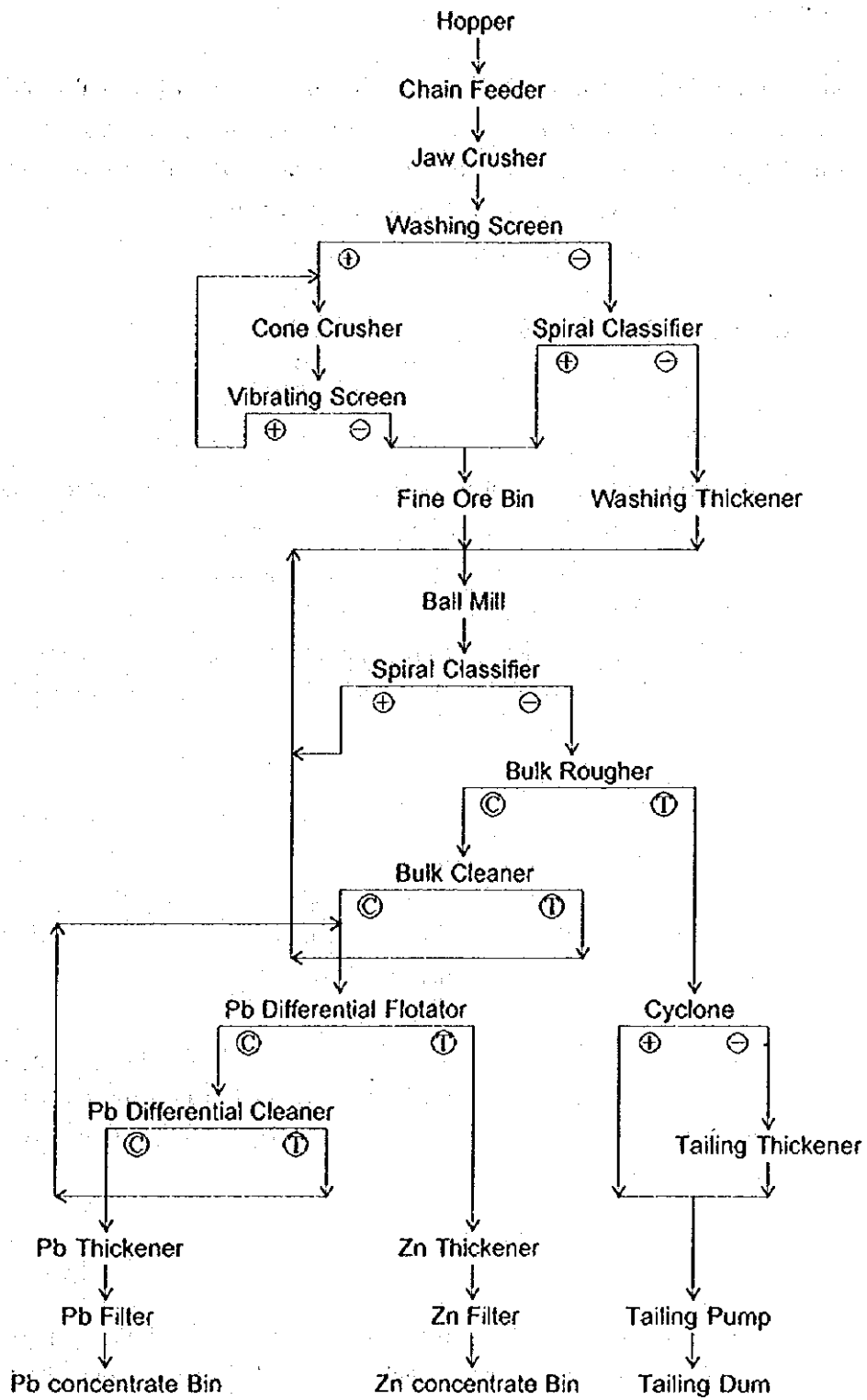


Fig.47 Process Flowsheet

(3) Grinding

Ore from the grinding section's bin is fed by conveyor to a ball mill (1500mm ϕ x 1200mmL) for grinding. Ground ore, in turn, enters the spiral classifier(600mm ϕ) and is separated into flotation feed and return sand. The return sand from the classifier is returned to the ball mill. The flotation feed is sent to the flotation section by a pump.

The grinding mill bin has a storage capacity of 100t.

(4) Flotation

The flotation process is composed of a single series of bulk flotation circuit(4 roughers of 0.6m³ and 8 cleaners of 0.28m³) and a single series of Pb differential flotation(4 roughers of 0.6m³ and 6 cleaners of 0.28m³). Flotation feed is subjected to bulk flotation roughing so that lead and zinc may be recovered as float, whilst the roughing tailing becomes the final tailing. The roughing float is further upgraded through two-stage cleaners and sent to the differential flotation. Cleaner tailings is returned to the grinding circuit.

Float in the bulk flotation is subjected to differential flotation whereby lead may be recovered as float while zinc becomes tailing. Differential flotation roughing float is upgraded to lead concentrate by the two-stage cleaners. Differential flotation cleaner tailing is returned to differential flotation feed. Zinc as differential flotation tailing is stored in the zinc concentrate thickener.

In the bulk flotation roughing and differential flotation, neither regrinding of cleaner tailing, etc. nor intermediate thickening within the flotation circuit is done because of easy liberation. Details of the flotation circuit has to be determined on a basis of pilot test results.

(5) Dewatering of concentrates

Lead concentrate and zinc concentrate, which are the final flotation products, enter their respective concentrate thickeners. Thickened concentrates are dewatered by the drum filters(900mm ϕ x 300mmL), respectively. Overflow of the both thickeners of concentrate are recycled to the flotation section.

Dewatered concentrates are sent directly to the concentrate stockyard by conveyors and stored there. When necessary during wintertime, they are dried by drum--type dryers before storage.

Concentrates at the stockyard are loaded on to trucks by a payloader and weighed by a truck scale before shipment.

2.1.4 Ancillary facilities

(1) Instrumentation

The instrumentation is limited to a minimum necessary level and installation of automation equipment is not considered. For instrumentation, pH meters are installed at the places where bulk flotation feed and differential flotation feed enter.

A control center is not envisaged.

(2) Flotation reagents, etc.

Flotation reagents to be used are sodium cyanide, copper sulfate, sodium sulfide, calcium hydroxide, isopropyl xanthate and MIBC.

Reagents are dissolved at the reagent preparation room, sent to storage tanks at the flotation section and added by constant feeders where necessary.

Following are the assumed requirements of reagents, etc. per ton of crude ore:

Sodium cyanide (g)	200
Copper sulfate (g)	70
Sodium sulfide (g)	50
Calcium hydroxide (g)	600
Isopropyl xanthate (g)	50
MIBC (g)	35
Balls for the ball mill (g)	675
Electric power (kWh)	43.2

(3) Dust collection

Dust covers are installed on the cone crushers and the vibrating screens of the crushing section, to draft dust particles, which are treated by a wet-type dust collector.

(4) Sampling

To check operation performance of the mineral dressing plant, one each of samplers is installed at the four points for sampling of the bulk flotation feed, bulk flotation tailing, final concentrate of differential flotation(Pb conc.) and differential flotation tailing(Zn conc.).

(5) Others

Power : Power for the mineral processing plant equipment are distributed at each of the three blocks, ie., 1) crushing block, 2) grinding-flotation-tailing pipage block, and 3) concentrate dewatering block.

Electric hoist : One each of 5t electric hoists is installed at the crushing and grinding sections while a 2t hoist at the flotation section, as these sections have heavy equipment.

Storage space for supplies : Appropriate spaces are provided at the crushing section, flotation section and workshop for storing supplies.

Workshop : The workshop built by the Japanese team near the shaft mouth is utilized.

Assay and laboratory : Rooms for assay, testing and sample preparation are built adjacent to the mineral dressing plant, to conduct the minimum necessary testing for the purpose of process control.

Office: A site office is provided within the mineral dressing plant.

2.2 Facilities for Tailing Disposal

2.2.1 Thickening

Flotation tailing with a concentration of around 25% is thickened by cyclones to around 45%. Cyclone overflow is sent to a tailing thickener (8m ϕ).

Thickened cyclone underflow and thickener underflow are sent together to the tailing dam by two sand pumps. Waste thickener overflow and tailing dam overflow are recycled to the crushing, grinding and flotation processes.

2.2.2 Tailing disposal

The tailing disposal has a capacity of 11-year service and is designed to allow further expansion. The dam site is selected at a location nearest possible to the mineral dressing plant and out of the area of ore deposits.

As the site is too gently inclined for tailing to be transported by the natural gradient, tailing will be transported by pipeline pressurized by Wahman pumps. However, a steep gradient is unnecessary for transportation of tailing dam overflow, which will be sent back by the natural gradient to the mineral dressing plant from the tailing dam to be sited in the upper side of the plant.

The tailing dam is an earth dam of a pond type with an embankment at the lower part to be made from soil excavated in the upper part of the site, taking advantage of the gentle gradient.

With a view to minimize the initial investment, the dam will be partitioned so it may be constructed in four separate phases, balancing the cutting volume with the banking volume.

In the upper side of the dam, an unlined channel is cut along the dam, whereby rain water is drained into a dry stream bed in the lower part.

For intake of the overflow water, a particular portion of the embankment is used for height adjustment, so that overflow can be controlled in relation to the ups and downs of the dam water level.

A plan, a location map, and a longitudinal section and a hydrographic map of the tailing dam are exhibited in Fig.48, and Apx.7, 8 and 9, respectively.

Design of various channels is based on the following assumptions:

- 60 minute rainfall depth probability : 7mm/hour
- Tailing transport volume : 300m³/8 hours
- Overflow water transport volume : 0.01m³/second

Main specifications of the tailing dam are shown in the following Table:

Descriptions	Quantity	Remarks
Volume	170,000m ³	
Area	43,000m ²	
Earth dam height	max. 5m	
Crest total length	1,300m	
Crest width	5m	
Slope gradient		
Inside wall	1 : 1.8	
Outside wall	1 : 2.0	
Cutting face of slope	1 : 1.5	
Tailing pipeline	1,350m	
Channel of overflow		
drainage cycle	640m	
Drainage for rainfall	1,560m	

Table 31 Main Specifications of the Tailing Dam

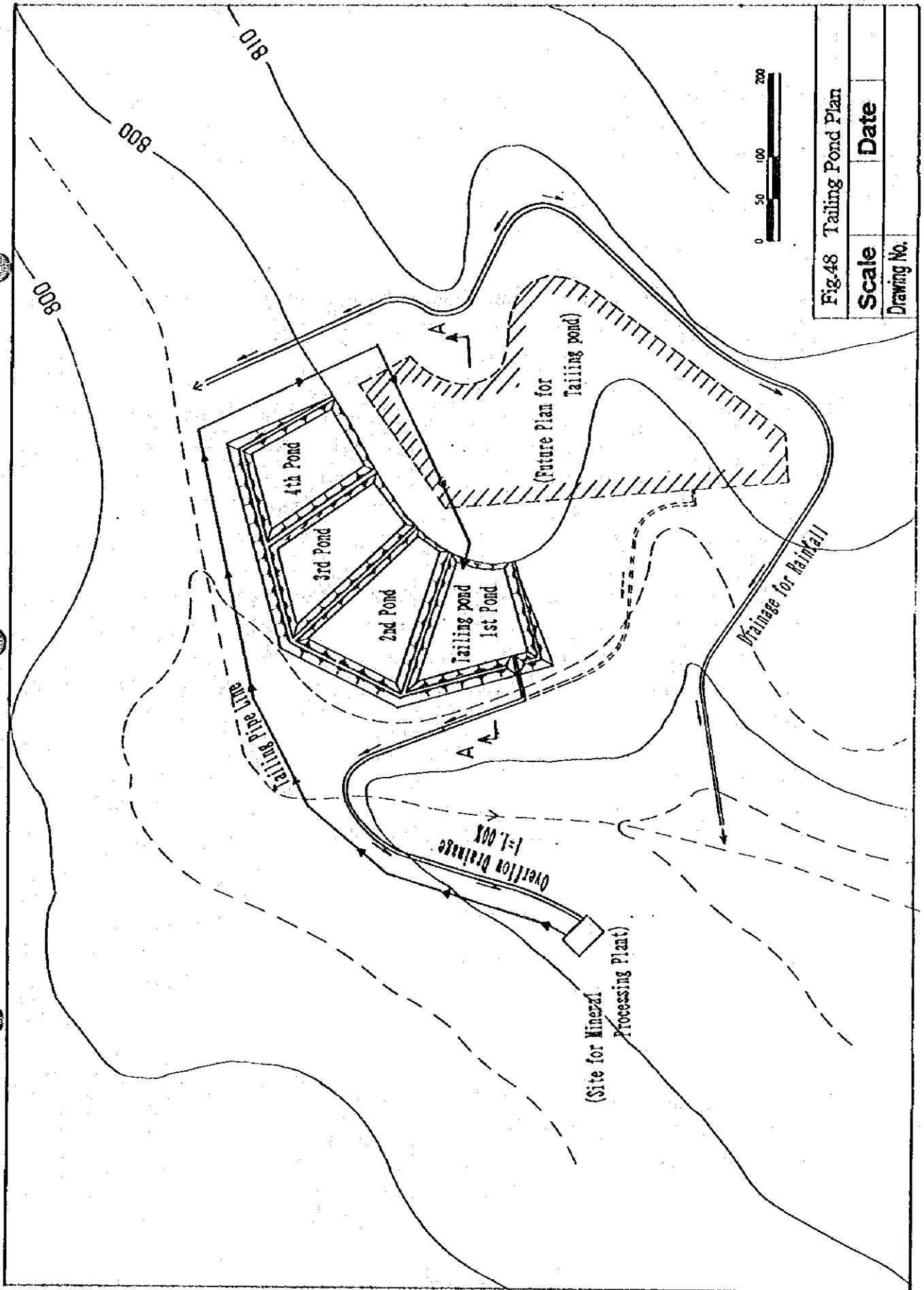


Fig.48 Tailing Pond Plan

Scale	Date
Drawing No.	

Chapter 3. Auxiliary Facilities Plan

3.1 Power Receiving and Distribution

3.1.1 General

For electric power supply, two alternatives were considered: (1) in-house power generation using the existing 750KVA generator which was used by the Japanese survey team; and (2) receiving power from a thermal power station in Choybalsan.

In case of the in-house power generation, light oil supply is uncertain and the price is expensive. The state-run power station in Choybalsan, cap. 36,000kW, is operated with lignite mined from Adun Choulung open-pit colliery and is supplying power to the city of Choybalsan and also to the three nearby villages of Helren, Baitomung and Toblagan.

Power is transmitted at 35KV from Choybalsan to Helren(approx. 50km) and at 10KV from Helren to Habilka(approx. 70km). From Habilka to Tsav, no transmission line has been laid. The Choibalsan power station is said to have a surplus supply capacity of 2,000 to 3,000kW in summertime and about 1,000kW in wintertime.

In order for the Tsav mine to receive power supply from the Choybalsan station, a 35KV transmission line would have to be laid by the power station from the village of Habilka to Tsav(approx. 80km). 50% of the cost is to be borne by the user.

In this project, the alternative of receiving power from Choybalsan is chosen, since the long-term stable power supply at low cost is essential. The alternative would be beneficial to the future development of the surrounding area, as well.

3.1.2 Power demand

The maximum power demand of the Tsav mine's production units and other facilities is estimated at about 600KW, whilst the annual power demand is about 2,300MWh, which is broken up as follows:

Section	Maximum Power Demand(KWh)	Annual Power Demand(MWh)
Mining	400	960
Mineral Dressing	200	1,296
Total	600	2,256

3.1.3 Power receiving and distribution facilities

In order for the Tsav mine to receive power from Choybalsan, to be added to the existing facilities are : (1) an outdoor cubicle for receiving power at 35KV, (2) a 750KVA transformer, and (3) a 3.3KV outdoor cubicle.

(1) Outdoor cubicle for power receiving at 35KV

The cubicle contains a disconnecting switch(DS) board and a vacuum circuit breaker(VCS) panel, to which a protective relay for power receiving has to be added.

(2) 750KVA transformer

The transformer is to step down from the receiving tension of 35KV to 3.3KV, the distribution tension within the mine. The required capacity is put at 750KV, considering the mentioned power demand.

(3) 3.3KV outdoor cubicle

This cubicle is to send the power stepped down by the transformer from 35KV to 3.3KV to the electric systems existing at the mine. It has no synchronizing device as parallel feed with the diesel generator is not considered.

3.1.4 Power cost comparison

Estimated power cost in case power is supplied by Choybalsan

Transmission line laying cost	US\$ 267,000.-
Power receiving facilities	335,000.-
Power charges (for mine life)	* ¹ 1,985,000.-
Total	US\$ 2,587,000.-

Estimated power cost in case of in-house generation

Light oil and lubricant *² US\$4,417,000.-

Remarks: *¹ (2,256,000kWh x 11 years x 0.08\$/kWh)

*² (\$1,100/day x 365days x 11 years)

The cost per day is based on the actual cost at Tsav.

In case of the in-house generation, labor cost for generator operators and generator repair costs have to be considered, in addition to the oil and lubricant costs. This indicates that receiving power from Choybalsan is far more economical than in-house generation.

3.2 Communication equipment

At present, communication to and from the mine site is done by wireless equipment provided respectively in Ulaan Baatar, Choybalsan and Tsav. No additional investment for communication such as telephone/facsimile via INMARSAT is contemplated in this project.

3.3 Water Supply Facilities

Currently, the drinking water is brought to Tsav by a water wagon from a well dug by an ex-USSR team 6km away from Tsav, stored in a 50m³ tank, and distributed to each section. This project follows the current system and contemplates no extra investment.

As for industrial water, 100 l /min out of some 200 l /min of the estimated total underground drainage will be sent to a water storage tank of the mineral

dressing plant. The fresh water will be used mainly for the cleaning process whilst, for the other processes, overflow of the tailing dam and thickeners will be recycled, in an effort to minimize water consumption.

3.4 Workshop

Repair of the underground heavy machinery and mineral dressing equipment is of great importance. In this project, utilization of the existing workshop (24m x 13m) built by the Japanese survey team near the shaft mouth of the No.4 vein is contemplated so that an additional investment may be done without.

3.5 Ancillary Facilities and Vehicles in Common Use

3.5.1 Office and Staff accommodations

A 660m² building which houses an office and staff accommodations is planned to be built at the site where accommodation for the Japanese survey team was located. The site is conveniently located in respect of water supply and drainage, sewage systems and electric power facilities.

For workers' accommodation, the existing building which was used as the Mongolians' accommodation during the survey period is utilized.

3.5.2 Vehicles in common use

A microbus for transporting personnel between Choybalsan and Tsav and a 11t dump truck for transporting concentrates to Hambilka station is included in this project, as vehicles in common use. Facilities such as the ambulance and hospital are not considered in this project.

3.6 Transportation of Concentrates

3.6.1 Stockyard

Lead concentrate and zinc concentrate are stored at a stockyard near the mineral dressing plant until shipment. Storage capacity of the yard is planned to meet the monthly output, i.e., 200t of lead concentrate and 110t of zinc concentrate.

3.6.2 Concentrate transportation route

Feasibility of concentrate shipment to Russia has been studied. Under the current economic conditions of the nation, however, the Russian smelters-refineries at Zabaykarsk and Sherlovaya Cora have curtailed or suspended operation and their future trends are hardly predictable. Therefore, it is assumed in this project that the concentrates are to be shipped to coastal smelters-refineries in Japan despite the problems of shipping lot and shipping cost.

For this alternative, the following two routes are considered:

- (1) Tsav → Borzya → Karymskoe → (the Siberian Railways) →
Vladivostok → (ocean transportation) → Japan
- (2) Tsav → Borzya → Zabaykarsk → (the Chinese Railways) →
Dalian → (ocean transportation) → Japan

The transportation costs come to US\$ 80/t and \$ 70/t, respectively. Apparently, the second alternative route via China is less expensive. However, in case of shipment via China, bulk shipment of concentrates is not allowed, which involves extra bagging costs; furthermore, troubles may arise from the difference between the rail gauge of China and that of Mongolia and Russia.

Taking all these factors into consideration, the first alternative route via Russia is chosen for this project. For the transportation of concentrates to the nearby Hambilka station, an 11t dump truck will be used.

Chapter 4. Production Plan and Personnel

4.1 Production Plan

The production plan is based on the following assumptions:

Ore reserves and grade: 1,544,627t

Cu	Pb	Zn	Au	Ag
0.22%*	6.84%	4.01%	1.3g/t*	263g/t

Average mining recovery: 18%

Average dilution: 21%

Minable crude ore and grade: 332,464t

Cu	Pb	Zn	Au	Ag
0.22%*	6.37%	2.94%	1.22g/t*	161g/t

Annual production of crude ore: 30,000t

Arithmetical mine life: 11 years

Mineral dressing recovery:

Pb	Zn	Au	Ag
88.3%	92.8%	79.0%	82.6%

Annual production of concentrates: Pb conc 2,731t

Zn conc 1,351t

Grade of concentrates:

	Cu(%)	Pb(%)	Zn(%)	Au(g/t)	Ag(g/t)
Pb conc	0.32	69.0	5.0	11.10	1,507
Zn conc	2.77	4.4	51.0	2.09	307

Remarks: * indicates an average grade of the proved and probable ore reserves.
(For the possible ore reserve, no assay has been done of Cu and Au.)

The mineral dressing performance shown in Table below is used for projection of mine revenues.

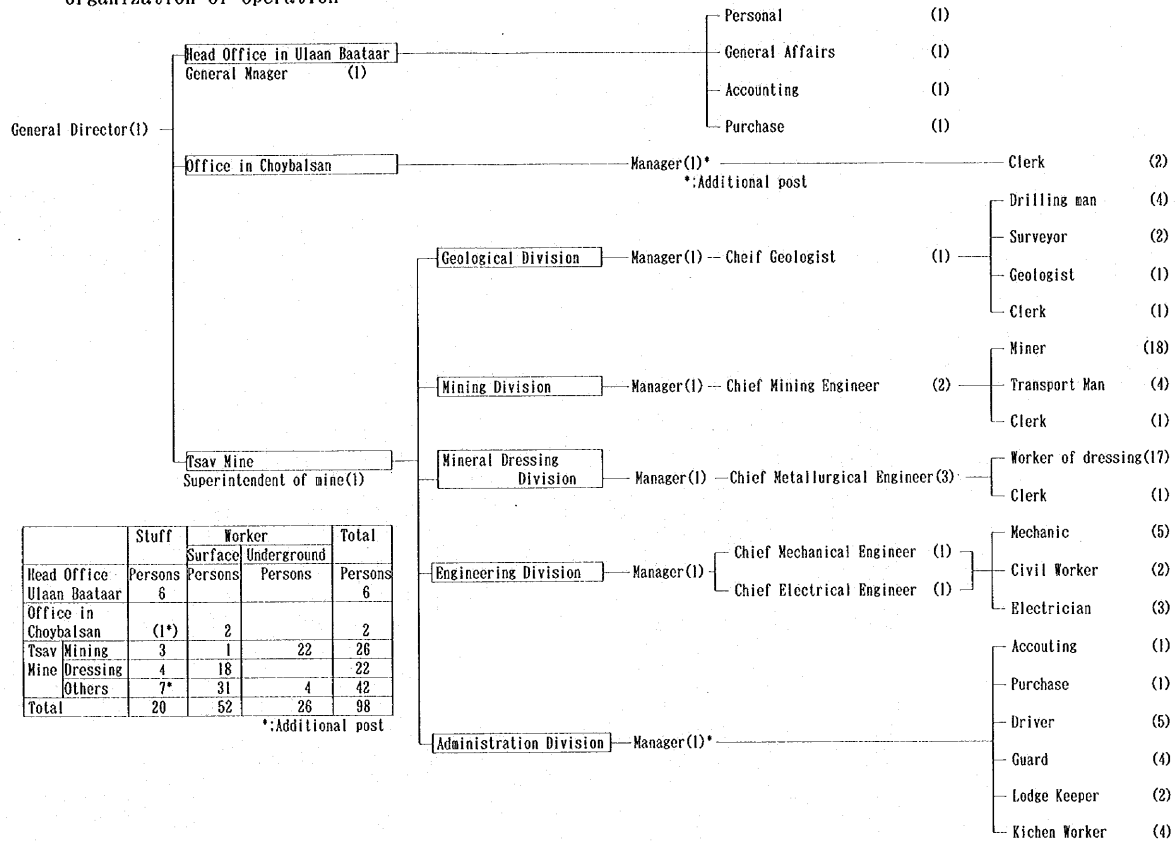
	Quantity (t)	Grade					Distribution				
		Au g/t	Ag g/t	Pb %	Zn %	Cu %	Au %	Ag %	Pb %	Zn %	Cu %
Crude ore	30,000	1.22	161	6.4	2.9	0.22	100.0	100.0	100.0	100.0	100.0
Pb con	2,371	11.01	1,507	69.0	5.0	0.32	71.3	74.0	85.2	13.6	11.5
Zn con	1,351	2.09	307	4.4	51.0	2.77	7.7	8.6	3.1	79.2	56.6
Tail.	26,278	0.29	32	0.9	0.2	0.08	21.0	17.4	11.7	7.2	31.9

Table 32 Mineral dressing performance

4.2 Personnel Plan

The organization for operation and personnel arrangement by section and class are shown in Fig. 49.

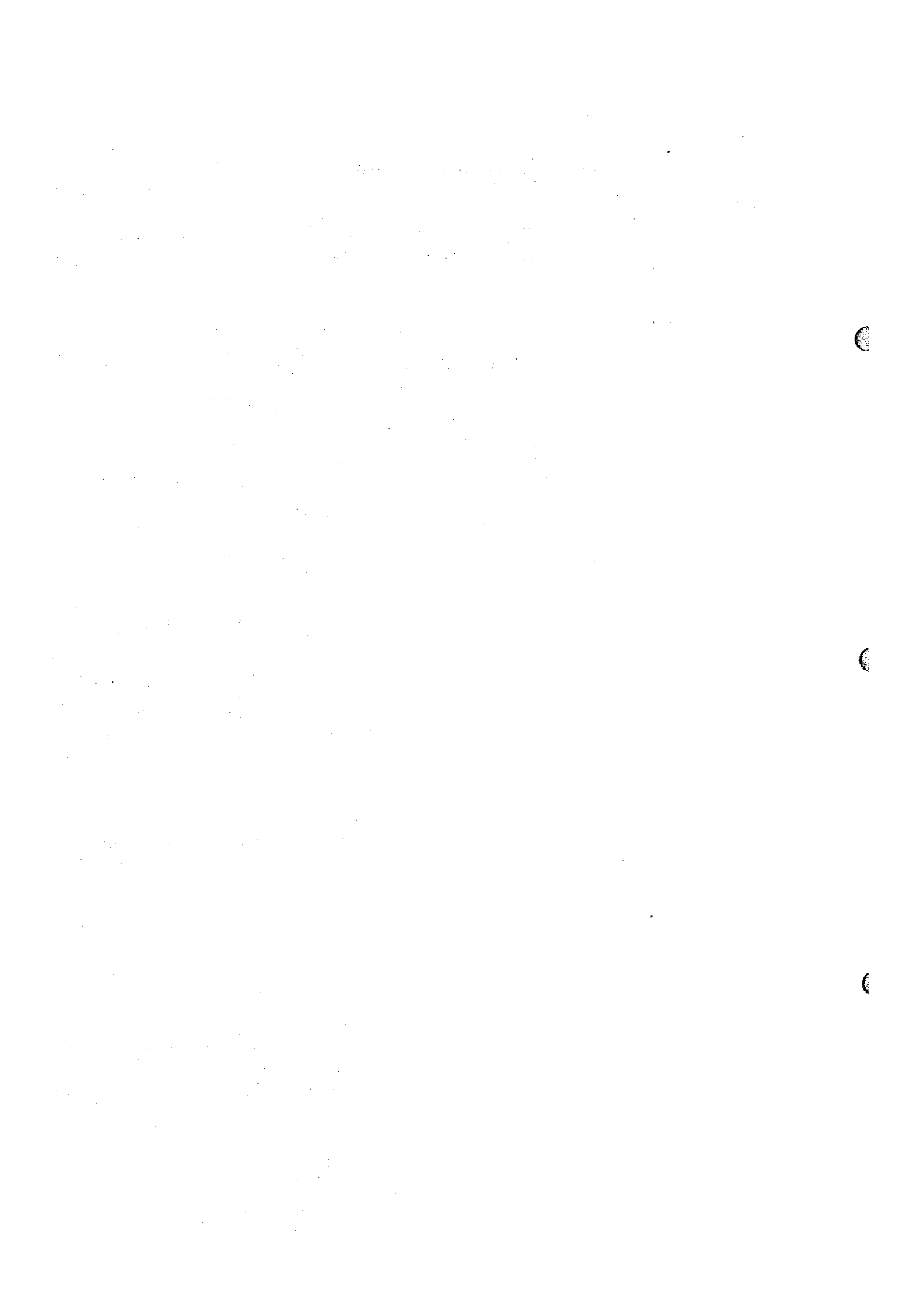
Organization of Operation



	Staff Persons	Worker		Total Persons
		Surface Persons	Underground Persons	
Head Office Ulaan Baataar	6			6
Office in Choybalsan	(1*)	2		2
Tsav Mining	3	1	22	26
Mine Dressing	4	18		22
Others	7*	31	4	42
Total	20	52	26	98

*:Additional post

Fig.49 Organization of Operation



Chapter 5. Environmental Survey

5.1 General

The Tsav area is situated at a gentle hill in the steppe without trees. There is no streams with constant water flow. Only during a limited period of a year, rain water occasionally form puddles at hollows on the surface but such surface water evaporates due to the region's dry climate and puddles gradually disappear. In some cases, the underground water table appears on the surface at sunken places, forming springs, which rarely last through a year, though. The local nomads draw up and use the ground water for their living.

In August when a survey was conducted, some puddles with rain water were seen here and there in the area; however, there was no ponds or swamps where surface water stays permanently, in the downstream side of the water systems near the planned sites for the mineral dressing plant and the tailing dam and near the water system, into which the underground mine water is currently drained. The drained water, while flowing a short distance, say 1km, on the surface, sinks into the ground.

In the light of these observations, it is considered that, after the mine has been developed, water pollution by the drainage from mine and mineral dressing plant is unlikely to widely spread over the downstream side of the local water system but likely to be confined within a limited area around the mine and plant. For this reason, the survey on soil and ground water was limited only to this area.

5.2 Soil

In the vicinity of Tsav deposits, surface soil samples were collected at four points at a dry stream into which the mine and plant drainage is expected to flow. The four points are: the upper side of the drainage point, near the drainage point and two points in the lower side of the drainage point. For comparison purpose, another soil sample was taken at a place away and independent from the mentioned dry stream. These samples were brought back to Japan for assay of the five heavy metal contents(Cu, Pb, Zn, Fe and Cd) as well as arsenic content.

The assay results in Table 33 indicate a certain difference in Pb and Zn concentration between the upper sampling point and the lower sampling points while no difference in

concentration of the other elements is indicated. Cu, Ad and As are in low grades whilst Fe is considered to be abundant over an extensive area, independently of the ore deposits. The area, in which the difference in Pb and Zn concentration is recognized, is not so wide. It is anticipated, therefore, that water pollution possibly caused by the mine development would be confined to a limited area in the lower side of the mineral dressing plant.

Assay of sample soil taken from the point chosen for comparison purpose indicated Cu 50ppm, Pb 340ppm, Zn 260ppm, Fe 2.5%, Cd <2.5ppm and As 31ppm, which serve as the background values before the mine development is commenced. The assay also indicates the arsenic content being somewhat high, which characterizes this area.

Sampling points	Upper side of shaft mouth upstream	Near shaft mouth immediately downstream	Lower side of shaft mouth mid-stream	Lower side of shaft mouth downstream	Comparative point (uninfluenced by ore deposits)
Samples taken on : 11 August					
Cu (ppm)	60	40	48	45	52
Pb (ppm)	1000	470	420	260	340
Zn (ppm)	480	290	320	190	250
T-Fe (%)	2.6	2.3	2.5	2.7	2.5
Cd (ppm)	<2.5	<2.5	<2.5	<2.5	<2.5
As (ppm)	53	35	31	29	30

Table 33 Environmental Survey around Tsav Deposits(Assay of soil)

5.3 Underground Water

In order to check the present state of pollution of the underground mine water and well water in Tsav area and also to obtain background values, water quality measurement was conducted three times on different days of sample water collected at two points underground (water used for drilling and underground spring water at a separate location) and also of sample water taken from a well that is used for drinking, the latter serving for comparison with the former.

Three samples collected on the final day of measurement and one sample taken from another well(different from the abovementioned well) were brought back to Japan for assay of the five heavy metal contents and arsenic content, similarly to the case of soil.

The results of the assay and water quality measurement are shown in Table 34 and 35, respectively.

Based upon these results, suitability of the Tsav underground water for mineral dressing use was also studied.

The items of water quality measurement are pH, electric conductivity, turbidity, dissolved oxygen, water temperature, Cu, Fe^{2+} , total Fe, Zn, Ni, Mn, Cr^{6+} , COD, NO_3-N and NH_4^+-N , of which pH, electric conductivity, turbidity, dissolved oxygen and water temperature were measured by instruments while the other items were checked by summary measurement with test papers. Underground water and well water were measured once every week over three weeks, but no significant difference was found.

Underground water taken at two points showed high Zn and total Fe among the metal contents while, among the organic components, COD, NH_4^+-N and NO_3-N were high. In the underground water, a minute amount of zinc was detected, which indicates that zinc contained in the ore deposits dissolves into underground water. The total Fe contained in the drilling water suggests influence of the iron piping. The recognized COD, NO_3-N and NH_4^+-N are presumed to derive from the pastured animals' droppings which flowed with rain water into the vertical shaft and decomposed, and/or to be influenced by components of the explosives used underground.

In the water samples taken from two different wells outside Tsav area, organic pollutants such as COD and NO_3-N of minute quantities were detected, which are also presumed to derive from the feces of pastured horses and cows. Except this, no other questions were encountered.

On the basis of the survey findings, suitability of the underground water for the mineral dressing process water was studied, as well. Although all the water surveyed is hard water with somewhat high electric conductivity, it may be concluded that there would be no problem whatsoever if the underground water is used for the mineral dressing of ore.

As for drinking water, it is desirable to use well water located in an area where Zn and Fe contents, as well as organic pollutant contents, are low, although it is not impossible to use the underground water after certain treatment.

Sampling points	Well water	Underground water	Underground drilling water	Well water near magazine
Samples taken on : 14 August				
Cu (ppm)	<0.01	<0.01	<0.01	<0.01
Pb (ppm)	<0.05	<0.05	<0.05	<0.05
Zn (ppm)	0.07	0.31	1.5	0.01
T-Fe (ppm)	0.55	0.22	1.5	0.07
Cd (ppm)	<0.005	<0.005	<0.005	<0.005
As (ppm)	<0.01	<0.01	<0.01	<0.01

Table 34 Environmental Survey around Tsav Deposits
(Water Quality Analysis)

Sampl- ing Points	Well water	Under- ground water	Under- ground water drill- ing	Well water	Under- ground water	Under- ground water drill- water	Well water	Under- ground water	Under- ground water drill- ing	Well water near Maga- zine
Date	taken on 2 August			taken on 8 August			taken on 14 August			
pH	8.2	8.2	7.4	8.5	8.2	7.2	8.4	8.1	7.3	7.7
Electric conductivity (mS/cm)	1.3	1.1	1.3	1.3	1.0	1.3	1.3	1.0	1.3	1.1
Turbidity (NTU)	0	10	100	2	6	240	2	12	111	4
Dissolved oxygen (ppm)	7.3	11.2	6.5	8.7	10.8	7.5	9.9	10.6	8.5	11.2
Water temperature (°C)	14.3	8.9	15.4	13.4	13.0	18.8	10.4	10.6	15.2	11.5
Measurement with test paper										
Cu (ppm)	<0.5	<0.5	<0.5	<0.5	<0.5	0.5	<0.5	<0.5	<0.5	<0.5
Fe ²⁺ (ppm)	<0.2	<0.2	<0.2	<0.2	<0.2	2	<0.2	<0.2	≤0.2	<0.2
T-Fe (ppm)	≤0.2	<0.2	0.4	≤0.2	<0.2	7	<0.2	≤0.2	1	≤0.2
Zn (ppm)	0	0	1	0	0	2	0	0	2	0
Ni (ppm)	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5
Mn (ppm)	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	0.5	<0.5
Cr ⁶⁺ (ppm)	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05
COD (ppm)	2	15	18	10	20	40	3	8	20	5
NO ₃ -N (ppm)	<0.006	0.03	<0.006	<0.006	0.04	<0.006	<0.006	0.03	<0.006	<0.006
NH ⁴⁺ -N (ppm)	0.6	0.6	0.8	0.4	0.4	0.6	0.4	0.6	1.2	0.4

Table 35 Environmental Survey around Tsav deposits
(Water Quality Measurement)

Chapter 6. Revenue Plan

6.1 Concentrate Prices

6.1.1 Assumptions

- (1) Quotation of metals: Pb \$650/t, Zn \$1,100/t, Au \$390/tr oz, Ag \$5.30/tr oz.
- (2) Payable metals: Pb concentrate – Pb : 95% (Minimum deduction 3%)
Au : 1g less; recovery 90%
Ag : 95% (Minimum deduction 100g)
Zn concentrate – Zn : 85% (Minimum deduction 8%)
Au : 1g less; recovery 65%
Ag : 4 tr oz less; recovery 60%
- (3) Treatment charges(T/C) and refining charges(R/C):
Pb concentrate – Pb : T/C \$160/DMT; scale + 14 ¢ /\$ (Base=\$600)
Ag : R/C 30 ¢ /tr oz
Zn concentrate – Zn : T/C \$190/DMT
Zinc quotation \$1,250 ~ \$1,250 ~ 1,000 ~ \$1,000
T/C scale +15 ¢ /\$ +13 ¢ /\$ –8 ¢ /\$
- (4) Penalty: Not applied as impurities are yet to be assayed.
- (5) Concentrate transportation to Japan via Siberian route: \$80/WMT, incl. transportation loss(0.5%) and moisture(8%)
- (6) Transportation insurance: 0.077% x (concentrate price – T/C – R/C)

6.2 Revenues

Revenues calculated on these assumptions are shown in Table 36.

Production 、 Revenue Plan

Quantity of mining crude ore:100t/day x 300days/year=30,000t/year

Quantity of treated ore:100t/day x 300days/year = 30,000t/year

Pb-Zn-Concentrate→Export to Japan

		unit	-1	1	2	3	4	5	6	7	8	9	10	11	12	Total
Crude ore production		30 '000t/y	%	30	30	30	30	30	30	30	30	30	30	30	30	330
Grade of Pb		6.40 %	%	6.40	6.40	6.40	6.40	6.40	6.40	6.40	6.40	6.40	6.40	6.40	6.40	6.40
Minable Zn		2.90 %	%	2.90	2.90	2.90	2.90	2.90	2.90	2.90	2.90	2.90	2.90	2.90	2.90	2.90
Au		1.22 g/t	g/t	1.22	1.22	1.22	1.22	1.22	1.22	1.22	1.22	1.22	1.22	1.22	1.22	1.22
Ag		161 g/t	g/t	161	161	161	161	161	161	161	161	161	161	161	161	161
Pb- Concentrate		Quantity	DMT/y	2,371	2,371	2,371	2,371	2,371	2,371	2,371	2,371	2,371	2,371	2,371	2,371	26,979
Grade of Pb		69.0%	Recovery 85.20%	%	69.00	69.00	69.00	69.00	69.00	69.00	69.00	69.00	69.00	69.00	69.00	69.00
Grade of Au			Recovery 71.30%	g/t	11.00	11.00	11.00	11.00	11.00	11.00	11.00	11.00	11.00	11.00	11.00	11.00
Grade of Ag			Recovery 74.00%	g/t	1,365	1,365	1,365	1,365	1,365	1,365	1,365	1,365	1,365	1,365	1,365	1,365
Zn- Concentrate		Quantity	DMT/y	1,351	1,351	1,351	1,351	1,351	1,351	1,351	1,351	1,351	1,351	1,351	1,351	14,862
Grade of Zn		51.0%	Recovery 79.20%	%	51.00	51.00	51.00	51.00	51.00	51.00	51.00	51.00	51.00	51.00	51.00	51.00
Grade of Au			Recovery 7.70%	g/t	2.10	2.10	2.10	2.10	2.10	2.10	2.10	2.10	2.10	2.10	2.10	2.10
Grade of Ag			Recovery 8.60%	g/t	579	579	579	579	579	579	579	579	579	579	579	579
Payable Metal Pb-C		Pb Transportation	95 %	t	1,546	1,546	1,546	1,546	1,546	1,546	1,546	1,546	1,546	1,546	1,546	17,009
Au loss 0.5%			90 %	toz	683	683	683	683	683	683	683	683	683	683	683	7,508
Unit Discount			-1 g													
Ag			95.0 %	toz	98,347	98,347	98,347	98,347	98,347	98,347	98,347	98,347	98,347	98,347	98,347	1,081,819
Zn-C		Zn Transportation	85 %	t	583	583	583	583	583	583	583	583	583	583	583	6,410
Au loss 0.5%			65.0 %	toz	31	31	31	31	31	31	31	31	31	31	31	340
Unit Discount			-1 g													
Ag			60.0 %	toz	11,788	11,788	11,788	11,788	11,788	11,788	11,788	11,788	11,788	11,788	11,788	129,673
Unit Discount			-4 toz													0
Conc Price Pb-C		Pb Price	650 \$/t	'000US\$	1,005	1,005	1,005	1,005	1,005	1,005	1,005	1,005	1,005	1,005	1,005	11,056
Au Price			390 \$/toz	'000US\$	266	266	266	266	266	266	266	266	266	266	266	2,928
Ag Price			5.3 \$/toz	'000US\$	521	521	521	521	521	521	521	521	521	521	521	5,734
Zn-C		Zn Price	1,100 \$/t	'000US\$	641	641	641	641	641	641	641	641	641	641	641	7,051
Au Price			390 \$/toz	'000US\$	12	12	12	12	12	12	12	12	12	12	12	133
Ag Price			5.3 \$/toz	'000US\$	62	62	62	62	62	62	62	62	62	62	62	687
Pb T/C		Scale at 600\$	114c/\$	'000US\$	394	394	394	394	394	394	394	394	394	394	394	4,333
Ag R/C			30 c/toz	'000US\$	30	30	30	30	30	30	30	30	30	30	30	325
Zn T/C		Scale at 1,250\$(115c/\$), 1,260\$	>1,000\$	'000US\$	255	255	255	255	255	255	255	255	255	255	255	2,810
Penalty			13c/\$, 1,000\$	'000US\$												0
Insurance			\$/DMT/%	'000US\$												0
(Pb-C Price-T/C-R/C)x0.077%		0.077 %		'000US\$	1.054	1.054	1.054	1.054	1.054	1.054	1.054	1.054	1.054	1.054	1.054	12
(Zn-C Price-T/C-R/C)x0.077%		0.077 %		'000US\$	0.354	0.354	0.354	0.354	0.354	0.354	0.354	0.354	0.354	0.354	0.354	4
Freight																0
Pb-C		Moisture 8%	80.0 \$/DMT	'000US\$	204	204	204	204	204	204	204	204	204	204	204	2,242
Zn-C		Moisture 8%	80.0 \$/DMT	'000US\$	116	116	116	116	116	116	116	116	116	116	116	1,278
Revenue Pb-C		Price-T/C,R/C-insu-Freel-Pn		'000US\$	1,164	1,164	1,164	1,164	1,164	1,164	1,164	1,164	1,164	1,164	1,164	12,806
Zn-C		Price-T/C,R/C-insu-Freel-Pn		'000US\$	344	344	344	344	344	344	344	344	344	344	344	3,780
Total Revenue				'000US\$	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	17,139

Table 36 Production 、 Revenue Plan

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Chapter 7. Initial, Additional and Replacement Investments and Operating Expenses

7.1 Estimated Initial Investment

7.1.1 Basis for assumption

As regards applicable Mongolian laws and regulations, and for estimation of salaries and wages, machinery prices, construction costs and general price level, the data and information as of September 1995 when the survey was conducted are used as the basis for assumption.

(1) Development and construction period : One year

(2) Infrastructure : The power transmission line from Helren to Tsav(80km) is laid by the state-run Choybalsan Electric Power Company. 50% of construction cost is to be borne by the Tsav mine.

(3) Procurement of equipment and supplies : Those which are available in Mongolia are reinforcing steel bars and cement. All the other equipment, machinery and supplies have to be imported from Russia, China or Japan.

(4) Customs duty : 7.5% of the FOR prices of imported equipment and supplies is included in the operating expenses.

(5) Exchange rates:

Mongolian Togrog(Tg) per US Dollar – 450Tg/\$

Japanese Yen(¥) per US Dollar – ¥100/\$

(6) Escalation : Not considered.

(7) Rate of interest during construction : 6% p.a.

7.1.2 Initial Investment Summary

An annual projection of estimated divisional initial investment (up to project start-up) is indicated in Table.37, which may be summarized as follows:

	US\$'000
(1) Mining division	
Excavation machinery, batch plant, trucks for mining operation	1,142
(2) Mineral dressing division	
Construction of mineral dressing plant and equipment	1,386
(3) Auxiliary(common cost) division	
Power receiving facilities, transmission line cost sharing, office and accommodation construction	937
(4) Tailing disposal	
(Initial-phase construction expenses are included in the operating cost)	341
(5) Development preparation	
Head office overheads, customs duties	138
(6) Interest during construction	240
(7) Working capital(10% of divisional initial investment)	347
	<u>4,531</u>
Initial Investment -- Total	4,531

7.2 Additional and Replacement Investments

US\$530,000 is appropriated for the replacement of two LHDs in the sixth year after start-up. In reality, the amount is insufficient for proper replacement capital since the other mining machinery and vehicles including the jumbo should also be replaced, which is burdensome to the project cash flow, though. Therefore, replacement investment has to be limited to the minimum necessary.

Additional investment in phased construction of the tailing dam is included in the repair expense under the mineral dressing division's operating expenses, as in the case of the initial investment, for the second, fifth and eighth years, respectively, after start-up of operation.

7.3 Estimated Operating Expenses

7.3.1 Basis for Estimation

- (1) Exchange rate : Same as the initial investment
- (2) Salary and wage : For estimation, personnel are classified into three categories: staff, surface and underground. (Further classification by type of job is not made.) To the estimated salaries and wages, social insurance premiums of 3% and 1.5%, and labor accident insurance premium of 1.0% are added.
- (3) Consumables and machine parts : All the consumable items and machine parts, excepting cement and reinforcing steel bars, are assumed to be imports, which include explosives, detonators, mineral dressing reagents and fuels. The surveyed local prices in Mongolia of these goods are supposed to include customs duties.
{Customs duties: 15% on general goods and 7.5%(reduced rate) on mining machinery }
- (4) Electric power rate :
At Choybalsan, the rate is 8 ¢ /kWh (= 36Tg/450Tg/US\$)
Ref. 3.5 ¢ /kWh in Ulaan Baartaar
- (5) Royalty : 10% of the revenues
- (6) Agent's commission : US\$5.00 per ton of concentrate
- (7) Corporate income tax :

Profit before tax (PBT)	Tax rate
\$1 ~ 1,000	0%
\$1,001 ~ 33,300	15%
\$33,301 ~ 66,600	\$500 + (PBT - \$33,300) x 25%
\$66,601 ~ 100,000	\$1,300 + (PBT - 66,600) x 35%
\$100,001 ~	\$2,500 + (PBT - 100,000) x 40%

7.3.2 Operating Expenses Summary

Annual projection of the direct (divisional) operating expenses (from mining to

concentrate production) and the indirect operating expenses are shown in Table 38 and 39, which may be summarized on an annual average basis, as follows:

	Annual average (US\$'000)	per ton of crude ore (US\$/t)
Mining	699	23.3
Mineral dressing	348	11.6
Head office	35	1.2
Direct operating exp – Total	1,082	36.1
Depreciation exp	317	10.6
Royalty	151	5.0
Agent's commission	19	0.6
Operating Expenses – Total	1,569	52.3

Chapter 8. Financial Valuation

8.1 Internal Financial Rate of Return

To estimate internal financial rate of return (IFRR), a leading index in the financial valuation, it is vital to make a financial projection based on a well-defined fund sources and application. In turn, cash inflow and outflow items are sorted out and a cash flow chart is drawn up, wherein the net inflow, or difference between cash inflow and outflow, is calculated so that a rate of return may be determined.

8.1.1 Sources and application of funds

Funds required for realization of the project are composed of the initial investment, additional investment, interest during construction and working capital.

Raising of the funds is planned as follows:

- (1) The project capital structure at the project start-up is assumed to comprise equity capital (30%) and borrowings (70%), which meets a normal equity-borrowings ratio in international projects. Funds required at the project start-up are those for the initial investment (in construction and equipment) and working capital. The working capital is estimated at 10% of the initial investment.
- (2) For the borrowing, low interest loans from an international financing agency such as the World Bank is contemplated, as the interest rates in Mongolia is very high in terms of international standards. The borrowing at the project start-up is a long-term loan while shortages of funds during operation is to be funded by short-term loans. Interest rate for these borrowings is assumed to be 6% p.a.
- (3) The 6% interest is to be paid against the outstanding loan balance as of the preceding year's end. The long-term loan principal is to be repaid in equal annual installments from the fourth to the eleventh year. The short-term loan principals are to be repaid whenever surplus cash flow is available.
- (4) Based on the assumptions in (1) thru (3) above, the total project capital consisting of equity capital and borrowings is assumed to be \$3,811,000, equal to the invested funds plus the working capital required for the operation phase. Therefore, the equity capital comes to \$1,143,000 while the borrowings to \$2,668,000.

8.1.2 Cash flow chart and IFRR

The project cash flow chart (profit and loss projection and fund sources and application) and IFRR are exhibited in Table 39.

The cash inflow side of the chart includes revenue from product sale and salvage value of equipment whilst investment expenditure, operating expenses, taxes and other expenses are included in the cash outflow side.

The corporate income tax is calculated in the following formula:

Corporate income tax = (Revenue - operating expenses - royalty - agent's commission - depreciation expense - interest) x applicable tax rate (ref. 5.3.1)

The straight-line depreciation which is generally used in Mongolia is applied to the project.

In the case of this project, the IFRR, a discount rate at which the present value of the total net cash inflow comes to zero, turns out to be (-)3.0%.

In this study, the income tax is calculated of the difference obtained by deducting all the expense (including interest) from the cash inflow (revenue) and, in turn, the tax is entered in the cash outflow; therefore, it is significant to evaluate the project's financial feasibility by comparing the IFRR and the interest rate for borrowing. The financial analysis for the project is considered unfavorable since the IFRR is far below the assumed interest rate of 6%.



Direct Operating Expense

RAILWAYS

Article	Unit	Price	1st year		2nd year		3rd year		4th year		5th year		6th year		7th year		8th year		9th year		10th year		Note	
			Quantity	Amount	Quantity	Amount	Quantity	Amount	Quantity	Amount	Quantity	Amount	Quantity	Amount	Quantity	Amount	Quantity	Amount	Quantity	Amount	Quantity	Amount		
Mining Division																								
Personal Expense																								
Staff	S/W	1,200.00	10	12,000	10	12,000	10	12,000	10	12,000	10	12,000	10	12,000	10	12,000	10	12,000	10	12,000	10	12,000		
Exterior	S/W	935.33	34	31,733	34	31,733	34	31,733	34	31,733	34	31,733	34	31,733	34	31,733	34	31,733	34	31,733	34	31,733		
Interior	S/W	1,185.00	26	28,110	26	28,110	26	28,110	26	28,110	26	28,110	26	28,110	26	28,110	26	28,110	26	28,110	26	28,110		
Total			70	79,853	70	79,853	70	79,853	70	79,853	70	79,853	70	79,853	70	79,853	70	79,853	70	79,853	70	79,853		
Material Expense																								
Nuts - Bolt	S/W	3.37	30,000	101,100	30,000	101,100	30,000	101,100	30,000	101,100	30,000	101,100	30,000	101,100	30,000	101,100	30,000	101,100	30,000	101,100	30,000	101,100		
Explosives	S/W	0.53	30,000	15,900	30,000	15,900	30,000	15,900	30,000	15,900	30,000	15,900	30,000	15,900	30,000	15,900	30,000	15,900	30,000	15,900	30,000	15,900		
Detonators	S/W	0.09	30,000	2,700	30,000	2,700	30,000	2,700	30,000	2,700	30,000	2,700	30,000	2,700	30,000	2,700	30,000	2,700	30,000	2,700	30,000	2,700		
Fuels	S/W	0.15	30,000	4,500	30,000	4,500	30,000	4,500	30,000	4,500	30,000	4,500	30,000	4,500	30,000	4,500	30,000	4,500	30,000	4,500	30,000	4,500		
Machinery - Electric Parts	S/W	0.90	30,000	27,000	30,000	27,000	30,000	27,000	30,000	27,000	30,000	27,000	30,000	27,000	30,000	27,000	30,000	27,000	30,000	27,000	30,000	27,000		
Depreciation of above mentioned	N	.30		24,800		24,800		24,800		24,800		24,800		24,800		24,800		24,800		24,800		24,800		
Total				418,800		418,800		418,800		418,800		418,800		418,800		418,800		418,800		418,800		418,800		
Development Expense																								
Nuts - Bolt	S/W	138.30	240	33,192	240	33,192	240	33,192	240	33,192	240	33,192	240	33,192	240	33,192	240	33,192	240	33,192	240	33,192		
Explosives	S/W	21.80	240	5,232	240	5,184	240	5,184	240	5,184	240	5,184	240	5,184	240	5,184	240	5,184	240	5,184	240	5,184		
Detonators	S/W	0.70	240	168	240	168	240	168	240	168	240	168	240	168	240	168	240	168	240	168	240	168		
Fuels	S/W	0.20	240	48	240	48	240	48	240	48	240	48	240	48	240	48	240	48	240	48	240	48		
Machinery - Electric Parts	S/W	158.60	240	38,184	240	38,136	240	38,136	240	38,136	240	38,136	240	38,136	240	38,136	240	38,136	240	38,136	240	38,136		
Depreciation of above mentioned	N	.20		4,855		4,855		4,855		4,855		4,855		4,855		4,855		4,855		4,855		4,855		
Total				130,951		130,951		130,951		130,951		130,951		130,951		130,951		130,951		130,951		130,951		
Electric Exp.	S/W	0.85	350,000	297,500	350,000	297,500	350,000	297,500	350,000	297,500	350,000	297,500	350,000	297,500	350,000	297,500	350,000	297,500	350,000	297,500	350,000	297,500		
Mining Direct Expense Total	S			638,745		638,745		638,745		638,745		638,745		638,745		638,745		638,745		638,745		638,745		
Per Ton of Mining Direct Expense	S/W			23.23		23.23		23.23		23.23		23.23		23.23		23.23		23.23		23.23		23.23		
Roasting Division																								
Personal Expense																								
Staff	S/W	1,200.00	4	4,800	4	4,800	4	4,800	4	4,800	4	4,800	4	4,800	4	4,800	4	4,800	4	4,800	4	4,800		
Exterior	S/W	935.33	18	16,836	18	16,836	18	16,836	18	16,836	18	16,836	18	16,836	18	16,836	18	16,836	18	16,836	18	16,836		
Total				21,636		21,636		21,636		21,636		21,636		21,636		21,636		21,636		21,636		21,636		
Material Expense and others																								
Chemical Reagent	S/W	4.53	30,000	135,900	30,000	135,900	30,000	135,900	30,000	135,900	30,000	135,900	30,000	135,900	30,000	135,900	30,000	135,900	30,000	135,900	30,000	135,900		
Balls - Mill Liners	S/W	0.14	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200		
Balls for B. C. and Filters	S/W	0.12	30,000	3,600	30,000	3,600	30,000	3,600	30,000	3,600	30,000	3,600	30,000	3,600	30,000	3,600	30,000	3,600	30,000	3,600	30,000	3,600		
Fuels	S/W	0.55	30,000	16,500	30,000	16,500	30,000	16,500	30,000	16,500	30,000	16,500	30,000	16,500	30,000	16,500	30,000	16,500	30,000	16,500	30,000	16,500		
Machinery - Electric Parts	S/W	1.50	30,000	45,000	30,000	45,000	30,000	45,000	30,000	45,000	30,000	45,000	30,000	45,000	30,000	45,000	30,000	45,000	30,000	45,000	30,000	45,000		
Roasting Expense	S/W	0.34	30,000	10,200	30,000	10,200	30,000	10,200	30,000	10,200	30,000	10,200	30,000	10,200	30,000	10,200	30,000	10,200	30,000	10,200	30,000	10,200		
Construction Expense of Mill	S/W		341,000		305,000		276,000		246,000		216,000		186,000		156,000		126,000		96,000		66,000		36,000	
Analysis and others	S/W	0.14	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200	30,000	4,200		
Electric Exp	S/W	0.64	1,250,000	800,000	1,250,000	800,000	1,250,000	800,000	1,250,000	800,000	1,250,000	800,000	1,250,000	800,000	1,250,000	800,000	1,250,000	800,000	1,250,000	800,000	1,250,000	800,000		
Service water Expense	S/W	0.18	30,000	5,400	30,000	5,400	30,000	5,400	30,000	5,400	30,000	5,400	30,000	5,400	30,000	5,400	30,000	5,400	30,000	5,400	30,000	5,400		
Total				270,290		245,500		220,500		195,500		170,500		145,500		120,500		95,500		70,500		45,500		
Roasting Direct Expense Total	S			341,000		305,000		270,290		245,500		220,500		195,500		170,500		145,500		120,500		95,500		
Per Ton of Roasting Direct Expense	S/W			11.31		11.31		11.31		11.31		11.31		11.31		11.31		11.31		11.31		11.31		
Lead Office																								
Personal Expense																								
Staff	S/W	1,200.00	6	7,200	6	7,200	6	7,200	6	7,200	6	7,200	6	7,200	6	7,200	6	7,200	6	7,200	6	7,200		
Overseas				1,000		1,000		1,000		1,000		1,000		1,000		1,000		1,000		1,000		1,000		
Transportation Expense				3,000		3,000		3,000		3,000		3,000		3,000		3,000		3,000		3,000		3,000		
Expenses on Machinery (Electric)	Complex			121,800		112,000		102,200		92,400		82,600		72,800		63,000		53,200		43,400		33,600		
Total				138,100		127,200		116,400		105,600		94,800		84,000		73,200		62,400		51,600		40,800		
Grand Total	S			618,190		610,175		597,125		584,175		571,125		558,175		545,125		532,175		519,125		506,175		
Per Ton of Direct Expense	S/W			22.37		22.37		22.37		22.37		22.37		22.37		22.37		22.37		22.37		22.37		

Table 38 Direct Operating Expense

SECRET



THE HISTORY OF THE UNITED STATES

The history of the United States is a complex and multifaceted story that spans centuries. It begins with the early Native American civilizations, such as the Mayans, Aztecs, and Incas, who developed advanced societies in the Americas. The arrival of European explorers in the late 15th and early 16th centuries marked the beginning of a new era. The Spanish, French, and British established colonies and territories across the continent, leading to a period of intense competition and conflict. The American Revolution (1775-1783) was a pivotal moment in the nation's history, as the thirteen original colonies declared their independence from Great Britain. This led to the formation of the United States of America, a new nation based on the principles of liberty, democracy, and the rule of law. The early years of the republic were marked by challenges, including the struggle for a stable government and the expansion of territory. The War of 1812 solidified the nation's independence and led to a period of national pride and expansion. The mid-19th century was a time of rapid growth and change, with the discovery of gold in California and the opening of the transcontinental railroads. However, this period was also marked by the struggle over slavery, which ultimately led to the Civil War (1861-1865). The war resulted in the abolition of slavery and the preservation of the Union, but it also left deep scars on the nation. The Reconstruction era (1865-1877) was a period of significant change and challenge, as the nation sought to rebuild and integrate the newly freed African Americans. The late 19th and early 20th centuries were a time of industrialization and progress, but also of social and economic inequality. The Progressive Era (1890s-1920s) was a period of reform and social change, as Americans sought to address the problems of the industrial revolution. The Great Depression (1929-1939) was a period of economic hardship and social despair, which led to the New Deal and the rise of Franklin D. Roosevelt. World War II (1941-1945) was a defining moment in the nation's history, as the United States emerged as a superpower and a leader in the world. The Cold War (1945-1991) was a period of tension and competition between the United States and the Soviet Union, which shaped the global landscape. The late 20th and early 21st centuries have been a time of significant change and challenge, with the end of the Cold War, the rise of the Internet, and the 9/11 attacks. The United States continues to be a major power in the world, and its history remains a source of inspiration and reflection for people around the globe.

THE HISTORY OF THE UNITED STATES

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Chapter 9. Economic Valuation

9.1 Shift from Financial Cost to Economic Cost

The financial analysis attempts to appraise an investment project from the private investor's standpoint. It lays emphasis on whether the project will generate a due reward and seeks for conditions for the profit maximization. On the other hand, the economic analysis is to evaluate project feasibility from the viewpoint of national economy, in search of the most efficient utilization of public resources as the evaluation criterion.

The economic analysis, therefore, requires adjustment of transfer costs employed in the financial analysis, calculation of opportunity cost, modification of exchange rates to be applied, adjustment of cost of public goods, etc., as detailed in the following paragraphs:

9.1.1 Adjustment of transfer cost

For computation of project economic cost, transfer costs such as taxes included in financial cost have to be adjusted or deducted. In this study, the customs duty imposed on imported goods, the commodity tax included in local commodity prices, the corporate income tax imposed on operating profit, and the royalty levied on sales revenue are deducted as transfer items. The other transfer costs are left unadjusted as they are considered negligible.

For the customs duty adjustment, 15% on general goods and 7.5% on mining machinery, etc. are deducted from the financial costs of imports. As for local goods, the 10% commodity tax is deducted from their financial costs.

In the actual calculation, 95% of material cost included in the (financial) operating cost is assumed to be imports while the remaining 5% is assumed to represent local procurement, from which 15% or 10% are deducted as the tax portions, respectively. 10% is also deducted from the local transportation cost.

As regards the initial investment cost, 30% of the cost of those equipment that requires erection work is assumed to be local costs (for erection and local transportation), from which 10% (commodity tax) is deducted, while 7.5% (customs

duty) is deducted from the remaining 70%(imported mining machinery).

9.1.2 Estimation of opportunity cost of labor

This study assumes that, as for demand and supply of skilled labor(staffs) in Mongolia, the market mechanism is relatively well functioning under nearly perfect competition and, therefore, labor cost is determined at a level reflecting the actual situation of the Mongolian economy, free from market distortions. Based on the assumption, opportunity cost of skilled labor is determined by the actual market rate, which is same as the labor cost in the financial analysis.

As for opportunity cost of unskilled labor, the question is not as simple as skilled labor. In Mongolia, as well as in Choybalsan, the unemployment rate is very high. The labor market is in a state of excess labor economy. This implies that opportunity cost of unskilled labor stays at a rate considerably inferior to the actual market rate of wages applied as the financial cost.

According to the public employment security office at Choybalsan, about 3,900 out of the city's total population of 40,000 are unemployed and 70% of the unemployed is youths under 32. In this study, therefore, opportunity cost(economic cost) of unskilled labor(workers other than staffs) is assumed to be a half of the financial labor costs.

9.1.3 Modification of exchange rate

It is a general practice to observe the national trade balance, changes in the wholesale price level, etc. to find out a real(shadow) exchange rate to be applied to the economic valuation of a project. In the relationship between the past Mongolian trade/price data and the official exchange rates, however, regularities are not necessarily recognizable, probably because the nation is still in the process of transition to a market economy since 1989.

Owing to the dear interest policy pursued in Mongolia to depress the hyper-inflation, the Tugrog seems to have been over-estimated. But inflation rate has declined from 325.5% in 1992 to 66.3% in 1994 and recently, it has settled down to a level of 2% per month. Besides, most of the project equipment and machinery which constitutes a major part of the project costs are imports which

are settled in US Dollars. Considering these factors, no modification is made in this study on the exchange rate used for the financial analysis.

9.1.4 Cost of public goods

Since the cost of laying the power transmission line is the public expenditure, only 50% of the total cost, which must be borne by a user, is included in the financial costs of the project. For economic analysis, however, the full cost must be counted in.

9.2 Internal Economic Rate of Return(IERR)

Unlike the financial analysis, the economic analysis focuses on a difference between cost and benefit in terms of economic price, after eliminating the transfer cost such as tax.

All the goods and services related to the project are divided into the foreign currency portion(traded goods) and the local currency portion(non-traded goods), the former's value being measured with a shadow exchange rate. (In this study, however, the same official exchange rate is applied, as explained.)

In accordance with these procedures, profit and loss projection, fund sources and application and IERR exhibited in Table 40 have been calculated, on the basis of the operating expenses, divisional initial investment cost and depreciation expenses exhibited in Table 41 and 42. The discount rate at which the present value of net benefit(benefit less cost) of this project comes to zero is 8.3%. In order to judge the project desirability from the national viewpoint, IERR is used as a criterion. The World Bank is said to consider an investment project feasible when IERR is not less than 12%, whilst 8% is the lower limit for the USAID and 10% for the Asian Development Bank. Whether or not this project is feasible from the viewpoint of national economy is a delicate question to answer.



Profit & Loss Statement-Funds-Sources and Application-Internal Economical Rate of Return

Profit & Loss Statement

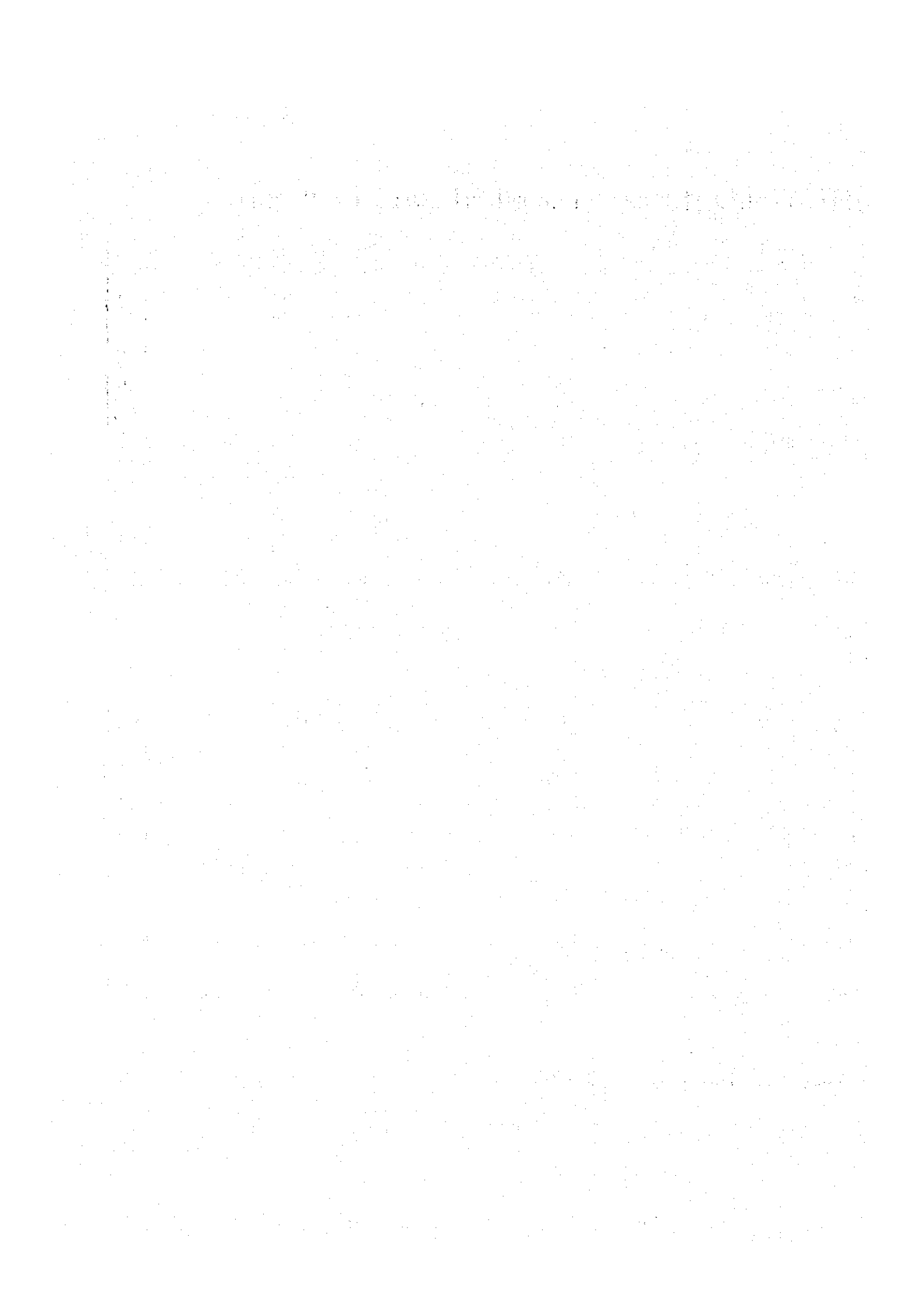
		Unit	-1	1	2	3	4	5	6	7	8	9	10	11	Total	
Revenue		'000US\$		1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	1,508	622	17,208
Expense																
Direct Operat-Mining		'000US\$	0	588	588	588	588	588	588	588	588	588	588	588		6,472
ting Expense Dressing		'000US\$	310	226	413	226	226	413	226	413	226	413	226	226		3,359
Head Office		'000US\$	11	51	11	11	11	11	51	11	11	11	11	11		210
Total		'000US\$	321	865	1,013	825	825	1,013	865	825	1,013	825	825	825		10,041
Royalty	Revenuex10%	0 %	0	0	0	0	0	0	0	0	0	0	0	0		0
Agent Comis, Conc Qualityx5%	5 %	'000US\$	0	19	19	19	19	19	19	19	19	19	19	19		214
Depreciation		'000US\$	0	432	437	437	437	437	301	301	301	301	146	50		3,580
Interest	6 %	'000US\$	0	175	170	168	168	147	126	105	84	63	42	21	-0	1,268
Total		'000US\$	321	1,492	1,639	1,449	1,449	1,616	1,312	1,251	1,417	1,299	1,033	916	-0	15,104
Profit before Tax		'000US\$	-321	16	-131	59	59	-108	196	257	91	299	475	592	622	2,105
Tax																
Corporate Profit<0	0%	'000US\$	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Income Tax Profit<1,500/450*000}	18%															0
Profit<3,000/450*000}	25%															0
Profit<4,500/450*000}	35%															0
Profit>4,500/450*000}	40%															0
Total		'000US\$	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Profit after Tax		'000US\$	-321	16	-131	59	59	-108	196	257	91	299	475	592	622	2,105

Funds-Sources and Application

		Unit	-1	1	2	3	4	5	6	7	8	9	10	11	Total	
Revenue	Profit after Tax	'000US\$	-321	16	-131	59	59	-108	196	257	91	299	475	592	622	2,105
	Depreciation	'000US\$	0	432	437	437	437	437	301	301	301	301	146	50		3,580
	Allowance for Reinvestment	'000US\$														0
	Equity of Capital	'000US\$	1,198													1,198
	Long-term Borrowings	'000US\$	2,796													2,796
	Short-term Borrowings	'000US\$	125													125
	Total	'000US\$	3,799	448	306	495	495	329	497	558	392	600	621	642	622	9,804
Expense	Investment	'000US\$	3,632						550							4,182
	Interest during construction	'000US\$	168													168
	Working Capital	'000US\$		363												0
	Repayment of long-term Borrowings	'000US\$					350	350	350	350	350	350	350	350		2,796
	Repayment of short-term Borrowings	'000US\$		85	40											125
	Total	'000US\$	3,799	448	40	0	350	350	880	350	350	350	350	-14	0	7,251
Cash flow surplus		'000US\$	-0	-0	265	495	146	-21	-382	209	42	251	272	656	622	2,553
Total Cash flow surplus		'000US\$	-0	-1	265	760	906	895	503	711	754	1,904	1,276	1,932	2,553	11,547
Cash flow		'000US\$	-3,952	260	476	663	663	476	93	663	476	663	663	1,026	622	2,791

Cashflow=Cash flow surplus-Equity Capital-Borrowings+Repayment+Interest
 DCFIRR= 8.3% NPV(8%)= 57
 NPV(9%)= -148

Table 40 Profit & Loss Statement-Funds-Sources and Application-Internal Economical Rate of Return







Investment & Depreciation of each division(Economical)

Article	Qty	Inventory No	Serial No	Original Book Value	Invest Date	1st year		2nd year		3rd year		4th year		5th year		6th year		7th year		8th year		9th year		10th year		11th year		Rate				
						Book Value	Deprecia	Book Value	Deprecia	Book Value	Deprecia	Book Value	Deprecia	Book Value	Deprecia	Book Value	Deprecia	Book Value	Deprecia	Book Value	Deprecia	Book Value	Deprecia	Book Value	Deprecia	Book Value	Deprecia		Book Value	Deprecia		
						1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000	1000		1000	1000	1000	
Water Division																																
Cable for Meters	1 set	1	318,000	5	31,500	0.183	318,000	55,800	234,200	55,800	188,400	55,800	142,600	55,800	86,800	55,800	31,000	31,000	31,000	31,000	31,000	31,000	31,000	31,000	31,000	31,000	31,000	31,000	31,000	31,000		
Water Plant	1 set	1	240,416	5	24,041.6	0.100	240,416	48,083.2	192,332.8	48,083.2	144,250.4	48,083.2	96,167.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	48,083.2	
Equipment of Stationery	1 set	1	316,000	5	31,600	0.100	316,000	63,200	252,800	63,200	189,600	63,200	126,400	63,200	63,200	63,200	63,200	63,200	63,200	63,200	63,200	63,200	63,200	63,200	63,200	63,200	63,200	63,200	63,200	63,200	63,200	
Water Truck (2nd)	1 set	1	40,000	5	8,000	0.200	40,000	7,200	32,800	7,200	25,600	7,200	18,400	7,200	11,200	7,200	4,000	4,000	4,000	4,000	4,000	4,000	4,000	4,000	4,000	4,000	4,000	4,000	4,000	4,000	4,000	
Food Build (2nd)	1 set	1	350,000	5	35,000	0.100	350,000	70,000	280,000	70,000	210,000	70,000	140,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	70,000	
Food Build (2nd) 2nd	1 set	1	180,000	5	18,000	0.100	180,000	36,000	144,000	36,000	108,000	36,000	72,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	36,000	
Truck (2nd) 2 pieces	1 set	1	32,000	5	3,200	0.100	32,000	6,400	25,600	6,400	19,200	6,400	12,800	6,400	6,400	6,400	6,400	6,400	6,400	6,400	6,400	6,400	6,400	6,400	6,400	6,400	6,400	6,400	6,400	6,400	6,400	
Water (2nd) 2 pieces	1 set	1	60,000	5	6,000	0.100	60,000	12,000	48,000	12,000	36,000	12,000	24,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	12,000	
Water Pump	1 set	1	45,000	5	4,500	0.111	45,000	9,000	36,000	9,000	27,000	9,000	18,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	9,000	
Total of Water Division																																
			1,252,416		125,241.6		1,127,174.4	225,482.8	901,691.6	225,482.8	676,208.8	225,482.8	450,726.0	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	225,482.8	
Municipal Division																																
Swallow (Facilities) (Water One Street)	2	2	324,880	5	32,488	0.100	324,880	64,976	259,904	64,976	194,928	64,976	129,952	64,976	64,976	64,976	64,976	64,976	64,976	64,976	64,976	64,976	64,976	64,976	64,976	64,976	64,976	64,976	64,976	64,976	64,976	
Wiring	2	2	252,200	5	25,220	0.100	252,200	50,440	201,760	50,440	151,320	50,440	100,880	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440	50,440
Insulation	2	2	222,216	5	22,221.6	0.100	222,216	44,443.2	177,772.8	44,443.2	133,329.6	44,443.2	88,886.4	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2	44,443.2
Concrete On (Water) (Filter Drive)	2	2	162,500	5	16,250	0.100	162,500	32,500	130,000	32,500	97,500	32,500	65,000	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500	32,500
Wiring (Water) (Facilities)	2	2	142,000	5	14,200	0.100	142,000	28,400	113,600	28,400	85,200	28,400	56,800	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400	28,400
Wiring (Water) (Obsolete Resources)	2	2	11,472	5	1,147.2	0.100	11,472	2,294.4	9,177.6	2,294.4	6,883.2	2,294.4	4,588.8	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4	2,294.4
Concrete (Water) (Filter)	2	2	18,500	5	3,700	0.100	18,500	3,700	14,800	3,700	11,100	3,700	7,400	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700	3,700
Water (Water) (Filter)	2	2	58,316	5	5,831.6	0.100	58,316	11,663.2	46,652.8	11,663.2	35,000	11,663.2	23,326.4	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2	11,663.2
Water (Water) (Filter) 2nd	2	2	178,064	5	17,806.4	0.100	178,064	35,612.8	142,451.2	35,612.8	106,838.4	35,612.8	71,676.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8	35,612.8
Total of Municipal Division																																
			1,248,356		124,835.6		1,123,520.4	224,705.2	900,815.2	224,705.2	676,110.0	224,705.2	451,404.8	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	224,705.2	
Water Division																																
Books of Construction Cost (Electric Power Line)	1	1	485,458	5	48,545.8	0.100	485,458	97,091.6	388,366.4	97,091.6	291,274.8	97,091.6	184,183.2	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	97,091.6	
Office (Secretary (600 sq)) 1 set	1	1	180,500	5	18,050	0.100	180,500	36,100	144,400	36,100	108,300	36,100	72,200	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100	36,100
Truck	1	1	62,000	5	6,200	0.100	62,000	12,400	50,600	12,400	38,200	12,400	25,800	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400	12,400
Truck for Transportation of Concrete (1st)	1	1	50,000	5	5,000	0.100	50,000	10,000	40,000	10,000	30,000	10,000	20,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000	10,000
Receiving Facility of Electric Power	1	1	358,000	5	35,800	0.100	358,000	71,600	286,400	71,600	214,800	71,600	143,200	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600	71,600
Total of Water Division																																
			1,139,958		113,995.8		1,025,962.2	205,191.6	820,770.6	205,191.6	620,579.0	205,191.6	410,389.4	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	205,191.6	
Total of all Divisions																																
			4,140,400		414,040		3,726,360	745,280	2,981,080	745,280	2,235,800	745,280	1,490,520	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	
Total of all Divisions																																
			4,140,400		414,040		3,726,360	745,280	2,981,080	745,280	2,235,800	745,280	1,490,520	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	745,280	

Table 42 Investment & Depreciation of each division(Economical)

1954-1955

