THE COLLABORATIVE STUDY ON THE COMPREHENSIVE ENERGY DEVELOPMENT PLAN IN THE ISLAMIC REPUBLIC OF IRAN

MARCH 19

PLAN & BUDGET ORGANIZATION (PBO)
THE ISLAMIC REPUBLIC OF IRAN

THE COLLABORATIVE STUDY

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THE COMPREHENSIVE ENERGY

DEVELOPMENT PLAN

IN

THE ISLAMIC REPUBLIC OF IRAN

FINAL REPORT Vol. 3 Appendix

MARCH 1994



INSTITUTE FOR RESEARCH IN PLANNING AND DEVELOPMENT

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## FINAL REPORT

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## I. Tables Corresponding to Figures in Chapters 2, 3, and 4 of the Main Report.

(The year of the Islamic Republic of Iran begins on March 21 of the Gregorian calendar and ends on the following March 20. To arrive at the corresponding Gregorian years, 621 years should be added to the Iranian years.)

Table 2.1 -2.8

THE PLE	-2.0							1	and the second of the	
										[Mrd. Rs/a]
Year	VAG	MINR+IN	VOI	VWP	VCO	VTRC	VSE	GD	IMPTO	IMPC
1353	1,394	782	4,826	84	564	674	2,697	11,610	1,335	1,331
1354	1,530	852	4,250	88	763	819	3,283	12,316	1,991	3,489
1355	1,706	1,106	4,781	. 91	1,150	866	3,774	14,250	2,151	3,803
1356	1,640	1,161	4,408	99	1,070	874	3,943	13,972	2,484	4,019
1357	1,747	1,042	3,144	99	964	813	4,028	12,551	1,679	2,908
1358	1,851	911	2,535	105	758	891	4,074	11,911	1,204	1,835
1359	1,915	1,019	866	92	763	903	3,952	10,321	1,175	1,738
1360	1,953	1,098	883	106	671	736	3,771	9,847	1,290	2,149
1361	2,091	1,062	1,948	127	696	770	3,774	11,110	1,251	2,308
1362	2,193	1,186	2,006	132	937	890	4,246	12,348	1,883	4,352
1363	2,354	1,327	1,626	148	890	906	4,354	12,363	1,638	3,867
1364	2,538	1,298	1,644	162	773	907	4,466	12,533	1,305	2,421
1365	2,651	1,210	1,403	174	649	785	3,869	11,353	946	2,199
1366	2,716	1,341	1,599	193	550	643	3,698	11,189	1,006	2,209
1367	2,648	1,358	1,754	186	433	600	3,431	10,824	791	1,869
1368	2,746	1,477	1,890	207	426	655	3,446	11,294	946	2,915
1369	2,968	1,707	2,265	247	438	796	3,703	12,673	1,274	
						VED 0				******
Year	IMPI	IMPC	CC	CR	CR	KTO	XTO	IMTO	IBTO	ITO
1353	4,266	1,017	408	1,535	1,756	3,658	5,159	500	1,134	1,634
1354	6,212	1,995	501	1,760	2,146	4,696	4,850	866	1,587	2,453
1355	6,713	2,250	511	1,621	2,379	6,385	5,404	904	2,425	3,329
1356	7,910	2,697	694	1,813	2,307	8,679	4,707	987	2,244	3,231
1357	5,350	2,114	811	1,910	2,347	11,377	3,457	592	2,031	2,623
1358	5,301	2,559	1,042	2,041	2,177	14,976	2,659	378	1,438	1,816
1359	6,207	2,899	1,338	2,190	1,968	17,080	869	358	1,490	1,848
1360	8,225	3,141	1,653	1,986	1,948	19,026	843	426	1,298	1,724
1361	6,861	2,676	1,936	1,936	1,910	19,564	1,726	473	1,368	1,842
1362	10,840	2,911	2,411	2,130	1,930	19,576	1,899	720	1,831	2,551
1363	8,310	2,317	2,641	2,192	1,811	20,915	1,546	828	1,734	2,562
1364	7,411	1,576	2,806	2,252	1,898	25,011	1,400	617	1,537	2,153
1365	5,461	1,695	3,132	2,143	1,508	38,286	1,221	320	1,326	1,646
1366	5,498	1,662	3,727	2,027	1,403	51,260	1,557	245	1,116	1,361
1367	4,829	1,479	4,330	1,893	1,396	56,817	1,730	278	894	1,173
1368	7,548	2,344	5,402	2,052	1,189	74,318	1,866	393	864	1,257
1369			6,864	2,395	1,337		2,253	518	918	1,436

Table 2.9 Total & Urban population

(Unit:Million)

					Omment,
Year	Total	Urban	Year	Total	Urban
1338	21,204	7.072	1370	57.263	32,585
1340	22.444	7.743	1372	60.162	34.57
1342	23.739	8.489	1374	62.962	36,549
1344	25.091	9.316	1376	65.891	38.64
1346	26.501	10.233	1378	68.822	40.752
1348	27.97	11.247	1380	71.884	42.959
1350	29.499	12.369	1382	75.081	45.265
1352	31.089	13.607	1384	78.268	47.574
1354	32.818	15.139	1386	81.59	49.975
1356	34.736	16.648	1388	84.886	52.367
1358	37.991	18.45	1390	88.315	54.849
1360	41.221	20.604	1392	91.883	57.427
1362	44.438	23.093	1394	95.408	59.982
1364	47.807	25.802	1396	99.068	62.63
1366	50.995	28.067	1398	102.666	65.241
1368	54.504	30.778	1400	106.396	67.94

Table 2.10 Crude Oil Price in the World Market & Domestic cons. of Oil

Year	Pxoil[\$/bl]	Doil[bl/a]	Year	Pxoil[\$/bl] Do	il[Mio. bl/a]
1348	n.a.	188.70	1376	20.51	524.85
1350	n.a.	217.18	1378	21.15	572.48
1352	n.a.	229.73	1380	21.70	623.19
1354	10.52	262.87	1382	22.17	677.08
1356	12.67	294.33	1384	22.57	734.21
1358	22.17	305.30	1386	22.92	794.68
1360	34.48	248.87	1388	23.21	858.57
1362	27.46	246.14	1390	23.47	925.94
1364	24.32	362.69	1392	23.69	996.85
1366	17.00	278.32	1394	23.87	1,071.38
1368	16.70	363.10	1396	24.03	1,149.55
1370	17.88	399.42	1398	24.17	1,231.43
1372	18.89	438.42	1400	24.29	1,317.04
1374	19.76	480.19			

Table 2.11 Consumption of Electricity and Natural Gas

Year	Elec.[GWh/a]	Gas[Mrd.m^3/a]	Year	Elec.[GWh/a]	Gas[Mrd.m^3/a]
1368	48.7	47.2	1386	225.9	517.6
1370	58.7	63.1	1388	262.9	656.4
1372	70.4	83.8	1390	304.9	828.1
1374	84.2	110.7	1392	352.5	1,039.2
1376	100.2	145.2	1394	406.1	1,297.7
1378	118.7	189.4	1396	466.5	1,612.4
1380	140.2	245.6	1398	534.0	1,993.9
1382	165.0	316.6	1400	609.5	2,453.8
1384	193.4	405.9			

Table 2.12 Rate of Increase of Electricuty & Gas Consumption

Year	Elec.[%]	Gas[%]	Year	Elec.[%]	Gas[%]
1368-1370	9.77	15.62	1384-1386	8.07	12.92
1370-1372	9.54	15.26	1386-1388	7.88	12.61
1372-1374	9.31	14.90	1388-1390	7.70	12.32
1374-1376	9.09	14.55	1390-1392	7.52	12.03
1376-1378	8.88	14.21	1392-1394	7.34	11.75
1378-1380	8.67	13.87	1394-1396	7.17	11.47
1380-1382	8.47	13.55	1396-1398	7.00	11.20
1382-1384	8.27	13.23	1398-1400	6.84	10.94

Table 2.13 Development of GDP and GDP per Capita

Year C	GDP[Mrd Rs/a]	GDP/pop[Th Rs/a]	Year	GDP[Mrd Rs/a]	GDP/pop[Th Rs/a]
 1338	2,485.7	117.2	1370	10,044.2	175.4
1339	2,707.0	124.1	1371	10,310.1	175.6
1340	2,936.6	130.8	1372	10,576.0	175.8
1341	3,116.6	135.0	1373	10,822.1	175.8
1342	3,286.2	138.4	1374	11,068.1	175.8
1343	3,517.6	144.1	1375	11,325.6	175.8
1344	4,029.3	160.6	1376	11,583.1	175.8
1345	4,411.5	171.1	1377	11,840.7	175.8
1346	4,927.5	185.9	1378	12,098.4	175.8
1347	5,493.7	201.8	1379	12,367.5	175.8
1348	6,179.9	220.9	1380	12,636.6	175.8
1349	6,836.7	238.0	1381	12,917.6	175.8
1350	7,685.0	260.5	1382	13,198.7	175.8
1351	9,033.7	298.3	1383	13,478.8	175.8
1352	9,833.9	316.3	1384	13,758.8	175.8
1353	10,544.0	330.0	1385	14,050.8	175.8
1354	11,043.9	336.5	1386	14,342.8	175.8
1355	12,921.8	383.3	1387	14,632.5	175.8
1356	12,625.5	363.5	1388	14,922.2	175.8
1357	11,310.8	313.5	1389	15,223.7	175.8
1358	10,545.0	277.6	1390	15,525.1	175.8
1359	9,032.3	227.8	1391	15,838.7	
1360	8,894.1	215.8	1392	16,152.3	175.8
1361	10,135.0	236.8	1393	16,462.1	175.8
1362	11,049.6	248.7	1394	16,771.9	175.8
1363	11,187.2	242.1	1395	17,093.6	175.8
 1364	11,379.7	238.0	1396	17,415.3	175.8
1365	10,318.5	209.0	1397	17,731.6	
1366	10,196.4	199.9	1398	18,047.9	
1367	10,410.3	197.6	1399	18,375.7	
1368	9,560.2	175.4	1400	18,703.5	175.8
1369	9,802.2	175.4			

Table 2.14 Consumption of Urban, Rural & Government Expenditure

		_						(Unit:Mrd Rs/a)
	Year	Rural	Urban	Government	Year	Rural	Urban	Government
	1338	972.1	677.2	173.5	1362	2,130.4	4,562.5	1,930.1
	1339	910.2	713.9	184.3	1363	2,192.2	4,879.8	1,810.8
	1340	878.8	749.3	179.9	1364	2,252.4	4,953.5	1,898.1
	1341	873.0	787.0	183.4	1365	2,143.1	4,316.5	1,507.6
	1342	849.6	827.1	197.7	1366	2,026.5	4,048.1	1,402.8
	1343	746.1	867.8	238.9	1367	1,893.1	4,226.6	1,396.1
	1344	782.6	906.2	317.9	1368	2,052.1	4,246.0	1,189.4
	1345	881.4	949.3	362.3	1370	2,126.1	4,657.8	1,229.2
	1346	963.0	1,049.7	418.2	1372	2,463.9	4,941.7	1,151.3
	1347	882.1	1,143.3	494.3	1374	2,543.1	5,302.3	1,089.2
	1348	812.3	1,365.6	588.6	1376	2,624.1	5,653.4	1,039.8
	1349	846.7	1,573.7	682.2	1378	2,799.1	5,962.5	1,000.5
	1350	955.7	1,814.1	898.9	1380	3,065.1	6,285.4	969.1
	1351	903.6	2,046.5	1,127.3	1382	3,361.0	6,622.8	944.2
	1352	999.1	2,352.6	1,236.5	1384	3,631.5	6,960.5	924.3
	1353	1,535.0	2,164.2	1,756.4	1386	3,861.9	7,405.3	908.4
•	1354	1,760.4	3,158.8	2,145.9	1388	4,164.7	7,759.6	895.8
	1355	1,621.2	3,297.3	2,379.4	1390	4,506.0	8,127.4	885.8
	1356	1,813.1	3,449.5	2,307.1	1392	4,881.6	8,509.3	877.7
	1357	1,909.5	3,492.5	2,346.9	1394	5,249.3	8,888.0	871.3
	1358	2,041.0	3,548.7	2,177.3	1396	5,402.4	9,528.5	866.3
	1359	2,190.4	3,125.7	1,968.4	1398	5,741.7	9,992.7	862.3
	1360	1,986.1	3,484.8	1,947.9	1400	5,997.7	10,572.2	858.5
	1361	1,935.5	3,922.6	1,910.1				

Table 2.15 Development of Capital Stock & Investment

(Unit:Mrd Rs/a)

Investment	Capital	Year	Investment	Capital	Year
1,747.9	23,038.3	1374	103.7	n.a.	1344
1,799.9	24,301.9	1376	164.7	n.a.	1346
1,877.8	25,594.1	1378	195.5	n.a.	1348
1,973.9	26,947.7	1380	252.5	n.a.	1350
2,061.8	28,340.8	1382	370.1	n.a.	1352
2,189.4	29,846.9	1384	2,453.0	n.a.	1354
2,282.7	31,388.2	1386	3,231.0	n.a.	1356
2,404.6	33,016.9	1388	1,815.8	n.a.	1358
2,509.2	34,690.7	1390	1,724.2	n.a.	1360
2,602.2	36,382.7	1392	2,551.1	n.a.	1362
2,713.3	38,126.3	1394	2,153.3	n.a.	1364
2,813.8	39,895.9	1396	1,360.6	n.a.	1366
2,904.1	41,669.1	1398	1,216.8	18,613.1	1368
3,002.8	43,461.8	1400	1,851.1	20,401.9	1370
			1,711.8	21,750.7	1372

Table 2.16 Import of Consumer, Intermediate & Capital Goods

(Unit:Mrd \$/a) INT CAPINT CAP Year CON Year CON 1338 0.16 0.27 0.11 1370 2.20 6.36 4,93 0.33 7.31 4.84 1340 0.16 0.13 1372 2.21 5.09 8.16 0.12 0.29 0.10 1374 2.23 1342 0.52 0.22 9.06 5.38 1344 0.16 1376 2,26 9.89 5.73 0.15 0.71 0.33 1378 2.30 1346 0.17 0.99 0.39 1380 2.35 10.68 6.12 1348 1350 0.24 1.34 0.48 1382 2.41 11.51 6.50 0.91 12.35 6.97 0.56 2.27 1384 2.46 1352 2.00 6.21 3.49 2.52 13.25 7.38 1354 1386 4.02 2.58 14.15 7.85 2.70 7.91 1388 1356 15.10 8.30 1358 2.56 5.30 1.84 1390 2.63 16.11 8.74 8.23 2.15 1392 2.69 1360 3.14 2.91 10.84 4.35 1394 2.75 17.14 9.23 1362 1364 1.58 7.41 2.42 1396 2.81 18.22 9.70 1366 1.66 5.50 2,21 1398 2.87 19.33 10.17 20.51 10.66 2.34 7.55 2.92 1400 2.93 1368

**Table 2.17 Export of Non-oil goods** 

(Unit:Mrd Rs/a)

				(Unit:Mid Ks/a)
	Year	Non-oil goods	Year	Non-oil goods
~	1338	80.4	1370	132.1
٠	1340	77.5	1372	134.0
	1342	75.9	1374	136.0
	1344	93.3	1376	137.9
	1346	89.1	1378	140.7
	1348	112.1	1380	144.5
	1350	160.5	1382	148.4
	1352	151.5	1384	152.4
	1354	129,5	1386	156.6
	1356	101.6	1388	160.8
	1358	102.0	1390	165.2
•	1360	31.6	1392	169.8
	1362	28.5	1394	174.4
	1364	31.5	1396	179.1
	1366	24.4	1398	183.9
	1368	113.0	1400	188.8

Table 2.18 Shadow Price of Foreign Exchange Reserves and Oil

			0		
Poil[\$/bl]	SFX[Rs/\$]	Year	Poil[\$/bl]	SFX[Rs/\$]	Year
35.0	404.0	1386	39.2	259.5	1370
34.9	426.9	1388	26.6	274.3	1372
33.8	451.2	1390	28.2	289.9	1374
37.0	476.9	1392	29.6	306.4	1376
35.3	504.0	1394	30.8	323.8	1378
32.8	532.6	1396	32.0	342.2	1380
33.0	562.9	1398	31.1	361.7	1382
20.7	1,041.4	1400	31.8	382.2	1384

Table 2.19 Crude Oil Price in the World Market

(Unit:\$/bl) POIL 3 POLI 4 POIL 1 POIL 2 Year Reference 10.28 10.28 10.28 10.28 1353 10.28 10.52 10.52 10.52 10.52 10.52 1354 11.29 11.29 1355 11.29 11.29 11,29 12.67 12.67 12.67 12.67 12.67 1356 12.65 12.65 1357 12.65 12.65 12.65 22.17 22.17 22.17 22.17 22.17 1358 35.46 35.46 35.46 35.46 35.46 1359 34.48 34.48 34.48 34.48 1360 34.48 28.75 28.75 28.75 28.75 28.75 1361 27.46 27.46 27.46 27.46 1362 27.46 26.73 26.73 26.73 1363 26.73 26.73 24.32 24.32 24.32 24.32 1364 24.32 12.88 12.88 12.88 12.88 1365 12.88 17.00 17.00 17.00 1366 17.00 17.00 14.09 14.09 14.09 14.09 1367 14.09 16.70 16.70 16.70 16.70 16.70 1368 18.69 20.46 23.45 17.88 1370 19.30 27.72 18.89 23.45 21.54 20.46 1372 25.83 30.40 19.76 1374 23.45 22.05 20.51 27.72 32.10 25.10 23.45 1376 21.15 24.71 29.21 33.17 1378 26.51 21.70 30.40 33.85 25.83 1380 27.72 22.17 28.75 26.83 31.35 34.27 1382 34.54 22.57 29.64 27.72 32.10 1384 22.92 28.51 32.70 34.71 1386 30.40 34.82 23.21 29.21 33.17 1388 31.06 29.84 33.55 34.89 23.47 1390 31.62 23.69 33.85 34.93 30.40 1392 32.10 30.90 34.08 34.95 23.87 1394 32.51 34.27 34.97 24.03 1396 32.87 31.35 31.75 34,42 34.98 24.17 33.17 1398 34.99 34,54 24.29 32.10 1400 33.43

Table 2.20 Development of GDP for Diff. Scenarios of Oil Prices

	Year	Reference	POIL_1	POIL_2	POIL_3	it:Mrd Rs/a) POIL_4
· · · · · · · · · · · · · · · · · · ·	1338	2,485.7	2,485.7	2,485.7	2,485.7	2,485.7
	1339	2,463.7	2,707.0	2,707.0	2,707.0	2,707.0
	1340	2,707.6	2,936.6	2,936.6	2,936.6	2,936.6
	1340	3,116.6	3,116.6	3,116.6	3,116.6	3,116.6
		3,110.0	3,286.2	3,286.2	3,286.2	3,286.2
	1342 1343		3,517.6	3,517.6	3,517.6	3,517.6
		3,517.6	4,029.3	4,029.3	4,029.3	4,029.3
	1344	4,029.3	4,029.5	4,029.3	4,029.3	4,411.5
	1345	4,411.5		4,411.5	4,927.5	4,927.5
	1346	4,927.5 5.403.7	4,927.5			
	1347	5,493.7	5,493.7	5,493.7	5,493.7	5,493.7
	1348	6,179.9	6,179.9	6,179.9	6,179.9	6,179.9
	1349	6,836.7	6,836.7	6,836.7	6,836.7	6,836.7
	1350	7,685.0	7,685.0	7,685.0	7,685.0	7,685.0
	1351	9,033.7	9,033.7	9,033.7	9,033.7	9,033.7
	1352	9,833.9	9,833.9	9,833.9	9,833.9	9,833.9
	1353	10,544.0	10,544.0	10,544.0	10,544.0	10,544.0
	1354	11,043.9	11,043.9	11,043.9	11,043.9	11,043.9
	1355	12,921.8	12,921.8	12,921.8	12,921.8	12,921.8
	1356	12,625.5	12,625.5	12,625.5	12,625.5	12,625.5
	1357	11,310.8	11,310.8	11,310.8	11,310.8	11,310.8
	1358	10,545.0	10,545.0	10,545.0	10,545.0	10,545.0
	1359	9,032.3	9,032.3	9,032.3	9,032.3	9,032.3
	1360	8,894.1	8,894.1	8,894.1	8,894.1	8,894.1
	1361	10,135.0	10,135.0	10,135.0	10,135.0	10,135.0
	1362	11,049.6	11,049.6	11,049.6	11,049.6	11,049.6
	1363	11,187.2	11,187.2	11,187.2	11,187.2	11,187.2
	1364	11,379.7	11,379.7	11,379.7	11,379.7	11,379.7
	1365	10,318.5	10,318.5	10,318.5	10,318.5	10,318.5
	1366	10,196.4	10,196.4	10,196.4	10,196.4	10,196.4
	1367	10,410.3	10,410.3	10,410.3	10,410.3	10,410.3
-	1368	10,845.5	10,845.5	10,845.5	10,845.5	10,845.5
	1370	11,137.3	10,348.3	11,129.3	11,108.7	9,562.2
	1372	12,915.5	12,271.4	13,097.6	13,303.7	10,927.3
	1374	15,292.3	14,582.2	15,962.8	16,485.4	12,682.4
	1376	16,420.9	15,459.4	17,961.2	19,499.0	13,227.6
	1378	17,177.5	16,150.8	18,884.6	21,568.2	13,734.4
	1380	17,894.8	16,778.7	19,920.1	23,148.3	14,192.1
	1382	18,887.0	17,574.6	21,059.1	24,795.3	14,721.2
	1384	19,782.6	18,443.7	22,790.1	25,881.4	15,265.1
	1386	21,119.7	19,315.8	23,930.9	26,710.7	15,814.1
	1388	22,377.2	20,683.1	24,677.7	27,438.6	16,361.6
	1390	23,213.6	21,731.3	25,334.4	28,227.0	17,073.5
	1392	23,825.0	22,434.5	25,982.7	29,144.4	17,744.3
	1394	22,638.0	21,350.8	24,816.6	28,398.0	16,987.1
	1396	22,802.7	21,438.5	25,463.7	30,226.8	17,447.7
	1398	23,075.8	21,687.6	26,413.6	34,317.4	17,969.0
	1400	23,471.9	22,036.3	28,531.1	44,118.4	18,399.7

**Table 2.21 Scenarios of Domestic Oil Consumption** 

(Unit:Mio.bl/a) Year Reference DOIL 1 DOIL 2 363.1 1368 363.1 363.1 1370 398.6 397.0 391.1 430.6 1372 435.8 413.9 1374 474.5 463.9 432,1 1376 514.8 496.5 446.5 556.5 528.3 1378 457.7 599.4 1380 559.1 466.5 1382 643.6 588.7 473.2 1384 688.8 617.2 478.3 1386 735.0 644.3 482.3 782.1 670.1 485.3 1388 1390 829.8 694.6 487.6 1392 878.2 717.7 489.4 927.0 739,4 1394 490.7 1396 976.2 759.9 491.7 1398 1,025.6 779.0 492.5 1400 1,075.1 796.8 493.1

Table 2.22 Shadow Prices of Crude Oil for Diff. Scenario of Domestic Oil Consumption

(Unit:\$/bl) DOIL 1 DOIL 2 Year Reference 1370 4.2 1.1 5.3 4.8 1.3 1372 6.1 1374 6.9 5.4 1.4 7.9 6.2 1.6 1376 1378 9.1 7.1 1.9 1380 10.4 8.2 2.2 9.4 2.5 1382 11.9 1384 13.6 10.7 2.8 15.6 12.3 3.2 1386 1388 17.9 14.0 3.7 4.2 20.5 16.1 1390 18.4 1392 23.4 4.8 5.5 1394 26.8 21.1 1396 24.1 30.7 6.4 1398 35.2 27.6 7.3 40.6 31.9 8.4 1400

Table 2.23 Shadow Prices of Foreign Exch. Res. for Diff. Scen. of Domes.
Oil Consumption

				(Unit:RS/\$)
******	Year	Reference	DOIL_1	DOIL_2
	1370	238.8	225.7	215.7
	1372	252.4	238.6	228.0
	1374	266.8	252.1	240.9
	1376	281.9	266.5	254.6
	1378	298.0	281.6	269.1
	1380	314.9	297.6	284.4
	1382	332.8	314.5	300.6
	1384	351.7	332.4	317.7
	1386	371.7	351.3	335.7
	1388	392.9	371.3	354.8
	1390	415.2	392.4	375.0
	1392	438.8	414.7	396.3
	1394	463.8	438.3	418.8
	1396	490.1	463.2	442.6
	1398	518.0	489.6	467.8
	1400	543.1	513.3	490.5

Table 3.1 Final energy uses per unit real exp. in rural and urban hous.

(Unit:BOE/Mio.Rs)

	(Onicidor)		
Year	Urban	Rural	
1361	9.43	17.26	
1362	9.13	16.14	
1363	9.83	16.14	
1364	10.11	16.39	
1365	11.75	17.12	
1366	13.01	17.27	
1367	14.34	18.43	
1368	14.82	17.22	
1369	14.63	15.95	

Table 3.2 Share of final energy consumption in rural and urban areas

	en e	(%)
Year	Urban	Rural
1361	52.11	47.89
1362	54.68	45.32
1363	57.42	42.58
1364	57.59	42.41
1365	58.47	41.53
1366	60.92	39.08
1367	63.18	36.82
1368	64.50	35.50
1369	63.14	36.86

Table 3.3 Development of final energy consumption in household

(Unit:MBOE/a)

Year	Elec	N. Gas	Pet. Prod	Trad Fuel
1361	4.94	4.74	40.46	21.94
1362	5 <b>.</b> 56	5.85	44.56	21.77
1363	6.27	7.69	49.72	22.53
1364	6.94	8.27	54.74	21.40
1365	7.59	9.23	53.21	21.11
1366	8.29	10.40	53.49	20.04
1367	8.64	13.68	56.43	21.29
1368	9.58	14.46	62.17	19.58
1369	10.73	16.19	60.36	20.79

Table 3.4 Development of final energy consumption in urban household

(Unit:MBOE/a) Elec N. Gas Pet. Prod Trad Fuel Year 4.02 4.71 24.47 4.36 1361 4.28 5,81 27.91 1362 4.51 32.25 4.71 7.61 1363 4.93 4.53 34.69 1364 5.32 8.06 3.89 5.97 8.93 34.50 1365 3.95 6.05 10.18 36.00 1366 4.72 38.74 6.46 13.29 1367 4.09 1368 7.08 14.04 43.03 7.72 4.26 1369 15.65 40.61

Table 3.5 Development of final energy consump. per Cap. in urban hous.

(Unit:BOE/a)

(0111111202),4)	,				
Trad Fuel	Pet. Prod	N. Gas	Elec	Year	
0.20	1.12	0.22	0.18	1361	
0.19	1.21	0.25	0.20	1362	
0.19	1.32	0.31	0.20	1363	
0.18	1.34	0.31	0.21	1364	
0.15	1.29	0.33	0.22	1365	
0.14	1.28	0.36	0.22	1366	
0.16	1.32	0.45	0.22	1367	
0.13	1.40	0.46	0.23	1368	
0.13	1.27	0.49	0.24	1369	

•			•								
Table 3.6 Dev	elopment of en	ergy consumpt	ion of a family	in urban areas	(1361)		<u> </u>				
YEAR	ELEC	N,GAS	LPG	KEROSENE	GAS OIL		CHARCOAL	Total	Elec	N. Gas	Pct, Proc
	(MJ)	(MJ)	(MJ)	(M1)	(MJ)	(MI)	(MJ)	(MJ)	[BOE/a]	[BOE/a]	(BOE/a
G_1	1380.35	68.58	1576.26	13668.84	332,85	620.89	891.53	18539.3	0.225	0.012	2.63
0_2	2114.87	166,18	2847.51	17100.35	440.43	2208.79	586.73	25464.9	0.345	0.028	3.45
G_3	2790.32	987.39	3615,46	18831.24	939.71	2446.11	853,43	30463.7	0.456	0.167	3.95
G_4	3886.36	2133.92	5041.93	20001.99	3032.97	2082.87	1005.83	37185.9	0,635	0.361	4,75
G_5	433B.52	2021.37	5341.90	21880.91	2228.51	2180.93	1280.15	39272.3	0.709	0.342	4.98
0_6	5494,34	4812.08	6053.58	23381.36	2722.52	1523.20	1522.17	45509.2	0,897	0.814	5.44
G_7	6729.75	7297.69	6860.72	26156.84	2456.41	4307.90	2419,14	56228.5	1.099	1.235	6.000
G_8	8338.34	12661.06	7171,16	27233.39	3908.13	7841.14	<b>2995.7</b> 2	70148.9	1.362	2,142	6.486
6_9	10703.83	22508.54	9313.20	29268.75	23587.91	5261.28	2177,12	103120.6	1.748	3.808	10.574
G_10	14600.28	31652.64	8575.91	36838.25	8914.05	35915.03	6785.36	143281.5	2.385	5.355	9,197
Table 3.7 Dev	elanment of en	erov consumnit	ion of a Camils	in urban arcas	(1363)						
YEAR	ELEC	N.GAS	120	KEROSENE	GAS OIL	F.WOOD	CHARCOAL	Total	Elco	N, Gas	Pct, Prod
	(MJ)	(M1)	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)	[BOF/a]	[BOE/a]	[BOE/a
G_1	1374.23	133.32	1749.26	15169.05	369.38	552.74	793.68	20141.7	0.224	0.023	2,926
G_2	2095.39	301.33	3160.04	18977.18	488.77	1966.36	522.34	27511.4	0.342	0.051	3.830
0_3	2766.21	922.19	4012.27	20898.05	1042.85	2177.64	759.76	32579.0	0.452	0.156	4.393
G_4	3869.18	1921.20	5595.31	22197.29	3365.86	1854.26	895.44	39698.5	0.632	0.325	n.a
G_5	4347.64	2412.54	5928.19	24282.43	2473.10	1941,57	1139.65	42525.1	0.710	0.408	n,a.
G_6	5534.77	6372.88	6717.98	25947.55	3021.33	1356.02	1355.11	50305.6	0.904	1.078	n.a.
G_7	6771.59	9614.57	7613.72	29027.66	2726.02	3835.09	2153.63	61742.3	1,106	1.627	па
G_8	8388.44	14033.32	7958.23	30222.37	4337.07	6980.55	2666.93	74586.9	1.370	2.374	n,a.
G_9	10768.56	27449.92	10335.36	32481.11	26509.70	4683.83	1938.17	114166.7	1.759	4.644	n.a.
G_10	14687.70	40923.29	9517.15	40881.40	9892.41	31973.21	6040.64	153915.8	2.399	6.924	n.a.
T-11. 10 D	.1		ion of a family	in urban areas	(1366)			•			
YEAR	ELEC	N,GAS	1.PG	KEROSENE	GAS OIL	F.WOOD	CHARCOAL	Total	Elec	N. Gas	Pet. Prod
	(MI)	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)	[BOE/a]	[BOE/a]	[BOE/a]
G_1	1681.68	211.83	1885.55	16350.94	398.16	499.06	716.59	21743.8	0.275	0.036	n.a.
G_2	2653.28	537.53	3406.25	20455.78	526.86	1775.38	471.61	29826.7	0.433	0.091	n.a.
G_3	3542,15	1786.05	4324.89	22526.30	1124.10	1966.14	685.97	35955.6	0.579	0.302	n.a.
G_4	4907.03	3571.55	6031.26	23926,78	3628.10	1674.17	808.47	44547.4	0.801	0.604	п.а.
 G_5	5475.88	4585.93	6390.08	26174.38	2665.79	1752.99	1028.96	48074.0	0.894	0.776	n.a.
G_6	6957.75	13109,42	7241.41	27969.24	3256.73	1224.32	1223.49	60982.4	1.136	2.218	n,a.
G_7	8508.57	17340.00	8206.93	31289.33	2938.41	3462.61	1944.46	73690.3	1.390	2.934	n.a.
G_8	10565.62	23900.14	8578.29	32577.12	4674.98	6302.56	2407.90	89006.6	1.726	4.043	8.8.
0.9	13571.11	33976.63	11140.63	35011.85	28575.19	4228.91	1749.93	128254.2	2.217	5.748	n.a.
G_10	18511.30	46300.26	10258.67	44066.64	10663.17	28867.79	5453.94	164121.8	3.024	7.833	n.a.
		·	e . e		(12(0)			4 * · · · · · · · · · · · · · · · · · ·			
YEAR	ELEC	N,GAS	1PG	in urban areas KEROSENE	GAS OIL	F.WOOD	CHARCOAL	Total	Elec	N. Gas	Pct. Prod
	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)	[BOE/a]	[BOE/s]	[BOE/a]
G_1	2030.78	428.93	1944.04	16358.09	410.51	476.02	683.52	22831.9	0.332	0.073	n.a.
6_2	3158.58	861.57	3511.90	21090.25	\$43.20	1693.43	449.84	31308.8	0.516	0.146	n.a.
G_3	4170.36	3470.13	4459.03	23225.00	1158.96	1875.38	654.31	39013.2	0.681	0.587	n.a.
G_4	5802.05	6425.44	6218.33	24668.91	3740.64	1596.89	771,15	49223.4	0.948	1.087	n.a.
0_5	6507.28	6500.58	6588.28	26986.22	2748.48	1672.07	981,46	51984.4	1.063	1.100	n.a.
6_6	8272.07	17091.15	7466.02	28836.75	3357.74	1167.80	1167.01	67358.6	1,351	2.892	n.a.
G_7	10121.81	22800.62	B461.49	32259.82	3029.55	3302.77	1854.70	81830.8	1.653	3.857	n,a.
G_8	12598.09	33252.36	8844,36	33587.56	4819.99	6011.63	2296.75	101410.7	2.058	5.626	n.a.
G_9	16173.62	54871.87	11486.18	36097.81	29461.50	4033.70	1669.15	153793.8	2.642	9.283	n.a.
		74774.4	10576.86	45433,45	10993.90	27535.24	5202.18	196577.2	3.603	12.651	п.а.
G_10	22061.19	14/14.4	10370.00	~JJJ,**J	10,73,70	2,000,00	JAUF. 10				

YEAR	ELEC	N.GAS	LPG	y in rural areas(1 KEROSENE	GAS OIL
	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)
G_1	349,20	6.79	545.99	10864.76	82.11
G_2	579.25	13.58	1333.73	15557.85	116.37
G_3	949.29	20.37	2147.47	19443.53	240.20
G_4	1344.51	33.95	2658.14	20896.88	407.50
G_5	1639.13	47.53	3222.76	20488.12	292.01
G_6	2125.81	67.91	4055.12	25288.87	936.20
G_7	2833.18	108.65	5187.45	28242.66	1991.83
G_8	3215.19	156.18	6025.64	30471.46	2024.32
G_9	4553.40	190.14	6691.92	27638.78	6876.12
G_10	5326.93	448.18	7755.57	33874.37	7447.85

YEAR	ELEC	N.GAS	LPG	KEROSENE	GAS OIL
	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)
G_1	436.87	15.40	561.72	11164.57	84.48
G_2	698.71	30.79	1372.16	15987.17	119.72
G 3	1216.08	46.19	2209.34	19980.07	247.12
G 4	1759.48	76.98	2734.73	21473.52	419.24
	2045.32	107.77	3315.61	21053.49	300.43
G 6	2884.48	153.95	4171.96	25986.72	963.17
G_7	4003.57	246.33	5336.92	29022.01	2049.22
G 8	4396.70	354.10	6199.25	31312.32	2082.65
G 9	6607.66	431.07	6884.73	28401.47	7074.24
G 10	7321.61	1016.10	7979.02	34809.13	7662.44

YEAR	ELEC	N.GAS	LPG	KEROSENE	GAS OII
	(MJ)	(MJ)	(MJ)	(MJ)	(M)
G_1	636.99	49.00	579.48	11465.53	n.a
G_2	1138.55	98.00	1415.55	16418.12	n.a
G_3	2021.87	147.00	2279.21	20518.66	л.а
G_4	3218.27	245.00	2821.21	22052.37	п.а
G_5	3806.53	343.01	3420.46	21621.01	n.a
G_6	5234.70	490.01	4303.89	26687.22	n.a
G_7	7413.12	784.01	5505.68	29804.33	n.a
G_8	8235.80	1127.02	6395.29	32156.37	n.a
G_9	12871.33	1372.02	7102.45	29167.06	n.a
G 10	14523.55	3234.05	8231.34	35747.45	n.;

YEAR	ELEC	N.GAS	LPG	KEROSENE	GAS OIL
	(MJ)	(MJ)	(MJ)	(MJ)	(MJ)
G_1	739.53	95.44	599.56	11792.50	n.a.
G_2	1256.82	190.88	1464.60	16886.33	n.a.
G_3	2255.68	286.32	2358.20	21103.81	n.a.
G_4	3353.05	477.20	2918.98	22681.25	n.a.
G5	4164.05	668.08	3539.00	22237.60	n.a.
G_6	6155.33	954.40	4453.05	27448.28	n.a.
G_7	8918.66	1527.04	5696.49	30654.29	n.a.
G_8	10120.21	2195.12	6616.93	33073.41	n.a.
G_9	15723.03	2672.32	7348.59	29998.85	n,a.
G 10	17741.30	6299.0	8516.61	36766.89	n.a.

Table 3.14 Development of useful energy consumption of

a family in urban areas(1361)						
YEAR	Elect.(GI)	Heating(GJ)	Cooking(GJ)			
G_1	1.38	5.59	1.69			
G_2	2.11	7.23	2.43			
G_3	2.79	8.75	2.92			
G_4	3.89	11.25	3.63			
G_5	4.34	11.37	3.90			
G_6	5,49	13.76	4.49			
G_7	6.73	16,55	5.29			
G_8	8.34	21.59	5.98			
G_9	10.70	41.36	7.55			
G_10	14.60	44.20	9.33			

Table 3.16 Development of useful energy consumption of

	family in urban ar	ear(1366)	
YEAR	Elect.(GJ)	Heating(GI)	Cooking(GJ)
G 1	1.68	6.68	2.00
G_2	2.65	8.67	2.90
G_3	3.54	10.62	3.50
G 4	4.91	13,86	4.38
G 5	5.48	14.63	4.77
G 6	6.96	20.43	5.86
G_7	8.51	24,25	6,86
G 8	10.57	30.12	7.66
G 9	13.57	53.01	9.46
G_10	18.51	55.08	11.37

Table 3.18 Development of useful energy consumption of a family

	in rural areas(1361)	2.5	
YEAR	Elect.(GJ)	Heating(GJ)	Cooking(GI)
G_1	0,35	6.52	0.93
G_2	0.58	10.26	1.65
G_3	0.95	13.01	2.23
G_4	1.34	13.83	2.47
G_5	1.64	14.24	2.78
G_6	2.13	18.08	3.49
G_7	2.83	20.41	4.06
G_8	3.22	22.27	4.57
G_9	4.55	24.71	4.99
G_10	5.33	28.44	5.59

Table 3.20 Development of useful energy consumption of a family

rural areas(1366)		
Elect.(GJ)	Heating(GI)	Cooking(GJ)
0,64	6.70	0.95
1.14	10.42	1.67
2.02	13.21	2.26
3.22	14.11	2,52
3.81	14.47	2.83
5,23	18.40	3.55
7.41	20.94	4.16
8.24	22.91	4.69
12.87	26.25	5.18
14.52	29.34	5.72
	Elect.(GJ)  0.64  1.14  2.02  3.22  3.81  5.23  7.41  8.24  12.87	Elect.(GI) Heating(GI)  0.64 6.70  1.14 10.42  2.02 13.21  3.22 14.11  3.81 14.47  5.23 18.40  7.41 20.94  8.24 22.91  12.87 26.25

Table 3.15 Development of useful energy consumption of

វា	family in urban ar			
YEAR	Elect.(GI)	Heating(GJ)	Cooking(GJ)	
G_1	1,37	6.19	1.86	
G_2	2,10	7.99	2.68	
G_3	2.77	9.51	3.21	
G_4	3,87	12,14	3.97	
G_5	4.35	12.61	4.31	
G_6	5,53	15.77	5.03	
G_7	6.77	19.01	5.92	
G_8	8.39	23.61	6.55	
G_9	10.77	47.05	8.51	
G_10	14.69	50.89	10.55	

Table 3.17 Development of useful energy consumption of

YEAR	Elect.(GI)	Heating(GJ)	Cooking(GJ)
G 1	2.03	6.99	2.07
G_2 -	3.16	9.09	3,00
G_3	4.17	11.83	3.73
G_4	5.80	15.80	4.71
G_5	6.51	16.05	5.04
G_6	8.27	23.04	6.29
G_7	10,12	27.70	7.43
G_8	12,60	35.78	8.51
G_9	16.17	65.70	11.20
G 10	22.06	71.53	13.66

Table 3.19 Development of useful energy consumption of a family

Elect.(GJ)	Heating(GI)	Cooking(GJ)
		Comageos
0.44	6.60	0.94
0.70	10.32	1.65
1.22	13.09	2.24
1.76	13.94	2.49
2.05	14.31	2.80
2.88	18.18	3.51
4.00	20.57	4,09
4.40	22,45	4.61
6.61	25.08	5.03
7.32	28.72	5.63
	0.70 1.22 1.76 2.05 2.88 4.00 4.40 6.61	0.70     10.32       1.22     13.09       1.76     13.94       2.05     14.31       2.88     18.18       4.00     20.57       4.40     22.45       6.61     25.08

Table 3.21 Development of useful energy consumption of a family

i i	in rural areas(1369)					
YEAR	Elect.(GJ)	Heating(GJ)	Cooking(GJ)			
G_1	0.74	6.80	0.96			
G_2	1.26	10.52	1.68			
G_3	2.26	13.35	2.29			
G_4	3.35	14.32	2.56			
G_5	4.16	14.67	2.87			
G_6	6,16	18.68	3.60			
G_7	8.92	21.41	4.24			
G_8	10.12	23.53	4.79			
G_9	15.72	27.85	5.38			
G_10	17.74	30.16	5.85			

Table 3.22 Value-added of industry and GDP in constant prices of 1361

(Unit:Mrd.Rs/a) Year Industry **GDP** Year Industry **GDP** 1338 97.3 2,177.6 1354 806.8 9,227.8 1339 107.9 2.384.4 1355 1,049.1 11,254,3 1340 2,598.6 1,101.3 116.8 1356 11,183,8 1341 135,7 2,778.6 1357 986.2 10,070.8 1342 149.0 2,936.9 1358 859.1 10,543.1 1343 157.9 3,158.7 1359 964,8 9,323.1 1344 178.0 3,621.6 1360 1.042.3 9,175,2 1345 206.4 3,992,8 1361 996.7 10,335.4 1346 237.4 4,440.3 1362 1.115.3 11,536.7 1347 273.5 5,001.7 1363 1,252,3 11,587.1 1348 309.6 5,653,3 1364 1,225,9 11,607,4 1349 338.5 6,252,3 1365 1,148.0 9,861.7 1350 397,7 7,045.5 1366 1,275.6 10,019.8 1351 470,4 8,201.9 1367 1,301.8 9,234,3 1352 561.8 8,956,3 1368 1,417.9 9,514.6 1353 745,7 9,342.7 1369 1,643.8 10,664.9

Table 3.23 Share of ind. value-added in GDP and GRP at constant prices(1361)

(Unit: %) Year IND/GDP IND/GRP Year IND/GDP IND/GRP 1338 4,468 7,528 1354 8.743 16,207 1339 4.525 7,692 1355 9.322 16.207 1340 4.495 8.046 1356 9.847 16,254 1341 4.884 9.038 1357 9.793 14,237 1342 5.074 9,470 1358 8.148 10.728 1343 4.999 9,492 1359 10,348 11,408 1344 4.915 9.424 1360 11.360 12.569 1345 5.169 10.168 1361 9.644 11.883 1346 5.346 10.561 1362 9.667 11.703 1347 5,468 11.109 1363 10.808 12,571 1348 5.476 11,793 1364 10,561 12.305 1349 5.414 11,857 1365 11.641 13,572 1350 5.645 12.532 1366 12.731 15,148 1351 5.735 12.346 1367 14.097 17,403 1352 6.273 13,508 1368 14,902 18,595 1353 7.982 16,510 1369 15,413 19.569

Table 3.24 Energy consumption in total of Large industry

Year	Elec.(Mio. kWh/a) Energy	(Mio. BOE)	Year	Elec.(Mio. kWh/a) Energy	(Mio, BOE)
1350	1452.66	14.06	1360	2398.10	n.a.
1351	1647,56	14.84	1361	2679.38	34.60
1352	2367.64	16.03	1362	2962,61	40.71
1353	4815.28	20,29	1363	3334.69	43.80
1354	4996.07	22.65	1364	2987,55	41.96
1355	5318.53	25.10	1365	3110.03	45.86
1356	n,a.	n,a,	1366	3970,14	46.44
1357	n,a.	n.a.	1367	5467,09	58.10
1358	2180.49	n.a.	1368	6385,02	70.59
1359	2448.95	n.a.	1369	8330,72	67.73

Table 3.25 Share of industry in energy consumption

Year	Energy(%)	Electricity(%)	Year	Energy(%)	Electricity(%)
1350	22.7	45.0	1361	22.7	29.8
1351	24.2	48.0	1362	20.8	31.0
1352	24.2	51.9	1363	19.9	30.6
1353	24.7	54.6	1364	18.3	28.7
1354	24.7	50.6	1365	17.8	26.7
1355	31.6	47,5	1366	17.9	20.8
1356	23.3	45.1	1367	17.9	21,7
1357	20.5	41.2	1368	19,5	21.2
1358	22,3	38.4	1369	19.2	22.7
1359	22,5	35.9	1370	19.6	21.6
1360	22.7	34.7			

Table 3.26 Share of energy carriers in energy consumption of industry

Year	Elec	N. Gas	Others	Pet. Prod
1350	6,06	0.00	0.00	93.94
1351	6.52	0.00	0.00	93.48
1352	8.67	0.00	0.00	91.33
1353	13.93	0.00	2.11	83.96
1354	12.94	0.00	2.29	84.76
1355	12.43	0.00	2.51	85.05
1356	n.a.	n.a.	n.a.	n.a.
1357	n.a.	n.a.	n.a.	n.a.
1358	n.a.	n.a.	n.a.	n.a.
1359	n.a.	n.a.	n.a.	n.a.
1360	n.a.	n.a.	n.a.	n.a.
1361	4.54	20.49	0.57	74.40
1362	4.27	27.96	0.47	67.30
1363	4,47	29.24	0.24	66.05
1364	4.18	31.18	0.47	64.18
1365	3.98	30.04	0.44	65.54
1366	5.02	30.36	0.00	64.63
1367	5.52	25.63	0.00	68.84
1368	5.31	29.25	0.00	65.44
1369	7.22	32.69	0.00	60.09

Table 3.30 Activity level of passenger transport modes

(Unit:Mio. p-km)

Year	Mini-Bus	Bus	M. Cycle	Train_Diesel	Air (Dom)
1349<	9,078	10,936	865	1,782	n.a.
1350	10,136	12,210	995	1,772	n.a.
1351	11,506	13,862	1,080	2,034	n.a.
1352	12,900	15,541	1,165	2,167	n.a.
1353	14,315	17,245	1,239	2,244	n.a.
1354	15,838	19,080	1,220	2,805	1,272
1355	18,151	21,867	1,278	3,476	1,490
1356	20,989	25,286	1,149	3,636	1,763
1357	22,549	27,165	1,139	2,951	1,630
1358	23,714	28,569	942	3,168	1,581
1359	24,978	30,091	1,430	2,677	1,170
1360	26,786	32,269	2,098	2,501	1,867
1361	27,966	33,690	2,167	4,687	2,085
1362	30,953	37,289	2,155	5,726	3,334
1363	34,932	42,083	2,190	6,069	4,107
1364	39,023	47,011	2,160	5,529	4,035
1365	40,737	49,076	2,083	4,592	4,695
1366	41,452	49,938	1,944	3,637	4,792
1367	41,315	49,772	1,684	4,614	4,194
1368	41,690	50,225	1,467	4,705	4,713
1369	41,911	50,490	1,227	4,528	5,700
1370	44,814	53,988	1,111	n.a.	5,369

Table 3.31 Activity of modes in Freight transportation

(Unit:Mio. t-km)

Air(Dom)	Train_Diesel	L.Truck	S.Truck	Year
n.a.	2,330	12,623	1,114	1349
n.a.	3,006	14,196	1,253	1350
n.a.	3,692	15,876	1,401	1351
n,a.	4,388	17,677	1,560	1352
n.a.	4,917	20,221	1,784	1353
134	4,943	27,715	2,445	
163	4,877	35,563	•	1354
199	5,017	•	3,138	1355
		46,569	4,109	1356
178	4,083	54,396	4,800	1357
174	3,124	57,995	5,117	1358
123	3,428	61,529	5,429	1359
217	3,861	63,735	5,624	1360
245	5,567	66,189	5,840	1361
398	6,762	76,275	6,730	1362
475	7,566	87,338	7,706	1363
410	6,888	98,539	8,695	1364
485	7,316	100,717	8,887	1365
582	8,625	101,037	8,915	1366
502	8,047	98,306	8,674	1367
533	7,963	95,020	8,384	1368
639	9,041	92,951	8,202	1369
526	n.a.	96,401	8,506	1370

Table 3.32 Fuel Consumption in Road Transport Sector

Otto Engine		·			(	Unit:MBOE/a)
Year	Car Tr.	MC.Tr	Mini-Bus Tr.	Bus Tr.	S.Truck Tr.	L.Truck Tr.
1349<	4.65	0.24	0.84	0.79	1.15	4.96
1350	5.42	0.27	0.94	0.88	1.29	5.58
1351	6.49	0.30	1.07	1.00	1.45	6.24
1352	7.71	0.32	1.19	1.12	1.61	6,95
1353	9.65	0.34	1.32	1.24	1.84	7.95
1354	12.61	0.34	1.46	1.37	2.53	10.90
1355	15.66	0.35	1.67	1.57	3.24	13.98
1356	19.32	0.31	1.93	1.82	4.20	18.27
1357	20.41	0.31	2.07	1.95	4.88	21,32
1358	21.57	0.25	2.17	2,05	5.19	22.71
1359	22,69	0.37	2.28	2.16	5.49	24.07
1360	22.95	0.54	2.44	2.32	5.67	24.91
1361	23.20	0.55	2.55	2.42	5.88	25,84
1362	23.89	0.54	2.81	2.67	6.74	29.67
1363	24.65	0.55	3.16	3.01	7.69	33.84
1364	25.07	0.53	3.51	3.35	8.61	38.05
1365	24.25	0.51	3.64	3.49	8.76	38.79
1366	23.26	0.47	3.70	3,55	8.75	38.83
1367	22.11	0.40	3.68	3.54	8.50	37.72
1368	20.92	0.35	3.70	3.56	8.20	36.42
1369	19.10	0.29	3.71	3.58	8.00	35.56
1370	18.04	0.25	3.94	3.81	8.26	36.76

Table 3.33 Final energy intensity in passenger transportation modes

(Unit:kJ/p-km)

Year	Car (Otto)	Car(Diesel)	Taxi	Mini-Bus	Bus	Train_Elec	Train_Diesel
1349<	1,681	1,716	2,052	548	426	290	446
1350	1,680	1,715	2,050	548	426	290	413
1351	1,678	1,713	2,048	548	426	290	354
1352	1,676	1,711	2,046	547	426	290	350
1353	1,675	1,710	2,044	547	426	290	334
1354	1,673	1,708	2,042	546	426	290	352
1355	1,672	1,707	2,041	545	426	290	380
1356	1,671	1,706	2,040	543	425	290	337
1357	1,623	1,657	1,981	542	425	290	375
1358	1,619	1,653	1,976	541	425	290	407
1359	1,610	1,643	1,965	540	425	290.	364
1360	1,578	1,611	1,926	539	425	290	382
1361	1,570	1,603	1,916	538	425	290	331
1362	1,570	1,603	1,916	537	424	290	268
1363	1,558	1,591	1,902	535	423	290	264
1364	1,564	1,597	1,909	531	422	290	318
1365	1,562	1,595	1,907	529	421	290	271
1366	1,559	1,591	1,903	527	420	290	293
1367	1,558	1,590	1,901	527	420	290	290
1368	1,559	1,591	1,903	525	419	290	290
1369	1,515	1,547	1,849	524	419	290	347
1370	1,491	1,522	1,820	520	417	n.a.	n.a.

Table 3.34 Final energy intensity in transportation sector

(Unit:kJ/t-km)

	4.5	* .		(Unit:kJ/t-km)
Year	S.Truck	L,Truck	Train_Dicscl	Total
1349<	6,109	2,325	883	2,378
1350	6,109	2,325	818	2,659
1351	6,109	2,325	700	2,485
1352	6,109	2,325	692	2,605
1353	6,109	2,325	662	2,647
1354	6,109	2,325	697	2,782
1355	6,097	2,324	753	2,793
1356	6,041	2,320	666	2,882
1357	6,009	2,317	743	2,824
1358	5,993	2,315	805	2,773
1359	5,978	2,313	720	2,646
1360	5,964	2,311	757	2,639
1361	5,949	2,308	655	2,595
1362	5,921	2,300	531	2,427
1363	5,897	2,291	523	2,420
1364	5,856	2,283	629	2,446
1365	5,830	2,277	536	2,428
1366	5,806	2,272	580	2,403
1367	5,794	2,269	575	2,406
1368	5,782	2,266	574	2,398
1369	5,768	2,262	688	2,380
1370	5,743	2,254	n.a.	2,525

Table 3.36 Development of share of expenditure groups in urban population										
Year	1368	1373	1378	1383	1388	1393	1398	1400		
UPOP_1&2	7.46	7.46	7.46	7.46	7.46	7.46	7,46	7.46		
UPOP_3&4	23.31	23.31	23.31	23.31	23.31	23.31	23.31	23,31		
UPOP_5&6	37.07	37.07	37.07	37.07	37.07	37.07	37.07	37.07		
UPOP_7&8	23.99	23.99	23.99	23.99	23.99	23.99	23.99	23.99		
UPOP_9&10	8.17	8.17	8.17	8.17	8.17	8.17	8.17	8.17		

Table 3.37 Development of share of expenditure groups in rural population								(Unit:%)		
Year	1368	1373	1378	1383	1388	1393	1398	1400		
RPOP_1+2	16.36	16.36	16.36	16.36	16.36	16.36	16.36	16.36		
RPOP_3+4	36.15	36.15	36.15	36.15	36.15	36.15	36.15	36.15		
RPOP_5+6	32.58	32.58	32.58	32.58	32.58	32.58	32.58	32.58		
RPOP_7+8	12.59	12.59	12.59	12.59	12.59	12.59	12.59	12.59		
RPOP_9+2	2.31	2.31	2.31	2.31	2.31	2.31	2.31	2.31		

Table 3.38 Development of Real expenditure of Urban & Rural Households

Year						(Unit:	1,000 Rs/C	Capita/a)
	1368	1373	1378	1383	1388	1393	1398	1400
Urban	164.8	164.8	164.8	164.8	164.8	164.8	164.8	164.8
Rural	96.5	96.5	96.5	96.5	96.5	96.5	96.5	96.5

Table 3.39 Development of Demand for Useful Energy in Rural Household

			*.				(U	nit:PJ/a)
Year	1368	1373	1378	1383	1388	1393	1398	1400
Heating	25.56	28.87	32.28	35.96	39.81	43.92	48.15	49.90
Air Cond.	3.25	3.67	4.10	4.57	5.06	5.58	6.12	6.34
Refrig.	2.86	3.24	3.62	4.03	4.46	4.92	5.40	5.59
Elec+TV	4.16	4.70	5.26	5.86	6.48	7.15	7.84	8.13
Lighting	1.15	1.29	1.45	1.61	1.78	1.97	2.16	2.24

Table 3.40 Development of Demand for Useful Energy in Urban Household

	•			(Unit:PJ/a)					
Year	1368	1373	1378	1383	1388	1393	1398	1400	
Heating	65.72	74.23	82.99	92,46	102.36	112.92	123.80	128.30	
Air Cond.	18.61	21.02	23,50	26.18	28.98	31.97	35.05	36.33	
Refrig.	7.56	8.54	9.55	10.64	11.78	12,99	14.24	14.76	
Elec+TV	8,57	9.68	10.83	12,06	13.35	14.73	16.15	16.74	
Lighting	3.05	3.45	3.86	4.30	4.76	5.25	5.75	5.96	

Table 3.41 Development of Demand for Useful Energy in Industry

							(Unit:PJ/a)	
Year	1368	1373	1378	1383	1388	1393	1398	1400
Heating	220.77	245.56	287.45	343.94	404.65	472.67	545.64	576.52
M. Power	28.90	32.15	37,63	45.03	52,97	61.88	71.43	75.47
Feed Stk	44.28	49,25	57.65	68.99	81.16	94.80	109.44	115,63
Elec	35.18	39,13	45.81	54,81	64.48	75.32	86.95	91.87

Table 3.42 Development of Demand for Useful Energy of UP Transport

		, i		$(x_1, \dots, x_{n-1})$			(	Unit:PJ/a)
Year	1368	1373	1378	1383	1388	1393	1398	1400
UP_Car	45,35	54.33	64.96	76.71	89.08	102.46	116.23	122,27
UP_Taxi	7.52	9.00	10.76	12.71	14.76	16.98	19.26	20.26
UP_MC	0.88	1.06	1.26	1.49	1.73	1.99	2.26	2.37
UP_M-Bus	6.86	8.21	9.82	11.59	13.46	15.49	17.57	18.48
UP_Bus	1.98	2.37	2.84	3,35	3.89	4.47	5.07	5.34
UP_Train	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
UP_TOT	62.58	74.97	89.64	105.85	122.93	141.39	160.38	168.72

Table 3.43 Development of Demand for Useful Energy of IP Transport

								(Unit:PJ/a)
Year	1368	1373	1378	1383	1388	1393	1398	1400
IP Car	1.44	1.76	2.10	2.47	2.86	3.27	3.69	3.87
IP M-Bus	4.14	5.04	6.03	7.09	8.20	9.39	10.61	11.11
IP_Bus	6.77	8.25	9.86	11.60	13.42	15.36	17.35	18.17
IP_D-Train	1.32	1.62	1.93	2.27	2.63	3.01	3.40	3.56
IP E-Train	0.01	0.02	0.02	0.02	0.03	0.03	0.03	0.03
IP_Air	4,48	5.47	6.53	7.68	8.89	10.17	11.50	12.04
IP_TOT	18.17	22.15	26.47	31.13	36.01	41.22	46.58	48.78

Table 3.44 Development of Demand for Useful Energy of Freight Transport

							(	Unit:PJ/a)
Year	1368	1373	1378	1383	1388	1393	1398	1400
Fr L-Truck	80.00	87.42	103.14	129.46	156.81	185.52	215.46	227.28
Fr S-Truck	13.46	14.71	17.36	21.79	26.39	31.22	36.26	38.25
Fr D-Train	1.70	1.85	2.19	2.74	3.32	3.93	4.57	4.82
Fr E-Train	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Fr Air	0.83	0.91	1.07	1.34	1.63	1.93	2.24	2.36
Fr_TOT	95.99	104.89	123.75	155.34	188.15	222.60	258.52	272.71

Fig. 4.6 Production of Petroleum Products	ction of Per	troleum 1	Products									-				D)	(Unit:Mio. BOE/a)	OE/a)
Year	1347	1348	1349	1350	1351	1352	1353	1354	1355	1356	1357	1358	1359	1360	1361	1362	1363	1364
LPG	0.4	0.6	2.9	5.0	5.5	6.8	9.9	6.8	6.7	7.6	5.0	5.4	4.1	3.4	4.3	5.0	5.5	5.6
Gasoline	16.9	16.6	17.5	19.5	19.2	20.7	21.3	23.9	26.2	27.4	29.1	31.7	26.7	22.6	25.1	28.7	32.7	33.9
J_Fuel	16.9	17.6	17.3	15.6	17.3	16.2	15.4	15.6		13.3	12.0	6.7	4.8	3.0	3.3	8.0	8.0	8.0
Kerosine	16.2	18.1	16.9	18.6	19.2	19.5	20.1	20.1		32.0	28.8	38.5	32.9	26.2	30.7	25.7	26.5	23.8
G_Oil	28.7	29.7	32.3	35.6	35.5	38.7	40.5	45.9	48.8	53.8	56.5	57.5	57.1	47.0	49.2	67.1	75.9	80.4
F_Oil	73.9	78.7	83.8	85.3	84.4	90.2	9.66	103.5	6.76	111.1	103.4	120.8	102.1	62.5	67.1	68.1	73.7	75.4
Year	1365	1366	1367.	1368	1369	1370	1371	1372	1373.	1374	1375	1376	1377	1378	1379	1380	1381	1382
LPG	5.2	5.3	5.9	7.2	10.4	10.8	13.6	17.1	21.5	21.2	21.0	20.8	20.6	20.3	21.7	23.2	24.8	26.5
Gasoline	29.3	30.7	30.6	38.7	41.8	47.6	53.5	60.1	9.79	70.0	72.5	75.1	77.8	80.6	83.5	86.5	89.7	92.9
J_Fuel	9.0	0.5	2.7	2.6	3.5	4.1	4.6	5.1	5.6	8.0	11.3	16.0	22.6	32.0	30.7	29.3	28.0	26.8
Kerosine	21.8	25.7	27.6	40.4	35.9	41.9	43.3	44.8	46.2	46.5	46.7	46.9	47.1	47.4	48.3	49.3	50.3	51.3
G_0il	71.3	62.9	66.5	78.9	89.1	98.2	98.3	98.4	98.6	104.4	110.6	117.2	124.1	131.5	136.4	141.4	146.7	152.1
F_Oil	72.9	70.7	76.2	6.86	102.7	119.2	114.1	109.2	104.5	109.8	115.4	121.2	127.4	133.8	136.3	138.9	141.6	144.3
Year	1383	1384	1385	1386	1387	1388	1389	1390	1391	1392	1393	1394	1395	1396	1397	1398	1399	1400
LPG	28.4	29.4	30.6	31.7	32.9	34.2	35.3	36.3	37.4	38.6	39.7	41.0	42.2	43.5	44.8	46.2	47.6	49.0
Gasoline	96.3	99.4	102.6	105.8	109.2	112.7	116.1	119.5	123.0	126.7	130.4	133.9	137.4	141.0	144.7	148.5	152.4	156.5
J_Fuel	25.7	26.5	27.3	28.1	29.0	29.9	32.4	35.0	37.9	40.9	44.3	46.8	49.4	52.1	55.0	58.1	61.4	64.8
Kerosine	52.4	52.9	53.3	53.8	54.4	54.9	55.4	55.9	56.5	57.0	57.6	57.7	57.7	57.8	57.9	58.0	58.1	58.2
G_Oil	157.7	163.4	169.2	175.3	181.5	188.0	197.0	206.4	216.3	226.6	237.5	245.4	253.6	262.1	270.8	279.9	289.3	298.9
F_Oil	147.0	150.2	153.5	156.8	160.2	163.7	171.0	178.7	186.6	195.0	203.7	210.1	216.7	223.5	230.6	237.8	245.3	253.0

1347  Jas 0.1  Jas 0.1  Jas 0.1  Jas 0.8  Jas 0.	1350 0.1 1.0 4.4 4.4 i final en	1355	1360	1365	1370	1373	1378	1383	1388	1393	1400
الما ندّا امما	0.1 1.0 4.4 final en	6.7				)					
	1.0 4.4 final en		14.1	24.7	51.5	76.0	105.9	49.1	50.1	18.3	19.9
	4.4 final en	2.5	6.1	13.6	7.1	7.3	8.1	8.7	11.7	31.5	49.4
	final en 360	8.3	9.6	23.2	31.3	59.0	52.1	95.4	9.96	117.4	135.5
1 1 7	final en 360								·		
1350 SEI 24.8 38.2 22.3 3.3 88.6 2	360	ergy consi	umption				(Unit:Mio.BOE/a)	.BOE/a)			
SEI 24.8 38.2 22.3 3.3 88.6 2	)	1370	1373	1378	1383	1388	1393	1400			
38.2 22.3 3.3 88.6 2	73.7	179.7	178.5	196.7	219.3	243.1	269.4	308.3			
22.3 3.3 88.6 2	70	126.4	169.1	169.6	189.1	214.2	242.2	284.9			
3.3	53.8	105.5	128.1	152.3	184.7	218.5	254.6	307.3			
88.6	13.7	33.8	30.9	34	40.3	46.7	52.9	60.7			
	211.2	445.4	506.6	552.6	633.4	722.5	819.1	961.2			
[%]								:			
HLD & SEI 28.0	34.9	40.3	35.2	35.6	34.6	33.6	32.9	32.1			
IND 43.1	33.1	28.4	33.4	30.7	29.9	29.6	29.6	29.6			
TRC 25.2	25.5	23.7	25.3	27.6	29.2	30.2	31.1	32.0			
AGR 3.7	6.5	7.6	6.1	6.2	6.4	6.5	6.5	6.3			
	٠										
Fig. 4.9 Emission of Pollutants in I. R. Iran	tants in	I. R. Iran		ł		-		(kt/a)		-	
1350	1360	1370	1373	1378	1383	1388	1393	1400			
C02 12.3	38.8	87.0	139.8	148.4	162.1	177.1	203.1	246.2			
CO 179.9 4	426.7	867.4	793.2	935.7	1110.8	1294.0	1490.7	1776.9			
NOX 189.9 4	466.9	1345.1	1354.3	1549.2	1829.9	2128.6	2461.7	2946.5			
SO2 108.7 2	287.5	536.6	541.2	516.5	747.0	846.0	1058.7	1318.0			

N-Gas   S73   96.2   108.1   95.9   106.1   139.0   80.3   89.8   111.5   95.3   94.5   144.1   105.2   11.9   11.4   10.5   1	Elec	7	11.8	13.4	21.0	12.4	15.1		31.3	11.8	13.4	21.0		12.4	15.1	31.3
10   16.8   11.4   10.5   15.9   106.1   159.0   80.3   89.8   111.5   11.4   10.5   16.6   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   10.5   11.4   11.7   13.7   13.7   13.5   11.8   11.9   14.1   11.7   13.7   13.7   13.8   1400   73   78   89   1400   73   78   89   1400   73   78   89   1400   73   78   89   1400   73   78   89   1400   73   78   89   1400   73   78   89   1400   73   78   89   1400   73   78   89   1400   121.7   131.8   82.5   82.5   106.4   110.4   115.2   82.5   116.0   141.2   142.6   142.6		(REF09)	(		(B)	ASE09)			(LOW	(60,		-	(HIGH08	) (e		
12.9   12.0   14.3   11.8   13.6   22.9   15.5   11.4   10.5   16.6   11.4   11.2   12.0   14.3   11.8   13.6   22.9   15.5   11.9   14.1   11.7   13.7	N-Gas	3	37.3	2.96	108.1	6.56	106.1		0.6	80.3	8.68	111.5		5.3	99.5	144.1
12.9   12.0   14.3   11.8   13.6   22.9   15.5   11.9   14.1   11.7   13.7     Consumption of Boergy Carriers in Inchestry of I. R. Iran   (Unit:MicaDO (Boergy Carriers in Inchestry of I. R. Iran   (Assembly)   (HIGHIO)   (HIGHIO	Pet Prod	÷	8.91	11.4	10.5	15.9	11.4		0.5	19.5	11.4	10.5		9.9	11.4	10.5
Consumption of Energy Carriers in Industry of I. R. Iran	Elec	1	12.9	12.0	14.3	11.8	13.6		2.9	15.5	11.9	14.1		1.7	13.7	23.0
Consumption of Energy Carriers in Industry of I. R. Iran   3																
Consumption of Energy Carriers in Industry of I. R. Iran   78 83 88 1400 73 78 83 88 1400 73 78 83 88 1400 73 78 83 88 1400 73 78 83 88 1400 73 78 83 88 1400 73 78 83 88 1400 73 86 123 59 76 91 107 143 58 89 11.9 162 82.1 82.7 100.0 121.7 131.8 82.5 98.2 105.4 110.4 115.2 82.5 116.0 141.2 142.6 15.9 15.1 10.1 7.9 52.8 16.9 11.9 10.1 7.9 52.8 16.9 11.9 10.1 7.9 52.8 16.9 11.9 10.1 7.9 52.8 16.9 11.9 10.1 7.9 52.8 16.9 11.9 10.1 7.9 52.8 16.9 11.9 10.1 7.9 52.8 16.9 11.9 10.1 7.9 52.8 16.9 11.9 10.1 7.9 52.8 16.9 11.9 10.1 7.9 52.8 10.1 10.1 10.1 10.1 10.1 10.1 10.1 10	•															
Curitation of Energy Carriers in Industry of L. R. Lian   T3 78 83 88 1400 73 78 83 88 1400 73 78 83 88   T3 78 85 1400 73 78 83 88 1400 73 78 83 88   T4 78 83 88 1400 73 78 83 88   T5 75 84 123 55 75 84 1004 1217 1318 825 982 1054 1104 1152 825 1160 1412 1426 1426 1421 172 202 24.1 28.4 40.4 19.4 24.6 25.8 26.7 28.1 19.2 28.5 33.8 40.6					ć											
Consumption of Energy Carriers in Industry of I. R. Iran   T3			é			-										
Consumption of Energy Carriers in Industry of I. R. Fran   (Unit-Mio.BG   73   78   85   1400   73   78   85   1400   73   78   85   88   1400   73   78   88   88   1400   73   78   88   88   1400   73   78   88   88   1400   73   78   88   88   1400   73   78   78   78   78   78   78   78	-							-				*.				
Consumption of Energy Carriers in Industry of I. R. Frank   1400   73   78   85   1400   73   78   85   1400   73   78   85   1400   73   78   85   88   1400   73   78   85   88   88   1400   73   78   88   88   1400   73   78   88   88   1400   73   78   78   88   88   1400   73   78   78   78   78   78   78   78																
Consumption of Bacrety Carriers in Industry of I. R. Iran   73																
(REF10)         73         78         83         88         1400         73         78         83         88           (REF10)         73         86         123         59         7.6         9.1         10.7         14.3         5.8         89         11.9         16.2           82.1         82.7         100.0         121.7         131.8         82.5         98.2         105.4         110.4         115.2         82.5         116.0         141.2         142.6           4         16.9         13.1         10.1         7.9         52.8         16.9         13.1         10.1         7.9         5.7         16.9         13.1         14.2           17.2         20.2         24.1         28.4         40.4         19.4         24.6         25.8         26.7         28.1         10.1         37.1           17.2         20.2         24.1         28.4         40.4         19.4         24.6         25.8         26.7         28.1         19.2         28.5         33.8         40.6           5.2         6.1         7.3         8.6         12.3         5.9         7.6         9.1         10.7         14.3         5.8	5 7 7 11 V	Posessmention	f Buston Ca	July all successions	hrefmu of I D	uou.									(Hait-Mic	ROE/
(REF01) (HIGHO1) (HIG	Year	73	78	83	88	1400	73	78	88	88	1400	73	78	83	88	1400
S2.2         6.1         7.3         8.6         12.3         5.9         7.6         9.1         10.7         14.3         5.8         8.9         11.9         16.2           82.1         82.7         100.0         121.7         131.8         82.5         98.2         105.4         110.4         115.2         82.5         116.0         141.2         142.6           1 10.2         13.1         10.1         7.9         5.7         16.9         13.1         10.1         37.1           17.2         20.2         24.1         28.4         40.4         19.4         24.6         25.8         26.7         28.1         19.2         28.5         33.8         40.6           KEETIO         7.3         8.6         12.3         5.9         7.6         9.1         10.7         14.3         5.8         8.9         11.9         16.2           82.1         87.6         100.0         112.2         142.7         88.4         106.0         104.9         102.5         93.6         87.5         123.0         137.4         150.1           d         0.1         0.1         0.1         0.1         11.7         1.5         1.4         1.4						(BA	(SE01)				H)	GH01)				
REJ	ු ප්	5.2		7.3	8.6		5.9	7.6	9.1	10.7		5.8	8.9	11.9	16.2	\$4.
Carrolloon   16.9   13.1   10.1   7.9   52.8   16.9   13.1   10.1   7.9   57.8   16.9   13.1   10.1   37.1     Carrolloon   17.2   20.2   24.1   28.4   40.4   19.4   24.6   25.8   26.7   28.1   19.2   28.5   33.8   40.6     Carrolloon   20.2   24.1   28.4   40.4   19.4   24.6   25.8   26.7   28.1   19.2   28.5   33.8   40.6     Carrolloon   20.2   26.1   23.2   23.1   22.2   25.0   31.0     Carrolloon   20.2   23.5   23.9   23.5   23.1   22.2   25.0   31.0     Carrolloon   20.2   23.5   23.9   23.5   23.1   22.2   25.0   31.0     Carrolloon   20.2   23.6   23.6   23.2   23.1   23.2   23.6     Carrolloon   20.2   23.6   23.6   23.7   23.1     Carrolloon   20.2   23.6   23.6   23.7   23.7     Carrolloon   20.2   23.6   23.6   23.7     Carrolloon   20.2   23.6   23.7     Carrolloon   20.2   23.6   23.6     Carrolloon   20.2   23.6   23.6     Carrolloon   20.2   23.6   23.6     Carrolloon   20.2     Ca	N-Gas	82.1	82.7	100,0	121.7	131.8	82.5	98.2	105.4	110.4	115.2	82.5	116.0	141.2	142.6	143.
(REF10)     (BASE10)     (BASE10)     (HIGH10)     (HIGH10)       S.2     6.1     7.3     8.6     12.3     5.9     7.6     9.1     10.7     14.3     5.8     8.9     11.9     16.2       82.1     87.6     100.0     112.2     142.7     88.4     106.0     104.9     102.5     93.6     87.5     123.0     137.4     150.1       d     0.1     0.1     0.1     0.1     11.7     1.5     1.4     1.4     1.3     11.0     10.7     16.1       17.2     19.4     22.6     25.5     32.9     13.6     23.2     23.1     22.2     13.6     22.2     26.0     31.0	Pet.Prod	16.9		10.1	7.9	52.8	16.9	13.1	10.1	7.9	5.7	16.9	13.1	10.1	37.1	20.1
(REF10)     (MASE10)     (MASE10)       5.2     6.1     7.3     8.6     12.3     5.9     7.6     9.1     10.7     14.3     5.8     8.9     11.9     16.2       82.1     87.6     100.0     112.2     142.7     88.4     106.0     104.9     102.5     93.6     87.5     123.0     137.4     150.1       d     0.1     0.1     0.1     0.1     11.7     1.5     14     1,4     1.3     11.0     10.7     16.1       d     0.1     0.1     0.1     11.7     1.5     1.4     1.4     1.3     11.0     10.7     16.1       17.2     19.4     22.6     25.5     32.9     23.0     23.1     22.2     13.6     22.2     26.0     31.0	Elec	17.2		24.1	28.4	40.4	19.4	24.6	25.8	26.7	28.1	19.2	28.5	33.8	40.6	45.3
5.2     6.1     7.3     8.6     12.3     5.9     7.6     9.1     10.7     14.3     5.8     8.9     11.9     16.2       82.1     87.6     100.0     112.2     142.7     88.4     106.0     104.9     102.5     93.6     87.5     123.0     137.4     150.1       d     0.1     0.1     0.1     11.7     1.5     1.4     1.4     1.3     11.0     10.7     16.1       17.2     19.4     22.6     25.5     32.9     13.6     23.2     23.1     22.2     13.6     22.2     26.0     31.0		(REF10)				(BA	(SE10)		-		IH)	GH10)				-
82.1 87.6 100.0 112.2 142.7 88.4 106.0 104.9 102.5 93.6 87.5 123.0 137.4 150.1 d 0.1 0.1 0.1 11.7 1.5 1.4 1.4 1.3 11.3 11.0 10.7 16.1 17.2 19.4 22.6 25.5 32.9 13.6 23.0 23.2 23.1 22.2 26.0 31.0	Sal	5.2		7.3	8.6	12.3	5.9	7.6	9.1	10.7	14.3	5.8	8.9	11.9	16.2	23.
rod 0.1 0.1 0.1 0.1 11.7 1.5 1.4 1.4 1.3 11.0 10.7 16.1 17.2 19.4 22.6 25.5 32.9 13.6 23.0 23.2 23.1 22.2 26.0 31.0 31.0	N-Gas	82.1	87.6		112.2	142.7	88.4	106.0	104.9	102.5	93.6	87.5	123.0	137.4	150.1	151.
17.2 19.4 22.6 25.5 32.9 13.6 23.0 23.2 23.1 22.2 26.0 31.0	Pet.Prod	0.1	0.1	0.1	0.1	0.1	11.7	1.5	1.4	1.4	13	.11.3	11.0	10.7	16.1	o,
	Elec	17.2			25.5	32.9	13.6	23.0	23.2	23.1	22.2	13.6	22.2	26.0	31.0	32.
	-															:
			÷													

# II. Record of Visits to Factories and Plants

- 1. Cement
- 2. Sheet Glass
- 3. Sugar
- 4. Iron and Steel
- 5. Power Generation
- 6. Oil Refining
- 7. Others

#### 1. Cement

#### 1.1 Tehran Cement Factories (No. 1 and No. 2)

#### 1.1.1 Outline

Tehran Cement Company, one of state-owed cement companies in this country, has 2 factories near to Tehran, one (No. 1) of which installed No. 1-6 lines and another (No. 2) No. 7 line. These plants are producing cement in their full operation, coping with rapid increase in demand for cement in recent years. More specifically, they are operating for 335 days per annum, andmaintenance period is curtailed as short as possible although 30 days are usually allocated for it. Some of indicators of these plants are shown in Table 1.1.

#### 1.1.2 Countermeasures (Devices) on Heat Consumption

#### (i) Outline of Heat Consumption

Indicators for considering countermeasures for promoting energy in No. 1 and No. 2 factories including capacity, production, energy consumption, and others are shown in Table 1.2 and 1.3 respectively.

Fig. 1.1 shows production flow in No. 2 factory (No. 7 line), which installed SP kiln with satellite coolers, and energy consumption per unit of production (970 kcal/kg-cl) is reported to be among the lowest of factories which have the similar scale of production capacity to this.

Temperatures of exhaust gas and clinker at No. 7 kiln are as follows

exhaust gas (at the outlet of kiln	1,200℃
exhaust gas (at the outlet of pre-heater)	450-500℃
exhaust gas (at the outlet of EP)	90-120℃
clinker (at the outlet of pre-heater)	800°C
clinker (at the outlet of cooler)	130℃

Table 1.1 Some Indicators of Tehran Cement Factories (NO.1 and NO.2)

Line	Capacity(t-cl/h)	Kilu type	Fuel	Established year
No1	300	Yet	FO, NG	1952
No2	300	Wet	<i>s</i> .	1957
No3	600	7et	,	1967
No4	2. 000	Dry		1973
No5	300	Wet	,	1961
No6	4,000	Lepol	FO/NG	1978
No7	2, 000	S P	FO/NG	1985

NOTE: "FO, NG" means that heavy fuel oil or natural gas is fired and "FO/NG" means that they are fired mixedly.

Table 1.2 Indicators on Energy Consumption in NO.1 Factory

		· · · · · · · · · · · · · · · · · · ·	· · · · · · · · · · · · · · · · · · ·
1 Factory		; 	
Yajor product	Portland o	cement	
Production	1988 1989	1990 1991	
	1.9 1.92	1. 64 1. 9	Mt-cl/Y
Operating hour	3 6 5 × 2	4	h/Y
No of employee	1,800		persons
2 Energy consumption	1991	1992	
Heavy Fuel oil	48, 738	82, 566	k l / Y
Natural gas	174, 158	132. 998	m,³/Y
3 Specific energy consumption			
Heavy Fuel oil	25. 7	~	l/t-cl
Natural gas	91.7	~	m <sub>a</sub> ³/t-cl
4 Energy cost			
Heavy Fuel oil	~		I R/k I
Natural gas	~		"

NOTE: ~ (See Table 1.1)

Table 1.3 Indicators on Energy Consumption in NO. 2 Factory

1 Factory			·····		. :
Total capacity	2, 0	0 0			t-cl/D
Production	1988	1989	1990	1991	
Production	409	414	502	472	k t-cl/Y
Emproyee	420	1	1	J.,	persons
Mech' engineer,	2				"
Chem' "	4				//
Elec' "	4				"
2 Energy consumption	11				
Fuel oil	8. 5			·	k l / h
N-gas	8, 0	0 0			ma³/h
3 Specific fuel consumption					
Fuel oil	94~	95		<u>.,,</u>	k g/t-pro
N-gas	100				m a³/t-pro
(Calory base)	970			k	cal/kg-cl
4 Energy cost			: : : : : : : : : : : : : : : : : : :		
Fuel oil	2.5(at	refiner	y), 5(at	factory	) IR/I
N-gas	5				IR/m <sub>a</sub> <sup>3</sup>
5 Lower calorific value					
Fuel oil	9, 6	0 0		k	cal/kg
N-gas	9, 4	00~9	, 600	k	$cal/m_n^3$

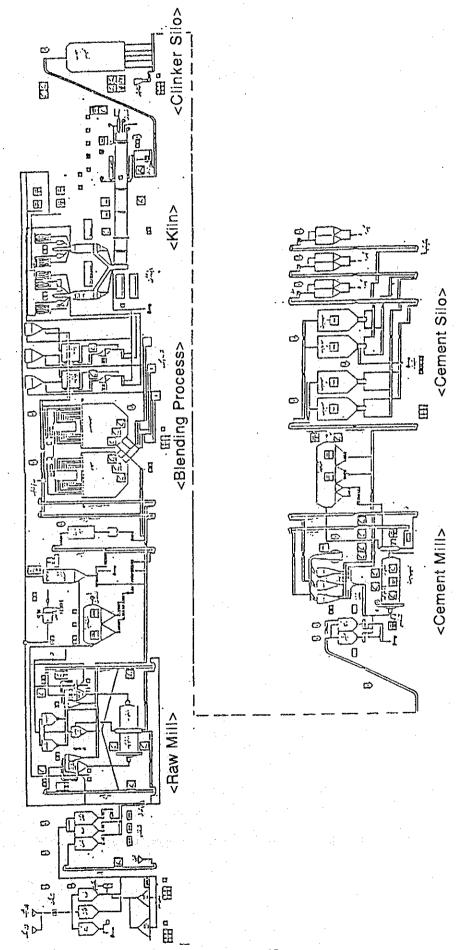


Fig. 1.1 Outline of NO.7 Line on Tehran Cement Co.

#### (ii) Countermeasures to be Considered

Energy consumption per kg of clinker in No. 2 factory is reported to be 970 kcal, which can be compared with 706 kcal in 1990 in Japan. Following countermeasures or devices can be recommended for the factory and No. 1 factory, which is less efficient in energy uses, to fill such a difference.

#### a) Countermeasures at the 1st step

- Rehabilitation of bricks in kilns.
- \* Rehabilitation of ducts for insulation of high-temperature combustion gas, combustion air, and clinker.
- \* Preventing high-temperature combustion gas, combustion air, and clinker from leakage.
- \* Preventing cool air from entering kiln.
- \* Quality control in preparing raw materials (reducing moisture and making the grains uniform, in particular).
- Managing fuel and combustion in kiln.

Additionally, special mention should be made of the necessity of preserving working environment in the factory. Preventing clinker as well as cement from dispersing within the factory might mean "money conservation" rather than energy conservation.

#### b) Countermeasures at the 2nd step

Wet type kilns (= 130-140 kg/t-cal) are installed in No. 1 factory except for No. 4 kiln (= 85 kg/t-cal) and No. 6 kiln (Lepole type; = 80 kg/t-cal) and are less efficient in energy usages. Following recommendations can be made mainly for these kilns.

- \* Installation of SP (suspension pre-heater)
- \* Installation of pre-calciner (new suspension pre-heater..... NSP)
- Recovery of exhaust heat from air cooler.

In addition, the installation of exhaust gas heat recovery power plants should be considered. Heat losses due to exhaust gas and radiation account for a major part of heat loss in kilns. In Japan, there has been a growing number of exhaust gas heat recovery power plant installed in cement factories where the temperature of exhaust gas at the outlet of pre-heater at SP kiln is 32 0 - 350°C. The temperature of exhaust gas of No. 7 kiln is reported to be 450-500°C, much

higher than that in Japan, and heat can be utilized for power generation through modifying pre-heater. The same suggestion is supposed to be able to be made for other kilns although any specific data could be obtained by Japanese experts.

#### c) Countermeasures at the 3rd step

As countermeasures at the 2nd step mentioned above and conversion from wet type kiln to dry type will require a large amount of investment, a comprehensive examination and decision including considering replacement of the wet type kilns with larger scale ones should be conducted. If the replacement is implemented, decrease in energy consumption per unit production caused by higher efficiency as well as by larger scale can be enjoyed in addition to decrease in production cost.

## 1.1.3 Countermeasures (Devices) on Electricity Consumption

#### (i) Outline of Electricity Consumption

Electric power used in this factory are supplied from outside.

The loads of main electricity users in No. 1 factory are as follows.

Raw mill 12.5 MW

Kiln 11.8 MW

Cement mill 15.4 MW

And the loads of main electricity user in No. 2 factory are as follows.

Raw mail 3.75 MW

Kiln 1.4 MW

Cement mill 3.8 MW

Electricity consumption per ton of clinker is reported to be 130-150 KWh in wet kilns and 95 - 110 KWh in dry kilns in No. 1 factory. Average consumption of electricity per ton of clinker in this factory is as follows.

1991 132 kWh/t 1990 123 kWh/t 1989 130 kWh/t And 90-92% of electricity is consumed for driving motors and 8-10% for heating and lighting in No. 1 factory. Consumption of electricity per ton of cement products is reported to be 117 KWh in No. 2 factory, which can be compared with 102 kWh in Japan in 1990. This comparison implies that even No. 2 factory, one of the most efficient factories in this country, still has much soon for saving electricity.

## (ii) Countermeasures to be Considered

- a) Countermeasures at the 1st step
  - Measuring and monitoring of electricity consumption to operate main facilities effectively
  - \* Reducing operation hour of main facilities and lowering peak load
- b) Countermeasures at the 2nd step
  - \* Controlling the volume of air flow and water flow by introducing inventer system
- c) Countermeasures at the 3rd step
  - \* Introducing more efficient crushers

    Crushers in raw and cement mills use about two-thirds of total electricity consumption in a cement factory. The effect of installing more efficient crusher, vertical one, is substantial in decreasing electricity consumption. In addition, introducing preliminary crushing system also brings effective utilization of electricity in the cement factories.
  - \* Conversion from wet type kiln to dry type kiln

    This device mentioned already can also contribute to reducing electricity consumption in

    No. 1 factory where four wet type kilns (No. 1, 2, 3, 5) are installed.

#### 2. Sheet Glass

#### 2.1 Ghazvin Glass Co.

#### 2.1.1 Outline of the factory

The factory is located in Ghazvin at about 200 km in the west of Teheran, being a national factory belonging to the Ministry of Industry. In 1968, the present No. 1 line was constructed, and 4 years later, No. 2 line and in succession No. 3 line were constructed. At present, with No. 4 line completed, the production capacity has been expanded to 550 t/d from the initial capacity of 70 t/d. It is the largest sheet glass factory in Iran (the share in 1992 is about 70%). Presently, with the cooperation of Nippon Sheet Glass Co., Ltd., a new line of float system is being planned.

The factory uses silica rocks, soda ash, dolomite, etc. sent from mines, and produces sheet glass (also patterned glass) by a process consisting of a crushing plant, mixing step, glass melting & clearing step, and molding & annealing & processing step.

It is said that a wet crushing factory is being constructed in Drekuhi (mine) at 50 km away from Ghazvin as a joint invested factory of four glass factories under the guidance of the government for rationalization of production and to avoid the problem of dust pollution. The crushing factory is scheduled to start deliveries two weeks later.

Most of the glass products are sold in the domestic market, and very recently export to the Middle and Near East has just started.

## 2.1.2 Present situation of the factory and energy saving indicators

The present situation of the factory and energy saving indicators are shown in Table 2.1.

Table 2.1 Present situation of the factory and indicators concerned

l	Factory	
	Total Capacity	120,000 product-t/Y
	Crushing Plant	35 (3 plant total) t/h
	Diesel-Generater (emergency)	860 kVA × 8 set, 530 kVA × 3 set
	Production (1992 actual)	146,000 product-t/Y
	Name of Product	Sheet Glass
	Operating Hour	365 × 24 = 8,760 h/Y
	No of Employee	1,400 persons
	No of Engineer	20 persons
2	Energy Consumption (1991)	
	Heavy Fuel Oil	= 200,000 l/d
	Gas oil	= 7,500 l/d
	Natural Gas	= 12,000 Nm³/d
	Electricity	~ kWH/Y
3	Specific Energy Consumption	
	Heavy Fuel Oil	5,257 Mcal/t
	Electricity	~ kWH/t

Note: The value of mark (~) are filed by the report after given by the factory.

## 2.1.3 Energy saving measures

A glass melting furnace is a major apparatus in the glass manufacturing industry. The melting temperature of glass is generally as high as 1400 to 1600°C, and glass melting accounts for about 9 0% of the heat energy consumption of the entire factory.

The specific energy consumption rates in the sheet glass industry of Japan are as follows:

- Specific heat energy consumption: 2,934 Mcal/t (in terms of fuel oil)
- Specific electric energy consumption: 229 kWH/t

The specific heat energy consumption of this factory is as very large as 5,257 Mcal/t as shown in Table 2.1.

## (i) Energy saving measures in the 1st step

The energy saving measures in the first stage are taken by intensifying equipment maintenance and improving operation. The older the equipment, the more effective these measures. Major matters found as a result of the field survey are as follows:

- a) Repair of furnace walls and prevention of ingress of cold air into furnaces
- b) Repair of ducts of hot gas, hot air, etc. to ensure more perfect heat insulation, and prevention of leak
- c) More intensive fuel and combustion control of respective furnaces
- d) Repair of meters and more intensive numerical control
- e) Prevention of scattering of raw materials and intermediate products
- f) Enhancement of yield by decreasing the quantity of broken glass, etc.
- g) Improvement of operation in the clearing step
- (ii) Energy saving measures in the 2nd step

#### a) Glass melting furnaces

- \* Especially in the glass manufacturing industry, the furnace walls are not often thermally insulated to keep the life of furnace materials as long as possible since the repair cost of furnace materials is very high. It is recommended to adopt high performance electrocast refractories for raising the refractoriness of the furnace materials and extending the continuous operation time, and also to thermally insulate them more perfectly.
- \* The loss due to the exhaust gas of melting furnaces is considered to be on the level of 60 to 70% though not measured. If high performance recuperators are installed for recovery of waste heat, to heat the secondary air to the level of 1000°C by the hot exhaust gas, the loss due to exhaust gas can be decreased to lower than 25%. In addition, this raises combustion performance, and greatly contributes to the improvement of glass quality.
- \* High performance burners should be adopted to lower the excess air ratio to lower than 1.15. The excess air ratio of the presently used burners is surmised to be more than 2.0

judging from the white smoke emitted from the stack, though not measured. A higher excess air ratio increases the loss due to exhaust gas, and exerts adverse effects such as the increase of hot flames blown out of the opening.

The fuel is planned to be changed to natural gas 2 years later. So, the above must of course be sufficiently examined.

#### b) Generators

The factory has eight 860 kVA diesel generators and three 530 kVA diesel generators for emergency in preparation for unstable electric power supply. In addition, in preparation for a new line to be installed, emergency diesel generators of 4 MW in total are being newly installed. Even if recuperators are installed for the melting furnaces, the exhaust gas temperature is still on the level of 300°C. So, it is recommended to install exhaust gas boilers and to constantly operate steam turbine driven generators for power generation, for reducing the purchased electricity. This is surmised to be effective for energy saving and economical.

#### c) Electric equipment

The factory uses large-capacity blowers. It is recommended to control their rotational speeds, for reducing the electric energy consumption.

#### (iii) Energy saving measures in the 3rd step

The energy saving measures in the second stage described above are concerned with the improvement of existing apparatuses. Adopting larger melting furnaces is also very effective for energy saving. This is recommended to be examined in connection with the modernization of equipment. This should of course be judged comprehensively, considering the market trends, economic effect, operation efficiency, etc.

#### 2.2 Abguineh Glass Mfg. Co.

#### 2.2.1 Outline of the factory

The factory is located in Alborz Industry City at about 150 km in the west of Teheran, being a national factory belonging to the Ministry of Industry. The factory contains glass production lines and glass processing lines. The outline is as follows:

- No. 1 line: Started operation in 1972. The present production capacity is 42,000 tons/year.
- No. 2 line: A new plant which was decided to be constructed in 1987 and started operation in July, 1992 with the cooperation of Nippon Sheet Glass Co., Ltd. (including a cullet regeneration plant). The production capacity is 54,300 tons/year.
- No. 3 line: Started operation as color glass line in 1982. The present production capacity is 18 tons/year.
- Automobile front glass processing line: Raw glass is imported from Turkey.
- Tempered glass processing line: Production capacity, 100,000 m2/year
- Glass laminate processing line

The factory is the second largest sheet glass factory next to the above mentioned Ghazvin Glass Co. in Iran.

Such raw materials as silica rocks, soda ash and dolomite sand sent from crushing plants at mines are mixed in an automated batch plant and the mixture is sent to the Nos. 1 and 2 lines.

A wet crushing factory is being constructed at Drekuhi (mine) at 50 km away from Alborz as a joint invested factory of four glass factories under the guidance of the government for rationalization of production and to avoid the problem of dust pollution, as described before.

Most of the products are sold in the domestic market, but 10,000 m2 of products per year are exported to Afghanistan, Turkmenistan, Bangladesh, etc.

Furthermore, a business strategy is being developed based on an estimate that 410,000 tons of total domestic glass consumption will be covered by domestically produced 310,000 tons and imported 10 0,000 tons.

#### 2.2.2 Present situation of the factory and energy saving indicators

The present situation of the factory and energy saving indicators are shown in Table 2.2.

Table 2.2 Present situation of the factory and indicators concerned

Note: The value of mark (~) are filed by the report after given by the factory.

## 2.2.3 Energy saving measures

As stated before, the specific energy consumption rates of the sheet glass industry in Japan are as follows:

- Specific heat energy consumption: 2,934 Mcal/t (in terms of fuel oil)
- Specific electric energy consumption: 229 kWH/t

The energy consumption rates and production quantities in this factory are unknown, not allowing accurate comparison. The consumption estimated from the natural gas consumption in April, 1993 (3,387,805 Nm<sup>3</sup>) and the nominal production capacity (100,000 tons/year) is 3,862 Mcal/t (in terms of fuel oil).

Judging from this value, the specific heat energy consumption can be said to be large.

## (i) Energy saving measures in the 1st step

In this factory, Nos. 2 line and the batch plant started their operation only recently, and so are

well maintained and adjusted. For the other plants, it is recommended to intensify equipment maintenance and to improve operation as energy saving measures.

- a) Repair of furnace walls and prevention of ingress of cold air into furnaces
- b) Repair of ducts for hot gas, hot air, etc., to ensure more perfect heat insulation, and prevention of leak
- c) More intensive fuel and combustion control of respective furnaces
- d) Repair of meters and more intensive numerical control
- e) Prevention of scattering of raw materials and intermediate products
- f) Raising yield by decreasing the quantity of broken glass, etc.
- g) Improvement of operation in clearing step
- (ii) Energy saving measures in the 2nd step

#### a) Glass melting furnaces

- \* Especially in the glass manufacturing industry, the furnace walls are not often thermally insulated to keep the life of furnace materials as long as possible since the repair cost of furnace materials is very large. High performance electrocast refractories are adopted only partially in No. 2 melting furnace. It is recommended to adopt the high performance electrocast refractories fully, for more perfect heat insulation.
- \* The temperature of the exhaust gas is said to be on the 750°C level in No. 1 melting furnace and on the 400°C level in No. 2 melting furnace, and the heat efficiencies are said to be 28% and 32% respectively. It is recommended to install exhaust gas boilers and to constantly operate the steam turbine driven generators for power generation, to reduce the electricity purchased. The available heat for glass and the recovered heat of the exhaust gas boilers together are expected to give a heat efficiency of more than 70% as shown in Table 2.3. The economic effect is also large, as well as the energy saving effect.

Table 2.3 Heat balance of glass melting furnace (with exhaust gas boiler installed)

Item	%
Combustion heat of fuel	100.0
Available heat for glass	35.0
Recovered heat of boilers	37.5
Radiation loss of furnace walls	14.0
Loss due to exhaust gas	13.5

At present, the excess air ratios of burners are said to be on the 1.2 level. No. 2 furnace has an automatic air ratio controller, and in addition, is designed to allow flow control of individual burners. So, the excess air ratios of burners can be easily adjusted. However, Nos. 1 and 3 furnaces are manually controlled, and the excess air ratios are surmised to be somewhat higher. The excess air ratio directly affects the loss due to exhaust gas.

## b) Electric equipment

This factory also uses large-capacity blowers. It is recommended to control their rotational speeds and also those of pumps, etc., for reducing the electric energy consumption.

#### (iii) Energy saving measures in the 3rd step

Nos. 2 line, batch plant, etc. are modernized in efforts to have efficient equipment. The difference between the new equipment and the old equipment is large. It is recommended to scrap the old equipment for substitution by new equipment, comprehensively considering the market trends, economic effect, operation efficiency, etc.

#### 3. Sugar

#### 3.1 Varamin Sugar Refining Factory

#### 3.1.1 Introduction

There are 36 sugar factories including cane sugar, beet sugar, and refining in this country. Varamin Sugar Factory which Japanese experts visited is one of state-owned factories, and was built in 1933 by using the technologies and equipments of Scoda Company of former Czechoslovakia. Crude sugar refined in this factory is imported from the Philippines, Thailand, Cuba, Brazil and others.

The flow of heat energy in the factory is shown in Fig.3.1. The main sources of heat utilized in its production line are low-pressure steam from turbine and steam generated in a boiler which was installed for supplying steam exclusively to distillation process.

#### 3.1.2 Countermeasures (Devices) on Heat Consumption

## (i) Outline of Heat Consumption

Indicators for considering countermeasures for promoting energy conservation in this factory including capacity, production, energy consumption and others are shown in Table 3.1. And the outline of boilers and generators is shown in Table 3.2.

#### (ii) Countermeasures to be considered

This factory is 60 years old and almost all parts of it have not been renovated.

- a) Boilers and generators
- 1) Countermeasures at the 1st step
  - \* Rehabilitation for appropriate combustion in boilers
  - \* Rehabilitation for insulation of steam pipes, high-temperature part of ducts, and others
  - Rehabilitation for preventing steam, high-temperature condensate, and others from leakage
  - Leveling off of boiler load

In addition, sudden and repeated stoppages and starts of the operation of a diesel generator (23 5 kW) for emergency use, which are caused by blackouts for around 2 hours every 2-3 days, are not desirable in terms of energy conservation.

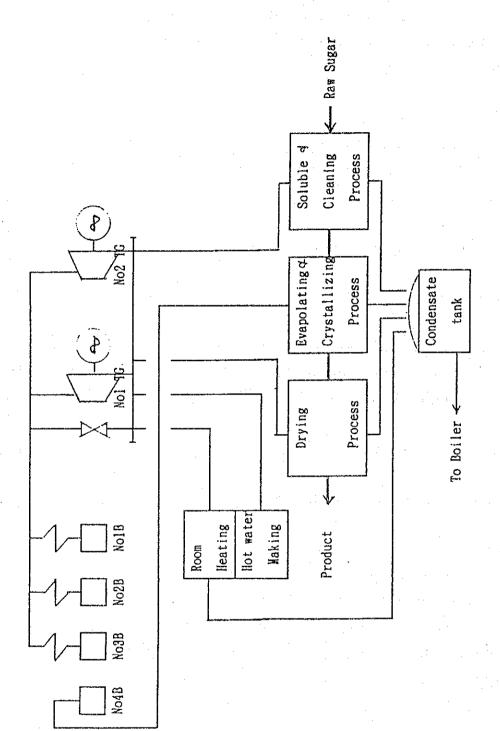


Fig. 3.1 Flow of Heat Energy in Varamin Sugar Factory

Table 3.1 Indicators on Energy Consumption in Varamin Sugar Factory

1 Factory					
Major product	White s	White sugar			
Production (based on product sugar)	1988	1989	1990	1991	
	55	53	50	42	kt/Y
Total capacity (based on raw sugar)	150				t/d
Raw sugar					
Crude sugar	70				t/d
Granulated sugar	130				t/d
Product price					
Official	30				IR/kg-prod.
Free market price	700				IR/kg-prod.
Subsidy	500				IR/kg-prod.
Operating hour	365	X	24		
Yield factor	200	/	150		
Number of employee	700				persons
Mech', Chem', Elec', Food Engineer	1	each			person
2 Energy Consumption					
Heavy fuel Oil	16.060	(1991	)		kl/Y
Diesel fuel oil	14	(1991	) -		kl/Y
Electricity (Commercial elec')	9,196				Mwh/Y
(Auto' generation)	3,456				Mwh/Y
3 Specific energy consumption	-				
Heavy fuel oil	382				kl/t-prod.
Diesel fuel oil	0.3				kl/t-prod.
Electricity	301				kwh/t-prod.
4 Energy cost					
Heavy fuel oil	8.4				IR/I
Diesel fuel oil	13				IR/I
Electricity	~				IR/kwh

Table 3.2 Outline of Boilers and Generators in Varamin Sugar Factory

No.1 ~ No.3 Boiler			<i>:</i>
Type Pressure		Water tube boiler	
		18	kg/cm2G
Temperature		350	Deg C
Evaporation	(Rating)	6	t/h
	(Actual)	8	t/h
Fucl		Heavy fuel oil	
Control		Manual	
No.4 Boiler			
Турс		Fire tube boiler	1.12
Pressure		150	lb/in2G
Temperature		sat <sup>i</sup>	* •
Evaporation	(Rating)	22,500	lb/h
Fuel		Heavy oil	
Control		Automatic	
No.1. No.2 Turbine			
Туре		Back pressure turbine	
Steam Pressure	(Inlet)	18	kg/cm2G
·	(Outlet)	1.8 ~ 2	kg/cm2G
Steam Temperature	(Inlet)	350	Deg C
Revolution		3.000	rpm
No1, No.2 Generator			
Voltage		380	V-
Cycle		50	Hz
Output		800	KVA

## 2) Countermeasures at the 2nd step

- \* Installation of economizers and air-heaters for heat recovery from exhaust gas of boilers
- \* Complete recovery of condensate from steam using facilities

  (Present ratio of condensate recovery is estimated to be about 60%)
- \* Installation of measuring instruments

Investments in these equipments and instruments should be finally determined after taking into account the cost of investments in countermeasures at the 3rd step mentioned below.

#### 3) Countermeasures at the 3rd step

Replacement of water tube boilers can be recommended as one of devices for modernizing facilities and equipments. The efficiency of the boilers is estimated to be less than 60%, considering over-load operation, type and date of manufacturing of them. The over-load operation should be avoided particularly in terms of safety.

#### b) Production line

Soluble tank, evaporator, and crystallizer are main users of steam in sugar factories. Consumption of heat energy per ton of crude sugar is estimated to be 382 1 of heavy fuel oil equivalent in this factory, which can be compared with 130-140 1 depending upon refining methods in Japan.

#### 1) Countermeasures at the 1st step

- Preventing molasses and others from leakage
- \* Leveling off of crystallizer load

  Steam utilization in the crystallizer varies substantially to influence heavily boiler load mentioned above. Improving the operation of the crystallizer can bring good results.
- \* Reducing exhaust vapor from crystallizer

  Heat energy of exhaust vapor from crystallizer is equivalent to about half of total heat energy consumption in sugar factories. Generation of the exhaust vapor can be reduced by improved operation of reducing feed water to crystallizer.

#### Countermeasures at the 2nd step

As a large volume of hot water is used in sugar factories, the installation of heat exchanger for heat recovery from the exhaust vapor of crystallizer is effective for supplying hot water to be used.

## 3.1.3 Countermeasures (Devices) on Electricity Consumption

## (i) Outline of Electricity Consumption

Main users of electricity in this factory are centrifugal separators, mixing machines, and vacuum pumps. Power loads of these facilities are as follows.

centrifugal separator:

720 kW (90 kW \*8)

mixing machine:

100 kW (5 kW \*20)

vacuum pump:

56 kW+47 kW

1,100 - 1,500 kW of electric power is supplied from the national grid, and 800 kW from auto generation plants. Annual electricity consumption is reported to be 9,196 MWh.

If the figure of 42,000 tons is used as annual production of sugar, electricity consumption per ton of sugar is calculated to be 301 kWh, which can be compared with 100 kWh in Japan.

#### (ii) Countermeasures to be Considered

- a) Countermeasures at the 1st step
  - \* Strengthening the management of maintenance and operation (the same as those in iron and steel)
- b) Countermeasures at the 2nd step
  - \* Managing peak load (the same as those in iron and steel)
  - Controlling the volume of air flow and water flow by introducing invertor system
  - Revising the capacity of motors to correspond to load in order to improve power factor

## 3.2 Haft Tappeh Cane Sugar Co.

## 3.2.1 Outline of the factory

The factory is located at 80 km in the north-northwest of Ahwaz and has an about 10,000 -hectare plantation of sugar canes. It is a crude sugar production-sugar refining factory and adjacent to it is a paper mill using bagasse as a raw material, to constitute a consistent complex as a whole. (The factory survey was conducted only for the crude sugar production-sugar refining factory.)

The factory is operated in a period from November 1 to March 15 only in relation with the harvest season of sugar canes.

## 3.2.2 Present situation of the factory and energy saving indicators

The present situation of the factory and energy saving indicators are shown in Table 3.3

Table 3.3 Present situation of the factory and indicators concerned

1,000 × 10 <sup>3</sup> Suger Cane-VY	
$120 \times 10^3$ product-VY	
$100 \times 10^3$ product-t/Y	
1,000 t/d	
5,000 (Terbine Driven × 6 unit) t/d	
68 t/h × 2 unit, 200 t/h × 1 unit	
3.15 MW × 2 unit	
1 MW × I unit	
30,753.9 product-t/Y	
Raw & Rifine Suger	
$100 \times 8 = 800 \text{ h/Y}$	
5,000 persons	
~ persons	
6,541.285 I/Y	
~ kWH/Y	
212.7 l/p-t	
~ kWH/p-t	

Note: The value of mark (~) are filed by the report after given by the factory.

## 3.2.3 Energy saving measures

The sugar factory is a crude sugar production-sugar refining factory with a plantation of sugar canes as described above. We have no such factory in Japan.

The sugar refining industry in Japan is high in the degree of refining and must produce various kinds in respectively small quantities to meet the market structure peculiar to Japan. So, the specific energy consumption is said to be relatively high. For reference, the national average specific energy consumption rates of the sugar refining industry in FY 1990 in Japan are shown below.

• Specific fuel consumption (in terms of crude oil)

Specific electric power consumption 102.8 kWH/RS-t

Especially the steam consumption in the crude sugar process heavily depends on the sugar content of sugar canes. According to our survey, the annual mean rainfall in the plantation is 250 to 3 00 mm, and the sugar canes are 32 to 33% in the mean sugar content and 52 to 54% in water content.

102.3 l/RS-t

## (i) Energy saving measures in the 1st step

The energy saving measures in the 1st step are recommended to be taken by intensifying equipment maintenance and improving operation, and are desired to be sufficiently taken since little investment is required.

## a) Boilers, generators, etc.

A sugar factory uses much low pressure steam for both crude sugar production and refining. So, it is often practiced to install turbine driven mills and turbine generators, for using the waste steam as a heat source for concentrators, crystallizers, etc.

The energy flow of this factory is also the same. The major particulars of the boilers and turbines are shown in Table 3.3. Steam is discharged from the boilers by 31 kg/cm<sup>2</sup> at 385°C, and from the turbines by 1.7 kg/cm<sup>2</sup>.

The fuel of the boilers is being converted from fuel oil to natural gas based on the request of the government due to unstable supply of fuel oil.

Major energy saving measures in the first stage for the boilers and turbines are enumerated below.

- 1) Low oxygen operation of boilers (decrease of loss due to exhaust gas by lowering excess air ratio)
- 2) More perfect heat insulation of steam pipes, hot ducts, etc.
- 3) Prevention of leak of steam and hot condensate
- 4) Leveling of boiler loads (reduction of crystallizer loads, cycle adjustment)
- 5) Maintenance of meters, and more intensive numerical control
- b) Production equipment

- 1) Prevention of scattering and leak of raw materials and intermediate products
- 2) Leveling of crystallizer loads (reduction of crystallizer loads, cycle adjustment)
- 3) Decrease of feed water to crystallizers (decrease of evaporated water)
- (ii) Energy saving measures in the 2nd step
- a) Boilers, generators, etc.
  - The following energy saving measures require the improvement of equipment for recovery of waste heat of boilers, etc.
- Heat recovery from exhaust gas of boilers, for preheating combustion air, and installation of process hot water making equipment
- More perfect recovery of condensate from steam-using apparatuses such as evaporators and crystallizers
- 3) Installation of energy control and measuring instruments
- b) Production equipment
- 1) Hot water and heat recovery from crystallizers
  - The crystallizers discharge a large quantity of about 65°C steam due to the evaporation of water from molasses. On the other hand, a large quantity of hot water is used for washing containers, floor, etc. So, the recovery of hot water and heat from the steam evaporated from the crystallizers is effective, and also contributes to the load reduction of vacuum pumps.
- 2) Utilization of CO2 gas in the exhaust gas of boilers
  - At present, a lime kiln is installed in the crude sugar cleaning process, and the coke used as the fuel for it is supplied from Isfahan Iron & Steel Complex. If the CO2 gas in the exhaust gas from the boilers in the crude sugar cleaning process is utilized, the kiln is not required. In Japan, no lime kiln is used.
- c) Electric equipment
  - It is recommended to control the rotational speeds of the blowers of boilers, etc. and water supply and drainage pumps, for reducing the electric energy consumption.
- (iii) Energy saving measures in the 3rd and 4th steps

This factory is one of agricultural product processing factories and is inevitably operated for a seasonally limited period, as described before. So, the factory operation rate is low and the energy saving effect and factory profitability are poor. Apart from the field production in a crude sugar factory, refining factories can be integrated to raise the operation rate of the refining process. This problem is recommended to be examined comprehensively together with the modernization of Varamin Sugar Refining Factory reported in 3.1.

In Iran, there exist the following factories concerned with sugar.

- 39 beet factories
- 2 cane factories
- 2 refining factories

It is planned to construct seven 100,000-ton factories (including plantations) by the end of 199 6. (At present, 50% of domestic consumption is covered by domestic production, while the balance of 50% is covered by import.)

For rationalization of the crude sugar factory, it is recommended to consider the construction of a food processing factory as an annex, and many other measures.

#### 4. Iron & Steel

#### 4.1 Isfahan Iron & Steel Complex

#### 4.1.1 Introduction

The iron and steel complex of Isfahan Steel Company is located at Dashte - Tabas, 45 km south of Isfahan city. The construction of the complex was started after a contract between Iran and former USSR was signed on January 13,1966, and No. 1 blast furnace, which has the production capacity of 600,000 tons of crude steel, was constructed by 1969. Additional construction works were made from 1974 to 1992 to reach the production capacity of crude steel of 1.9 million tons. The modernization and expansion of the complex has been planned, in which the production capacity of crude steel will be increased to 2.5 million tons, 3.7 million tons, and 5.0 million tons as the first, second, and third step respectively.

As can be seen in Fig. 4.1, facilities including sintering plant, coke oven, blast furnace, basic oxygen furnace, continuous casting unit, hot rolling mill are installed in the complex, which is only one iron & steel complex installed with blast furnace in this country.

#### 4.1.2 Countermeasures (Devices) on Heat Consumption

#### (i) Outline of Heat Consumption

Indicators for considering countermeasures for promoting energy conservation in this complex including capacity, production, energy consumption and others are shown in Table 4.1. The outline of facilities visited by Japanese experts are as follows.

#### a) Coke oven

No. 1 coke oven, which has the capacity of 500,000 ton per annum (58 cells), and No. 2, which has the capacity of 600,000 ton per annum (72 cells), are operated at the cell cycle 20 m/∞ Both of them are heated directly by coke oven gas (COG) and wet quenching method is adopted. 1.3 million tons of coking coal, around half of which is imported from foreign countries including Australia, are used in the coke ovens. Expansion of capacity through replacing the existing equipments is being considered. The temperature air and exhaust gas is as follows.

Heated air	800 - 900°C
Exhaust gas (at the outlet of coke oven)	850°C
Exhaust gas (at the outlet of cooler)	75°C

#### b) Blast furnace

No. 1 blast furnace, which has the capacity of 1,033 m<sup>3</sup>, and No. 2, which has the capacity of 2,000 m<sup>3</sup>, are installed in this complex with the total production of pig iron being 2,050,000 tons per annum. Fig. 4.2 shows the energy flow and other indicators of operation at No. 2 blast furnace which Japanese experts visited.

#### c) Basic oxygen furnace

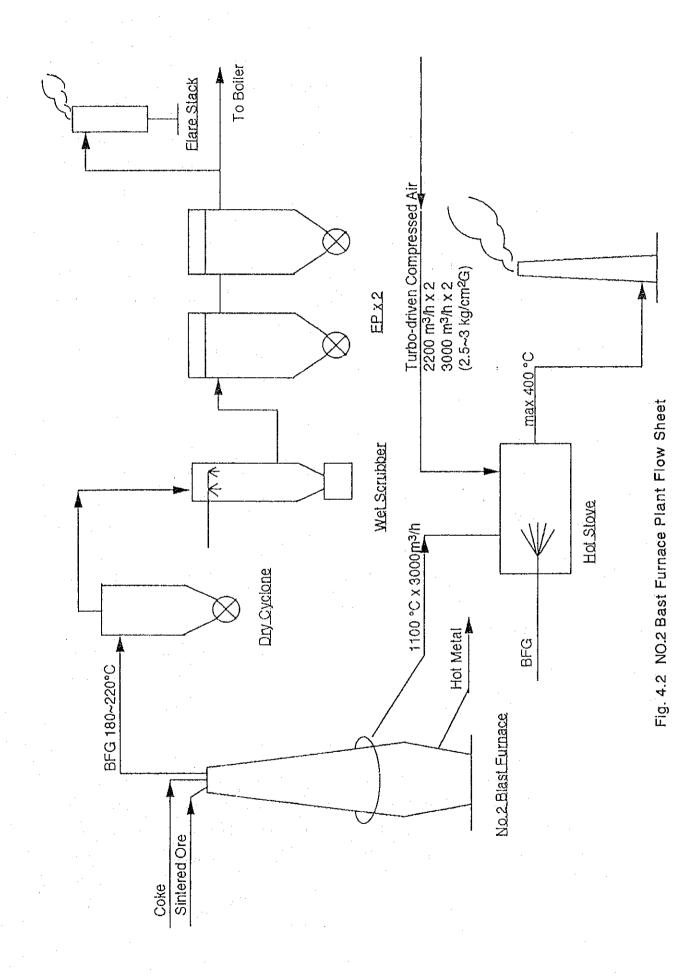
Three units of basic oxygen furnace, which has the capacity of 100 tons for each, are installed.

1.9mt/A To Fuel Gas System Steel\_Products I Beam Angle Round Bar Flat Bar H Beam Water pond HOT ROLLING MILL B-Gas N-Gas 40,000 - 50,000m3/h C-Gas BOF Stoam Generation 70 -- 110th (40 / 10Kg/cm2G) Exhaust Gas \* Energy Balance Coal 85% N-Gas 15% (B-Gas Flaring 3% ) 400,000m3/h 85,000m3/h (C-Gas N-Gas Wet Scrubber - Water REHEATER Fuel (No.2 P/S) Hot Stove 330VA 7,865 9,093 390 4,700 16,200 57,870 250°C 180 ~ 220°C Byprostuct Solvent B.T.X. Benzole Phenole H2SO4 (NH4)2SO4 3 340,000Nm3/h 1,400-1,700<sup>-</sup>C 맖 Wet Scrubber CHEMICAL RECOVERY PLANT BASIC OXIGEN FURNACE Water OXYGEN PLANT 3,000Nm3/h ő 1001 x 3) Fig. 4.1 Energy Flow in Isfahan Steel Mill Fuel Consumption(m3/h)
N.Gas 16,000
C.Gas 6,000
B.Gas 190,000 10% Dry Collector B-Gas 400,000m3/h 1,000m3 2,000m3 Sorap 🗠 1,100°C BLAST FURNACE No.1 No.2 Ę -\* (C-Gas Leak; 5%) Steam Generation No.1 140th/t40kg/cm2G)
15th to Factory at 10BAR and
10th Recovery by Condensate
No.2 440th/t100Kg/cm2G) C|Gas Power Station No.1 24MW(Generation) No.2 110MW(Generation) SINTERING PLANT COKE OVEN Power Consumption 130 - 135MW (100,000t/A × 1) No.1 500,000VA No.2 600,000VA Natural Gas Limestone Iron Ore

Table 4.1 Outline of Operation and Energy Consumption in Isfahan Steel Mill

1	Eactor	
1	Factory  The languity (based on hot metal)	1,900 kt / Y
1	Total capacity(based on hot metal)	2,100 kt / Y
	Production(based on hot metal)	365 x 24 h / Y
1	Operating hour	110.5 %
	Operating ratio	
	Pig iron	
Î	Crude steel	2,200 kt / Y
ŀ	Steel products	~ kt/Y
	Annual sales amount	~ IR/Y
2		
	Energy consumption rate	
	(based on steel product ton)	9 Gcal / t
1	Coal consumption rate	1
	(based on hot metal ton)	~ Gcal / t
	N-gas consumption rate	
1	(based on hot metal ton)	~ Gcal / t
3	Energy consumption	
	(1) Coal consumption	1,300~1,500 kt / Y
1	(2) N-gas consumption	100,000 Nm3/Y
4	Energy cost	
	(1) Coal	~  R/t
	(2) N-gas	~ IR / Nm3
5	Cost of commercial electricity	
	(1) for sale (mean)	7.5 IR / kwh
	(2) for buying (mean)	l" IR / kwh
6	Generated gas consumption	
	(1) COG	40~50,000 Nm3 / h
	(2) BFG	400,000 Nm3/h
7		
	(1) Coal	
	(2) N-gas	9,500 kcal / Nm3
	(3) COG	4,000 kcal / Nm3
	(4) BFG	900~1,000 kcal / Nm3
8	Energy consumption by each process	Nout / Hills
`	(equivalent value / crude steel ton)	
	(1) Coal	~ ~/t
1	(2) N-gas	~ ~/t
	(3) COG	~ ~/t
	(4) BFG	~ ~/t ~ ~/t
9	Treatment for slag	~/!
۱۶		[
[	(1) Sand wool	5 %
	(2) Slag aggregate	80 %
L	(3) Others	15 %

NOTE:  $\sim$  indicates that figures will be filled later.



The flow of exhaust gases and other indicators at the furnaces are shown in Fig. 4.3. The capacity expansion to 130 tons for each unit is being planned.

## d) Power plant for own use

Demand for electricity in this complex is usually fully supplied by two power plants constructed for own use, one (No. 1) of which has the capacity of 24 MW and another (No. 2) 115 MW. There are two units of turbines in No. 2 power plant which was visited by Japanese experts (Fig. 4.4), and the extract steam of one unit (No. 3....4 stage extract steam condensate turbine) is confirmed to be used for heating water and as the heat source of heat exchanger for heating the complexes' building (8 kg/cm<sup>2</sup> G x 110°C). Another unit (No. 4....3 stage extract steam condensate turbine) is not supplying its extract steam for utilization for un-identified reasons.

Three boilers are installed in No. 2 plant, mixed - firing natural gas (NG), blast furnace gas (BFG), and COG.

#### (ii) Countermeasures to be Considered

As mentioned above, this complex has been planning to modernize and rationalize its facilities as well as to expand its production capacity. As details on its planning could not be confirmed during Japanese experts' visit there, recommendations on countermeasures or devices for promoting energy conservation are made in this report without taking into account the planned modernization and rationalization. Some of our recommendations might have been already adopted or implemented by the management.

The present energy consumption per ton of steel products in this complex, however, is reported to be around 9 Gcal, which can be compared with 5.7 Gcal in Japan, showing that there is much room for this complex to save energy in future.

#### a) Countermeasures at the 1st step

Strengthening the management of maintenance and operation of individual facilities is the countermeasure at the 1st step as mentioned earlier. Individual effects of such countermeasures are not so great, but a large amount of effect can be accumulated in total. In other words, such a kind of devices leads to "the elimination of wastes." Following devices can be recommended as those at the 1st step.

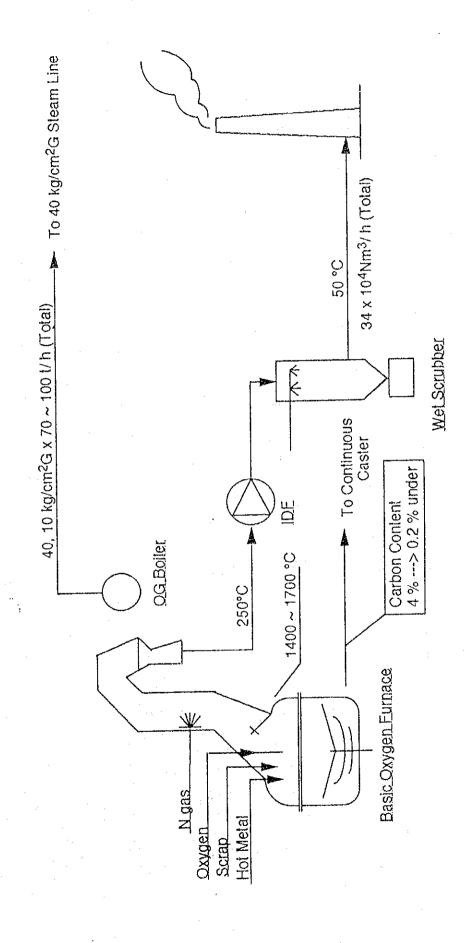


Fig. 4.3 Basic Oxygen Plant Flow-Sheet

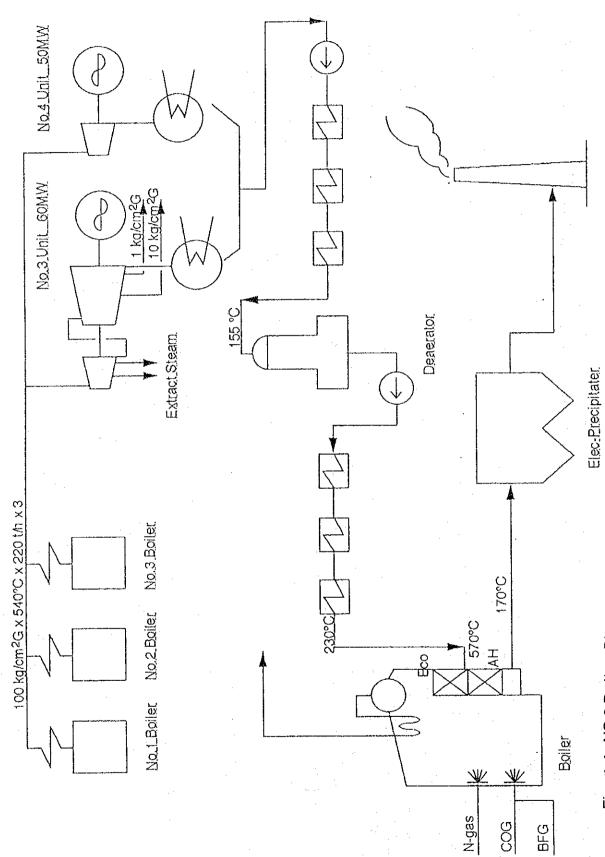


Fig. 4.4 NO.2 Boiler Plant Flow-Sheet

- \* Rehabilitation of furnaces and boilers for insulation and the prevention of cool air from entering.
- \* Rehabilitation of pipes and dusts for insulation and for the prevention of steam, hightemperature gas and air from leakage.
- \* Management of fuel and combustion in furnaces and boilers.

In order to accelerate these devices, the executives and employees are requested to have the consciousness of participating in the campaign for such acceleration.

### b) Countermeasures at the 2nd step

Total amount of energy emitted from iron and steel works as the forms of exhaust gas, exhaust hot water and the sensible heat of intermediate products and others are estimated to account for around 40% of energy consumed in the works. The effective utilization of the exhaust energy is very important not only for reducing costs but also for accelerating environmental protection measures including those in the global point of view.

### 1) For iron-making process

Since energy consumption in iron-making process accounts for around 60% of total energy consumption in iron and steel works, countermeasures for the process is especially important for promoting energy saving. Adopting following devices in order can be recommended if references are made to the experience of rationalization in Japan.

- \* Strengthening the making of the grains of iron ore and coke uniform.
- \* Hi-pressure operation of blast furnace(Pressure at the top of blast furnace is 1 kg/cm<sup>2</sup> G).
- Expansion of the scale of blast furnace
- \* Operation of blast furnace in de-humidity of air injected.
- \* Installation of TPT (top pressure recovery turbine) at blast furnace.
- \* Installation of CDQ (coke dry quenching) at coke oven.

### 2) For steel - making process

The energy of exhaust gas from basic oxygen furnace is the biggest of energies exhausted from this process. This works has already adopted OG (oxygen gas) method to recover the heat of the exhaust gas, but the amount recovered could not be confirmed by Japanese experts. In Japan the enhanced recovery of OG has been intended through improving the skirt of basic oxygen furnace.

3) Improving measuring systems to increase measured items

Investments in facilities and equipments mentioned in 1. and 2. above should be effective in terms of getting return mainly because of high costs. And in order to assess the investments being effective, it is indispensable to grasp detailed and accurate data and to analyze them to evaluate the effect of the investments. In this regard, it seems to Japanese experts that this works should be much better equipped with measuring systems to collect a great number of detailed and precise data.

### c) Countermeasures at the 3rd step

Adopting continuous caster and hot direct rolling contributes substantially to increasing yield and rationalizing production facilities. Lossess in the sensible heat of intermediate products and solids is the largest of losses in exhaust heat in the integrated iron and steel works, and it is reported that the lossess accounts for around 18% of total energy consumption in the works in Japan. To introduce continuous casting and other devices is very effective for energy conservation in the steel works as one of measures reducing the lossess in the sensible heat. It is supposed that the yields of steel products in this works, which has already installed continuous casters, is higher than other works which still installs ingot making process, although specific figures on yields were not obtained during our visit.

### d) Power plants for own use

Since two power plants are supplying all power load in this works, the stable supply of power from these plants should be considered seriously. The power plants are reported to have continued their operation at the load factor of more than 100%. Supposing such situations, following suggestions can be made for No. 2 power plant which was visited by Japanese experts.

### 1) Countermeasures at the 1st step

\* Usual operation of gas turbine generators

Operating power plants at the maximum efficiency at the endof generation results in the largest effect of energy conservation in the plants. Some measures should be adopted for reducing high load at present, and the usual operation of generators (2 units of 27 MW gas turbine generator) installed as emergency use are supposed to be one of realistic solutions in which power plants in the iron and steel works will operate at the maximum

efficiency.

\* Utilization of extract steam of turbine

As mentioned earlier, the extract steam of No. 4 turbine is not utilized at present for un-identified reasons. The utilization of the extract steam can be recommended to increase the efficiency of Rankin cycle.

\* Enhancing the degree of vacuum of condenser

The degree of vacuum of condenser has been reduced for unidentified reasons. Operating value was 0.76 kg/cm<sup>2</sup> abs. at No. 3 turbine, which could be compared with designed value (0.04 kg/cm<sup>2</sup> abs. at No. 3 turbine; 0.035 kg/cm<sup>2</sup> abs. at No. 4 turbine). To investigate the reasons why the degree of vacuum has decreased can be recommended for enhancing the efficiency at the end of generation.

### 2) Countermeasures at the 2nd step

It is supposed that the reduced capability of air cooling tower has caused the reduced degree of vacuum of condenser. If it is the case, increasing the capacity of air cooling tower and improving method of cooling water of condenser will need to be considered and implemented.

### 4.1.3 Countermeasures (Devices) on Electricity Consumption

### (i) Outline of Electricity Consumption

### a) Power generation

This steel works installs two power plants, which are supplying almost all electricity used inside it in recent years. BFG, COG and NG are used as fuels for power generation. The outline of the plants is shown below.

Frequency:

50 Hz

Voltage:

63 kv (No. 1)

230 kv (No. 2)

Capacity:

24 MW (No. 1)

115 MW (No. 2)

Surplus of generated electricity can be sold to the national grid although the sold volume has

been negligible since 1991. The price of selling and buying electricity is 7.5 IR/KWh, and the contracted volume of electricity bought from the national grid is 70 MW.

### b) Power utilization

Annual consumption of electric power is reported about 1,161,000 MWh, the largest part of which is used in oxygen plants (45MW). Six oxygen plants generate 340, 000 m<sup>3</sup> of oxygen per hour. The load factor of the works is very high (about 97%) and its power factor more than 80%. If we use the figure of 2.2 million tons as an annual crude steel production, we can get the figure of 527 KWh per ton as a unit consumption of electricity, which can be compared with 450-480 KWh in Japan.

### (ii) Countermeasures to be Considered

### a) Countermeasures at the 1st step

- 1) Strengthening the management of maintenance and operation
  - \* Electrical equipments and machines should be operated at a proper load because of lower efficiency of conversion from electric power to motive power at lower load.
  - \* The voltage of power sources should be maintained at an appropriate level.
  - \* Lack of lubricant in machines, looseness in belts, etc, should be avoided.
- 2) Installing more efficient lamps in hot rolling mills Converting mercury lamps to sodium lamps in hot rolling mills are estimated to total to 40% saving of electricity.
- b) Countermeasures at the 2nd step
- 1) Managing peak load to improve power factor to more than 90% in each shop by introducing measuring systems.
- 2) Controlling the volume of air flow and water flow by introducing inventer system.
- 3) Effective utilization of nitrogen generated at oxygen plant

As mentioned above, electricity consumption of oxygen plant is the largest in this works. In this plant, electricity is also consumed for generating nitrogen, the volume of which is four-fold of

oxygen generated there and is not utilized at all. Nitrogen can be utilized for cooling, preventing oxidization and others.

### 4.2 Ahwaz Steel Co.

### 4.2.1 Outline of the complex

Ahwaz Steel Co. adopts a direct reduction steel making process, like Mobarakeh Steel Co. which started operation in 1992, and is one of three major steel complexes belonging to NISCO (National Iranian Steel Company) under the control of the Ministry of Metals and Mines, and Isfahan Iron & Steel Complex reported in PR1 is another of the three complexes.

This complex began to be constructed before the 1979 revolution with Swindell Dressler, USA as a consultant, and the construction was suspended by the Iran-Iraq war. In February, 1989, the construction was completed independently by the complex alone, to start production. The outline of the present facilities is shown in Fig. 4.5.

Iron ores and coal for coke making are imported from Brazil, India, Australia, etc. and transported by freight car from Bandar Imam Khomeini port.

The production of blooms and slabs (no mill line) planned to be achieved in FY 1992 (Iranian fiscal year from March 21 to March 20; hereinafter this applies) is 800,000 tons, and that in 1993, 1,0 00,000 tons.

At present, the products are supplied to nearby Kaavian Steel Co., Nasr Steel Co., etc., and because of deficiency in the mill capacity of INSIG (Iran National Steel Industry Group), semi-finished products are exported to China and Germany.

# 4.2.2 Present situation of the factory and energy saving indicators

The present situation of the factory and energy saving indicators are shown in Table 4.2.

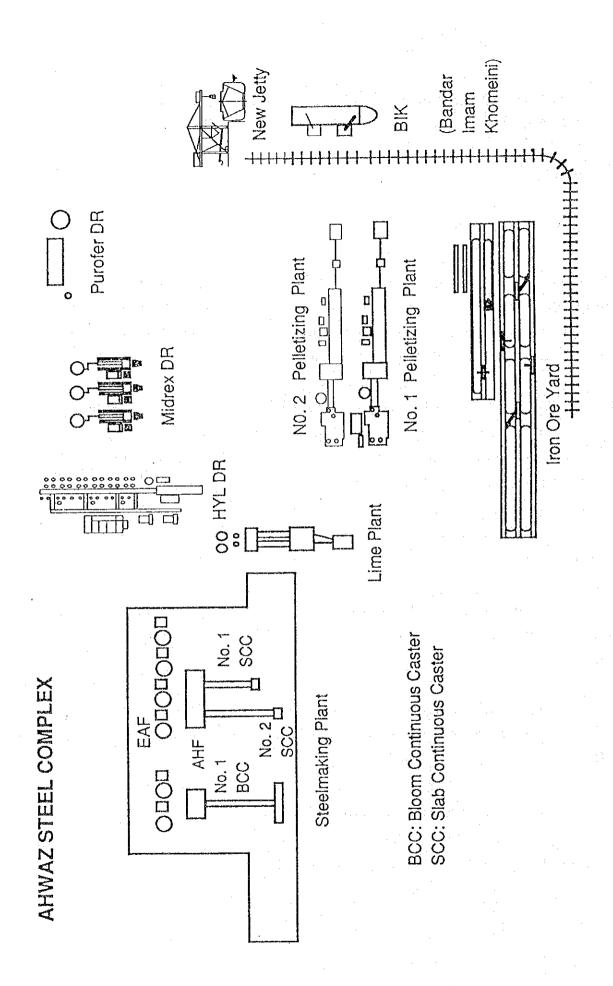


Fig. 4.5 Plant outline of Ahwarz Steel Complex (1)

Table 4.2 Present situation of the factory and energy saving indicators

l Factory			
Total Capacity	$1,500 \times 10^3 \text{ t/Y}$		
Pellet Plant	$2,500 \times 10^3$ pellet-t/Y × 2 plant		
DR Plant (PUROFER)	$330 \times 10^3$ pellet-t/Y × 1 plant		
(MIDREX)	$400 \times 10^3$ pellet-t/Y × 3 plant		
(HYL)	$1,000 \times 10^3$ (3 plant total (U/C))		
Continuous Casting	$1,500 \times 10^3$ product-t/Y (3 plant total)		
Electric Ark Furnace	$1,600 \times 10^3$ product-t/Y (6 plant total)		
Production	804,752 t/Y (1992)		
Name of Product	Bloom, Slab		
Operating Hour	$24 \times 11 \times 30 = 8,000 \text{ h/Y}$		
No of Employee	5,000 P		
No of Engineer	⇒ 300 P		
2 Energy Consumption (1992)			
Natural Gas	286,164,728 Nm³/Y		
Electricity	872,600 MWH/Y		
3 Specific Energy Consumption			
Natural Gas	3.34 Gcal/t		
Electricity	1,084 kWH/t		

### 4.2.3 Energy saving measures

The steel making plant of the complex adopts a direct reducing furnace-electric furnace process as described above, and since the process is not adopted for commercial operation in Japan, it is difficult to compare the specific energy consumption. Compared to the specific energy consumption of a typical direct reducing furnace-electric furnace process shown in Table 4.3, the specific energy consumption of natural gas is somewhat lower, and that of electricity is higher.

Table 4.3 Specific energy consumption of typical DR steel making plant

	DR Plant	Electric Ark Furnace	Continuous Caster	Total
Yield (%)	,	90	95	
DRI Mixing Ratio (%)		85		
Specific Energy Consumption	:			
Natural Gas (Gcal/t)	2.85	0.47	0.47	3.79
Electricity (kWH/t)	130	700	20	850

### (i) Energy saving measures in the 1st step

The energy saving measures by way of intensified equipment maintenance and improved operation are small in the effect of each measure, but their cumulative effect is large as a feature of these measures. Typical measures are enumerated below.

- a) Repair of furnace walls to ensure more perfect heat insulation, and prevention of ingress of cold air into furnaces
- b) Repair of pipes of hot gas, hot air, steam, etc. to ensure more perfect heat insulation, and prevention of leak
- c) More intensive fuel and combustion control of respective furnaces
- d) Prevention of scattering of raw materials and intermediate products
- e) Repair of meters and more intensive numerical control
- (ii) Energy saving measures in the 2nd step

### a) DR plant

A typical energy balance of the field-surveyed Midrex plant is shown in Fig. 4.6. As can be seen from the drawing, large heat loss includes the sensible heat loss of DRI (70.8%), loss due to exhaust gas of top gas (9.6%) and loss due to exhaust gas of combustion gas (9.2%). These waste heat losses amount to 89.6%.

# MIDREX Process Energy Balance

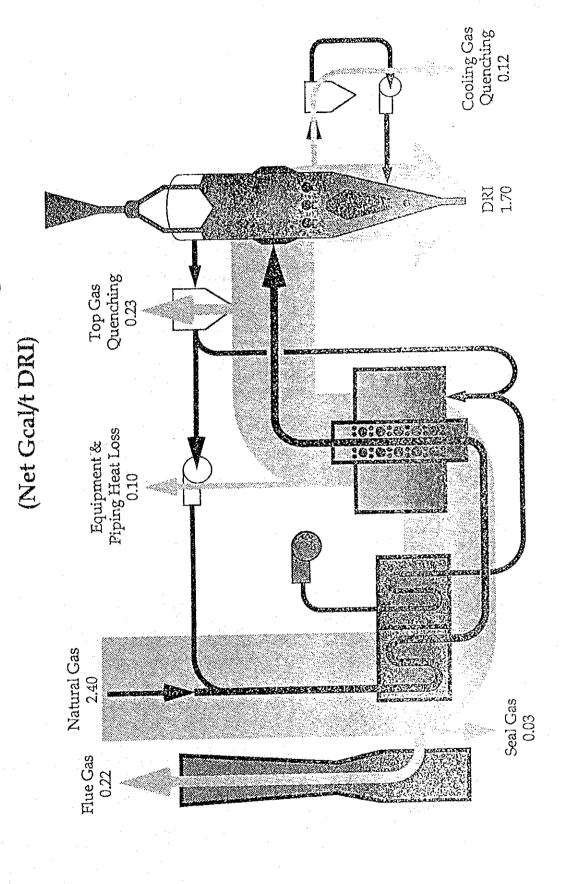


Fig. 4.6 Energy ballance of Midrex Plant (2)

It can be understood that the waste heat must be recovered more perfectly.

### b) Electric furnaces

The electric furnaces of this complex are relatively large in capacity, and are relatively modernized, being provided with continuous casters, Flicker compensator system and preheating equipment by natural gas. The consumption in FY 1992 was 710.8 kWH per ton of molten steel.

Simple comparison with the consumption by electric furnaces in Japan cannot be made, since scraps are used as the raw material in Japan. Anyway, the specific electric energy consumption in the Japanese electric furnace steel making industry in 1990 was 515 kWH per ton of products as a mean of the whole country, and the lowest consumption reported was 340 kWH per ton of products.

Among the improvement measures taken for lessening the energy consumption in Japan, typical energy saving measures surmised to be effective for equipment improvement and waste heat recovery in the electric furnaces of the complex are enumerated below.

- 1) Oxygen enriching equipment
- 2) Preheating of scraps by the exhaust gas of electric furnaces
- 3) Adoption of water-cooled furnace walls (adoption rate in Japan: more than 75%)
- 4) More perfect sealing at the openings of preheating furnaces and electric furnaces

  Most of these measures greatly contribute to not only energy saving, but also to dissolution
  speedup, quality improvement and productivity enhancement.

### c) Electric equipment

The iron industry uses large-capacity blowers and pumps. If their rotational speeds are controlled, the consumption of electric energy can be very effectively decreased.

### (iii) Energy saving measures in the 3rd and 4th steps

### a) DR plants

The sensible heat loss of DRI at DSR plants is very large, as described above. It is recommended to examine the direct supply of DRI into the electric furnaces since it is one of very effective measures.

### b) Mills

The complex does not have any mill as described above. The installation of mills can make substantially a consistent steel making factory. This should be studied preferentially from a comprehensive viewpoint of increasing the production capacity of rolled steels, reducing the transport cost, etc. This will of course greatly contribute to production enhancement and quality improvement, with a resultant large contribution to energy saving.

### c) Electric power supply

The electric power supply to the complex is being improved recently, but the shortage of power supply in the summer peak season compels them to curtail their operation. In addition to existing two 2.5 kVA diesel generators, they are installing additional two 2.5 MW gas turbine generators in preparation for service interruption. Electric power plants are being constructed one after another for ensuring stable power supply which is a problem to be solved before talking about energy saving measures.

### d) Utilization of scraps

The utilization of scraps as a raw material for the electric furnaces is very low. The establishment of a scrap recovery system for using more scraps will greatly lower the specific electric energy consumption of the electric furnaces. The raw material for steel making by electric furnaces in Japan is scraps, and their specific energy consumption is as described before. The utilization of scraps is needless to say preferable also in view of the re-utilization of resources. In Japan, the scrap utilization accounts for about 35% in the raw materials of steel making, and the recycling rate of steel cans reaches 50%.

### 5. Power Station

### 5.1 Montazer Ghaem Power Station

### 5.1.1 Introduction

This power station is located in Shahriyar region to the south-west of Tehran. An agreement on installing steam units was concluded in 1967 between Iranian Ministry of Energy and General Electric Company of the U.S.A. No. 1 and No. 2 units of generator were commissioned in 1972 and No. 3

and No. 4 in 1974 (156 MW for each). A gas turbine unit (24 MW) was also constructed. The construction works of 6 gas turbines (116 MW for each) as parts of combined cycle power plants are under way with two of them having already been commissioned. The construction of 6 steam turbines as parts of the plants are planned although no contracts on the construction have been made yet.

This station owned by Tavanir, state-owned electric power generation and transmission company under the Ministry of Energy, is supplying electricity to Tehran area together with four other power stations located in the area. In addition to these power stations, electricity is supplied to Tehran area by other stations including hydro and thermal ones in Esfahan, Tabriz and other places.

Table 5.1 shows the outline of operation in this power station.

### 5.1.2 Countermeasures (Devices) on Heat Consumption

### (i) Outline of Heat Consumption

Indicators for considering countermeasures for promoting energy conservation in this power station are shown in Table 5.2.

### (ii) Countermeasures to be Considered

### a) Countermeasures at the 1st step

### 1) To enhance total heat efficiency

Heat efficiency at the end of generation was reported to be 35 - 36% when Japanese experts visited the station. The efficiency at the end of transmission was not identified, but it was reported that own use of electricity is about 6% for each generator and about 7% for the power station. All of steam pressure at the outlet of boiler heater (1,750 p s i), steam temperature at the same outlet (990°C), and vacuum degree of condenser (23 inch-Hg..... 11.7 inch. Hg-a b s) were observed to be lower than planned ones while figures on heat efficiency at planning stage were not given. And it was explained that the operation of boilers had been conducted at lower pressure and temperature than planned ones because of the water tube of the boilers being corroded, but the cause of decreased degree of vacuum could not be confirmed.

Table 5.1 Outline of Boilers and Generators in Montazer Ghaem Power Station

1	Boiler	
	Type	Natural circulating one drum
		water tube boiler
	Maker	CE (USA)
	Normal working steam pressure(SH outlet)	1,875 psi
	Normal working steam temp'(SH outlet)	1, 005 °F
	Continious maximum evapolation	1, 100, 000 lb/h
	Reheater steam temperature(RH in/outlet)	688/1.005 °F
	Reheater steam flow rate	988,000 lb/h
	Air heater air temperature(AH in/outlet)	635/311 °F
	Heavy fuel oil	77,800 lb/h
	Thermal efficiency (planning)	90.57 %
<u> </u>	Feed water treatment	Demineralizer
2	Turbo-generater	
	Type	Tandem-compound type δ stage
		extract condencing unit
-	Waker	GE (USA)
	Turbine revolution	3,000 rpm
	Voltage	15 k v
	Output	176.471 mvA
	Cycle	5 0 H z
	Condenser cooling type	Air cooling tower type
	Condenser vacume	2.5 inch Mg-abs
	Generater cooling type	H₂ gas c∞ling type

Talle 5.2 Indicators on Energy Consumption in Montazer Gheam Power Station

Total generated power(1991)	3, 643, 966 mwh/Y
Peak lord	= 700~750 mw
Vean lord	⇒ 500~6.00  "
Power consumption for plant	6~7 %
Operating hour	365×24 h/Y
Operating ratio(mean in 1991)	70.29 %
Total fuel consumption(1991)	857,000 k1/Y
Heavy fuel oil	
Specific gravity	0.9641
Lower calorific value	9,695 kcal/kg
Fuel cost	

The decreased pressure, temperature, and vacuum degree are considered to have a negative effect on the heat efficiency at the end of generation. To increase them to at least planned levels can be recommended for enhancing the heat efficiency.

Corresponding figures in power stations in Japan, which install around the same scale of generation units and operate in around the same condition of steam, are as follows.

\* Heat efficiency (at the end of generation) 38.15%

\* Heat efficiency (at the end of transmission) 35.74%

\* Own use of electricity 5.70%

### 2) To control boilers' heat efficiency

Heat efficiency of boilers was reported to be 90%, around the same as that of planning stage. Following devices, however, can be suggested for strengthening the management of maintenance and operation of boilers.

- \* Control of fuel usage (fuel's temperature in particular)
- \* Low oxygen combustion for reducing exhaust gas
- \* Controlling water quality
- \* Preventing steam, combustion gas and air from leakage
- Controlling the blow of boiler water
- Preventing heat transfer surface from being soiled and corroded

### 3) Relating to turbine

Soiling of cooling pipe at condenser, decreased capability of ejector and cooling tower, and air leakage are considered to be main causes for the decreased vacuum degree of condenser. Countermeasures for coping with these items should be taken for increasing heat efficiency in this power station.

# 4) Measuring and monitoring data

It was observed that automatic control and measuring instruments in a monitoring center in the power station were well equipped. Detailed measurements, however, seemed not to be conducted there. In Japan, data including heat efficiency are measured and managed at least to one place of decimals every hour. If heat efficiency drop by 0.1%, increase in fuel consumption will be 309 tons of heavy fuel oil per annum for each unit of boiler and generator in this station. This figure implies that control in power stations should be conducted through utilizing detailed

and reliable figures.

- b) Countermeasures at the 2nd step
- 1) Conversion of boiler fuel from heavy fuel oil to natural gas. This power station is planning to convert its fuel from heavy fuel oil to natural gas. Such conversion is important for preventing heating surface from being soiled and corroded as well as for environmental protection.
- Establishing auxiliary heat surface in boilers
  Establishing auxiliary heat surface in boilers will increase boilers' heat efficiency because the dew point of exhaust gas from natural gas is lower than that from heavy fuel oil.
- 5.1.3 Countermeasures (Devices) on Electricity Consumption
- (i) Outline of Electricity Consumption

As mentioned above, own use of electricity is about 6% for each generator and about 7% for the station as a whole. When Japanese experts visited the station, it was observed that 8 MW was used for own use at No. 3 generator the output of which was 80-90 MW. These figures can be compared with 5.7% in Japan.

(ii) Countermeasures to be Considered

Rehabilitation or more efficient operation for reducing own use of electricity (at the 1st step)

- 6. Oil Refinery
- 6.1 Tehran Oil Refinery
- 6.1.1 Introduction

Tehran Oil Refinery, which composes of No. 1 (South) and No. 2 (North) refineries, is located

south of Tehran city. The former was constructed in 1967 and the latter in 1974. Total refining capacity is 220,000 b/d at present.

# 6.1.2 Countermeasures (Devices) on Heat Consumption

### (i) Outline of Energy Consumption

Gas and oil are used as fuel for heating furnaces and boilers in this refinery. Fuel gas used here is a mixture of stabilizer off-gas, isomax off-gas, hydrogen off-gas, platformer off-gas, and natural gas which is supplied through national pipeline network when needed.

Fuel oil is a mixture of furfural extract, vacuum residue, visbreaker bottom, waste oil, etc...

It was observed that furnaces in process units and boilers were not installed with any devices such as economizer and air pre-heater for recovering heat from high-temperature exhaust gases.

Accordingly, heat efficiency of many furnaces is estimated to be 60-70%, which can be compared with the appropriate level of more than 80%. In addition, some of furnaces; have not installed any instruments for controlling excess air and the instruments in others are not in services.

Typical examples of exhaust gas temperature are as follows:

No. 1/No. 2 Crude furnace	900	°F
Vacuum furnace	900	°F
Platformer furnace	1,400	°F
Boiler plant	500-700	°F

Demand for electric power is satisfied with supply from auto-generation in this refinery. Exceptionally, a part of generated power there is being supplied to neighboring NIOPDC's deposit for heating tank. No. 1 and No. 2 refineries have a power plant respectively, the generation capacity of which is 21.6 MW (7.2 MW \* 3), although an integrated operation of two plants are conducted.

Four units of boilers (320,000 Lb/h for each) are installed in No. 1 refinery and three units (the

same as in No. 1) in No. 2.

According to the refineries' record, internal use and loss of energy is 7.2% in terms of crude oil input in January, 1993, in which 5.8% is accounted for by fuel uses and 1.4% by losses. The standard ratio of internal use and loss is estimated 4.5% for the similar type of refinery.

### (ii) Countermeasures to be Considered

A committee for energy conservation has already been established for a few years in this refinery, according to the instruction of Refinery Expansion & Development Center of NIOC. 3-4 projects for implementing energy saving are reported to have been at their construction steps and some on application for construction. All of countermeasures mentioned below including setting air pre-heater system might have been seriously considered in the refinery.

- a) Countermeasures at the 1st step
  - Rehabilitation of pipes and other parts for insulation
  - Proper management of excess air control for combustion
- b) Countermeasures at the 2nd step
  - Installation of economizers and air pre-heaters in furnaces and boilers

### 7. Others

### 7.1 Kaavian Steel Co.

### 7.1.1 Outline of the complex

Kaavian Steel Co. is located in Ahwaz, being a national factory belonging to the above Ahwaz Steel Complex. The construction started in 1976, and the operation started in 1980 but suspended by the Iran-Iraq war. Six years ago, re-construction started, and was completed four years ago. Operation was resumed one and a half years ago.

The factory is engaged in the hot rolling of the slabs (250 \* 1200 \* 4000 mm) and blooms (85

to 130 mm t) mainly supplied from Ahwaz Steel Complex, and produces slabs, blooms and plates of 8 to 40 mm in thickness.

They produced 109,000 tons in 1992, and plan to produce 400,000 tons in 1993 and 800,000 tons/year two years later. However, since their products are not officially qualified, the sales are rather poor, to lower the operation rate.

### 7.1.2 Present situation of the factory and energy saving indicators

The present situation of the factory and energy saving indicators are shown in Table 7.1.

Table 7.1 Present situations of the factory and indicators concerned

1	Factory	
	Total Capacity	800,000 product-t/Y
	Slab	400,000 product-t/Y
	Bloom	300,000 product-t/Y
	Plate	100,000 product-t/Y
	Furnace Capacity	120 t × 1 plant, 150 × 1 plant
	Production (1992 actual)	109,000 product-t/Y
	Name of Product	Slab, Bloom, Plate
	Operating Hour (1992 actual)	5,300 h/Y
	No of Employee	960 persons
	No of Engineer	60 persons
	Yield	= 90%
2	Energy Consumption (1992)	
	Natural Gas	21,462,851 Nm <sup>3</sup> /Y
	Gas oil	95,903 kg/2 months
	Electricity	10,469,732 kWH/Y
3	Specific Energy Consumption	
	Fuel	1.92 Gcal/t
-	Electricity	96.05 kWH/t
		<u></u>

### 7.1.3 Energy saving measures

There is no appropriate factory comparable to this factory in Japan. For reference, a specific

heat energy consumption of about 0.32 Gcal/t was achieved in Japan for heating cold billets only in a converter steel making-hot rolling process. Compared to the value, the above consumption is very high.

### (i) Energy saving measures in the 1st step

As described also for Ahwaz Steel Complex, essential energy saving measures by intensified equipment maintenance and improved operation are as enumerated below.

- a) Repair of furnace walls to ensure more perfect heat insulation, and prevention of ingress of cold air into furnaces
- Repair of ducts of hot gas, hot air, etc. to ensure more perfect heat insulation, and prevention of leak
- c) More intensive fuel and combustion control of respective furnaces
- d) Repair of meters and more intensive numerical control

A further other cause for the high specific heat energy consumption of the factory is surmised to be a low operation rate. The fuel consumption required for the start-up of the heating furnaces and the fuel consumption required for keeping the internal temperature of the furnaces remaining out of operation are large.

### (ii) Energy saving measures in the 2nd step

### a) Heating furnaces

The heating furnaces have recuperators installed for recovery of waste heat, and the outlet temperature of the exhaust gas is 800°C at the highest and on the level of 300°C normally. It is recommended to use the exhaust gas for preheating the steel, and this will also contribute to the improvement of product quality.

### b) Electric equipment

This factory uses various blowers and pumps including the large-capacity blowers for the heating furnaces. If their rotational speeds are controlled, the consumption of electric energy will be very effectively reduced.

### (iii) Energy saving measures in the third stage

This factory is an intermediate product factory relying on other factories working upstream and downstream, unpreferably in view of factory management. This situation of course greatly affects the operation rate. A fundamental study in this regard is required.

## 7.2 Khuzistan Pipe Manufacturing Co., Ltd.

### 7.2.1 Outline of the factory

The factory is located in Ahwaz, being a private factor which produces 45,000 tons/year (target of 1993) of cast steel pipes of ductile cast iron and gray cast iron for city water and drainage, and also various joints (in conformity with DIN and ISO), using 50% of scraps and 50% of pellets (imported from Brazil) as raw materials.

### 7.2.2 Present situation of the factory and energy saving indicators

The present situation of the factory and energy saving indicators are shown in Table 7.2.

Table 7.2 Present situation of the factory and indicators concerned

1 Factory	Maria de la companya
Total Capacity	~ product-t/Y
Electrical Induction Furnace	2.5 MW × 3 line
Holding Furnace	750 kW × 1 set, 350 kW × 1 set
Annealing Furnace	~×1 line
Casting Plant	3 line
Production (1993 target)	45,000 product-t/Y
Name of Product	Cast Iron Tube & Fitting
Operating Ratio	74%
Yield	83%
No of Employee	1,200 persons
No of Engineer	15 persons
Electric Capacity	16 MW
2 Energy Consumption (1992)	
Natural Gas	~ Nm³/Y
Gas oil	~ kJ/Y
Electricity	~ kWH/Y
3 Specific Energy Consumption	
Fuel	~ Gcal/t
Electricity	~ kWH/t

Note: The value of mark (~) are filed by the report after given by the factory.

### 7.2.3 Energy saving measures

The factory is a casting factory using electric induction furnaces only as stated above, and we have no factory of this type in Japan. The casting of this scale is effected by a cupola.

### (i) Energy saving measures in the 1st step

The energy saving measures in the first stage are taken by intensifying equipment maintenance and improving operation. Typical measures are enumerated below.

a) Repair of furnace walls of electric induction furnaces and annealing furnace to ensure more

perfect heat insulation, and prevention of ingress of cold air into furnaces

- b) More intensive fuel and combustion control of annealing furnace
- c) Shortening of waiting time in process
- d) Repair of meters and more intensive numerical control
- (ii) Energy saving measures in the 2nd step

The first step of energy saving measures is to identify the present conditions. This is the reason why measuring instruments for energy control must be installed. This is a problem common to equipment in general.

### a) Annealing furnace

- 1) The waste heat temperature of the annealing furnace is estimated to be on the level of 300 to 500°C, though not confirmed because of no measurement made. The preheating of cast iron pipes by the exhaust gas is effective not only for energy saving but also for product quality improvement. The identification of the present conditions, numerical analysis and examination of economic values are surmised to be necessary. The heat recovery for preheating combustion air is one of relatively easy waste heat recovery methods.
- 2) Improving the sealing structure at the portion where cast iron pipes are inserted is also effective for energy saving as well as for product quality improvement. The examination of this item is surmised to be as valuable as that of the above item.
- b) Electric equipment

This factory uses various blowers and pumps. If their rotational speeds are controlled, the consumption of electric energy will be very effectively decreased.

- (iii) Energy saving measures in the 3rd step
- a) Electric power supply

At present, electric power supply is unstable (service interruption occurred for 1,360 hours in 1992). So, in addition to two existing 2 MW emergency diesel generators, two 2.5 MW gas turbine generators were ordered and are scheduled to be installed six months later in preparation

for service interruption. It is recommended to examine the additional installation and constant operation of gas turbine generators, based on the economic effect analysis in reference to power loads, power cost reduction effect, drop of factory operation rate due to decreased production, etc. This will also enhance energy saving.

### b) Utilization of scraps

Scraps account for 50% of the raw materials at present, and the supply from a scrap collection company under the control of the Ministry of Heavy Industry is said to be stable. It is recommended to examine measures for stabilizing the quality of scraps and to increase the utilization of scraps. This contributes to not only energy saving but also the recycling of resources.

### 7.3 Bafkar Textile Co.

### 7.3.1 Outline of the factory

The factory is located in Teheran and is one of four largest national factories belonging to the Ministry of Industry. It began to be constructed as a joint concern of an American company and the Iranian government in 1937, and started operation in 1958, being managed under the American company till 1969.

The raw cotton and chemical fibers used are 100% domestic products, and the dyes are imported from Germany, France, China and India. It is a consistent factory consisting of the steps of spinning, weaving, bleaching, dyeing and textile finishing, and produces various printed fabrics. (The share of the products is about 2%.)

At present, they produce 3,520 tons/year (22,000,000 m<sup>2</sup>/year). They are modernizing the spinning step and changing the exhaust gas treatment in the spinning step from open type to closed type (the rate of recovering raw cotton from the exhaust gas will be 80%), and after completion of the improvement, they will increase the production to 4,300 tons/year.

They have filed an application for the permission to move the dyeing line to Zanjan at about 400 km in the west-northwest of Teheran within 5 years. This decision is said to have been triggered by

the request from the municipal government, which requires additional investment for the treatment of their waste water. (They can receive a subsidy of seven million US dollars and will be exempted from tax for 10 years if they take any environmental protection measure in conformity with the regulations of the Ministry of Industry.)

### 7.3.2 Present situation of the factory and energy saving indicators

The present situation of the factory and energy saving indicators are shown in Table 7.3.

Table 7.3 Present situation of the factory and indicators concerned

l Factory	
Production	$22,000 \times 10^3$ product-m <sup>2</sup> /Y
	3,520 product-t/Y
Name of Product	Textile (print)
Operating Hour	$275 \times 24 = 6,600 \text{ h/Y}$
No of Employee	2,000 persons
No of Engineer	45 persons
2 Energy Consumption (1991)	
Natural Gas	35,640,000 Nm³/Y
Gas oil	150,000 I/Y
Electricity	31,680,000 kWH/Y
3 Specific Energy Consumption	
Fuel (oil equivalent)	10,441 i/t
Electricity	9.0 kWH/kg

### 7.3.3 Energy saving measures

Among textile products, especially clothing is highly fashion-oriented and seasonal. So a textile factory high in the production ratio of clothing like this factory is forced to produce many items in respectively small amounts, and as a result, is poor in efficiency in view of energy consumption. In addition, a factory with steps of bleaching, dyeing and textile finishing is higher in the fuel cost proportion in the production cost than factories of other categories.

Also in Japan, the textile industry engaged in the weaving of short-fibers of cotton and chemical fibers and dyeing & textile finishing recorded the following average specific energy consumption rates in three years till 1990.

- Specific heat energy consumption: 1280.1 l/t (in terms of fuel oil)
- Specific electric energy consumption: 6.13 kWH/kg

The factory is very large in specific heat energy consumption, since it has a history of about 35 years as stated before. The specific electric energy consumption is also large, though not so large as the specific heat energy consumption.

### (i) Energy saving measures in the 1st step

The energy saving measures in the first stage are taken by intensifying equipment maintenance and improving operation. Main measures are enumerated below.

- a) Prevention of leak of steam, condensate, hot water, compressed air, etc.
- b) Repair of hot pipes and hot ducts to ensure more perfect heat insulation
- c) More intensive fuel and combustion control of boilers, direct fire type dryers, etc.
- d) Repair of walls and prevention of ingress of air of boilers, direct fire type dryers, etc.
- e) More thorough decrease of hot waste water
- f) Repair of meters and more intensive numerical control
- g) Decrease of re-processing and failure of cloth
- h) Decrease of waiting time in process

Many cylinder dryers are operated in this factory, and the heat balance of such a cylinder dryer is shown in Table 8. Water evaporation of cloth and radiation loss account for a large percentage. The recovery and re-utilization of the heat is being developed in Japan, but is substantially difficult. The next large heat loss item is the leak of steam at the joint of cylinder rotary portion and at the steam trap. This steam consumption can be positively decreased by intensifying the maintenance.

### (ii) Energy saving measures in the 2nd step

The energy saving measures in the second stage accompany equipment investment for recovery

of waste heat, etc.

For proper judgment of investment, as shown in Table 8, it is first of all necessary to accurately numerically identify and analyze the supplied energy, effective heat energy, discharged energy and present temperature level for each step of the process. This is the reason why measuring instruments are required.

Table 7.4 Heat balance of cylinder dryer

Item	%
Water evaporation of cloth	38.2
Radiation loss	23.7
Leak of steam at joint and trap	17.6
Loss due to pause	11.5
Others	9.0
Total	100.0

Also for this factory, it is recommended to install energy control instruments and to intensify the numerical control based on the instruments.

### a) Spinning

More than 90% of the energy consumed in this step is electricity, and in the electric energy consumption, cotton and dust collectors account for more than 60%. In the factory, the equipment are being modernized as described before, and it is recommended to introduce rotational speed control for suction fans.

### b) Dyeing and processing

# 1) Recovery and effective utilization of steam drain

All the steps of bleaching, dyeing and textile finishing use heat energy consuming apparatuses, with much waste energy discharged from them. The waste energy includes the exhaust gas from dryers, hot waste water from washing machines and dyeing machines, the heat due to radiation and steam drain generated from the liquid surfaces of washing tanks and hot water

storage tanks, etc.

Especially cylinder dryers, washing machines, dyeing machines, heat setters and steam pipes discharge condensates of various pressures and temperatures. They should be positively used for boiler feed, flush steam, etc.

### 2) Heat recovery from hot waste water

As important as the recovery and effective utilization of steam drain as an energy saving measure in the dyeing and processing step is the heat recovery from the hot waste water generated in large quantities by washing and dyeing. It is recommended to use plate type heat exchangers, etc. for cascade utilization of heat, and to use heat pumps for utilizing hot waste water at a higher temperature.

### c) Boilers and generators

The factory has two 3,000 kVA condensate turbine generators and one 1,250 kVA diesel generator for emergency in preparation for unstable electric power supply, but the condensate turbine generators are little used since they are superannuated.

The dyeing and processing step uses a large amount of steam for various heat sources and hot water production as described before. This factory has the following boilers.

- Water tube boiler for power generation: 41 kg/cm<sup>2</sup> \* 360°C \* 16 t/h \* 2 units
- Fire tube boiler: 6 kg/cm<sup>2</sup> saturated \* 4 units
- Flue and smoke tube boiler: 135 lb/in<sup>2</sup> saturated \* 4 units

Normally, low pressure boilers are operated (56 t/h in the rated quantity of evaporation by 7 units), using natural gas as the fuel.

For the fire tube boilers and flue and smoke tube boilers now in operation, it is recommended to more thoroughly recover the drain for utilization for feed, and also to more thoroughly recover heat from the exhaust gas as described before.

### (iii) Energy saving measures in the 3rd step

### a) Dyeing and processing

In Japan, jet streaming type dyeing apparatuses and economical dye liquor applicators are introduced already as novel energy saving type dyeing equipment. As of 1991, 225 units of the former (adoption rate 16%) and 41 units of the latter (adoption rate 9%) are introduced for contribution to rationalization of production. However, since they are very expensive for

investment, production scale, marketability of products and funding plan must be examined as well as technical aspect. For example, available for this approach are the wince type dyeing machines different in performance such as liquor ratio as shown in Fig.7. 3.

Furthermore, making the flow in the dyeing and processing step continuous, allowing production of many kinds in respectively small lots, speed-up, enhancement of product yield, etc. are rationalization measures which also remarkably affect energy saving.

In the current construction of a new factory for dyeing and processing, it is expected that these matters are sufficiently taken into account in addition to simply renewing the existing superannuated apparatuses.

### b) Boilers and generators

The heat efficiency of the existing fire tube boilers is considered to be as very low as less than 60%. This problem is surmised to be solved by the new boilers installed in the new factory, as in the above case.

	· ·			
Туре	Wince	Liquor flow type wince (winpact)	Liquor flow type wince (dash line)	Liquor flow type wince (super flow)
Textile velocity	60 m/min	80 m/min	80 m/min	210 m/min
Liquor circulating cycle	<del></del>	60 sec	30 sec	20 sec
Liquor ratio	1:20	1:15	1:10	1:5
Productivity	1 revolution/D	2 revolutions/D	2 revolutions/D	4-5 revolutions/D

Fig. 7.3 Characteristic value of Wince Type Dyeing Machines (3)

# III. Materials on "Energy and Environment"

- 1. Unit Conversion Factors and Emission Factors
- 2. Parameters for Emission Estimation(1~4)
- 3. Estimation of Energy Balance Table with Forecast to 2021(1~6)
- 4. Estimation of Emission Volumes by Use of Energy Balance Table(1∼8)
- 5. Selected Ambient Quality Indicators for Various Cites in the World(1~3)
- Comparison of Pollutant Emission Level in the World(1~7)
   (Source: OECD, 1993, and others)
- 7. Effectiveness of Countermeasures for Environmental Improvement
- Environmental Administration in Japan
   (Source: Environmental Agency, Japan, 1989)
- Institutional Mechanism for Financing Environmental Administration in Japan
   (Source: Michio Hashimoto, "Development of Environmental Policy and Its Institutional Mechanism of Administration and Finance, 1985)

# 1. Unit Conversion Factors and Emission Factors

	Unit	TOE	BOE	GJ	1000 Kcal	TOE/ton
Crude Oil	KI	0.890	6.289	37,179	8,882	1.000
Gasoline	KI	0.780	5.525	32,657	7,801	1.070
Jet Fuel	KI	0.860	6.063	35,839	8,562	1.065
Gas Oil	KI	0.870	6.190	36.593	8.742	1.035
Fuel Oil	KI	0.920	6.502	38,435	9,182	0.960
Gas	1000 m3	0.880	6.198	36.635	8,752	
Coal	Ton	0.625	4,356	27,214	6,501	
Fuel Wood	Ton					

After JICA's Energy Balance of IRAN

	SOx Emission (SO2 equivalent)		S Content %wt. @IRAN	Avg. SO2 Emission		
Crude Oil	20 x 5%	*0.46 x S%	kg/ton	3	20	0.46 kg/ton
Gasoline	20 x S%	•	kg/ton	008 - 0.10	1.8	kg/ton
Jet Fuel	3.2		kg/ton	0.005 - 0.01	3.2	kg/ton .
Gas Oil	20 x S%	•	kg/ton	0.8 - 1.0	18	kg/ton
Fuel Oil	20 x S%		kg/ton	3.0 - 3.5	65	kg/ton
Gas	0.0092		kg/1e10cal		0.0092	kg/1e10ca
Coal	15.5 x S%	•	ka/ton	. 2	31	kg/ton
Fuel Wood	0.86		kg/toe	·	0.86	kg/toe
		:@Refinery			@	Refinery

\*:@Refinery After The Science and Technology Agency, Government of Japan

NOx Emission F	actor	Unit: kg/ton					·	
	Refinery	Power Gen.	Industry	Air Trans.	Road Trans.	Other Trans.	Residential	Agric. & Commercial
Crude Oil	0.24	7.24	5.09			5.09	1.70	3.05
Gasoline		16.71	16.71	16.71	31.7	16.71	16.71	16.71
Jet Fuel				10.50				4.3
Gas Oil		27.37	9.62	54.13	27.4	54.13	3.21	5.77
Fuel Oil		10.00	5.84	54.13	27.4	54.13	1.95	3.50
Gas *		4.40	2.24			2.24	1.57	1.57
Coal	j	9.95	7.50			7.50	1.88	3.75
Fuel Wood * *			00.0				6.00	

<sup>\* ;</sup> kg / 1e10 cal. \*\* ; kg/ toe

After The Science and Technology Agency, Government of Japan

CO2 Emission	Factor	
Crude Oil	3,165	ton/ton
Gasoline	3,132	ton/ton
Jet Fuel	3.157	ton/ton
Gas Oil	3.187	ton/ton
Fuel Oil	3.219	ton/ton
Gas	2.31E-04	g-CO2/cal.
Coal	3.905	ton/toe
Fuel Wood	4.366	ton/toe

After The Science and Technology Agency, Government of Japan

Emission Factor	for "Other Fo	uel"	Unit: kg/TOE	•				
	Relinery	Power Gen.	Industry	Air Trans.	Road Trans.	Other Trans.	Residential	Agric, & Commercial
SOx kg/loe	0.86	0.86	0.86	0.86	0.86	0,86	0.86	0.86
NOx kg/toe	6	6.00	6.00	6.00	6.0	6.00	6.00	6.00
CO2 Ton/toe	4.366	4.366	4.37	4.366	4.366	4.366	4.37	4.366

# 2. Parameters for Emission Estimation (1)

10	1 74		T			
[Pup, and GDP; World Table '92 IRAN]	7978	1971	1972	1973	1974	1975
Population (NEC	28,429,008	29,300,000	30,213,008	31,167,008	32,164,000	33,206,00
GNP per capita (USS, curr. pr.)  Gross National Product (local,curr. pr.)	798,199,971,840	430 968,199,962,624	510	690	950	1,32
	891,100,104,192	1,014,300,016,640	1,235,000,229,888 1,264,400,203,776	1,836,399,460,352	3,079,400,325,120	3,497,399,418,88
Gross Domestic Product (local; curr. pr.) GDP Deflator (1987 = 100, index)	834,100,104,192	1,014,50,010,010	1,204,400,203,776	10200,000,1	3,089,900,765,184	3,512,100,451,40
GDP Deflator (1985=100,index)		10	. 11	10	16 22	2
Gross Domestic Product (local, 1985, pr.)	10,184,761,784,899	10,405,126,363,723			14,026,981,637,807	14,364,168,140,41
<u> </u>	10,10 ,1101,3 , 11,122	101100111010011100	11,111,1115,015,510	15,504,125,110,305	11,020,301,037,007	14,504,140,140,41
[Pop. and GDP; Prepared by IRANIAN Counterpart]	1970	1971	1972	1973	1974	1975
Population	N/A	29,499,000	30,286,000	31,089,000	31,951,000	32,818,00
Gross Damestic Product (local, 1982 pr.)	N/A	7,045,500,000,000	8,201,900,390,625	8,956,299,804,688	9,342,700,195,313	9,227,799,804,68
Gross Domestic Praduct (local, current pr.)	N/A	902,700,012,207	1,130,199,951,172	1,678,800,048,828	2,986,500,000,000	3,302,500,000,000
	<del></del>			······································		
[Primary Energy Requirement]						
;Energy Balance Table , H. KIBUNE '93	1970	1971	1972	1973	1974	1975
Solid Fuel (MM bbl Oil Eq.)	1.40	1.60	2.50	4.20	4.60	8,4
Petrolcum (MM bbl Oit Eq.)	, 84.36	89.99	93.16	117.02	133.65	155.5
Natural Gas (MM bbl Oil Eq.)	10.34	13.01	15.24	19.88	20.05	21,6
Hydro (MM bbl Oil Eq.)	2.60	4,20	5.50	4.40	5.30	5,4
Othres (MM bbl Oil Eq.)	21.50	20.49	19.37	18.97	17.85	17.2
Non-Comm. (MM bbl Oil Eq.)	4.00	3.80	3.70	. 3.50	3.40	3.40
Primary Energy Requirement Total (MM bbl Oil Eq.)	124.20	133.09	139.47	167.97	184.85	211.6
Francisco Olico Other 1979 1976 Person In	1010	70.4.	10.77	10-1		AC
[Flare Gas; OPEC, (Value 1970-1976; Estimated)]	1970	1971	1972	1973	197-1	1975
Flared Natural Gas (M3)	18,574,000,000	22,021,000,000	24,367,000,000	28,431,000,000	29,210,000,000	25,953,000,000
Flated Natural Gas (MM bbl Oil Eq.; 6.198 BOE/1,000M3)	115.12	136.49	151.03	176.22	181.04	160.86
[CO2 Emission Est. ; JICA Team '93]	1970	1971	1972	1973	10+4	10.75
CO2 Emission Estimation (CO2 million ton)	44.66		<del></del>		1974	1975
Total CO2 Emission Estimation (Carbon million ton)	12.18	46.57 12.70	49.75 13.57	58.10	62.98	71.83
Total one charged Strengered Consultation (only	12.10	12.70]	13.37	15.84	17.18	19.59
[CO2 Emission from FLARE GAS; JICA Team '93]	1970	1971	1972	1973	1974	1975
Cal. Value Flate Gas (cal.) @8752 Kcal/M3	1.63E+17	1.93E+17	2.13E+17	2.49E+17	2.56E+17	2.27E+17
CO2 from Flare Gas (CO2 million ton) @0.0002312 g-CO2/eal	37.58	44.56	49.31	57.53	59.11	52.51
CO2 from Flate Gas (Carbon million ton)	10.25	12.15	13.45	15.69	16,12	14.32
(SOx Emission Est. by Fuel; JICA Team '93)	1970	1971	1972	1973	1974	1975
Solid Fuel	0.0100	0.0114	0.0178	0.0299	0.0327	0.0342
Petroleum	0.252	0.264	0.277	0.346	0.380	0.460
Gas	0.000000827	0.000002092	0.000004994	0.000010758	0.000013577	0.000015817
Others	0.00266	0.00253	0.00240	0.00235	0.00221	. 0.00213
Non-Commercial	0.000495	0.000470	0.000458	0.000433	0.000420	0.000420
Total SOx Emission Estimation (SO2 million ton)	0.265	0.279	0.298	0.379	0.416	0.496
		<del></del>				
[SOx Emission from FLARE GAS; JICA TEAM '93]	1970	1971	1972	1973	1974	1975
Flared H2S (litters) @ H2S 4 mol %	742,960,000,000	880,840,000,000	974,680,000,000	1,137,240,000,000	1,168,400,000,000	1,038,120,000,000
H2S (g-mols)	33,167,857,143	39,323,214,286	43,512,500,000	50,769,642,857	52,160,714,286	46,344,642,857
H2S (gries)	1,127,707,142,857	1,336,989,285,714	1,479,425,000,000	1,726,167,857,143	1,773,464,285,714	1,575,717,857,143
SOx from Flace Gas (SO2 million too)	2,123	1,335,989	1,479,425 2.785	1,726,168	1,773,464	1,575,718
			2.103	3.249	3.338	7.300
[NOx Emission Est. by Fuel; JICA Team '93]	1970	1971	1972	1973	1974	1975
Solid Fuel	0.0024	0.0028	0.0043	0.0072	0.0079	0.0083
Petroleum	0.1149	0.1253	0.1346	0.1612	0.1808	0.2182
Gas	0.0002	0.0008	0.0019	0.0040	0.0051	0.0059
Others	0.0185	0.0177	0,0167	0.0164	0.0154	0.0149
Non-Commercial	0.0035	0.0033	0.0032	0.0030	0.0029	0.0029
Total NOx Emission as NO2 (million ton)	0.1395	0.1498	0.1606	0.1917	0.2121	0.2502
[NOx Emission from FLARE GAS; JICA Team '93]	1970	1971	1972	1973	1974	1975
Cal. Value Flare Gas (cal.) @8752 Kcal/M3	1.635+17	1.93E+17	2.13E+17	2.49E+17	2.566.+17	2.27E+17
NOx from Place Gas (NO2 million ton) @2.24 NO2 kg / 1e10 cal.	0.036	0.043	0.048	0.056	0.057	0.051
to 1 out to 1 out to 1	1970	1971	1972	1973	1974	1975
[Crude Oil Production; Arab Oil & Gas Directory]				2120.22	2197.88	1952.79
[Crude Oil Production; Arab Oil & Gas Directory] Annual Crude Oil Production [MM bbl]	1397.59	1656.92	1838.46	2139.23	2137.001	
Annual Crude Oil Production (MM 661)	1397.59					
		1656.92		1973	1974	1975
Aunual Crude (3) Production (MM bbl)  Year  Centent Production [million ton]	1397.59					
Aunual Crude Oil Production (MM bbl)  Year	1397.59			1973		

# 2. Parameters for Emission Estimation (2)

10 1400 to 1101 to 1011	1076	2027	1978	1979	1980	1981
[Pop. and GDP; World Table '92 IRAN]	1976 34,294,000	1977	36,617,008	37,848,000	39,124,000	40,450,000
Population	<u> </u>	35,431,008		2,080	1,990	2,540
GNP per capita (USS, cuer. pr.)	1,890	2,170	1,970			8,379,801,010,176
Gross National Product (local, corr. pr.)	4,691,699,171,328	- 5,849,500,090,368	5,343,801,245,696	6,390,801,235,968	6,628,101,324,800	8,349,199,368,192
Gross Domestic Product (local,cuts. pr.)	4,696,898,011,136	5,947,500,003,328	5,529,597,378,560	6,335,401,820,160		50
GDP Deffator (1987=100,lodex)	20	23	26	33	43	
GDP Deflator (1985=100,Index)	28	33	. 37	47	61	· 71
Gross Domestic Product (lucal, 1985, pr.)	16,877,803,625,802	18,005,466,594,486	14,930,492,538,390	13,557,106,474,238	10,936,703,386,382	11,829,066,270,621
	1		70.0	1020	1980	1981
[Pup, and GDP; Prepared by IRANIAN Counterpart]	1976	1977	1978	1979		
Population	33,709,000	34,736,000	36,077,000	37,991,000	39,646,000	41,221,000
Gross Damestic Product (local, 1982 pr.)	11,254,299,804,688	11,183,799,804,688	10,070,799,804,688	10,543,099,609,375	9,323,099,609,375	9,175,200,195,313
Gross Domestic Product (local, current pr.)	4,440,799,804,688	5,177,000,000,000	5,095,500,000,000	6,158,200,195,313	6,471,100,097,656	7,884,299,804,688
				4 + 1		
(Primary Energy Requirement)					1000	1981
;Energy Balance Table , H. KIBUNE '93	1976	1977	1978	1979	1980	
Solid Poel (MM bbl Oil Eq.)	8.40	8.50	4.80	7.50	7,90	6.60
Petroleum (MM bbl Oil Eq.)	179.08	202.60	197.25	212.33	189.58	198.97
Natural Gas (MM bbl Oil Eq.)	23.62	26.60	24.75	37.97	33.72	35.83
Hydro (MM bbl Oil Eq.)	6.20	6,60	9.80	8.50	8.80	9.70
Othres (MM bbl Oil Eq.)	17,24	17.14	17.85	17,14	17.85	17.04
Non-Comm. (MM bbl Oil Eq.)	3.40	. 3.50	3.40	3.50	. 3.40	3.60
Primary Energy Requirement Total (MM bbl Oil Eq.)	237.94	264.94	257.85	286.94	261.25	271.74
	1	****	1036	20-0	1980	1981
(Flare Gas; OPEC, (Value 1970-1976; Estimated))	1976	1977	1978	1979		
Flared Natural Gas (M3)	28,538,000,000	26,384,000,000	25,728,000,000	15,793,000,000	9,470,000,000	8,200,000,000
Flared Natural Gas (MM bbl Oil Eq. ; 6.198 BOE/1,000M3)	176.88	163.53	159.46	97.89	58.70	50.82
						1001
[CO2 Emission Est.; JICA Team '93]	1976	1977	1978	1979	1980	1981
(302 Emission Estimation (CO2 million ton)	81.70	95.45	95.61	104.28	98.45	103.69
Tutal CO2 Emission Estimation (Carbon million ton)	22.28	26.03	26.07	28.44	26.85	28.12
			_ · · · · · -			
[CO2 Emission from FLARE GAS ; JICA Team '93]	1976	1977	1978	1979	1980	1981
Cal. Value Flace Gas (cal.) @8752 Kcal/M3	2.50E+17	2.31E+17	2.25E+17	1.38E+17	8.29E+16	7.18E+16
CO2 from Flate Gas (CO2 million ton) @0.0002312 g-CO2/cal	57.75	53.39	52.06	31.96	19.16	16.59
CO2 from Flare Gas (Carbon million ton)	15.75	14.56	14.20	8.72	5.23	4.53
				***************************************		
[SOx Emission Est. by Fuck JICA Team '93]	1976	1977	1978	1979	1980	1981
Solid Feel	0.0363	0.0605	0.0370	0.0534	0.0562	0.0470
Petroleum	0.532	0.609	0.641	0.669	0.647	0.703
Gas	0.000018599	0.000021957	0.000020335	0.000035560	0.000038349	0.000046281
Others	0.00213	0.00212	0.00221	0.00212	0.00221	0.00211
Non-Commercial	0.000420	0.000433	0.060420	0.000433	0.000420	0.000445
Total SOx Emission Estimation (SO2 million ton)	0.571	0.672	0.681	0.725	0.706	0.753
[SOx Emission from FLARE GAS; JICA TEAM '93]	1976	1977	1978	1979	1980	1981
Flated H2S (litters) @1128 4 mol%	1,141,520,000,000	1,055,360,000,000	1,029,120,000,000	631,720,000,000	378,800,000,000	328,000,000,000
H3S (g-mols)	50,960,714,286	47,114,285,714	45,942,857,143	28,201,785,714	16,910,714,286	14,642,857,143
H2S (gems)	1,732,664,285,714	1,601,885,714,286	1,562,057,142,857	958,860,714,286	574,964,285,714	497,857,142,857
H2S (ton)	1,732,664	1,601,886	1,562,057	958,861	574,964	497,857
SOx from Place Gas (SO2 million ton)	3.261	3.015	2.940	1.805	1.082	0.937
		· ·		10-0	1980	1981
[NOx Emission Est. by Fuel; JICA Team '93]					1990	1701
Braze thursdays cost of their direct tenni sed	1976	1977	1978	1979		2.7
Solid Fuel	0.0088	0.0146	0.0090	0.0129	0.0136	0.0114
	0.0083 0.2580	0.0146 0.3110	0.0090 0.3215	0.0129 0.3366	0.2918	0.3134
Solid Fuel	0.0088 0.2580 0.0066	0.0146 0.3110 0.0080	0.0090 0.3215 0.0074	0.0129 0.3366 0.0125	0.2918 0.0128	0.3134 0.0141
Solid Fuel Petroleum	0.0088 0.2580 0.0066 0.0149	0.0146 0.3110 0.0080 0.0148	0.0090 0.3215 0.0074 0.0154	0.0129 0.3366 0.0125 0.0148	0.2918 0.0128 0.0154	0.3134 0.0141 0.0147
Solid Fuel Petroleum Gas Others Non-Commercial	0.0088 0.2580 0.0066 0.0149 0.0029	0.0146 0.3110 0.0080 0.0148 0.0030	0.0090 0.3215 0.0074 0.0154 0.0029	0.0129 0.3366 0.0125 0.0148 0.0030	0.2918 0.0128 0.0154 0.0029	0.3134 0.0141 0.0147 0.0031
Solid Fuel Petroleum Gas Others	0.0088 0.2580 0.0066 0.0149	0.0146 0.3110 0.0080 0.0148	0.0090 0.3215 0.0074 0.0154	0.0129 0.3366 0.0125 0.0148	0.2918 0.0128 0.0154	0.3134 0.0141 0.0147
Solid Fuel Petroleum  Gas Others Non-Commercial  Total NOx Emission as NO2 (million ton)	0.0088 0.2580 0.0066 0.0149 0.0029 0.2911	0.0146 0.3110 0.0080 0.0148 0.0030 0.3515	0.0090 0.3215 0.0074 0.0154 0.0029 0.3562	0.0129 0.3366 0.0125 0.0148 0.0030 0.3799	0.2918 0.0128 0.0154 0.0029 0.3365	0.3134 0.0141 0.0147 0.0031 0.3568
Solid Fuel Petroleum Gas Others Non-Commercial Total NOx Emission as NO2 (million ton) [NOx Emission from FLARE GAS; JICA Team 93]	0.0083 0.2580 0.0066 0.0149 0.0029 0.2911	0.0146 0.3110 0.0080 0.0148 0.0030 0.3515	0.0090 0.3215 0.0074 0.0154 0.0029 0.3562	0.0129 0.3366 0.0125 0.0148 0.0030 0.3799	0.2918 0.0128 0.0154 0.0029	0.3134 0.0141 0.0147 0.0031
Solid Fuel Petroleum Gas Others Non-Commercial Total NOx Emission as NO2 (million ton) [NOx Emission from FLARE GAS; JICA Team 93] Cal. Value Flare Gas (ral.) @8752 Keal/M3	0.0088 0.2580 0.0066 0.0149 0.0029 0.2911	0.0146 0.3110 0.0080 0.0148 0.0030 0.3515	0.0090 0.3215 0.0074 0.0154 0.0029 0.3562	0.0129 0.3366 0.0125 0.0148 0.0030 0.3799	0.2918 0.0128 0.0154 0.0029 0.3365	0.3134 0.0141 0.0147 0.0031 0.3568
Solid Fuel Petroleum Gas Others Non-Commercial Total NOx Emission as NO2 (million ton) [NOx Emission from FLARE GAS; JICA Team 93]	0.0083 0.2580 0.0066 0.0149 0.0029 0.2911	0.0146 0.3110 0.0080 0.0148 0.0030 0.3515 1977 2.31E+17	0.0090 0.3215 0.9074 0.0154 0.0029 0.3562 1978 2.25E+17	0.0129 0.3366 0.0125 0.0148 0.0030 0.3799	0.2918 0.0128 0.0154 0.0029 0.3365 1980 8.296+16	0.3134 0.0141 0.0147 0.0031 0.3568 1981 7.185+16
Solid Fuel Petroleum Gas Others Non-Commercial Total NOx Emission as NO2 (million ton) [NOx Emission from FLARE GAS; JICA Team 93] Cal. Value Flare Gas (ral.) @8752 Keal/M3	0.0088 0.2580 0.0066 0.0149 0.0029 0.2911	0.0146 0.3110 0.0080 0.0148 0.0030 0.3515 1977 2.31E+17	0.0090 0.3215 0.9074 0.0154 0.0029 0.3562 1978 2.25E+17	0.0129 0.3366 0.0125 0.0148 0.0030 0.3799	0.2918 0.0128 0.0154 0.0029 0.3365 1980 8.296+16	0.3134 0.0141 0.0147 0.0031 0.3568 1981 7.185+16
Solid Fuel Petroleum  Gas Others Non-Commercial  Total NOx Emission as NO2 (million ton)  [NOx Emission from FLARE GAS; JICA Team 93]  Cat. Value Place Gas (cal.) @8752 Keal/M3  NOx from Flace Gas (NO2 million ton) @ 2.24 NO2 kg / 1c10 cal.  [Crude Oil Production; Arab Oil & Gas Directory]	0.0088 0.2580 0.0066 0.0149 0.0029 0.2911 1976 2.50E+17 0.056	0.0146 0.3110 0.0080 0.0148 0.0030 0.3515 1977 2.31E+17 0.052	0.0090 0.3215 0.0074 0.0154 0.0029 0.3562 1978 2.25E+17 0.050	0.0129 0.3366 0.0125 0.0148 0.0030 0.3799 1979 1.38E+17 0.031	0.2918 0.0128 0.0154 0.0029 0.3365 1989 8.296+16 0.019	0.3134 0.0141 0.0147 0.0031 0.3568 1981 7.1811+16 0.016
Solid Fuel Petroleum  Gas Others Non-Commercial  Total NOx Emission as NO2 (million ton)  [NOx Emission from FLARE GAS; JICA Team 93]  Cal. Value Flare Gas (cal.) @8752 Keal/M3  NOx from Flace G45 (NO2 million ton) @ 2.24 NO2 kg / 1c10 cal.	0.0088 0.2580 0.0066 0.0149 0.0029 0.2911 1976 2.50E+17 0.056	0.0146 0.3110 0.0080 0.0148 0.0030 0.3515 1977 2.31E+17 0.052	0.0090 0.3215 0.0074 0.0154 0.0029 0.3562 1978 2.25E+17 0.050	0.0129 0.3366 0.0125 0.0148 0.0030 0.3799 1979 1.38E+17 0.031	0.2918 0.0128 0.0154 0.0029 0.3365 1980 \$.296+16 0.019 1980 \$37.05	0.3134 0.0141 0.0147 0.0031 0.3568 1981 7.18[;+16 0.016] 1981 480.30
Solid Fuel Petroleum Gas Others Non-Commercial Total NOx Emission as NO2 (million ton)  [NOx Emission from FLARE GAS; JICA Team 93] Cal. Value Place Gas (cal.) @8752 Keal/M3 NOx from Flace Gas (NO2 million ton) @2.24 NO2 kg / 1c10 cal.  [Crude Oil Production; Arab Oil & Gas Directory]	0.0088 0.2580 0.0066 0.0149 0.0029 0.2911 1976 2.50E+17 0.056	0.0146 0.3110 0.0080 0.0148 0.0030 0.3515 1977 2.31E+17 0.052	0.0090 0.3215 0.0074 0.0154 0.0029 0.3562 1978 2.25E+17 0.050	0.0129 0.3366 0.0125 0.0148 0.0030 0.3799 1979 1.38E+17 0.031 1979	0.2918 0.0128 0.0154 0.0029 0.3365 1980 8.29E+16 0.019 1980 537.05	0.3134 0.0141 0.0147 0.0031 0.3568 1981 7.181;+16 0.016 1981 480.30
Solid Fuel Petroleum Gas Others Non-Commercial Total NOx Emission as NO2 (million ton)  [NOx Emission from FLARE GAS; JICA Team 93] Cat. Value Plate Gas (cal.) @8752 Keal/M3 NOx from Place Gas (NO2 million ton) @ 2.24 NO2 kg / 1e10 cal.  [Crade Oil Production; Arab Oil & Gas Directory] Annual Crude Oil Production [MM bb1]	0.0083 0.2580 0.0066 0.0149 0.0029 0.2911 1976 2.50E+17 0.056	0.0146 0.3110 0.0080 0.0148 0.0030 0.3515 1977 2.31E+17 0.052	0.0090 0.3215 0.9074 0.0154 0.0029 0.3562 1978 2.25E+17 0.050	0.0129 0.3366 0.0125 0.0148 0.0030 0.3799 1979 1.38E+17 0.031	0.2918 0.0128 0.0154 0.0029 0.3365 1980 \$.296+16 0.019 1980 \$37.05	0.3134 0.0141 0.0147 0.0031 0.3568 1981 7.18(;+16 0.016) 1981 480.30
Solid Fuel Petroleum Gas Others Non-Commercial Total NOx Emission as NO2 (million ton)  [NOx Emission from FLARE GAS; JICA Team 93] Cat. Value Plate Gas (cal.) @8752 Kcal/M3 NOx from Flace Gas (NO2 million ton) @ 2.24 NO2 kg / 1c10 cal.  [Crade Oil Production; Arab Oil & Gas Directory] Annual Crude Oil Production [MM bb1]  Year Cement Production [million ton]	0.0083 0.2580 0.0066 0.0149 0.0029 0.2911 1976 2.50E+17 0.056	0.0146 0.3110 0.0080 0.0148 0.0030 0.3515 1977 2.31E+17 0.052 1977 2066.93	0.0090 0.3215 0.0074 0.0154 0.0029 0.3562 1978 2.25E+17 0.050 1978 1913.22	0.0129 0.3366 0.0125 0.0148 0.0030 0.3799 1979 1.38E+17 0.031 1979 1156.28	0.2918 0.0128 0.0154 0.0029 0.3365 1980 \$.296+16 0.019 1980 537.05	0.3134 0.0141 0.0147 0.0031 0.3568 1981 7.18E+16 0.016 1981 480.30
Solid Fuel Petroleum Gas Others Non-Commercial Total NOx Emission as NO2 (million ton)  [NOx Emission from FLARE GAS; JICA Team 93] Cat. Value Place Gas (cal.) @8752 Keal/M3 NOx from Place Gas (NO2 million ton) @ 2.24 NO2 kg / 1c10 cal.  [Crude Oil Production; Arab Oil & Gas Directory] Annual Crude Oil Production [MM bb1]	0.0088 0.2580 0.0066 0.0149 0.0029 0.2911 1976 2.50E+17 0.056	0.0146 0.3110 0.0080 0.0148 0.0030 0.3515 1977 2.31E+17 0.052 1977	0.0090 0.3215 0.0074 0.0154 0.0029 0.3562 1978 2.25E+17 0.050 1978 1913.22	0.0129 0.3366 0.0125 0.0148 0.0030 0.3799 1979 1.38E+17 0.031 1979	0.2918 0.0128 0.0154 0.0029 0.3365 1980 8.29E+16 0.019 1980 537.05	0.3134 0.0141 0.0147 0.0031 0.3568 1981 7.185;+16 0.016 1981 480.30

# 2. Parameters for Emission Estimation (3)

				(		
[Pop. and GDP; World Table '92 IRAN]	1982	1983	1984	1985	1986	1987
Population	41,832,000	43,276,000	44,787,008	46,374,000	48,051,008	49,824,000
GNP per capita (USS, curr. pr.)	3,140	3,530	3,750	3,990	3,960	3,650
The state of the s	11,152,000,024,576	14,021,000,429,568	15,151,000,453,120	16,521,999,941,632	18,106,994,917,376	21,280,203,997,184
Gross National Product (local curr. pr.)	11,152,101,736,448	14,027,800,444,928	15,162,000,015,360	16,555,902,500,864	18,124,996,870,144	21,269,986,672,640
Gross Dumestic Product (local, curr. pr.)						
GDP Dellator (1987=100,ledex)	58	66	68	71	84	100
GDF Deffator (1985 * 100, Index)	82	У	96	100	- 119	142
Gross Domestic Product (local, 1985, pr.)	13,605,095,770,735	14,981,405,324,795	15,736,842,681,720	16,555,902,500,864	15,253,877,217,312	15,015,146,246,038
			· · · · · · · · · · · · · · · · · · ·		*	<u> </u>
[Pup. and GDP; Prepared by IRANIAN Counterpart]	1982	1983	1984	1985	1986	1987
Population	42,800,000	44,438,000	46,201,000	47,807,000	49,363,000	50,995,000
Gross Domestic Product (local, 1982 pr.)	10,335,400,390,625	11,536,700,195,313	11,587,099,609,375	11,607,400,390,625	9,861,700,195,313	10,019,799,804,688
Gross Domestic Product (local, current pr.)	10,335,400,390,625	12,930,000,000,000	14,242,400,390,625	15,167,799,804,688	15,614,000,000,000	19,284,000,000,000
	• • • • • • • • • • • • • • • • • • • •					
[Primary Energy Requirement]	]					
(Energy Balance Table, 11, KiBUNE '93	1982	1983	1984	1985	1986	1987 .
Solid Fuel (MM bbl Qil Eq.)	8,90	.8,40	6.50	6.40	6.30	6,20
	222.01	271.26	300.62	318.35	292.90	312.81
l'etraleum (MM bb) Oil Eq.)	i					
Natural Gas (MM bbl Oil Eq.)	41.69	47.64	55.28	55.05	52.60	66.69
Hydro (MM bbl Oil Eq.)	10.10	9.70	9.00	8.70	11.70	13,10
Othres (MM bbl Oil Eq.)	18.36	24.84	22.37	20.28	23.57	26.16
Non-Comm. (MM bbl Oil Eq.)	3.50	3.50	- 3.50	3.50	3.50	3.30
Primary Energy Requirement Total (MM bbl Oil Eq.)	304.56	365.34	397.27	412.28	390.57	428.26
						4.4
[Flare Gas; OPEC, (Value 1970-1976; Estimated)]	1982	1983	1981	1985	1986	1987
Flared Natural Gas (M3)	14,250,000,000	9,700,000,000	6,500,000,000	5,400,000,000	5,300,000,000	4,800,000,000
Placed Natural Gas (MM bbl Oil Eq. ; 6.193 BOE/1,000M3)	88.32	60.12	40.29	33.47	32.85	29.75
			· · · · · · · · · · · · · · · · · · ·		1.5	
[CO2 Emission Est.; JICA Team '93]	1982	1983	1984	1985	1986	1987
CO2 Emission Estimation (CO2 million ton)	114.72	139.80	148.61	160.35	152.94	162.96
Total CO2 Emission Estimation (Carbon million ton)	31.29	38.13	40.53	43.73	41.71	44.44
Total Cos Emission Escimation (Catona militan ion)	31.23	36.13			711-1	
CONTRACTOR OF THE PROPERTY OF	1982	1983	1984	1985	1986	1987
[CO2 Emission from FLARE GAS; JICA Team '93]				<del></del>		
Cal. Value Flace Gas (cal.) @8752 Kcal/M3	1.25E+17	8.49E+16	5.69E+16	4.736+16	4.64E+16	4.2015+16
CO2 from Plaze Ges (CO2 million ton) @0.0002312 g-CO2/cai	28.83	19.63	13.15	10.93	10.72	9.71
CO2 from Flace Gas (Carbon million ton)	7.86	5.35	3.59	2.98	2.92	2.65
	,					
[SOx Emission Est. by Fuel; JICA Team '93]	1982	1983	1984	1985	1986	1987
Solid Fuel	0.0633	0.0598	0.0463	0.0455	0.0448	0.0441
Petroleum	0.752	0.928	1.041	1.168	1.120	1.102
Gas	0.000053902	0.000061634	0.000071554	0.000071255	0.000068073	0.000085723
Others	0.00227	0.00307	0.00277	0.00251	0.00291	0.00323
Non-Commercial	0.000433	0.000433	0.000433	0.000433	0.000433	0.000408
Total SOx Emission Estimation (SO2 million ton)	0.818	0.991	1.090	1.216	1.169	1.150
[SOx Emission from FLARE GAS ; JICA TEAM '93]	1982	1983	1984	1985	1986	1987
	570,000,600,000	388,000,000,000	260,000,000,000	216,000,000,000	212,000,000,000	192,000,000,000
Placed H2S (litters) @ H2S 4 mol-						
li2S (g-mols)	25,445,428,571	17,321,428,571	11,607,142,857	9,642,857,143	9,464,285,714	8,571,428,571
H2S (gtms)	865,178,571,429	588,928,571,429 588,929	394,642,857,143	327,857,142,857	321,785,714,286	291,428,571,429
H2S (ton) SOx from Flate Gas (SO2 million ton)	865,179 1.629	1.109	394,643 0.743	327,857 0.617	321,786 0.606	291,429 0.549
The state of the s	1.029	1-103	0.745	0.017	0.000	
[NOx Emission Est, by Fuel; JICA Tram '93]	1982	1983	1984	1985	1986	1987
Solid Fuel	0.0153	0.0145	0.0112	0.0110	0.0108	0.0107
	0.3401	0.4201	0.4611	0.5173	0.4896	0.5041
Petroleum						
Gas	0.0172	0.0194	0.0221	0.0218	0.0202	0.0281
Others	0.0158	0.0214	0.0193	0.0175	0.0203	0.0226
Non-Commercial	0.0030	0.0030	0.0030	0.0030	0.0030	0.0028
Total NOx Emission as NO2 (million ton)	0.3915	0.4785	0.5167	0.5706	0.5440	0.5683
[NOx Emission from FLARE GAS; HCA Team '93]	1982	1983	1981	1985	1986	1987
	1704	1983 8.49E+16	5.69E+16	4.73E+16	4.64E+16	4.20E+16
	1 2612 . 1 21			4.7.35+16 0.01 i	0.010	4.206+16
Cal. Value Flate Gas (cal.) @8752 Kcal/M3  NOx (rom Flate Gas (NO2 million ton) @2.24 NO2 kg / 1e10 cal.	1.255+17		ถูกเร!			0.007
NOx from Flare Gas (NO2 million ton) @ 2.24 NO2 kg / le 10 cal.	[.25E+17 0.028	0.019	0.013	0.011	0.010	
NOx from Flare Gas (NO2 million ton) @ 2.24 NO2 kg / 1e10 cal.			0.013			1987
NOx from Fiere Gas (NO2 million ton) @2.24 NO2 kg / 1e10 cal. [Crude Oil Production; Arab Oil & Gas Directory]	0.028	0.019	1984	1985	1986	1987
NOx from Flare Gas (NO2 million ton) @ 2.24 NO2 kg / 1e10 cal.	0.028	0.019				1987 838,63
NOx from Flare Gas (NO2 million ton) @ 2.24 NO2 kg / Tello cal.  [Crude Oil Production; Arab Oil & Gas Directory]  Annual Crude Oil Production [MM bbl]	0.028 1982 872.82	983 891.22	1984 743.86	1985 800.20	1986 743.55	838.63
NOx from Fiere Gas (NO2 million ton) @2.24 NO2 kg / 1e10 cal. [Crude Oil Production; Arab Oil & Gas Directory]	0.028	0.019	1984	1985	1986	838.63 1987
NOx from Flare Gas (NO2 million ton) @ 2.24 NO2 kg / 1e10 cal.  [Crude Oil Production; Arab Oil & Gas Directory]  Annual Crude Oil Production [MM bb1]  Year	9.028 1982 872.82	0.019 1983 891.22	1984 743.86	1985 800.20	1986 743.55	838,63
NOx from Flare Gas (NO2 million ton) @ 2.24 NO2 kg / 1e10 cal.  [Crude Oil Production; Arab Oil & Gas Directory]  Annual Crude Oil Production [MM bb]]	9.028 1982 872.82	0.019 1983 891.22	1984 743.86	1985 800.20	1986 743.55	838.63 1987
NOx from Flate Gas (NO2 million ton) @2.24 NO2 kg / 1e10 cal.  [Crude Oil Production; Arab Oil & Gas Directory]  Annual Crude Oil Production [MM bbl]  Year  Coment Production [million ton]	9.028 1982 872.82 1982	1983 891.22 1983 10.912	1984 743.86 1984 (11.803)	1985 800.20 1985 12.10	1986 743.55 1986 11.27	838.63 1987 12.62

## 2. Parameters for Emission Estimation (4)

<u>et i jaron de la seta di la casa di la casa</u>			
[Pop. and GDP ; World Table '92 [RAN]	1988	1989	1990
Population	51,698,000	53,681,008	55,779,008
GNP per capita (USS, curr. pr.)	3,070	2,580	2,490
Gross National Product (local curr. pr.)	23,597,808,615,424	28,138,897,670,144	36,463,097,937,920
Gross Domestic Product (Incal curr, pr.)	23,587,859,726,336	28,123,512,963,072	36,441,992,200,192
GDP Deflator (1987=100, Index)	119	137	162
GDP Dellator (1985 = 100, Index)	168	195	229
Gross Domestic Product (local, 1985, pr.)	14,043,636,413,372	14,453,812,552,201	15,910,289,668,741
[Pop. and GDP; Prepared by IRANIAN Counterpart]	1988	1989	1990
Population	52,672,000	54,504,000	56,401,000
Gioss Doméstic Product (local, 1982 pr.)	9,234,299,804,688	9,514,599,609,375	10,664,900,390,625
	21,753,599,609,375	27,028,800,781,250	35,755,000,000,000
Gross Domestic Product (local, current pr.)	21,730,377,007,373	27,020,000,701,2501	33,133,000,000,000
Daine Propriate and	1		
[Primary Energy Requirement] (Racegy Balance Table, II. KIBUNE '93	1983	1989	1990
	· · · · · · · · · · · · · · · · · · ·	4,70	4.70
Solid Fuet (MM bbì Oìl Eq.)	6.40		
Petroleum (MM bbl Oil Eq.)	314.49	330.26	348,66
Natural Gas (MM bbl Oil Eq.)	69.51	91.34	119.44
Hydro (MM bbi Oil Eq.)	11.40	11.70	9.50
Othres (MM bbl Oil Eq.)	33.00	31.68	24.90
Non-Comm. (MM bbl Oil Eq.)	3.40	.3.20	3.20
Primary Energy Requirement Total (MM bbl Oil Eq.)	438.20	472.88	510.40
IT C ONCO OL 1920 1027 Parantal	1988	1989	7990
[Flare Gas; OPEC, (Value 1970-1976; Estimated)]	<del></del>		11,350,000,000
Flared Natural Gas (M3)	4,000,000,000	1,500,600,000	
Flared Natural Gas (MM bbl Oil Eq. ; 6.198 BOE/1,000M3)	24.79	9.30	70.35
[CO2 Emission Est.; JICA Team '93]	1988	1989	1990
CO2 Emission Estimation (CO2 million ton)	167.98	180.13	185.08
Total CO2 Emission Estimation (Carbon million ton)	45.81	49.13	50.48
Total Cos Emission Estimation (Catoon militor con)	15.01		
[CO2 Emission from FLARE GAS; JICA Team '93]	1988	1989	1990
Cal. Value Flare Gas (cal.) @8752 Kcal/M3	3.50E+16	1.31E+16	9.93E+16
CO2 from Flare Gas (CO2 million ton) @ 0.0002312 g-CO2/cal	\$.09	3.04	22.97
CO2 from Place Gas (Carbon million toa)	2.21	0.83	6.26
[SOx Emission Est. by Fuel; JICA Team '93]	1988	1989	1990
Solid Fuel	0.0455	0.0334	0.0334
Petroleum	1.124	1.175	1.225
Gas	0.000087969	0.000113201	0.000139061
Others	0.00408	0.00392	0.00308
Non-Commercial	0.000420	0.000396	0.000396
Total SOx Emission Estimation (SO2 million ton)	1.174	1,213	1.262
Total Cold Tarricology Extended (Sector annual Con-	A V CONTACTOR DOCUMENT		
[SOx Emission from FLARE GAS; JICA TEAM '93]	1988	1989	1990
Flared H2S (litters) @142S 4 mol%	160,000,000,000	60,000,000,00	454,000,000,000
HZS (g-mols)	7,142,857,143	2,678,571,429	20,267,857,143
H2S (gims)	242,857,142,857	91,071,428,571	689,107,142,857
H2S (ton)	242,857	91,071	689,107
SOx from Place Gas (SO2 million ton)	0.457	0.171	1.297
[NOx Emission Est. by Fuel; JICA Team '93]	1988	1989	1990
	ļ	0.0081	0.0081
Solid Fuel Petroleum	0.0110	0.5392	0.0031
1 Octobrolli	0.5015 0.0285	0.0354	0.0428
Gas			
Others	0.0285	0.0273	0.0215
Non-Commercial	0.0029 0.5724	0.0028	0.0028
Total NOx Emission as NO2 (million ton)	0.3724		5.0571
¡SOx Emission from FLARE GAS; JICA Team '931	1988	1989	1990
Cal. Value Flare Gas (cal.) @8752 Kcal/M3	3.501:+16	1.31E+16	9.935+16
NOx from Flare Gas (NO2 million ton) @ 3.24 NO2 kg / 1c10 cal.	0.008	0.003	0.022
[Crude Oil Production; Arab Oil & Gas Directory]	1988	1989	1990
Annual Crude Oil Production [MM bb]	843.79	1027.14	1116.66
hammer and an expectation that and	. 41		
Year	1988	1989	1990
Cement Production [million ton]	[2.12]	12.83]	15.15
CO2 from Cement Production [0.12 Carbon ton / Cement ton]			
COT HAM Centent Lingsetton forth Cataont and Centent and	1988	1989	1990
CO2 from Cement Production [Carbon million ton]	1988 1.45	1989	1990 1.82

# 3. Estimation of Energy Balance Table with Forecast to 2021 (1)

	Year	1968	1069	1670	1073	Q.											
Production(生産)					12/1	7761	19/3	1974	1975	1976	1977	1978	1979	1980	1981	1982	1983
Solid Fuel	Sorp	1.1	13	1.4	1.6	2.5	4.7	**	0	0	c		į		,		
Crude Oil	O. P.D	1,088.7	1,257.8	1.421.5	1,688.0	1 227 0	0.71.0	0.00	* 0	, o c .	2.8	4. xo	7.5	7.9	9.9	6.9	8.4
Natural Gas	GAPR	149.5	168.9	1927	257.0	2 1 2 1	V:141,4	6.081,2	1,930.1	235.5	2,078.2	1,833.1	1,202.7	531.0	540.5	2.626	986.6
Hydro	HYPD			2 6		0.753	1.057	380.7	781.9	51.4.9	418.0	273.7	259.2	101.5	9.7.6	185.4	173.3
Others	CATO	73.0	21.0		i d	, ,	4 1	5.3	5.4	2.0	6.6	8.6	8.5	80 80	5.7	10.1	9.7
Neg-College	O A C N	7			20.5	φ',Α' <sup>†</sup>	19.0	17.9	17.2	17.2	17.1	17.9	17.1	17.9	17.0	18.4	24.8
Prod. Total	T. P.	1 267 0	1 456.2	7 542 7	8.8	3.7	3.5	3.4	3,4	3,4	3.5	3.4	3.5	3,4	3.6	3.5	3.5
	1	1,207.7	7.004.1	1,043./	1.9/6.9	2,121.8	2,470.8	2,612.7	2,262.3	2,529.7	2,527.9	2,141.1	1,494.9	9.999	672.4	1,201.6	1,202.4
Import(輸入)	_																
Solid Fuel	SOIM	0.0	0.0	0.0	c	c				ļ							
Petroleum Products	PTIM	0.0	0.0	000	9 6		7 6	4.0	4. J. (	0,4  ,	4.1	1.9	3.7	3.8	2.6	4.4	3.9
Impo. Total	MLIT	0.0	0.0	0.0	0	0.00	7.0	4 0	2,4	0.4	7.	1.9	3.7	3.8	21.2	34.5	58.7
							5	0.0	0.0	0.0	8.5	3.8	7.4	7.6	23.8	38.9	62.6
Export(輸出)			÷.			-		~						:			
Solid Fuel	S	0.0	0.0	0.0	0.0	0.0	00	o o		c							
Crude Oil	A KIN	-936.5	-1,070.6	-1.218.6	-1.475.0	-1 624 5	9 7 40 1.	2001	1000	2	0,000	0.0	0.0	0.0	0.0	0.0	0.0
Petroleum Products+Bunker	PTE XX	-43.0	-89.1	-113.6	-96.2	135.7	-1,717.0	117.8	1246	C.024,1-	-1,790.6	-1,565.9	-902.7	271.0	-346.0	-772.5	-763.4
Natural Gas	GAEX	0.0	0.0	-6.1	-35.6	.517	2 4 7	5.25	0.441		0.0/-	-230.2	-142.3	-57.0	4,4	-15.4	-1.2
Impo. Total	対説に	-979.5	-1.159.7	-1 338 3	-1 606 8	1 611 0	0.000	0.70.0	5.00-	4.55.4	.59.1	-32.4	-22.0	0.0	0.0	0.0	0.0
				200000	2,000,0	-1,011,7	-2,089.8	6.021.2-	-1,872.3	-2,040.2	-1,926.3	-1,368.5	-1,067.0	-328.0	-341.6	-787.9	-764.6
Stock Change & Some loss(在展変動はか)	(1) (H					:		· . :									
	SOSC	0.0	0.0	0.0	00	C	000	00		0	Š	,					
10 sp. 0	88	32.1	\$ .	7.7		9 6	) V	3	0, 6	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
7 Petroleum Products	PTSC	67.2	2.5.5		, <u>.</u>	0 4	p .	4.1	0.1	0.3	6.7	5.4	5.3	1.9	2.6	-1.8	5.4
Natural Gas	CASO	-148 5	8 7 5 1.	. 5921.	2000	14.0	4. 6	5.5	13.0	-29.0	-19.2	152.9	45.6	-19.1	-14.9	-2.5	-14.9
(Nat. Gas Fleair +In;)		1234	130.5	316.3	131.0	-190.9	5.52.5	1.606-	-199.9	-230.9	-332.3	-216.5	-199.2	-67.8	-61.8	-143,7	-125.7
Statis, Diff. Total	JS LL	783.	101.8	121.7	22.7	-14/4	109.0	-172.5	-146.3	-178.8	-249.3	-203.2	-172.3	-59.8	-54.0	-120,7	-101.9
		0.001	0.17.7.	7.101-	0'/67-	-1/0.4	-213.5	301.8	-186.9	259.5	-344.8	-58.2	-148.3	-85.0	-74.1	-148.0	-135.1
Primary Energy Requirement(一次供給)	· · · · · · · · · · · · · · · · · · ·								: - : - :							-	
Solid Fuel	SOPR	1.1	1.3	1.4	1.6	2.5	4.2	4.6	8.4	2.0	30						
Crade Oil	CRPR	184.3	188.7	195.2	217.2	214.4	7 0 7 7	8 272	262.0	t . 6 9 7 C	0.00	4.0	?	ο.	6.6	8.9	80 4
Petroleum Prod.	PTPR	-110.2	-114.6	-110.9	.127.2	2 151.	7 611	1001	404.9	403,0	2,44,5	272.6	305.3	261.9	197.1	205,4	228.6
Natural Gas	GAPR	1,0	1.1	10.3	13.0	15.2	7.777	1.66	6,101-	-80.3	-91.7	-75.4	-93.0	-72.3	1.9	16.6	42.6
Hydro	HYPR			2,6	7	1	74.7	1.02	7.17	23.6	26.6	24.8	38.0	33.7	35.8	41.7	47.6
Othres	OTPR	0 80	9		1 6		d 1	6.0	5.4	6.2	6.6	ev eo	8. 2.	8.8	7.6	10.1	5.7
Non-Confid.	NOBB			7	20.5	4.4	19.0	17.9	17.2	17.2	17.1	17.9	17.1	17.9	17.0	18,4	24.8
Primary, Total	0d II	0 701	4 50	0,7	5.5	3.7	3.5	3.4	3.4	3.4	3.5	3.4	3.5	3.4	3.6	ы М	6
(Sun of energy exclude net one)	\ \ \ \	216.0	210.7	124.2	133.1	139.5	168.0	184.9	211.6	237.9	264.9	257.9	286.9	261.3	271.7	304.6	365.3
Personial form Commence of the		0.017	6.812	1.667	200.3	260.7	280.7	294.0	319,0	324.2	356.7	333.2	279.9	333.5	2696	288.0	1 250
In order to produce the Tabel following days courses are mored.	ation is aser	ibed to the Jic	A team.										:	<u>.</u>	:	> ·	1.77

In order to produce the Tabel, following data sources are turned to account.

1) for the Primary energy, NIOC data book " ? "

2) same as, 'Energy balance Table in IRAN,' by Ministry of Energy

3) for the industrial sector, Iranian authority named ?

4) for 'Other' energy in the household sector, Mr. Darabi's estimation

5) 'Non-OECD Energy Balance' by OECD/IEA is not so useful.

Conversion Sector(転換部門)

	7083	-228 6	212.0	-14.7	
	1982	-205.4	3 201	-7.8	
: '	1981	-197.1	182.6	-14.5	
	1980	-261.9	254.2	7.7-	
	1979	-305.3	287.7	-17.6	
į	1978	-272.6	261.6	-11.0	
	1977	-294.3	275.9	-18.5	
	1976	-265.3	250.1	-15.3	
	1975	-262.9	251.1	11.8	
	1974	-242.8	228.5	-14.2	
	1973	-229.7	215.0	-14.8	
	1972	-214.4	200.8	-13.6	
	1971	217.2	202.5	-14.7	
2000	0, 51	195.2	189.0	-6.2	
070	5061	188.	1,0.3	-10.4	
10.69	194.7	169 6	100.0	7.57	
L	46.00	Fara	40.44	1 1776 1	J
Refinary	'ude Oil innit	t. Prod. Output	myersion loss		

3. Estimation of Energy Balance Table with Forecast to 2021 (2)

										,,,,		0.40	000	1000	1081	. 685	1983
	Year	1968	1969	1970	1971	1972	1973	1974	975	0/6	21.6	8/8	1979	1200			
Electric Utility									G	c	c	c	c	0.00	0.0	0.0	0.0
Solid Fuel for Power	SOEL	0.0	0,0	0.0	0.0	0.0	0.0	0.0	0.0	5 6	0.0	) t	25.5	7.57	18 2	0 % [-	-74.9
Pet. Pro. for Power	PTEL	-3.5	0.4.0	-5.4	4.9	4.5	-7.8	0.8	-10.8	12.5	-13.6	-15.7	0.01-		7.017		, , ,
Gas for Power	CAEL	0.2	-0.1	0.1	-1.0	-2.1	-4.5	5.9	-6.7	6.0	-9.5	4,5	-14.5 C1	+ + + + + + + + + + + + + + + + + + + +	2 1	15.5	1 1 7
Generation	ELEL	2,0	1.9	2.5	3.2	4.0	5.5	9.9	7.5	80 4.	9.3	10.2	11.4	11.7	7.5.	15.5	57.7
Hydro for Power	HYEL	£.	5.	-2.6	4.2	-5.5	4,4	-5.3	4.5.4	-6.2	9.9-	.9.8	8. 5.	×6 ×6	٠٨./	1.01.	7.7
Nuclear for Power	E E	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	3
Convers Toss of Pow	TIET	2.9	4.	-5.6	-6.9	-8.1	-11.2	-12.6	-15.4	-17.3	-20.4	-23.8	-27.1	-26.9	-29.4	2.55-	1.65
Efficial Gene (%)		40.6	30.1	30.8	31.9	33.2	32.9	34.3	32.8	32.6	31.2	30.0	29.7	30.3	31.0	31.8	31.4
Auto Generation	·											1		ŗ		* >	8 9
Petro, input	PTAU	-1.9	-4.9	-5.1	-5.2	-5.2	5.2	-5.3	-5.7	, 8.	-6.8	9.5	ų, ,	1	÷ (	* t	9 0
Auto Output	ELAU	0.8	1.5	1.6	1.6	1.7	1.7	1.8	1.9	1.9	2.1	1.7	2.5	\$.U.	7.7	2.7	9 9
Loss of auto.	TLAU	-1.1	-3.4	-3.5	-3.5	-3.5	-3,5	-3.5	-3.8	-3.9	-4.7	-3.9	-3.9	6.0	.5./	/-6-	7
				:	:			÷								;	1
Own Use		-								Š		i c			00	000	C
Refinary	PTOW	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	9 6	2 6	1 6	
Power Plant	ELOW	-0.3	-0.4	-0.5	-0.6	-0.7	-0.9	-1.2	-14	-I.S	9:1-	-1.9	7.7.	000	2.5	2.7	
Own Use Total	MOTL	-0.3	٠٥.4	-0.5	-0.6	-0.7	-0.9	-1.2	-1.4	-1.5	-1.6	-T-	1.7.	S'O	-7.7.	7.3	
	r																. :
Statistical Difference				,		C	0		9 :		000	40	0.0	0.0	0.0	0.0	0.0
Solid	SOS	0.0	0.0		<b>9</b> 5	50 6	2 6	2.4	, c	, 5 , 8 , 6	) t	, 6	5 6	-14.3	4.7	-18.0	-12.8
Petroleum	FISD	7.6-	) i	-14.4	, ç	0.0	7.77-		0.07	100		2.0	0	0.0	0.0	0.0	0.0
Gas	1 Car	0 0	) ) (	) ) (	0.0	2 6	3 6	0	2 0	0:0	9	0.0	0.0	0.0	0.0	0.0	0.0
Total SD	C C L	200	0.9	14.4	5.7	3.6	-11.2	-16.7	-24.2	-21.4	-11.7	-9.2	-9.5	-14.3	-4.7	-18.0	-12.8
4 × 50 H 37 H 6																	
First chergy Demand Total(技术ーケントー岩状)	としている。	1	0701	1970	1001	1072	1073	1974	1975	1976	1977	1978	1979	1980	1981	1982	1983
7:01 1:01	75 11	1700	20 18	10 76	101 71	109 96	126.37	136.69	155.11	178.52	208.09	208.05	226.82	213.34	216.97	239.13	291.58
Solid Enel	S	01.1	1 30	1.40	1.60	2.50	4.20	4,60	4.80	5.10	8.50	5,20	7,50	7.90	6.60	8.90	8.40
Petroleum	NE LA	43.36	48.78	53.30	59.52	66.19	78,01	89.43	106.66	127.27	152.05	155.40	164.18	153.28	156.13	171.87	213.04
Gas	GA FIN	0.80	1.00	10.20	12.00	13.10	15.40	14.20	15.00	16.70	17.10	16.20	23.50	19.60	21.20	22.00	25.20
Blectricity	E	2.50	3.00	3.60	4.30	5.10	6.30	7.20	8.00	8.80	9.80	10.00	11,00	11:30	12.40	14.50	16.60
Others	OTEN	23:02	21.91	21,50	20.49	19.37	18.97	17.85	17.24	17.24	17.14	17,85	17.14	17.85	17.04	18.36	24.84
Non-Commercial	NOFN	4.30	4.20	4.00	3.80	3.70	3.50	3.40	3.40	3.40	3.50	3.40	3.50	3.40	3.60	3.50	2.50
Industrial Sector			٠.				٠:										
Total	ZI F	12.42	13.76	15.61	17.26	20.15	27.42	30.89	35.16	40.27	46.74	43.70	49.82	53.24	56.55	59.78	66.74
Solid Fuel	SOIN	1.10	1.30	1.40	1.60	2.50	4.20	4.60	4.80	5.10	8.50	5.20	7.50	7.90	6.60	8.90	8.40
Petroleum Total	NITA	9.42	10.26	11.51	12,36	12.85	15.52	17.19	20.26	23.17	26.74	27.80	79.72	30.34	25.05	55.76	47·74
Gas oil		2,95	3.17	3.61	4.02	4.36	5.41	6.06	7.35	8.65	10.82	11.29	11.25	11.05	12.00	15.60	35.50
Fuel Oil		6.47	7.08	7.90	8.34	8,49	10,11	11.13	12.91	14.51	15.92	16.50	16.37	19.78	21.05	0 40	00.00
Gas	GAIN	0.30	0.40	0.50	09.0	1,60	3.70	4.50	5.30	0.60	0.10	08.4	9.60	20.00	01.11	230	6 10
Elec.	ELEN	1.60	1.80	2.20	2.70	3.20	00.4	90.6	4.80	21.5	10 8	2 55	2 6	9 12	8 65	9.54	10.01
Food	77.F0	2.51	2.78	3.15	3,49	4.0.4	4,0	67.0	01.7		2.71	2 44	1 2 3	5.73	4 63	36.3	4.76
Textile	TLIX T	1.20	1.33	10.0	1.67	0 f.	0 60.7	3,50	0.26	0.27	0.26	30	0.50	0.53	0.47	0.78	0.94
wood & Fro.	3 6	0.10	7 7 7	500	† (°	92.0	35.0	0.40	0.43	0.50	09:0	0.59	0.56	0.84	1.33	1.07	1.03
raper of ruip	5 5	0.10	9 6	107	2		1.87	2.11	2.25	4.55	5,93	6.22	7.61	5.02	5.80	4.50	4.96
City of Non-metal	i k	5.27	, K.	6.62	7.32	8.54	11.62	13.10	15.02	17.96	21.25	20.88	23.57	27.89	31.74	33.06	33.59
Prinary Metal	T PM	1.33	1.47	1.67	1.84	2.15	2.93	3,30	3.65	3.39	3.44	1.52	1.19	1.17	1.43	1.81	60.9
Machinary	1 M	1.00	1.10	1.25	1.39	1.62	2.20	2.48	2.36	2.52	2.62	2.20	2.86	3,45	2.49	3,63	54.6
Other Manufacturings	TLOT	0.00	00'0	00.00	0.00	0.00	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	70.0	0.02	70.0
				İ	i												

3. Estimation of Energy Balance Table with Forecast to 2021 (3)

Total		1968	1969	1970	1971	1972	1973	1974	1975	1976	1977	1978	1979	1980	1981	1982	1983
	TT TT	12.31	13.71	15,90	18.14	20.15	24.84	28.80	35.55	43,48	54.06	55.77	56.42	51.14	49.23	55.06	68.62
Petoroleum Total	PTTR	12.31	13.71	15.90	18.14	20.15	24.84	28.80	35.55	43.48	54.06	55.77	56.42	51.14	49.23	55.06	68.62
Cor Dond & Train	p.L.L.	10.93	12.05	13.77	15.60	17.26	21.12	24.52	30.33	37.28	46.32	49,46	53.03	47.74	47.66	51.85	64.58
		503	5.71	6.56	7.55	8.54	10.30	12.40	15.63	19.97	24.69	26.87	30.53	25.62	23.67	24.24	31.85
		20.5	25.3	727	8.05	8.72	10.82	12.12	14.70	17.30	21,64	22.59	22.50	22.12	23.99	27.61	33.13
	Y Clubated	26.	1,66	2.13	2.55	2.89	3.72	4.29	5.22	6.20	7.74	6.32	3,40	3.40	1.57	3.21	3.64
	2	2.7	99.1	2.13	2.55	12.83	3.72	4.29	5.22	6.20	7.74	6.32	3.40	3.40	1.57	3.21	5.64
	1	7												,			
	Г																
Agricultural Sector	0.4	, r	2 4 2	1 80	4 37	4 68	5.78	6.56	7.92	9.28	11.66	12.16	12.11	12.01	13.10	15 19	18.29
	11.00	01.6	0.00	2 70	4 22	85 7	89 5	98 9	7.72	9.08	11.36	11.86	11.81	11.61	12.60	14 49	17.39
	FIAC	0.10	0.5.0	010	010	9 0	0.10	0.20	0.20	0.20	0.30	0.30	0:30	0.40	0.50	0.70	0.90
	DW13	00.5	2													,	
						-			.:						1		
Residential/Commercial Sector			16.00	16 11	46.00	40.00	52.18	55.34	60.27	62.69	75.84	77.62	88.46	83.14	86.20	98.40	123.53
	11.RE	44.40	45.99	10.11	20,70	47.30	25.25			000	000	00.0	0.00	0.00	0.00	0.00	00.0
:	SS	0.00	000	0000	0.00	00.0	0.00	91.58	36.42	43.04	49.79	50.27	58.92	50.59	48.95	55.84	70.59
	717	10.23	07.07	12:61		. 01.0	0.0	010	0.00	0.50	1.30	1.30	3.30	5.40	9.90	12.20	15.00
	CAKE	000	00.5	90.0	9 5	08.	2.20	2 40	3.00	3.50	4.10	4.80	5.60	5.90	6.70	8.50	9.60
	ELKE	06.00	0. T. C	200	07.00	20.4	20.81	17.85	17.24	17.24	17.14	17.85	17.14	17.85	17.04	18.36	24.84
Other Fuel	CIRE FOR	23.02	16.17	4 00	08.6	15.51	3.50	2.40	3.40	3.40	3.50	3,43	3,50	3.40	3.60	3.50	3.50
191	333	201							-		79.2						
nousemond sector	71.11	07 07	71.75	41.34	41 89	92 44	45.65	48.25	51.87	58.12	64.77	68.89	75.12	66.80	65.12	74.54	95.81
	11.40	40.09	41.73	41.34	47.07		2	7									
	용				ţ	1000	000	26.00	70 07	35 78	41.83	42.02	50.73	40.95	38.13	44.75	57.75
	PIHO	12.99	15.24	15.30	70.71	77.77	46.34	10:07	900	51.0	00 FF	0.38	0.98	1.60	2.93	3.61	4.52
	GAHO	00.0	0.00	0.00	0.00	50.0	500	200	00.0	1 5	06	2.23	2.76	3,01	3.42	4.32	5.21
-	EL HO	0.38	0.41	0.48	0.58	7/:0	10.04	0.00	1		> - t-	17.85	17.14	17.85	17.04	18.36	24.84
	отно	23.02	21.91	21.50	20.49	19.37	18.97	17.85	17.74	17.24	17.77 CS C	07.6	7.14	3.40	3.60	3.50	3.50
Non-Commercial	NOHO	4.30	4.20	4.00	3.80	3.70	3.50	3.40	3.40	3.40	3.30	Of the	20:5				
Commercial Sector											**			26.25	80 10	78 20	27.72
	TLCM	3.76	4.24	4.78	5.09	5.40	6.49	7.08	8.40	7.57	11.0	11.72	¥2.51	20.01	20:44	2000	
	800M							1		ţ	40 €	36.8	α	0 64	10.82	11.09	12.84
	NO.	3.24	3.54	3.95	4.17	4.24	20.5	0000	0.00	35.0	20.0		2.50	3 80	6.97	8.59	10.48
	S	0.00	0.00	0.00	0.00	0.07	0.0	0.0	100	. 40	2000	25.5	28.5	2.89	3.28	4.18	4.39
	FO El	0.52		0.82	0.92	1.08	1.36	1.45	7.80	1,90	07:7	9 0	1 0	òò		000	9
	OTCM	00'0	0.00	0.00	00:00	0.00	0.00	0.00	0.00	0.00	00.0	0.00	20.0	30.5	3.5		
		. :						٠		٠		÷					
Non-Energy Use	3,000	G	0.00	12 60	35.00	16.00	16.20	15.10	16.20	17.80	19.80	18.80	20.00	13.80	11.90	10.70	14.40
ıcrgy	H.N.E.	2.80	3.30	12.50	13.00	15.00	10.20	24.21	24.01	2 S S	01 01	9.70	9.40	09.6	11.70	10.50	14.20
	PINE F	2.30	2.70	2.80	3.60	3.60	11.60	9.50	0.70	9.30	9.70	9.10	10,60	4.20	0.20	0.20	0.20
	GAINE	טכיט	0.00	2,12	71.40	74.47	24.44	>	1								

3. Estimation of Energy Balance Table with Forecast to 2021 (4)

. •	.:											
	Year	1984	1985	1986	1987	1988	1989	1990	1994	2001	2011	2021
Production(生涯)		,	,	,	;	,	•	,				,
Solid Fuel	SOPD	6.5	6.4	6.3	6.2	6,4	4.7	4.7	5.087	5.844	6,455	7.131
Crude Oil	CE PS	867.6	907.5	796.5	891.7	933.3	1,075.1	1192	1423	1681	1681	1681
Natural Gas	GAPR	193.1	217.0	161.4	194.5	219.5	333.0	402	517	803	1308	2130
Hydro	HYPD	9.0	8.7	11.7	13.1	11.4	11.7	9.5	13,44	21.75	31,13	40.9
Others	OTPD	22.4	20.3	23.6	26.2	33.0	31.7	24.9	27.97	29.37	37.98	43.13
Nep-Correct	NOPR	3.5	3.5	3.5	9 60	3,4	3.2	3.2	3.507	3.682	0	
Prod. Total	TLPD	1,100.2	1,161.9	1,001.5	1,133.5	1,205.7	1,458.5	1,636.3	1,990.0	2,544.6	3,064.6	3,902.2
Import(輸入)									-			
Solid Fuel	SOIM	1.9	1.5	1.6	1.4	1.3	6.0	r i	0.04	0.127	0.824	1.742
Petroleum Products	PTIM	37.9	61.6	58.0	72.4	68.9	49.6	45.3	46.6	1567.4	1024.6	1208.5
Impo. Total	TLIM	39,8	63.1	59.6	73.8	70.2	50.5	46.3	46.6	1,567.5	1,025.4	1,210.2
										:		
Export(数出)												
Solid Fuel	SOEX	0.0	0.0	0.0	0.0	0,0	0.0	0.0	0.0	0.0	0.0	0.0
Crude Oil	ğ	-620.0	-652.2	-557.0	-635.0	-699.3	-726.6	-828	-1019	-1164	-1060	-975
Petroleum Products+Bunker	PTEX	0.6-	-0.3	-10.4	-1.4	-15.3	32.5	-107.3	-50.6	-1408.6	-715.4	-777.1
Natural Gas	GAEX	0.0	0.0	0.0	0.0	0.0	-6.7	-13,6	-8-	-283.6	-703.4	-1446.5
Impo. Total	XALE	-611.0	-652.5	-567.4	-636,4	-684.0	-765.8	-948.9	-1,153.6	-2,856.2	-2,478.8	-3,198.6
Stock Change & Some bose 在原數件日本	(4)											
Solid Fuel	SOSC	0.0	0.0	0.0	0.0	00	0.0	0.0	0.0	0,0	0.0	0.0
Orade Oil	SSC	3,4	6.7	5.9	-26.1	13.2	43.1	46,4	-46.4	-46.4	46,4	-46,4
Petroleum Products	PTSC	20.7	-5.0	11.6	11.3	13.7	7.8	. 93	93	93	66	93
Natural Gas	GASC	-137.9	162.0	-108.8	-127.8	-150.0	-235.0	-268.5	-268.5	-268.5	-268.5	-268.5
(Nat. Gas Fleair +Inj.)		-102.3	-124.9	-86.0	-104.2	-122.3	-141.8	-163.5	0.0	0.0	0.0	0.0
Statis. Diff. Total	TLSC	-113.8	-160.3	-103.1	-142.6	-123.1	-270.3	-221.9	-221.9	-221.9	-221.9	-221.9
Primary Energy Requirement(一次供給)	ଝି								660.8			
Solid Fuel	SOPR	6.5	6.4	6.3	6.2	6.4	4.7	4.7	5.127	5,971	7.279	8.873
Crude Oil	CR.	251.0	262.0	233.7	230.6	247.2	305.4	317.7	357.9	470.7	575	659.8
Petroleum Prod.	PTPR	49.6	56.4	59.2	82.2	67.3	24.9	30.9	68.9	251.7	402	524.4
Natural Gas	GAPR	55.3	55.0	52.6	66.7	69.5	91.3	119.4	164	250,7	335.8	415.1
Hydro	HYPR	0.6	8.7	11.7	13.1	11.4	11.7	9.5	13.44	21.75	31.13	40.9
Othres	OTPR	22.4	20.3	23.6	26.2	33.0	31.7	24.9	27.97	29.37	37.98	43,13
Non-Courn.	NOPR	3.5	3.5	3.5	3,3	3.4	3.2	3.2	3.507	3.682	0	. 0
Primary. Total	TLPR	397.3	412.3	390.6	428.3	438.2	472.9	510.3	8,099	1,033.9	1,389.2	1,692.2
(Sum of energy exclude pet.pro.)		347.7	355.9	331.3	346.0	370.9	448.0	479.4	571.9	782.2	987.2	1,167.8
Remark: Any Erroneous of the estimation is	ration is a:											
In order to produce the Tabel, following dat	wing data:	٠										
1) for the Primary enrgy, NIOC data book 7	ata book *											
2) same as, Energy balance Table in IRAN,	in IRAN,											
3) for the industrial sector, Irania.	n authorit											
4) for 'Other' energy in the household sector	hold sector							,				
5) Non-OECD Energy Balance' by OECD/IE	OECD/IE											

Conversion Sector(机效的Pf)												
Refinary		1984	1985	1986	1987	1988	1989	1990	1994	2001	2011	2021
Crude Oil input	CRPT	-251.0	-262.0	-233.7	-230.6	-247.2	-305.4	-317.7	-357.9	-470.7	-575	-659.8
Pet.Prod. Output	PTPT	234.1	240.1	218.0	217.8	233.3	292.8	303.6	341.9	449.8	549.4	630.4
Conversion Loss	TLPT	-16.9	-21.9	-15.6	-12.7	-13.9	-12.6	-14.13	-15.92	-20.94	-25.57	-29.34

3. Estimation of Energy Balance Table with Forecast to 2021 (5)

			2001	7001	1087	3801	000	000	1004	2001	2011	2021
Electric Hallay	ıcar	1304	7027	2001	3	200.4	\D.\.\	2001				
Solid Finel for Power	SOFL	0.0	0.0	0.0	0.0	0.0	0.0	0	0	0	0	0
Pet Pro for Power	PTEL	-30.7	-36.8	-37.1	-32.3	-34.4	-34.5	-38,35	-54.24	.87,79	-125.66	-165.12
Cas for Power	GAEL	-24.1	-24.7	-23.9	-33.8	-35.5	-42.5	-51.5	-72.9	-118	-168.9	-221.9
Generation	ELEL	20.0	21.6	23.0	25.0	25.7	28.7	32.3	46.6	78.11	123.5	179.26
Hydro for Power	HYEL	-9.0	-8.7	-11.7	-13.1	-11.4	-11.7	-9.5	-13.44	-21.75	-31.13	-40.9
Nuclear for Power	NGEL	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Convrsn Loss of Pow.	TLEL	-43.8	-48.6	-49.8	-54.2	-55.5	-60.0	-67.1	-98.3	-165.4	-257.4	-367.5
Effic. of Gene.(%)		31.4	30.8	31.6	31.6	31.7	32.3	32.5	32.5	32.5	32.5	32.5
				٠								
Auto Generation						į		٥	150	81.01	2.7.3	30 21
Petro, input	PIAU	٠	1.0-	-1.0	4.4.	ئ. ين د	) v	, , , ,	7 831	3.495	4 784	5.131
Auto Culput	DATE:	×	, i	Y	4,1	1.6	2.0	2.4	71 27	13.68	15.58	17.38
Loss of auto.	NET .	0.4.	4.2	7.7	-S.	/ 7-	4.0.	1.5	, 6,44	À L		
(a) [ 1:0					-							
CWII ONG						0	0	00	0	0.0	0.0	0.0
Refinary	P10W	0.0	0.0	7.0	0.0	0.0	0.0 0.4	D 6		-14.57	-20.84	-27.36
Fower Flant	2 E		2,6	0.0	7.6	7 4	7.5	44	60.	-15.7	-24.4	-34.9
Own Use 101at	3077	5.5.	0.6.	0.0								
Sestissical Difference	i ·											
Solid	GSOS	0.0	0.0	0.0	0.0	0.0	0.0	0	0	0	0	0.
Petroleum	USTA	-10.0	-4.1	-5.9	.14.5	-14.3	-19.5	-31.1	-31.1	-31.1	-31.1	-31.1
Gas	GASD	0.0	0.0	0.0	0.0	0.0	0.0	0	0	0	0	0
Electricity	ELSD	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Total SD	TLSD	•10,0	-4.1	-5.9	-14.5	-14.3	-19.5	-31.i	-31.1	-31.1	-31.1	-31.1
	į			:								
Final Energy Demand 10tal(最終日子)トー語	第一十七	7007	9001	7001	1007	0001	0001	1000	1994	201	2011	2021
*****	71 50	1901	1200	211 20	220 14	347.25	369.60	386 30	\$05.13	811.16	1,102,51	1.348.53
10121	12.00	049.11	167.54	4:110	00.0	0,00	00.		5117	4 071	7 2 7 0	8 873
Solid Fuel	SOFN	0.50	04.0	06.0	07.0	04.0	255 72	7.4.7	337	572.4	783.4	946,3
Gas	CAFIN	31.20	30.30	28.70	32.90	34.00	48,80	67.9	91.1	132,7	166.9	193.2
Electricity	ELEN	18.40	20.00	21,10	21.80	22.50	25.50	28.5	40.43	67.04	106.95	157.03
Others	OTEN	22.37	20.28	23.57	26.16	33.00	31.68	24.9	27.97	29.37	37.98	43.13
Non-Commercial	NOFN	3.50	3.50	3.50	3.30	3.40	3.20	3.2	3.507	3.682	0	0
Thursday Sector	14.	10.70	70 03	77 21	70 16	79 00	59 00	100 0	9 011	160.3	209.8	236.7
Solid End	NIOS	03.9	00.07	05.4	6.20	04.9	4 70	4.7	5.127	5.971	7.279	8.873
Petroleum Toral	Z Z	46.71	51.13	49.91	50.26	50.80	51.63	53.94	57.62	82.05	106.81	120.29
Gas oil		17.93	20.88	19.64	21.12	20.86	21.14	22.64	24.19	34.44	44.83	50.49
Fuel Oil	* .	28 78	30.26	30.27	29.14	29.94	30.49	31.30	33.43	47.61	61.98	69.80
Gas	GAIN	14.90	14.60	14.40	15.50	15.50	26.80	33.6	37.94	57.51	76.3	85.62
回 86.	ELIN	6.60	6.70	. 02.9	6.20	6.20	7.50	8.7	10.18	14.82	19.4	21.88
Food	TLFO	10.69	11.76	12,32	12.46	12.58	14.44	16.09	19.17	22,48	26,81	30.8
Textile	T,T	5.01	5.49	4.80	4.86	4.90	5.63	6.27	7.28	13.05	13.58	21.56
Wood & Pro.	TLWO	26'0	0.94	0.92	0.93	0.94	1.08	1.2	1.259	64	2.812	2.998
Paper & Pulp	TLPA	1.32	1.48	96'0	0.97	0.98	1.13	1.25	2.585	4.89	6.555	7,196
Chemical	ij	5.04	10.9	7.94	8.03	8.10	9.31	10.36	11.88	24.71	76.67	46.12
Ceramics & Non-metal	E N	37.93	38.39	37.19	37.60	37.95	42.50	48.55	100	16.66	11 25	32.55
Primary Metal	E S	61.4		8,8	, co	/0.6	10.42	10.11	6 457	7.688	2 5 1 5 C	80% 5
Machinary Other Month formations	S E	4,00	3.21	4.60	10,4	ין כ קיל	20.0	n e	25.00	0.054	0.074	0.085
Office retainmentings	7,777	3	70.70	30.50	200	3	22:5	;	222		,	

3. Estimation of Energy Balance Table with Forecast to 2021 (6)

2011 2021			358.5 433					10.883 12.591				70.14 97.11			362.8 431.1				52.6 62.49		0				123.36 139.88							0.00 0.00							
2001		254.9	254.9	246.4	119.12	127.28	8.587	8.587	-		58.93	47,44		٠	284.6	0.	146.1	64.71	40.73	29.37	3.682	•	181.92	00.0	100.43	23.15	25.29	29,37	3.682		102.65	00'0	45.65	41.57	15.43	500	2000		268
1994		124.4	124.4	120.1	58.06	62.04	4.268	4.268			39,19	35.21	6	;	200.4	0	6.86	43.69	26.28	27.97	3.507		149.28	0.00	73.34	27.23	17.23	27.97	3.507		51.08	00.00	25.57	16.46	9.05	0.00			15.05
1990	1990	90.5	90.5	88.8	42.93	45.87	1.64	1.64			26.82	24.62	7.7	e.	144.3	0	76.7	21.9	17.6	24.9	3.2		120.49		61.07	21.12	10.2	24.9	3.2		23.81		15.63	0.78	7.4	0.00			2,000
1989	1989	86.38	86.38	83,66	40.11	43.55	2.72	2.72			25.37	23.37	00.4	,	151.12	0.00	82.44	17.80	16.00	31 68	3.20		123.52		63.69	15.66	9.29	31.68	3.20		27.61		18.75	2.14	6.71	0.00			01.93
1988	1988	82.88	82.88	80.01	38.28	41.72	2.88	2.88			24:72	22.92	7		141.75	0.00	74,15	16.70	14.50	33.00	3.40		113.69		59.18	9.88	8.23	33.00	3.40		28.06		14.97	6.82	6.27	0.00			0.00
1987	1987	84.50	84.50	80.66	38.42	42.24	3.84	3.84			25.68	24.18	200	1.	134.09	0.00	73.84	16.70	14,10	26.16	3.30		103.58		59.27	6.82	8.04	26.16	3.30		30.52		14.57	9.88	90.9	0.00			05.31
1986	1986	78.90	78.90	75.39	36.11	39.28	3.50	3.50			21.92	20.62	2		120.86	00.0	66.59	14.10	13.10	23.57	3.50	•	96.22	:	51.45	10.39	7.30	23.57	3.50		24.64		15.14	3.71	5.80	0.00			5
1985	1985	83.62	83.62	80.25	38.50	41.75	3.37	3.37			23.42	21.92	3		130.54	00.0	79.45	15.50	11.80	20.28	3.50		102.33		64.33	7.57	6.65	20.28	3.50		28.20		15.13	7.93	5.15	0.00			12.50
1984	1984	74.71	74.71	71.18	35.32	35.86	3.53	3.53	٠		19.93	18.83	7		125.11	0.00	72.44	16.10	10.70	22.37	3.50		94.97		58.05	5.13	5.92	22.37	3.50		30.14		14.39	10.97	4.78	0.00			24.70
Year	[ 	TLTR	PTTR	PTTRR			PITTRA	1			TLAG	PTAG	2		TLRE	SORE	PTRE	GARE	ELRE	OTRE	NORE		TLHO	сноз	PTHO	GAHO	ЕГНО	OTTHO	NOHO		TLCM	SOCIA	PTCM	GACM	ELOM	OTCM		Г	Ē
	Fransportation Sector	Total	Petoroleum Total	for Road & Train	Gasoline	Gas oil	for Air	Jet fuel		Agricultural Sector	Total	Gas Oil		Residential/Commercial Sector	Total	Solid Fuel	Petroleum	Gas	Electricity	Other Fuel	Non-Commercial	Household Sector	Total	Solid Fuel	Petroleum	Gas	Electricity	Other Fuel	Non-Commercial	Commercial Sector	Total	Solid Fuel	Petroleum	Gas	Electricity	Other Fuel		Prorev Use	Non-Energy Use Total Non-Energy

# 4. Estimation of Emission Volumes by Use of Energy Balance Table (1)

# SOX

Chit; SOZ Million 10h															
Year	1968	1969	1968 1969 1970 1971	1971	1972	1973	1974	1975	1976	1977	1978	1979		1981	1982
TOTAL EMISSION	0.2044	0.2347	0.2044 0.2347 0.2649 0.2787 (	0.2787	0.2979	0.3785	0.4155	0.4965	0.5706	0.6721	6089.0	0.7247	0.7061	0.7529	0.8183
Conversion Sector	0.0497	0.0628	0.0767	0.0738	0.0701	0.1025	0.1051	0.1349	0.1518	0.1658	0.1820	0.1826	0.1671	0.2007	0.2077
Industrial Sector	0.0771	0.0849	0.0771 0.0849 0.0945 0.1011	0.1011	0.1098	0.1400	0.1541	0.1758		0.2395 0.2227	0.2227	0.2377	0.2680	0.2837	0.3096
Transportation Sector	0.0270	0.008	0.0298 0.0341 0.0387	0.0387	0.0428		0.0609	0.0753		0.1148	0.1217	0.1289	0.1164	0.1155	0.1264
Agricultural Sector	0.0076	0.0081	0.0081 0.0093	0.0103	0.0112		0.0156	0.0189	0.0222	0.0278	0.0290	0.0289	0.0284	0.0308	0.0354
Residential/Commercial Sector	0.0431	0.0491	0.0431 0.0491 0.0504 0.0548	0.0548	0.0640	0.0697	0.0798		0.1078	0.1243	0.1255	0.1466	0.1263	0.1222	0.1392

Unit: NO2 Million Ton

Year	1968 1969 1970 1971	1969	1970	1971	1972	1973	1974		1976	1977	1978	1979	1980	1981	1982
TOTAL EMISSION	0.1090 0.1277 0.1395 0.1498	0.1277	0.1395	0.1498	0.1606	0.1917	0.2121	!	0.2911	0.3515	0.3562	0.3799	0.3365	0.3568	0.3915
Social Conversion Sector	0.0184	0.0307	0.0184 0.0307 0.0335 0.0344	0.0344	0.0347	0.0415	0.0433	0.0501	0.0535	0.0611	0.0586	0.0629	0.0408	0.0628	0.0671
Industrial Sector	0.0114	0.0126	0.0114 0.0126 0.0141	0.0154	0.0178	0.0242	0.0268		0.0348	0.0444	0.0397	0.0447	0.0478	0.0492	0.0555
Transportation Sector	0.0449	0.0449 0.0498 0.0572	0.0572	0.0651	0.0722	0.0885	0.1029		0.1566	0.1946	0.2053	0.2161	0.1942	0.1905	0.2086
Agricultural Sector	0.0024	0.0026	0.0024 0.0026 0.0030 0.0033	0.0033	0.0036	0.004	0.0050		0.0071	0.0089	0.0093	0.0093	0.0091	0.0099	0.0114
Residential/Commercial Sector	0.0318	0.0319	0.0318 0.0319 0.0318 0.03	0.0316	0.0323	0.0331	0.0341		0.0392	0.0425	0.0433	0.0469	0.0446	0.0445	0.0490
				Contract of the Contract of th											

CO2 Unit; Carbon Million Ton															
Year	1968	1969	1970		1972	1973	1974	1975	1976	1977	1978	1979	1980	1981	1982
TOTAL EMISSION	10.67	11.53	12.18		13.57	15.84	17.18	19.59	22.28	26.03	26.07	28.44	26.85	28.12	31.29
Conversion Sector	0 91	1.34	1.55	1.60	1.66	2.3.1	2.47	2.99	3:25	3.76	3.79	4.33	3.60	4.54	5.09
Industrial Sector	1.38	1.53	1.71	1.85	2.14	2.92	3.26	3.74	4.29	5.18	4.78	5.45	5.90	6.21	6.71
Transportation Sector	1 42	1.58	1.83	2.09	2.32	2.86	3.32	4.10	5.00	6.22	6.42	6.49	5.89	5.68	6.36
Agricultural Sector	0.37	0.39	0.45	0.50	2.0	0.67	0.75	0.91	1.07	1.34	1.40	1.39	1.37	1.49	1.71
Residential/Commercial Sector	6.59	6.69	6.65	99.9	6.91	7.09	7.38	7.85	8.66	9.53	69.6	10.78	10.09	10.19	11.42

# 4. Estimation of Emission Volumes by Use of Energy Balance Table (2)

## SOX

Unit; SO2 Million Ton

10. 10. 10. 10.												
Year	1983		1985		1	1988	1989	1990	1994	2001	2011	2021
TOTAL EMISSION	0.9910		1.2164	۲۱		1.1742	1.2127	1.2623	1.6528	2.4969	3.7013	4.2626
Conversion Sector	0.2680	0.3251	0.3842	0.3860	0.3354	0.3548	0.3696	0.4077	0.6103	0.8520	1.2855	1.4034
Industrial Sector	0.3463	0.3659	0.3865		-	0.3834	0.3773	0.3887	0.4318	0.5985	0.7039	0.6862
Transportation Sector	0.1582	0.1730	0.1949	0.1833	0.1961	0.1941	0.2029	0.2148	0.2809	0.5725	1.1031	1.4838
Agricultural Sector	0.0425	0.0460	0.0536	0.0504	0.0591	0.0560	0.0571	0.0602	0.0843	0.1132		0.1957
Residential/Commercial Sector	0.1761	0.1803	0.1972	0.1661	0.1842	0.1858	0.2058	0.1910	0.2456	0.3608	0.4544	0.4935
									***************************************			

# Z

Unit; NO2 Million Ton

The state of the s												
Year	1983		1985	1986	1987	1988	1989	1990	1994	2001	Į	2021
TOTAL EMISSION	0.4785	-	0.5706	0.5440	0.5683	0.5724	0.6127	0.6394	0.8341	1.4821	2.5490	3.3129
Conversion Sector	0.0799	_	0.1012	0.1001	0.0930	0.0957	0.1173	0.1290	0.1785	0.2695		0.5247
Industrial Sector	0.0614		0.0690	0.0671	0.0683	0.0689	0.0704	0.0752	0.0843	0.1175	0.1384	0.1349
Transportation Sector	0.2616		0.3211	0.3021	0.3232	0.3194	0.3336	0.3526	0.4615	0.9416	1.8112	2.4342
Agricultural Sector	0.0136	0.0148	0.0172	0.0162	0.0189	0.0180	0.0183	0.0193	0.0270	0.0363	0.0495	0.0627
Residential/Commercial Sector	0.0620		0.0622	0.0585	0.0649	0.0704	0.0730	0.0633	0.0828	0.1172	0.1457	0.1564

# 202

Unit; Carbon Million Ton

Year	1983	1984	1985	1986	1987	1988	1989	1990	1994	2001	2011	2021
TOTAL EMISSION	38.13	40.53	43.73	41.71	44.44	45.81	49.13	50.48	66.38	104.60	156.11	194.47
Conversion Sector	6.19	7.12	8.00	7.94	8.00	8.37	9.56	10.88	15.83	25.68	39.99	55.19
Industrial Sector	7.45	8.16	8.66	8.48	8.59	8.69	9.55	10.43	11.81	16.72	19.69	18.93
Transportation Sector	7.92	8.62	9.65	9.11	9.76	9.57	9.97	10.4	13.72	28.09	53.71	71.96
Agricultural Sector	2.05	2.22	2.59	2.43	2.85	2.70	2.76	2.91	4 07	5.47	7.46	9.45
Residential/Commercial Sector	14.52	14.41	14.83	13.75	15.25	16.47	17.29	15:81	20.95	28.64	35.27	38.94

5. Selected Ambient Quality Indicators for Various Cites in the World (1)

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		rowth	91 91		w	w	U	U\	U1	U)	w	Ų,	U1	٠٠ •											<i>-</i> 0		•	~	_					<i>د</i> د د	
		Av ann growth rate for series	(percent)	÷	-2.7	-1.6	-6.1	7.4	2.5	3.8	0.3	-0.4	5.7	6.7	:	:	2.4	3.5	-1.1	-1.0	0.5	03	-1.5	2.7	3. 2. 3. 1.		-9.1	:	. :	-6.0	4.5	-2.4	-1.3	6, 1, 9, 7,	2.4
	matter	<u> </u>	_		m	<u></u>	<u>(0</u>	4	<u>0</u>	0	ν.	55	3	0	:	· 	4	1		:	:	1	:	: ]	<u> </u>				:		:	51	<u>~</u>	0.4	<del></del>
-	ticulate	te on	1987-90		41	37	16	23	25	29	435	4	55	58			14	137						. '	185 496							×	53	119	4
	ded par	entrati bic me	p-m4		0	0	00	σı	4	0	5		Ś	S			σ	_	0	3	0	0	:	_,	4:		∞	:	;	<b>~</b>	7	<b>∞</b>	.~	v o	, <i>ι</i> ν
	Suspended particulate matter	an conc	1983-86		50	38	19	20	21	23	475	48	51	48			10	10	14	39	31	46	301	77	3		86			17	18	24	25	135	3
		Annual mean concentration (micrograms per cubic meter)	12		175	112	248	46	224	240	409	171	668	101	:	:	119	.80	154	110	89	09	312	43	159 745		134	:	:	224	061	977	215	172 155	193
		Ann (micr	1979-82		4	4			7	64	4	4	(C)	A	•	:	_			4	4	<b>V</b>	מו נ	V	[-					Ġ		(4	CA.		
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		wth			3.5	13	-0.6	7.7	2.5	9.2	2.5	1.8	4.7	-1.4	11.0	-1.2	:	:	3.8	4.6	8.9	12.0	23.9	:	: :		-7.5	2.5	-1.5	8.4	-9.7	6.9	-2.7	12.4	; ; į
		Av ann growth rate for series	percent)			•	,						,		7				•																
		Av a rate	9			100					~	~~			~~		<b></b>		•												_	10			<del></del>
	Sulfur dioxide	er)	987-90		10,	11.	ιχ	95	8	701	118	õ	ġ,	100	<b>∓</b>	~		•		•	•		•	•	•		41		•	•	•	165	\$	·	,
	Sulfur	n concentration per cubic meter)			_				_								,																		
ļ			1983-86		115	141	78	107	55	%	100	127	107	111	101	157	•	;	23	54	36	86	93	•			4	85	4	34	27	115	61	. 4	1
		ial mea	- 1																									1				٠			
		Annual (microgra	1979-82		77	132	100	59	99	57	105	80	138	116	Ŋ	;	:	;	23	71	36	42	16	;	: :		78	69	43	57	48	130	114	12	:
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		Type of	site		222	CCR	ည္သ	CCR	ပ္သ	CCR	$\frac{1}{2}$	XX.	S	K K	ပ္က	SR	SI	SR	သ	ည္သ	SR	ည်း	ž č	ž;	S. S.			ည္သ	CCR	$\mathcal{C}\mathcal{C}\mathcal{C}\mathcal{C}\mathcal{C}\mathcal{C}\mathcal{C}\mathcal{C}\mathcal{C}\mathcal{C}$		ပ္တန္	ᄎ (	ა გ	S
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			či	omies	Beijing	Beijing	Guar	Guar	Shanghai	Shan	Shen	Shen	Xian	Xian	Cairo	Carro	Accra	Accra	Bombay	Calcutta	Calcutta	O C	Delhi	Jakaria	Lahore	Middle-income economies	Sao 1	Santiago	Santiago	Athens	Athens	Tehran	enran	Kua Kua	Davao
				Low-income economies											Rep.	Rep.	* ·									me ec	•			.*		Rep.	Kep.		
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			Country	Low-	China	China	China	China	China	China	China	China	China	China	Egyp	Egyp	Ghana	Ghana	India	India	India	India	India	Indonesia 1- 4-1-1-1	Indonesia Pakistan	Midd	Brazil	Chile	Chile	Greece	Greece	ran'	ıran,	Malaysia Malaysia	Philip
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5. Selected Ambient Quality Indicators for Various Cites in the World (2)

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	atter	Av ann growth rate for series	(percent)	°.	: :			-2.5 -2.6	0.8	-2.4	-1.7	-2.6	2.5	4 8 c		-2.8		တို လ	-2.2	4,000	3.5.				14.9	: :	:	
	Suspended particulate matter	ation meter)	1987-90	:	:	: :	: (	8 8	244	105	135	91	:	: :	: :	68	: 72	35,	57	42	: :	•	81	4 6	132	: :	: :	
	Suspended	Annual mean concentration (micrograms per cubic meter)	1983-86	:	:	: :	: :	72.	247	163	127	117	58	58 58	77	68	8 %	36	88	20.	χ. Σ	55	62	36	8	:	: :	
		Annual m (microgran		3	:	:	: . :	85	213	136	114	129	71	100 76	47	102	102	28	9 6	22	v 9	53	72	2 2	:	:	: :	
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		Av ann growth rate for series	(percent)	-12.0	4 v		5.4 5.5	-3.0	, ; ;	-1.7	6 4 δ 6	-0.9	-14.3	-10.9	-11.5	:	4:	0.11-	16.0	-7.0	-2.7	-5.7		ا ا	47.3	3.2	-7.1	
	:	Av ar	<u>ğ</u>											<u>.</u>						: :			: <	<u> </u>	) 7	7 -	<del></del>	
	Sulfur dioxide	ition neter)	1987-90		23	27	2.4	27	Ń7	14:	21	47		: :	•	: :	•	: :	14		•		. 9	25	3.2	32	t ·	
	Sul	Annual mean concentration (micrograms per cubic meter)	1983-86	34	 32 132	T &	5 4	21	<b>4</b>	:: 12	27 107	99	<b>v</b> o	28 15	4. 2. t.	<b>'</b> 0	36	253	grant <del>part</del>	: :	: C	27.	: (	28 7. 28	25.55	34	8	
		Annual me (micrograms	1979-82 1	73	47.	ر در د		32	Į.	15	32	33	1	51 31	4.0	· ·	32	4 i 27	: 01	21	18	33 6	24	27	- :	40	) 16	
	_	Type of	site	IS	သည်	 S C S C S C S C	38	CCR	× 5	SR	000	SR	222	SICC	ည	CCC	SR	၁ဗ္ဗ	သည္သ	200	8 8 7	)   	222	SS C	ز : د	IJ {	38	
	•		City	Manila	Warsaw	Warsaw	wroclaw Wroclaw	Lisbon	Lisbon Bangkak	Bangkok	Caracas	Zagreb	nomies Melboume	Sydney Sydney	Brussels	Brusseis Hamilton	Hamilton	Montreal Montreal	Toronto	Vancouver	Vancouver	Copenhagen	Helsinki	Helsinki	Fizhkiut Hong Kong	Dublin	Dublin Tel Aviv	
			Country	Philippines	Poland	Poland	Poland Poland	Portugal	Portugal	Thailand	Venezuela	r ugostavia Yugoslavia	High-income economies Houstralia Melb		Belgium	Belgium Canada	Canada	Canada Canada	Canada	Canada	Canada	Denmark	Finland	Finland	Germany Hono Kone	Ireland	Ireland Israel	

5. Selected Ambient Quality Indicators for Various Cites in the World (3)

			S	Sulfur dioxide				Suspended particulate matter	iculate m	atter
-	•	Annual	nean conce	ration	Av ann growth		Annual n	Annual mean concentration	g	Av ann growth
2	Type of	(microgra	ams per cubic meter)	meter)	rate for series		(micrograi	(micrograms per cubic meter)	eter)	rate for series
Milan	CCC	150.7	06		(percent)	7	70-6/61		06-10	(100,000)
Milan	CCR	259	114	: 1	411.4	. [-	:	: :	: :	:
Osaka	200	37	28	28	4.8-	4	51	4	4	-6.3
Osaka	SR	34	26	24	0.8-	14	61	49	72	4.1
Tokyo	သည	42	23	20	6.8-	17	61	50	:	4.9
Tokyo	SR	42	30	20	-5.7	17	54	51	:	4.5
Amsterdam	သသ	33	24	:	-6.7	15	:	:	:	;
Amsterdam	SR	34	53	:	-1.8	13	;	ï	:	٠.
Auckland	သည	10	m	:	-17.6	ġ	:	:	:	:
Auckland	CCR	∞	m	;	-37.2	9	:	;	:	:
Christchurch	SI	37	43	;	6.9		:	:	:	
Christchurch	SR	20	18	61	-3.5		:	:	:	-:
Madrid	သ	105	54	36	8.6-	17		:	:	:
Madrid	SR	45	28	19	-8.4		:	:	•	:
Glasgow	ည	73	52	:	∞ <u>.</u>	∞,	:	:	:	:
Glasgow	ij	62	41	:	8.6-	σ	:	:	:	;
London	ည	99	4	;	-11.4	13	:	:	:	:
London	SI	56	34	-:	-11.3		:	:	;	;
Birmingham	ည	:	:	:	:	m	83	75		-3.0
Chicago	ij	:	:	:	•	7	121	ጽ	:	-6.2
Fairfield	SI	:	:	:		'n	7.1	53	•	-5.6
Hamis Co.	SR	:	:	•	•	m	89	54	:	4.
Houston	ည	:	:	:		ന	82	62	;	-7.3
Houston	SR	18	œ	:	-32.0	∞	93.25	\$	:	-6.3
New York City	CCR	79	09	:	-5.8	9	63	61	•	-2.2
New York City	SR	38.	31	•	-5.9		- 49	46	:	-2.7

CCC--city center commercial; CCR--city center residential; SI--suburban industrial; SR--suburban residential; SC--suburban commercial. Type of site:

To maximize the number of cities for which data are presented, information is given on only two site types, though more data than this may be available. There are two methods for calculating concentrations of suspended particulate matter; gravimetric measurement and the smoke stain method. These Numbers in parentheses denote the number of years of observations. Data have been presented only when they are available for four or more years. Growth rates are calculated using the entire time-series available, although only part of that series may appear in the concentration data presented. methods are not comparable. Because most air monitoring stations use the former method, only data derived from this method are presented.

Source: The World Bank, 1991

Notes: