5) Amortization

The pre-operation cost and IDC are amortized in equal installments for five years after the plant operation.

6) Summary of the Operational Costs

The summary of the operation costs for model plants based upon the above conditions is shown in Table VII.2-6-1 (without escalation) and Table VII.2-6-2 (with escalation).

2.4 Sources of Funds

2.4.1 Equity

Since there are no long term loans available in Romania at the moment, the study is premised on the preparation by SIDEX of an amount equivalent to the local portion of the project costs for equity, and the remaining project costs are supplemented by a foreign loan.

2.4.2 Loan

Besides the equity, the remaining project costs are scheduled to be fully supplemented by foreign loans whose details are shown below. The foreign borrowing is estimated based on three loan conditions, CASE A, B, and C. CASE A is based upon the condition of an ODA fund from governmental institutions, CASE B, a soft loan from foreign banks, and CASE C, a typical long-term commercial credit.

(1) Long-term Foreign Currency Loan

1. CASE A

Interest rate:

3% per annum

Grace period:

seven years

Repayment:

equal annual installments for eighteen years after

grace period

oppi Hess

* returns

edlowing

2. CASE B

Interest rate:

5% per annum

Grace period:

five years

Repayment:

equal annual installments for ten years after grace

period

3. CASE C

Interest rate:

15% per annum

Grace period:

four years, which is the same period of construction

of facilities

Repayment:

equal annual installments for eight years after

grace period

2.4.3 Summary for the sources of fund

For the conclusion of this Section, the total amount of this project and the source of the funds required for the project are exhibited in Table VII.2-7-1 (without escalation) and Table VII.2-7-2 (with escalation) below.

2.4.4 Hedging of foreign currency fluctuation on long-term debts

Though it is difficult to mention hedging the fluctuations of foreign currencies on long-term loans at the present stage because the currencies on long-term debts have not been decided yet, the following hedging (minimizing) is considered and recommended in general:

- a) Swapping to stabilized currency in international money market
- b) Forward exchange contract in international foreign exchange market
- c) Direct settlement with foreign currency earned by export of products

2.5 Cost Effective Analysis by Financial Internal Rate of Return

2.5.1 Definition

The financial internal rate of return (FIRR) is defined as discount rate equalizing net present value of costs and net present value of returns earned by investments, and shown an "R" calculated in the following

formula:

$$\sum_{t=0}^{n} \frac{1t}{(1+R)^{-t}} = \sum_{t=0}^{n} \frac{St}{(1+R)^{-t}}$$

It : Costs funds in the t-th year

St: Returns in the t-th year

According to the above formula, FIRR is calculated in the following conditions:

FIRR = profit before tax + depreciation cost + amortization cost of deferred assets + interest expense - interest income + book value of fixed assets and inventories at the projection year end + working capital fund at the projection year end

2.5.2 Results of Financial Internal Rate of Return

The result of cost effective analysis for each model plant is summarized in Table VII.2-8-1 (without escalation) and Table VII.2-8-2 (with escalation), and the FIRR for total energy saving, one of the most important figures, is shown below. While FIRR in a fundamental industry like the steel industry is generally around 8.0~15.0%, the revolving rate of capital tends to be high for energy saving projects in general. Irrespective of the difference in the long-term loan conditions in the three cases, CASE A. CASE B, and CASE C, the FIRRs are approximately 19.5% (without escalation), 21.0%(with escalation) in CASE A, 19.2% (w/o escal.), 20.6% (w/ escal.) in CASE B, and 17.2% (w/o escal.), 18.6% (w/ escal.) in CASE C. Therefore, we can say that the investment for energy savings in the study is financially feasible. Since at present LIBOR 6 month (London Inter - Bank Offered Rate) as of September 30, 1994, is 5.6%, the FIRRs in this project are approximately 13 - 15 % better than LIBOR. This means that investment in this project is 13 - 15 % more profitable, if the same amount as the investment were deposited in a bank, although this % range of profit carries an element of variable risk for the project's operation and implementation.

Financial Internal Rate of Return on Total Energy Saving (Model Plants)

	< Without Escalation >	< With Escalation >
CASE A	19.5 %	
CASE B	19.2 %	20.6%
CASE C	17.2 %	18.6%

2.6 Sensitivity Analysis on FIRR

The sensitivity in terms of the savings and the costs to the FIRRs for model plants is analyzed for each loan case, and the result is indicated in Figure VII. 2-1-1. ~ Figure VII .2-3-1. for without-escalation, and Figure VII. 2-1-2. ~ Figure VII .2-3-2. for with-escalation. As a result of the sensitivity analysis, it can be concluded that the viability of the project can be maintained, even if the savings and the costs fluctuate by 5% through 20%.

2.7 Economic Analysis for Energy Saving

In evaluating economic impact for energy saving for model plants by using economic internal rate of return (EIRR) from a country point of view, the key is energy prices that are base for calculating amount of savings. In this study, energy prices are adjusted with international prices listed in Diagram VII 2-2 as the optimal allocated prices of resources. As regards adjustments to shadow wage, shadow exchange coefficient and so on, please note that the same information on wages and exchange rates as those used for the FIRR are adopted in the calculating EIRR, partly because basic information required for calculation is insufficient or not ready for use due to the transition period to the market economy from the socialist planned economy, and partly because most of the costs under the existing

system can be utilized as sunk costs, which indicates that the impact of new input data to be converted by shadow conversion factors is small. The summary of the EIRRs is shown below.

Economic Internal R	ate of Return on Total Energ	y Saving (Model Plants)
. 4==4=================================	<pre>< Without Escalation ></pre>	
CASEA	21.3 %	22.8 %
CASE B	20.9 %	22.4 %
CASE C	18.9 %	20.4 %

2.8 Appraisal of Effectiveness of Other Related Plants on Energy Saving

2.8.1 General

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Evaluated were the effect of investment in other related plants, to which most of the same measures on model plants are applied in the same manner as that in the model plants. The objective sectors are coke oven batteries including CDQs and chemical plants, sintering plants, and blast furnaces. The results of the evaluation from a technical standpoint is described in Article 7 of Chapter IV. Please note that any information or any analysis considered plants are not included in other related plants in Article 2.8 of Chapter VII.

2.8.2 Basis of calculation of FIRR on related plants

The project costs and the amounts of energy saving, as base data for cost effective analysis for other related plants, are respectively US\$ 127,238,000.- and US\$ 21,095,600.-/year. As regards the details, please refer to Table VII.2-9. The schedule of plant construction whose period is 4 years is planned to be started after completion of construction of model plants. The project life is considered to be 15 years from the

commencement of commercial operations.

2.8.3 Analysis of effect

The result of cost effective analysis in the case is summarized in Table VII.2-10-1 (without escalation) and Table VII.2-10-2 (with escalation), and the financial internal rate of return for total energy saving in the case is shown below in order to provide a big picture for consideration.

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Financial Internal Rate of Return on Related Plants for Energy Saving to which the measurements of Model Plants are extended (Related Plants)

·	< Without Escalation >	< With Escalation >
CASE A	8.9 %	10.0 %
CASE B	8.6 %	9.7 %
CASE C	7.1 %	8.1 %
======= =============================		=======================================

As the above FIRRs suggest, it is difficult to say if this investment for other related plants is financially feasible. This is partly because the model plants, compared with the other related plants, can preferentially be operated from a productive efficiency point of view, and this is partly because the other related plants are so obsolete that the investment for other related plants could not gain higher profitability than that for model plants. Because the study of other related plants was only a preliminary one, more detailed survey would be recommendable. Yet please notice that as regards cokes oven batteries, the FIRRs in all loan cases are over 20 %. Therefore, the effect on energy saving of No. 6 & No.7 cokes oven battery (including CDQs) can be said to be financially feasible, in case that the same measurement for No.5 coke model plant is rippled to No. 6 & No.7 cokes.

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3 COST ANALYSIS FOR ENVIRONMENTAL POLLUTION CONTROL

3.1 Cost Effectiveness Analysis

3.1.1 General

Strategies on environmental policy differ from country to country, such as Best Available Control Technology (BACT) in the United States, Best Practical Means (BPM) approach in the United Kingdom, a combined form of BACT and Precautionary approach in EU, and so forth. On the other hand, as regards economic analysis of environmental impacts, there are many methods from an academic standpoint, such as valuation methodology, cost-benefit approaches, willingness-to-pay versus willingness-to-accept approach, and so forth. Those methods are not easily accepted publicly since the economic costs of a project are not relatively easy to quantify, in cases where significant externalities such as environmental impacts are involved. In this study, as described in Chapter VII, 1.1.2, the method of cost-effectiveness analysis is adopted.

Although stage-wise programs for abatement of environmental pollution are supposed to be prepared at the beginning of the study, we set up overcoming Romanian environmental standards as the target.

As ways (= technologies) of achieving the target, particularly, dust collectors and discharging phenol, the technologies for measurement that are described in Chapter III are generic ones and there are little alternatives on the technologies.

As regards NOx from the cokes plant and the sintering plant, the measurement for energy saving concurrently leads to overcoming the environmental emission standards for waste gas.

Although, as regards SOx from the sintering plant in this study, dry type of de-sulfurization system by moving bed of activated coke is recommended, while there is another technology for de-sulfurization, wet type of de-sulfurization system, which additionally requires facilities for

treatment for waste water and needs the same cost as that for the dry type of de-sulfurization system, or a little higher cost. In terms of protecting concomitant pollution out of the first measurement of environmental protection and in terms of monetary view, the dry type of de-sulfurization system is recommended. We have deeply discussed the measurements of SOx with one of our counterparts, SIDEX from technical and economic points of view since the second site survey. As a result of our discussion, the dry type of de-sulfurization system was chosen, which expands that our recommendation has been established based upon the method of cost-effectiveness analysis.

As a result of the evaluation based upon the method of cost-effectiveness analysis, the estimated costs for the environmental pollution control, including the cost of capital and the operational cost are shown as least costs in 3.1.2 and 3.1.3 below.

3.1.2 Cost of capital

The cost for environmental pollution control for model plants and other related plants is estimated in the same manner and the same conditions as those for energy saving. As regards the summary of costs, please refer to Table VI.1-2. (The escalation factor is not considered in the case.) Besides, the costs sorted in the modification costs and the renewal costs of equipment are shown below.

Table VII. 3-1. : Sorted Capital Cost for Environmental Pollution Control

	A) Model Plants	(Unit: K US\$/Y	ear)
	a) Modification of Equipment b) Renewal of Equipment		
	Total		
÷.	B) Other Related Plants	(Unit: K US\$/Y	ear)
	a) Modification of Equipment	28,362	
	b) Renewal of Equipment		
	Total	95,668	

3.1.3 Operational cost

The cost of electricity and active coke for each plant, indicated in Table VII.3-2 below, is required annually.

Table VII. 3-2.: Variable Cost on Investment for Environmental Pollution Control for Model Plant and Other Related Plant

 Control of the property of the pr	
A) Model Plant	(Unit: US\$/Year)
No. 5 Cokes Oven Battery Plant	426,000
No.7 Sintering Plant	3,564,000
No.6 Blast Furnace	560,000
Total	4,550,000
B) Other Related Plant	(Unit: US\$/Year)
No. 5 Cokes Oven Battery Plant	589,000
No.7 Sintering Plant	2,730,000
No.6 Blast Furnace	374,000
Total	3,693,000

3.2 Analysis of Benefits of Environmental Pollution Control and Alternatives

As regards benefits out of the measurements for environmental pollution control, such benefits are considered;

- benefits on health of human beings, such as reduction of occurrence ratio for sickness,
- benefits on living environment, such as the beauties of nature, and
- benefits on economics, such as increase of land prices thanks to the beauties of nature

Since those benefits are difficult enough to measure in monetary terms, the decision maker must determine that the potential benefits justify the costs involved. Accordingly, it is recommended that a decision on environmental pollution control be made mainly from three points of view, : a monetary one, such as investment costs; a legal one, such as environmental

standards; and a scientific one, such as decreased amount of SOx. Since SIDEX is forced to accord with Romanian environmental standards that is not inferior to that in the EU and the technology on environmental pollution control that SIDEX will promote has already been practiced in Japan, it is recommended that SIDEX carry out the benefits on environmental pollution control based upon the study.

For reference, the financial internal rate of return on total investment for both energy saving and environmental pollution control against the amount of savings, as return, from only energy saving for model plants is calculated and shown in Table VII.3-3. These figures illustrate the profitability for the total investment for both energy saving and environmental pollution control from a company, SIDEX's point of view, which means those minimum values can be earned from the study.

Table VII.3-3.: Financial Internal Rate of Return on Total Project

	< Without Escalation >	< With Escalation >
CASE A	9.9 %	10.8 %
CASE B		10.3 %
CASE C		7.9 %

4. COST ANALYSIS FOR OPERATIONAL ASSISTANCE

4.1 Cost of Operational Assistance

The cost for operational assistance for the model plants is estimated in the same manner as that for energy saving. As regards the summary of the cost, please refer to Table VI.4-1. (The escalation factor is not considered in the case.) Note it is difficult to evaluate the impact of the operational assistance on energy savings because the effect varies depending upon to what extent the operational assistance would technically be transferred and to what extent that assistance would be recognized by operators for appropriate and stable operations. Therefore, in the study, the cost of operational assistance is estimated under normal practice based upon the experience of the study team.

Table VII, 4-1. Cost on Operational Assistance

	=======================================
	(Unit: US\$)
No. 5 Cokes Oven Battery Plant	310,000.
No.6 Blast Furnace Plant	250,000
Total construction of the second	560,000

4.2 Effect of Operational Assistance

The effect of operational assistance on energy saving on a 100% technically transferred basis is evaluated in Table VII. 4-2:

Table VII.4-2. Effect of Operational Assistance

en de la companya de La companya de la co	(Unit: US\$/Year)
No. 5 Cokes Oven Battery Plant	327,000
No.6 Blast Furnace Plant	9,283,000
Total	9,610,000

5. ECONOMIC ANALYSIS

5.1 Effect of Foreign Currency Saving

In this study, the foreign portion (85.03%) in the amount of savings without escalation used in the financial analysis on energy saving directly illustrates the effect of foreign exchange saving. In order to precisely determine the net amount of savings of foreign currency, it can be calculated by subtracting the foreign portion of the repayments and the interest for long-term borrowing and the payment for the variable cost from the amount of savings. The summary of Balance of Foreign currencies is shown in Table VII.5-1. The result of calculation is as follows;

	Total Amount	The Annual Average
CASE A	US\$ 556,714,000.	US\$ 37,114,000.
CASE B	US\$ 546,320,000.	U\$\$ 36,421,000.
CASE C	US\$ 438,119,000.	US\$ 29,208,000.

5.2 Improvement of Environment and Its Technical and Educational Influence

As described in Chapter III, the countermeasure on environmental pollution control based on this study leads to reducing the emissions air & water pollution, and waste from SIDEX, and contributes to the improvement of the environment around the works and the workshops. Technology on facilities and know-how in terms of environmental protection based upon the study will have an influence on not only other steel plants, but also other industries in Romania as well as surrounding countries. In this sense, this project is a step in the improvement of the environment by the Romanian iron making industry. In addition, concern for environmental preservation will be sweeping through people around SIDEX and in Romania generally, which will help SIDEX as well as the government of Romania in order to establish a production system for preserving ecological foundations and promote the environmental consciousness of the people.

5.3 Advancement of Energy Saving Technology, and Effective Use of Natural Resources

The measurement on the energy saving based upon the study will promote a steady supply of energy, which will contribute to improvements of the whole industrial structure in Romania. It will also promote the suitable usage of energy, enable the people and companies to utilize existing resources efficiently, and reduce environmental degradation generated by such energy consumption.

5.4 Effect of Environmental Pollution Control and Energy Saving on Other Industries

When this project is completed, it is expected that technology for the saving of energy and environmental pollution control will extend socio-economic added values to all over Romania, and that it will have ripple-effects on other industries that are deeply connected with the steel making industry, such as;

- a) Construction
 - b) Piping and other engineering industries
 - c) Transportation, and repair and maintenance
 - d) Manufacturing and distribution of parts and materials.

Tak	Table VII. 2-1.	1	gy price	Energy price of SIDEX		
	Ene	Energy Unit Price	8	Carolific Value	/alue	Unit price
Item	s)	Lei.				(\$/Gcal)
COKING COAL	00.09		S/t	7,000 kcal/kg	al/kg	8.57
ENERGETIC COAL	45.00		S/t	6.000 kcal/kg	al/kg	7.50
COKE (BLAST FURNACE)	83.64	138,000	\$/t	6,300 kcal/kg	al/kg	13.28
COKE (SINTERING PLANT)	55.27	91,200	5/4	6,300 kcal/kg	al/kg	8.77
TAR	40.61	67,000	lei/t	8.500 kcal/kg	al/kg	4.78
LIGHT OIL	116.97	193,000	lei/t			
втх	123.64	204,000	lei/t			
NH3	30.30	20,000	lei/t			
NATURAL GAS	90.00		\$/kNm3	8,050 kcal/Nm3	al/Nm3	11.18
ELECTRIC POWER	40.61	67,000	\$/MWh	2,450 kcal/kWh	al/kWh	16.57
HIGH PRESSURE STEAM	16.38	27.030	lei/Gcal	35-40 ata	et	16.38
MID. PRESSURE STEAM	10.73	17.700	lei/Gcal	8 -13 ata	et	10.73
BFG	8.95	14,760	14,760 lei/kNm3	800 kc	800 kcal/Nm3	11.18
900	47.52	78,400	78,400 lei/kNm3	4,250 kcal/Nm3	al/Nm3	11.18
02	28.33	46,750	lei/kNm3	1,710 kcal/Nm3	al/Nm3	16.57
N2	16.57	27,341	lei/kNm3	1,001 kcal/Nm3	al/Nm3	16.55
AIR	16.57	27.340	27.340 lei/kNm3	1,000 kcal/Nm3	al/Nm3	16.57
(Exchange Rate: 1.5 = 1.650 Lei.)	 : <u>s</u>					

Diagram VII. 2-1. CALCULATION OF COKE PRICE

Average Yield Rate of Coke; 75.0 %
Unit Rate of COG; 305 Nm³/t
Yield Rate of Tar; 2.9 %
Yield Rate of Light Oil; 1.0 %
Yield Rate of Ammonia; 0.2 %

Unit Rate for Fuels ; 669 x 10³ kcal/t Unit Rate for Electricity ; 32 kWh/t Unit Rate for Steam high press.; 378 kg/t medium press.; 143 kg/t

Coal Cost ; 60 \$ /t
COG Cost ; 11.18 \$ /10⁶ kcal
Tar Cost ; 67,000 lei/t
Light Oil Cost ; 193,000 lei/t
Ammonia Cost ; 50,000 lei/t

Fuel Price ; 11.18 \$/10⁶kcal
Electricity Price ; 67.0 lei/kWh
Steam Price high press. 27,030lei/t
medium press. 17,700lei/t

: Average Price for Cost = Coal Cost + Processing Fees - (COG, Tar, Ammonia,etc)

(Variable Cost) Average Yield of Coke

= 79.5 \$/t

: Price of Coke Powders = Price for Lumps of Coke \times 0.66

(0.66 = price ratio as of Sept., 1994)

Assuming that the ratio between lumps of coke and coke powders is 85% to 15% and that the ratio is applicable for calculating those prices in the study, each price for the lumps of coke and the coke powders is set up, as follows:

Price for Lumps of Coke = 83.8 \$ /t Price for Coke Powders = 55.3 \$ /t

Table VII. 2-2. Summary for Saving Amounts

(Unit: K US\$/Year)

Sect	Measurement for Energy Saving	Basic Saving Amounts	Escalated Saving Amounts
1)	No. 5 Coke Oven Battery Plant	6,583.55	7,632.14
2)	No.7 Sintering Plant	6,024.35	6,983.87
3)	No.6 Blast Furnace Plant	30,216.09	35,028.73
4)	No.3 Reheating Furnace Plant	11,313.00	13,114.87
5)	Energy Supply	4,950.00	5,738.41
	TOTAL FOR ENERGY SAVING	59,086.99	68,498.02

The escalated saving amounts are calculated by multiplying the basic ones by an escalation factor, 1.03^5.

Table Vil.2-3-1. Summary for Escalated Capital Cost, Preoperation Cost, and IDC (Without Escalation)

					٠						(Unit: K US\$)	(nss)
	Sap	Capital Investment	nent	Pre.	Pre-Operation cost	cost		OCI			표	
	F. Portion	F. Portion L. Portion Sub-TTL	SUPTIL	F. Portion	F. Portion L. Portion: Sub-TTL	Sub-TTL	F, Portion	Portion L. Portion	Settle	F. Portion L. Portion	Pertion	ij
No.5 Coke Oven Battery Plant												
Case A	6,769	17.128	23,898	389	0	389	302	Ö	305	7,460	17,129	24,589
Case B	6,769	17,129	23,898	389	0	383	510	Ö	510	7,668	17,129	24,797
S ass	6,769	17,129	23,898	280	0	389	1,608	Ö	1,608	8,766	17,129	25,895
No.7 Sintering Plant												
Case A	7,830	7,430	15,260	339		339	989	0	989	8,855	7,430	16,285
Case B	7,830	7,430	15 260	339	0	339	8	O	1,166	9,335	7,430	16,765
ು ಕಾಶು	7,830	7,430	15,260	339	· · ·	339	3,846	0	3,846	*-	7,430	
No. 6 Blast Furnace Plant												
Case A	70,620	19,270	89,890	389		389	3,604	0	3,604	74,613	19,270	93,883
Case B	70,620	19,270	89,890	389	Ö	389	6,077	Ö	6,077	77,086	19,270	
Casa C	70,620	19,270	08.08	389	····	386	19,283	Ö	19,283	90,292	19,270	109,562
No.3 Reheating Furnace												
Case A	10,175	8,584	18,759	339	Ö	339	978	0	978	11,492	8,584	20,076
Case B	10,175	8,584	18,759	339	Ö	339	1,665	o	1,665	•	8,584	20,763
Oase C	10,175	8,584	18,759	339	0	339	5.560	Ö	5,560	16,074	8,584	24,658
Energy Supply												
Case A	29 767	8,658	38,425	8	0	5	1,640	0	049,	31,507	8,658	40,165
Case B	29,767	8,658	38,425	\$	0	5	2,768	Ö	2,768	32,635	8,658	41,293
O esao	29,767	8,658	38,425	8	O	\$	8,840	Ö	8,840	38,707	8,658	47,365
Total for Energy Saving												
Case A	125,161	61,071	61,071 186,232	1,556	Ö	1,556	7,210	0	7,210	7,210 133,927	61,071	194,998
Cese B	125,161	61,071	61,071 186,232	1,556	Ö	1,556	12,186	O	12,186	12,186 138,903	61,071	61,071 199,974
Case C	125,161	61.071	61.071 186,232	1,556	Ö	1,556	39,137	O		39,137 165,854	61,071	61,071 226,925

Table VII.2-3-2. Summary for Escalated Capital Cost, Preoperation Cost, and IDC (With Escalation)

Flant												(Unit: K USS)	(SSD)
F. Portion L. Pontion Sub-TTL F. Pontion L. Pontion Sub-TTL F. Pontion L. Pontion L. Pontion L. Pontion L. Pontion Sub-TTL F. Pontion L. Pontion L. Pontion Sub-TTL F. Pontion L.		S	tal Investr	nent	Pre	Speration	cost		ည်			Ę	
7,430 18,783 26,213 420 0 420 327 00 7,430 18,783 26,213 420 0 420 551 0 7,430 18,783 26,213 420 0 420 1,738 0 7,430 18,783 26,213 420 0 420 1,738 0 7,430 18,783 26,213 420 0 420 1,738 0 7,430 1,6094 353 0 353 1,222 0 353 7,841 16,094 353 0 353 4,031 0 7,6,818 20,789 97,607 414 0 414 3,883 0 7,6,818 20,789 97,607 414 0 414 20,751 0 7,6,818 20,789 97,607 414 0 414 20,751 0 7,6,818 20,789 97,607 414 0 414 20,751 0 7,6,818 20,789 97,607 414 0 414 20,751 0 7,6,818 20,789 97,607 414 0 414 20,751 0 7,6,818 20,789 97,607 414 0 414 20,751 0 7,6,818 20,789 97,607 414 0 414 20,751 0 7,6,818 20,789 97,807 113 0 113 1,759 0 7,6,818 20,789 9,380 41,629 113 0 113 9,475 0 7,708 135,389 65,767 20,155 1,648 0 1,648 13,021 0 7,6,818 135,389 65,767 20,155 1,648 0 1,648 13,021 0 7,6,818 135,389 65,767 20,155 1,648 0 1,648 13,021 0		F. Portion	L Pondon		F. Portion	L. Portion		F. Porton	L Porton	Sub-TT.	F. Portion	Portion L Portion	Ę
7,430 18,783 26,213 420 0 420 327 0 7,430 18,783 26,213 420 0 420 551 0 8,253 7,841 16,094 353 0 353 720 0 8,253 7,841 16,094 353 0 353 1,222 0 8,253 7,841 16,094 353 0 353 1,222 0 76,818 20,789 97,607 414 0 414 6,544 0 76,818 20,789 97,607 414 0 414 6,544 0 10,638 8,974 19,612 348 0 348 1,736 0 10,638 8,974 19,612 348 0 348 5,790 0 32,249 9,380 41,629 113 0 113 2,268 0 32,249 9,380 41,629 113 0 113 2,268 0 135,388 65,767 20,155 1,648 0 1,648 1,785 0	No.5 Coke Oven Battery Plant												
7,430 18,783 26,213 420 0 420 551 0 7,430 18,783 26,213 420 0 420 1,738 0 8,253 7,841 16,034 353 0 353 720 0 8,253 7,841 16,034 353 0 353 1,222 0 76,818 20,789 97,607 414 0 414 3,883 0 76,818 20,789 97,607 414 0 414 6,544 0 76,818 20,789 97,607 414 0 414 20,751 0 76,818 20,789 97,607 414 0 414 20,751 0 76,818 20,789 97,607 414 0 414 20,751 0 10,638 8,974 19,612 348 0 348 1,736 0 10,638 8,974 19,612 348 <td< th=""><th>Case A</th><th>7,430</th><th>-</th><th></th><th>•</th><th>0</th><th>624</th><th>327</th><th>ö</th><th>327</th><th>8 177</th><th>18,783</th><th>% %</th></td<>	Case A	7,430	-		•	0	624	327	ö	327	8 177	18,783	% %
8.253 7,841 16,094 353 0 353 720 0 353 720 0 353 1,222 0 344 1,223 1,242 0 344 1,223 1,242 0 344 1,223 1,23 1,23 1,244 1,244 1,244 1	Case B	7.430	-			0	420	551	Ö	551	8,401	18,783	27,184
8,253 7,841 16,094 353 0 353 720 0 0 353 720 0 0 353 7,841 16,094 353 0 353 1,222 0 0 353 7,841 16,094 353 0 353 4,031 0 0 35,818 20,789 97,607 414 0 414 6,544 0 76,818 20,789 97,607 414 0 414 20,751 0 10,638 8,974 19,612 348 0 348 1,019 0 10,638 8,974 19,612 348 0 348 1,736 0 32,249 9,380 41,629 113 0 113 2,368 0 113,2249 9,380 41,629 113 0 113 2,368 0 113,32,249 9,380 41,629 113 0 113 3,475 0 113,32,249 9,380 41,629 113 0 113 3,475 0 113,32,249 9,380 41,629 113 0 113 3,475 0 113,32,249 9,380 41,629 113 0 113 3,475 0 113,32,249 9,380 41,629 113 0 113 3,475 0 113,32,249 9,380 41,629 113 0 113 3,475 0 113,32,249 9,380 41,629 113 0 1144 2,41785	೧೩೩೦	84.7		26,213		Ö	8	1,738	0	1,738	9,588	18,783	28,371
8,253 7,841 16,094 353 0 353 720 0 78,841 16,094 353 0 353 4,031 0 76,818 20,789 97,607 414 0 414 3,883 0 76,818 20,789 97,607 414 0 414 20,751 0 76,818 20,789 97,607 414 0 414 20,751 0 10,638 8,974 19,612 348 0 348 1,019 0 110,638 8,974 19,612 348 0 348 1,019 0 32,249 9,380 41,629 1113 0 1113 2,968 0 135,326 9,380 41,629 113 0 1113 2,968 0 135,326 9,380 41,629 113 0 113 2,968 0 115,326 9,380 41,629 113 0 113 2,368 0 113,32,349 65,767 201,155 1,648 0 1,648 7,708 0 15,32,349 65,767 201,155 1,648 0 1,648 7,708 0 1135,386 65,767 201,155 1,648 0 1,648 7,708 0 1,648 13,021	No.7 Sintering Plant												
8,253 7,841 16,094 353 0 353 1,222 0 353 8,253 7,841 16,094 353 0 353 4,031 0 3 353 1,031 0 3 353 1,032 0 353 1,031 0 3 3 3 3,031 0 3 3 3 3,031 0 3 3 3 3,031 0 3 3 3 3,031 0 3 3 3 3,031 0 3 3 3 3,031 0 3 3 3 3,031 0 3 3 3 3,031 0 3 3 3 3,031 0 3 3 3 3,031 0 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3	Case A	8,253	7,841		353	O	353	8	Ö		9,326	7,841	17,167
8,253 7,841 16,094 353 0 353 4,031 0 76,818 20,789 97,607 414 0 414 6,544 0 76,818 20,789 97,607 414 0 414 6,544 0 76,818 20,789 97,607 414 0 414 20,751 0 76,818 20,789 97,607 414 0 414 20,751 0 10,638 8,974 19,612 348 0 348 1,019 0 10,638 8,974 19,612 348 0 348 5,790 0 10,638 8,974 19,612 348 0 348 5,790 0 32,249 9,380 41,629 113 0 113 9,475 0 32,249 9,380 41,629 113 0 113 9,475 0 135,388 65,767 201,155 1,648	88	8,253	7,841				353	1,222	0	•	9,828	7.84	17,669
76,818 20,789 97,607 414 0 414 3,883 0 76,818 20,789 97,607 414 0 414 20,751 0 76,818 20,789 97,607 414 0 414 20,751 0 10,638 8,974 19,612 348 0 348 1,019 0 10,638 8,974 19,612 348 0 348 5,790 0 32,249 9,380 41,629 113 0 113 2,968 0 32,249 9,380 41,629 113 0 113 9,475 0 135,388 65,767 201,155 1,648 0 1,648 7,708 0 135,388 65,767 201,155 1,648 0 1,648 13,021 0	Case C	8,253	7,841	16,094	353		353	4,031	Ö	4,031	12,637	7,841	20,478
76,818 20,789 97,607 414 0 414 6,544 0 76,818 20,789 97,607 414 0 414 6,544 0 76,818 20,789 97,607 414 0 414 20,751 0 10,638 8,974 19,612 348 0 348 1,019 0 10,638 8,974 19,612 348 0 348 5,790 0 32,249 9,380 41,629 113 0 113 2,968 0 32,249 9,380 41,629 113 0 113 2,968 0 113,32,249 9,380 41,629 113 0 113 9,475 0 113,385 65,767 201,155 1,648 7,708 0 1,6	No. 6 Blast Fumace Plant											ı	
76,818 20,789 97,607 414 0 414 6,544 0 76,818 20,789 97,607 414 0 414 20,751 0 7 6,818 20,789 97,607 414 0 414 20,751 0 7 6,818 20,789 97,607 414 0 414 20,751 0 7 6,818 1,019 1 7 6,818 1,019 1 7 6,818 1 7	Case A	76,818					414		O		81,115	•••	20,789 101,904
76,818 20,789 97,607 414 0 414 20,751 0 10,638 8,974 19,612 348 0 348 1,019 0 10,638 8,974 19,612 348 0 348 5,790 0 32,249 9,380 41,629 113 0 113 2,368 0 32,249 9,380 41,629 113 0 113 2,368 0 135,388 65,767 201,155 1,648 0 1,648 7,708 0 135,389 65,767 201,155 1,648 0 1,648 7,708 0 135,389 65,767 201,155 1,648 0 1,648 7,708 0 135,389 65,767 201,155 1,648 0 1,648 7,708 0	Case B	76,818					4 4	6,544	Ö		83,776	•••	20,789 104,565
10,638 8,974 19,612 348 0 348 1,019 0 10,638 8,974 19,612 348 0 348 1,736 0 1 10,638 8,974 19,612 348 0 348 5,790 0 32,249 9,380 41,629 113 0 113 2,968 0 32,249 9,380 41,629 113 0 113 2,968 0 13,249 9,380 41,629 113 0 113 9,475 0 113,388 65,767 201,155 1,648 7,708 0 1	ರಿ ಶಾಶ್ರ	76,818					414	20,751	Ŏ.		97,983	20,789	118,772
10,638 8,974 19,612 348 0 348 1,019 0 10,638 8,974 19,612 348 0 348 1,736 0 1 10,638 8,974 19,612 348 0 348 5,790 0 32,249 9,380 41,629 113 0 113 2,968 0 32,249 9,380 41,629 113 0 113 2,968 0 135,388 65,767 201,155 1,648 0 1,648 7,708 0 1 135,388 65,767 201,155 1,648 0 1,648 13,021 0 1 154,815 0 1 1648 13,021 0 1 154,815 0 1 1648 13,021	No.3 Reheating Furnace												
See 10,638 8,974 19,612 348 0 348 1,726 0 348 1,726 0 348 1,726 0 348 2,790 0 348 3,790 0 348 3,790 0 348 3,790 0 348 3,790 0 348 3,790 0 348 3,790 0 348 3,790 0 348 3,790 0 348 3,790 0 348 3,790 0 348 3,708 3	Case A	10,638					378	•		Ī	12,005	8,974	20,979
5.790 0 348 5,790	Carso B	10,638					348		-	7	12,722	3,974	21,696
32,249 9,380 41,629 113 0 113 1,759 0 13.0 2,249 9,380 41,629 113 0 113 2,968 0 13.0 13.2 2,968 0 13.0 2,249 9,380 41,629 113 0 113 9,475 0 13.0 2,368 0 1,648 7,708 0 1,648 7,708 0 1,648 135,388 65,767 201,155 1,648 0 1,648 7,708 0 1.648 135,388 65,767 201,155 1,648 0 1,648 13,021 0 1,648 13,021 0 1,648 13,021 0 1,648 13,021 0 1,648 13,021 0 1,648 13,021 0 1,648 13,021 0 1,648 13,021 0 1,648 13,021 0 1,648 13,021 0 1,648 13,021 0 1,648 14,785 14,785 14	S strey	10,638					88		0		16,776	8.974	25,750
32,249 9,380 41,629 113 0 113 1,759 0 32,249 9,380 41,629 113 0 113 9,475 0 32,249 9,380 41,629 113 0 113 9,475 0 135,388 65,767 201,155 1,648 0 1,648 7,708 0	Energy Supply												
32,249 9,380 41,629 113 0 113 2,968 0 0 32,249 9,380 41,629 113 0 113 9,475 0 1135,388 65,767 201,155 1,648 0 1,648 7,708 0 135,388 65,767 201,155 1,648 0 1,648 13,021 0 135,388 65,767 201,155 1,648 0 1,648 13,021 0	Case A	32,249					113			-			
135,388 65,767 201,155 1,648 0 1,648 13,021 0 135,388 65,767 201,155 1,648 0 1,648 13,021 0	Case 8	32,249					113				35,330	9,380	44,710
135,388 65,767 201,155 1,648 0 1,648 7,708 0 135,388 65,767 201,155 1,648 0 1,648 13,021 0 1,548 13,021 0	U 33	32,249					113		- 5 ·		41,837	9,380	51.217
135,388 65,767 201,155 1,648 0 1,648 7,708 0 135,388 65,767 201,155 1,648 0 1,648 13,021 0 14,538 65,767 201,155 1,648 0 1,648 41,785 0	Total for Energy Saving												
135,386 65,767 201,155 1,648 0 1,648 13,021 0	V 4880	135,388		201.155			•				144,744		55,767 210,511
125 250 55 757 301 155 1 648 0 1 648 41 785 0	Case B	135,388		201,155					0		150,057		65,767 215,824
20,000 (00,000)	Case	135,388	· · · · · · · · · · · · · · · · · · ·	201,155	1,648		1.648	41,785	٠.	1	178.821		65,767 244,588

Table VII. 2-4-1. Summary for Annual Project Costs (Without Escalation)
Rate of escalation= 0.00%

		1995	1996	1997	1998	1999	TOTAL	
Vo.5 Coke	Total of Foreign (W/ Esc)		1,436	3,360	2,634		7,430	28.3° 71.3°
Öven Plant	(fotal of Local (W/ Esc)	0	3,634 3,670	9,160 12,520	5,989.		7,430 18,783	71,74
••••	Sub Total		5,070	17,520	8,623	••••	26,213	*************
lo.7 Sintering	Total of Foreign (W/Esc)	2,342 2,187	5,337 4,843	574			8,253 7,841	313
last	Total of Foreign(W/Esc)			811			7,84)	48.7
	Sub Total	4,529	10,180	1,385			16,024	
lo 6 Blasi	Total of Foreign (W/Esc)	1,056			14,675		76,818	78.79
urnace Flant	Total of Local (W/Esc)	1,557.			2,174		20,789	21.3
	Sub Total	2,613	31,669	46,476	16,849		97,607	
to 3 Reheating	Total of Foreign (W/Esc)	5,240		•			10,638	54.24
urnace	Total of Local (W/Esc)	4,421					8,974	45.89
••••	Sub Total	9,661	9,951			•••••	19,612	
nergy	Total of Foreign (W.Esc)	6	13,790	9,758	6,701		32,249	77.39
UPP'Y	Total of Local (W/Esc)	0:	4,593				9,380 41,629	22.59
	Sub Total		20,383	12,596	8,650	•••••	41,629	
nerdy	Total of Foreign (W/Esc)	8,638	31,749	50,991	24,010		135,388	67.39

	· · · · · · · · · · · · · · · · · · ·	1995	1996	1997	1998	1999	JATOT	
No.5 Coke	Total of Foreign (W/ Esc)	195	0	o	225		420	100.04
Oven Plant	I oral of Local (W/ Esc)	0:	Ó.	0	Ö.	••••	Ò	0.00
••••••	Sub Total	193	O,	0	225		420	•••••
No.7 Sintering	Total of Foreign (W/Esc)	189	O	164			353	100.03
Plant	Total of Foreign(W/Esc)	0.	0	0:			0	0.0%
****	Sub Total	189	Q.	164			353	
No.6 Blast	Total of Foreign (W/Esc)	189	0	o _i	225		414	100.03
Furnace Plant	Total of Local (W/Esc)	0.	0	0	0		0.	0.0%
*****	Sub Total	189	0	0	225		414	
No.3 Reheating	Total of Foreign (W/Esc)	189	159				348	100.07
Furnace	Total of Local (W/Esc)	0	O.				0	0.0%
	Sub Total	189	159				348	
Energy	Total of Foreign (W/Esc)	0	0	0;	113		113	100.0%
Supply	foral of Local (W/Esc)	O.	Ű.	O:	Ö.		0	0.07
	Sub Total	. 0	0	0	113		103	•
Se-	Total of Foreign (W/Esc)	762	159	164	563		1.648	100.0%
Operation	Total of Local (W/Esc)	···					\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	0.0%
Cheranon Loral	HOTAL	762	139	164	363		1,648	Y.Y.X

		1995	1926	1997	1998	1999	TOTAL	
lo.5 Coke	Case A (Interest: 30%)	3	27	100	197		327 331	
oven Plant	Case B (Interest: 5.0%)	5	46	168. 520.	332		551	
	Case C (Interest: 15.0%)	15	132	520;	1,064		1,738	
lo.7 Sintering	Case A (Interest: 3.0%)	38	157	253	272		720	
lant	Case 8 (Interest: 5.0%)	63	263	428	468		1,222	
	Case C (Interest: 15.0%)	190	808	1,385	1,648		4,031	
lo 6 Blast	Case A (Interest: 3.0%)	19	395	1,323	2,146	,,	3,883	
urnace Plant	Case 8 (Interest: 5.0%)	311	639.	2,219:	3,635		6,544	
	Case C (Interest: 15.0%)	93	1,985	6,864	11,809	.,,,,	20,751	
io 3 Reheating	Case A (Interest: 3.0%)		249	339	350		1,019	
บเบอด4	Case B (interest: 5.0%)	136	417	577:	606.		1,736	
	Case C (interest: 15.0%)	407	1,292	1,903	2,188		5,790	
neigy	Case A (Interest: 3.0%)		237	627	895		1,759	
unply	Case B (Interest; 5.0%)	Ŏ:	395	1,053	1.520:		2,968	,,
	Casa C (Interest: 15.0%)	0,	1,184	3,278	5,013		9,475	
	Sub Total						ļ	
	Case A (Interest; 3.0%)	• 142	1,065	2,642:	3,859		1,708	7,70
	Case 8 (Interest; 5.0%)	235	1,780	4,445	6,5611	*********	13,021	13.02
	Case C (interest: 15.0%)	703	5,408	13,950	21,722		41,785	41,78

		1995	1996	1997	1998	1999	TOTAL.	
Total	Total of Foreign (W/ Esc)		İ				l	
	Case A (Info:est: 3.0%)	9,542	52,973	53,797	28,432		144,744	144
	Case B (Interest: 5.0%)	9,635	\$1,688	55,600	31,134		150,057	150
	Case C (Interest: 15.0%)	10.105	57,316:	65.105	46.295		178.821	178

Table VII. 2-4-2. Summary for Annual Project Costs (With Escalation)
--	------------------

See State Control of Control	TOTAL	29	1	1998	1997	1996	1995		
Section	7,430 28 18,783 71, 28,713 71,			2,634 5,989 8,623	3,360 9,160 12,520	1,438 3,634 3,070	0 0	Total of Local (VV/ Esc)	io 5 Colu Oven Plant
10.00 10.0	8,233 7,841 16,054		·····			3,337	2,342 2,187 4,529	Total of Foreign (W/Esc) Total of Foreign(W/Esc) Sub-Total	
Color Colo	76,818 78 20,789 21 97,807			14,675 2,174 16,849		23,788 7,881 31,662	1,056 1,557	Total of Local (WESC)	
Secretary Grad of Conference 1 1 1 1 1 1 1 1 1	10,638 34 8,974 43 19,612						5 240 4 421 9 661	Total of Local (VV/Esc)	
B) Pre-Operation (Escalated)	32,249 77 9,380 22 41,829 22			6,701 1,949 8,650	9.758 2.838 12.596		0	Total of Local (W/Esc)	
B) Pre-Operation (Escalated)	135,388 67 65,767 11 201,155			24,010 10,132 34,122	50,991 21,986 72,977	\$1,749 25,564 77,253	8,638 8,165 16,803	Total of Local (W.Esc)	aving
1995 1996 1997 1998 1999 1998 1999 1998 1999 1998 1999 1998		L				1		ion (Escalated)	B) Pre-Operat
Sob Total 193 0 225 4 4	TOTAL :	99	Ш		1	1996			,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,
Sob Total 193 0 164 33 33 34 34 34 34 34	420 100 0 0			n.	0	0	195	Total of Foreign (W/ Esc)	Vo.5 Coka Non Plant
Stant	420			225	ŏ	ŏ		Sub Total	
Sub Total 189	353 100 0 0						189	Total of Foreign (W/Esc)	No.7 Sintering
Social Cotal of Equip (WEsc) 189 0 0 223 4	353				164	ŏ	189	Sub Total	
Supply Total of Local (W.Esc) 189 159	414 100 0 0 414			225 0 223	. 0:	0. 0	189 0 189	Total of Local (W/Esc)	
Total of Local (W/Esc)	348 100 0 0					159 0 159	189	Total of Foreign (WEsc) Total of Loca! (W€sc) Sub Total	
Operation India of Local (W/Esc) O	113 100 0 0 113)13 0 113	0 0 0		0 0 0	Total of Local (W/Esc)	
1975 1996 1977 1998 1999 101A	1,645 100 0 0 1,648			U.	O.	0	Ų.	Total of Local (W/Esc)	Pre- Operation Total
No.7 Sintering Case A. (Interest: 3.0%) 38 137 233 272 7 Plant Case B. (Interest: 5.0%) 63 263 428 468 4.0 No.6 Blast Case A. (Interest: 3.0%) 19 355 1,333 2,146 3.8 Furnace Plant Case B. (Interest: 3.0%) 31 659 2,219 3,633 6.3 Furnace Plant Case B. (Interest: 15.0%) 93 1,985 6,864 11,809 20.3 No.3 Reheating Case A. (Interest: 3.0%) 81 249 319 330 1.0 Furnace Case B. (Interest: 15.0%) 93 1,985 6,864 11,809 20.3 No.3 Reheating Case A. (Interest: 3.0%) 81 249 319 330 3.0 Furnace Case B. (Interest: 15.0%) 907 1,292 1,900 2,188 37 Case C. (Interest: 15.0%) 907 1,292 1,900 2,188 37 Case C. (Interest: 15.0%) 907 1,292 1,900 2,188 37 Case C. (Interest: 15.0%) 90 325 1,053 1,520 3,530 Case C. (Interest: 15.0%) 90 1,184 3,278 5,013 9,4 Sub Total Case A. (Interest: 3.0%) 9,4 Case B. (Interest: 15.0%) 705 1,408 11,950 21,712 47,7 GRAND TOTAL (A)+B)+C))	IUIXL !	77 T	·	- 3661	-	1998 1	1995	crest During Construction)	C) 1DC (= Int
No.7 Sintering Case A. (Interest: 3.0%) 38 137 233 272 7 Plant Case B. (Interest: 5.0%) 63 263 428 468 4.0 No.6 Blast Case A. (Interest: 3.0%) 19 355 1,333 2,146 3.8 Furnace Plant Case B. (Interest: 3.0%) 31 659 2,219 3,633 6.3 Furnace Plant Case B. (Interest: 15.0%) 93 1,985 6,864 11,809 20.3 No.3 Reheating Case A. (Interest: 3.0%) 81 249 319 330 1.0 Furnace Case B. (Interest: 15.0%) 93 1,985 6,864 11,809 20.3 No.3 Reheating Case A. (Interest: 3.0%) 81 249 319 330 3.0 Furnace Case B. (Interest: 15.0%) 907 1,292 1,900 2,188 37 Case C. (Interest: 15.0%) 907 1,292 1,900 2,188 37 Case C. (Interest: 15.0%) 907 1,292 1,900 2,188 37 Case C. (Interest: 15.0%) 90 325 1,053 1,520 3,530 Case C. (Interest: 15.0%) 90 1,184 3,278 5,013 9,4 Sub Total Case A. (Interest: 3.0%) 9,4 Case B. (Interest: 15.0%) 705 1,408 11,950 21,712 47,7 GRAND TOTAL (A)+B)+C))	327			197	100	27	3	Case A. Cinterest: 3.0%)	No 5 Coke
No.6 Blast	327 331 1,738 720		•		168 520			Case B. (Interest: 5.0%) Case C (Interest: 15.0%)	Oven Plant
No.3 Reheating Case A. (Interest: 3.0%) 81 249 339 350 1,0 Furnace Case B. (Interest: 5.0%) 136 411 577 606 1,7 Case C. (Interest: 15.0%) 407 1,222 1,003 2,188 5,7 Energy Case A. (Interest: 3.0%) 0 237 627 895 1,7 Supply Case B. (Interest: 5.0%) 0 355 1,055 1,520 2,5 Case C. (Interest: 15.0%) 0 1,184 3,278 5,013 9,4 Sub Total Case A. (Interest: 3.0%) 142 1,055 2,642 3,859 7,7 Case B. (Interest: 5.0%) 215 1,760 4,445 6,561 13,0 Case C. (Interest: 15.0%) 7,05 5,408 13,950 21,732 GRAND TOTAL (A)+B)+C))	3,222 4,031			468 1,648	428 1,385	263 808	63 190	Case B (Interest: 5,0%) Case C (Interest: 15,0%)	No.7 Sintering Plant
Corgy Case A. (interest: 3.0%) 0 237 627 895 1,7 Sepply Case B. (interest: 5.0%) 0 395 1,053 1,520 2,6 Case C. (interest: 15.0%) 0 1,184 3,278 5,013 5,4 Sub Total 2,40 A. (interest: 3.0%) 142 1,055 2,642 3,859 7,7 Case B. (interest: 5.0%) 7,55 3,408 13,950 21,722 41,7 GRAND TOTAL (A)+B)+C))	3,683 6,544 20,751			3,635 11,809	1,323 2,219 6,864	659 1,985	31 93	Case B (interest: 5.0%)	No.6 Blast Furnace Plant
Supply Case 8. (Interest; 5.0%) 0 393 1,033 1,520 2,5	1,019 1,736 3,790			2,188	577	1,392	407	Case 8 (interest: 5.0%)	
Case A (referest: 3.0%) 142 1,055 2,642 3,859 7,7 7,7 7,5	1,759 2,968 9,475			895 1,520 5,013	627 1,053 3,278	237 393 1,184	0	Case 8 (Interest: 5.0%)	Energy Supply
	7,768 13,021 13,785			3,859 6,561 21,722	2,642 4,445 13,950	1,085 1,780 5,408	142 233 705	Case A (Interest: 3.0%)	
1995 1996 1997 1998 1999 TOTA								AL (A)+B)+C))	GRAND TOT
	TOTAL	22		1998	1997	1996	1995		
Total Total of Foreign (W.Esc.) Case A. (Interest: 3.0%) 9,542 52,973 53,797 28,432 144,7 Case B. (Interest: 5.0%) 9,633 53,688 53,600 31,134 150,0 Case C. (Interest: 15.0%) 10,105 37,316 65,105 66,265 178,8	144,744 144 150,057 150 178,821 179			28,432 31,134	53.797 53.600	52,973 53,688	9,542 9,633	Case A (interest: 3 0%) Case B (interest: 5 0%)	Tota!

Table VII. 2-5. Salaries Levels for Operators in SIDEX

			on June 30t	h, 1994
	Basic salary	Additional salaries for	Tax	Pension
	;	special working condition	\$	
	lei (@)	= @ * %	= @ * %	= @ * %
coke-maker	184,000	60	30	3
analyst	184,000	60	30	3
blast-furnace worker	172,500	55	30	3
sintering worker	172,500	55	30	3
locksmith, mechanic, electrician	166,750	55	30	3
for maintenance				
reheating furnace operator	172,500	55	30	3
Hot Strip Rolling Mill	243,800	50	30	3
engineer (university)	254,150	45	30	3
unskilled worker	126,500	50	30	3

Table Vil.2-6-1. Summary for Annual Operation Cost (Without Escalation)

						(DO - ACC V 1860)	/ 200
							·
	Veriable Costs	Labor Cost	Maintenace	Engineering	Equip. & Matts	Amortization	E
No.5 Coke Oven Battery Plant		4*****					
Case A	24.0	00	563.3	233.0	1,022.3	138.2	1,980.8
Case B	24.0	o	563.3	233.0	1,022.3	179.8	2,022.4
Case C	24.0	0.0	563.3	233.0	1,022.3	399.4	2,242.0
No.7 Sintering Plant							
Case A	6.53	9.6	496.0	184.2	663.1	205.0	8.109.1
Case B	6.54	9.6	0.967	184.2	663.1	301.0	1,697.8
Case C	63.9	9.6	496.0	184.2	663.1	837.0	2,233.8
No. 6 Blast Furnace Plant							
Case A	0.08	23.9	1,798.0	1,014.2	4,546.2	798.6	8,270.9
S esta S	90.0	23.9	1,798.0	1,014.2	4,546.2	1,293.2	8,765.5
) 97E)	9.0	23.9	1,798.0	1,014,2	4,546.2	3,934.4	11,406.7
No.3 Reheating Furnace							
Case A	19.0	0.0	375.0	208.6	923.6	263.4	1.789.6
Case B	19.0	0.0	375.0	208.6	923.6	400.8	1,927.0
೦೫೮೦	19.0	0.0	375.0	208.6	923.6	1,179.8	2,706.0
Energy Supply			.,,,,,,,,				
Case A	38.0	0.0	769.0	403.2	1,812.1	348.0	3,370.3
Case B	38.0	0.0	769.0	403.2	1,812.1	573.6	3,595.9
O oseo	38.0	0	769.0	403.2	1,812.1	1,788.0	4.810.3
Total for Energy Saving							
	215	ੜ	8,4	2,043	8,967		17,013
	215	**	8	2,043	8,967	2,748	18,009
	215	8		2.043	8.967	8,139	23,399

(") The depreciation of engineering and the amortization are valid for 5 years from the start-up of operations base upon the startight-line mentios, and the depreciation of equipment and machinery, 15 years.

Table VII.2-6-2. Summary for Annual Operation Cost (With Escalation)

						(Unit: K USS/Year)	SS/Year)
				Oepredauon	Gauon	;	
	Variable Costs	Labor Cost	Maintenace	Engineering	Equip, & Mads	Amortization	T.
No.5 Coke Oven Battery Plant							
Caso A	26.0	0.0	563.3	255.8	1,121.5	149.4	2,116.0
Case 8	26.0	0.0	563.3	255.8	1,127.5	194.2	2,160.8
Case C	26.0	0.0	563.3	255.8	1,121.5	431.6	2,398.2
No.7 Sintering Plant							
Case A	6.03	9.6	496.0	18.2	699.3	214.6	1,657.6
Cato B	43.9	9.6	496.0	194.2	699.3	315.0	1,758.0
Case C	63.9	9.6	496.0	<u>\$</u>	699.3	876.8	2,319.8
No. 6 Blast Fumace Plant							
Case A	98.0	83.9	1,952.0	1,103.2	4,941.5	859.4	8,978.0
Case 8	98.0	23.9	1,952.0	1.183.2	4,941.5	1,391.6	9,510.2
S eses	98.0	23.9	1,952.0	1,103.2	4,941,5	4,233.0	12,351.6
No.3 Reheating Furnace							
Case A	20.0	0.0	392.0	218.0	965.6	273.4	1,869.0
Case B	8	0.0	392.0	218.0	965.6		2,012.4
Case C	20.0	0.0	392.0	218.0	965.6	1,227.6	2,823.2
Energy Supply							
Case A	42.0	0.0	833.0	436.8	1,963.2	374.4	3,649.4
Case 8	42.0	00	833.0	436.8	1,963.2	616.2	3,891.2
O SSEO	42.0	0.0	833.0	436.8	1,963.2	1,917.6	5,192.6
Total for Energy Saving							
	8 8	R	4,236	2,210	9,691	1,871	18,272
Market angles	230	35	4,236	2,210	9,691	2,934	19,335
	230	28	4,236	2,210	9.691	8,687	25.087
(1) The decreasion of engineering and the smortization are valid for 5 years, from the startists of engineering	nd the smortzation	are valid for 5 v	ats off mont year	State of the State		Adeisabeta	l

(*) The deprecation of engineering and the amortization are valid for 5 years from the start-up of operations base upon the startight-line mehitos, and the deprecation of equipment and machinery, 15 years.

Table VII. 2-7: Required Funds

CASE A	W	th Escalation		Witt	hout Escalatio	n ,
· ·		(Unit: K	(US\$/Year)		(Unit: 1	K US\$/Year)
	Loan	Equity	Total	Loan	Equity	Total
No.5 Cokes Oven Battery Plant	8,177	18,783	26,960	7,460	17,129	24,589
No.7 Sinter Plant	9,326	7,841	17,167	8,855	7,430	16,285
No.6 Blast Furnace Plant	81,115	20,789	101,904	74,613	19,270	93,883
No.3 Reheating Furnace Plant	12,005	8,974	20,979	11,492	8,584	20,076
Energy Supply	34,121	9,380	43,501	31,507	8,658	40,165
Total for Energy Saving	144,744	65,767	210,511	133,927	61,071	194,998
	68.76%	31.24%		68.68%	31.32%	

CASE B	Wi	th Escalation		With	nout Escalatio	n
		(Unit: k	(US\$/Year)		(Unit:	K US\$/Year)
	Loan	Equity	Total	Loan	Equity	Total
:						
No.5 Cokes Oven Battery Plant	8,401	18,783	27,184	7,668	17,129	24,797
No.7 Sinter Plant	9,828	7,841	17,669	9,335	7,430	16,765
No.6 Blast Furnace Plant	83,776	20,789	104,565	77,086	19,270	96,356
No.3 Reheating Furnace Plant	12,722	8,974	21,696	12,179	8,584	20,763
Energy Supply	35,330	9,380	44,710	32,635	8,658	41,293
Total for Energy Saving	150,057	65,767	215,824	138,903	61,071	199,974
	69.53%	30.47%		69.46%	30.54%	

CASE C	Wi	th Escalation		Witt	nout Escalatio	n
		(Unit: k	(US\$/Year)		(Unit: 1	K US\$/Year)
	Loan	Equity	Tolal	Loan	Equity	Total
No.5 Cokes Oven Battery Plant	9,588	18,783	28,371	8,766	17,129	25,895
No.7 Sinter Plant	12,637	7,841	20,478	12,015	7,430	19,445
No.6 Blast Furnace Plant	97,983	20,789	118,772	90,292	19,270	109,562
No.3 Reheating Furnace Plant	16,776	8,974	25,750	16,074	8,584	24,658
Energy Supply	41,837	9,380	51,217	38,707	8,658	47,365
Total for Energy Saving	178,821	65,767	244,588	165,854	61,071	226,925
	73.11%	26.89%		73.09%	26.91%	

Table VII. 2-8-1. Summary of FIRR on Energy Saving of Model Plants (Without Escalation)

	CASEA	CASEB	CASEC
1) Cokes Oven Battery	19.1%	19.0%	18.2%
2) Sintering	20.2%	19.9%	17.9%
3) Blast Furnace	21.4%	21.0%	18.9%
4) Reheating Furnace	27.5%	27.0%	24.7%
5) Energy Supply	5.9%	5.6%	4.1%
6) Total (Energy)	19.5%	19.2%	17.2%

The word, FIRR means "Financial Rate of Return."

a) Equity Condition	Since there are no long term loan available locally in Romania at present, this study is examined based upon premise that	locally in Romania at present, this study i	s examined based upon premise that
	SIDEX could prepare an amount equivalen	t to the local portion of inflated project cos	SIDEX could prepare an amount equivalent to the local portion of inflated project cost as equity and that the remained project costs
	could be supplemented by foreign loan(s) for each case.	or each case.	
b) Loan Conditions			
	CASE A	CASE B	CASEC
Interest Rate	3% per annum	5% per annum	15% per annum
Repayment Period	25 years (inclining Grace Period)	15 years (ind. G/P)	12 years (incl. G/P)
Grace period	7 years	5 years	4 years(=Modernization Period)

Table VII. 2-8-2. Summary of FIRR on Energy Saving of Model Plants (With Escalation)

	CASE A	CASEB	CASEC
1) Cokes Oven Battery	20.4%	20.2%	19.5%
2) Sintering	22.1%	21.7%	19.7%
3) Blast Furnace	22.8%	22.4%	20.2%
4) Reheating Furnace	29.5%	29.0%	26.7%
5) Energy Supply	6.8%	6.5%	4.9%
6) Total (Energy)	21.0%	20.6%	18.5%

The word, FIRR means "Financial Internal Rate of Return."

Hemarks		- 1		•
a) Equity Condition	Since there are no long term loan available	no long term loan available locally in Romania at present, this study is examined based upon premise that	ined based upon premise that	
	SIDEX could prepare an amount equivalent	SIDEX could prepare an amount equivalent to the local portion of inflated project cost as equity and that the remained project costs	uity and that the remained project costs	
	could be supplemented by foreign loan(s) for each case.	or each case.		
b) Loan Conditions				
	CASE A	CASEB	CASEC	
Interest Rate	3% per annum	5% per annum	15% per annum	:
Repayment Period	25 years (inclining Grace Period)	15 years (incl. G/P)	12 years (incl. G/P)	
Grace period	7 years	5 years	4 years(=Modernization Period)	;

CASE A (FIRR W/O Escal.)

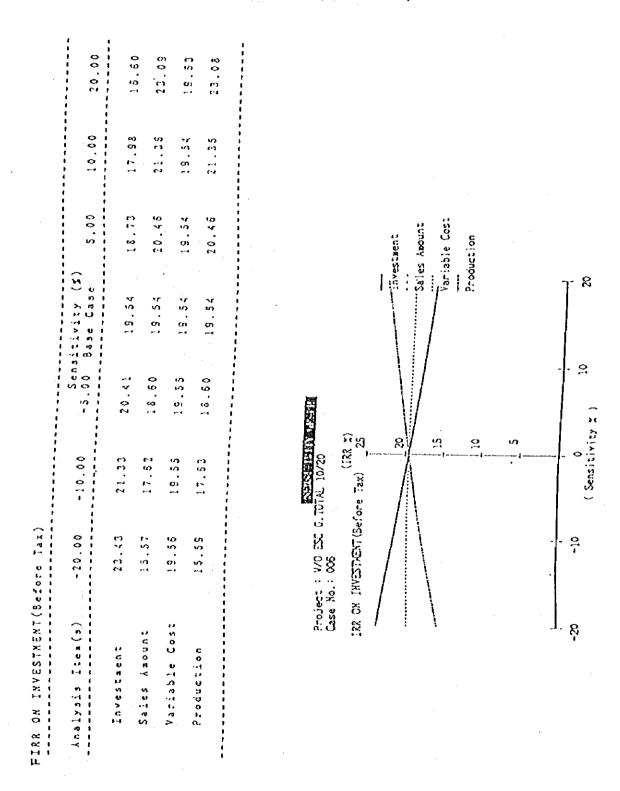


Fig. VII.2-1-1. Case A: Sensitivity analysis (without escalation)

CASE B (FIRR W/O Escal.)

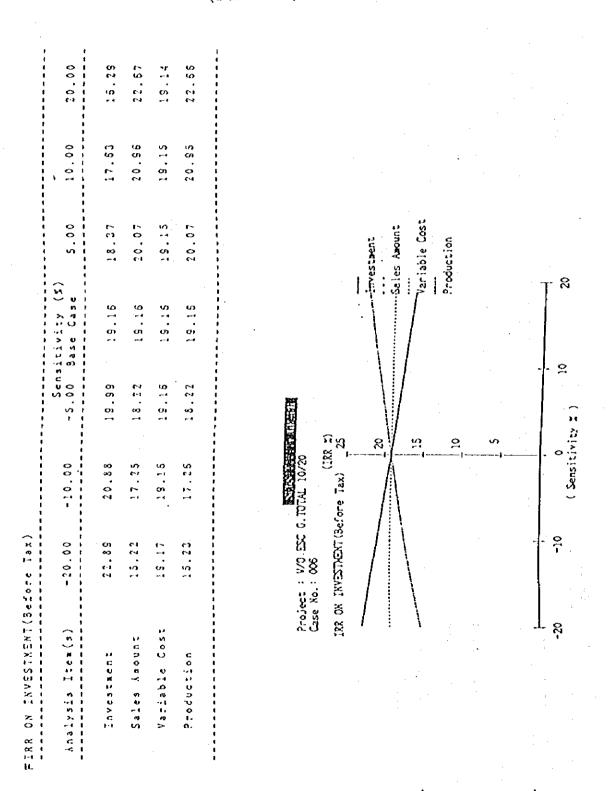


Fig. VII.2-2-1. Case B: Sensitivity analysis (without escalation)

CASE C (FIRR W/O Escal.)

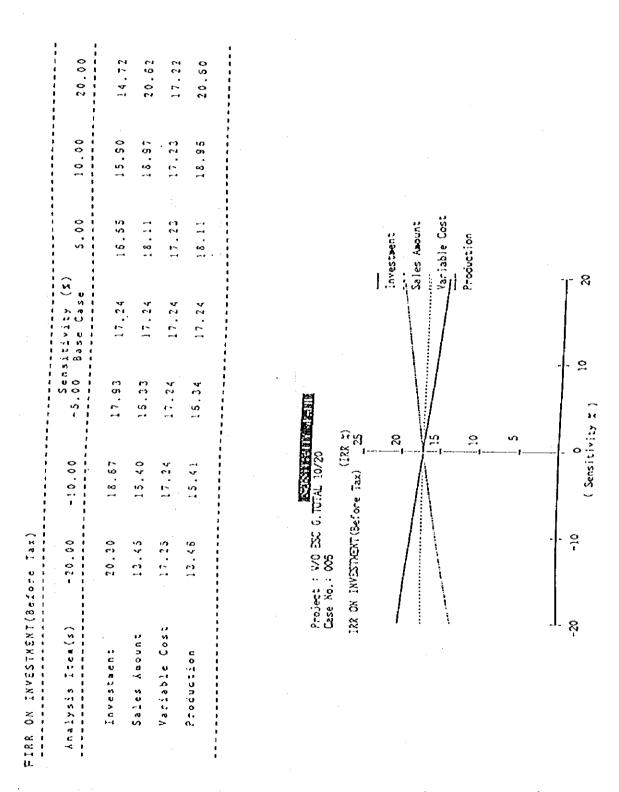


Fig. VII.2-3-1. Case C: Sensitivity analysis (without escalation)

CASE A
(FIRR W/ Escal.)

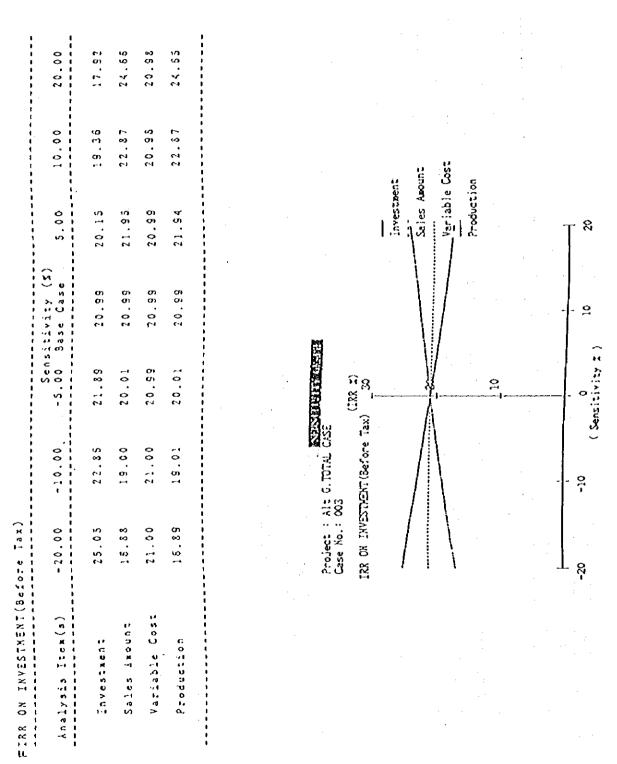


Fig. VII.2-1-2. Case A: Sensitivity analysis (with escalation)

CASE B (FIRR W/ Escal.)

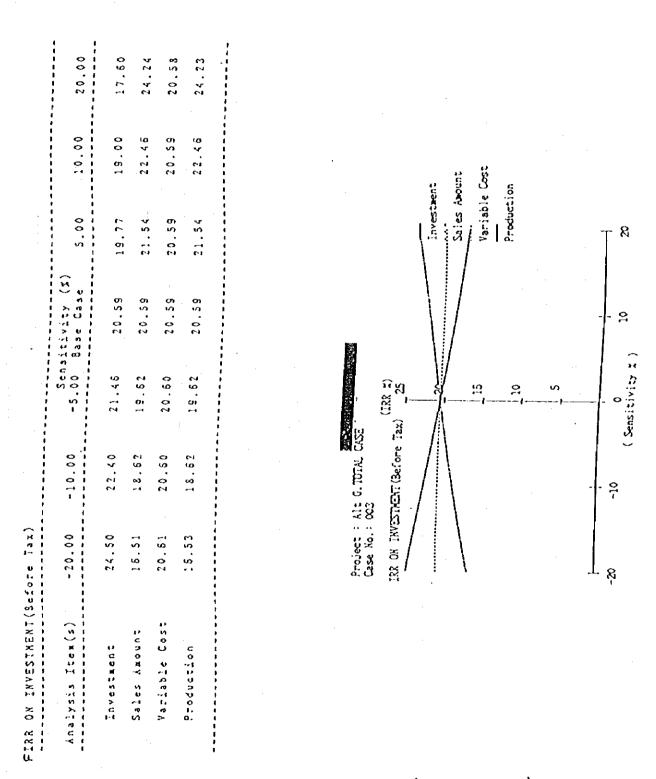


Fig. VII.2-2-2. Case B: Sensitivity analysis (with escalation)

CASE C (FIRR W/ Escal.)

Sales Awount 14.71 16.73 19.35 18.63 17.91 17.24 16.00 Sales Awount 14.71 16.73 17.69 18.63 19.54 20.43 22.13 Variable Cost 18.64 18.63 18.63 18.63 18.62 18.62 Production 14.72 15.73 17.70 18.63 18.54 20.42 22.12 Stocker: All G.TUTAL CASE TRANSMIRM MATERIAL AND MAT	Assign Horse (n)	- 20,00	10.00	Sea - 5.00	Shthemay (M) Base Gase	8.00	00.01	20.00
Sales Amount 14.71 15.73 17.69 18.63 18.54 20.43 22 Variable Cost 15.64 18.53 18.65	0 4 0 4 0 0 0	on				1 0	17.24	1 0
Production 14.72 15.73 15.70 18.62 18.62 18.62 22 Production 14.72 15.73 17.70 18.62 19.54 20.42 22 Case No. 1003 IRR ON INVESTIGATION 25 10	Sales Amount	14.71	16.73	17.69		•	20.43	
Production 14.72 15.73 17.70 13.53 19.54 20.42 22 22 22 22 22 23 24.72 25 25 25 25 25 25 25 25 25 25 25 25 25	S O	₩ ••••••••••••••••••••••••••••••••••••	61 50 80	18.53	•	•	18,62	
Project : Alt G. 101AL CASE Case No.: 003 IRR ON INVESTIGNT(Sefore Tax) 25 20 20 20 -20 -10	·- I	14.72	15.73	7.30	•		20.42	22.12
Diect : Alt G. 707AL CASE Se No. : 003 ON INVESTINGNT (Sefore Tax) 25 10 10 -10 -10 0	1 1 1 1 1	1	1 1 1 1 1 1 1					1
Duect : Alt G.:DTAL CASE se No.: 003 ON INVESTIGATION ON INVESTIGATION 10 10 10 10			4					
Seet: Alt G. TOTAL CASE Se No.: 003 ON INVESTIGATION INC.: 003 ON INVESTIGATION INC.: 003 INC.								
ON INVESTIGNT (3efore Tax) 25 20 20 15 16 10 -10 0		Project : Case No. :	AIS G. TOTAL CO	SE TENTA				
15 10 -10 -10		EVKI NO ARI	STAENT (Before	Tax) (TRR ±)				
15 10 -10 -10 10				<u>.</u>		Invest	9653 t	
15 10 -10 -10 10						. 28 S	Mount	
-10						Variab	le Cost	
-10			:	2		Product	ion	t.
-10				1			-	
0.01		-		I	÷			
0,000	•	:			:		†.	
		-20		. 0		3 -		

Fig. VII.2-3-2. Case C: Sensitivity analysis (with escalation)

Diagram VII. 2-2. International Energy Price for EIRR

1) Natural Gas

· Reference:

BP REVIEW OF WORLD GAS, Aug. 1993 (p.18)

· Method of Calculation:

Average price of OECD Europe,

USA(Wellhead), USA(Import) in 1992

 $2.23US\$/MMBTU = 88.5US\$/KNm^{2}$

2) Electricity

· Reference:

SRI PEP YEARBOOK 1991 (p.21)

Method of Calculation

Average price of USA, WEST GERMANY, JAPAN

(3.7+4.92+7.94) / 3 = 5.42 /kWh = 54.2 \$/mWh

3) Coke

· Reference:

Statistics of Japan Customs Institute, 1993

· Method of Calculation:

Since cokes purchased from other countries are very

little at present and in the future as long as the cokes are produced in SIDEX, those cokes have to be multiplied by economic conversion factor, because those are non-tradeable costs. However, basic data for setting up economic conversion factor is insufficient at the present, 83.8\$/t (lumps of coke) and 55.3\$/t (coke powders), used for calculating FIRRs, are also adopted as the unit prices for coke in the economic evaluation.

4) Metallurgical Coal

· Reference:

COAL MANUAL 1994 (p. 118)

· Method of Calculation:

Average price of coaking coal based upon US\$ per MT

internationally

41.20US\$/t

5) Energetic Coal for PCI

· Reference:

COAL MANUAL 1994 (p. 119)

· Method of Calculation:

Average price of coaking coal based upon US\$ per MT

internationally

32.41US\$/t

1) Capital Cost for Related Plant (Energy Saving only) Without Escalation

(Unic K USS)

Local Sub-Total Total for Energy Saving 28,490 86,265 98 739 Local Sub-Total Foreign Encrys Supply Local Sub-Total Reheating Furnace Plant Foreign Sub-Total 5,432 73,243 8 969'68 3,961 Blast Furnace Plant 800 80 8,860 3 5.432 71,443 3,961 Sub-Total Foreign 850 11,278 2,310 15,265 327 Sintering Plant 2,810 7,860 5,050 Local 7,405 Local Sub-Total Foreign 8 6228 1.47 19.504 427 870 Coke Oven Battery ö 10,909 1.477 8,595 10,499 123 Foreign Eouipment & Materials Sub Total (1) Engineering Fee Civil & Enction ransportation Contingency

194,924

127.238

(Unit: K USS)

2) Capital Cost for related Plant (Energy Saving only) With Escalation

113,424 138,613 Sub-Total Total for Energy Saving 11,583 30 824 हे | | 5 142 94,183 107 789 24 Foreign Sub-Total Energy Supply [SCS] Foreign Local Sub-Total Foreign Local Sub-Total Reheating Furnace Plant 46.5 7,665 80,140 98,083 Blast Furnace Plant 9619 1,954 565 5.944 78,186 88,464 Local Sub-Total Foreign Local Sub-Total Foreign 11,888 8 16,089 897 2,964 Sintening Plant 2,964 5,327 8,291 897 8,5 3,5 7.78 21,396 1.623 \$8 8 2,41 Coke Oven Battery 861 12,914 954 9,436 Foreign .623 468 11.527 Equipment & Materials Sub Total (1) Engineering Fee Civil & Ercaion Transportation Contangency

3) Energy Saving for Related Plant

(Unit: K USS/Year)

	Basic Saving	Escalated Saving
	Amount	Amount
No.5 Coke Oven Battery Plant	7215.20	8364.30
No.7 Siricaing Plant	1524.00	1766.70
No.6 Blast Furnace	12356.40	14324.50
FOTAL FOR ENERGY SAVING	21095.60	24455.50

1) Staring Date of Construction

2) Starting Date of Operation 3) Loan Condition

4) Other conditions

This means the above IRRs are calculated based upon presant value of 2001 year, 1st year,

January 1, 2005

The loan conditions are the same as those used for IRR for Model plants. The other conditions are the same as those used for IRR for Model plants

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Table VII. 2-10-1. Summary of FIRR on Energy Saving of Related Plants (Without Escalation)

		< E0< C	1000	
		そりのそう	CASE B	CASEC
F	1) Cokes Oven Battery	22.0%	21.7%	20.5%
γ	2) Sintering	0.6%	0.3%	26:0-
ଚି	3) Blast Furnace	6.5%	6.2%	4.6%
(9	6) Total (Energy)	8.9%	8,5%	7.1%

Table VII. 2-10-2. Summary of FIRR on Energy Saving of Related Plants (With Escalation)

		CASEA	CASEB	CASEC
1	1) Cokes Oven Battery	23.4%	23.2%	21.9%
5	2) Sintering	2.0%	1.7%	4.0%
က်	3) Blast Furnace	7.4%	7.1%	5.5%
(9	6) Total (Energy)	10.0%	9.7%	8.1%

Table VII. 5-1 Balance of Saved Foreign currencies

).	(Unit: K USS)
	1999	2000	2001	2002	2003	2004	2005	2006	2007	2008	2009	2010	2011	2012	2013	
Saving Amounts without escalation	44,315	59,087	59,087	59,087	59,087	59,087	59 087	59,087	59,087	280'65	59,087	59,087	59.087	59,087	59.087	871,533
Saving Amounts in Foreign Currency	37,681	50,242	50,242	50,242	50,242	50,242	50,242	50,242	50,242	50,242	50,242	50,242	50,242	50,242	50,242	741,064
Consumables from outside Romania	174	232	232	232	232	232	83	232	232	232	232	82	232	232	232	3,422
Sub Total	37,507	50.010	50,010	50,010	50,010	50,010	50,010	50,010	50,010	50,010	50,010	50.010	50,010	50.010	50,010	737,642
Case A		•		***********	***********	·•••••••••••••••••••••••••••••••••••••		,								
Repayment on Long-term Loan				8,041	8,041	8,041	8,041	8,041	8,041	8,041	8,041	8,041	8,041	8,04	56,291	144,742
Interest on Long-term Loan				4,342	4,101	3,860	3,619	3,377	3,136	2,895	2,654	2.412	2,171	1,930	1,689	36,186
Annual Foreign Currency Saving	37,507	37,507 50,010	50,010	37,627	37,868	38,109	38,350	38.592	38.833	39,074	39,315	39.557	39.798	40.039	-7.970	556.714
Case 8			-,,,6,		-**,******					.,,						
Repayment on Long-term Loan		15,005	15,005	15,005	15,005	15,005	15,005	15,005	15,005	15,005	15,009	•••••••				150.054
interest on Long-term Loan		7,503	6,752	6,002	5,252	4,502	3,751	3,001	2,251	1,501	8					41,268
Annual Foreign Currency Saving	37,507	27,502	27,502 28,253	29,003	29,753	30,503	31,254	32,004	32,754	33,504	34.248	50,010	50,010	50,010	50,010	546,320
) ese					·••·											
Repayment on Long-term Loan	22,353	22,353	22,353	22,353	22,353	22,353	22,353	22,350				••••••				178,821
Interest on Long-term Loan	26.823	23.470	20,117	16.764	13,411	10,058	6,705	3,354			••••		•••••••	•		120,702
Annual Foreign Currency Saving	-11,669	4,187	- 1	7,540 10,893	14,246	17,599	20.952	24,306	50,010	50,010 50,010	50,010	50,010	50,010	50,010	50,010	438,119
:																

(Remark)
Annual Foreign Currency to be saved is calculated as follows:

Sub-Total(Saving Amts in F.C.- Consumables)

♣ Repayment

♣ Interest.

Annual Foreign Currency to be saved

VIII. CONCLUSION

The Study for energy saving and environmental pollution control for SIDEX were conducted by a team of Japan International Cooperation Agency (JICA) since November 1993. The Study was in compliance with the Agreement made between the Government of Romania and Government of Japan.

Under the initiative of the Government of Romania, Iron and Steel Industries of Romania have launched a program for Restructuring and Modernization to be completed in the year 2002. JICA's study has therefore paid due regard to this restructuring and modernization program, and the study is complimentary to the goals of SIDEX. Mainly the studies were conducted on selected representative model plants for each group of production units that were in the scope of JICA's study. Besides, we roughly studied the other related plants to which the same measures as that of the model plants are applied.

The study highlights the following:

- Measures for efficient and effective way in energy saving and environmental pollution control
- Cost effective analysis of investment in terms of Financial Internal Rate of Return and Economic Rate of Return
- Maximum utilization of Romanian manufacturers to achieve minimum cost for implementation

The results of the cost effective analysis show that when the proposed measures are implemented, the energy saving is quite considerable from standpoint of cost effectiveness. The measures of environmental pollution control will meet the legal regulations which are being strictly implemented by the Government of Romania.

The Study recommends early implementation for the economical benefit of SIDEX in particular and for the overall beneficial effects in general that the cities and surroundings will gain from the anti-pollution measures.

In a nutshell, the following are the results of the major items of the study:

1. Energy saving

From the view point of effective utilization and saving of energy, and suppression of the pollutants, the Study proposes a positive integration of the production plants (to reduce the variety of the production units to a minimum operating numbers) with all that to achieve the production target of the year 2002 as projected in the Restructuring Program.

The energy consumption of the production plants which were in the scope of study, account for more than 70% of the total consumption of the Steel Complex. By implementing the measures proposed in the Report, SIDEX can save approximately 1.5 G cal. of energy for every ton of crude steel produced which works out to an annual savings of 700 million Nm3 of natural gas, 170 Gwh of electric power and 700,000 tons of coke.

The dependency on high priced purchased natural gas for fuel could decrease to 12% from the present dependency of 42% which has the added benefit of not having to depend too much on the seasonally unstable supply of natural gas and the precarious operation at levels of insufficient energy can be alleviated.

The Financial Internal Rate of Return (FIRR) are calculated for three cases of financial sources.

Case-A Overseas Development Aids from Government of Japan (ODA).

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Case-B Soft Loan

Case-C Commercial bank Loan

The FIRR is in the range of 17% to 21% for any of the above financial sources. Besides, the investment in the energy saving measures will certainly improve the financial performance of SIDEX.

2. Environmental Pollution Control

To meet the legal regulations which shall be in place by year 2002, it is essential to implement the environmental protection measures as detailed in chapter III of the Report.

These measures will greatly reduce the pollution to the town of Galati and river Danube. Particularly, the emission rate of SO2 and NO2 in the exhaust gas could be reduced by 66% and 20% respectively, and as a result the pollution by the Steel Complex in the center of the town will be less than 2 ppb and 3 to 5 ppb respectively.

The visible soot and dust particles from the coke oven batteries and the sintering plants which are the two major sources of emission, will be reduced to the same level as other OECD countries. This will be a significant improvement and benefit the town area.

The cyanides in the waste water discharged from SIDEX will reduce by 93%, Organic contaminants of Phenol by 99% and Ammonia by 83%. The combined effect on the water quality in the river Danube will be significant.

Besides the above advantageous effects on the surrounding, the working atmosphere in the plant itself will improve to make the work place conducive for efficient working by improved morale of the workers. This means that international standards on environmental control would have been met and this will generate an unquantifiable knock-on effect in the technological, educational and psychological fields throughout Romania.

It is recommended that the implementation of the environmental pollution control measures be appraised from three points of views, legal Regulations, and financial & technical viability.

Romanian Authorities have indicated their determination to apply stringent standards for environmental protection as that of other OECD countries. This policy will make it obligatory for SIDEX and other industries to follow the Law.

- The present market economy suggests that funds will be not sufficient. Therefore, the estimation in the study has taken into consideration the least cost necessary to meet the regulations for the environmental protection.
- With regards to the technical viability, technologies which have proven performances and which are most suitable for SIDEX are proposed taking into consideration the local conditions.

In conclusion, in order to ensure an early return on investment on advanced Energy Saving and Environmental Pollution control measures and to manifest their effectiveness on a long term basis, enhancement of Operation and Maintenance Skills are essential. For this purpose, it will be effective and beneficial to introduce operation and/or maintenance technologies from other advanced countries along with the introduction of the Equipment.

The Study suggests that through the implementation of the measures for energy saving and environmental pollution control, ripple effects such as technical transfer to the domestic companies in Romania, will be generated. This in turn will propagate that influence upon other steel works and industries in Romania.

IX. RECOMMENDATION

Foreword

Sidex is the largest industrial facility in Romania and this JICA Study tries to bear this in mind in developing an effective strategy to a shape the cleaner, more efficient and therefore profitable future. Sidex should become a model works with modern standards applied to the efficient use of energy and the control of environmental pollution. The recommendations, which are all considered essential and therefore they are not list in any priority, are divided into three categories:-

Recommendations 1 to 3 General matters

Recommendations 4 to 5 Energy efficiency

Recommendations 6 to 11 Pollution control

General matters

Recommendation 1

Sidex and the Romanian Government should study energy saving and environmental pollution control for the facilities other than the facilities covered in this report as they are in a similar condition.

Recommendation 2

Soft-loans will be needed for the foreign currency to import equipment and local funding for construction costs to actually take the measures recommended by this Study.

The Romanian Government should extend guarantees and other financial support so that Sidex can have access to the necessary amount of the foreign currency and preferably take over the costs temporarily or re-loan the necessary amount of money with manageable rates of interest.

Recommendation 3

The use of appropriate technology developed in advanced countries should be positively introduced to solve the actual environmental problems and to achieve effective energy saving.

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Energy Efficiency

Recommendation 4

Promotion of comprehensive measures for energy saving in steelworks

Energy saving in steelworks starts first by focusing on reduction of energy loss, second on the enhancement of efficiency in each manufacturing process and third on recovery of energy.

Comprehensive energy measures linked with the following production improvements should be effectively developed:

- i Energy saving by improvement of productivity and quality, yield,
- ii Energy saving by successive or omission of processes,
- iii Reduction of energy cost by the tic-up of production control and energy control,
- iv Reinforcement of energy and thermal control in each plant.

Recommendation 5

Promotion of energy saving by the Government

In addition to the energy saving effort of Sidex it is essential that the Government or the local self-governing body promotes parallel policies encouraging energy efficiency in the same way that the administrative organizations of most modern countries including Japan do. The following suggestions may be relevant to Romania:-

- i Encouraging a supply-demand structure based on estimated energy supply-demand in the long and medium term for the whole country by drafting regulations in energy saving to each industry.
- ii Setting macro targets for the saving of energy and giving guidance in energy saving to each industry.
- iii Establishing an organization for energy saving education making it possible for people to acquire special skills in practical thermal control technology.
- iv Publication of actual case studies in energy saving.
- To penetrate the consciousness and skill of energy saving into every company encourage a government controlled qualification system to certify energy control specialists and legally control the employment of specialists in each industry.
- vi Establish regulations on energy and technical standards, and require by regulation all large consumers to arrange an energy control systems.
- vii Standardize efficient energy control by means of the publication of guidelines.
- viii Motivate employees by adopting a prize system for energy saving.
- Wherever possible structure the tax system so it becomes a supporting system for promoting energy saving.
- x Assist companies financially by adopting low interest rate loans for investment in energy saving.

Pollution Control

Recommendation 6

Promotion of comprehensive measures for environmental pollution control in steelworks

This report describes the details of investigation on measures for environmental pollution control in the coke plant, sintering plant and blast furnace, which are the main processes which pollute the environment. After taking the recommended measures in those plants, the steel making plant and material yard should be the next areas to be improved with regard to dust emission and the treatment of sewage.

Recommendation 7

The followings items should be implemented as soon as possible as set out in the report.

- i Expansion of environmental monitoring equipment and system,
- ii Amplification of re-cycle system by effective utilization of waste.

Recommendation 8

Promotion of pollution control by the Government

In order to control discharge of contaminants, in addition to the controlling regulations, it is important that the Government assists companies by adopting an advantageous loan system and a tax system encouraging the prevention of pollution at the time a new plant is built.

The Romania Government should study economic stimulating policies, a surcharge policy, etc. referring to the Japanese systems, and is expected to reinforce the domestic environmental policy.

In Japan there is a loan system with low interest rates (monetary step), a system of short depreciation periods, and a tax exemption system for fixed asset (tax step) and other incentives. The following are concrete examples:-

(Example of loaning system with low interest)

Loan organizati on	Subject of loan	Ratio of loan	Intere st	Term of redemption
	[Anti-pollution facilities] Conversion to non-pollution process, Facilities with protective measures for ozone layer	within 40 %	4.4 %	10 years 1 year deferment
Japan Developme nt Bank	[Anti-pollution facilities] Treatment equipment of soots, dusts, sewage, industrial waste, De-SOx device, De-NOx device, Noise/smell-proof facilities, etc.	within 40 % (within 30 % for smellproof facilities)		10 years 1 year deferment
	[Effective utilization of resources] Resource re-cycle facilities, Effective utilization facilities of water resource	within 40 %	4.4 %	10 years 1 year deferment
	[Environmental control of factory, plant, etc.]	within 30 %	4.4 %	

(Example of life of assets for depreciation)

Facilities	Туре	Details	Life
Soots treatment	Structure	Tank, tower, waterway, and reservoir, built by reinforcement concrete or brick	30 years 20 years
Sewage treatment	Machinery and device		7 years

Recommendation 9

The re-cycling of slag requires total teamwork and the combined effort of the "supplier" and "user". Political assistance is also important.

Sidex as a supplier needs to:-

- i expand the slag water granulation equipment,
- ii install a crushing and pulverizing equipment, and
- iii stabilize the quality of product.

Users mainly the cement, civil engineering and construction industries should be encouraged to study extending the use of re-cycled products. In order to support them the Government and other administrative organizations should take supporting measures, such as approval of the quality standard, designation of materials for public construction.

Recommendation 10

A special organization should be established for promoting environmental protection and pollution control. It should have as its policy the enlightenment and motivation of individuals, companies, research organizations and universities by encouraging developed technology, improvement case studies, and by introducing the ISO environmental control system in relation to environmental control.

Recommendation 11

A government controlled qualification system encouraging and educating pollution engineers and controllers and a system that stations the qualified engineers and controllers in a company should be legally framed to penetrate the sense and technology about environmental pollution control in every industry.

Appendix-1 NAME OF MAIN COUNTERPARTS

1. Council for Coodination Strategy and Economic Reform

CECILIA VLASCEANU Counselor

2. Ministry of Industry

DANION POPESCU

Secretary of State, Financial & Strategy

IANC PETRU

General Director, Strategy of Metallurgical

Industry...

CAPOTA ION

Deputy General Director

SAVA NICOLAE

Expert of Energy

CHISER ZAMFIR

Special Adviser

3. Ministry of Environment

AUREL CONSTANTIN LLIE

Minister

LUCIA CEUCA

Director International and Public Relations

SPERANTA IANCULESCU

Director

DUMITRU MIHU

Director

GEORGE MIHAI PRETORIAN

Head of Regulatory Activity

SERENA ADLER

Expert

TANIA PAPADOPOL

Expert

4. Ministry of Finance Romania

MIHAI BOGZA

General Director for International Relation

5. The Integrated Iron and Steel Complex "SIDEX" S.A. GALATI

FLORENTIN SANDU

General Manager

SEBASTIAN STAVAR

Assistant General Manager

DUMITRU NICOLAE

Assistant General Manager

ALEXANDRU FLOREA

Technical Manager

ALEXANDRU DOBRE

Maintenance Manager

CONSTANTIN ZAHARIA

Manager Planning & Economical Operation

RACHITAN CONSTANTIN

Chief Engineer Coke plant

BANU STEFAN

Chief Engineer Blast furnace

BELCIUG SPILIDON

Chief Engineer Blast furnace

DAN IONEL

Chief Engineer Rolling mill

CHICULITA MIHAI

Chief of Modernization Dept.

GROSU ION

Chief of Environment office

OSTACHE STAN

Chief of Energy office

CULESCA CONSTANTIN

Investment

CHIMET MARIA

Environment

MARIAN BAKLAN

DIPL Engineer

6. Engineering center

6.1. IPROMET S.A

PRISECARU ION

Director General

PANAIT TEOKEANU

Technical Director

BULUC DUMITRU

Head of Designing shop, Environmental

Protection

IORDACHE DUMITRU

Head of Designing shop, Water treatment

AMANCEI LUCIAN

Head of branch technology

6.2 IPROLAM S.A

NEDELESCU PETRE

Director General

STOENESCU ALEXANDRU

Director Technical

MAUTHNER ANDREI

Head of Designing Shop

CAMPENU DAN

Head of Designing Shop And Anti-

6.3 ICEM S.A

CONSTANTIN RADU GERU

Director General

DOBRESCU MIRCEA

Vice President steel making

DEBIASIRODICA

Head of Laboratory "Environment Protection"

7. Romania National Bank

VASILE EMIL

Director Adjunct

8. Environmental Control Agency of Galati

TLIE TRUTA

Manager

GEORGE TUDOSESCU

General Inspector

CARMEN ANDREI

Inspector

ION DRUGAN

Inspector

9. ECOSIDER

MIHAI TEACA

Chief Ecological Laboratory

10. RENEL (Romanian Electric Authority)

10.1. Head office

GABRIEL POPESCU

Director Strategy & Economic

Development Division

ION TUDOR IONESCU

Director Operation Division

CATALIN - MARIN DRAGOSTIU

Deputy Director Finance &

Accounting Division

10.2. Galati blanch

GROSARIU

Director Technical General Manager

Appendix-2 MEMBERS LIST OF JICA TEAM

gradinisti Pillada antarii ka		1st. Site survey	2nd. Site survey	3rd. Site survey
Name	In charge	From Nov.22.93	From Hy.06.94	From Nov.26.94
		To. Dec. 18.94	To Aug. 10.94"	To Dec.13.94"
Hiroshi Tsutsumi	Team Leader	О	0	0
Takuzou Shimizu		0	0	0
Mitsuaki Takeuch		0	0	0
Hideo Tatemichi	Leader for the study on Energy saving /Reheating furnaces	0	0	0
Masato Kato	Coke plants	0	0	0
Kazunori Hayashi	Coke chemical plants	0	0	0
Kunihiro Imada	Sintering plants	0	0	0
Reiji Ono	Blast furnaces and Hot stoves	0	0	0
Shigeki Inoue	Environmental analysis	0		
Hiroyuki Mitake	Maintenance	0	0	0
Yuji Murata	Planning of Electrical systems		0	
Yoshikazu Aono	Planning of Instrumentation systems	0	0	
Yoji Morishita	Financial/ economical analysis		0	0
Tamotsu Inoue	Coordinator	0	0	0

