Waste water discharged from the coal and coke yards is likely to contain fine particulate of coal, and acidic substance which give acidity. Thus, a neutralization plant adding alkaline to waste water and a settlement facility to remove fine particulate are required. Fig. 7-5 shows a conceptual diagram of the process.

(4) Environmental impacts of water pollutants and evaluation of control measures

The effluent from the coke plant will be discharged through two routes, the combined process effluent from the north side of the plant and the yard water from the south side, both off the wharf accommodating the coal carrier. Discharge pipes are 1m in diameter, from which water is directly discharged to the lake. As shown in table 10–11, BOD in effluent water shall be about 10 ppm.

The effluent is carried by tide and moves southward at high tide and northward at low tide, creating a risk of polluting lake water.

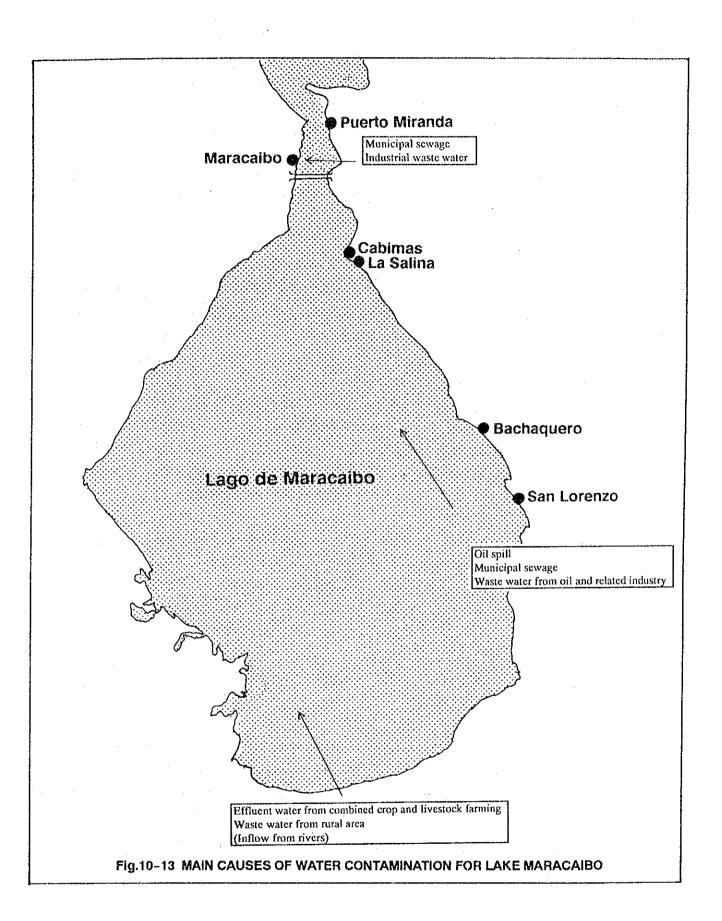
So far, CORPOZULIA engineers have explained that direct discharge of effluent from the plant would not present any problem so long as emission standards are complied with. If this is true, effluent from the coke plant will be able to meet emission standards applied to Lake Maracaibo and surrounding waters. It will not bring significant environmental impacts on the lake and its surrounding areas.

Although the lake is connected to the sea through the Gulf of Venezuela, it is essentially a closed water area and does not have the ability to dilute pollutants. Thus, once polluted, it is difficult to restore the lake to its original state.

Local newspapers often report about the lake's pollution, and some people claim that a fish catch on the lake decreases due to water contamination.

On the other hand, CORPOZULIA's engineers explain that major causes for the pollution are crude oil spilled from oil wells, loading facilities, and tankers, as well as untreated sewage from the city and its surrounding areas. So, it is assumed that water contamination of Lake Maracaibo is three main causes as shown in figure 10-13.

Also, the fish catch has decreased due to excessive fishing, and the fish size caught in the lake becomes smaller. Recently, various fishing restrictions have been introduced, and the use of fishing nets with larger meshes is expected to work as a deterrent for reckless fishing.



It is the fact that there have been no emission standards in Venezuela, including Lake Maracaibo, and waste water from households and industrial effluent have been discharged without treatment to the lake. Starting in April 1994, however, effluents from petroleum refining and other industrial facilities are restricted by new regulations. Also, a public sewage treatment plant for the city is under construction. As a result, the discharge of water pollutants which deteriorate the lake's water quality will be significantly reduced in the near future.

The study team attempted to obtain background data which indicate how the lake water is contaminated by which pollutant. Furnished data by CORPOZULIA, as shown in Table 10-5, and ICALM's report which published Jan, 1994 do not contain COD, SS and other items associated with water pollution by organic matters.

ICLAM's report above mentioned is summarized as follows.

Surface water of Lake Maracaibo contains a large amount of dissolved oxygen and shows a low BOD level. BOD, which is 5.2ppm at the mouth of the lake, is shown max. 3.7ppm in the lake. Other measuring points are less than 3.0ppm. On the other hand, dissolved oxygen ranges between 6ppm and 7ppm on average. Thus, lake water seems to be clean on the surface.

However, dissolved oxygen content in the bottom of the lake decreased to one half the level near the surface, while BOD exceeds 10ppm and reaches 20 - 30ppm at many measuring points. Where surface water is relatively clean, the near anaerobic condition prevails deep into the bottom. This is because organic matters carried to the bottom are hard to be decomposed.

The above analysis suggests that Lake Maracaibo may be highly susceptible to contamination by organic matters.

Therefore, preserving the lake environment is an important issue to be carefully dealt with, and more data need to be collected to determine the quality of the lake water system, followed by detailed analysis and evaluation. Table 10-12 lists is one of the proposed study and research to be conducted for the purpose.

Table 10-12 PROPOSED STUDY AND RESEARCH RELATED TO WATER QUALITY OF LAKE MARACAIBO AND ENVIRONMENTAL IMPROVEMENT

- (1) Understanding of tide current conditions in Lake Maracaibo (literature survey, hearing, and field survey)
- (2) Field investigation on water contamination sources (manufacturing, agriculture and livestock farming, oil drilling and transportation, urban sewerage, etc.)
- (3) Monitoring of lake water contamination(comparison of simulation results and actual conditions)
- (4) Effects of water contamination on industries and local residents (fishery, water transportation, tourism, recreation, etc.)
- (5) Analysis of ongoing measures to control water contamination, and development and evaluation of possible measures (effect of present water quality standards applied to the sake, and proposing and evaluation of other measures)
- (6) Forecasting and evaluation of future water quality
 (based on the above results, desirable water quality in the future is discussed and established)

10.4 Noise and Vibration

(1) Current state

At present, a major industrial activity in the La Cañada industrial park is the loading of Tachira and Colombian coals to ships through the wharf.

Coal is brought into the site by trucks and is unloaded at a specific location, where forklifts equipped with large buckets pile up the coal.

When a barge comes alongside the berth, the fork-lifts carry the piled coal to a makeshift belt conveyor through which the coal is loaded onto the barge.

During these operations, noise and vibration are limited to those produced by trucks, forklifts, and belt conveyor, which are not very high.

(2) Target levels of noise and vibration control

The plant is designed to comply with existing noise standards which are set forth in Decree No.2217 dated April 23, 1992. Table 10–13 summarizes noise standards applied to the battery limit.

	Continuou	s Noise	Intermit	lent Noise
	Daytime 6:30 a.m. – 9:30 p.m.	Nighttime 9:31 p.m. – 6:29 a.m.	Daytime 6:30 a.m. – 9:30 p.m.	Nighttime 9:31 p.m. – 6:29 a.m.
Zone 1	55 dBA	45 dBA	60 dBA	50 dBA
Zone 2	60	50	65	55
Zone 3	65	55	70	60
Zone 4	70	60	75	65
Zone 5	75	65	80	70

Table 10-13 NOISE STANDARDS

Note that Zone 1 requires very quiet environment such as detached houses and hospitals. Zone 2 also covers residential areas with a lower level of noise control, mainly consisting of attached houses. Zone 3 is applied to mixed-use areas including houses, commercial facilities, and schools. Zone 4 is the commercial and industrial district where no school and hospital is allowed. Zone 5 represents marginal zones around airports and highways. The industrial estate belongs to Zone 4.

Since there is no standard to regulate vibration in Venezuela, target levels of vibration control at the battery limit are tentatively set on the basis of applicable standards in Japan, as follows:

	Daytime	Nighttime
Zone 1	65dB	60dB
Zone 2	70dB	65dB

Note that Zone 1 covers residential areas, and Zone 2 commercial/industrial or industrial areas.

(3) Estimation of noise and vibration sources at the plant and evaluation of proposed control measures

Machinery and equipment which produce noise and vibration at the coke making plant are machine tools (repair shop), compressors, blowers, coal crushers, coke graders and screening equipment. Also, combustion in boilers and other heating equipment produces some noise. In addition, mobile equipment around the coke oven makes large buzzer sounds.

Noise and vibration sources during the plant construction period are bulldozers, pile driving equipment, concrete breakers, and trucks and fork-lifts.

Noise Levels of major noise sources summarized as follows:

Туре	Distance from source	Noise level
Trucks and construction equipment	30m	50 – 78 dBA
Crushers and screening equipment	1m	80 –100 dBA
Compressors	1m	70 – 88 dBA
Blowers	1m	75 - 80 dBA
Burners and boilers	1m	70 - 88 dBA
Machine tools	1m	70 - 90 dBA

Table 10-15 MAJOR NOISE SOURCES AND NOISE LEVELS

A major vibration source will be pile driving operation during the plant construction period.

Noise control measures are described as follows. First of all, crushers, screening equipment, and machine tools which produce large noise will be installed in buildings. Other noise-generating machinery and equipment will be provided with sound and vibration insulation measures for their installation bases, in addition to accommodation inside the building. Note that many sound insulation measures also work for vibration. Also, the sound insulation effect is affected by presence of openings.

As for plant layout, facilities not generating noise, such as parking facilities and office buildings, are arranged in sections facing public roads. 50m wide green belts are provided around the battery limit. As a result, major noise sources will be 60m - 100m away from the battery limit. It is said that noise abates by 3dBA at 10m from a point source, the layout is considered as effective measures to insulate noise and vibration from the surrounding area.

The above control measures are expected to satisfy noise standards at the battery limit. Also, piling work during the construction period will produce vibration and should be conducted in selected working hours.

Basically, there is no residence nor factory around the site, so that a risk of noise pollution to the surrounding area is minimal, and proposed noise control measures will suffice even after the surrounding are is developed.

10.5 Solid Waste

(1) Possible sources

Solid wastes produced from operation of the coke plant include bottoms in distillation towers, residual matters in decanters and tanks, surplus sludges in the ASM process, and sludge sediments in waste water from the coal and coke yards.

Also, around 700 workers at the plant will produce a variety of household wastes as well as raw sewage, which are estimated to amount to 200 kg - 300 kg per day. (Note that a person living in Japan reportedly produces 1kg of solid waste per day)

(2) Target levels of solid waste control

Various measures will be introduced to minimize the amount of solid waste produced from the plant.

(3) Estimation of solid waste sources and evaluation of control measures

Solid wastes produced from plant operation include bottoms in distillation towers, residues in decanters and tanks, and surplus sludges in the ASM process, and sludge sediments in waste water discharged from the coal and coke yards. The project plan envisages that these solid wastes will be all returned to the coke oven or related facilities for recycling, thus none of them will be disposed to the environment as they are.

Residues in decanters and tanks, and surplus sludges in the ASM process, and sludge sediments in waste water from the coal and coke yards mainly contain carbonaceous and hydrocarbons. They can be carbonized in the coke oven to produce coke, although it contains relatively large amounts of impurities. Thus, these solid wastes will be charged with coal to the coke oven.

Bottoms in distillation towers are sent to the decanter to remove water. Also, sludge sediments in waste water from the coal and coke yards can be used as a raw material for briquette. Thus, the proposed plant will adopt self-sufficient solid waste disposal measures as far as possible to minimize environmental impacts.

On the other hand, household wastes and waste paper produced from cafeterias and offices need to be disposed carefully. One method is to burn them in a small incinerator within the

plant. It requires full-time workers but offers an advantage in keeping confidentiality. Another method is to hire a reliable outside contractor. This way, solid wastes can be economically disposed by incineration or reclamation, according to local conditions. It is important to dispose all the solid wastes properly so as not to create undue environmental impacts.

Raw sewage will be treated in a septic tank installed at each source. The treated water is expected to have minimal environmental impacts.

Thus, proposed disposal methods will minimize the amount of solid waste discharged to the environment.

10.6 Malorder

(1) Current state

Since Venezuela has not regulation to control Malorder, control measures are tentatively established on the basis of Japanese standards, which cover the following 12 substances. Among them, ammonia, hydrogen sulfide, and styrene are produced in the coke oven.

TABLE 10-16 SUBSTANCES SUBJECT TO JAPANESE REGULATION DUE TO MALORDER

Ammonia, methyl mercaptan, hydrogen sulfide, methyl sulfide, methyl disulfide, tri-methyl amine, acetic aldehyde, styrene, propione acid, normal butanoic acid, normal valeric acid, isovaleric acid

In addition, the light oil fraction – a major by–product produced in large quantities – contains benzene, toluene, and tar, which produce characteristic smells.

(2) Target levels of malorder control

Target control levels for 4 substances – ammonia, methyl mercaptan, hydrogen sulfide, and styrene – in terms of concentration are tentatively established on the basis of applicable Japanese standards as follows.

	Upper Limit for Concentration
Ammonia	1 - 5
Methyl mercaptan	0.002 - 0.01
Hydrogen sulfide	0.02 - 0.2
Styrene	0.4 - 2

TABLE 10-17 TARGET CONTROL LEVELS FOR SMELL-PRODUCING SUBSTANCES

In addition, benzene produces strong odor and is a carcinogen. Its concentration should be controlled below 1ppm (a level no smell is detected) within the plant. Also, the concentration at the battery limit should be controlled at a level similar to that of styrene.

Thus, the plant is required to control concentrations of 4 odor-producing substances, namely ammonia, hydrogen sulfide, benzene, and styrene.

(3) Estimation of smell sources and evaluation of control measures

At the coke oven, while each carbonization chamber is operated in batch, other equipment is operated as the continuous process. Also, the plant is designed and/or operated to prevent intermediate products from escaping outside from enclosed equipment, except for the pushing operation to take out red-hot coke. As a result, there is little risk of releasing the smell-producing substances to the air.

Ammonia in ammonia liquor is gasified with other dissolved gas constituents at the ammonia distillation plant, is separated from dissolved salts and returned to COG. Hydrogen sulfide is absorbed by an alkali solution and is converted to sulfur through the liquid-phase air oxidation process, finally to sulfuric acid. Sulfuric acid and ammonia are used to produce ammonium sulfate. Thus, these smell-producing substances are deodorized and taken out of the process.

There are a limited number of locations where smell-producing substances may find way to the outside, such as axles of motors, and sludge removal ports of the decanter. These locations will be provided with cover to protect workers from offensive smell. As a result, no odor will not leak to the outside. Thus, all the smell-producing substances will be contained within the battery limit and will be maintained at the concentration level which does not have an adverse effect on the surrounding environment.

10.7 Protection of Natural Environment (including wild animals and plants, and landscapes)

(1) Current state

The La Cañada industrial park is covered with the sparse forest made up of dry weatherresistive small bushes, grasslands, dotted with cactuses, which are typically found in the savanna under the dry and tropical climate zone.

Compared to other areas around Maracaibo, the area has less trees which are relatively small, giving an impression that the land has once been cleared for development, and the nature is coming back as it has been left intact more than a decade.

Nearby buildings are a thermal power plant, petroleum refineries, and tank yards.

The industrial park is virtually unused and gives a look of wasteland. There are not data on wild animals and plants residing in the area, which is not habitable for large carnivorous animals.

(2) Estimation of impacts on natural environment and evaluation of preventive measures

The La Cañada site has land area of 6,800ha. It was originally selected and prepared as the site for an integrated steelmaking plant using blast furnace. The vast land was acquired to build the plant having annual production capacity of 5 million tons, a 2.5 million plant in the first phase and another 2.5 million plant in the second phase, including a coke plant.

The project will use 830,000 m², accounting for 1.22% of the entire site. Even if construction of access roads is added, the percentage will not exceed 1.5%. Thus, most of the site will be preserved as it is.

50m wide green belts will be provided along the battery limit by planting local trees, if desired. Thus, the project is not like to create significant impacts on natural environment including wild animals and plants in the surrounding area.

As for landscape, a large plant including a 120m high smokestack and a coke oven which is 200m long and 50m high (coal tower) will be constructed in the vacant site.

It can be viewed from the city of Maracaibo, General Urdaneta bridge, and/or Santa Lita on the opposite side of the lake, as well as airplanes landing and taking off the La Chinita Airport.

Thus, the plant can become a new landmark in the area, although its aesthetic value has to be determined in the future.

10.8 Impacts on Traffic Conditions

(1) Current state

Within the La Cañada industrial park, a main road (one-lane on each side) runs in a north-south direction, 1.5km west of the lake shore. The road is paved and connected at the northern end of the site to National Highway Route 252 which connects Maracaibo and Rosario.

From the main road to the plant site, there is an access road which is not in good condition.

Highway 252 is two lanes on each side between Maracaibo and Rosario, but one lane in a Rosario – La Fria section which will be used to transport raw coal from mines to the coke plant.

The La Cañada industrial park contains the port of Puerto Siderurgico along Lake Maracaibo, which has a 243m long wharf with water depth of 3m, and off-shore navigation channels are dredged to 12m. The port does not have any handling facility and equipment. At present, Tachira and Colombian coals are shipped through the wharf to a 2,000-ton barge. The coal carried on the barge is transshipped to a Panamax-class (60,000 tons) ship anchoring off the shore.

(2) Estimation of impacts on traffic conditions and consideration of improvement measures

The coke plant will affect local traffic conditions on road and sea, accompanied by environmental impacts.

First of all, an access road connecting the main road in the industrial park and the plant site needs to be built or at least paved.

Traffic conditions between La Fria and Maracaibo, and future demand forecast, according to CORPOZULIA, are discussed in Chapter 6(6.8.1).

As discussed before, if Tachira and Colombian coals are produced at full capacity of 520,000 tons annually and transported by 50-ton trucks, traffic volume will increase at a rate of 33 vehicles per day, which is equivalent to a 3.5% increase in the degree of congestion. If all the imported coal is converted to domestic coal or Colombian coal, traffic volume will increase by 94 vehicles per day (9.9% in degree of congestion).

Theoretically, the coal can be transported via Highway 252 until year 2020. If the degree of congestion required to maintain smooth traffic is 80% or below, and if the coke plant starts operation in 2010, trucks carrying coal will increase by 33 vehicles per day, and the degree of congestion will soon exceed 80%. Note that the above figures do not include passenger cars used for commuting. Thus, traffic congestion will occur on the highway and may bring adverse environmental impacts if no improvement measures are taken.

There are several improvement measures to reduce traffic volume due to the start of plant operation. One method is to widen the highway between Rosario and La Fria for increase traffic capacity. The second method is to construct a railroad between La Fria and Maracaibo. The third method is coal transportation by barge from a port planned to construct near La Concha. Each of the cases involves new construction which is planned and implemented as early as possible.

In any case, traffic improvement measures should be considered as part of infrastructure development which would require the higher cost than the proposed project.

Chapter 11 Conclusion and Recommendation

Chapter 11 Conclusions and Recommendations

Conclusions

The present study is designed to evaluate feasibility of the proposed investment project to produce blast furnace coke by using coking coal available in the state of Tachira. The project is proposed in line with the national policy of Venezuela to decrease the dependency of the Venezuelan economy on oil, while serving the interests of fostering regional development.

The present study has examined the proposed project for two cases; one based on availability of coal and other relevant conditions confirmed at present, and the other based on conditions expected to be satisfied in the future. In addition, the case to use Guasarc coal produced in the state of Zulia has been evaluated, although not included in the original study plan. Basic assumptions and considerations common to all these cases are as follows:

1) Venezuela does not have a blast furnace to produce pig iron, nor have any plan to build one in the foreseeable future. On the other hand, demand for blast furnace coke in the U.S., which is expected to decline in absolute terms, will grow relative to supply capacity that will decrease at a faster rate since many coke ovens will shut down due to increasingly strict environmental standards. This creates a good export opportunity for the proposed coking plant, provided that it has international competitiveness. Another market opportunity is identified in Brazil where coke demand is expected to arise in order to replace charcoal for pig iron production. Thus, coke produced by the project is assumed to be entirely exported.

Also, it is assumed that most of by-products will be exported. In this connection, the price of coke oven gas is evaluated to equivalent of natural gas.

- 2) The coke oven will be of chamber type that is widely used worldwide from the viewpoint of ensuring the level of coke quality suitable for the U.S. market. The production capacity is set at 1 million tons annually with consideration of the economic scale.
- 3) The plant site has been selected in Maracaibo among three candidate areas including Santo Domingo and Puerto Ordaz, on the basis of comparison of locational conditions including transportation costs for coal and coke, sales opportunity for coke oven gas, and government regulations.
- 4) The plant design incorporates environmental considerations based on strict standards applied to Lake Maracaibo, as well as those in Japan and Clean Air Act in the U.S. Environmental assessment related to air pollution was conducted and revealed that the plant would produce a minimum environmental load.

Case 1 Evaluation of feasibility based on verified resource conditions

In Tachira, there are 5 coal deposits, namely FNO, SAN, LOB, HAT, and LAS. Among them, coal from two deposits are considered to be suitable at present, FNO containing medium volatile coal and LAS high volatile coal. Coal reserves in FNO are smaller than expected. Boyaca coal in Colombia is low volatile coking coal, but its production is limited. As a result, U.S. coal must be blended in quite proportion.

Transportation of the Tachira and Colombian coals to Maracaibo is assumed to be done by truck that shows the highest economic advantage.

Finally, the price of coke in the U.S. is currently at US\$100 or less. However, supply is expected to become tight in the near future for the reason stated above, so that it is assumed to be US\$135 which is the highest level experienced during the previous supply shortage. Based on the above assumptions, the FIRR is -1.37% to make the project unjustifiable.

Case 2 Evaluation of feasibility based on resource conditions expected in future

In Tachira, coal exploration surveys are under way and the development of medium volatile coal seems to be viable. If the prospect becomes reality, coke for the U.S. market can be produced from Tachira coal as well as the low volatile Colombian coal. Thus, the case assumes that the U.S. coal in Case 1 will be entirely replaced with the Tachira and Colombian coals. (Domestic coal 80%, Colombian coal 20%)

As a result, the FIRR has improved to 5.54%. Nevertheless, it is not sufficient to justify the project.

Clearly, the development of coal deposits in Tachira is not a satisfactory condition to justify investment in the coking plant. There are several favorable prospects, however. If a railroad construction project planned between Tachira and Maracaibo is constructed, the coal transportation cost for the Tachira, as well as Colombian coal will decline by around US\$2.

Secondly, the coke price in the U.S. – assumed to be US\$135 in Case 1 – may go up to US\$150 if supply shortage becomes more serious than expected.

If these factors are timely realized, the FIRR may rise to a feasible level.

Case 3 Evaluation of feasibility based on the use of the Guasare coal available in Zulia.

The Guasarc coal is found near Maracaibo. It has large reserves, can be exploited economically by open mining, and has relatively low ash and sulfur contents. From the viewpoint of coke production, however, Guasare coal has a low coking capacity and a very high volatile content. Evaluation on the use of Guasare coal to a maximum extent in response to the request of the state of Zulia is made.

- 1) Experiments have been conducted to find the maximum practicable blending ratio of the Guasare coal to replace U.S. coal in Case 1, which is estimated at 10%.
- 2) If the blending ratio is raised to 15% as proposed by the Venezuelan side, the required quality of coal can be maintained by using a sufficient amount of the HAT coal in place of the LAS coal.
- The maximum blending ratio of Guasare coal, obtained by reducing or replacing the Tachira coal where necessary, is estimated at 23%.

The FIRRs for above three cases are 0.19%, 0.94%, and 2.78% respectively. One reason for the low FIRRs is relatively a small difference in price between coking and non-coking coal. In the third case, the FIRR does not improve significantly because of an increased percentage of U.S. coal to compensate for the high volatile Guasare coal.

Recommendations

The study has examined financial feasibility of the coke oven project using coal available in Tachira. The result shows that the project is not suitable for investment under the currently confirmed resource conditions. There are various reasons for this: the need for exporting all the projects; a large percentage of U.S. coal to secure the required coke quality; and the high construction cost partly due to strict environmental considerations.

However, if coal resources in Tachira are developed as expected, and other conditions are improved simultaneously, the financial prospect for the project will improve, possibly to an acceptable level. Thus, it is desirable to conduct an additional feasibility study when the development of coal resources in Tachira reaches a commercial level.

Although Guasare coal has advantages in availability, quality, and price, it has very low coking capacity and high volatile content, not suitable for coke production at the conventional coke oven. The development of the process to produce blast furnace coke by using non- or light coking coal has been carried out worldwide. The continuous formed process has been developed from such development efforts. In Japan, production tests have been conducted at a 200-ton/day pilot plant, and formed coke produced from the plant has been used in a 4,500m3 blast furnace. Also, the feasibility of commercial production at 3,000 tons daily (equivalent to 1 million tons annually) has been successfully evaluated. The analysis of the technology and its applicability to the project, therefore, will be one promisting area to be examined in more detail.

Appendix-1 FINANCIAL AND ECONOMIC STATEMENTS FOR BASE CASE

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(US\$/T)

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UNIT SALES PRICE (US\$/T)

SALES REVENUE

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SALES REVENUE

(US\$, MILLION) *** COKE PLANT PROJECT IN VENEZUELA *** PRODUCTION AND SALES PLAN BASE CASE (DOMESTIC/IMPORTED COAL) -

2017 2016 2015

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PAGE 3

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TOTAL SALES REVENUE

SALES REVENUE

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(US\$, MILLION) *** COKE PLANT PROJECT IN VENEZUELA ***
 working capital statements
- Base case (Domestic/imported coal) -

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*** COKE PLANT PROJECT IN VENEZUELA *** WORKING CAPITAL STATEMENTS - BASE CASE (DOMESTIC/IMPORTED COAL) - (US\$, MILLION)

2017 2016 2015

YEAR

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CHANGE IN WORKING CAPITAL

PAGE 3

*** COKE PLANT PROJECT IN VENEZUELA ***
 iNCOME STATEMENTS
 BASE CASE (DOMESTIC/IMPORTED COAL) - (USS, MILLION)

OPERATING INCOME	0.0	0.0	0.0	80.255	111.861	114.747	114.747	114.747	114,747	114,747
TOTAL SALES REVENUE	0.0	0.0	0.0	80.255	111.861	114.747	114.747	114.747	114.747	114.747
COST OF SALES	0.0	0,0	0.0	06	83		120,624	120.624	120.624	120.624
VARIABLE COST	0.0		0.0	54.923	58, 654	68.654	68.654	1 • •	68.654	68.654
DIRECT FIXED COST DEPRECIATION AND AMORTIZATION	00	00		19.938 19.028	800 000 000 000	358 81 32 033	32 838 32 033	358 81 37 033	19,938 37 033	855 61 650 65
INC. IN PRODUCT INVENTORY	00		0.0	13.901	1.786	0.0	0.0	0.0	0.0	0.0
PROFIT ON SALES	0.0	0.0	0.0	-12.738	-8.977	-5.877	-5.877	-5.877	-5.877	-5.877
A SALES EXPENSES	0.0	0.0	0.0	0.0	0.0	0	0 0	0.0	0.0	0,0
- 10	0	0.0	0.0	-12.738		-5.877	-5,877	-5.877	-5.877	-5.877
NON-OPERATING EXPENSES	0.0	0.0	0.0	23.162	23,531	23.697	23.586	23,457	23,323	23.181
INTEREST ON LONS TERM DEBT	00	00 00	00	23.162	22.004	20.845 2.851	19.687	18.529 4.928	17.371 5.951	16.213 6.968
NET PROFIT OR (LOSS) BEFORE TAX	0.0	0.0	0.0	-35,900	-30,508	-29.574	-29.463	•	-29.200	-29.058
	0,0	0.0	0,0	0,0	0.0	0.0	0.0	0.0	0.0	0.0
NET PROFIT OR (LOSS) AFTER TAX	0	0.0	0.0	-35,900	-30.508	-29.574	-29.463	-29,335	-29,200	-29.058
DIVIDENDS	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0,0	0.0
RETAINED EARNINGS	0.0	0 * 0	0.0	006198-	-30.508	-29.574	-29:463	-29.335	-29.200	-29.058

PAGE 1

(US\$, MILLION) *** COKE PLANT PROJECT IN VENEZUELA *** INCOME STATEMENTS - BASE CASE (DOMESTIC/IMPORTED COAL) -

YEAR

68.654 19.938 32.033 0.0 114.747 114.747 114.747 114.747 4.632 16.678 114.747 120.624 21.310 -27.188 -5.877 -5.877 -27.138 0.0 0.0 0.0 120.624 120.624 68.654 19.938 32.033 0.0 5,790 15,751 114.747 -5,877 -27.418 -27,418 -5.877 21.541 0.0 0 0.0 68,654 19,938 32,033 0.0 6 948 14 812 114.747 -27.638 -27.638 -5,877 21.761 -27.638 -5.877 111111 0.0 0 0.0 68,654 19,938 32,033 21.970 114.747 120.624 8.107 13.864 -27.847 -27.847 -5.877 -5.877 -27.847 0.0 0.0 0.0 68 654 19 938 32 033 0 0 114.747 9.265 12.905 114.747 120.624 22.169 -28.047 -28.047 1111111 -28.047 -5.877 -5.877 1 1 1 1 1 1 1 0.0 0 0 0 114.747 114.747 114.747 68,654 19,938 32,033 0,0 114,747 10.423 11.936 120.624 -28.237 -28.237 ł 22.359 -28.237 -5.877 1111111 -5.877 0.0 0.0 0.0 1111 68.654 19.938 32.033 0.0 114.747 120.624 -28.417 22.540 -28.417 -28.417 -5.877 -5.877 11.581 10.959 ------1 0.0 0.0 0.0 114.747 114.747 114.747 68 654 19,938 32,033 0,0 12.739 9.973 -28.589 120.524 -28.589 -28.589 -5,877 22.712 -5.877 0.0 0.0 0.0 114.747 68.654 19.938 32.033 13,897 8,979 120.624 -28.753 22.876 -28.753 -28.753 -5.877 -5.877 -----1 1 0.0 0.0 0.0 0.0 114.747 68 654 19 938 32 033 0 0 -28.910 120 624 23.032 15.055 7.977 -28.910 -28.910 -5.877 -5.877 0.0 0.0 0.0

VARIABLE COST DIRECT FIXED COST DEPRECIATION AND AMORTIZATION INC. IN PRODUCT INVENTORY NET PROFIT OR (LOSS) BEFORE TAX NET PROFIT OR (LOSS) AFTER TAX INTEREST ON LONG TERM DEBT INTEREST ON SHORT TERM DEBT NON-OPERATING EXPENSES TOTAL SALES REVENUE GROSS PROFIT ON SALES L OPERATING PROFIT OPERATING INCOME SALES EXPENSES COST OF SALES INCOME TAX DIVIDENDS

A1

RETAINED EARNINGS

-27.188

-27.418

Q.

PAGE

2014

2013

2012

2011

2010

2009

2008

2007

2006

2005

*** COKE PLANT PROJECT IN VENEZUELA *** INCOME STATEMENTS - BASE CASE (DOMESTIC/IMPORTED COAL) - (US\$, MILLION)

2017 2016 2015

ITAL SALES REVENUE 114.747 14.747 14.747 14.747 OF SALES 120.624 120.624 120.624 120.624 RECT FIXED COST 19.938 19.938 19.938 19.938 RECT FIXED COST 0.0 0.0 0.0 0.0 IC. IN PRODUCT INVENTORY 0.0 0.0 0.0 0.0 S. PROFIT ON SALES -5.877 -5.877 -5.877 -5.877 LES EXPENSES 0.0 0.0 0.0 0.0 0.0 ATING PROFIT NSALES -5.877 -5.877 -5.877 -5.877 OPERATING EXPENSES 0.0 0.0 0.0 0.0 0.0 0.0 ATING PROFIT -5.877 -5.877 -5.877 -5.877 -5.877 OPERATING EXPENSES -5.877 -5.877 -5.877 -5.877 -5.877 OPERATING EXPENSES -117.554 18.498 17.554 18.498 -5.877 -5.877 OPERATING EXPENSES -5.877 -5.877 -5.877 -5.874 -5.816 -5.816 -5.816 -5.816 -5.816	OPERATING INCOME	114.747	114.747	114.747
OF SALES 120.624 120.624 120.624 Riable cost 68.654 68.654 19.938 PRECIATION AND AMORTIZATION 32.033 32.033 32.033 C. IN PRODUCT INVENTORY 32.033 32.033 32.033 S PROFIT ON SALES -5.877 -5.877 -5.877 S PROFIT ON SALES -5.877 -5.877 -5.877 ATING PROFIT -5.877 -5.877 -5.877 COERATING EXPENSES 21.068 20.814 TEREST ON LONG TERM DEBT 17.594 18.498 TEREST ON LONG TERM DEBT 17.594 18.498 TEREST ON LONG TERM DEBT -5.6.946 -26.691 TEREST ON LONG TERM DEBT -5.6.946 -26.691 TEREST ON LOSS BEFORE TAX 0.0 0.0 0.0 COME TAX -26.946 -26.661 - TEREST ON LOSS BEFORE TAX 0.0 0.0 0.0 0.0 </td <td>TOTAL SALES REVENUE</td> <td>114.747</td> <td>114.747</td> <td>114.747</td>	TOTAL SALES REVENUE	114.747	114.747	114.747
RIABLE COST RECT FIXED COST 68.654 68.654 68.654 RECT FIXED COST 32.033 32.033 32.033 PRECIATION AND AMORTIZATION 32.033 32.033 32.033 IC. IN PRODUCT INVENTORY 0.0 0.0 0.0 S PROFIT ON SALES -5.877 -5.877 -5.877 LES EXPENSES 0.0 0.0 0.0 0.0 ATING PROFIT -5.877 -5.877 -5.877 ATING PROFIT -5.877 -5.877 -5.874 PROFIT OR (LOSS) BEFORE TAX<	OF SALES	120 624		120.6
RECT FIXED COST 19.938 19.938 PRECI FIXED COST 0.0 0.0 0.0 S: PROFIT ON SALES -5.877 -5.877 -5.877 S: PROFIT ON SALES -5.877 -5.877 -5.877 LES EXPENSES 0.0 0.0 0.0 ATING PROFIT -5.877 -5.877 -5.877 LES EXPENSES 0.0 0.0 0.0 ATING PROFIT -5.877 -5.877 -5.877 LES EXPENSES 0.0 0.0 0.0 0.0 ATING PROFIT -5.877 -5.877 -5.877 DOFERATING EXPENSES -5.877 -5.877 -5.877 OPERATING EXPENSES 21.068 20.814 TEREST ON LONG TERM DEBT 17.554 18.498 TEREST ON LONG TERM DEBT 17.554 18.498 PROFIT OR (LOSS) BEFORE TAX -26.946 -26.651 COME TAX -26.946 0.0 0.0 VIDENDS 0.0 0.0 0.0 0.0	VARIABLE COST	68.654	1	1
IC. IN PRODUCT INVENTORY 0.0 0.0 0.0 I.ES EXPENSES -5.877 -5.877 -5.877 I.ES EXPENSES 0.0 0.0 0.0 ATING PROFIT -5.877 -5.877 -5.877 ATING PROFIT -5.877 -5.877 -5.877 ATING PROFIT -5.877 -5.877 -5.877 OPERATING EXPENSES 21.068 20.814 OPERATING EXPENSES 21.068 20.814 OPERATING EXPENSES 21.068 20.814 OPERATING EXPENSES 21.068 20.814 PROFIT ON KLOSS BEFORE TAX -26.946 -26.691 PROFIT OR (LOSS) BEFORE TAX -26.946 -26.691 COME TAX -26.946 -26.661 PROFIT OR (LOSS) AFTER TAX -26.946 -26.651 VIDENDS 0.0 0.0 0.0	IRECT FIXED COST EPRECIATION AND AMORTIZATION	19,998 30,000		19.938
S PROFIT ON SALES -5.877 -5.877 -5.877 -5.877 LES EXPENSES 0.0 0.0 0.0 0.0 ATING PROFIT -5.877 -5.877 -5.877 -5.877 ATING PROFIT -5.877 -5.877 -5.877 -5.877 OPERATING EXPENSES -21.068 20.814 2.316 TEREST ON LONG TERM DEBT 3.474 2.316 -2.316 TEREST ON LONG TERM DEBT 17.534 18.498 -2.619 PROFIT OR (LOSS) BEFORE TAX -26.946 -26.631 - COME TAX -26.946 -26.631 - - PROFIT OR (LOSS) BEFORE TAX -26.946 -26.631 - VIDENDS 0.0 0.0 0.0 0.0 0.0	INC. IN PRODUCT INVENTORY	0.0		0.0
LES EXPENSES 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	GROSS PROFIT ON SALES	-5.877	-5,877	-5.877
ATING PROFIT -5.877 -5.877 -5.877 OPERATING EXPENSES 21.068 20.814 TEREST ON LONG TERM DEBT 3.474 2.316 TEREST ON SHORT TERM DEBT 3.474 2.316 PROFIT OR (LOSS) BEFORE TAX -26.946 -26.691 COME TAX -26.946 -26.691 PROFIT OR (LOSS) BEFORE TAX 0.0 0.0 COME TAX -26.946 -26.691 PROFIT OR (LOSS) BEFORE TAX 0.0 0.0 VIDENDS VIDENDS -26.946 -26.691	ALEO EXPENSES	0.0	0.0	0
OPERATING EXPENSES 21.068 20.814 TEREST ON LONG TERM DEBT 3.474 2.316 TEREST ON SHORT TERM DEBT 3.474 2.316 PROFIT OR (LOSS) BEFORE TAX -26.946 -26.651 PROFIT OR (LOSS) BEFORE TAX -26.946 -26.651 PROFIT OR (LOSS) BEFORE TAX -26.946 -26.651 VIDENDS 0.0 0.0 0.0 VIDENDS 105 0.0 0.0 0.0	OPERATING PROFIT	نې ۱	-5.877	8 I I I I I I I I I I I I I I I I I I I
TEREST ON LONG TERM DEBT 3.474 2.316 TEREST ON SHORT TERM DEBT 3.474 2.316 PROFIT OR (LOSS) BEFORE TAX -26.946 -26.631 PROFIT OR (LOSS) BEFORE TAX 0.0 0.0 COME TAX -26.946 -26.631 PROFIT OR (LOSS) BEFORE TAX 0.0 0.0 PROFIT OR (LOSS) AFTER TAX -26.946 -26.631 VIDENDS 0.0 0.0 0.0 VIDENDS 0.0 0.0 0.0	TING EXPENSES	1		20.5
PROFIT OR (LOSS) BEFORE TAX -26.946 -26.651 COME TAX 0.0 0.0 PROFIT OR (LOSS) AFTER TAX -26.946 -26.651 PROFIT OR (LOSS) AFTER TAX 0.0 0.0 VIDENDS -26.946 -26.651	T ON LONG TERM D T ON SHORT TERM		- ~ ~	1
COME TAX 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	FIT OR (LOSS) BEFORE	-26.946	-26,631	-26.424
PROFIT OR (LOSS) AFTER TAX -26.946 -26.691	E TAX	0	0,0	
IDS 0.0 0.0 2.0 EARNINGS -26.631	AFTER	-26.946	-26.691	
EARNINGS ~26.691	ENDS	0.0	0.0	
		-26.946		-26

PAGE 3

-----*** COKE PLANT PROJECT IN VENEZUELA *** FUNDS FLOW STATEMENTS BASE CASE (DOMFSTICTIMODATES ACCOVE

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	- BASE CA	CASE (DOMES	(DOMESTIC/IMPORTED COAL)	TED COAL)	SO) -	(USS WILLION)	(N			
Y EAR	1995	1996	1997	1998	1999	2000	2001	2002	2003	2004
SOURCE OF FUNDS	66.176	330.880	264.704	49.845	82.083	104.127	124.719	145,183	165.512	185,699
	0.0			0	l in	26 155	26,155	26.155	26 155	26,155
PROFIT AFT. TAX. BFR INT. DEPRECIATION AND AMORTIZATION FINANCIAL RESOURCES	0.0 0.0 66.176	0.0 330.880	264.704		-6.977 -6.977 32.033 57.028			-5.877 -5.877 32.033 119.028	-5.877 -5.877 32.033 139.356	-5.877 -5.877 32.033
SHARE CAPITAL LONG TERM DEBT SHORT TERM DEBT	19.853 46.323 0.0	99.264 231.616 0.0	79.411	0.0 0.0 30.550	0.0 0.0 57.028	0.0	0.0 0.0 38.564	0.0	0.0 139.356	000
USES OF FUNDS	64.301	321,505	257.204	68.594	82.083	104.127	124.719	145.183	165.512	185,699
FIXED CAPITAL EXPENDITURE		321,505	1 2	0.0	0.0	0 0	0.0	0.0	0.0	0,0
NON-DEPRECIABLE ASSETS DEPRECIABLE FIXED ASSETS INTEREST DURING CONSTRUCTION	0.236 61.328 2.737	 	0,944 245.312 10,948	000	000	000	0.00	0.00	000	000
CHANGE IN WORKING CAPITAL	0 0	0.0	0	22.271	4,840	0.240	0.0	0,0	0.0	0.0
DERT SERVICES	0	0.0	0,0	10	1 4	03.886	124.71	5.18	165.512	185,699
REPAYMENT OF LONG TERM DEBT REPAYMENT OF SHORT TERM DEBT INTEREST ON LONG TERM DEBT INTEREST ON SHORT TERM DEBT	0000	0000	0000	23.162 2.0 23.162 23.162 0.0	22.552 1.552.552 1.552.552.552 1.552.552 1.552.552	23.162 57.023 20.845 2.351	23.162 77.971 19.687 3.899	23.162 188.564 188.564 18.529 229	23.162 119.028 17.371 5.951	23.162 139.356 16.213 6.968
D1 V 1 DENDS	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
CASH INCREASE OR (DECREASE)	1.875	9.375	7.500	-18.750	0,0	•	0,0	· ·	1	0.0
BEGINNING CASH BALANCE Ending Cash Balance		1.875	11.250		00	00	0.0	0.0	0.0	0.0

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-5,877 32,033 351,879 23.162 333.563 4.632 16.678 0.0 0.0 0.0 0.0 0.0 0.0 315.015 333.563 351.879 0.0 000.0-26.155 378,035 378.035 373.03! -0.000 1 1 1 1 1 1 000 0.0 2014 o N 26.155 23.162 315.015 5.790 15.751 359.718 000 01 PAGE 322.403 341,170 359,718 -5.877 -5.877 32.033 32.033 315.015 333.563 341.170 359.718 ---------0.000 0.0 000 0.0 2013 ь ò 1 1 1 26,155 341,170 23 162 296 248 6 948 14 812 -----....... -0.000 0.0 2012 000 0.0 0 0.0 0.0 296.248 26,155 -5.877 32.033 296.248 322.403 000.0-23.162 277.271 8.107 13.854 322.403 ----------0.000 11111 ------2011 0.0 000 0.0 0 0.0 (NOITIW 'SSN) 26, 155 0.0 0.0 277.271 000 -5,877 32,033 277,271 23 162 258.095 9.265 12.905 000 0-303,426 303.426 303.426 -0.000 ------0.0 0.0 0 2010 -5.877 32.033 258.095 0.0 0.0 258.095 284.251 284.251 284.251 26.155 23.162 238.730 10.423 11.936 -0,000 ------0.000 11112124 1111111 ----0.0 000 0.0 *** COKE PLANT PROJECT IN VENEZUELA ***
 FUNDS FLOW STATEMENTS
 BASE CASE (DOMESTIC/IMPORTED COAL) - (2003 0 26.155 -5.877 32.033 238.730 0.0 0.0 0.0 0.0 219.183 238.730 23.162 219.183 11.581 10.959 245.339 264,885 254,885 264,885 ****** **** 11111111 2008 000 0.0 00 0 0 0.0 0 26.155 0.0 -5.877 32.033 219.183 23.162 199.465 12.739 9.973 245 339 -----245.333 , 000 0.0 0.0 00 2007 o 1 + 2 1 1 1 o. 00 0,0 0,0 0,0 0,0 179,582 199,465 225.620 225.620 23.162 179.582 13.897 8.979 225.620 ----------000 2006 0.0 0.0 0.0 0 00 0 o o 26,155 0.0 205.738 -5 877 32 033 179 582 23.152 159.544 15.055 7.977 205.738 205.738 -----------000 2005 0.0 0.0 0.0 00 00 PROFIT AFT. TAX. BFR INT DEPRECIATION AND AMORTIZATION FINANCIAL RESOURCES NON-DEPRECIABLE ASSETS DEPRECIABLE FIXED ASSETS INTEREST DURING CONSTRUCTION REPAYMENT OF LONG TERM DEBT REPAYMENT OF SHORT TERM DEBT INTEREST ON LONG TERM DEBT INTEREST ON SHORT TERM DEBT ********* CASH GENERATED FROM OPERATION USES OF FUNDS CHANGE IN WORKING CAPITAL CASH INCREASE OR (DECREASE) BEGINNING CASH BALANCE ENDING CASH BALANCE SHARE CAPITAL LONG TERM DEBT SHORT TERM DEBT DEBT SERVICES SOURCE OF FUNDS

YEAR

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DIVIDENDS

*** COKE PLANT PROJECT IN VENEZUELA *** FUNDS FLOW STATEMENTS - BASE CASE (DOMESTIC/IMPORTED COAL) - (

(NOSE, MILLION)

2016 2015

	I		431.483
CASH GENERATED FROM OPERATION	26.155	26.155	26.155
PROFIT AFT. TAX. BFR INT.	-5.877		
DEPRECIATION AND AMORTIZATION			32,033
	369.954	387.774	405.327
SHARE CAPITAL	0.0	0.0	0.0
LONG TERM DEBT	0.0	0,0	0.0
SHORT TERM DEBT	369.954	õ	405.327
I USES OF FUNDS	336 109	396 109 413,929 431 483	431.483
C TELEVISION	0.0	0.0	0 0
NON-DEPRECIABLE ASSETS	0.0	0.0	0.0
DEPRECIABLE FIXED ASSETS		0.0	0.0
INTEREST DURING CONSTRUCT	0.0 NG	0.0	0.0
DEPRECIABLE FIXED ASSETS DEPRECIABLE FIXED ASSETS INTEREST DURING CONSTRUCTION	0.0 0.0 N		000

431.483	0	000	0.0 431.433 331.443 337.142 19.389 19.389
413.929	0.0	000	0.0 23.162 35.23.162 35.23.316 18.23.316 18.23.316 18.23.316 18.23.316 18.23.316 18.23.16 18.23.16 18.23.16 19.23 10.23 1
396.109	0	000	396.109 351.879 351.879 351.879 351.879 351.879 351.879 351.879 351.879 351.879 351.879 351.879 351.879 351.879 351.879 351.879 351.879 351.879 351.759 474

DEBT SERVICES

CHANGE IN WORKING CAPITAL

REPAYMENT OF LONG TERM DEBT REPAYMENT OF SHORT TERM DEBT INTEREST ON LONG TERM DEBT INTEREST ON SHORT TERM DEBT DIVIDENDS

CASH INCREASE OR (DECREASE)

BEGINNING CASH BALANCE ENDING CASH BALANCE

-0.000

-0.000 000.01

000.001

2017

PAGE 3

YEAR

SOURCE OF FUNDS

2.360 613.280 27.370 277.939 5.721 23.162 159.544 0.0 9.562 23.511 198.528 -213.038 277,939 -14.510 451.855 33.073 418.783 643.010 224.228 466.366 451.355 188.426 -----.......... 0.0 2004 ***** *** 0.0 9.562 23.511 2.360 613.280 27.370 301.101 5.721 23.162 139.356 PAGE 301.101 483, 888 33.073 450.815 643.010 192.195 469.340 168.239 14.548 198.528 198.528 -154.780 -183.980 ----------0.0 2003 2.360 613.280 27.370 472.172 5 721 23 162 119 028 0.0 9.562 23.511 324.262 515.920 160.163 147, 910 324.262 43.748 33.073 482.848 643.010 ***** -------0.0 0.0 2002 2.360 613.280 27.370 347.424 0.0 5.721 23.162 98.564 347.424 547.953 0.0 9.562 23.511 198.528 -125.445 127,446 73.083 514.880 643.010 128.130 474.870 33,073 0.0 2001 (USS. MILLION) 2.360 613.280 27.370 370.586 0.0 0.0 9.562 23.511 5.721 23.162 77.971 370.586 198,528 -95,982 579,985 643.010 36.098 477.439 546.913 106.854 102.546 33.073 0 2000 2.360 613.280 27.370 611,777 5.721 23.162 57.028 0.0 9.321 23.511 393.747 0.0 198.528 -66.408 643.010 578,945 85,910 393.747 32.832 64,065 479,657 132.120 11111111111 0.0 0 666 *** COKE PLANT PROJECT IN VENEZUELA *** BAIANCE SHEET BASE CASE (DOMESTIC/IMPORTED COAL) + 2.360 613.280 27.370 637.826 0.0 6.688 20.160 4.577 23.162 30.550 416.909 0.0 198,528 -35,900 643.010 416.909 26.848 610.978 475.197 162.628 -----32.033 58.288 11111111 0 0 1998 2.360 613.280 27.370 661,760 440 070 0 0 0 0 23.162 0.0 198.528 0.0 643.010 440.070 643.010 198.528 18.750 1 1 1 1 1 1 1 463 232 23.162 000 0 0.0 1997 1.416 367.968 16.422 397,056 119.117 0.0 277.939 385.806 385,806 11.250 277.539 27.7.939 119.117 -----0.0 000 1996 0 000 o ó 000 o. 0.236 61.328 2,737 19.853 19.853 0.0 46.323 0.0 64.301 64.301 66.176 1.875 46.323 46.323 000 000 1995 0 0.0 0 0 L/T DEBT LESS: ACC, DEPRECIATION CTHER FIXED LIABILITIES SHARE CAPITAL ACC. RETAINED EARNINGS ACCOUNT PAYABLE CURRENT PORTION OF SHORT TERM DEBT OPERATING CASH ACCOUNT RECEIVABLE INVENTORIES NON-DEPR. ASSETS DEPRECIABLE ASSETS AMORTIZATION CURRENT LIABILITIES STOCK HOLDERS EQUITY FIXED LIABILITIES NET FIXED ASSETS ACC. EXCESS CASH CURRENT ASSETS INVESTMENT -----LIABILITIES ASSETS ----YEAR

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LIABILITIES & S/H EQUITY

483,838 515.920 547.953 661.760 397.056

579,985 611.777 637.826

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ACCOUNT PAYABLE CURRENT PORTION OF L/T DEBT SHORT TERM DEBT LONG TERM DEBT BALANCE OTHER FIXED LIABILITIES LESS: ACC. DEPRECIATION ACC. RETAINED EARNINGS LIABILITIES & S/H EQUITY ACCOUNT RECEIVABLE INVENTORIES NON-DEPR, ASSETS DEPRECIABLE ASSETS AMORTIZATION CURRENT LIABILITIES STOCK HOLDERS EQUITY FIXED LIABILITIES OPERATING CASH NET FIXED ASSETS ACC. EXCESS CASH SHARE CAPITAL CURRENT ASSETS INVESTMENT LIABILITIES ASSETS

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*** COKE PLANT PROJECT IN VENEZUELA *** BALANCE SHEET - BASE CASE (DOMESTIC/IMPORTED COAL) - (

(NOLTIN .SSU)

YEAR	Ж	2015	IJ	2016		2017	7	
š	ASSETS	່. ເອັ ເ ເອັ ເ	498	67.46	មារ	35	664.	
	RRENT	с) ()	0	33.	თ		20	
	OPERATING CASH	0	0	0.0			0	
	ACCOUNT RECEIVABLE	-	562	9.56	20	6	562	
	INVENTORIES		511	23.5			511	
4	ACC. EXCESS CASH		0.000	-0.00		9	000	
	NET FIXED ASSETS	56.	425	34.39	001 001	8	360	
	INVESTMENT	643	010	643.01	0	643	010	
	NON-DEPR. ASSETS DEPRECIABLE ASSETS AMORT IZATION	613 27	360 280 370	2.36 613.28 27.31	360 280 370	2.360 613.280 27.370	360 370 370	
	LESS: ACC. DEPRECIATION	576	585	508.61	8	640.	650	
LIA	(B1L T1ES	421.	00 (00 1 00 1	416.65	124	411.	540	
o	URRENT LIABILITIES	338	836	416.6	~	411	.048	
1	ACCOUNT PAYABLE ACCOUNT PAYABLE CURRENT PORTION OF SHORT TERM DEBT	000 00 00 00 00 00 00 00 00 00 00 00 00	721 954	5.721 23.162 387.774	•	4 1000	5.721 5.327 5.327	
ւ	S		.162	°.			000	
	LONG TERM DEBT BALANCE OTHER FIXED LIABILITIES	23.162	1950	0.000		00		
stoc	STOCK HOLDERS GOUITY	-322		-349.19		-375,616	616	
	SHARE CAPITAL ACC. RETAINED EARNINGS	198.	8.528 21.029	-547.720			528	

35.433

67,465

99,498

LIABILITIES & S/H EQUITY

PAGE 3

*** COKE PLANT PROJECT IN VENEZUELA ***
 LONG TERM DEBT
 BASE CASE (DOMESTIC/IMPORTED COAL) - (US\$, MILLION)

20 YEAR-EQUAL-INSTALLMENT-REPAYMENT (ANNUAL REPAYMENT) BALANCE AFT. PAYMENT 45, 323 277, 333 24460, 272 4460, 272 333, 747, 333 347, 585 3347, 585 337, 477 231, 101 2301, 101 3374, 262 3324, 262 103 2371, 101 103 256, 171 162, 131 152, 808 115, 808 1 DEBT SERVICE 5 000 PER CENT/YEAR INTEREST 463.232 PRINCIPAL AMOUNT OF DEBT INTEREST RATE SER. NO - 20 4 10 20 -REPAYMENT YEAR

0.0

706.427

243.197

163.230

TOTAL

PAGE 1

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*** COKE PLANT PROJECT IN VENEZUELA ***
PROFITABILITY AND FINANCIAL INDICATORS
- BASE CASE (DOMESTIC/IMPORTED COAL) - (

(USS, MILLION)

(11)* CASH B.E.P. CAPACITY UTILIZE (PCT)	0 - 00 - 00 - 00 - 00 - 00 - 00 - 00 -	124.0
(10) * CASH B.E.P. SALES PRICE PRICE	2 2 2 2 2 2 2 2 2 2 2 2 2 2	160.3
(9)* PROFIT B.E.P. CAPACITY UTILIZE (PCT)	ИГ	165.7
(8) L/T DEBT -TO- S/H EQUITY	1 1 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	0.43 214 / *** 0.44 167 / -67
(7) DEBT SERVICE RATIO	00000000000000000000000000000000000000	
(6) QUICK RATIO	00000000000000000000000000000000000000	0.0 0.05
(5) CURRENT RATIO	00000000000000000000000000000000000000	-14.5 0.17 0.05 -13.3 0.13 0.04
(4) AFT TAX PROF IT -TO- S/CAPITAL S/CAPITAL		ון 19 19
(3) BFR TAX PROFIT -TO- INVESTMENT (PCT)	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	44 84
(2) AFT TAX PROFIT -TO- -TO- S/H EQUITY (PCT)	2007 2007 2007 2007 2007 2007 2007 2007	ERAGE1 -25.7 3.7 ERAGE2 -25.4 30.2
(1) AFT TAX PROFIT -TO- SALES REV (PCT)	4 5 5 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	-25.7
YEAR	86000000000000000000000000000000000000	AVERAGE1 AVERAGE2

(AVERAGE1) : SUM OF ANNUAL FIGURES OF PERCENTAGE AND RATIO IS DIVIDED BY NO. OF YEARS(SIMPLE AVERAGE) (AVERAGE2) : AVERAGE FIGURES ARE CALCULATED BY ACTUAL VALUES ACCUMULATED OVER THE PROJECT LIFE(WEIGHTED AVERAGE) * NOTE FOR (9)(10)(11) WHEN THERE ARE TWO OR MORE PRODUCTS, AND DURING THE YEARS WHEN ALL OF PRODUCTS ARE NOT PRODUCED AT THE SAME RATE OF CAPACITY UTILIZATION, ABOVE BREAK-EVEN-POINTS CANNOT GIVE CORRECT FIGURES.

	4) BFR-TAX (5) AFT-TAX NET IN-FLOW NET IN-FLOW (2)-(1) (4)-(3)	- 261,555 26,155
ICE) (US%, MILLION)	<pre>(4) BFR-TAX (5) AFT-TAX NET IN-FLOW NET IN-FLO (2)-(1) (4)-(3)</pre>	
	I NCOME TAX	
IN VENEZUELA ; (IN '93 FIXED RTED COAL) -	(2) GROSS (3) CASH IN-FLOW	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
*** COKE PLANT PROJECT IN VENEZUE FINANCIAL RATE OF RETURN (IN '33 FI BASE CASE (DOMESTIC/IMPORTED COAL)	DEPRECIATN (2)	0 0 0 2 2 2 0 0 2 3 2 2 0 0 2 3 2 0 0 2 3 2 0 0 2 3 2 0 0 3 3 0 0 0 0 0 0
- m	OPERATING PROFIT	
ι.	(1) GROSS CAPITAL EXPENDTR	61.564 307.820 22.271 4.840 0.240 0.02 0.02 0.0 0.0 0.0 0.0 0.0 0.0 0.0
	CHANGE IN WORKING CAPITAL	2000 2000 2000 2000 2000 2000 2000 200
	FIXED CAPITAL EXPEND.	8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8
	YEAR	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2

INTERNAL RATE OF RETURN

ON (4) BFR-TAX NET IN-FLOW (2)-(1) -1.37 PER CENT ON (5) AFT-TAX NET IN-FLOW (4)-(3) -1.37 PER CENT

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	ACC.NET IN-FLOW	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 1.22,501 1.15,213 0.23,547 1.2,213 0.23,547 1.2,213 0.23,547 1.2,213 1.3,213 1
LL I ON Y	(3) NET IN-FLOW (1)-(2)	211 - 22 - 23 - 23 - 24 - 24 - 25 - 25 - 25 - 25 - 25 - 25
XED PRICE) XED PRICE) (USS. MILLION)	ACC. OUT-FLOW	0.00 0.00
*** COKE PLANT PROJECT IN VENEZUELA *** Foreign currency earnings (in '93 Fixed Price) Base case (domestic/imported coal) - (USS.	(2) TOTAL OUT-FLOW	0.0 0.0 0.0 0.0 101.872 111.537 111.537 110.232 100.1125.7354 102.4538 102.4538 102.45638 102.45638 102.45638 100.006 95.373 93.657 93.757 93.657 93.657 93.657 93.657 94.557 94.557 94.557 957 957 957 957 957 957 957 957 957
PLANT PROJECT IN VENEZUE RRENCY EARNINGS (IN '93 (DOMESTIC/IMPORTED COAL)	REPAYMENT ON	0.0 23.162 23.222 23.162 23.222 23.162 23.2222 23.2222 23.2222 23.2222222222
*** COKE PL FOREIGN CURF BASE CASE (I	INTEREST ON L/T	22.000 23.000 23.000 23.000 23.000 24.0000 24.0000 24.0000 24.0000 24.0000 24.0000 24.0000000000
	IMPORT COAL & MATERIALS	0.0 0.0 0.0 6.7.55 7.55
	ACC.	000 100 100 100 100 100 100 100
	<pre><1> !N-FLOW FROM SALES</pre>	0000 11111 11111 11111 11111 111111
	<1> YEAR	1565 1566 1566 1566 1566 1566 1566 1566

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	AFT-TAX 1N-FLOW 1-(3)	-55 237 237 237 237 232 27 232 27 932 932 27 932 932 27 932 27 932 932 27 932 932 932 932 932 932 932 932 932 932
	(5) AF W NET 11 (4)	
ICE> MILLION>	<pre>(4) BFR-TAX (5) AFT-TAX NET !N-FLOW NET !N-FLO (2)-(1) (4)-(3)</pre>	59 59
PX-CR) (US6)	I NCOME TAX	
VENEZUELA ### N '93 FIXED PR ED COAL) -	e e	
IN VENE 1N VENE 087ED CO/	(2) GROSS CASH IN-FLOW	80000000000000000000000000000000000000
PLANT PROJECT MATE OF RETURN (DOMESTIC/IMP	DEPRECIATN	0,0 0,0 0,0 0,0 29,577 29,577 29,577 29,577 29,577 29,577 29,577 29,577 29,577 29,577 29,577 29,577 29,577 272 272 272 272 272 272 272 272 272
*** COKE PLANT PROJECT IN VENEZUELA *** ECONOMIC RATE OF RETURN (IN '93 FIXED PRICE) BASE CASE (DOMESTIC/IMPORTED COAL) - (US\$	OPERATING PROFIT	00000000000000000000000000000000000000
(ECONOMIC) - 8	(1) GROSS CAPITAL EXPENDTR	23 23 23 23 24 24 24 24 24 24 24 24 24 24
Â	CHANGE IN WORKING CAPITAL	2000 200 2000 2
	F I XED CAP1 TAL EXPEND.	22 22 22 22 22 22 22 22 22 22 22 22 22
	YEAR	1935 1935 1935 1935 1935 1935 2000 2000 2001 2011 2012 2012 2013 2013

INTERNAL RATE OF RETURN

ON (4) BFR-TAX NET IN-FLOW (2)-(1) -0.58 PER CENT ON (5) AFT-TAX NET IN-FLOW (4)-(3) -0.58 PER CENT

Appendix-2 FINANCIAL AND ECONOMIC STATEMENTS FOR ALT. CASE

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 PRODUCTION AND SALES PLAN
ALT. CASE (DOMESTIC COAL INC.BOYACA) - (USS, MILLION)
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SALES REVENUE

I SALES REVENUE

A2

SALES REVENUE

SALES REVENUE

SALES REVENUE

RATED CAPACITY (TOTAL COKE) CAPACITY UTILIZATION BF COKE PRODUCTION (1000TPY) INCREASE IN INVENTORY (1000TPY) BF COKE TO EXPORT (1000TPY) BF COKE TO EXPORT (1000TPY)

BREEZE PRODUCTION (1000TPY) INCREASE IN INVENTORY (1000TPY) BREEZE TO EXPORT (1000TPY) UNIT SALES PRICE (USS/T)

SALES REVENUE

SALES REVENUE

RATED CAPACITY (TOTAL COAL) CAPACITY UTILIZATION TAR PRODUCTION (1000TPY) INCREASE IN INVENTORY (1000TPY) NCREASE IN INVENTORY (1000TPY) UNIT SALES PRICE (USS/T)

C SALES REVENUE
BENZEME PRODUCTION (1000TPY)
INCREASE IN INVENTORY (1000TPY)
BENZEME TO EXPORT (1000TPY)

BENZENE TO EXPORT (1000TP UNIT SALES PRICE (USS/T)

SALES REVENUE

SULFATE PRODUCTION (1000TPY) INCREASE IN INVENTORY (1000TPY) SULFATE TO EXPORT (1000TPY) UNIT SALES PRICE (US\$/T) SALES REVENUE SALES REVENUE

TOTAL SALES REVENUE

*** COKE PLANT PROJECT IN VENEZUELA *** Production and sales plan - Alt. case (domestic coal inc.boyaca) - (US\$, Million)

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PAGE 2

2014

2013

*** COKE PLANT PROJECT IN VENEZUELA ***
 PRODUCTION AND SALES PLAN
- ALT. CASE (DOMESTIC COAL INC.BOYACA) - (US\$, MILLION)

2017 2016 2015

> RATED CAPACITY (TOTAL COKE) CAPACITY UTILIZATION EAPCITY UTILIZATION INCREASE IN INVENTORY (1000TPY) BF COKE TO EXPORT (1000TPY) UNIT SALES PRICE (US\$/T)

SALES REVENUE

▋▎▎▎▋▋▋▋₿द⋫┊↑╡╡▋▋₿₿┋╪₽▋₿₽₽┊╪┇▋ BREEZE PRODUCTION (1000TPY) INCREASE IN INVENTORY (1000TPY) BREEZE TO EXPORT (1000TPY) UNIT SALES PRICE (US\$/T) SALES REVENUE

SALES REVENUE RATED CAPACITY (TOTAL COAL) CAPACITY UTILIZATION TAR PRODUCTION (1000TPY) INCREASE IN INVENTORY (1000TPY) TAR TO EXPORT (1000TPY) C UNIT SALES PRICE (USS/T)

BENZENE PRODUCTION (1000TPY) INCREASE IN INVENTORY (1000TPY) BENZENE TO EXPORT (1000TPY) UNIT SALES PRICE (USS/T) SALES REVENUE

SULFATE PRODUCTION (1000TPY) INCREASE IN INVENTORY (1000TPY) SULFATE TO EXPORT (1000TPY) UNIT SALES PRICE (US\$/T)

SALES REVENUE

TOTAL SALES REVENUE

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*** COKE PLANT PROJECT IN VENEZUELA ***
 PRODUCTION COST STATEMENTS
- ALT. CASE (DOMESTIC COAL INC.BOYACA) - (US\$, MILLION)

2017 2016 2015 850.000

850,000

228,323 11,228,323 228,323 20,02,333 20,0393 20,333 20,333 20,333 20,333 20,333 20,333 20,333 20,033 20,033 20,033 20,033 20,033 20,033 20,00 20,033 20,00 20,033 20,033 20,00 20,033 20,00 20,033 20,00 20,033 20,00 20,033 20,00 20,033 20,00 20,033 20,00 20,033 20,033 20,00 20,033 20,035

YEAR

BF COKE PRODUCTION (1000TPY)	850,000
is i	40.226 28.393
IMPORTED COAL (BOYACA) IMPORTED COAL (U.S.A)	11.833
AS	2.983
ULLUTES COST ELECTRICITY	~ ~
•	0.099
CAT/CHEM	1 304
u u u u u u u u u u u u u u u u u u u	.62
COKE OVEN GAS VARIABLE COST	-6.622 38 787
EMPLOYMENT COST	6.115
0	4 077
OVERHEAD	2,038
MAINTENANCE COST	10.607
ō	312.5
ASH FACTORY COST	58.725
RECIABLE ASSI	30.318
RE-OPERATIONAL EXP	•
INTEREST DRG C	1.368
PRECIATION AND AMOR	
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UNIT FACTORY COST	90,757 106,7732,10
S EXPENSES	0.0
INTEREST ON LONG TERM DEBT	3.447
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INTEREST ON SHORT TERM DEBT

TOTAL PRODUCTION COST UNIT PRODUCTION COST

94.205 93.055 91.906 110.8288 109.4770 108.1251

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CURRENT ASSETS

YEAR

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CHANGE IN WORKING CAPITAL

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- 8 A2

*** COKE PLANT PROJECT IN VENEZUELA *** WORKING CAPITAL STATEMENTS - ALT. CASE (DOMESTIC COAL INC.BOYACA) - (US\$, MILLION)

2015 2016 2017

CURRENT ASSETS

ACCOUNT RECEIVABLE INVENTOR!ES PRODUCT INVENTORY PRODUCT INVENTORY

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CHANGE IN WORKING CAPITAL

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PAGE 3

	+** CC	COKE PLANT INCON CASE (DOMES	PLANT PROJECT IN VE INCOME STATEMENTS (DOMESTIC COAL INC.	PLANT PROJECT IN VENEZUELA INCOME STATEMENTS (DOMESTIC COAL INC.BOYACA)	¥ ⊁ ¥ [(USS, MILLION)	CN CN		PAGE	***
YEAR	រះ ភូ ភូ ភូ	965	1997	1998	806 L	2000	2001	2002	2003	2004
OPERATING INCOME	0	0.0	_	80.300	26	114.816	.81	14.81	. 81	114.816
TOTAL SALES REVENUE	0,0	0,0	0.0	80.300	111.928	114.816	114.816	114,816	114.816	114.816
COST OF SALES	ò		0.0	N.	с. С	90.757	<u>۲</u>	75	. 75	90.757
VARIABLE COST	0.0	0.0	0.0	31.030		• •	1 10	38.787	38 787	38 787
DIRECT FIXED COST	0.0	0.0	0	ത	, co	19.938	19,938	, oi	່ຫ່	855.61
DEPRECIATION AND AMORTIZATION INC. IN PRODUCT INVENTORY	0.0	00	00	32.033 10.804	32.033 1.010	32.033 0.0	32.033 0.0	32.033 0.0	32.033 0.0	32.033 0.0
GROSS PROFIT ON SALES	0.0	0.0	00	8.104	22.180	24.058	24.058	24,058	24.058	24.058
C SALES EXPENSES	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
1 OPERATING PROFIT	0.0	0,0	0.0	8.104	22.180	24.058	24.058	24.058	24,058	24.058
NON-OPERATING EXPENSES	0,0	0.0	0.0	22.982	22.295	ø	ហ	ů.	53	16.087
INTEREST ON LONG TERM DEBT	00	00 00	00	80	21.833 0.463	20,684	19.534	18 385	17.236	16.087
NET PROFIT OR (LOSS) BEFORE TAX	0.0	0.0			-0.115	٦.	4,524	5.673	6,822	7,971
	0.0	0.0	0	0.0	0.0	0.955	1.357	1.702	2.047	2.391
NET PROFIT OR (LOSS) AFTER TAX	0.0	0.0		-14.878	-0.115	2.228		•	. 77	5,580
DIVIDENDS	0	0.0	0.0	0.0	0,0	0.0	0.0	0 0	0.0	0.0
RETAINED EARNINGS	0,0	0.0	0.0	-14.878	-0.115	2.228	3.167	3.971	4.775	5.580

N PAGE *** COKE PLANT PROJECT IN VENEZUELA *** INCOME STATEMENTS - ALT. CASE (DDMESTIC COAL INC.BOYACA) - (US\$, MILLION)

38.787 19.938 32.033 0.0 4.596.0 114.816 114.816 114.816 114.816 114.816 114.816 114.816 114.816 114.816 114.816 114.816 114.816 114.816 4.596 5.839 24,058 24.058 19.462 90.757 13.623 0.0 -----0 0 38,787 19,938 32,033 0,0 5.745 5.745 0.000 90.757 18,313 5,494 12.819 24.058 ******* 24.053 0.0 0.0 0 38 787 19 938 32 033 0 033 6, 895 0, 000 17.164 90.757 24.058 24.058 5.149 12.015 6.895 0.0 0.0 38.787 19.938 32.033 0.0 114.816 8.044 0.000 90.757 16.015 4.804 24.058 24.058 8.044 11.210 -----1 1 1 1 1 1 ----0.0 0.0 38.787 19.938 32.033 0.0 114.816 90.757 9.193 0.000 9, 193 14.866 24.058 24.058 4.460 10.406 ----------....... 0.0 0.0 38.787 19.938 32.033 0.0 114.816 10.342 0.000 90.757 10.342 4.115 24.058 24.058 13.717 9,602 -----0.0 0.0 38,787 19,938 32,033 0,0 11.491 114.816 90.757 24.058 24.058 11.491 12.568 3.770 8.797 1111111111 0.0 0.0 0 38.787 19.938 32.033 0.0 14.816 12.640 0.000 12.640 11.418 3.426 7.993 24.058 24.058 90,757 --------------0.0 0 38.787 19.938 32.033 0.0 13.789 13.789 10.269 3.081 114.816 90.757 7.189 24.058 24.058 ------------0.0 0.0 1 114.816 38.787 19.938 32.033 0.0 14.938 0.000 114.816 24.058 14 938 9.120 2.736 0.0 90.757 6.384 24.058 ---------------0.0 VARIABLE COST. DIRECT FIXED COST DEPRECIATION AND AMORTIZATION NET PROFIT OR (LOSS) BEFORE TAX NET PROFIT OR (LOSS) AFTER TAX

13,623

12.819

12.015

11.210

10.406

9.602

8.797

7.993

7.189

6.384

RETAINED EARNINGS

DIVIDENDS

INTEREST ON LONG TERM DEBT

INCOME TAX

1

NON-OPERATING EXPENSES

INC. IN PRODUCT INVENTORY

GROSS PROFIT ON SALES

SALES EXPENSES 1 OPERATING PROFIT

A2

YEAR

TOTAL SALES REVENUE

COST OF SALES

OPERATING INCOME

1

		ZATION		2 3 4 8 8	DEBT	RE TAX	3 TAX	\$ 1 9 9 9 9
OPERATING INCOME	TOTAL SALES REVENUE COST OF SALES	RIABLE COST RECT FIXED COS PRECIATION AND C. IN PRODUCT	GROSS PROFIT ON SALES		NUNCTERST ING EXTENSES	NET PROFIT OR (LOSS) BEFORE	NET PROFIT OR (LOSS) AFTER	RETAINED EARNINGS

2017	114.816 114.816 114.816	90 757 38 787 38 787 19 938 32 033	24,058 4	24.058	1 149	22.909	16.036 0.0	16.036
2016	114.816 	90.757 38.787 38.787 38.938 32.033	24.058 	24.058	2.298	21.760	15.232	15.232
2015	114.816	90.757 38.787 38.787 32.033 32.033	24.058	24.058	3,447 3,447 3,447 0,000	20.611 6.183	14.428	14.428

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*** COKE PLANT PROJECT IN VENEZUELA ***
 iNCOME STATEMENTS
- ALT. CASE (DOMESTIC COAL INC.BOYACA) - (US\$, MILLION)

PAGE 3

21.667 22.033 0.0 22,982 0.0 16.087 0.000 53.699 53,699 46.251 60.882 39.069 39.065 14.631 0.0 000 2004 1 **~~** i 22.012 32.033 0.0 0,0 40.218 PAGE 22.982 0.0 17.236 0.000 54,044 0.0 32.425 46.251 54.044 40.218 13.826 2003 000 000 0,0 000 1 54.389 22 033 22 033 25 033 000 22.982 0.0 18.385 0.000 0,0 54.389 41 367 19.403 32.425 13.022 41,367 ----2002 000 0 0 22.701 32.033 0.0 22.982 0.0 19.534 0.000 7.186 54.734 54.734 42.516 42.516 12.218 0.0 000 0.0 000 0.0 2001 000 *** COKE PLANT PROJECT IN VENEZUELA *** FUNDS FLOW STATEMENTS ALT. CASE (DOMESTIC COAL INC.BOYACA) - (US\$, MILLION) 55.136 23.104 32.033 0.0 47.950 22.932 3.852 20.684 0.193 47.710 0.0 7.186 55, 136 -----7.186 0.241 2000 000 000 0.0 54.213 22.180 32.033 3.852 0,0 22,982 9,256 21,833 0,463 0,0 0,0 3,852 58.065 58.065 54 533 3.531 000 00 0 1999 0 0 8.104 32.033 9.256 0.0 0.0 9.256 22.982 22.982 C.0 13.610 0.0 40.137 ******* 63.003 49.393 45.963 17.039 -13.610 -----| | | | | | | 0.0 000 0.0 1998 0.0 0.0 0.0 0.0 0.0 0.0 65.652 328.310 262.648 78,794 183,854 0,0 321.505 257.204 0.944 245.312 10.948 8.166 13.610 257.204 262.648 5,444 0.0 0 0000 0000 1997 a 0 1.180 306.640 13.685 58.493 229.817 0.0 328.310 321.505 1.361 8.166 6.305 0.0 0000 1996 0 0.0 0.236 61.328 2.737 65,662 19.699 45.963 0.0 0.0 0.0 1.361 1.361 0.0 0.0 1995 -----0000 0000 ī PROFIT AFT. TAX, BFR INT, DEPRECIATION AND AMORTIZATION FINANCIAL RESOURCES NON-DEPRECIABLE ASSETS DEPRECIABLE FIXED ASSETS INTEREST DURING CONSTRUCTION REPAYMENT OF LONG TERM DEBT REPAYMENT OF SHORT TERM DEBT INTEREST ON LONG TERM DEBT INTEREST ON SHORT TERM DEBT CASH GENERATED FROM OPERATION FIXED CAPITAL EXPENDITURE CHANGE IN WORKING CAPITAL CASH INCREASE OR (DECREASE) BEGINNING CASH BALANCE ENDING CASH BALANCE SHARE CAPITAL LONG TERM DEBT SHORT TERM DEBT DEBT SERVICES SOURCE OF FUNDS

- USES OF FUNDS

A2

000

0.0

0.0

DIVIDENDS

YEAR

18.220 32.033 0.0 50.252 0.0 4.596 0.000 228,754 50.252 ------27.578 27.578 22.982 22.674 000 0 0 0.0 2014 000 000 N 18.564 32.033 0.0 50.537 28.727 22.982 0.0 5.745 0.000 PAGE 185,819 206,884 206,884 228,754 50.597 21.870 28.727 ----------000 0.0 0 0 0 0 0 0 0.0 0.0 2013 18.909 32.033 0.0 50.942 22.982 0.0 6.895 0.000 ----50.942 29.876 29.876 -----**** -------21.066 ----000 0.0 0.0 0.0 2012 000 000 1 19.254 32.033 0.0 31.025 51.286 22.982 0.0 8.044 0.000 165.557 185.819 51.286 20.261 ----31.025 000 000 2011 0.0 0.0 *** COKE PLANT PROJECT IN VENEZUELA *** FUNDS FLOW STATEMENTS - ALT. CASE (DOMESTIC COAL INC.BOYACA) - (US\$, MILLION) 19.559 32.033 0.0 32.174 32.174 51.631 22.982 0.0 9.193 0.000 146.101 165.557 51 631 ----------------19.457 000 0,0 000 2010 0,0 000 19.943 32.033 0.0 22.982 0.0 10.342 0.000 18.652 127.448 146.101 51.976 33.323 51.976 -----33,323 0.0 000 0.0 0.0 000 2009 000 52.321 20,288 32,033 0.0 . 34.473 11.491 0.000 109.600 127.448 22.982 0.0 52.321 34,473 17.848 0,0 000 0.0 2008 000 0.0 000 20.633 32.033 0.0 52.665 22.982 0.0 12.640 0.000 92,556 109,600 52.665 ----35.622 -----35,622 17.044 ----.......... 0.0 000 0.0 2007 000 0.0 000 53.010 20.978 32.033 0.0 53.010 22.982 0.0 13.789 0.000 76.317 92.556 36.771 16.239 36.771 ----000 000 2006 0 0 0. 0 0. 0 53.355 21.322 32.033 0.0 53.355 000 0.0 60.882 76.317 37.920 ----37.920 22.982 0.0 14.938 0.000 15.435 0,0 2005 000 o 0 PROFIT AFT. TAX, BFR INT. DEPRECIATION AND AMORTIZATION FINANCIAL RESOURCES BEGINNING CASH BALANCE ENDING CASH BALANCE NON-DEPRECIABLE ASSETS DEPRECIABLE FIXED ASSETS INTEREST DURING CONSTRUCTION REPAYMENT OF LONG TERM DEBT REPAYMENT OF SHORT TERM DEBT INTEREST ON LONG TERM DEBT INTEREST ON SHORT TERM DEBT CASH GENERATED FROM OPERATION I USES UN VULLE EXPENDITURE CHANGE IN WORKING CAPITAL CASH INCREASE OR (DECREASE) SHARE CAPITAL LONG TERM DEBT SHORT TERM DEBT

DEBT SERVICES

DIVIDENDS ----------

YEAR

SOURCE OF FUNDS

A2

*** COKE PLANT PROJECT IN VENEZUELA *** FUNDS FLOW STATEMENTS - ALT. CASE (DOMESTIC COAL INC.BOYACA) - (USS, MILLION)

2017 2016 2015

F FUNDS	49.	49.563	49,218
GENERATED FROM OPERATIO	100.0	19.5	49.218
PROFIT AFT. TAX, B DEPRECIATION AND A FINANCIAL RESOURCES	32.7	17.530 32.033 0.0	17.186 32.033 0.0
SHARE CAPITAL LONG TERM DEBT SHORT TERM DEBT	000	0.00	0.00
USES OF F	26.429	25.280	24.131
XED CAPITAL EXPENDIT	0.0	0.0	0.0
NON-DEPRECIABLE ASSETS DEPRECIABLE FIXED ASSETS INTEREST DURING CONSTRUCTION	000	0.00	0.00
CHANGE IN WORKING CAPI	0.0	0.0	0.0
SERVICES	26.	25.280	24.131
REPAYMENT OF INTEREST ON	22.982 0.0 3.447 0.000	22.982 2.098 2.298 2.298 0.000	22.982 0.0 0.149
DIVIDENDS	0.0	0.0	
CASH INCREASE OR (DECREASE)	23.479	24.28	25.087
1 14			

PAGE 3

YEAR

SOURCE OF FUNDS

CASH INCREASE OR (DECREASE)

299.190 324.277

274.907 299.190

251.428 274.907

0.0 9.558 14.476 2.360 613.280 27.370 3.232 22.982 0.0 275.780 0.0 196.986 4.728 24.043 503.708 418.783 643.010 301.994 26 214 275.780 201.714 60.832 503.708 224.228 2004 2.360 613.280 27.370 0.0 9.568 14.476 3,232 22,982 0,0 196,986 539.316 521.110 321.744 298.762 0.0 0.0 196.134 521.110 643.010 324.976 298.762 PAGE 24.043 46.251 450,815 192.195 ----26:214 1 2003 2.360 613.280 27.370 0.0 9.568 14.476 3.232 22.982 0.0 196.986 -5.628 321 744 643.010 191,358 539,316 24.043 32.425 482.848 160.163 347.958 26.214 1 1 1 1 -----2002 344.726 0.0 9.568 14.476 2.360 613.280 27.370 558.327 3.232 22.982 0.0 187.387 196.986 -9.599 514.880 643.010 128.130 370,939 26.214 344.726 558.327 24.043 19.403 ----...... 0.0 2001 *** COKE PLANT PROJECT IN VENEZUELA *** BALANCE SHEET ALT. CASE (COMESTIC COAL INC.BOYACA) - (US\$, MILLION) 2.360 613.280 27.370 367,707 0.0 9.568 14.476 3.232 22.982 0.0 196.986 -12.765 367.707 0.0 643.010 578.142 546.913 184.221 578.142 7.186 96.098 393.921 26.214 24.043 -----------...... 2000 2.360 613.280 27.370 390, 689 0, 0 0.0 9.327 14.476 3.232 22.982 3.852 196, 386 -14, 993 643.010 390,689 602.748 420.755 181.993 602.748 578 945 ----30.066 23.803 64.065 ----0.0 1999 2.360 613.280 27.370 413,671 196.986 2.586 22.382 9.256 413.671 0.0 6.691 12.934 630.603 643.010 182,108 630,603 610.978 448.494 19.625 34.824 -----32.033 ------0.0 1998 2.360 613.280 27.370 0.0 22.982 0.0 436.652 0.0 196.986 0.0 656,620 643.010 643.010 436.652 196.986 656.620 13.610 459.634 22.982 -----0 o 000 1997 ö 000 275.780 0.0 1.416 367.968 16.422 118.192 0.0 275.780 335.806 275.780 393.972 393.972 385,806 118.192 8.166 ----------...... 0. 0 000 0 0.0 000 1996 45.563 70.563 0.236 61.328 2.737 19.699 65,662 0 64.301 64.301 45,363 19,699 65.662 45.963 -----1.361 ----------0.0 0,0 1995 000 000 000 ö 000 0581 LONG TERM DEBT BALANCE OTHER FIXED LIABILITIES LESS: ACC, DEPRECIATION 5 SHARE CAPITAL ACC. RETAINED EARNINGS LIABILITIES & S/H EQUITY ACCOUNT PAYABLE CURRENT PORTION OF SHORT TERM DEBT OPERATING CASH ACCOUNT RECEIVABLE NON-DEPR. ASSETS DEPRECIABLE ASSETS AMORTIZATION -----CURRENT LIABILITIES STOCK HOLDERS EQUITY FIXED LIABILITIES ACC. EXCESS CASH NET FIXED ASSETS CURRENT ASSETS **INVENTORIES** INVESTMENT LIABILITIES **** ASSETS A2 - 16

2.360 613.280 27.370 0.0 9.568 14.476 3.232 22.982 0.0 45,964 0.0 196.986 104.766 24.043 251.428 643.010 301.752 373.929 98.458 26.214 404.417 393.450 383.287 373,929 72.177 544.552 45.964 2014 N 288.128 0.0 9.568 14.476 2.360 613.280 27.370 68.945 0.0 3.232 22.982 0.0 196.986 91,142 PAGE 95.159 ------643.010 383.287 24.043 228.754 512.520 26.214 68.945 130.490 2013 0.0 9.568 14.476 2.360 613.280 27.370 3.232 22.982 0.0 91.927 275,309 196.986 78.323 206.884 480.488 393,450 162.523 643.010 26.214 91.927 24.043 118 141 2012 2.360 613.280 27.370 0,0 9,50 14.476 8 3.232 22.982 0.0 114.909 263.295 196.986 66.308 185.819 643.010 194.555 448.455 141.122 404.417 24.043 26.214 114.909 ----2011 ALT. CASE (DOMESTIC COAL INC. BOYACA) - (USS, MILLION) 2.360 613.280 27.370 137 890 0 0 0.0 9.568 14.476 3.232 22.982 0.0 252.084 196.986 55.098 428.764 416.188 643.010 26.214 137,890 416.188 226.588 416.423 24.043 165.557 164.104 111111111 ----------2010 2.360 613.280 27.370 0 0 9 568 868 868 3.232 22.982 0.0 196.986 44.692 26.214 160.872 0.0 241.678 146.101 258.620 643.010 384.390 187.086 428,764 24.043 160.872 ----2009 *** COKE PLANT PROJECT IN VENEZUELA *** Balance Sheet 1 0.0 9.568 14.476 2.360 613.280 27.370 3.232 22.982 0.0 24.043 183.854 0.0 196.986 35.091 442.144 127.448 290,653 643.010 352.358 210.068 183.854 232.077 442.144 26.214 ----..... 2008 2.360 613.280 27.370 0.0 9.568 14.476 233.049 206.835 0.0 3.232 22.982 0.0 196, 986 26, 293 643.010 223.279 456.329 322.685 320.325 206,835 455.329 24.043 109.600 26.214 -----------2007 0.0 9.568 14.476 2.360 613.280 27.370 229.817 0.0 256.031 3.232 22.982 0.0 215.286 196.986 18.300 471.317 471.317 354.718 643.010 24,043 92.556 288.293 26.214 229,817 ---------------2006 487.111 0.0 9.568 14.476 386.750 2 360 613 280 27 370 279.013 196.986 11.112 3.232 22.982 0.0 208.098 24.043 643.010 256.260 487.111 76.317 26.214 2005 ï 1 DEBT LESS: ACC. DEPRECIATION LONG TERM DEBT BALANCE OTHER FIXED LIABILITIES ۲/٦ SHARE CAPITAL ACC. RETAINED EARNINGS LIABILITIES & S/H EQUITY OPERATING CASH ACCOUNT RECEIVABLE INVENTORIES NON-DEPR. ASSETS DEPRECIABLE ASSETS AMORTIZATION ACCOUNT PAYABLE CURRENT PORTION OF SHORT TERM DEBT CURRENT LIABILITIES STOCK HOLDERS EQUITY FIXED LIABILITIES ACC. EXCESS CASH NET FIXED ASSETS CURRENT ASSETS **NVESTMENT** LIABILITIES -----ASSETS

> A2 - 17

*** COKE PLANT PROJECT IN VENEZUELA *** BALANCE SHEET - ALT. CASE (DOMESTIC COAL INC.BOYACA) - (US\$, MILLION)

2017 2016 2015

ASSETS

24.043

11111

OPERATING CASH ACCOUNT RECEIVABLE INVENTORIES

CURRENT ASSETS

ACC. EXCESS CASH NET FIXED ASSETS

1

LESS: ACC. DEPRECIATION

NON-DEPR. ASSETS DEPRECIABLE ASSETS AMORTIZATION

A2 - 18

INJESTMENT

0.0 9.568 14,476 24.043 2.360 613.280 27.370 2.360 643,010 643.010 643.010 3.232 299.190 324.277 576,585 608,618 640,650 2.360 613.280 27.370 0.0 9.568 14.476 34,393 26.214 2.360 613.280 27.370 0.0 9.568 14.476 274.907 24.043 66.425

3, 232 22, 982 0, 0 26.214 49,195 26.214 3.232 22.982 0.0 ACCOUNT PAYABLE CURRENT PORTION OF L/T DEBT SHORT TERM DEBT

CURRENT LIABILITIES

LIABILITIES

3.232 3.232 0.0 0.0 0.000 0.000 0.000 0.000 22.982 22.982

195.986

STOCK HOLDERS EQUITY

FIXED LIABILITIES

LONG TERM DEBT BALANCE OTHER FIXED LIABILITIES

LIABILITIES & S/H EQUITY

365.375 357,626 350,680

ო PAGE

*** COKE PLANT PROJECT IN VENEZUELA ***
 LONG TERM DEBT
 ALT. CASE (DOMESTIC COAL INC.BOYACA) - (US\$, MILLION)

0.0

700.940

241.308

159.634

TOTAL

•--

*** COKE PLANT PROJECT IN VENEZUELA *** PROFITABILITY AND FINANCIAL INDICATORS - ALT. CASE (DOMESTIC COAL INC, BOYACA) - (USS, MILLION)

(11)* CASH B.E.P. CAPACITY UTILIZE (PCT)	ພ≻≻໙໙໙໙໙໙໙໙໙ຏຏຏຏຏຏຏຏຏ −ຏ−ຆຑ≻໐ຨຆഗ໐ຒຌຬຬຏ4ຒ-ຒຨ ໐ຉຆຌຎຎຒ໐ຩ4⊷ຎຏຒ໐ຩ4−∞໙ຒ	
(10) * CASH B.E.P. SALES PRICE (PRICE	177111111111000000000 1700011001110000000000	
(9)* PROF1T B.E.P. CAPACITY UT1L1ZE (PCT)	、 、 、 、 、 、 、 、 、 、 、 、 、 、	
(8) L/T DEBT -10- S/H EQUITY	66 67 66 <td< td=""><td>·</td></td<>	·
<pre><7) DEBT SERVICE RATIO</pre>	0	
(6) QUICK RATIO	 C C C C C C C C C C C C C C C C C C C	
(5) CURRENT RATIO	00000000000000000000000000000000000000	
(4) AFT TAX PROFIT -TO- S/CAPITAL S/CAPITAL (PCT)	II ≻O⊷⊷ И И И И И И И И И И И И И И И И И И	
(3) BFR TAX PROFIT -TO- INVESTMENT (PCT)	1 000000000000000000000000000000000000	
(2) AFT TAX PROFIT -TO- S/H EQUITY (PCT)	ו סָרָש אַרָש אַרָש אַרָש אַרָש אַרָש אַרַש אַרַש אָרָש אַרָש אַרַש אַרַש אַרַש אַרַש אַרַש אַרַש אַרַש אַרַש אַר אָרָש אַרַש אַרַש אַרַש אַרַש אַרַש אַרַש אַרַש	
(1) AFT TAX PROF1T -TO- SALES REV (PCT)	1 0 0 0 0 0 0 0 0 0 0 0 0 0	
YEAR	A2 - 20	

(AVERAGE1) : SUM OF ANNUAL FIGURES OF PERCENTAGE AND RATIO IS DIVIDED BY NO. OF YEARS(SIMPLE AVERAGE) (AVERAGE2) : AVERAGE FIGURES ARE CALCULATED BY ACTUAL VALUES ACCUMULATED OVER THE PROJECT LIFE(WEIGHTED AVERAGE) * NOTE FOR (9) (10) (1) * NOTE TORE (9) (10) (1) WHEN THERE ARE TYO OR MORE PRODUCTS, AND DURING THE YEARS WHEN ALL OF PRODUCTS ARE NOT PRODUCED AT THE SAME RATE OF CAPACITY UTILIZATION, ABOVE BREAK-EVEN-POINTS CANNOT GIVE CORRECT FIGURES.

	<pre>4) BFR-TAX (5) AFT-TAX NET iN-FLOW NET iN-FLOW (2)-(1) (4)-(3)</pre>	
(NO I T	(4) BFR-TAX NET IN-FLOW (2)-(1)	4 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
c* PRICE) (USS, MILLION)	I NCOME TAX	00000000000000000000000000000000000000
₹ ₩ ₩ ₩	(e)	•
IN VENEZUELA *** (IN '93 FIXED PR - INC, BOYACA) -	(2) GROSS CASH IN-FLOW	0000 00000 0000 0000 0000 0000 0000 0000 0000 00000
COKE PLANT PROJECT CIAL RATE OF RETURN CASE (DOMESTIC COAL	DEPRECIATN (2)	6 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
*** COKE PLANT PROJECT IN VENEZUELA *** FINANCIAL RATE OF RETURN (IN "93 FIXED PRICE) ALT. CASE (DOMESTIC COAL INC BOYACA) - (US3	OPERATING PROFIT	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
ч. I	<pre><1> GROSS CAPITAL EXPENDTR</pre>	2867 2877 2877 2875 2875 2875 2875 2875 287
	CHANGE IN WORKING CAPITAL	000, 000, 000, 00, 00, 00, 00, 00, 00,
	F I XED CAPITAL EXPEND.	61.556 245.256 245.256 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.
	YEAR	S S S S S S S S S S S S S S S S S S S

INTERNAL RATE OF RETURN

5.54 PER CENT ON (5) AFT-TAX NET IN-FLOW (4)-(3) 4.95 PER CENT ON (4) BFR-TAX NET IN-FLOW (2)-(1)

	ACC.NET		0.0	0.0	0.0	16.402	62.953	113.542	165.279	218.166	272.201	327.386	383.719	441.202	499.834	559.615	620.545	682.625	745.853	810.230	875.757	942.432	1010.257	1079.231	1149.354	
LE I ONS	(3) NET IN-FLOW	(1) - (2)	0.0	0.0	0.0	16.402	46.551	50,588	51.737	52,887	54.035	55.185	56,334	57.483	58.632	59.781	60,930	62,079	63.228	64.377	65.526	56, 676	67.825	68.974	70.123	1149.352
FOREIGN CURRENCY EARNINGS (IN '93 FIXED PRICE) ALT. CASE (DOMESTIC COAL INC. BOYACA) - (USS, MILLION)	ACC. C	-	0,0	0.0	0.0	63,898	129.274	193,502	256.580	318,509	379.289	438.920	497.401	554.734	610.918	665.952	719.838	772.574	824,162	874.600	923. 885	972.029	1019,020	1064.862	1109.555	. 1
GS (IN - 93 FI L INC. BOYACA)	(2) TOTAL	-	0.0	0.0	0.0	63.898	65.376	64.227	63.078	61.929	60.780	59.631	58.482	57.333	56,184	55.035	53.885	52.736	51,587	50.438	49.289	48.140	46.331	45.842	44.693	1109.553
ZENCY EARNIN	LN	L/T	0.0	0.0	0.0	22.982	22.982	22.932	22.982	22,982	22.982	22.982	22.982	22.982	22.982	22.982	22,982	22.982	22,982	22.982	22.982	22.982	22,982	22.982	22.982	459.634
FOREIGN CURP	INTEREST ON	171	0.0	0.0	0.0	22.982	21.833	20.684	19.534	18.385	17.236	16,087	14.538	13.789	12.640	11.491	10.342	9,193	8.044	6,895	5.745	4,596	3 447	2.298	1.149	241,308
I	IMPORT COAL & MATERIALS		0.0	0.0	0	17.935	20.562	20.562	20.562	20.562	20 562	20.562	20.562	20.562	20.562	20.562	20.552	20.562	20.562	20.562	20.562	20,562	20.562	20 562	20 562	408.613
	ACC.		0.0	0.0	0,0	80.300	192.228	307.043	421.859	536.674	651,490	766.306	881.121	995,937	1110.752	1225.568	1340.384	1455.199	1570.015	1684.831	1739.646	1914,462	2029.277	2144.093	2258,908	
	(1) IN-FLOW FROM	SALES	0.0	0.0	0.0	80.300	111.928	114.816	114.816	114.816	114.816	114.816	114.816	114.815	114.816	114.816	114.816	114.816	114.816	114.816	114.816	114.816	14.816	114.816	114.816	2258,906
	1)	YEAR	1995	1996	1997	1998	1999	2000	2001	2002	2003	2004	2005	2006	2007	2008	2009	, 2010	2011	2012	2013	2014	2015	2016	2017	

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*** COKE PLANT PROJECT IN VENEZUELA *** COREIGN CURRENCY EARNINGS (IN °93 FIXED PRICE) ALT. CASE (DOMESTIC COAL INC, BOYACA) - (USS. N

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	<pre>(5) AFT-TAX NET IN-FLOW</pre>	$\begin{array}{c} 1 \\ 1 \\ 2 \\ 2 \\ 2 \\ 2 \\ 2 \\ 2 \\ 2 \\ 2 \\$	547.518
WILL ION	(4) BFR-TAX NET IN-FLOW (2)-(1)	222 222 222 222 222 222 222 222	241.018
IN VENEZUELA *** (IN '93 FIXED PRICE) INC BOYACA) - (USS)	I NCOME TAX		0.0
	(2) GROSS (3) CASH IN-FLOW	00000000000000000000000000000000000000	
*** COKE PLANT PROJECT CONOMIC RATE OF RETURN LT. CASE (DOMESTIC COAL	DEPRECIATN	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	5
*** COKE PLANT PROJECT ECONOMIC RATE OF RETURN ALT. CASE (DOMESTIC COAL	OPERAT I NG PROF I T	288,2995 295 295 295 295 295 295 295 295 295	n - t
(ECONOMIC)	(1) GROSS CAPITAL EXPENDTR	222.60 222.60 23.51 23.52	n t
CEC.	CHANGE IN WORKING)
	FIXED CAPITAL EXPEND.	и и о и о и о и о и о и о и о и о и о и	r
	YEAR	1999 999 999 999 999 900 900 90 90 90 90	

INTERNAL RATE OF RETURN

ON (4) BFR-TAX NET IN-FLOW (2)-(1) 6.27 PER CENT ON (5) AFT-TAX NET IN-FLOW (4)-(3) 6.27 PER CENT

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Annex-1 Utilization of Guasare Coal for Coke

Utilization of Guasare Coal for Coke

1. Forward

The study on Guasare coal produced from Zulia state is not the part of this feasibility study. However, strong requests from Corpozulia, one of counterpart of this study, the team studied Guasare coal using the sample provided from them on July 1993 and the result of the study is included in the main report. In here possible blending ratio of Guasare coal are shown using new data.

2. Property of New Guasare Coal

It was informed during second field survey that the coal sample provided from Corpozulia on July 1993 was weathered one. Therefore new sample were taken from the seam no.4 in the Guasare coal mine together with counterpart. This sample was analyzed at INZIT-CICASI for total sulfur content, dilatation measured by dilatometer, maximum fluidity by Gieseler plastometer and maceral analysis. In order to differentiate and clarify between new and old sample it is defined for convenience as;

Weathered coal..... The coal sample provided at July 1993 New coal Coal sample collected and analyzed at Feb.1994

Table 1 show the comparison of the property value of the two.

Sample	Ash	Volatile	Total Sulfur	Dilatation	Fluidity	SI	CBI	CSR
	(%, d.)	(%, d.)	(%, d.)	(%)	(logD)			
lew Guasare Coal	2.9	39.8	0.55	32	1.99	2.7	0,5	30 *
Veathered Guasare Coal	1.0	39.2	0.41	0	0.48	2.7	0.6	25 *

Table 1 PROPERTY VALUES OF NEW GUASARE COAL

Note: * Estimated value

The new Guasarc coal contains 39.8(%,d) volatile matters which is more or less the same as that of the weathered coal, and is classified as high-volatile coal.Coking capacity

indicate by 32% dilatation and fluidity of 1.99(LogDDPM), compared to 0% and 0.48(LogDDPM), respectively, for the weathered coal. From those data, the new Guasare coal is classified as high-volatile, weak coking coal. CSR in the Table is estimated at 30 from the result of maceral analysis.

3. Basic Conditions in Order to Estimate the Coke Quality

3.1 Basic Data

In order to determine the blending amounts with different coal, the data tabulated in Table-2 are used. For Guasare coal it is used the new data and others are quoted from main report.

Name	Ash	Volatile	Total	Total	Fluidity	SI	CBI	CSR
	Content	Matter	Sulfur	Dilatation				
	(%, d.)	(%, d.)	(%, d.)	(%)	(logD)	-		
FNO	7.6	23.2	0.85	124	2.96	5.06	2.39	70
LAS	3.9	37.9	0.59	203	4.10	2.86	0.85	41
HAT	1.7	31.8	1.15	310	4.31	3.75	0.78	45*
Boyaca	7.5	21.4	0.95	41	1.04	6.91	4.91	70
Pinnacle	5.6	16.7	0.76	42	0.60	7.28	5.66	47
Blue Cr.	8.9	25.4	0.85	239	3.60	4,60	0.63	60
Saraji	10.5	18.8	0.57	62	1.70	6.93	3.58	74
New-GUA	2.9	39.8	0.55	32	1.99	2.77	0.59	30*

Table 2 PROPERTY VALUES OF COALS USED FOR ESTIMATION OF COKE QUALITY

* Estimated value

3.2 Target Quality Requirement

The target quality of the coke are set at the level sufficient to export in the international market. Table- 3 are those required items and qualitative value. However each quality of the coking coal is varies and quality of blending coal is different depending on the selection of the coal and operation process, therefore required property of the blending coal, and quality of coke are set as shown in Table-4.

Table 3 TARGET QUALITY OF COKE

Standard Quality	
Moisture (%)	4 - 5
Ash (%)	10.5 (Max.)
Volatile matters (%, d.)	1.0 (Max.)
Fixed carbon (%, d.)	88.5 (Min.)
Total sulfur (%, d.)	0.8 (Max)
TI ₂₅ 59 (Min)	
Coke breeze ratio(-25mm)(%)	5.0 (Max.)
Others important characteristic values	arna maanaan maaliyyyi sijiraaso maaraan amaalaa a
CSR	53 - 60
P (%, d.)	0.04
K20 + Na20 (%, d.)	0.2 - 0.25
Mean size (inch)	2

Table 4 REQUIRED PROPERTY OF THE BLENDING COAL AND TARGET QUALITY OF COKE

Ash (%, d)	: 10.3	T125	: 61
Total Sulfur (%,d.)	: 0.76	CSR	: 58

3.3 The Property of Blending Coal and Estimation of Quality of Coke.

The property of blending coal and quality of coke is estimated by Mitsui Mining Co.s own method.

4. Consideration of Coal Blending Conditions for Maximum Use of New Guasare Coal

To determine the coal blending ratio to allow the maximum use of the Guasare coal the following three cases are considered:

 Replace U.S. coal by Guasare coal as much as possible.(It is found that blending ration of Las 27%, Boyaca 5%, FNO 5%, US coal 65% satisfy all conditions and coke quality was verified by box test and SCO test. Basic consideration of this blending ratio was based on the coal production capacity from Tachira state, and annual coke production is one million ton per year.

- (2) Blending ratio proposed by the counterpart
- (3) Without consideration of availability from Tachira state, but use maximum Guasare coal according to the quality of raw coal

4.1 Replacement of US Coal by Guasare Coal

Since Guasarc coal characterize the high volatile character it is most favorably exchanged with Blue Creek which is the coal with medium volatile matter.

As shown in the Table-5 it is found that maximum blending ration of Guasare coal is at 10% and this is the limit to satisfy CSR and TI25 requirement.

The reason to be able to increase the blending ration from 5% to 10% is because of the increase of capacity of coking. It is considered that only 10% of blending is caused by Guasare coal which has high volatile content(39.8%,d),while CSR is low(30)and coking capacity measured by total dilatation is low(32%)

	Coal Blend No.	1	2	3	- 4	5	6	7
Ratio of (%)	FNO (Venezuela)	5	5	5	5	5	5	5
	LAS (Venezuela)	27	27	27	27	27	27	27
	Boyaca (Colombia)	3	3	3	3	3	3	3
Blending Coal	Pinnacle (U.S.)	25	25	25	25	25	25	25
Ble	Blue Creek (U.S.)	40	35	30	25	20	15	10
	New-Guasare (Venezuela)	0	5	10	15	20	25	30
	Ash (%, d.)	6.6	6.3	6.0	5.7	5.4	5.1	4.8
36	Volatile Matter (%, d.)	27.0	27.1	27.8	28.6	29.3	30.0	30.7
Char	Total Sulfur (%, d.)	0.76	0.75	0.73	0.72	0.70	0.69	0.67
Coal	Total Dilation (%)	168	158	148	137	127	117	106
Properties of Coal Charge	Max. Fluidity (log DDPM)	2.88	2.80	2.72	2.63	2.55	2.47	2.39
operti	SI	4.89	4.80	4.71	4.62	4.53	4.44	4.34
Pn	СВІ	2.16	2.16	2.16	2.16	2.16	2.15	2.15
	ΣCSR	52	51	49	48	47	45	44
~	Ash (%, d.)	8.9	8.7	8.4	8.2	8.0	7.7	7.5
Coke Quality	Total Sulfur (%, d.)	0.66	0.65	0.64	0.63	0.62	0.60	0.59
oke (TI25	63	63	62	62	61	60	59
O O	CSR	59	.58	. 58	57	56	55	53

Table 5 CONDITION OF BLENDING LIMIT FOR GUASARE COAL(COKE PRODUCTION - 1 MILLION TONS PER YEAR)

TI25	64 62 60 58						Target	(61)
CSR	58 56 54 52 50				•	, , , , , , , , , , ,	Target	(58)
FNO-	-LC30	5	5	5	5	5	5	5
LAS-	-LC25	27	27	27	27	27	27	27
BOYACA		3	3	3	3	3	3	. 3
PINNACLE		25	25	25	25	25	25	25
BLUE	E. C.	40	35	30	25	20	15	10
GUA:	SARE	0	5	10	15	20	25	30
Na	ime			Blei	nding ratio	(%)		

Weathered Guasare Coal

Fig.-1 RELATIONSHIP BETWEEN CONSUMPTION OF GUASARE COAL AND COKE QUALITY

4.2 Coal Blending Proportions for 15% Blending of the New Guasare Coal (Proposed by the Venezuela Counterpart)

 Coal blending conditions based on present production volumes Blending proportions required to use the new Guasare coal at a proportion proposed by the Venezuelan counterpart with the Fax dated March 8, 1994 are 32% Tachira coal and 15% Guasare coal, as shown in Table 7.

Table 7 COAL BLENDING PROPORTIONS FOR 15% BLENDING OF THE NEW GUASARE COAL (PROPOSED BY THE VENEZUELA COUNTERPART)

Coal Type	Blending Ratio (%)
Tachira	32
Zulia	15
Colombia	3
U.S.	50

Venezuela's proposal does not specify brands for each coal type. Since coke quality cannot be estimated without knowing specific brands, brands of Tachira and U.S. coals and their blending proportions have been determined by the following method.

First of all, blending proportions of Tachira coals are estimated from potential production in the state, namely FNO 5% and LAS 27%. Then, those of U.S. coal have been determined from the viewpoint of securing the required CSR level in produced coke, namely Pinnacle 10% and Blue Creek 40%.

Table 8 shows estimated blending proportions by brand, on the basis of Venezuela's proposal. From these blending proportions, property values of coal blend and coke are estimated as shown in Table 9.

From Table 9, the coal blend proposed by the Venezuelan side has sufficient coking capacity (dilatation of 167%), but is not sufficient in rank of coalification, judging from volatile content 31.84 (%, d.a.f.) and the average reflectivity 1.09 (%, oil).

As shown in the column showing coke qualities in Table 9, therefore, TI_{25} meets the

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target level (61) whereas CSR is 56, slightly short of 58. It is concluded that the coal blend cannot produce blast-furnace coke exportable to the international market.

Bland	Blending Ratio (%)
FNO	5
LAS	27
Boyaca	3
Pinnacle	10
Blue Creek	40
Guasare	15

Table 8BLENDING PROPORTIONS BY BRAND,AS PROPOSED BY THE VENEZUELAN COUNTERPART

Table 9 ESTIMATED QUALITIES BASED ON BLENDING PROPORTIONS PROPOSED BY THE VENEZUELAN COUNTERPART

Estimated property val	ues of coal blend	Estimated property values of coke		
Ash	6.22 (%,d.)	Ash	9.00 (%, d.)	
Volatile matter	31.84 (%, d.a.f.)	Sulfur	0.64 (%, d.)	
Sulfur	0.73 (%, d.)	TI ₂₅	61	
Average reflectivity	1.09 (%, oil)	CSR	56	
Dilatation	167 (%)			

2) Replacement of HAT coal with LAS coal

The result of simulation to estimate coke quality based on the above blending proportions reveals that the target quality levels have been achieved for TI_{25} , but not for CSR. A major reason for this seems to come from the rank of coalification is low for the coal brand.

To maximize the rank of coalification while the blending ratio of the new Guasarc coal is held at 15%, the LAS coal with high volatility has to be eliminated and replaced with Boyaca or FNO coal that shows low volatile content and high CSR.

However, production of Boyaca and FNO coals is limited, and thus an attempt is made to use HAT coal which seems to show a higher rank of coalification than LAS coal.

In this alternative, the blending ratio of HAT coal is assumed to be 27% to totally replace LAS coal, as shown in Table 10. This way, the rank of coalification for the coal brand improves apparently: as shown in Table 11, volatile content is 29.88 (%, d.a.f.) and the average reflectivity 1.14 (%, oil), compared to 31.84 (%, d.a.f.) and 1.09 (%, d.) for the 27% LAS blend shown in Table 9.

However, total sulfur content in the coal brand amounts to 0.88 (%, d.), up 0.15 (%, d.) from 0.73 (%, d.) for the 27% LAS blend, because sulfur content of HAT coal is 1.15 (%, d.) in Table 2.

As for estimated coke qualities, while ash content decreases slightly to 8.02 (%, d.), sulfur content is 0.76 (%, d.), closer to the upper limit.

Target levels for TI₂₅ and CSR are satisfied, 62 and 58 respectively.

The above analysis indicates that, by replacing LAS coal with HAT coal in whole amount, the rank of coalification for the coal brand rises to satisfy quality requirements for coke, although total sulfur barely clears the upper limit.

Bland	Blending Ratio (%)	
FNO	5	
НАТ	27	
Boyaca	3	
Pinnacle	10	
Blue Crcek	40	
Guasare	15	

Table 10 BLENDING PROPORTIONS WHEN LAS COAL IS REPLACED WITH HAT COAL

Table 11 ESTIMATED QUALITIES B	ASED ON BLENDING PROPORTIONS PROPOSED
BY THE VENEZUELAN COU	JNTERPART (REPLACEMENT OF LAS COAL
WITH HAT COAL)	

Estimated property val	lues of coal blend	Estimated property values of coke		
Ash	5.62 (%,d.)	Ash	8.02 (%, d.)	
Volatile matter	29.88 (%, d.a.f.)	Sulfur	0.76 (%, d.)	
Sulfur	0.88 (%, d.)	TI ₂₅	62	
Average reflectivity	1.14 (%, oil)	CSR	. 58	
Dilatation	196 (%)			

4.3 Blending Limits for Guasare Coal

To use the new Guasare coal as much as possible, it is necessary to blend coal that can compensate for high volatility, low CSR, and low coking capacity which Guasare coal has.

Among coals produced in Venezuela and Colombia, 2 brands are considered to serve the purpose; Boyaca coal which is effective in improving CSR and controlling volatile matters and FNO coal which can be used to reduce volatility and supplement coking capacity.

If Boyaca coal with low coking capacity is used to reduce volatility, coking capacity of the resultant coal blend decreases. As seen in Table 2, the imported coal, Blue Creek, can compensate for coking capacity without scarifying CSR.

Thus, the maximum use of Guasare coal is estimated when four brands, Boyaca, FNO, Blue Creek, and Guasare are blended.

Note that volatile content indicates that FNO and Blue Creek are classified as medium-volatile coal, namely 23.2(%, d.) and 25.4(%, d.). On the other hand, they show highly opposite data in CSR and coking capacity. While FNO coal shows high CSR and low coking capacity, Blue Creek shows low CSR and high coking capacity. To complement deficiency in CSR and coking capacity, the two medium-volatile brands are blended by the ratio of 1:1.

The maximum blending ratio for the new Guasare coal is estimated by using a triangular graph which consisting of three elements, the Boyaca coal having low volatile content and high CSR, a mixture of FNO and Blue Creek which are medium-volatile, high coking, and high CSR coals, and the new Guasare coal.

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First of all, the optimum range of each property value is determined on the graph, which is overlaid to estimate proportions of the three raw coals to satisfy all the quality requirements.

Estimated qualities of the coal blend and coke are shown on the triangular graphs in Figures 2 through 5.

Fig.2 shows the relationship between blending proportions of the three raw coals, and distribution of volatile content in the coal blend. Since the optimum volatile content level ranges between 26 and 30(%, d.a.f.), the optimum range of blending becomes the optimum VM zone.

Fig.3 shows the blending proportions and distribution of total dilatation. Since dilatation of the coal blend needs to be over 85%, the optimum range of blending determined from dilatation becomes the optimum TD zone.

Fig.4 shows the blending proportions and distribution of TI_{25} which has to be at least 61. Thus, the optimum range of blending determined from TI_{25} becomes the optimum TI_{25} zone.

Fig.5 shows the blending proportions and distribution of CSR. Since CSR must be 58 or over, the optimum range of blending from CSR becomes the optimum CSR zone.

Finally, Fig.6 synthesizes Figures 2 through 5, and blending proportions satisfying all the requirements for volatile content, total dilatation, TI25 and CSR represent the optimum blending zone.

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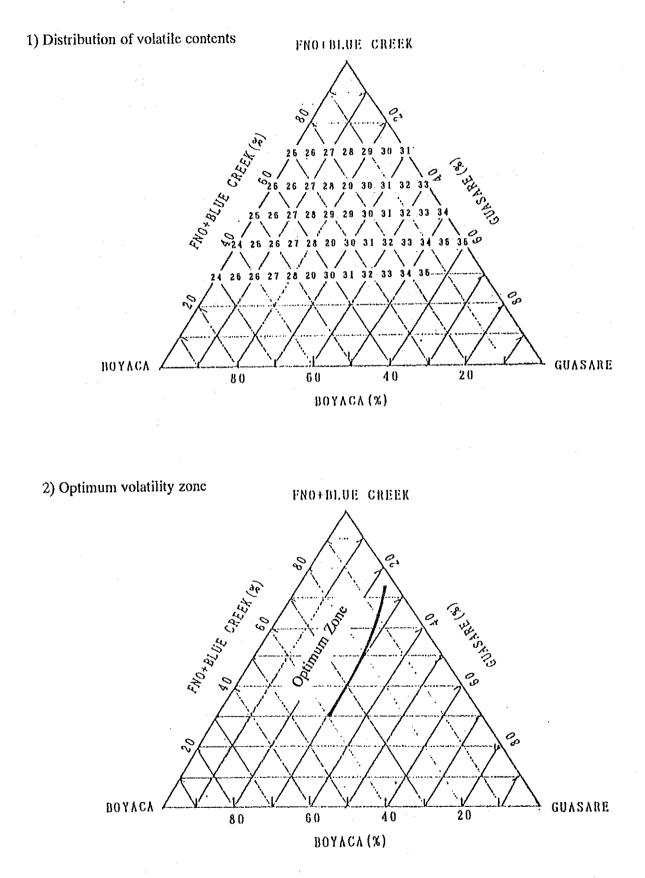
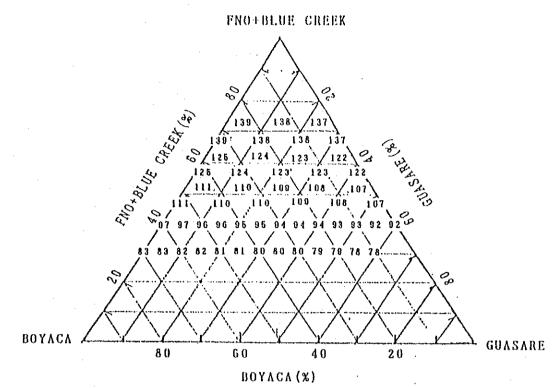


Fig.2 DISTRIBUTION OF VOLATILE CONTENTS FOR DIFFERENT COAL BLENDS ON THE TRIANGULAR GRAPH AND OPTIMUM VOLATILITY ZONE

1) Distribution of total dilation



2) Optimum dilatation zone

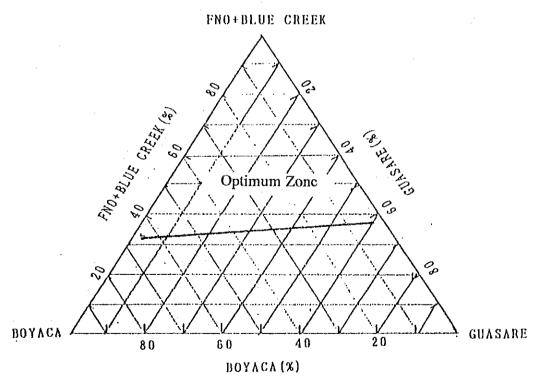


Fig.3 DISTRIBUTION OF TOTAL DILATATION FOR COAL BLENDS ON THE TRIANGULAR GRAPH AND OPTIMUM DILATATION ZONE

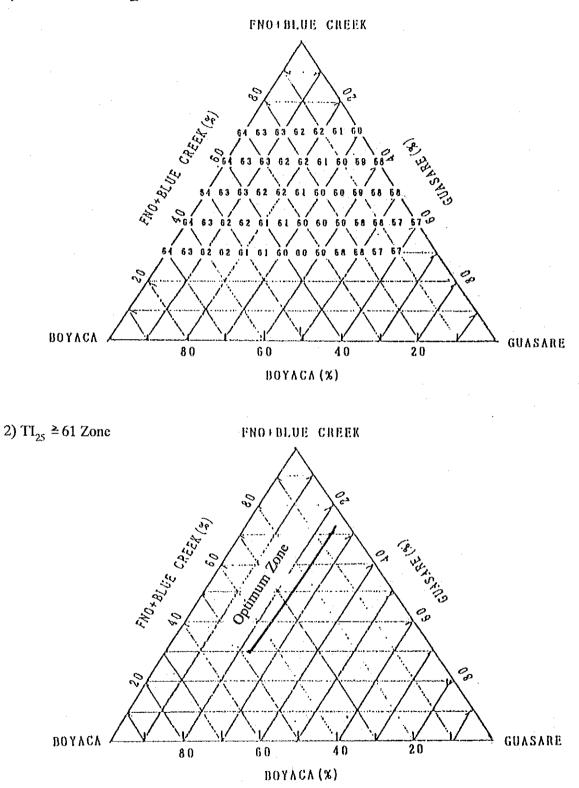


Fig.4 DISTRIBUTION OF TI₂₅ FOR DIFFERENT COAL BLENDS ON THE TRIANGULAR GRAPH AND TI₂₅ $\stackrel{>}{=}$ 61 ZONE

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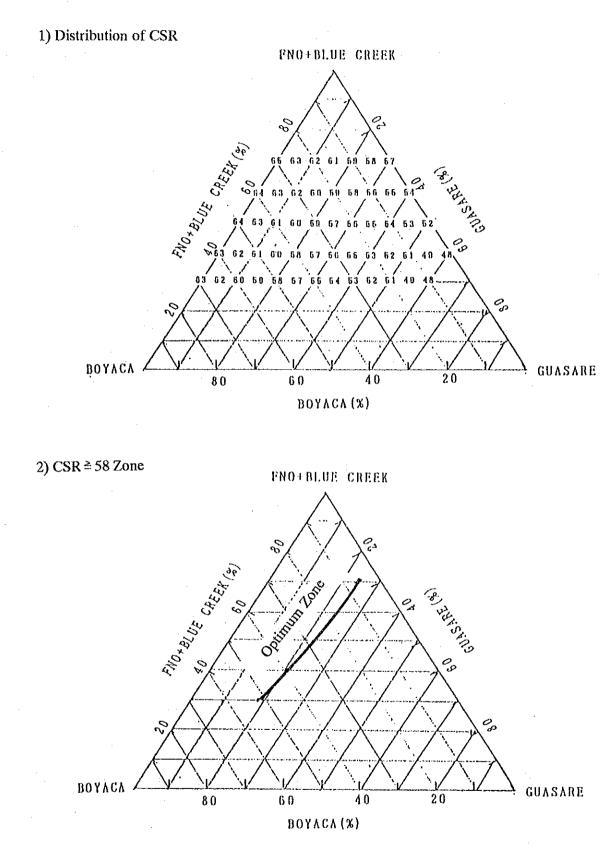
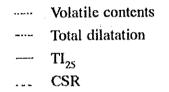
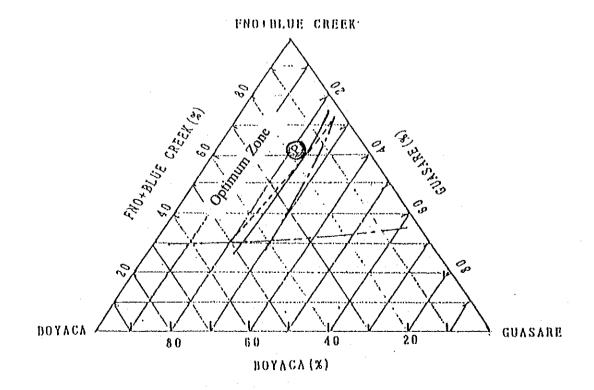
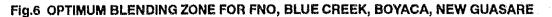


Fig.5 DISTRIBUTION OF CSR FOR DIFFERENT COAL BLENDS ON THE TRIANGULAR GRAPH AND CSR ≥ 58 ZONE

Within the optimum blending zone, the largest amount of blending for the new Guasare coal is at point P and is 23%. The blending proportion, the estimated property values of the coal blend, and estimated coke quality are summarized in Table 6.







Blending proportions	
FNO	29 (%)
Blue Creek	29 (%)
Воуаса	19 (%)
Guasare	23 (%)
Property values of coal blend	
Ash	6.85 (%, d.)
Volatile	29.33 (%, d.a.f.)
Sulfur	0.80 (%, d.)
Dilatation	120 (%)
Fluidity	2.56 (logDDPM)
Average reflectivity	1.189 (%, oil)
Coke quality	
Ash	9.31 (%, d.)
Sulfur	0.70 (%, d.)
TI ₂₅	61
CSR	58

Table 6 ESTIMATED BLENDING PROPORTIONS, AND QUALITIES OF COAL BLEND AND COKE WHEN THE MAXIMUM AMOUNT OF THE NEW GUASARE COAL IS USED

In this case, ash content is 6.85 (%, d.), volatile content 29.33 (%, d.a.f.), average reflectivity 1.189 (%, oil), and dilatation 120(%). These values indicate that the coal blend is suitable for making blast-furnace coke, as measured by the rank of coalification and coking capacity.

As for quality of coke produced, ash content is 9.31 (%, d.), total sulfur 0.70 (%, d.), TI_{25} 61, and CSR 58.

Thus, the maximum blending ratio of the new Guasare coal when requirements related to the use of raw coal are neglected is estimated to be 23%.

5. Conclusion

- 1) The new Guasare coal is rated as high-volatile, light coking coal from its property values; ash content 2.9 (%, d.), volatile content 39.8 (%, d.), total sulfur 0.55 (%, d.) dilatation 32 (%), and Gieseler plastometer's maximum fluidity 1.99(logDDPM).
- 2) The upper limit for blending of the new Guasare coal is estimated as follows:
 (1) 10% in basic proportion
 (2) 23% when production the FNO coal and the Boyaca coal is neglected
- 3) Blending proportions for the 15% blending of the new Guasare coal, proposed by the Venezuelan side, are as follows:

FNO	:	5 %
НАТ	:	27 %
Boyaca	:	3%
Low-volatile U.S.	:	10 %
Medium-volatile U	.S.:	40 %
Guasare	:	15 %

6. Proposal of Coal Blending

As shown in Table 12, if production of Tachira and Colombian coals are taken into account and Zulia coal (Guasare coal) is blended by 15%, CSR falls below the target level of 58. Thus, the maximum allowable blending ratio of Zulia coal is limited to 10% as shown in Table-5. On the other hand, if the HAT deposit will be commercially developed to replace LAS coal, the blending ratio of Zulia coals are produced in large quantities, the blending ratio can be raised to 23%, as shown in Case-3.

		FIV Proposal	Case Study			
			-	Case-1	Case-2	Case-3
			Based on the Production Capacity	Based on the Production Capacity	1.AS'-> HAT	Based on the Quality of Tachir Coal
	Tachira	FNO	5	5	5	2
		LAS	. 27	27		
%) (%		НАТ			27	
Blending Ratio (%)	Zulia	New-Guasare	15	10	15	2
	Colombia	Boyaca	3	3	3	1
Ble	U.S.A.	Pinnacle	10	25	10	
		Blue Creek	40	30	40	2
		Total	100	100	100	10
		Ash (%, d.)	9.00	8.40	8.02	9.3
Coke Quality		T-S (%, d.)	0.64	0.64	0.76	0.70
		TI25	61	62	62	6
		CSR	56	58	58	58

Table 12 ESTIMATED COKE QUALITIES

7. Coke and Coal Chemical Production Plan

Based on the result of the simulation on the effective use of Guasare coal, production volumes and product mix forming the basis of blending design are summarized in Table 13. Also, basic assumptions to calculate target production volumes, such as property values of coal charge and product yields, are summarized in Table 14. Note that material balance remains unchanged even if the blending ratio of Guasare coal is changed.

Item	Production/Am	Remarks	
	Daily	Annually	
Raw coal (wet)	4,070 ton	$1,485 \times 10^3$ ton	
Coal charge (dry)	3,700 ton	$1,351 \times 10^3$ ton	
Coke in total	2,740 ton	1,000 x 10 ton	
Lump coke	2,330 ton	850×10^{3} ton	
Coke breeze	410 ton	150 x 10 [°] ton	-25mm or less
COG	1,241 x 10 ³ Nm ³	$453 \times 10^6 \text{ Nm}^3$	4,500 Kcal/Nm ³
Tar	123 ton	$45 \times 10^{3}_{3}$ ton	
Light oil	41 ton	15 x 10 ² ton	· ·
Ammonium sulfate	44 ton	16 x 10 ³ ton	· .
Sulfuric acid	17 ton	6.2×10^3 ton	Raw material for
(byproduct)	· .		ammonium sulfate

Table 13 PRODUCTION BALANCE

Table 14 BASIC ASSUMPTIONS FOR PROPOSED PRODUCTION VOLUMES

Item	Yield	Remarks
Moisture content of coal charge	9%	
Volatile matter of coal charge	27.6%	
Coke yield	74%	Coal basis
Lump coke yield	85%	Coke basis
COG yield	335Nm ³ /1-coal	4,500kcal/Nm
Proportion of COG sold	55% : 45%	
Tar yield	3.3%	Coal basis
Light oil yield	1.1%	Coal basis
Ammonium sulfate yield	1,2%	Coal basis
By-product sulfuric acid yield	0.5%	Coal basis, captive private

8. Financial and Economic Analysis

The maximum possible blending ratio of Guasare coal available in Zulia State is discussed from the point of financial and economic aspect.

In this chapter, financial and economic analysis is made on the following cases as calculated in the previous chapter.

Case 1 – Blending ratio for Guasare coal is 10%

- Case 2 Guasare coal is 15% with expectation that HAT coal are available so that LAS coal to be replaceable in future.
- Case 3 Guasare coal is 23% with expectation that FNO coal and Boyaca coal are available in future.

8.1 Assumptions

The assumptions for the above cases are summarized in the Table 15, 16, and 17. Since the assumptions on financial and economic analysis have been made in the main report, the assumptions newly established and the points to the considered are described below.

(1) Raw coal

From the results of raw coal and material balance as stated in the previous chapters, the coke yield for all the cases is 74% (in the calculation 74.019% is employed), and the blending ratio is summarized as follows:

Raw Coal	Case 1	Case 2	Case 3
Domestic coal (FNO/LAS or HAT)	32%	32%	29%
Domestic coal (Guasare)	10%	15%	23%
Colombian coal (Boyaca)	3%	3%	19%
U.S. coal (Pinnacle/Blue Creek)	55%	50%	29%
Total	100%	100%	100%

BLENDING RATIO FOR ADDITIONAL CASES

Regarding purchase price of Guasare coal, 20 US\$/ton in a dry coal basis is employed in this calculation, which, the price of Guasare coal is 4 US\$/ton lower than that of FNO/LAS coal. HAT coal is the same price as FNO/LAS coal because of location in Tachira.

With the above coke yield and blending ratio, production of COG, crude tar, crude benzene and ammonium sulfate will increase compared with those for the base case.

(2) Investment cost

Investment cost for the cases above excluding initial working capital is assumed the same as that for the base case of main report.

Breakdown of initial working capital is shown in Table 19.

8.2 Financial and Economic Analysis

Based on the assumptions described heretofore, the result of the analysis for the additional cases is summarized in Table 18.

The FIRR (before tax) for the case-1 is 0.19%, 0.94% for case-2, and 2.78% for case-3.

Regarding financial position, the results for case 1 and 2 shows that DSR(Debt Service Ratio) is almost 1.0 or less throughout the project life, indicating cash shortage from the first year of operation, while the result for case 3 shows DSR is less than 1.0 during the first 5 years from the start of operation and grows above 1.15 in the 9th year, indicating cash shortage for 11 years after the start of operation.

The BF coke production cost as a average in the tenth year of operation, or in 2007 is shown below.

BF COKE PRODUCTION COST

(Unit: US\$/ton)

Item	Case 1	Case 2	Case 3
- Not including depreciation and interest	82.50	79.01	69.72
- Including depreciation and interest	143.29	137.92	123.63

From the above table, the costs for all the cases including depreciation and interest are higher than the sales price of BF coke (US\$ 120/ton).

In addition to the above analysis, the amount of foreign currency carned from the project is calculated.

The total foreign currency earnings over the project life is US\$ 386 million for case-1, US\$ 474 million for case-2 and US\$ 658 million for case-3. The EIRR for the case-1 is 0.95%, 1.69% for case-2, and 3.52% for case-3.

Table 15 PROJECT PROFILE AND FINANCIAL ANALYSIS SUMMARY FOR CASE 1 (1/3)

1. Project

2.

Title Location Project Case/Study Date Selected Coal (Domestic) (Imported) Maximum Operable Days	: Establishment of Coke Plant Project : La Canada, Venezuela : Case 1/June 6, 1994 : FNO/LAS/Guasare : Pinnacle/Blue Creek (U.S.A.) Boyaca (Colombia) : 365 DPY
Coke Production @100%	: 2,740 TPD x 365 DPY = 1,000,000 TPY
Yield of Coke Product	: 74.019% of Feed Coal Input
Feed Coal Input (Dry Coal Basis)	: 3,701 TPD x 365 DPY = 1,351,004 TPY
Production Start Year	: 1998
Monetary Unit	: US dollars(\$) in terms of fixed
Exchange Rate for Caluculation	price in 1993 : 1 US\$ = 115 Yen as an average in 1993 : 1 US\$ = 95 Bs during site survey in 1993
Schedule	
Contract Award	: Dec. 01, 1995
Mechanical Completion	: Feb. 28, 1997
Production Start	: May. 01, 1998
Project Phase Out	: Dec. 31, 2017
Project Life	: 20 Years from Production Start
Project Year	: May to April
Construction and Commissioning	: 29 months from Contract Award

3. Financing Required and Financing Plan in 1993 Price Base

Financing Required	US\$, MM	Financing Plan	US\$, MM
Land/Site Development	2.36	Equity : 30.0%	198.28
Erected Plant Cost Coke Oven	606.36 (177.23)	Foreign Soft Loan: 70.0% - Interest : 5.00%	462.67
 Coal/Coke Storage By-Products 	(164.60) (142.02)	Short Term Loan: - Interest : 5.00%	Balance
 Common Facility Engineering Service, etc 	(46.50) (76.01)	Financing Plan	660.95
Pre-Operational Expense Interest during Construction	6.92 27.37		
Fixed Capital Cost Initial Working Capital	643.01 17.94		
Financing Required	660.95		

Table 15 PROJECT PROFILE AND FINANCIAL ANALYSIS SUMMARY FOR CASE 1 (2/3)

Inputs		Unit	Per Coal	(Dry)	Per BF co	ke Annua	al
	Unit	Cost	Consumption	n Cost	Cost	Consumption	n Cost
		\$/Unit	Unit/Unit	\$/Unit	\$/Unit	(MM, Unit)	\$, MM
Raw Material exc. Moisture @	9%		ń.	÷			,
 Domestic Coal(FNO/LAS) 	Ton	26.37	0.320	8.44	13.41	0.4323	11.400
 Domestic Coal(Guasare) 	Ton	21.98	0.100	2.20	3.49	0.1351	2.970
 Imported Coal(Boyaca) 	Ton	43.96	0.030	1.32	2.10	0.0405	1.782
 Imported Coal(U.S.A) 	Ton	65.93	0.550	36.26	57.63	0.7431	48.989
Coke Oven Gas Utilities	Nm ³	0.015	150.89	2.26	3.60	203.85	3.058
- Electricity	kwh	0.013	45.388	0.59	0.94	61.32	0.797
- Water	m ³	0.029	2.539	0.07	0.12	3.43	0.099
Cat/Chem	Ton	1.304	0.740	0.97	1.53	1.000	1.304
(1) Variable Cost					82.82	0.850	70.399
Operating Staff	M-Y	5,824			4.80	700	4.077
Overhead	Ope.	Staff x 5	50%		2.40		2.038
Maintenance Cost	Plan	t Direct C	ost x 2.0%		12.48	—	10.607
Tax & Insurance	Fixe	d Capital	Cost x 0.5%		3.78	-	3.215
(2) Direct Fixed Cost	_		<u> </u>		23.46	0.850	19.937
Credits							
– Coke Oven Gas	Nm ³	0.015	335.31	5.03	7.99	453.00	6.795
– Crude Tar	Ton	50.00	0.033	1.65	2.62	0.04458	2,229
– Crude Benzene	Ton	240.00	0.011	2.64	4.20	0.01486	3.566
 Ammonium Sulphate 	Ton	100.00	0.012	1.20	1.91	0.01621	1.621
 Coke Breeze (Export) 	Ton	40.00	0.11103	4.44	7.06	0.15000	6.000
(Local)	Ton	66.32		-			
(3) Total Credits	_	_		_	23.78	0.850	20.211
(4) Production Cost = (1)+(2)-	-(3)	<u> </u>		,- 	82.50	0.850	70.125

4. Inputs and Pricing (CIF at the Plant in 1993 Price Base)

Table 15 PROJECT PROFILE AND FINANCIAL ANALYSIS SUMMARY FOR CASE 1 (3/3)

5. Outputs and Pricing (FOB at the Plant with Full Capacity Utilization in 1993)

			Un	it				Annual	₩ ₩ ₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩	ng €/*/dad ta¥ kakartapi atkar muno kumunikum
	Outputs	and a second		Pric	:e	Production			Sales	
		Unit		(\$/Ur	nit)	· (N	/M, Un	nit)	(\$, MI	v)
	BF Coke [*]	Ton		12	0.0		0.850		102.0	00
	(Note) *:FOB Venezuel	a Price	e = CIF	USA	(135 \$	/t) - C)cean F	Freight	(15 \$/t)	
6.	Operation Schedule			·	Proje	ct Yea	ır		: ^{, ,}	(Unit: %)
			(-)3	()2	(-)1	1	2	3	20	Total/
			95	96	97	98	99	00	2017	Avarage
_	Financing Disbursemer	nt	10	50	40					
	BF Coke Production									
	 Rated Capacity Utilization Inventory Increase Inventory Sales 	ation				80 10 10 70	100 2 12 98	100 0 (12 100	(-)12 0	1,980 0 0 1,980
-	Depreciation/Salvage V Amortization/Salvage V Corporate Income Tax			-		raight line/Zero salva raight line/Zero salva			-	
	Debt Service		Movir	num G	rano		nnual			
	Loan Type			Maturit			rest Ra	ite In	stallmer	nts
	Long Term Loan/Foreig Short Term Loan/Local	n	3 + 20 0 + 1				.00 .00		20 1	
	BF Coke Inventory Coke Breeze Inventory Crude Tar Inventory Crude Benzene Inventor Ammonium Sulfate Inve Domestic Coal Inventor Imported Coal Inventor Account Receivable/Pa	entory 'Y Y	1.0 1.5 3.0 1.0 0.5 1.5	5 monti 5 monti 5 monti 5 monti 5 monti 5 monti	h hs hs h hs	nonth			· · .	

Table 16 PROJECT PROFILE AND FINANCIAL ANALYSIS SUMMARY FOR CASE 2 (1/3)

1. Project

	Title	: Establishment of Coke Plant Project
	Location	: La Canada, Venezuela
	Project Case/Study Date	: Case 2/June 6, 1994
		•
	Selected Coal (Domestic)	: FNO/HAT/Guasare
	(Imported)	: Pinnacle/Blue Creek (U.S.A.)
		Boyaca (Colombia)
	Maximum Operable Days	: 365 DPY
	Coke Production @100%	: 2,740 TPD x 365 DPY = 1,000,000 TPY
	Yield of Coke Product	: 74.019% of Feed Coal Input
	·····	
	Feed Coal Input (Dry Coal Basis)	: 3,701 TPD x 365 DPY = 1,351,004 TPY
	Production Start Year	: 1998
	Monetary Unit	: US dollars(\$) in terms of fixed
		price in 1993
	Exchange Rate for Caluculation	: 1 US\$ = 115 Yen as an average in 1993
	Exercise Face for exidentialeri	: 1 US\$ = 95 Bs during site survey in 1993
		1000 = 30 D3 during site survey in 1995
2,	Schedule	
	Contract Award	: Dec. 01, 1995
	Mechanical Completion	: Feb. 28, 1997
	Production Start	: May. 01, 1998
	Project Phase Out	: Dec. 31, 2017
	Project Life	: 20 Years from Production Start
	Project Year	: May to April
	Construction and Commissioning	: 29 months from Contract Award

3. Financing Required and Financing Plan in 1993 Price Base

Financing Required	US\$, MM	Financing	Plan	US\$, MM
Land/Site Development	2.36	Equity	: 30.0%	198.14
Erected Plant Cost Coke Oven	606.36 (177.23)	Foreign Soft Lo – Interest	an: 70.0% : 5.00%	462.32
- Coal/Coke Storage - By-Products	(164.60) (142.02)	Short Term Loa – Interest		Balance
 Common Facility Engineering Service, etc 	(46.50) (76.01)	Financing Plan	722 - 537 - 57 - 56 - 77 - 56 - 76 - 76 - 76 - 7	660.46
Pre-Operational Expense	6.92			
Interest during Construction	27.37			
Fixed Capital Cost	643.01			
Initial Working Capital	17.45			
Financing Required	660.46			

Table 16 PROJECT PROFILE AND FINANCIAL ANALYSIS SUMMARY FOR CASE 2 (2/3)

Inputs	:	Unit	Per Coal	(Dry) F	Per BF co	ke Annua	ıl
	Unit	Cost	Consumption	n Cost	Cost	Consumption	n Cost
		\$/Unit	Unit/Unit	\$/Unit	\$/Unit	(MM, Unit)	\$, MM
Raw Material exc. Moisture @	2004						
- Domestic Coal(FNO/HAT)	Ton	26.37	0.320	8.44	13.41	0.4323	11.400
- Domestic Coal(Guasare)	Ton	21.98	0.150	3.30	5.24	0.2027	4.454
- Imported Coal(Boyaca)	Ton	43.96	0.030	1.32	2.10	0.0405	1.782
- Imported Coal(U.S.A)	Ton	65.93	0.500		52.39	0.6755	44.536
Coke Oven Gas	Nm ³	0.015	150.89	2.26	3.60	203.85	3.058
Utilities		0.0,10	100.00	L.L.V	0.00	200.00	0.000
- Electricity	kwh	0.013	45.388	0.59	0.94	61.32	0.797
– Water	m ³	0.029	2.539	0.07	0.12	3.43	0.099
Cat/Chem	Ton	1.304	0.740	0.97	1.53	1.000	1.304
(1) Variable Cost					79.33	0.850	67.430
Operating Staff	M–Y	5,824			4.80	700	4.077
Overhead		Staff x £	50%		2.40		2.038
Maintenance Cost	Plant	t Direct C	ost x 2.0%		12.48		10.607
Tax & Insurance	Fixed	d Capital	Cost x 0.5%		3.78	-	3.215
(2) Direct Fixed Cost					23.46	0.850	19.937
Credits					· .		
 Coke Oven Gas 	Nm ³	0.015	335.31	5.03	7.99	453.00	6,795
– Crude Tar	Ton	50.00	0.033	1.65	2.62	0.04458	2,229
 Crude Benzene 	Ton	240.00	0.011	2.64	4.20	0.01486	3,566
 Ammonium Sulphate 	Ton	100.00	0.012	1.20	1.91	0.01621	1.621
 Coke Breeze (Export) 	Ton	40.00	0.11103	4.44	7.06	0.15000	6.000
(Local)	Ton	66.32					-
(3) Total Credits					23.78	0.850	20.211
(4) Production Cost = $(1)+(2)$ -	-(3)		· • • • • • • • • • • • • • • • • • • •		79.01	0.850	67,156

4. Inputs and Pricing (CIF at the Plant in 1993 Price Base)

Table 16 PROJECT PROFILE AND FINANCIAL ANALYSIS SUMMARY FOR CASE 2 (3/3)

5. Outputs and Pricing

(FOB at the Plant with Full Capacity Utilization in 1993)

		Unit	Annual			
Outputs Unit	Price	Production	Sales			
	Unit	(\$/Unit)	(MM, Unit)	(\$, MM)		
BF Coke*	Ton	120.0	0.850	102.000		

(Note) *: FOB Venezuela Price = CIF USA (135 \$/t) - Ocean Freight (15 \$/t)

6. Operation Schedule

6.	Operation Schedule		÷	Proje	ect Yea	ar			(Unit: %)
		()3	(-)2	()1	1	2	3	20	Total/
		95	96	97	98	99	00	2017	Avarage
_	Financing Disbursement	10	50	40					
	BF Coke Production								·
	 Rated Capacity Utilization Inventory Increase Inventory Sales 				80 10 10 70	100 2 12 98	100 0 12 100	()12 0	1,980 0 0 1,980
	Depreciation/Salvage Value Amortization/Salvage Value Corporate Income Tax		-					age valu age valu	
B errot	Debt Service Loan Type		num G Maturity			nnual rest Rat	te In	istallmer	nts
	Long Term Loan/Foreign Short Term Loan/Local		3 + 20) + 1			.00 .00		20 1	
	BF Coke Inventory Coke Breeze Inventory Crude Tar Inventory Crude Benzene Inventory Ammonium Sulfate Inventory Domestic Coal Inventory Imported Coal Inventory Account Receivable/Payable	0.5 months 1.5 months) 15 15 1 15 15	ionth				

Table 17 PROJECT PROFILE AND FINANCIAL ANALYSIS SUMMARY FOR CASE 3 (1/3)

1. Project

	Title Location Project Case/Study Date Selected Coal (Domestic) (Imported)	: Establishment of Coke Plant Project : La Canada, Venezuela : Case 3/June 6, 1994 : FNO/Guasare : Blue Creek (U.S.A.) Boyaca (Colombia)
	Maximum Operable Days	: 365 DPY
	Coke Production @100% Yield of Coke Product	: 2,740 TPD x 365 DPY = 1,000,000 TPY : 74.019% of Feed Coal Input
	Feed Coal Input (Dry Coal Basis)	: 3,701 TPD x 365 DPY = 1,351,004 TPY
	Production Start Year	: 1998
	Monetary Unit	: US dollars(\$) in terms of fixed price in 1993
	Exchange Rate for Caluculation	: 1 US\$ = 115 Yen as an average in 1993 : 1 US\$ = 95 Bs during site survey in 1993
2.	Schedule	
	Contract Award	: Dec. 01, 1995
	Mechanical Completion	: Feb. 28, 1997
	Production Start	: May. 01, 1998
	Project Phase Out	: Dec. 31, 2017
	Project Life	: 20 Years from Production Start
	Project Year	: May to April
	Construction and Commissioning	: 29 months from Contract Award

3. Financing Required and Financing Plan in 1993 Price Base

Financing Required	US\$, MM	Finan	US\$, MM	
Land/Site Development	2.36	Equity	: 30.0%	197.79
Erected Plant Cost - Coke Oven	606.36 (177.23)	Foreign Sot – Interest	t Loan: 70.0% : 5.00%	461.52
 Coal/Coke Storage By-Products 	(164.60) (142.02)	Short Term – Interest		Balance
 Common Facility Engineering Service, etc 	(46.50) (76.01)	Financing F	lan	659.31
Pre-Operational Expense	6.92		÷ .	
Interest during Construction	27.37			
Fixed Capital Cost	643.01			
Initial Working Capital	16.30		· .	
Financing Required	659.31		:	

Table 17 PROJECT PROFILE AND FINANCIAL ANALYSIS SUMMARY FOR CASE 3 (2/3)

Inputs		Unit	Per Coal	(Dry)	Per BF co	ke Annua	al
	Unit	Cost	Consumption	Cost	Cost	Consumptio	n Cost
· .	CLERI DO LAMOR	\$/Unit	Unit/Unit	\$/Unit	\$/Unit	(MM, Unit)	\$, MM
			494,				
Raw Material exc. Moisture (@9%					-	
- Domestic Coal(FNO)	Ton	26.37	0.290	7.65	12.15	0.3918	10.332
- Domestic Coal(Guasare)	Ton	21.98	0.230	5.06	8.03	0.3107	6.830
- Imported Coal(Boyaca)	Ton	43.96	0.190	8.35	13.28	0.2567	11.284
- Imported Coal(U.S.A)	Ton	65.93	0.290	19.12	30.39	0.3918	25.831
Coke Oven Gas Utilities	Nm ³	0.015	150.89	2.26	3.60	203.85	3.058
- Electricity	kwh	0.013	45.388	0.59	0.94	61.32	0.797
- Water	m³	0.029	2.539	0.07	0.12	3.43	0.099
Cat/Chem	Ton	1.304	0.740	0.97	1.53	1.000	1.304
(1) Variable Cost	_			_	70.04	0.850	59.535
Operating Staff	M-Y	5,824			4.80	700	4.077
Overhead	Ope	. Staff x 5	50%		2.40		2.038
Maintenance Cost	Plan	t Direct C	ost x 2.0%		12.48	<u> </u>	10.607
Tax & Insurance	Fixe	d Capital	Cost x 0.5%		3.78		3.215
(2) Direct Fixed Cost	_				23.46	0.850	19.937
Credits							
 Coke Oven Gas 	Nm ³	0.015	335.31	5.03	7.99	453.00	6.795
– Crude Tar	Ton	50.00	0.033	1.65	2.62	0.04458	2.229
- Crude Benzene	Ton	240.00	0.011	2.64	4.20	0.01486	3.566
 Ammonium Sulphate 	Ton	100.00	0.012	1.20	1.91	0.01621	1.621
 Coke Breeze (Export) 	Ton	40.00	0.11103	4.44	7.06	0.15000	6.000
(Local)	Ton	66.32	_		<u> </u>	_	-
(3) Total Credits		<u>.</u>			23.78	0.850	20.211
(4) Production Cost = (1)+(2)	-(3)				69.72	0.850	59.261

4. Inputs and Pricing (CIF at the Plant in 1993 Price Base)

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Table 17 PROJECT PROFILE AND FINANCIAL ANALYSIS SUMMARY FOR CASE 3 (3/3)

5. Outputs and Pricing (FOB at the Plant with Full Capacity Utilization in 1993)

Outpute		Unit					al		
Outputs	Price (\$/Unit)		Production (MM, Unit)			Sales (\$, MM)			
Unit									
BF Coke [*] Ton	,,,,,	12	0.0		0.850		102.0	000	
(Note) *:FOB Venezuela Pric	ce = Clf	USA	(135 \$	/t) – C	cean I	reigh	t (15 \$/t)		
Operation Schedule	ï		Proje	ct Yea	ar			(Unit: %	
:	(-)3	(-)2	_	1		3	20	Total/	
	95	96	97	98		00	2017		
Financing Disbursement	10	50	40						
BF Coke Production									
 Rated Capacity Utilization Inventory Increase Inventory Sales 				80 10 10 70	100 2 12 98	100 0 12 100	(-)12 0	1,980 0 0 1,980	
Depreciation/Salvage Value Amortization/Salvage Value Corporate Income Tax		•		-					
Debt Service		_							
Loan Type						ite l	Installmer	nts	
Long Term Loan/Foreign Short Term Loan/Local							20 1		
Domestic Coal Inventory	1.0 1.5 3.0 y 1.0 0.5	monti monti monti monti monti	n hsth hs n			an th	• • • • •		
	(Note) *:FOB Venezuela Prio Operation Schedule Financing Disbursement BF Coke Production - Rated Capacity Utilization - Inventory Increase - Inventory Increase - Inventory - Sales Depreciation/Salvage Value Corporate Income Tax Debt Service Loan Type Long Term Loan/Foreign Short Term Loan/Local BF Coke Inventory Coke Breeze Inventory Crude Tar Inventory Crude Tar Inventory Crude Benzene Inventory Ammonium Sulfate Inventor	(Note) *:FOB Venezuela Price = ClfOperation Schedule(-)3 95Financing Disbursement10BF Coke Production10- Rated Capacity Utilization - Inventory Increase - Inventory - Sales10Depreciation/Salvage Value Amortization/Salvage Value Corporate Income TaxMaxir + MDebt Service Loan TypeMaxir + MLong Term Loan/Foreign Short Term Loan/Local3BF Coke Inventory Crude Benzene Inventory Ammonium Sulfate Inventory Imported Coal Inventory1.5	(Note) *:FOB Venezuela Price = CIF USAOperation Schedule	(Note) *:FOB Venezuela Price = CIF USA (135 \$Operation Schedule $Proje(-)3(-)2(-)3(-)2(-)1959697Financing Disbursement105040BF Coke Production- Rated Capacity Utilization- Inventory Increase- Inventory- SalesDepreciation/Salvage ValueCorporate Income TaxDebt ServiceLoan TypeLong Term Loan/ForeignShort Term Loan/LocalBF Coke InventoryCrude Tar InventoryCrude Benzene InventoryAmmonium Sulfate InventoryDomestic Coal Inventory1.5 months1.0 month0.5 months1.5 months1.5 months1.0 month0.5 months$	(Note) *:FOB Venezuela Price = CIF USA (135 \$/t) - COperation ScheduleProject Yea $(-)3$ $(-)2$ $(-)1$ 1 95 96 97 98 Financing Disbursement10 50 40 BF Coke Production10 50 40 BF Coke Production10 50 40 Imported Capacity Utilization80- Inventory Increase10- Inventory10- Sales70Depreciation/Salvage Value20 years straight IAmortization/Salvage Value20 years straight ICorporate Income Tax 30% Debt ServiceMaximum Grace + MaturityLong Term Loan/Foreign Short Term Loan/Local $3 + 20$ BF Coke Inventory Crude Tar Inventory1.5 months 1.0 month 3.0 monthsBF Coke Inventory Ammonium Sulfate Inventory Domestic Coal Inventory1.5 months 1.0 month 0.5 monthsImported Coal Inventory1.5 months	(Note) *:FOB Venezuela Price = CIF USA (135 \$/t) - Ocean FOperation ScheduleProject Year $(-)3$ $(-)2$ $(-)1$ 1 2 95 96 97 98 99 Financing Disbursement10 50 40 BF Coke Production- Rated Capacity Utilization - Inventory Increase - Inventory 80 100 2 Rated Capacity Utilization - Inventory Increase - Inventory 80 100 2 Rates 10 2 2 Neventory - Sales 10 2 2 O years straight line/Zei 20 years straight line/Zei 20 years straight line/Zei 30% $3 + 20$ 5.00Debt Service Loan TypeMaximum Grace + MaturityAnnual Interest Rai $3 + 20$ Long Term Loan/Foreign Short Term Loan/Local $3 + 20$ 5.00 BF Coke Inventory Crude Bareze Inventory Crude Benzene Inventory 1.5 months 1.5 months 5.00 BF Coke Inventory Crude Benzene Inventory Inported Coal Inventory 1.5 months 1.5 months 5.00	(Note) *:FOB Venezuela Price = CIF USA (135 \$/t) - Ocean FreighOperation ScheduleProject Year $(-)3$ $(-)2$ $(-)1$ 1 2 3 95 96 97 98 99 00 Financing Disbursement105040BF Coke Production105040- Rated Capacity Utilization - Inventory Increase - Inventory80100100- Inventory - Sales1020Depreciation/Salvage Value Corporate Income Tax20 years straight line/Zero salv 30%20 years straight line/Zero salv 30%Debt Service Loan TypeMaximum Grace + MaturityAnnual Interest RateLong Term Loan/Foreign Short Term Loan/Local3 + 205.00BF Coke Inventory Crude Tar Inventory1.5 months 1.0 month 0 mestic Coal Inventory1.5 months 1.0 month 0.5 months 1.0 month 0.5 monthsBF Coke Inventory Crude Tar Inventory1.5 months 1.0 month 0.5 months3.500		

			Case 1	Case 2	Case 3
	Coke production Coke yield	(tons/year) (%)	1,000,000 74.02	1,000,000 74.02	1,000,000 74.02
	Coal blending ratio				
	 Domestic coal (FNO/LAS or HAT) Domestic coal (Guasare) 	(%) (%)	32.00 10.00	32.00 15.00	29.00 23.00
	 Imported coal (Boyaca) 	(%)	3.00	3.00	19.00
	 Imported coal (U.S.A) 	(%)	55.00	50.00	29.00
······	B.F. coke sales volume for export	(tons/year)	850,000	850,000	850,000
1)	Capital Investment Cost	(million dollars)	660.95	660.46	659.31
2)	Financing Plan	(million dollars)			
	Equity	(30%)	198.28	198.14	197.79
	Long-term loans	(70%)	462.67	462.32	461.52
	Total		660.95	660.46	659.31
3)	Major Assumptions for Plant Operation	I			
	Sales prices for export	(FOB)			
	- B.F. cokes	(\$/ton)	120.0	120.0	120.0
	- Coke breeze	(\$/ton)	40.0	40.0	40.0
	Coal for coke making	(CIF, Dry base)	00.07	00.07	00.07
	 Domestic coals (FNO/LAS) Domestic coals (Guasare) 	(\$/ton) (\$/ton)	26.37 21.98	26.37 21.98	26.37 21.98
	- Imported coals (Boyaca)	(\$/ton)	43.96	43.96	43.96
	 Imported coals (U.S.A) 	(\$/ton)	65.93	65.93	65.93
	Operating staff		700	700	700
	Service life on depreciation		20	20	20
	Interest rate on loan	(%)	5.0	5.0	5.0
	Repayment period		20	20	20
4)	Results of Financial Economic Analysi	S .			
	Financial internal rate of return(FIRR)	(before tax, %)	0.19	0.94	2.78
		(after tax, %)	0.19	0.94	2.66
	Debt service ratio	(DSR)			
	 1st year of operation 2nd year of operation 		0.50	0.55	0.67
	 – 2nd year of operation – 3rd year of operation 		0.65 0.67	0.72 0.75	0.89 0.94
	Average production cost	(per B.F. cokes, \$		0.10	0.01
	 Cost not including 	(r	,,		
	depreciation and interest - Cost including depreciation		82.50	79.01	69.72
	and interest		143.29	137.92	123.63
	Sensitivity analysis on FIRR	(before tax, %)			
	 Sales price including Breeze 	(up 20%)	4.97	5.54	7.00
	- Coal prices	(down 20%)	3.25	3.76	5.04
	 Investment cost 	(down 20%)	2.86	3.65	5.61
	Economic internal rate of return	(EIRR, %)	0.95	1.69	3.52
	Foreign currency earnings	(million, dollars)			
	- Whole project life		385.55	474.26	657.69

Table 18 PROJECT CASES COMPARISON SUMMARY ON COKE PLANT PROJECT

Note Exchange rate: \$1 = 115 yen = 95Bs Pricing lebel: US\$ in terms of fixed price in 1993 Project life: 23 years including 3 years of construction

				(Unit: 1,000US\$)
Item	Case 1	Amount Case 2	Case 3	Remarks
- Inventory of products	8,930	8,631	7,834	1.51 months of the production cost in the initial year, not including depreciation ^(Note)
- Inventory of imported coal	5,077	4,632	3,721	1.5 months of the imported coal cost in the initial year
- Inventory of domestic coal	479	529	572	0.5 months of the omestic coal cost in the initial year
- Account receivable	7,694	7,694	7,694	1 month of sales including By products except COG in the initial year
- Account payable	▲4,240	▲4,041	▲3,516	1 month of variable cost in the initial year
Total	17,940	17,445	16,296	**************************************

Table 19 BREAKDOWN OF INITIAL WORKING CAPITAL

(Note)

The inventories of products including BF coke and by-products except COG are taken into account as follows.

– BF coke	: 1.5 months
 Coke Breeze 	: 1.0 month
~ Crude Tar	: 1.5 months
 – Crude Benzene 	: 3.0 months
- Ammonium Sulfate	: 1.0 month

Allocating the costs on the base of the above inventory period and sales revenue (deemed to correspond to cost) by each product, the average inventory period becomes 1.51 months.

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It is essential to use coking coal in order to obtain required coke strength for blust furnace use. But unfortunately reserve of coking coal is limited in comparison with non-coking coal. Many studies have been conducted to use non-coking coal into formed coke, which can be used as the principal fuel source for blust furnaces. And now the formed coke process is considered as the alternate process to be replaceable to conventional chamber type process.

In Japan steel industry has started their work for developing the utilization of the noncoking coal into formed coke since 1979. In 1986 pilot plan which produces 200 ton per day by continuous manufacturing process has start operation. The formed coke were tested in the blust furnace with the capacity of 4,000 ton per day though only 20 to 40% are blended. It is reported the test was successful.

The feasibility study of formed coke production plant with the capacity of 3,000 ton per day have completed. But until now commercial production has not materialized yet.

In Close 10, information pertaining the formed coke process are attached.

10. Information Pertaining the Formed Coke Process

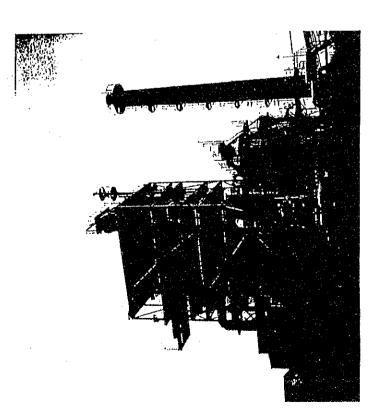
- Pamphlet of the Japan Iron and Steel Federation, " THE FORMED-COKE PROCESS"
- (2) T. Okamura, Y. Izumiya, Y. Kondo, "Development of Formed Coke Process", Coke Making International, Vol.2, 1990 p9-p16
- (3) S.Kubo, et al., "Result of the Test with Formed Coke at Tobata No.4 Blust Furnace", 1990 Ironmaking Conference Processing p405-p412
- (4) I. Komaki, et al., "Development of Advanced Formcoke Process", The First International Congress of Science and Technology of Ironmaking, 1994

Information 1

Pamphlet of the Japan Iron and Steel Federation, "THE FORMED-COKE PROCESS"

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THE FORMED-COKE PROCESS



Introduction

The manufacturing of pig iron requires the melting of iron ore and, for this, large amounts of coke are used as a fuel for blast furmates. The steel industry's consumption of coke totalded 36 million tons, or 482 kilograms of coke per tan of pig iron produced in 1986.

The type of coal that can be used is limited. Coke destined for coheneking must be high quality, so coking coal is used in existing coke overs. (Desponor-coking coal, which is popularly used as a fuel for power generation, is of little use because it detricortes coke quality. Moreover, while coal is the most abundant energy source on the earth, with recoverable reserves is non-coking 300 billion tone, some 75 percent of these reserves is non-coking coal. After years of studying how to use these abundant reserves of non-coking cost, Japan's sreel industry recently developed a continuous manufacturing process that processes non-coking coal into furnaces.

The project was carried out by four steelmakers under the auspices of the Committee for Research and Development on the Formed Coke Forcess, which was created by the Japan iron and Steel Federation in 1978. The four companies are Kawasaki Steel, Kobe Steel, Nippon Steel and Nippon Kokan.

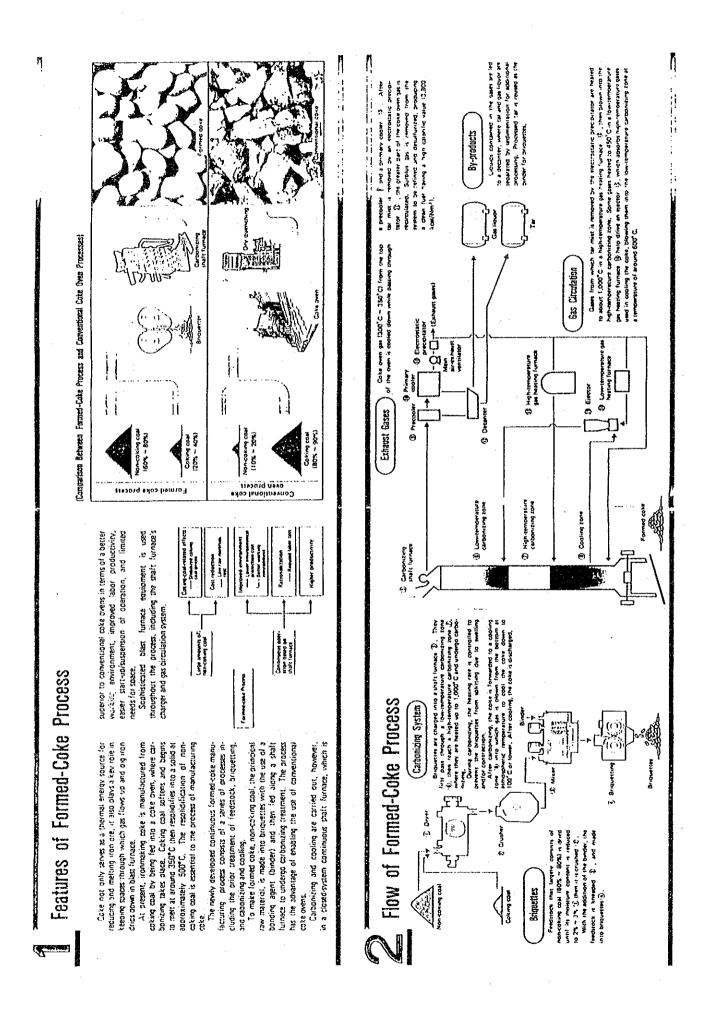
A pilot plant with a capacity of 200 tonu/day was constructed at the Yawata Works of Nippon Steel Corporation in 1984. For the next three years, R & D was carried out on formed cake manuticiting technology, including the running of demonstration tests on the use of the experimentality produced formed coke in a large blast furnace.

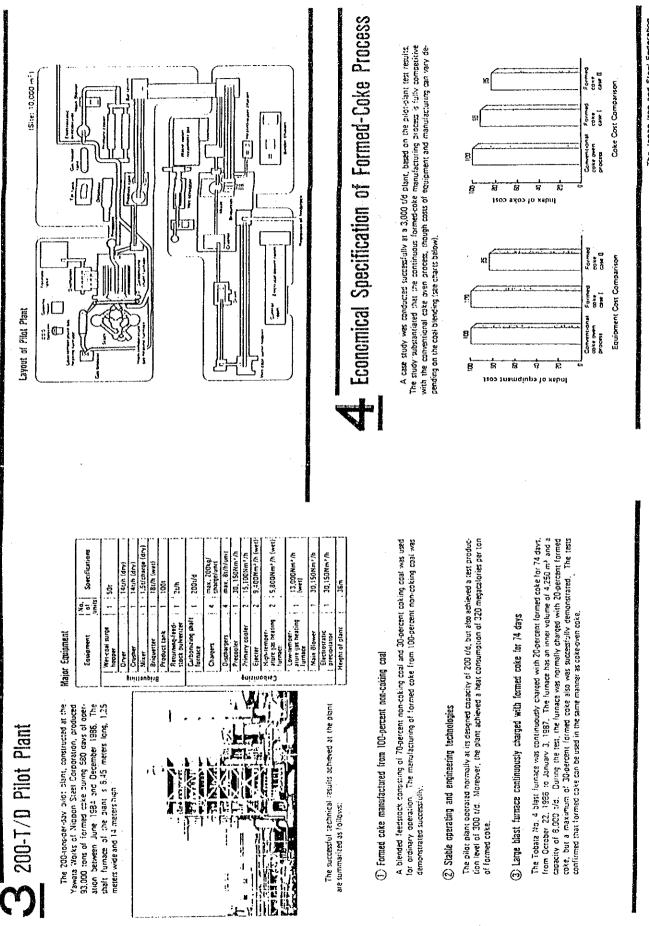
The result was the spoch-making discovery of technology for the manufacture, and use of formed toke from 100-percent non-coking coal feedstock.

Today, the manufactors of formed coke and its use as the princi-

pal fuel source in blast furnaces is about to be commercialized. For the steel indistry, this breakthrough will translate into two important benefics: the effective utilization of resources and the reduction of cost of raw materials and fuel.

The Japan Iron and Steel Federation





The Japan Iron and Steel Federation

Information 2

T. Okamura, Y. Izumiya, Y. Kondo, "Development of Formed Coke Process", Coke Making International, Vol.2, 1990 p9-p16

Development of Formed Coke Process

T. Okuhara*, Y. Izumiya* and Y. Konno**

1. Introduction

The manufacture of blast furnace coke by the conventional chamber oven process requires coking coal with caking properties as the principal raw material. The maximum proportion of noncoking coal that can be used in the chamber oven process is 20 to 30% of the coal charge, even when the briquette blend coking process and preheated coal charging process are applied as coal preparation techniques. Use of noncoking coal, claimed to account for three-fourths to four-fifths of the world's hard coal reserves. as the principal raw material in the manufacture of blast furnace coke is an important issue for coal resource conservation and coke production cost reduction. The coke-oven battery is composed of many coking chambers and involves many problems associated with automation and labor saving, as well as air pollution and a poor working environment.

To solve these problems of the chamber oven process, the development of various formed coke processes has been undertaken by many countries in the world [1]. Formed coke for blast furnaces has a history of over 40 years of research and development, but it has not yet been manufactured on a commercial basis. Nippon Steel developed a new formed coke process after many years of research [2]. To commercialize the formed coke process, Nippon Steel conducted joint research with three other steelmakers using a pilot plant [3 to 5] and succeeded in the development of the techniques required for the process. This report introduces the new formed coke process, with emphasis placed on the research and development work with the pilot plant.

2. History of Research and Development

As shown in Figure 1, research in this process was conducted over nine years from 1978 to 1986. A pilot plant was constructed in four years from 1980 to 1983, followed by three years of test operation. Formed coke produced by the pilot plant was tested in a blast furnace in 1986. Various improvements on the process were studied in parallel with the pilot plant study.

Engineering Division, Plant Engineering & Technology Bureau; Nippon Steel Corp.

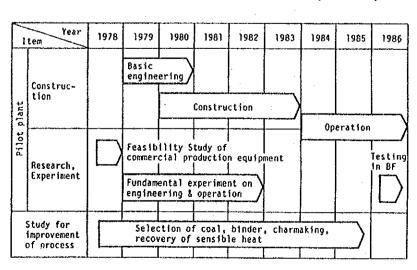


Figure 1. Development schedule.

3. Pilot Plant with Production Capacity of 200 t/d

Process Flow. In the formed coke process, cold briquettes are continuously carbonized in a shaft furnace using gas as the heating medium. The process is based on the research undertaken by Nippon Steel [2]. The pilot plant is designed to produce 200 tons of formed coke per day. It consists of a series of processes, such as coal preparation, coal briquetting, briquette carbonization and gas cooling as shown in Figure 2. In the briquetting process, coal is dried in advance and soft pitch is used as the binder. The pilot plant is entirely continuous, except for the kneading step in which the coal is mixed with the binder on a batch basis.

The formed coke process has a number of innovative features in the carbonizing process. The basic principle of the carbonizing process is that cold briquettes are continuously carbonized in a shaft furnace by controlling the carbonization behavior of cold briquettes according to the heat pattern concerned [2]. The carbonizing temperature pattern based on the principle in schematically shown in Figure 3. The key innovations tried for the first time in the carbonization process are as follows:

- The briquettes are heated by two rows of tuyeres to impart a heat pattern required to control their carbonization behavior, such as collapsing, sticking, swelling and cracking.
- For carbonizer simplification, all operations from carbonization to cooling are continuously performed in a single carbonizer.
- For high-calorie gas recovery, the generated gas is indirectly preheated and recirculated as the heating gas.
- 4) To utilize the sensible heat of coke for heating briquettes, the gas used for cooling is withdrawn from the carbonizer and recirculated to the low-temperature tuyeres.

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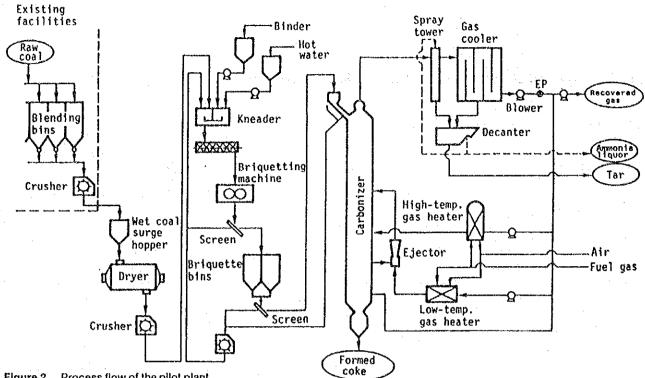


Figure 2. Process flow of the pilot plant.

The pilot plant was built in the coke plant of Yawata Works. The supply of raw materials and utilities needed and the treatment of products obtained depended entirely on the coke plant. The raw coals blended and crushed at the coke plant were transported by belt conveyors to the pilot plant. The recovered gas was piped to the generated gas main of the coke plant where it was mixed with the gas gencrated there and fed into the gas refining process.

Features of Carbonizing Equipment. The carbonizer is schematically illustrated in Figure 4. The carbonizer has a rectangular cross section. To avoid the scale-up problem, the carbonizer of the pilot plant has the same width and height as those of commercial carbonizers but its length is less than that of the latter. Four charging devices and four discharging devices are installed along the length of the carbonizer. Five tuyeres are installed along each header pipe for moving the heating gas and cooling gas in and out of the carbonizer. An ejector is provided on each side of the carbonizer to remove and circulate the gas used for cooling the formed coke. The low-temperature heating gas is indirectly preheated by a recuperator, while the high-temperature heating gas is preheated by hot stoves. The pyrolysis of hydrocarbons in the circulating gas forms carbon, which

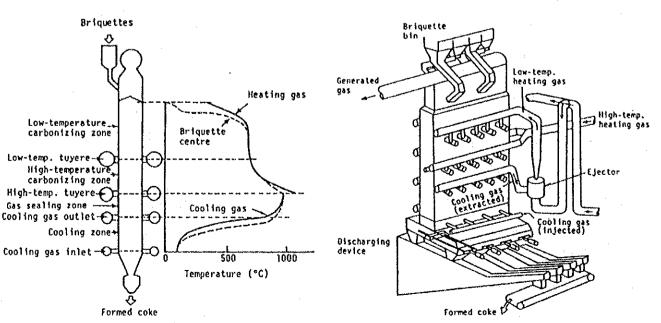


Figure 3. Profile of a carbonizer.

builds up in the high-temperature gas circulation system. The deposited carbon is burned off by air introduced during the changing of the hot stoves.

4. Test Operation of Pilot Plant

Outline of Test Operation. The pilot plant was operated for two years and six months from June 1984 to December 1986 in nine stages as initially planned. During this period, the pilot plant operated for 579 days and produced a total of 93.000 tons of formed coke, 61.000 tons of which were tested in a blast furnace. The formed coke was tested in the blast furnace in the last half of 1986.

Stable Operating Technology. The changes in the production rate and operating rate of the pilot plant during the test operation arc shown in Figure 5. In the fifth to eighth

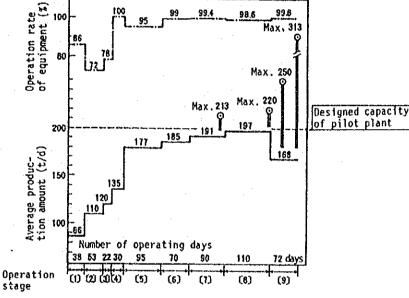


Figure 5. Transitions of production amount and operation rate.

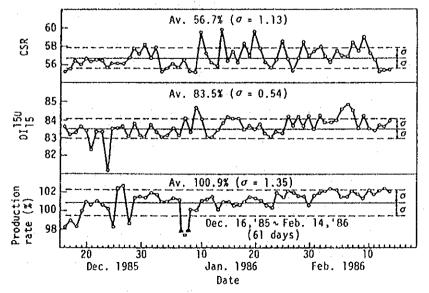


Figure 6. Operating results at 100% production rate.

stages of test operation in which formed coke samples for testing in a blast furnace were produced, the pilot plant was continuously run for a minimum of 70 days and a maximum of 110 days. The carbonizer was shut down due to troubles for less than 1% of each of the test periods (The low operating rate in the fifth stage was attributable to troubles in the briquetting process).

The pilot plant gradually increased the production of formed coke and accomplished as average daily production rate of 197 tons, just short of the designed capacity of 200 t/d, for 110 days of continuous operation in the eighth stage. A maximum daily production rate of 313 tons was recorded in the ninth stage. In the seventh stage, the pilot plant ran at the designed production rate of 200 t/d for 61 consecutive days, as shown in Figure 6. It was thus confirmed that the pilot plant was fully stable in the production quantity and quality of formed coke.

> The automation and sealing of devices for charging and discharging briquettes and formed coke, and for circulating the heating gas were as initially expected. In the shutdown periods in the nine stages of test operation, all devices but the hot stoves were cooled to ambient temperature. No troubles occurred in the equipment and operation of the pilot plant. The carbonizing equipment took four days each to shut down and restart. These figures proved that the carbonizing equipment was flexible enough to meet any production adjustments required.

Formed Coke Manufacturing Conditions. It was made clear that the carbonization conditions required to ensure the smooth descent of briquettes in the carbonizer and stabilize the quality of formed coke can be established by adjusting the top gas temperature and low-temperature tuyere gas temperature. The properties of the coal blend were found to exert a great effect on the top gas temperature and low-temperature tuyere gas temperature. For coal blends with high caking properties, it is desirable to raise the top gas temperature and lower the low-temperature tuyere gas temperature, as shown in Figure 7. The top gas temperature should be lowered to reduce heat consumption for carbonization but must not be lower than about 270°C, lest the tar vapor in the gas should condense.

It was found that the desired strength of formed coke can be maintained even if the high-temperature tuyere gas temperature is lowered to 850° C - 900° C, as shown in Figure 8. The amount of binder that must be added to form briquettes was successfully decreased to about 6.5%.

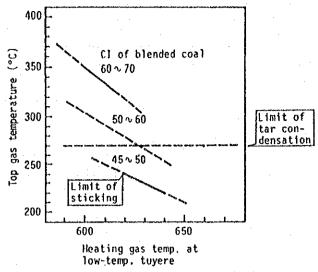


Figure 7. Relation between properties of blended coal and optimum carbonizing conditions.

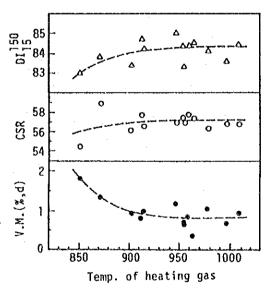


Figure 8. Relation between the heating gas temperature at high temperature tuyere and coke qualities.

		Samples	1	11	111	17	Y.
	Blending ratio	Non-coking coal	65	68	78	100	75
9 ons		Caking coal	35	32	22	0	25
Blending conditions	(%,d)	Binder	8.0	7.4	7.4	7.4	7.0
Blend condi	Coking	V.M. (X,d)	26.7	25.8	25.0	24.8	34.4
	property	C.I.	69.9	65.7	56.5	52.4	68.4
	Size distri- bution (%)	+50 (nm)	9.2	6.4	3.1	1.9	4.1
Quality of formed coke		50 v 25 (mm)	83.8	87.0	90.4	93.9	83.3
		-25 (mm)	8.0	6.6	6.1	4.5	12.6
	Strength CSR	D1150 D115	84.1	83.9	84.4	86.3	81.2
		CSR	56.7	56.8	55.8	56.1	47.5
	Porosity	(%)	38.5	40.1	34.0	29.6	42.4

Table 1. Typical blending conditions and qualities of formed coke.

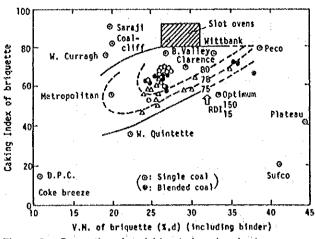


Figure 9. Properties of coal, blended coal and coke.

Coal Blending Conditions and Formed Coke Quality. The coals and coal blending conditions used in the test operation of the pilot plant are shown in Figure 9. The noncoking coals (caking index < 80) ranged from 19 to 45% (d) in volatile matter. The coal blends containing the binder ranged from 24 to 38% (d) in volatile matter and from 45 to 72 in the caking index. Several examples of coal blending conditions and formed coke quality are given in Table 1. When the blending ratio of noncoking coals was 65 to 100%, strength of formed coke produced was high enough as blast furnace coke. This result confirmed that the formed coke process can use noncoking coal as the principal raw material and can produce blast furnace coke from noncoking coal of suitable nature.

> The particle size of formed coke is mostly in the range of 50 to 25 mm and the porosity of formed coke is smaller than that of coke made by the conventional chamber oven process.

> Mass and Heat Balances in Carbonizing Process. The production yields of coke, tar and gas in the carbonizing process of the pilot plant are compared with those in the conventional cokemaking process in Figure 10. The formed coke process has a tar yield about twice that of the chamber oven process but a far lower gas yield than that of the latter process. The calorific value of gas recovered from the formed coke process was about 3.700 kcal/Nm³, as shown in Table 2. This value is low compared with that of the conventional chamber oven process but is exceptionally high for a formed coke process. The tar produced in the new formed coke process exhibits properties of low-temperature tar of low weight and small condensation degree, because it is not subjected to secondary pyrolysis at high temperatures as in the chamber oven process.