Table 2-13(1)	The Results of the Estimation for Each Index	
	Element by the CMB Method (Ist Survey)	

MS1

MS2

Element		Calculated (ns/m ³)	Observed (ng/n ⁺)	<u>Calculated</u> Observed
Index elements	Al Br Ca Cr Fe X Hn Na Ni Pb Sb Sc Se Ti Y Zn C Corr	1544.680 80.356 237.305 8.933 784.282 914.378 51.488 1116.683 9.869 473.892 0.296 0.123 0.445 74.809 12.375 71.602 15631.883 3353.184	$\begin{array}{c} 1300.000\\ 42.000\\ 2100.000\\ 6.500\\ 1700.000\\ 1300.000\\ 1300.000\\ 1100.000\\ 450.000\\ 450.000\\ 29.000\\ 0.200\\ 0.450\\ 67.000\\ 12.000\\ 720.000\\ 15300.000\\ 8700.000\\ \end{array}$	$\begin{array}{c} 1.19\\ 1.91 + \\ 0.11 - \\ 1.37\\ 0.46 - \\ 0.70\\ 0.86\\ 1.92\\ 0.52 - \\ 1.052 - \\ 0.01 - \\ 0.62 - \\ 0.99\\ 1.12\\ 1.03\\ 0.10 - \\ 1.02\\ 0.39 - \\ \end{array}$
Total 😳		24366.783	32906,150	0.74

Element		Calculated (ng/m ²)	Observed (ng/m²)	<u>Calculated</u> Observed
Index elements	Al Br Ca Cr Fe K Hn Na NI Pb Sb Sc Sc Se ti Y	989,046 32,761 246,933 9,651 709,371 619,838 52,987 1724,819 11,563 165,451 0,335 0,078 0,379 47,990 14,903	810.000 17,000 1200.000 1300.000 1300.000 1100.000 \$8.000 1700.000 1590.000 64.000 0.130 0.500 86.000 16,000	$\begin{array}{c} 1.22\\ 1.93\\ 0.21\\\\ 1.32\\ 0.55\\ -\\ 0.56\\ -\\ 0.91\\ 1.01\\ 1.16\\ 0.10\\\\ 0.60\\ -\\ 0.60\\ -\\ 0.76\\ 0.56\\ -\\ 0.93\\ \end{array}$
	Zn Care Care	72.119 13877.363 2513.216	960.000 13500.000 5800.000	0.08 1.03 0.43
Total	•	21088.866	28218.930	0.75

M S 3

M S 4

Element		Calculated (ng/m²)	Observed (ng/m³)	Calculated Observed
Index elements	Ai Br Ca Cr Fe K Mn Na Ni Pb Sc Sc Sc Sc Sc Ti V Zn C	1321.682 68.544 627.745 46.547 3021.493 807.878 267.251 1412.057 40.191 494.477 2.380 0.104 1.318 65.672 34.743 302.729 16729.996 3350.655	$\begin{array}{c} 1100.000\\ 31.000\\ 2600.000\\ 31.000\\ 4700.000\\ 1700.000\\ 360.000\\ 1400.000\\ 47.000\\ 780.000\\ 17.000\\ 0.190\\ 1.000\\ 130.000\\ 35.000\\ 3760.000\\ 16400.000\\ 16400.000\\ \end{array}$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$
Total	·	28775.471	43832.190	0.66

Elezent		Calculated (ng/m³)	Observed (ng/n²)	Calculated Observed
index elements	Al Br Ca Cr Fe K Mn Na Ni Pb Sb Sc Se Ti Y Zn C	1629.855 57.342 244.557 6.895 975.355 44.904 1529.258 5.154 313.559 -0.034 0.130 0.331 78.824 7.133 60.046 16574.312 3238.669	$\begin{array}{c} 1400.000\\ 37.000\\ 1600.000\\ 5.100\\ 1700.000\\ 1200.000\\ 75.000\\ 1500.000\\ 5.000\\ 290.000\\ 1500.000\\ 0.200\\ 0.400\\ 140.000\\ 7.400\\ 760.000\\ 16200.000\\ 9400.000\\ \end{array}$	$\begin{array}{c} 1.16\\ 1.55 \\ \cdot \\ 0.15 \\ - \\ \cdot \\ 0.31\\ 0.60 \\ - \\ 0.60 \\ - \\ 1.02 \\ 1.03 \\ 1.08 \\ - \\ 0.65 \\ - \\ 0.83 \\ 0.56 \\ - \\ 0.96 \\ 0.03 \\ - \\ 1.02 \\ 0.34 \\ - \end{array}$
fotai		25496.466	34337.100	0.74

MS 5

Element		Calculated (ng/a²)	Observed (ng/m³)	<u>Calculated</u> Observed
lndex elements	Al Br Ca Cr Fe X Mn Na Ni Pb Sb Sc Se Ti Y Zn Cal- Car- Car-	$\begin{array}{c} 2643,747\\7,533\\184,978\\4,520\\638,449\\1552,589\\26,295\\1153,068\\5,642\\31,873\\0,625\\0,212\\0,694\\128,762\\4,391\\35,547\\3761,973\\1603,416\end{array}$	$\begin{array}{c} 2200.000\\ 18.000\\ 2100.090\\ 3.300\\ 1100.000\\ 2000.000\\ 41.000\\ 1100.000\\ 30.000\\ 5.400\\ 0.230\\ 0.950\\ 150.000\\ 5.000\\ 150.000\\ 5.000\\ 140.000\\ 5500.000\\ 5700.000\end{array}$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$
Total		17769.418	24097.890	0.74

(Calculated/Observed)

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Table 2-13(2) The Results of the Estimation for Each Index Element by the CMB Method (2nd Survey)

MS1

M S 2

Eleaent		Calculated (ng/m")	Observed (ng/u²)	<u>Calculated</u> Observed
Index elements	Al Br Ca Cr Fe K Mn Na Ni Pb Sc Sc Sc Sc Ti Y Zn C Cc	$\begin{array}{c} 870.342\\ 14.653\\ 160.346\\ 5.053\\ 414.016\\ 544.630\\ 27,879\\ 1478.572\\ 5.204\\ 53.560\\ 0.331\\ 0.069\\ 0.309\\ 42.388\\ 5.161\\ 33.029\\ 7699.875\\ 1321.108\\ \end{array}$	$\begin{array}{c} 760.000\\ 14.000\\ 730.000\\ 3.700\\ 700.000\\ 640.000\\ 50.000\\ 1400.000\\ 3.500\\ 50.000\\ 5.100\\ 0.110\\ 1.100\\ 97.000\\ 6.400\\ 250.000\\ 7500.000\\ 7500.000\\ 4300.000\\ \end{array}$	$\begin{array}{c} 1.15\\ 1.05\\ 0.22 \\\\ 1.37\\ 0.59 \\ -\\ 0.85\\ 0.56 \\ -\\ 1.06\\ 1.49\\ 1.07\\ 0.06 \\\\ 0.63 \\ -\\ 0.28 \\\\ 0.44 \\ -\\ 0.81\\ 0.16 \\\\ 1.03\\ 0.31 \\ -\end{array}$
Total		12682.525	16510.910	0.77

Element		Calculated (ng/u²)	Observed (ng/m³)	<u>Calculated</u> Observed
lndex elements	Al Br Ca Fe K Mn Na Ni Pb Sb Sc Se ti Y Zn C Corr	341.211 14.990 138.370 7.212 147.035 294.885 14.159 2849.858 21.145 19.870 1.453 0.026 0.677 17.190 25.624 50.477 7730.535 1167.984	$\begin{array}{c} 310.000\\ 9.000\\ 400.000\\ 10.000\\ 420.000\\ 350.000\\ 11.000\\ 2800.000\\ 19.000\\ 20.000\\ 1.400\\ 0.054\\ 51.000\\ 98.000\\ 98.000\\ 82.000\\ 82.000\\ 82.000\\ 82.000\\ 82.000\\ 600.000\\ \end{array}$	$\begin{array}{c} 1.10\\ 1.67\\ +\\ 0.50\\ -\\ 0.73\\ 0.35\\ -\\ 0.84\\ 1.29\\ 1.02\\ 1.11\\ 0.99\\ 1.04\\ -\\ 0.99\\ 1.04\\ -\\ 0.01\\ -\\ 0.18\\ -\\ 0.99\\ 0.62\\ -\\ 1.03\\ 0.29\\ -\end{array}$
Total		12902.802	16107.454	0.80

MS 3

MS4

Element		Calculated (ng/m³)	Observed (ng/m²)	<u>Calculated</u> Observed
	AL	574.714	490.000	1.17
	Br	43.551	19.000	2.29 ++
	Ca	241.465	2000.000	0.12
	Cr	16.745	10.000	1,67 +
	Fe	206.005	2000.000	0.10
	ĸ	405.469	1300,000	0.31
Index	Xa	24.943	200.000	0.12
elements	Na	2140.176	2100.000	1.02
CICACIES	NI	50.376	55.000	0.92
	Pb	269.834	380.000	0.71
	Sb	4.019	6,500	0.62 -
	Sc	0.044	0.078	0.57 -
	Se	1.739	1.500	1.16
	ti	29.741	57,000	0.52 -
	l v	56,861	63.000	0.90
	Zn	113.893	2900,000	0.04
		11797.414	11500.000	1.03
	C	2087.456	5300.000	0.39 -
	C	2001.400	000,000	
îotal		18054.446	28382.078	0.64

Elegent		Calculated (ng/m²)	Observed (ng/m ³)	<u>Calculated</u> Observed
index elements	Al Br Ca Cr Fe K Mn Na Na Sb Sc Se Ti Y Zn Ca	780.470 15.426 183.194 4.862 216.116 514.601 14.299 1990.674 7.353 50.517 1.054 0.062 0.577 38.356 4.226 47.794 11819.266 1922.789	650.000 11.000 1600.000 2.900 400.000 750.000 24.000 1900.000 6.009 50.000 1.700 0.076 0.500 50.000 4.500 100.000 11500.000	$\begin{array}{c} 1.20\\ 1.40\\ 0.11\\ 1.68 +\\ 0.54 -\\ 0.69 -\\ 1.65 -\\ 1.23 -\\ 1.01 -\\ 0.62 -\\ 0.82 -\\ 1.15 -\\ 0.77 -\\ 0.94 -\\ 0.48 -\\ 1.03 -\\ 0.33 \end{array}$
Total	Corv	17612.656	22850.676	0.77

MS 5

689.247	670.000	
	$\begin{array}{c} 570.000\\ 12.000\\ 250.000\\ 0.770\\ 260.000\\ 540.000\\ 15.000\\ 1800.000\\ 3.000\\ 5.000\\ 0.470\\ 0.071\\ 0.950\\ 82.000\\ 2.100\\ 18.000\\ 6200.000\\ \end{array}$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$
	$\begin{array}{c} 1.153\\ 94.450\\ 461.546\\ 1.432\\ 2010.291\\ 2.703\\ 5.032\\ 0.387\\ 0.055\\ 0.282\\ 33.615\\ 2.036\\ 15.130\end{array}$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$

(Calculated/Observed)

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Table 2-13(3) The Results of the Estimation for Each Index Element by the CMB Method (3rd Survey)

MS 1

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Element		Calculated (ng/m ²)	Observed (ng/a ³)	<u>Calculated</u> Observed
<u></u>	AI	713.921	770.000	0.93
	Br	37.488	26.000	1.44
	Ca	187.702	1700.000	0.11
	Cr	9 499	7.900	1.20
	Fe	648.470	1200.000	0.54 -
	K	433.545	400.000	1.08
Index	Na 🦾	52.119	71.000	0.73
ele∎ents	Na	760.479	780.000	0.97
	Ni	8.221	5.000	1.64 +
	Pb	231.136	220.000	1.05
	Sb	0.594	5.600	0.11
	Sc	0.057	0.150	0.38
	Se	0.406	1.700	0.24
	1 TI	34.856	62.000	0.56 -
1.1.1	· V	6.675	8.700	0.77
	Zn	72.637	960.000	0.08
	C	10795.746	10600.000	1.02
	Cers	2128.732	2700.000	0.79
Total		16122.284	19518.050	0.83

Element		Calculated (ng/m³)	Observed (ng/#3)	<u>Calculated</u> Observed
	AI	466.560	410.000	1.14
	Br	7.012	4.500	1.56 +
	Ca	135.547	800.000	0.17
	Cr	7.862	7.900	1.00
4.	Fe	340.066	840.000	0.40
1. Sec. 19	K	299.957	1400.000	0.21
Index	Я́л	29.501	23.000	1.28
elements	Na	969.502	1000.000	0.97
	Ni	13.747	22,000	0.62 -
	Pb	40.539	1100.000	0.04
1	Sb	1.186	32,000	0.04
4	Sc	0.037	0.110	0.33
1997 - C. 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 19	Se	0.572	0.500	1.14
	1 TI	23.277	20.000	1.16
	Ŷ	13.359	13.000	1.03
	Źn	54.779	370.000	0.15
	C	5571.926	5500.000	1.03
1	Core	912.733	2000.000	0.46
Total	· · · · · · · · · · · · · · · · · · ·	8988.162	13543.010	0.66

MS 3

MS4

Element		Calculated (ng/m²)	Observed (ng/m³)	Calculated Observed
jndex elements	Al Br Ca Cr Fe K Mn Na Ni Pb Sc Sc Sc Ti Y Zn Cata Cara	480,183 20,840 180,013 10,874 625,162 300,474 57,935 823,559 16,849 122,555 0,639 0,033 0,424 23,555 21,214 71,855 8314,117 1522,801	$\begin{array}{c} 410.000\\ 9.500\\ 1300.000\\ 7.300\\ 1700.000\\ 1100.000\\ 12.000\\ 840.000\\ 18.000\\ 230.000\\ 10.000\\ 0.100\\ 0.100\\ 0.400\\ 65.000\\ 22.000\\ 1100.000\\ 8100.000\\ 8100.000\\ \end{array}$	$\begin{array}{c} 1.17\\ 2.19\\ ++\\ 0.14\\\\ 1.49\\ 0.37\\\\ 0.74\\ 0.98\\ 0.94\\ 0.56\\ -\\ 0.07\\\\ 0.38\\\\ 1.06\\ 0.36\\\\ 0.96\\ 0.07\\\\ 1.03\\ 0.48\\\\ \end{array}$
Total	•	12601.161	18185.300	0.69

Element		Calculated (ng/m²)	Observed (ng/m³)	<u>Calculated</u> Observed
	AI	716.630	820.000	0.87
	Br	25.460	15.000	1.70 +
	Ca	156.055	1500.000	0.10
	Cr	5.950	4.500	1.32
	Fe	405.389	940.000	0.43
Index	K	442.915	400.000	1.11
	Ma	29.717	34.000	0.87
elements	Na	1022.368	1100.000	0.93
	Ni	6.390	5.000	1.28
	Pb	140.459	140.000	1.00
	Sb	0.507	4.100	0.12
	Sc	0.057	0.140	0.41
	Se	0.361	0.350	1.03
	Ti	34.938	59.000	0.59 -
	V	5.699	6.300	0.90
a Alan a	Zn Cata Cara	49.285 9962.352 1827.459	370.000 9700.000 4000.000	0.13 1.03 0.46
Total		14831.991	19098.390	0.78

M S 5

		······		
Element		Calculated	Observed	<u>Calculated</u>
		(n s/m³)	(n g/m ¹)	Observed
	AI	723.439	740.000	0.98
	Br	7.945	7.200	1.10
	Ca	112.521	1300.000	0.09
	Cr	5.590	5.000	1.12
	Fe	344.264	450.000	0.77
	X	439.167	450.000	0.98
Index	ไปก่	25.428	21.000	1.21
elezents	Na	791.229	790.000	1.00
	Ni	6.493	15.000	0.43
	РЬ	44.405	40.000	1.11
	SÞ	0.845	3,100	0.27
	Sc	0.058	0.150	0.33
	Se	0.459	0.300	1.53 +
	Ji	35.642	51.000	0.70 -
	Y	3.398	3.400	1.00
	Zn	40.651	160,000	0.25
	C	4105.918	4000.000	1.03
	C	698.811	2000.000	0.35
Total		7386.262	10035.150	0.74

≧4.0 ≧2.0 ≧1.5 ≦0.7 ≦0.5 ≦0.25 (Calculated/Observed)

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(6) The results of the estimate by the CMB method in consideration of the secondary particle

Table 2-14 shows the production of the particulate matter (the diameter is less than 5 μ m) on earth—classified into natural products and artificial products—estimated by Ellsaesser³⁷⁾. Though the estimate is never accurate, it can be regarded as one of the criteria; the natural products are 69% of all particle matter and the secondary particles are 45%.

		The production of particulate matter: diameter is less than 5 μ m (unit: 10 ⁶ ton.)				
: .		Natural products	Artificial products			
Primary partcle						
Sea salt Soil Forest fire Volcano Factory, Plant, Incin	erator, etc.	500 100 5 25 —	150* 60* 			
Sub total	870 (100%)	630 (72%)	240 (28%)			
Secondary particle						
Sulphide Nitride Hydrocarbon		335 60 75	200 35 15			
Sub total	720 (100%)	470 (65%)	250 (35%)			
Total	1590 (100%)	1100 (69%)	490 (31%)			

Table 2-14 The Production of the Particulate Matter on Earth

* attending on the artificial actions indirectly

The secondary particle is a general term for the particulate matter changed from the emitted gas through chemical chain reactions. Some examples of emitted gas are sulfur compounds (SO₂ and H₂S, etc.), nitrogen compounds (NO_x and NH₃, etc.) and vegetable hydrocarbon (terpen, etc.).

In the following estimate, it is assumed that most of the secondary particles are nitrate and sulphate and that NO_3^- and SO_4^{2-} exist as ammonium salts. Further it is necessary for the estimate of the sulphate ion in the secondary particle to subtract the sulphate ion that originated in Sea salt (primary particle) from the total sulphate iron.

Then S, the concentration in Sea salt $[S_{sea}]$ is estimated with sea salt concentration based on the report by Mizobata²⁵ that indicates S is 2.6% in sea salt. So the contribution concentrations of the secondary particles are estimated with the following equation:

 $[NO_3^-]$: NO_3^- concentration on particulate matter measured by Low-volume sampler $[SO_4^{2-}]$: SO_4^{2-} concentration on particulate matter measured by Low-volume sampler

Table 2-15 shows the contribution rates of the secondary particle added to the contribution rates on particulate matter estimated by the CMB method with 7 emission sources (Table 2-12).

|--|

[First survey]					(%)
Component	HS 1	HS 2	HS 3	HS 4	HS 5
Sea sait Soil + Road dust Diesel automobile Gasoline aulomobile Iron and steel Ind. Fuel oil combustion Glass industry	4.5 41.0 34.8 5.6 2.1 0.4 0.1	8.9 29.3 36.8 1.9 2.7 0.6 0.1	4.5 23.8 28.5 3.5 10.7 0.9 1.0	6.5 43.1 37.8 3.6 1.8 0.2 -0.2	4.4 76.2 24.5 0.1 0.3 0.1 0.5
Sub Lotal	88.6	80.4	72.9	92.9	106.2
Secondary	12.5	19.1	16.1	14.7	10.4
Total	101.1	99.5	89.0	107.6	116.6

recipal annual

(%)

[Second Survey]					1 76 7
Component	HS 1	XS 2	XS 3	HS 4	MS 5
Sea salt Soil + Road dust Diesel automobile Gasoline automobile Iron and steel Ind. Fuel oll combustion Glass industry	12.2 41.6 32.7 0.8 2.0 0.3 0.4	22.6 13.7 29.0 -0.4 0.4 1.6 2.0	10.7 14.8 27.0 2.4 0.1 2.4 3.7	15.8 35.1 47.6 0.4 0.3 0.2 1.4	21.3 41.7 33.9 -0.2 -0.7 0.1 0.7
Sub total	89.8	68.9	61.1	100.9	96.9
Secondary	14.0	24.9	16.9	15.7	11,1
Total	103.8	93.8	78.0	116.6	108.0

[Third survey]			. '		(%)
Component	HS 1	HS 2	XS 3	HS 4	XS 5
Sea salt Soil + Road dust Diesel automobile Gasoline automobile Iron and steel Ind. Fuel oil combustion Glass industry	5.0 28.3 38.0 3.8 3.8 0.3 0.5	9.7 26.2 28.7 0.1 2.6 1.1 2.1	5.7 18.7 29.8 1.9 4.0 1.3 0.7	7.4 30.5 37.6 2.4 2.0 0.3 0.6	8.4 47.1 23.1 0.5 2.3 0.2 1.6
Sub total	79.8	70.4	62.1	80.7	83.3
Secondary	11.5	25.9	20.3	11.1	10.8
Tolaj	91.3	96.3	82.4	91.8	94.1

The result indicates that the total contribution rates are over 100% at some monitoring stations. This is because all SO_4^{2-} and NO_3^{-} on the particulate matter are regarded as secondary particles (ammonium salts). In addition, the results that the total contribution rates are under 100% at some stations may be due to production by unknown emission sources (most of it may due to slash and burn agriculture).

2.2.4 Consideration

The contribution rates of each emission source type—Sca salt, Soil+Road dust, Diesel automobile, Gasoline automobile, Iron and steel industry, Fuel oil combustion and Glass industry—on particulate matter are estimated by the CMB method (shown in Table 2-12), and the results of this estimate are considered as follows:

(1) Sea salt

The contribution rates of Sea salt are high at some monitoring stations: MS2, MS3 and MS4. This may be because these stations at near the Chao Phraya River (shown in Fig. 2-3). In addition, the contribution rates at MS2 are higher than others. This may be because MS2 is located on the leeward of the river, while the stream direction and wind direction are parallel at MS3 and MS4. With regard to the seasonal change, the contribution rates are high during the second survey period. This may be because the wind blows from the river frequently as shown in Fig. 2-4.

(2) Soil+Road dust

The reason why the contribution rates of the Soil+Road dust are high at MS1, MS4 and MS5 is shown as follows: MS1 locates at 90 m west from Sukhumvit Road (traffic volume is 77,000 cars/day) and MS4 locates at 100 m east from Sukhumvit Road (traffic volume is 35,000 cars/day), so these stations may be suffering from road dust. MS5—where the contribution rates of Soil+Road dust are highest—locates at 120 m south from Theparak Road (unpaved road). Furthermore, all around this station the surface soil is exposed. So this station may be suffering from road dust and blown-up soil.

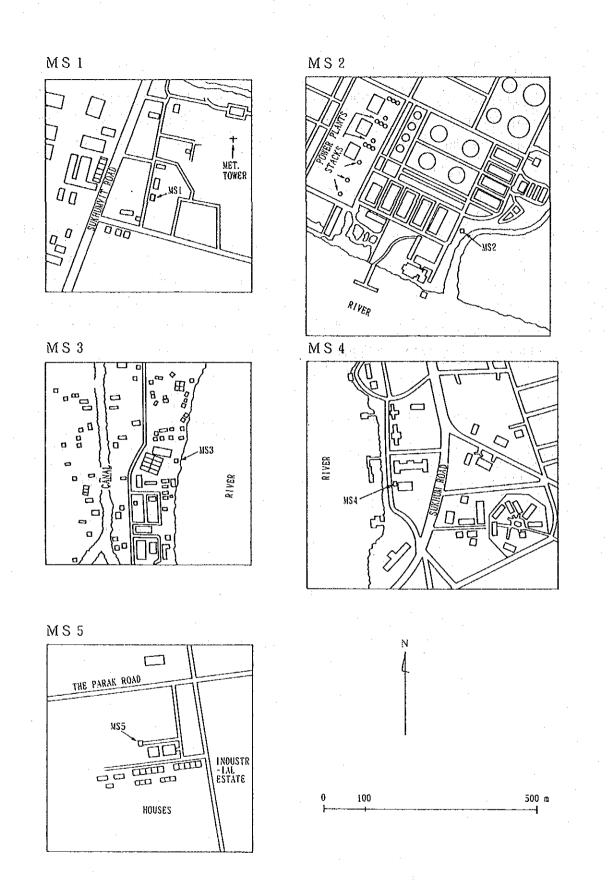


Fig. 2-3 Location of the Monitoring Sites

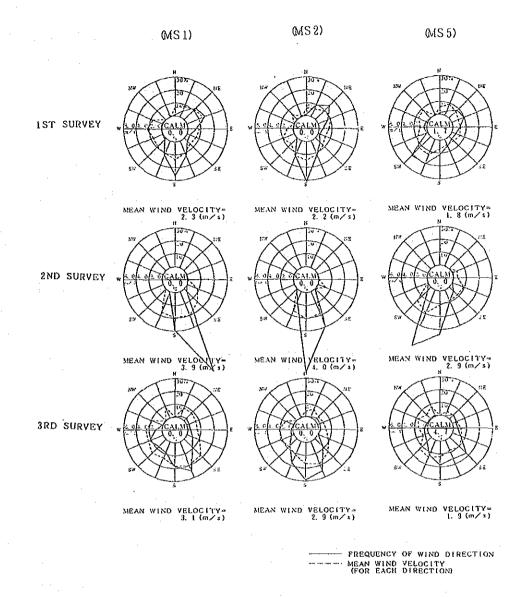


Fig. 2-4 Wind that Arose during the Short-term Field Survey

(3) Diesel automobile, Gasoline automobile

The reason why the contribution rates of Diesel automobile and Gasoline automobile are high at MS1 and MS4 may be the same as above. The contribution of Diesel car varies $23\sim48$ pct whereas that gasoline car maintains only $0\sim5$ pct.

(4) Iron and Steel industry

The reason why the contribution rates of the Iron and Steel industry are high at MS3 may be that the iron mill (electrosteel) stands on the other side of Chao Phraya River. The wind mostly blew from steel plant site (NE) in the 1st survey period, which is thought the cause of higher contribution. The frequency of NE winds was less in the 2nd and 3rd survey periods.

(5) Fuel oil combustion

Though the contribution rates of Fuel oil combustion are relatively high at MS2 and MS3, the absolute rates are low (about 2%). Furthermore, at the other stations the contribution rates are under 1%. Especially, the rates at MS5 are very low (about 0.1%). Besides, the contribution rates of Fuel oil combustion at MS2—which stands in the power plant ground—are low (about 1%) may be because of high chimney (104 m height).

(6) Glass industry

The contribution rates of Glass industry varies from 0.1% to 2% and have no regional character. However, to be considered is that aluminum smelting factory also emits same chemical components as those of glass factories, and both share the contribution.

(7) The contribution rates of natural products and the artificial producdts

Though it was not possible to distinguish between Soil (natural product) and Road dust (artificial product) in this estimate, the results show that the largest emission source type of artificial products is the Diesel automobile (black smoke in the exhaust gas) and the second emission source is Road dust and the contribution rates of Fuel oil combustion and the Iron and Steel industry are very low (several percent). However, as the ratio of natural products and artificial products varies seasonally, it can be regarded as fifty-fifty. This estimated result agrees with the common value measured in many countries.

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PART VI REMEDIAL EFFORTS AGAINST EMISSION SOURCE IMPROVEMENTS AND THEIR EFFECTIVENESS

1. Summary

In view of what is discussed in the previous Chapter, it is clear that the ambient concentrations of SO₂ and NO₂ in Samut Prakarn province today (as of 1988) meet the environmental standards of Thailand at all areas. However, if the 6th state economic and social development plan is completed and the succeeding similar plan are carried forward, it is most likely that environmental deterioration is inevitable as the result of such developments. Accordingly, we have first predicted the ambient concentrations of SO₂ and NO₂ for the future years of 1992 and 1999 assuming that the economic development is carried out without appropriate control measures taken for the emission sources. This revealed that NO₂ ambient concentration would exceed the environmental standard in 1999 in this area. Then, concrete remedial measures for emission sources and their effectiveness have been studied to improve NO₂ ambient concentrations in future years. In addition, while SO₂ ambient concentration will not exceed the environmental standard even if economic and social development is made progress, the contribution rates at high concentration points are greatly occupied by factories; in Thailand no SO₂ emission control for factories has presently been enforced, very likely causing a problem of unfairness among factories relating to SO₂ emission under the status quo. This part, therefore, discribes the methods of SO₂ emission control for factories and the forecast of ambient concentration of SO₂ after implementation of emission control in future (1999).

2. Emission Volumes of SO₂ and NO_x in Future Years without Countermeasures against Sources

2.1 Factory

Though it goes as a rule that the air pollutant emission volumes in future years have to be estimated based on the detailed emission source data reported by enterprises. In this study, however, the estimation was made by resorting to another method because such data were unavailable from enterprises. Namely, what are used as information for forecasting are the increase rate of the gross domestic product price (from the Thailand Development Research Institute; G.D.P. by Sector, July 1988) and the elastic modulus of energy. The fuel consumptions in future years were firstly predicted by using equation (2-1). The emission volumes of SO₂ and NO_x in future years were then calculated from these values multiplied by the emission factors of SO₂ and NO_x:

 $W_i = W_o \times (1 + e \cdot p)^n \quad$ (2-1) where

 W_t : fuel consumptions of factories in 1992 and 1999

 W_o : fuel consumptions of factories in 1988

p : increase rate of the gross product price

e : modulus of elasticity; 0.8

n : number of years

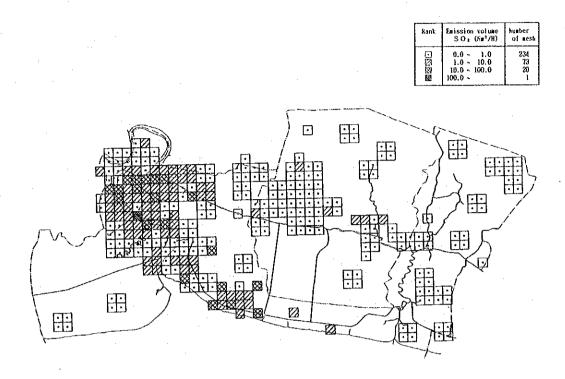
The values of p (annual rate) are 0.0578 for 1988~1991, 0.0513 for 1991~1996 and 0.0542 for 1996~2001. The increase rate of the fuel consumptions in 1992 and 1999 obtained by substituting these values for the equation (2-1) compared to 1988 base year are 1.192 and 1.590, respectively. Quantities of SO_2 and NO_x emitted from factories in future years obtained from such calculations are shown in Table 2-1 and Fig. 2-1. In estimation of the SO_2 and NO_x emission volumes in future years, the factories who will be established in the industrial estate constructed by Thai government in the Samut Prakarn industrial district, which are shown in Table 2-2, were also added as the future emission sources. The fuel consumptions of these factories were estimated by knowing the fuel consumption units per one employee (Chapter IV, Table 2-27).

Name of source of source		Туре	S 0 2	emission volu	me (ton/year)	NO _x emission volume (ton/year)			
		of source	1988	1992 (92/88)	1999 (99/88)	1988	1992 (92/88)	1999 (99/88)	
	Questionnaire return	point	13649	16269 (1.19)	21701 (1.59)	8108	9665 (1.19)	12892 (1.59)	
Stationary	Questionnaire nothing	area	4681	5580 (1.19)	7443 (1.59)	712	848 (1.19)	1132 (1.59)	
sources -	Industrial estate	arca		298 ()	298 (-)		28 (—)	28 (-)	
	Sub tot	al	18330	22147 (1.21)	29442 (1.61)	8820	10541 (1.20)	14052 (1.59)	
Roa	id way	line	1474	1829 (1.24)	2261 (1.53)	7812	10448 (1.34)	15119 (1.94)	
	Vessels (sailing)	point	1263	1505 (1.19)	2007 (1.59)	1623	1935 (1.19)	2581 (1.59)	
Vessels and Ferryboats	Ferryboats (anchoring)	point	8	11 (1.38)	17 (2.16)	26	36 (1.38)	57 (2.16)	
	Ferryboats (sailing)	point	59	82 (1.38)	128 (2.16)	221	304 (1.38)	476 (2.16)	
	Sub tot	al	1330	1598 (1.20)	2152 (1.62)	1870	2275 (1.22)	3114 (1.67)	
	TOTAL		21134	25574 (1.21)	33855 (1.60)	18502	23264 (1.26)	32285 (1.74)	

Table 2-1 SO2 and NOx Emission Volume Emitted from Samut Prakarn Prefecture in Future Years	Table 2-1 SO2 and NO,	x Emission Volum	e Emitted from	Samut Prakarn	Prefecture in Future Years
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		· · · · ·							
Site	Factory	Product	Code	Area	Number of em ployee	Fuel gener. (0,01	Fuel consu- mption	SO: esti- ssion volume	NO x egi- ssion voluse
	SiteFactory nameProductCodeArea codeof em- ployce (0, 0) (m²)gone - ployce (0, 0) (m²)consu- mption (m²)consu- mption (m²)consu- mption (m²)consu- mption (m²)consu- mption (ki/y) (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption (ki/y)consu- mption 	(t/y)							
Bangplee Loduct-	Petrochemi-		42	64,488	160	250	- 400	18.60	1.74
	(Thailand)	Brass & Bronze valve	64 (8)	1,600	150	72	108	5.02	0.47
		D (b.).	10(2)	5,064	(163)	100	1.010	75.14	
Thanawat O.,LTI	O.,LTD	Prawn Unip	10(2)	6,384	206	438	1,010	15.14	7.03
D	Southeast	C	7(1)	13,340	90		0.00	100.00	15.05
		tanned 1000	7(1)	6,616	700	4.93	3,460	160.89	15.05
Indust- rial L Estate	(Thailand)	Tire & Tube	51	26, 194	205	250		23.85	2.23
	Dyeing	Dyeing	22(2)	11,830	200	155	310	14.42	1.35
	TOTAL							297.92	27.81

Table 2-2 Summary of Factories Planned for Construction



SO₂ in 1999

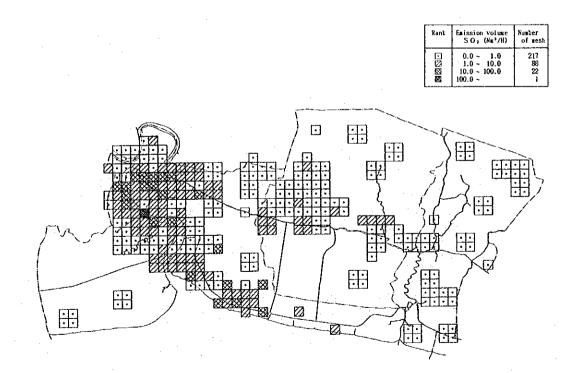
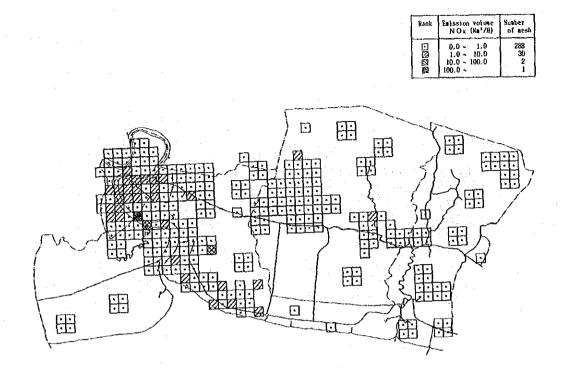


Fig. 2-1(1) SO₂ Emission Volume by Mesh Emitted from Factories



NO_x in 1999

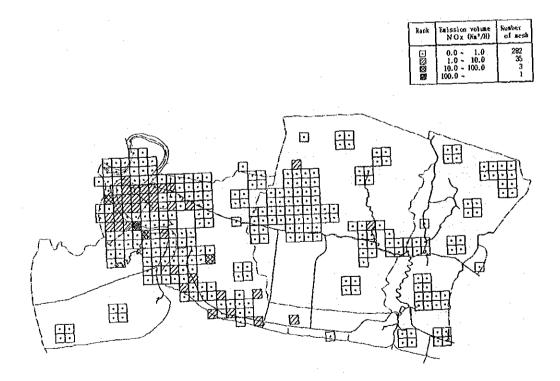


Fig. 2-1(2) NO_x Emission Volume by Mesh Emitted from Factorics

2.2 Vessels

The growth of the number of vessels was considered proportional to the growth of the gross product price and thus the number of vessels were estimated in the same manner as the factory. Then this number was multiplied by the SO_2 and NO_x emission factor for calculation of the SO_2 and NO_x emission volume of the coming years. The result is shown in Table 2-1 and Fig. 2-2.

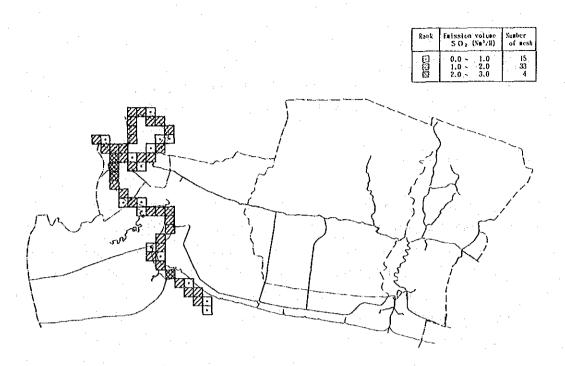
2.3 Vehicles and Ferryboats

Based on the number of cars for year 1991 and 2001 listed in the forecast of the number of cars owned in Samut Prakarn province (Mr. Mikimasa Yoshida; Asia Economy Institute, Ms. Chuta Manasphaibul; Associate Professor, Faculty of Economics, Chulalongkorn University, Ms. Orajit Singkalavanich; Director, Planning Division, Dept. of Export Promotion, Ministry of Commerce, 1980 Economic Development Policy in Thailand, Asia Economy Institute, 1989), the number of cars for 1992 and 1999 was estimated and this number was multiplied by the SO₂ and NO_x emission factors to calculate the SO₂ and NO_x emission volume from cars in the future. The result is shown in Table 2-1 and in Fig. 2-3. The growth of the number of cars owned is as shown in Table 2-3.

Valiata tara	Growth of numb	per of cars owned	- Remarks			
Vehicle type	1992/1988	1999/1988				
Light vehicle Heavy vehicle	1.241	L.53 <u>2</u>	Growth rate of number of trucks and buses was applied.			
Gasoline LPG	1.529	2.725	Growth rate of number of cars was applied.			
Motor cycle	1.526	3.034	Growth rate of number of motor bicycles was applied.			

Table 2-3	Growth	of Number	of Cars	Owned

Future emission volumes of SO_2 and NO_x from ferry boats were calculated as follows: We assumed that the number of ferryboats in operation was proportional to the number of cars running on Puchao Saming Phla Road and that it increased at rates of 1992/1988=1.376 and 1999/1992=2.155. On the basis of this assumption, the number of ferryboats to be operated in future was calculated and then, to calculate the SO_2 and NO_x emission volume, that numbers were multiplied by the emission factors of SO_2 and NO_x . The results are shown in Table 2-1 and Fig. 2-2.



NO₂ in 1999

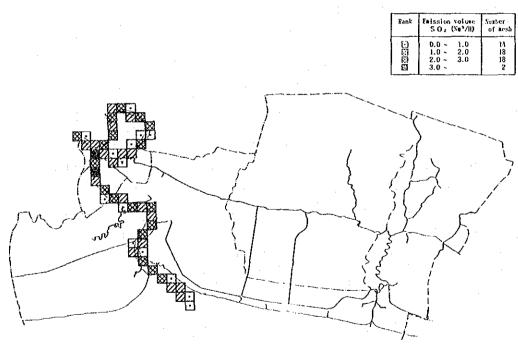
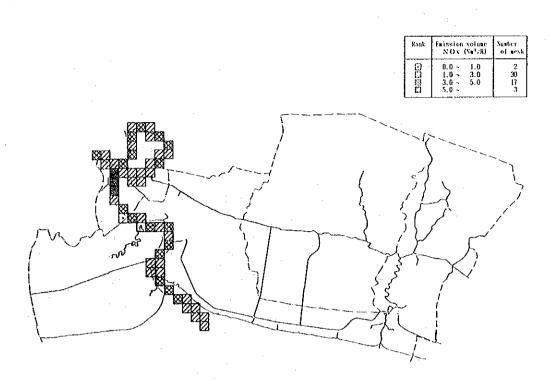


Fig. 2-2(1) SO₂ Emission Volume Emitted from Vessels and Ferryboats



NO_x in 1999

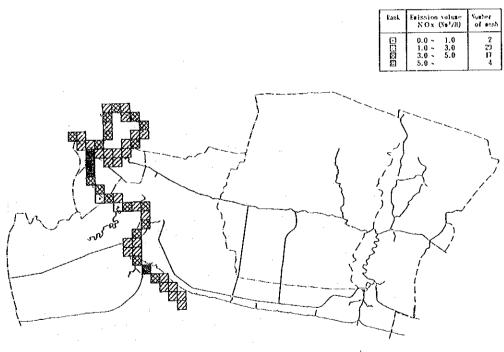
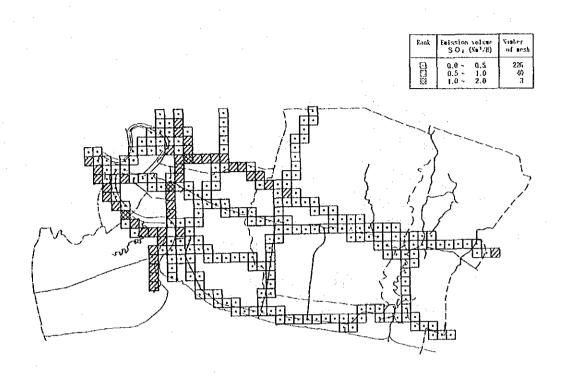


Fig. 2-2(2) NO_x Emission Volume Emitted from Vessels and Ferryboats



SO₂ in 1999

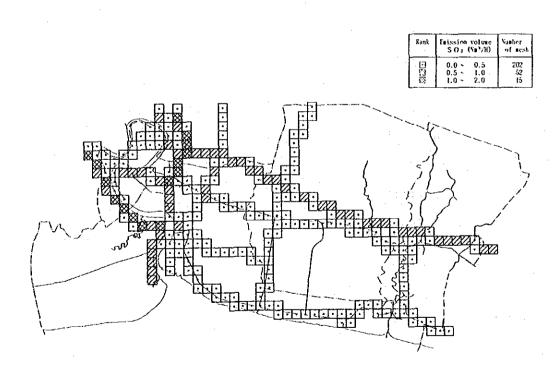
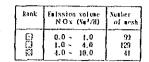
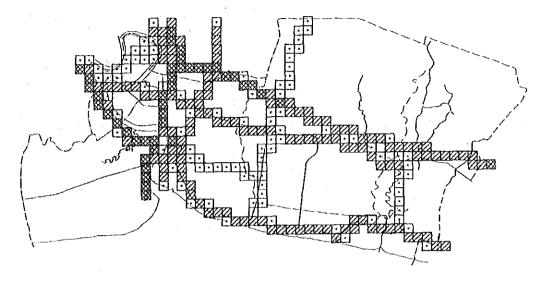


Fig. 2-3(1) SO₂ Emission Volume Emitted from Vehicles







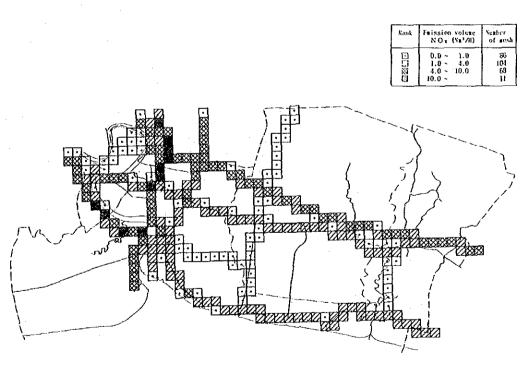
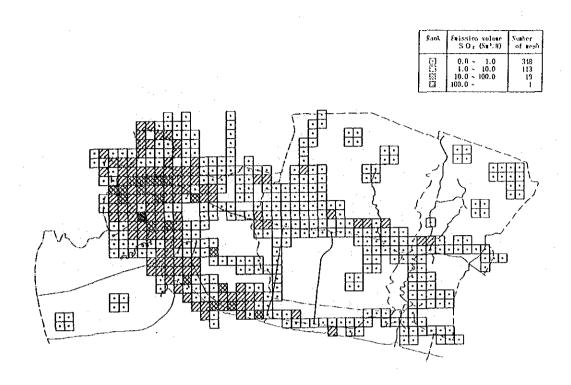


Fig. 2-3(2) NO_x Emission Volume Emitted from Vehicles

2.4 SO₂ and NO_x Emission Volumes Emitted from the Whole Samut Prakarn Region in Future Years in the Case of Taking No Countermeasures for Emission Sources

The SO₂ and NO_x emission volume from factories, cars, vessels, and ferries in Samut Prakarn Province for the case where there are no countermeasures for emission sources were summed up. This result is shown in Table 2-1. The SO₂ and NO_x emission volumes from the whole Samut Prakarn Province by mesh are shown in Fig. 2-4. These results show that the total emission volumes of SO₂ and NO_x in 1992 are 25,574 and 23,264 metric ton/year respectively. Those figures of 1992 compared with emission volumes in 1988 (SO₂; 21,134 t/y, NO_x; 18,502 t/y) show the increase of both pollutants, 1.21 times in SO₂ and 1.26 times in NO_x against the base yeaer of 1988. In similar manner, the SO₂ and NO_x emission volumes in 1999 were estimated to be 33,855 and 32,285 tons per year respectively, or 1.60 and 1.74 times increase against the base year of 1988.



SO₂ in 1999

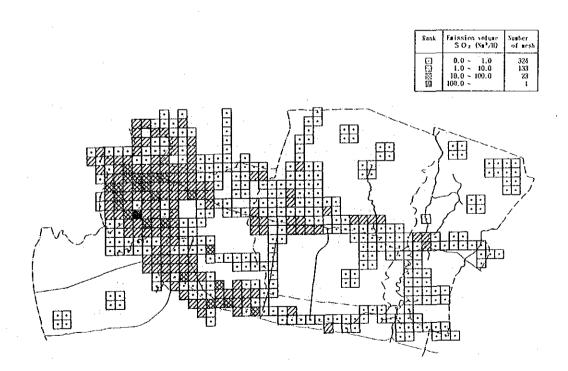
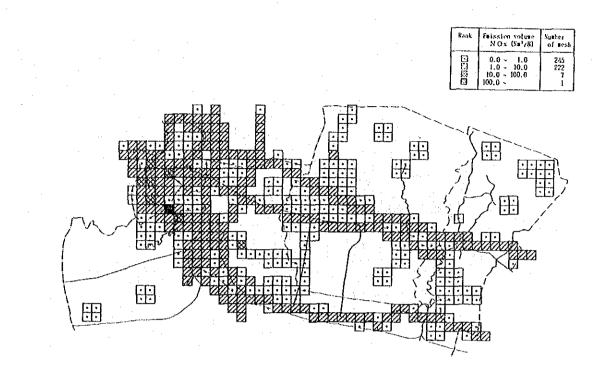


Fig. 2-4(1) SO₂ Emission Volume Emitted From All Emission Sources



NO_x in 1999

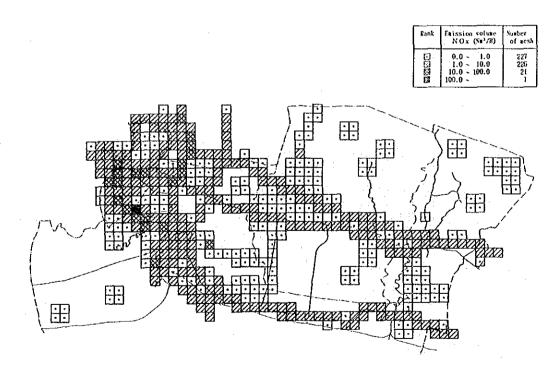


Fig. 2-4(2) NO_x Emission Volume Emitted From All Emission Sources

3. Forecasting of Ambient SO₂ and NO₂ Concentrations in the Case of Taking No Countermeasures Taken against Emission Sources

3.1 Modeling of Smoke Sources Data

In order to predict SO_2 and NO_2 ambient concentration in the future years by using SO_2 and NO_x emission volume mentioned in the previous chapter as input data, the data of factory smoke sources (stationary point sources) were modeled. Namely, we supposed that the measures for increasing the fuel consumption of existing facilities in factories are taken according to the following priority order. A list of measures for increasing the fuel consumption is shown in Table 3-1:

- (1) Increase of load factor
- (2) Extension of operating hours
- (3) Fuel distribution to the same facilities
- (4) Increase of facilities with the same scale as the existing ones

Measures	Year of 1992	Year of 1999
 Increase of load factor 	First, increase the load factor without c factor normally leads to the increase of	hanging the operating hours. Increase of the load the flue gas volume.
② Extension of operating hours	If the step ① can't absorb the increment hours.	t of the fuel consumption, extend the operating
③ Fuel distribution to the same	If the steps (1) and (2) can't absorb it, di capacity, if there is one.	stribute the fuel to a facility with a surplus burning
facilities	(Put one unit of facilities out of service into operation.) 3-47-3	 1-64-3: Put facilities out of service into operation.) 3- 5-2: Put facilities out of service into operation.) 3- 9-3: Has a surplus capacity.) 3-14-4: Put facilities out of service into operation.) 3-47-3: Put facilities out of service into operation.) 3-57-2: Put facilities out of service into
	· · · · · · · · · · · · · · · · · · ·	operation.)
(4) New cincrease of	If steps (1), (2) and (3) can't apply it, new	vly increase the facilities.
facilitics	2-12-101 3- 4-101 2 facilities above were newly increased.	2-17-101 3- 4-101 3-14-101 3-23-101, 102, 103 3-33-101 3-42-101 3-57-103
		3-77-101 3-78-101 3-105-101 15 facilities above were newly increased.

Table 3-1 Meas	ures for	Increasing	the Fuel	Consumption _
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3.2 Diffusion Condition

The simulation model which was used to predict the future ambient pollutant concentrations is an atmospheric diffusion model which was mentioned in Chapter V since that model can well reproduce the actually measured present ambient pollutant concentrations. For the meteorological condition necessary for forecasting the future ambient pollutant concentrations, the same condition as applied to calculation of the present concentration was employed on the assumption that the average annual meteorological condition will not significantly change in future, as well.

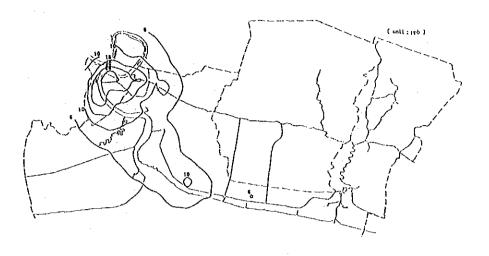
3.3 Comparison of Ambient Pollutant Concentrations of the Whole Area to the Environmental Control Standards of Thailand

We predicted the annual average ambient concentrations of SO_2 , NO_x and NO_2 in all areas of Samut Prakarn prefecture in 1992 and 1999. The results are shown in Fig. 3-1 and Table 3-2. The number of mesh by concentration rank is also shown in Table 3-3. These results revealed that if no countermeasures for emission sources are taken, as indicated in Table 3-4, both SO_2 and NO_2 fulfilled the environmental standards of Thailand in all areas in terms of current figures (1988), whereas NO_2 would exceed the standards at 31 points in 1999. Fig. 3-2 shows the points where NO_2 would exceed the environmental standard.

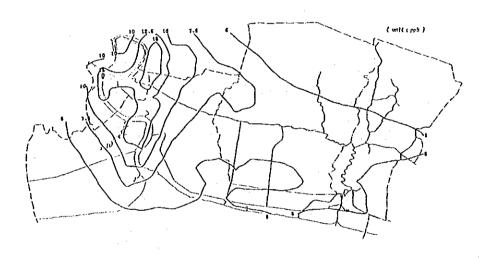
3.4 Contribution Rate by Emission Sources

The points where NO₂ ambient concentration will exceed the environmental standards in future are as shown in Fig. 3-2. The contribution rates by emission sources of high contribution-top 8 points were calculated, and the results are shown in Table 3-5. While the ambient concentration of SO₂ will not exceed the environmental standard, the table also shows the contribution rates by emission sources at high concentration-top 8 points for SO₂ ambient concentration.

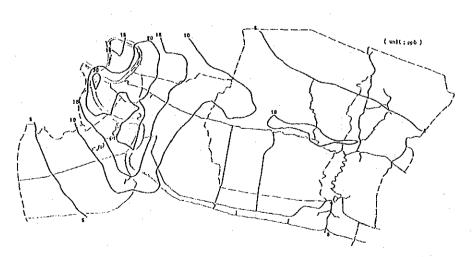
According to these results, the contribution rates by emission sources at the points where NO_2 concentration will exceed the environmental standard in 1999 are 2.6 to 7.6% for factories, 32.4 to 83.4% for cars, 2.2 to 11.4% for ships, and 0.1 to 35.6% for ferryboats, demonstrating a great contribution rates by cars. This trend is same for the rates in 1992. As for SO₂, contribution by factories occupies about 75 to 88% in both 1992 and 1999 against 6% for cars.

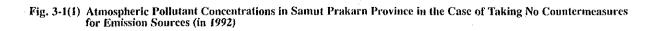


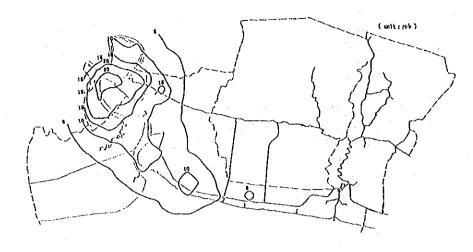
 NO_2



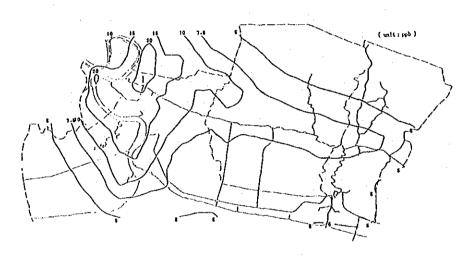












 NO_x

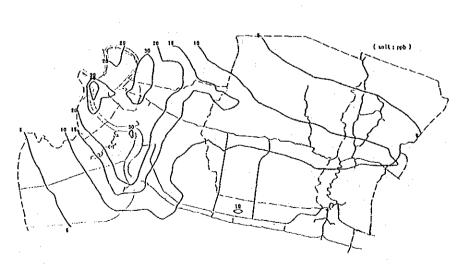


Fig. 3-1(2) Atmospheric Pollutant Concentrations in Samut Prakarn Province in the Case of Taking No Countermeasures for Emission Sources (in 1999)

Table 3-2(1) Average Annual SO₂ Concentrations in Samut Prakarn Province in the Case of Taking No Countermeasures for Emission Sources (Unit: 0.1 PPb)

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Table 3-2(3) Average Annual NO_x Concentrations in Samut Prakarn Province in the Case of Taking No Countermeasures

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Table 3-3 Number of Mesh by Rank of Air Pollutant Concentration (Case of Taking No Countermeasures)

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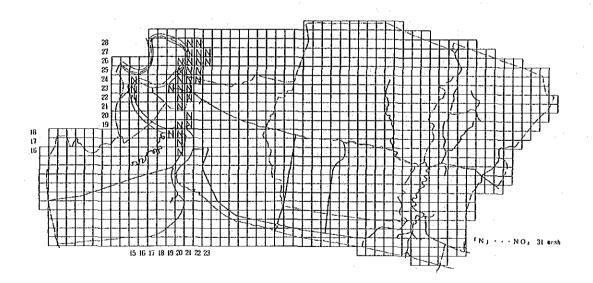
i			<u> </u>					
Rank of	Number of mesh							
cocentra- tion (ppb)	1988	1992	1999					
0.0~ 5.0	977	929	885					
5.0~10.0	128	154	150					
10.0~15.0	28	42	67					
15.0~20.0	21	16	24					
20.0~25.0	- 5	14	13					
25.0~30.0	0	4	13					
30.0~35.0	0	0	- 6					
35.0~40.0	0	0	1					
TOTAL	1159	1159	1159					

			(NO ₂)
	Rank of	Numb	er of	nesh
9	cocentra- tion (ppb)	1988	1992	1999
5	0.0~ 5.0	674	476	300
0	5.0~ 7.5	305	429	437
7	7.5~10.0	109	104	190
4	10.0~12.5	64	-93	68
3	12.5~15.0	. 7	46	55
3	15.0~17.5	Ò	10	68
6	17.5~20.0	0	. 1	28
1	20.0~22.5	0	0	7
9	22.5~25.0	0	0	6
	TOTAL	1159	1159	1159

· · ·		(NO:	k)						
Rank of	Number of mesh								
cocentra- tion (ppb)	1988	1992	1999						
0.0~ 5.0	277	223	169						
5.0~10.0	676	643	544						
10.0~15.0	116	141	228						
15.0~20.0	79	92	68						
20.0~25.0	9	51	68						
25.0~30.0	2	7	61						
30.0~35.0	0	1	13						
35.0~40.0	0	1	- 6						
40.0~45.0	0	0	0						
45.0~50.0	0	. 0	1						
50.0~55.0	0	0	1						
TOTAL	1159	1159	1159						

 Table 3-4 Number of Mesh at Which Environmental Standards Are Exceeded (Case of Taking No Countermeasures)

Year	SO ₂	NO ₂
1988	0	0
1992	0	0
1999	0	31



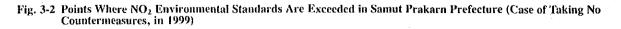


 Table 3-5(1)
 Contributive Concentration by Emission Sources at High SO2
 Concentration Points (Case of Taking No

 Countermeasures, in 1992)
 Countermeasures, in 1992)

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nk 6 IX, IY=15, 22)	Rate	85	400000000000000000000000000000000000000	21. P	2040040	100.0		Rate Soft	1-0000000000000000000000000000000000000	25.3 61.1	00000000000000000000000000000000000000	100.0
	Conce.	contr (ppb)		5.328 12.314	0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.100 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.000000	23.831	3, 23)	Conce. of contr. (ppb)		14:58 14:58	800000 802883900 84210883001	23.075
	f source	Coun Fact Sta. ty No. No.		ining stacks sub total	Factory (area source) Factory(industrial estate) factory(industrial estate) Vessels (sailing) Ferrybats (anchoring) Back ground	OTAL	Rank 8 IX, IY=18,	Type of source BD) Coun Fact Sta.	బంటుటుటుటుటు వేనేనయార్గా	Remáining stacks Sub total	ca source) ustrial estate) iling) anchoring) (sailing)	TOTAL
(Rank	Type of	SEQ) (SER)	විදුකු විදී විදුකු විදී විදුකු විදී	Remainin Sub	Factory (ar Factory (ind Roadways Vessels (sa Ferryboats Ferryboats Back ground	TC	(Ra	Type o	ලිකෙතනානෙක දුළු විදු	Rens	Factory (are source) factory(industrial es Ractory(industrial es Racdages Vessels (sailing) Ferrybats (ancing Perrybats (sailing) Back ground	1.
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	Rate	S.	194444000-01- 1000000000-01-	22.1	2040000 9000004 9000004	24.075 100.0		Solt Bate		909 899	80410-0 806.0-27	100.0
[Rank 5 IX, IY=17, 24]	Conce.	contr (ppb)		5.473	001-1000 0000 0000 0000 0000 0000 0000		[Rank 7 IX, IY=15, 21]	Conce. of contr (ppb)		11.530	-00-00000000000000000000000000000000	23.095
	Type of source	Šta. No.	<u></u>	Remaining stacks Sub total) state) g)	TOTAL		Sta. No.	ന ്നാ പ്പംപാപ്പംപ 	cks	state) state) g)	
		y Fact			Factory (area source) factory (ndustrial estate) foctory (industrial estate) Vessels (sailing) Ferrybasts (anchoring) Back ground Back ground			source In Fact	<u>444</u> ±5008244	Remaining stacks Sub total	source trial e ing) mchorir ailing)	LAL
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8	Conçe.			15.512 28	1-0-1-0-00 88888888888 888888888888888 88888888	26.338 100.	ສ	Conce. Rat of contr. cont (pob)		15.253 24. 13.438 53.	00000000000000000000000000000000000000	25.286 100.
(, IY=16,23)	Conce.	Sta. contr. No. (ppb)	60.400.400.000	6.353 15.512	ate) 7.558	88		Conce. Sta. contr No. (ppb)		15.253 24.	င်းဆင်းသင် င်းဆင်းသင် င်းသို့သို့သို့ င်းသို့သို့သို့ င်းသို့သို့သို့ င်းသို့သို့ င်းသင်းသင် င်းသို့ င်းသင် င် င် င် င် င် င် င် င် င် င် င် င် င	236 100.
2 IX, IY=16, 23)		Fact Sta. contr. No. No. (ppb)	Ба <u></u>	6.353 15.512	ate) 7.558	AL 26.33	IX, IY=15,	Parte Conce. Fact Sta. contr No. No. (pob)	10-44-40-20-20-20-20-20-20-20-20-20-20-20-20-20	15.253 24.	င်းဆင်းသင် င်းဆင်းသင် င်းသို့သို့သို့ င်းသို့သို့သို့ င်းသို့သို့သို့ င်းသို့သို့ င်းသင်းသင် င်းသို့ င်းသင် င် င် င် င် င် င် င် င် င် င် င် င် င	L 25.236 100.
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	source	Fact Sta. contr. No. No. (ppb)	<u>−∞∞∞∞∞∞∞∞∞∞</u> №∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞	maining stacks 6.353 Sub total 15.512	ate) 7.558	0TAL 26.338	IX, IY=15,	Parte Conce. Fact Sta. contr No. No. (pob)	<u>- ఆలుతుర్ర- అంద్రి</u> బయిదుడుడుడులు గర్రెడిడిడి లా చెప్పెనిజిని లం చిత్రం రాశింతం లా రాశింతం రాశింతం రాశింతం లా రాశింతం రాశిం రాశింతం రాశింతం రాశం రాశింతం రాశం రాశం రాశింతం రాశింతం రాశిం	15.253 24.	င်းဆင်းသင် င်းဆင်းသင် င်းသို့သို့သို့ င်းသို့သို့သို့ င်းသို့သို့သို့ င်းသို့သို့ င်းသင်းသင် င်းသို့ င်းသင် င် င် င် င် င် င် င် င် င် င် င် င် င	L 25.236 100.
	of source	Coun Fact Sta. contr ty No. No. (ppb)	₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩	maining stacks 6.353 Sub total 15.512	rea source) dustrial estate) 0.000 aniling) a (anchoring) 0.002 a (sailing) 0.002 a (sailing) 0.100	0TAL 26.338	IX, IY=15,	Type of source Conce. SEQ) Coun Fact Sta. confr ty No. No. Gebb	55 57 57 57 57 57 57 57 57 57	15.253 24.	Factory (area source) 5.787 22. Factory (industrial estate) 0.006 0. Roadway (industrial estate) 0.006 0. Vessels (aniling) 2.201 10. Ferryboats (aniling) 0.2020 1. Back ground (aniling) 0.2020 0.	L 25.236 100.
	of source	SEQ) Coun Fact Sta. contr ty No. No. (ppb)	<u>−∞∞∞∞∞∞∞∞∞∞</u> №∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞∞	maining stacks 6.353 Sub total 15.512	rea source) dustrial estate) 0.000 aniling) a (anchoring) 0.002 a (sailing) 0.002 a (sailing) 0.100	100.0 TOTAL 26.33	IX, IY=15,	e of source Conce. Of Coun Fact Sta. contr ty No. No.	a.4.4.4.6.000000000000000000000000000000	15.253 24.	28.0 Factory (area source) 5.737 22. 0.0 Factory (industrial estate) 5.006 0. 1.1 Factory (industrial estate) 0.006 0. 1.1 Factory basis (sailing) 0.278 10. 0.1 Factry basis (sailing) 0.210 0. 0.1 Factry basis (sailing) 0.210 0.	100.0 TOTAL 25.286 100.
(Rank 2	Type of source	contr. SED) Coun Fact Sta. contr (%) to No. No. (pob)		Remaining stacks 6.353 Sub total 15.512	7.188 35.7 Factory (area source) 7.58 0.006 0.0 Pactory (industrial estate) 0.000 2.180 0.0 Pactory (industrial estate) 0.000 2.190 0.4 Pactory (industrial estate) 0.000 2.190 0.4 Pactory (industrial estate) 1.763 0.005 0.1 Pactory backs (sailing) 1.763 0.10 0.004 Pactryboats (aniling) 0.004 0.10 0.004 Pactryboats (sailing) 0.166	26.849 100.0 TOTAL 26.338	.23) [Rank 4 IX, IY=15,	Type of source Conce. SEQ) Coun Fact Sta. confr ty No. No. Gebb	0.000000000000000000000000000000000000	Remaining stacks 6.253 24. Sub total 13.433 53.	7.155 28.0 Factory (area source) 5.787 22. 0.002 0.0 Ractory (industrial estate) 5.787 22. 1.002 Reactory (industrial estate) 0.006 0.006 0.006 0.006 1.002 9.0 Reactory (industrial estate) 0.006	25.567 100.0 TOTAL 25.286 100.
(Rank 2	Rate Type of source	Sta. contr. contr. SED Coun Fact Sta. contr. No. (ppb) Cost Contr. (ppb)		5.335 22.0 Remaining stacks 6.353 15.335 57.3 Remaining stacks 15.512	7.188 35.7 Factory (area source) 7.58 0.006 0.0 Pactory (industrial estate) 0.000 2.180 0.0 Pactory (industrial estate) 0.000 2.190 0.4 Pactory (industrial estate) 0.000 2.190 0.4 Pactory (industrial estate) 1.763 0.005 0.1 Pactory backs (sailing) 1.763 0.10 0.004 Pactryboats (aniling) 0.004 0.10 0.004 Pactryboats (sailing) 0.160	26.849 100.0 TOTAL 26.338	.23) [Rank 4 IX, IY=15,	Conce. Rate Type of source Conce. C	0120201-400- 0120200-000 0120-0000 0120000	5.433 30.5 Remaining stacks 15.233 33.	7.155 28.0 Factory (area source) 5.787 22. 0.002 0.0 Ractory (industrial estate) 5.787 22. 1.002 Reactory (industrial estate) 0.006 0.006 0.006 0.006 1.002 9.0 Reactory (industrial estate) 0.006	25.567 100.0 TOTAL 25.286 100.
1X, 1Y=16, 24) [Rank 2	Rate Type of source	Fact Sta. contr. contr. SED Com Fact Sta. contr. No. Contr. Contr. No. Contr. Contr. No. Contr. Contr.	10 10 10 10 10 10 10 10 10 10	5.335 22.0 Remaining stacks 6.353 15.335 57.3 Remaining stacks 15.512	7.188 35.7 Factory (area source) 7.58 0.006 0.0 Pactory (industrial estate) 0.000 2.180 0.0 Pactory (industrial estate) 0.000 2.190 0.4 Pactory (industrial estate) 0.000 2.190 0.4 Pactory (industrial estate) 1.763 0.005 0.1 Pactory backs (sailing) 1.763 0.10 0.004 Pactryboats (aniling) 0.004 0.10 0.004 Pactryboats (sailing) 0.160	26.849 100.0 TOTAL 26.338	3 IX, IY=17, 23) [Rank 4 IX, IY=15,	WICE Conce. Rate Type of source Conce. Rect Sta. contr. contr. SED Coun Fact Sta. contr No. No. No. No. No. Cerb.	1111444 - 31 - 31 - 31 - 31 - 31 - 31 -	5.433 30.5 Remaining stacks 15.233 33.	7.155 28.0 Factory (area source) 5.787 22. 0.002 0.0 Ractory (industrial estate) 5.787 22. 1.002 Reactory (industrial estate) 0.006 0.006 0.006 0.006 1.002 9.0 Reactory (industrial estate) 0.006	25.567 100.0 TOTAL 25.286 100.
(Rank 2	of source Conce. Rate Type of source	Coun Fact Sta. contr. contr. contr. SED Coun Fact Sta. contr. ty No. No. (ppb) Coff.		22.0 Remaining stacks 6.353 57.3 Sub total 15.512	7.188 35.7 Factory (area source) 7.58 0.006 0.0 Pactory (industrial estate) 0.000 2.180 0.0 Pactory (industrial estate) 0.000 2.190 0.4 Pactory (industrial estate) 0.000 2.190 0.4 Pactory (industrial estate) 1.763 0.005 0.1 Pactory backs (sailing) 1.763 0.10 0.004 Pactryboats (aniling) 0.004 0.10 0.004 Pactryboats (sailing) 0.160	26.849 100.0 TOTAL 26.338	[X, IY=17, 22] [Rank 4 [X, IY=15,	e of source Conce. Rate Type of source Conce. Coun Fact Sta. contr. contr. SED Coun Fact Sta. contr ty Vo. No. (pob)	0120201-400- 0120200-000 0120-0000 0120000	23.5 Remaining stacks 16.233 24. Sub total 13.438 S3.	7.155 28.0 Factory (area source) 5.787 22. 0.002 0.0 Ractory (industrial estate) 5.787 22. 1.002 Reactory (industrial estate) 0.006 0.006 0.006 0.006 1.002 9.0 Reactory (industrial estate) 0.006	25.567 100.0 TOTAL 25.286 100.
1X, 1Y=16, 24) [Rank 2	source Conce. Rate Type of source	Fact Sta. contr. contr. SED Com Fact Sta. contr. No. Contr. Contr. No. Contr. Contr. No. Contr. Contr.	 силиски склонование б	5.335 22.0 Remaining stacks 6.353 15.335 57.3 Remaining stacks 15.512	25.7 Factory (area source) 7.588 0.0 Rectory (industrial estate) 0.000 0.1 Rectory (industrial estate) 1.753 10.4 Ferryboats (sailing) 1.753 0.1 Ferryboats (sailing) 0.004 0.3 Ferryboats (sailing) 0.004 0.4 Ferryboats (sailing) 0.156 0.4 Beck from the formation (sailing) 0.156	26.849 100.0 TOTAL 26.338	3 IX, IY=17, 23) [Rank 4 IX, IY=15,	WICE Conce. Rate Type of source Conce. Rect Sta. contr. contr. SED Coun Fact Sta. contr No. No. No. No. No. Cerb.	దుటుటుటుటుటులు 	5.433 30.5 Remaining stacks 15.233 33.	28.0 Factory (area source) 5.737 22. 0.0 Factory (industrial estate) 5.006 0. 1.1 Factory (industrial estate) 0.006 0. 1.1 Factory basis (sailing) 0.278 10. 0.1 Factry basis (sailing) 0.210 0. 0.1 Factry basis (sailing) 0.210 0.	25.567 100.0 TOTAL 25.286 100.

Table 3-5(2) Contributive Concentration by Emission Sources at High NO₂ Concentration Points (Case of Taking No Countermeasures, in 1992)

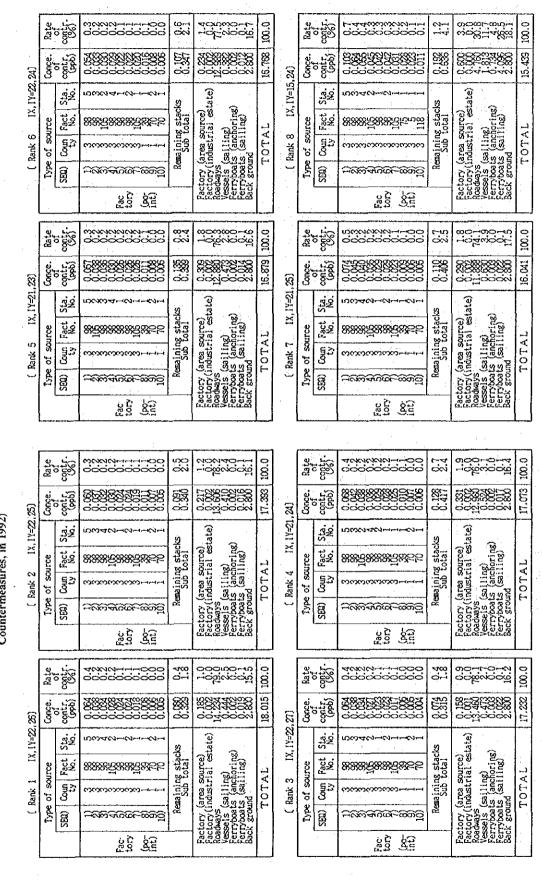
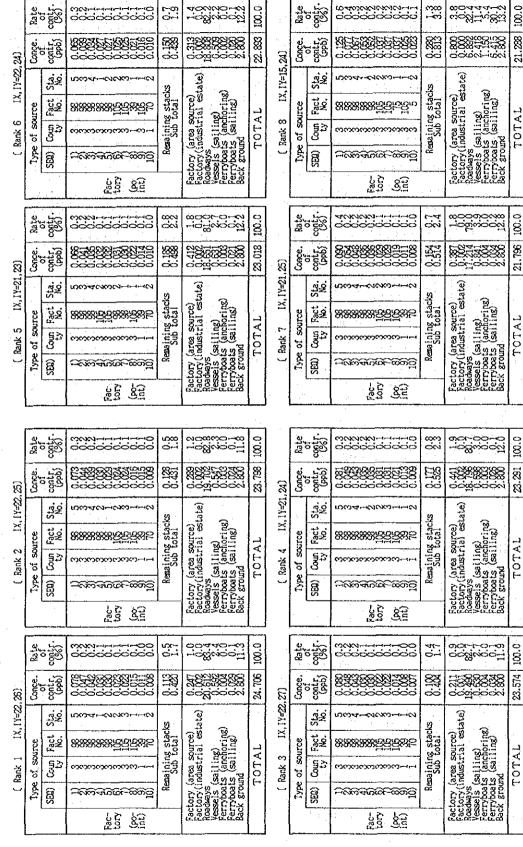


Table 3-5(3) Contributive Concentration by Emission Sources at High SO₂ Concentration Points (Case of Taking No Countermeasures, in 1999)

			·						1997 - A.			
	Rate Serie	1044400000	888 7-55	80490000	100.0		Rate	Sites	44400000000000000000000000000000000000	6.98 889	2000000	100.01
24)	Conce. of contr (ppb)		1.270	0.0110008 0.0110008 0.01110008 0.01110008 0.001110008 0.00111008 0.0011008 0.0011008 0.0011008 0.00008 0.0008 0.00008 00000000	31.059	ିଞ୍ଚ	Conce.	contr (ppb)		1.874	800-1-000 872875000 877875000	29.453
(Rank 6 IX, IY=17, 24,	Type of source SEQ) Coun Fact Sta.	55 85 	Remaining stacks Sub total	Factory (area source) factory (industrial estate) Reachays (sailing) Vessels (sailing) Ferryboats (anchoring) Ferryboats (sailing) Back ground	TOTAL	(Rank 8 IX, IY=18, 23)	Type of source	SEQ) Coun Fact Sta. ty No. No.	⁵ ⁶ ⁵ ³ ⁶ ⁶ ⁵ ⁶ ⁵ ⁶ ⁵ ⁶ ⁵ ⁶ ⁵ ⁶	Remaining stacks Sub total	Factory (area source) Factory (industrial estate) Ractory (industrial estate) Nessels (sailing) Ferryboats (anting) Ferryboats (anting) Beck ground	TOTAL
	ેટુંદુ હુદ્દ	-1-10-1000000	8.2 9.4 20.4	0.5 0.5 0.5 0.5 0.5 0.5 0.5 0.5 0.5 0.5	100.0		Rate	Et .	20000-4000-	27.0 49.1	804-0-0 NOR8-199	100.0
50) 50	Conce. R of contr (pob)		15.123 E	0.1000 11 2	31.219 10	21)	Conce. R		1-1	8.140 2 14.812 4	00	20.159 10
(Rank 5 IX, IY=15, 22)	Type of source SEQ) Coun Fact Sta. 6 ty No. No.	55 55 55 55 55 55 55 55 55 55 55 55 55	Remaining stacks Sub total	Factory (area source) Pactory (industrial estate) Roadways Vessels (sailing) Ferryboats (unchoring) Ferryboats (sailing) Back ground	TOTAL	[Rank 7 IX, IY=15,21	Type of source	SEQ) Coun Fact Sta.	55 55 55 55 55 55 55 55 55 55 55 55 55	Remaining stacks Sub total	Factory (area source) Factory(industrial estate) Roadways (sailing) Perrybats (anchoring) Ferrybats (sailing) Back ground	
	Rate Solf	ଦ୍ୟାମରା ଭାରଣ ବାର ବାର ଭୁମ୍ଚରା ଭାରଣ ବାର	5.50 20.00	80.400 80.400 80.400 80.400	100.0		Rate	Satt Satt	කයුහාගයාගුගුගුගු ත්යාන්තා කර්ගත් කර	57:4	8000-000 40000-000	100.0
8	Conce. of (ppb)	4	8, 133 133 133	0.01% 0.00% 1.00%{	34.066	8	Conce.	contr (ppb)	2.1-1-1-0 2.2-2-2-2-2-2-2-2-2-2-2-2-2-2-2-2-2-2-2	7.180 18.618	90-0000 200-0000 400000000000000000000000	32.424
(Rank 2 IX, IY=16, 23)	Type of source SE2) Coun Fact Sta.	55 57 55 55 55 55 55 55 55 55 55 55 55 5	Remaining stacks Sub total	Factory (area source) Reactory(industrial estate) Reachers Vessels (sailing) Ferrybats (sailing) Back ground	TOTAL	(Rank 4 IX, IY=17, 23)	Type of scurce	SEQ) Coun Fact Sta.	500 - 200 -	Remaining stacks Sub total	Factory (area source) Factory(industrial estate) Roadways (sailing) Ferryboats (aniling) Farryboats (sailing) Back ground	TOTAL
	Rate Soft	5.000-1-0044 00000-1-0044	25.9 26.9	2040000 000000000	100.0		Rate	contr.	040000-0-0-0-0 	25.5 25.5	80000-00 330000 330000	100.0
(72)	Conce. of (ppb)	0.000000000000000000000000000000000000	zd:78	9000-00 8885-00-00 8885-00-00-00-00-00-00-00-00-00-00-00-00-00	\$5.258	,23)		contr (ppb)	20000000000000000000000000000000000000	17.522	2.1719 2.15888 2.15888 2.1588 2.1588 2.1588 2.1588 2.1588 2.1588 2.1588	33.804
(Rank 1 IX, IY=15, 24)	Type of source SBD) Coun Fact Sta. ty No. No.	二子 5 5 5 5 5 5 5 5 5 5 5 5 5	Remaining stacks Sub total	Factory (area source) Factory(industrial estate) Readways Vessels (sajling) Ferrybats (anihorig) Back ground	TOTAL	[Rank 3 IX, IY=15, 23]	Type of source	SEQ) Coun Fact Sta.	ດີ ເດິດ ເດີດ ເດີ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີດ ເດີ ເດີ	Remaining stacks Sub total	Factory (area source) Reactory (industrial estate) Reachers (sailing) Vessels (sailing) Ferrybotis (sailing) Back ground	TOTAL

Table 3-5(4) Contributive Concentration by Emission Sources at High NO₂ Concentration Points (Case of Taking No Countermeasures, in 1999)



4. Remedical Efforts against Emission Source Improvements and their Effectiveness

It was clarified that the atmospheric NO_2 concentration in Samut Prakam Province would exceed the environmental standards in 1999 and that cars would occupy most of the contribution rates by emission source at the points where the said NO_2 concentration would exceed the standard. Then, with cars as a target, specific remedial measures for NO_2 emission sources (such as adoption of NO_x emission controlled cars) were studied, coupled with forecast of the ambient concentration of NO_2 after adoption of restricted cars.

Although it was predicted that the ambient concentration of SO_2 would not exceed the environmental standard despite the progress of economic and social development, the contribution rates at high concentration points would be greatly occupied by factories. Thus, this led to forecast of the extent to which the environment would be improved if SO_2 emission control is implemented for factories in future.

4.1 SO₂ Emission Control for Factories

At present, no SO_2 emission control is in force in Thailand. In other words, it is presently permissible no matter how much SO_2 may be emitted. This leads to lack of fairness among factories, suggesting that some measure should be taken. Thus, environmental remedy was examined in case that K-value control of Japan was adopted as a specific control measure for emission sources for factories with 1999 as the target year. This K-value control is the control of maximum concentration on the ground level as shown in the equation (4-1), which can be met by either making stacks higher or reducing SO_2 emission volume. Specific K value was established making reference to that of an area of Japan similar to Samut Prakarn Province.

$$K = \frac{q}{He^2} \times 10^3 \qquad (4-1)$$

where q is the quantity of sulfur oxide and He is the effective stack height calculated from equations (4-2) and (4-3).

$$He = H_{o} + 0.65 (Hm + Ht)(4-2)$$

$$Hm = \frac{0.795 \sqrt{Q \cdot V}}{1 + \frac{2.58}{V}}$$

$$H_{t} = 2.01 \times 10^{-3} \cdot Q \cdot (T - 288) \cdot \left\{ 2.30 \log J + \frac{1}{J} - 1 \right\}$$

$$J = \frac{1}{\sqrt{Q \cdot V}} \left\{ 1460 - 296 \times \frac{V}{T - 288} \right\} + 1$$

$$(4-2)$$

where

- He : effective stack height (m)
- H_0 : actual stack height (m)
- Q : exhaust gas volume at $15^{\circ}C$ (m³/s)
- V : discharge speed of exhaust gas (m/s)
- T : temperature of exhaust gas (°K)

4.1.1 Establishment of the K Value

Table 4-1 shows the volume of SO_2 per area emitted from factories in Samut Prakarn province, and Table 4-2 shows those from factories in the regions of Japan which are similar to the foregoing province. These data indicate that in the Samut Prakarn region the SO_2 volume per area is 19.52 tons/year/km², whereas in Japan the SO_2 volume obtained by averaging those regions with a K value of 13.0 accounts for 11.72 tons/year/km². Likewise, those regions with a K value of 10.0 give an average volume of 9.06 tons/year/km², and those with 8.0 have an average of 8.37 tons/year/ km². As a consequence, K=13.0 is considered most suitable to be applied to the Samut Prakarn region judging from the emission volume of SO_2 per area. Looking at the K values in Table 4-2, the volume of SO_2 per area greatly varies among prefectures and cities even though they have the same K value. This is because the K value in Japan is determined based on the considerations including not only the density of factories and the scope of smoke diffusion, but also the feasibility of administrative control.

Name of county	① SOz emission volume (ton/y)	② Area (km²)	(3)=(1)÷(2) SO ₂ volume per area (ton/y/km ²)
1 Muang	5163	356	14.50
2 Bang Plee	932	534	1.75
3 Phra Pradaeng	12235	49	249.69
TOTAL	18330	939	19.52

Table 4-1 SO₂ Volume per Area Emitted from Factories in Samut Prakarn Province during 1988

Table 4-2 SO2 Volume per Area Emitted from Factories in the Regions of Japan Similar to Samut Prakarn

		Yearly	0	Ø	(() ÷ (2)
		average	SO2		SO2
К		SO2	entistion		emission
	Name of city	concent-	volume	Area	volume
value		ration	in 1985		per area
		in 1987			(ton/y
	:	(ppb)	(ton/y)	(km²)	/ka²)
	Shibukawa	9	1373.6	51.84	26.50
	Numazu	7	452.0	151.20	2.99
	Mishima	5	1043.2	61.81	16.88
	Tamano	10	180.7	103.35	1.75
	Komatsujima	7	1093.3	44.38	24.63
13.0	Naruto	6	730.6	135.41	5.40
	Anan	7	4608.3	252,83	18.23
	Kurume	7	1675 1	123.93	13.52
	Itoman	2	249.9	44.98	5.56
	Okinawa	3	86.9	48,74	1.78
	Kushiro	11	5417.5	218.85	24.75
	Takefu	5	446.1	184.98	2.41
10.0	Sabae	9	386.0	84.23	4.58
	Saseho	5	1123.7	250.46	4.49
	Otaru	. 9	504.5	244.65	2.06
	Asəhikawa	8	1877.7	749.42	2.51
	Sakata	4	1358.9	175.00	7.77
	Utsunomiya	8	1024.8	312.53	3.28
	Kanuma	8 6 6	229.2	311.74	0.74
8.0	Mouka	6	891.5	111.49	8.00
	Tsuruga	6	1262.9	249.51	5.06
	Takehara	8	5464.7	117.54	46.49
	Mihara	10	1349.8	204.35	6.61
	Onomichi	8	125.9	110.73	1.14

Remark : The reason why difference of SO₂ emission volume is seen at the areas adopted the same K-value is due to institutional judgement social-ecomonical factors.

Table 4-3 shows actual stack heights required to achieve the K values (8.0, 10.0, 13.0). Suppose the K value is 13.0, except for extremely low stacks with an actual stack height of around 5 m, it is sufficient to add to the stack heights of 10 to 15 m to reach about 20 m, and this is thought to be the most feasible in view of economic efficiency.

Based on the above consideration, the concept of K value control in Japan was adopted for the control of SO_2 emission from factories in Samut Prakarn province, and the specific K value was thought to be 13.0.

4.1.2 SO₂ and NO_x Emission Volume after Implementation of SO₂ Emission Control

In implementing K-value control, the K-value may be satisfied either by increasing stack height as described above, or reducing the emission volume of SO_2 . This allowed us to compute an actual stack height and an SO_2 emission volume required to fulfill K=13. The results are shown in Table 4-4. According to these results, some factories would have to cut back their current emission volumes of SO_2 to about 1/7 if they attempt to achieve the K-value by reducing the emission volume. Since that would be impossible, the other alternative of increasing stack heights was thought to be realistic to achieve the K-value. It should be kept in mind that a higher stack will not expand the scope of pollution; if emission volumes are same, the ground level concentration of a pollutant emitted from a high altitude will no doubt be lowered compared with that from a low altitude under an identical diffusion condition. That is to say, Fig. 4-1 shows axial ground level concentrations on the down wind distance (CU/Q) in a single stack when the effective stack height He is varied, indicating that higher stacks exhibit lower ground level concentrations in any leeward distances as compared with lower stacks.

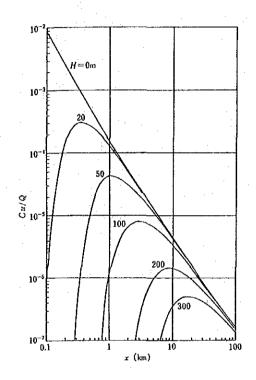


Fig. 4-1 Axial ground level concentration for different effective stacks heights He (u; wind speed, Q; emission volume)

						:
S S S	8-7	8115442 811544 811584 81158 81		0004108282622	288888888888	2222222222200 2222222200 22222222200
Actual stack height based o K-value (田)	K=10	991441916.60 666441916.60 666666666666	1288818818888 88881888888 8888188888 88881888888	22238225464-3 2223822254664-3	85585555555555555555555555555555555555	2333 2333 2421 2421 2421 2421 2421 2421
Act heig K-	K=13	လိုက္ရပ္က်ဆွတ္လတ္ တိုက္ရက္လ စင္းကို တစ္တတ္ ကိုက္ရွိဆိုလ္ရွိ	90.02 15.20 15.20 15.20 15.000	12.2.2.4.2.2.2 112.2.2.4.5.5.5.5.5.5 112.2.2.4.5.5.5.5.5.5 112.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2	15.0 11.4 11.4 15.3 15.3 15.3 15.3 15.3 15.3 15.3 15.3	2010.5 2013 2013 2013 2014 2014 2014 2014 2014 2014 2014 2014
Effec- tive stack height	活 (目) 	ឆ្កី១ឆ្កើលក្មុកស៊ីតុខ្ល ស៊ី១ស៊ីស៊ីស៊ីទីទីទីទីទីទីទីទីទីទីទីទីទីទីទីទ	_{֍Ⴠ} ႾႯႣჽႢႳႳჀ ႽჇჇჇႦႦ	588888888 511585888888 5888888888888888	20078999988 88925258888	8151889.00 2288888888
Normal SO2 Enission volume	q(h ^a /h)		450,000,000,000,000,000,000,000,000,000,		9.52.52.52.52.52.52.52.52.52.52.52.52.52.	9-1-9-1-222.0-0 2-822-228882288
Normal Exhaust gas volume	(s/ ₂ m) ()	80.00 80	0.519 0.125	0.932 1.885	2.005 2.005 2.005 2.005 2.005 2.005 2.005 2.005 1.005	-00004440- 8888468881- 8888488881-
368	T (*K)	<u> </u>	<u>88888888888</u>	<i>Ğ</i> £ <u>3</u> <u>8</u> <u>8</u> <u>8</u> <u>6</u> <u>6</u> <u>6</u> <u>6</u> <u>6</u> <u>6</u>	***************************************	៩៩៩៩៩៩៩៩៩៩
Gas velo- city	(S/ш/S)	9999941-999 8888848888	පරගරපතර ශ්ශ්ය පිරිහිරි පිරිහිරි පිර	00000000000000000000000000000000000000	ବ୍ଦ୍ଦ୍ଦ୍ୱ୍ୟୁର୍ବ୍ନର ୫୫୫୫୫୫୫୫୫୫୫୫୫	99999999988888888888888888888888888888
St Cal) ક	<u>ຼ</u> ຼິຼຒ໙ຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎຎ	සු කත්ත සිසි සිසි සිසි සිසි සිසි සිසි සිසි ස	<u>ទី«សីសីសីសីទី2</u> សី	<i>占리</i> 징긍정금ଇ 쫖 전진정정	833558888°r
Value Value		86888818888888888888888888888888888888	xxxxxxxxxxxxxx xxxxxxxxxxxxxxxxxxxxxxx	85.23 88.728 88.728 88.728 88.728 89.728 89.728 89.728 800	86.999 86.257 87.257 87	4444 4444 4444 4444 4444 4444 4444 4444 4444
Sta- ck		-09400-00-00-	0000000000		0000-0-0	000000000
Fac- tory No.		ឝននេននងនេន	aesses:18235	ៜៜਲ਼ਸ਼ਲ਼ਖ਼ਫ਼ਫ਼ੑਫ਼ਫ਼ਖ਼	<u> 74 0 8 8 8 6 0 8 8 9 8 9 8 9 8 9 8 9 8 9 8 9 8 9 8 9</u>	<u>8508888</u> 288
Coun ty code		000-0000-	00000000	<u></u>	<u>നപയപപതയന</u> ചയ	0000000-0
2EG)		ବ୍ରଚ୍ଚର୍ବ୍ଦର୍ବନ୍ତ୍ରନ୍	388839995888	ଲିଷିକ୍ଷିକ୍ଷିକ୍ଷିକ୍ଷିକ୍ଷିକ୍ଷିକ୍ଷିକ୍ଷିକ୍ଷିକ	ଟି <u>ଷ୍ପି</u> ଷ୍ପିଷ୍ପିଷ୍ପିଷ୍ପିଷ୍ଟି	<u> କ</u> ର୍ଷ୍ଣକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକୁକ୍ତିକ

Table 4-4 Actual Stack Heights and SO₂ Emission Volumes Required to Fulfill K=13.0

			· ·				
stack	s Normal Let Sui- or K=13	(¶ر¶°)۹	4.576 10.001 10.001 10.001 10.000 1412 141 141 141 141 141 141 141 141 14	1046888888888888888888888888888888888888	2488 11-1488 124888 124888 12488 12488 12488 12488 12488 12488 12488 12488 124		8.88 2.25 2.25 2.25 2.25 2.25 2.25 2.25
Actual	solution of the second	Ho (m)	8.6.7.2.9.0.6.7.9.8 8.6.7.2.9.0.0.0.0.8 8.6.7.2.9.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0	90091689889 9009160009	81221688889 0-10245569550	1222111460 1222111460 122233104460	85555880 ⁰⁻
Effec-	stack height	He (m)	80,000,000,000,000 80,000,000,000,000 80,000,00	∞ <u>₩</u> ΞΫΫΫΫΫΫΫ 888828348886	81128188888 199758288888 199758289888	2299284299888 2999284299888 28886425488888	<u>%=%=%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%</u>
Normal	volue volue	q(Nu ³ /h)	31.687 5.510 2.25300 2.2530 2.2530 2.253000 2.253000 2.25300 2.253000 2.253000 2.253000 2.253000 2.253000 2.25300000000000000000000000000000000000	0.02 0.02 0.02 0.02 0.02 0.02 0.02 0.02		20002002002002000200000000000000000000	8.1-2-1-2228 8.8255888228882 8.82888888888888888
Normal	conaust gas volume	(s/=1/s)	25.05 25.05	0.559 0.125	0.888 1.688 1.688 1.884 2.3319 2.23311 2.23312 2.2331 2.23	2.025 5.466 9.631 1.026 1.027 1.026 1.026 1.026 1.027 1.026 1.026 1.027 1.0266 1.026 1.026 1.026 1.026 1.026 1.026 1.026 1.026 1.026 1.026	0.556 0.556 0.658 0.658 0.658 0.658 0.658 0.658 0.658 0.198 0.198 0.1141 0.00141 0.0000000000
Gas	rature	T (°K)	#\$\$\$\$\$\$\$\$\$\$\$\$	<u>88883388888</u>	<i>Ğ²2333868636</i>	<u> </u>	£&&&&&&&&&&&&&&&&&&&&&&&&&&&&&&&&&&&&&
Gas	city	(s/ш/s)	0000041-000 8888888888888888888888888888888888	00000000000000000000000000000000000000	00000000000000000000000000000000000000	0000840080 88882888888	82888888888888888888888888888888888888
Actual	scack	H。 (m)	ឨ៰៰៷៷៷៱៷ៜ៷៱៰៷	කතනයිසින්තනිසිස් තතනිසිස් තතනිස් තතනිස් තතනිස් තතනිස් තතනිස් තතන ස් තතන ස් ත තතන ස් ත ත ත ත ත ත ත ත ත ත ත ත ත ත ත ත ත ත	ರ್ರೂಪಡೆಸಿದವಿಿ ಸನ	2222288859988	ක්ට්ට්ට්හිහිපිත්ත සිට්ට්හිහිසිත්ත සිට්ට්හිනිසිත්ත
2		20102	89988888888888888888888888888888888888	xxxxxxxxxxxxx BXXXXXXXXXXXXXXXXXXXXXXXX	89.69 89.69 89.69 89.69 89.69 89.69 80	16.555 16.515 16.515 16.515 16.525 16.5555 16.5555 16.5555 16.5555 16.5555 16.5555 16.5555 16.5555 16.55555	72722222222222222222222222222222222222
	Sta- Ka-	2		000000	~~~~~~~~~~	00000000000000000000000000000000000000	000000000-
СК	Fact tory		K¥X88222888	apsssuiszző	85888888888888888888888888888888888888	208325m8352	<u>\$50888858888</u>
STA	a S S			<i>∾∾⊶⊶∞∞⊶∞∞∞</i>		ೲ ⊶ೲೲ⊶ო	0000000-000
	28		ୁବିଚରମ୍ବରହନନନ୍ଦ	38839995888	ୖୖ୶ୠୖୖୖୖୖୠୡୖ୶ୠୠୖ୶ୠୖୡୠୖୡ	ୢୄୖ୶ଢ଼ଢ଼ୡୡଢ଼ୡୡୡ	<u> କିଷ୍ଣସ୍ପସ୍ଥିତ୍ତ୍ୱକ୍ରେ</u> ଷ୍ଟର

Thus, SO₂ emission volume after improvement of K-value control is same as that when no source countermeasure is taken, showing 29,442 tons/year as presented in Fig. 2-1(1) and Table 2-1. In addition, the emission volume of NO_x also remains unchanged because of no improvement in combustion plants, amounting to 14,052 tons/year as exhibited in Fig. 2-1(2) and Table 2-1.

In order to achieve the K value, in addition to increasing the stack height to enhance He, another way is to reduce the caliber of stack and increase gas ejection velocity, thus having greater He. In the case of a stack with umbrella, in addition, the ejection velocity will be raised if the umbrella is removed, so that the stack height will not have to be increased more than necessary. Therefore, taking into consideration economic efficiency as will be described in Part VII, the stack caliber was made smaller to have a gas ejection velocity of 15 m/s, coupled with a limited stack height. Table 4-5 shows the results of the above measures.

	ST/			Actual height(slack e)	Diamet	er (a)	Gas ve	locity (m/s)
SEQ)	Coun ty code	Fac- tory No.	Sta- ck No.	before count.	after count.	before count.	after count.	before count.	after count.
1)2)3)4)5)6)78990 10)	*****	75 34 23 68 23 24 95 39 39	1342512121	555520572565 15	38.0 17.0 12.5 37.0 10.0 10.5 3.0 13.0 8.5 31.5	9.9 9.9 9.9 1.5 9.9 0.4 0.2 9.9 0.6 0.5	$\begin{array}{c} 1.55\\ 0.55\\ 0.53\\ 0.96\\ 0.65\\ 0.22\\ 0.14\\ 0.78\\ 0.03\\ 0.63\\ \end{array}$	$\begin{array}{c} 0.00\\ 0.00\\ 0.00\\ 6.09\\ 0.00\\ 4.46\\ 7.58\\ 0.00\\ 0.00\\ 0.00\\ 0.00\\ 0.00\\ \end{array}$	15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0
 11) 12) 13) 14) 15) 16) 17) 18) 19) 20)	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	19 97 68 66 59 111 56 14 14 109	2 1 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	6 5 15 10 22 6 20 20 12	10.5 6.5 21.0 18.5 19.0 33.0 11.0 27.5 27.5 17.0	1.2 9.9 1.2 0.4 0.7 1.2 0.6 0.8 0.8 0.8	0.28 0.11 0.50 0.46 0.49 0.95 0.44 0.81 0.81 0.36	$\begin{array}{c} 0.00\\ 0.00\\ 2.64\\ 0.00\\ 9.32\\ 0.00\\ 15.30\\ 15.30\\ 0.00\\ \end{array}$	15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0
21) 22) 23) 24) 25) 26) 27) 28) 29) 30)	3	90 70 35 54 35 16 102 68 66 16	1321141323	10 6 15 15 15 13 20 14 15	14.5 10.5 18.0 23.5 18.0 23.0 21.5 22.5 21.5 20.5	0.8 1.7 0.6 0.7 0.6 0.5 1.5 0.6	0.36 0.46 0.43 0.50 0.43 0.50 0.55 0.55 0.55 0.54 0.45	$\begin{array}{c} 0.00\\ 0.00\\ 5.69\\ 0.00\\ 5.69\\ 0.00\\ 2.00\\ 2.03\\ 0.00\\ 0.00\\ 0.00\\ 0.00\\ 0.00\\ \end{array}$	15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0
31) 32) 33) 34) 35) 36) 37) 38) 37) 38) 39) 40)	31311333313 13333133 13	47 2 109 64 70 5 16 16 70 54	3 1 1 2 2 1 2 1 2 1 2 1 2	12 12 15 10 18 24 15 15 18 18 18	20.0 18.0 19.5 12.0 23.5 29.5 18.0 18.0 21.5 23.0	0.7 0.6 0.5 0.6 0.6 0.8 0.6 0.6 0.6	0.55 0.50 0.41 0.30 0.96 1.22 0.39 0.39 0.85 0.51	$\begin{array}{c} 0.00\\ 0.00\\ 0.00\\ 38.04\\ 34.79\\ 0.00\\ 0.00\\ 30.38\\ 0.00\\ \end{array}$	15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0
41) 42) 43) 44) 45) 46) 47) 48) 49)	372311313	54 110 5 28 55 55 14 64 95	3261 12322	18 10 10 30 30 20 6 7	23.0 10.5 11.5 35.5 35.5 20.0 6.0 7.0	0.9 0.3 0.5 0.6 0.6 0.8 0.3 0.3	0.51 0.28 0.29 0.25 0.70 0.70 0.57 0.16 0.33	0.00 12.61 0.00 0.00 0.00 7.65 0.00 0.00	15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0

Table 4-5 Improvements in Factory Stacks

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4.2 Adoption of NO_x Emission Restricted Cars

In Samut Prakarn province it is predicted that the ambient concentration of NO_2 will exceed the environmental NO_2 standard in 1999, mostly attributable to automobiles (with a contribution rate of about 80%). As a consequence, automobile exhaust control will be required to fulfill the environmental control standard of NO_2 in future years.

Table 4-6 shows NO_x emission factors by auto emission restriction yuear established by the Ministry of Construction of Japan. While the NO_x emission factors of this table are classified by 6 vehicle types, Table 4-7 shows NO_x emission factors made correspondent with the 5-type classification in Thailand (see Part IV, 3, 4). Table 4-8 shows the reduction rate of the NO_x emission volume from automobiles in each year when NO_x emission restriction is adopted from 1973, using the NO_x emission factors shown in Table 4-7 as well as the composition of cars by type, traffic volume by road, and car speed in Samut Prakarn province. On the other hand, the reduction rate of contributory concentration by cars, which is required to lower the concentrations of NO_2 at the points where they will exceed NO₂ environmental standard in 1999 down to NO₂ environmental standard value (18 ppb) by instituting NO_x restricted cars, are figured out as shown Table 4-9, revealing that a 47.9% reduction is necessary. Because of the proportional relationship between the NO_x emission volume and the NO₂ diffusion concentration, the reduction rates of NO_x emission volume in 1999 is computed as 47.9%. If these reduction rates are allowed to match the NO_x reduction rates when restricted cars are adopted (Table 4-8), it is understandable that adoption of 1978 controlled cars by Japan will be required in 1999 to accomplish NO₂ environmental standard. Table 4-10 shows the automobile emission volumes of NOx in Samut Prakarn province due to the adoption of restricted cars, and Fig. 4-2 shows NO_x emission volume by mesh.

 Table 4-6 NOx Emission Factors by Year of Automobile Emission Restriction (Established by the Ministry of Contruction in Japan)

ïchicle type	Section		s sé la re			Rest	riction year		jeti i	- 21				[
ia JAPAN	velocity	non	1973	1974	1975	1976	1977	1338	1979	1380	1981	1982	1983	unit
Passenger Car	42 is∧a 52 is∧a 62 is∧a 62 is∧a	2.62 2.55 2.58 3.15 3.43 3.75 4.63	2.58 2.16 2.12 2.13 2.11 2.04 2.61 3.63		1.38 1.13 1.08 1.06 1.02 0.95 1.29 2.54	0.87 0.73 0.72 0.73 0.73 0.73 0.70 1.28 2.65		0.30 0.25 0.25 0.25 0.25 0.24 0.24 0.44 0.50			-	TTTTTT	1 1 1 1 1 1	(g/im/car)
Light cargo vehicle	10 5% 20 5% 30 5% 30 5% 5% 5% 5% 5% 5% 5% 5% 5% 5% 5% 5% 5%	6.98 5.59 5.26 5.26 4.74 4.74 4.98 8.03	4.19 3.45 3.33 3.29 3.20 3.02 4.61 7.44	411111	2.346 2.346 2.377 2.327 2.327 2.328 3.45 3.61	1111111	* * * * * * * *		1.98 1.65 1.64 1.37 1.59 1.33 1.58 1.32 1.55 1.29 1.47 1.23 2.32 1.91 3.76 3.14		9 0.79 6 0.77 0 0.73 4 1.16			(e/tou/car) leftmiddle class (L.7~2.5ton) rightlight class (L.7ton or less)
Heavy duty gasoline vehicle	20 ba/h 30 ba/h 40 ba/h 50 ba/h 60 ba/h 80 ba/h	7.25 6.04 5.92 5.92 5.84 5.60 7.54 8.68	5.00 4.53 4.53 4.53 4.53 4.53 4.53 4.53 5.672		111111	1111111	4.23 3.28 3.88 3.88 3.88 3.88 4.92 5.5		3.35 2.73 2.74 2.74 2.70 2.59 3.49 4.82			2.91	111111	(g/lav/car)
Diesel vehicle Oirect fuel isjociton)	40 ks/h 50 ks/h 60 ks/h 80 ks/h	2.074 13.90 1.654 11.08 1.550 10.38 1.478 9.90 1.381 9.25 1.237 8.29 1.143 7.66 1.864 12.49		1.655 11.15 1.332 9.13 1.309 8.77 1.234 8.69 1.240 8.31 1.157 7.75 0.984 6.99 1.679 7.23	111111 111111 1111111	111111 111111	1,406 9,42 1,150 7,70 1,106 7,40 1,084 7,26 1,086 7,01 0,977 6,54 0,870 5,56 0,911 6,10		1.168 7.82 0.355 6.40 0.918 6.15 0.900 6.63 0.859 5.82 0.811 5.44 0.650 4.62 0.756 5.07		1111. 1111.	11111 	1.016 6.81 0.831 5.57 0.799 5.35 0.793 5.25 0.756 5.07 0.706 4.73 0.600 4.02 0.658 4.41	
Diesel vohicte (von-direct fuel injection)	-30 kovta 40 kovta 50 kovta 60 kovta	1.185 5.21 1.019 4.48 1.027 4.52 1.057 4.65 1.075 4.73 1.067 4.69 1.489 6.55 1.533 8.51		1.013 4.46 0.872 3.84 0.878 3.87 0.904 3.98 0.920 4.05 0.913 4.02 1.274 5.61 1.654 7.28		1.511111 1.511111	0.855 3.76 0.736 3.24 0.741 3.26 0.741 3.26 0.775 3.42 0.770 3.39 1.075 4.73 1.366 6.14	1111 1111	0.766 3.37 0.659 2.90 0.664 2.92 0.624 3.01 0.626 3.05 0.620 3.04 0.953 4.24 1.220 5.50			0.653 2.87 0.561 2.47 0.566 2.49 0.582 2.56 0.592 2.61 0.588 2.59 0.820 3.61 1.055 4.69		left (g/ou/car/ton) right (g/iau/car)
Diesel vehicle (Swirt chawber (ype)	10 ks/s 20 ks/s 30 ks/s 40 ks/s 50 ks/s 50 ks/s 50 ks/s 50 ks/s 50 ks/s 50 ks/s 50 ks/s 50 ks/s	1.148 2.30	н н 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	0.852 1.70 0.743 1.49 0.759 1.52 0.791 1.52 0.814 1.63 0.819 1.64 1.029 2.30 1.427 2.85			0.119 1.44 0.627 1.25 0.660 1.28 0.667 1.33 0.687 1.37 0.681 1.33 0.928 1.86 1.30 2.41	1111	0.644 1.29 0.552 1.12 0.574 1.15 0.578 1.20 0.616 1.23 0.619 1.24 0.831 1.66 1.079 2.16		11111	0.543 1.10 0.473 0.96 0.433 0.96 0.509 1.02 0.524 1.05 0.528 1.05 0.708 1.42 0.919 1.84		

Table 4-7 NOx Emission Factors by Year of Automobile Emission Restriction Based on 5-Type Classification in Thailand

												(unit:g	/ka/car)
Yehicle type	Section					Restric	tion ye	аг				:	
in Thailand	Velocity	non	1973	1974	1975	1976	1977	1978	1979	1980	- 1981	1982	1983
Light vehicle	10km/h 20km/h 30km/h 40km/h 50km/h 60km/h 80km/h 100km/h	2.75 2.27 2.21 2.21 2.21 2.14 2.14 2.14 2.14 2.15 2.15 2.15 2.15 2.15 2.15 2.15 2.15	2.05 1.74 1.73 1.75 1.76 1.72 2.44 3.54	2.01 1.709 1.209 1.209 1.209 1.209 2.397 2.397 2.397	1.455 1.455 1.458 1.458 1.458 1.458 1.458 1.458 1.458 1.458 1.458 1.458 1.458 1.458 1.458 1.458 1.4555 1.4555 1.4555 1.4555 1.4555 1.4555 1.4555 1.4555 1.4555 1.4555 1.	Same as left	52222	Some as left	1.18 1.01 1.04 1.05 1.05 1.05 1.05 1.47 2.09	Same as left	1,0390,255,550	0.93 0.88 0.88 0.88 0.88 0.88 0.88 0.88 0.8	Sane as left
Neavy vehicle	10k#/h 20k#/h 30k#/h 40k#/h 50k#/h 60k#/h 80k#/h 100k#/h	129909999999999999999999999999999999999	Same as left	9.446927777 8.4469277777 8.4469277777	Sase as left	Sane as Teft	877777777 777777777 777777777 932	Saae as left	22222222222222222222222222222222222222	Same as icfl	Same as left	4498679884 6.5.675884 6.5.675884	6071153895 6054553895 6055525 705
Gasol ine	10ks/h 20ka/h 30km/h 40ks/h 50ks/h 60ks/h 80ks/h 100ks/h	222352 222352 222352 222552 22552 22552 22552 22552 22552 22552 22552 22552 22552 22552 22552 22552 22552 22552 22552 22552 23552 25552 25552 25552 25552 25552 25552 25552 25552 25555 25	86223144 82223144 8263 8263 8263 8263 8263 8263 8263 8263	Sane as left	1.38 1.00 1.00 1.00 1.00 0.29 0.29 2.54	0.87 0.772 0.773 0.773 0.773 0.770 0.728 0.285	Same as left	0.30 0.25 0.25 0.25 0.25 0.25 0.24 0.44 0.90	Same as left	Same aş left	Same as left	Same as left	Same as left
LPG	10k#/h 20k#/h 30k#/h 40km/h 50k#/h 60k#/h 80k#/h 100k#/h	21-425 255 255 255 255 255 255 255 255 255	499564572 200564572 2005655 200555 200555	Sane as left	1.39 1.149 1.007 1.007 1.007 0.330 1.357	0.785 00.655 00.6552 00.6524 00.6524 00.6524 00.6524 00.1436	Same as left	0.29 0.24 0.24 0.24 0.24 0.23 0.423 0.423 0.425	Same as left	Same as left	Same as left	Sarc as left	Same as left
Motor cycle	10k#/h 20k#/h 30k#/h 30k#/h 50k#/h 60k#/h 80k#/h 100k#/h	0.26 0.25 0.35 0.35 0.35 0.35 0.47 0.46	0.26 0.22 0.21 0.21 0.21 0.21 0.20 0.26 0.36	Sanc aș left	0.14 0.11 0.11 0.11 0.10 0.10 0.13 0.25	$\begin{array}{c} 0.09\\ 0.07\\ 0.07\\ 0.07\\ 0.07\\ 0.07\\ 0.13\\ 0.27\\ \end{array}$	Same as left	0.03 0.03 0.03 0.03 0.03 0.02 0.02 0.04 0.09	Same as left	Same aş left	Same ás left	Same as left	Same aş left

Restriction year	Cut percent of NOx emisson volume (%)
non restriction	0.00
1973	15.74
1974	21.25
1975	33.24
1976	36.52
1977	44.64
1978	49.25
1979	55.84
1980	55.84
1981	56.67
1982	61.82
1983	62.38

Table 4-8 Reduction Rate of NO_x Emission Volume due to Adoption of Restricted Cars

Table 4-9 Reduction Rates of Automobile Contributory Concentration Required to Achieve NO₂ Environmental Standard in 1999

Mesh	code	NO2 Concentration (ppb)	Environmental standard value (ppb)	Reduction in concentration (ppb) 'Pb)	Automobile contributory concentration (ppb)	Automobile contributory concentration required to achieve environmental standard (ppb)	Reduction rate of automobile contributory concentration (%)
20-	16-0	18.1	18.0	0.1	12.95	(2.85	0.8
20-	17-0	19.0	18.0	1.0	13, 98	12.98	7.2
19-	18-0	18, 1	18.0	0.1	13, 13	13.03	0.8
20-	18-0	19.8	- 18.0	1.8	15.00	13. 20	12.0
20-	19-0	18.5	18.0	0.5	13.72	13. 22	3.6
21-	19-0	19.0	18.0	1.0	14.58	13.58	6. 9
21-	20-0	18.6	18.0	0,6	14, 13	13.83	4. 2
20-	21-0	18. 7	18.0	0.7	14.26	13.56	4.9
15-	22-0	18.7	18.0	0.7	8.86	8. 16	7.9
20-	22-0	19.7	18.0	l.7	15, 15	13. 45	11.2
21-	22-0	20.3	18.0	2.3	16.07	13.77	14. 3
15-	23-0	29. 0	18.0	2.0	7. 78	5.78	25.7
19-	23-0	18.4	18.0	0.4	12.96	12.56	3.1
20-	23-0	20.8	18.0	2.8	15.90	13.10	17.6
21-	23-0	23.0	18.0	5.0	18.65	13.65	26.8
15-	24-0	21.3	18.0	3.3	6. 89	3.59	47.9
20-	24-0	[9.1	18.0	1.1	14.00	12.90	7,9
21-	21-0	23. 3	18.0	5.3	18.80	13.50	25.2
22-	24-0	22. 9	. 18.0	4.9	18.81	13. 91	26.0
	25-0	18.6	18.0	0.6	13. 15	12.55	4.6
21-	25-0	21.8	18.0	3.8	17.21	13.41	22.0
22-	25-0	23.8	18.0	5.8	19.70	13.90	29.4
20-	26-0	18. 1	18.0	0.4	12.65	12.25	3. 2
21-	26-0	20.7	18.0	2.7	16.02	13. 32	16. 9
22-	26-0	24.7	18.0	6.7	20.61	13.91	32.5
23-	26-0	18.0	18.0	0.0	14.23	14.23	0.0
21.	27-0	20. 1	18.0	2. i	15.26	13.16	13.8
22-	27-0	23.6	18.0	5.6	19.49	13.89	28.1
23-	27-0	18.9	18.0	0.9	15.07	14. 17	6, 0
21.	28-0	19.2	18.0	1.2	14.51	13.34	8.3
22-	28-0	20. 4	18.0	2. 4	16.35.	13.95	14.7

Table 4-10 NO_x Emission Volume due to Car Running in Samut Prakarn Province

	Year	NOx emission volume (ton/year)	Remarks
	1988	7,812	
	1992	10, 448	
	Before taking countermeasures	15,119	
1999	After taking countermeasures	7,673	Japanese 1978 restricted cars to be adopted

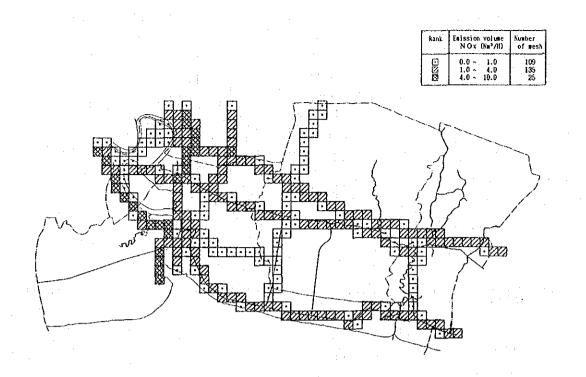


Fig. 4-2 (1) NO_x Emission Volume from Automobiles by Mesh (after taking countermeasures in 1999)

4.3 SO₂ and NO_x Emission Volumes after Implementation of Countermeasures for Emission Sources

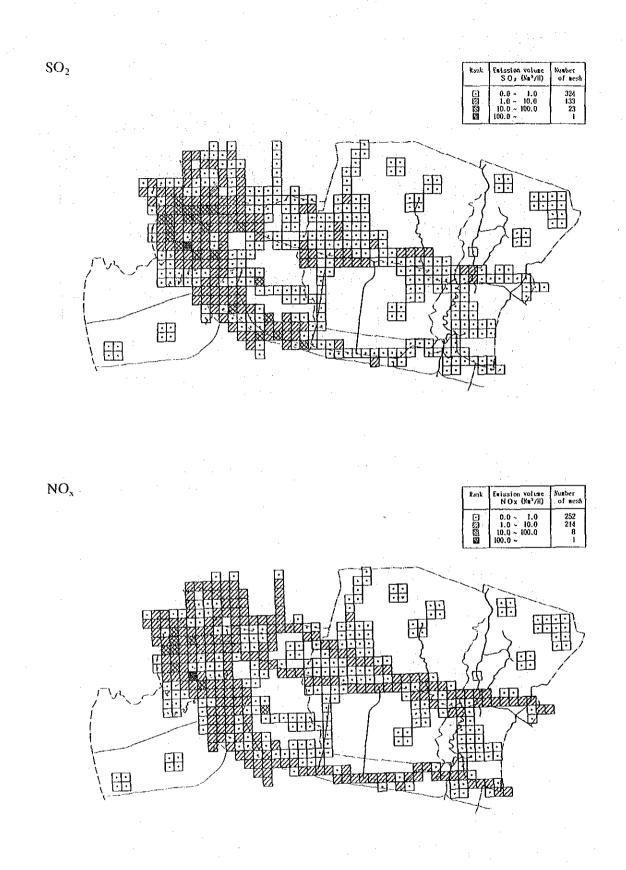
Table 4-11 and Fig. 4-3 show the volumes of SO_2 and NO_x emitted from all areas of Samut Prakarn Province after implementation of countermeasures for emission sources. Since the countermeasure for emission sources relating to SO_2 is the K-value control method which is making stacks higher, SO_2 emission volume is the same as that (33,855 tons/year) when no source countermeasure is taken. On the other hand, NO_x emission volume reaches 24,839 tons/year due to adoption of NO_x controlled cars, accounting for a reduction of 7,446 tons/year compared with NO_x emission volume 32,285 tons/year when no countermeasure for emission sources is taken. Table 4-11 Emission Volumes of SO₂ and NO_x from Sources in Samut Prakarn Province (upon implementation of source countermeasures)

 SO_2

		Туре		SO2 caissio	n volume (ton/ye	ar)
Nare (of source	of source	1988	1992 (92/88)	1999 (99/88) before count.	1999 (99/88) after count.
	Questionnaire return	point	13649	16269 (1.19)	21701 (1.59)	
Stationary	Questionnaire nothing	агеа	4681	5580 (1.19)	7443 (1.59)	
sources	sources Industrial estate			298 (-)	298 (-)	
	Sub tol	al	18330	22147 (1.21)	29442 (1.61)]
Roa	ad way	line	1474	1829 (1.24)	2261 (1.53)	same
V 1	Vessels (sailing)	point	1263	1505 (1.19)	2007 (1.59)	as left
vessels and	Vessels and Ferryboats Ferryboats (sailing)		8	11 (1.38)	17 (2.16)	
Ferryboats			59	82 (1.38)	128 (2.16)	
Sub tot		al	1330	1598 (1.20)	2152 (1.62)	
	TOTAL		21134	25574 (1.21)	33855 (1.60)	

 NO_{x}

		Туре		NO _x enission	n volume (ton/ye	ar)
Name (of source	of source	1988	1992 (92/88)	1999 (99/88) before count.	1999 (99/88) after count.
	Questionnaire return	point	8108	9665 (1.19)	12892 (1.59)	12892 (1.59)
Stationary	Questionnaire nothing	area	712	848 (1.19)	1132 (1.59)	1132 (1.59)
sources	Industrial estate	area		28 (—)	28 (-)	28 (-)
	Sub tot	al	8820	10541 (1.20)	14052 (1.59)	14052 (1.59)
Roa	id way	line	7812	10448 (1.34)	15119 (1.94)	7673 (0.98)
	Vessels (sailing)	point	1623	1935 (1.19)	2581 (1.59)	2581 (1.59)
Vessels and	Ferryboats (anchoring)	point	26	36 (1.38)	57 (2.16)	57 (2.16)
Ferryboats	Ferryboats (sailing)	point	221	304 (1.38)	476 (2.16)	476 (2.16)
	Sub to	al	1870	2275 (1.22)	3114 (1.67)	3114 (1.67)
······································	TOTAL			23264 (1.26)	32285 (1.74)	24839 (1.34)





4.4 Ambient SO₂ and NO_x Concentrations after Implementation of Countermeasures for Emission Sources

Forecast was made of SO_2 ambient concentration when K-value control would be instituted for factories in 1999. Another forecast was made of NO_2 ambient concentration when cars equivalent to 1978 NO_x emission controlled cars of Japan would be introduced in Thailand in the same year.

4.4.1 Comparisons between Ambient Pollutant Concentrations and Environmental Standard Values of All Areas

Fig. 4-4, 4-5 and Tables 4-12, 4-13 show the results of calculation of the yearly average ambient concentrations of SO_2 , NO_x and NO_2 in all areas of Samut Prakarn Province. Also, Table 4-14 shows the number of meshes by concentration rank. Some areas will exceed NO_2 environmental standard in 1999 when Thailand advances the economic and social development that it has planned without taking any countermeasure for emission sources, but it can be seen that adoption of NO_x emission controlled cars will prevent any points from exceeding the environmental standards. In addition, while SO_2 concentration will in no way exceed the environmental standards in future, it is understood that implementation of K-value control for factories in 1999 will lead to further improvement of environment.

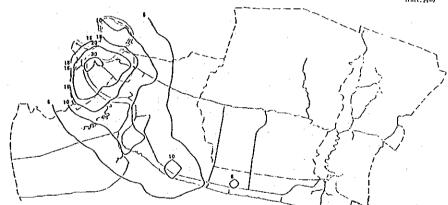


Fig. 4-4 Ambient SO₂ Concentration in Samut Prakarn Province after Implementation of K-value Control in 1999 Table 4-12 Yearly Average Concentration of SO₂ in Samut Prakarn Province after Implementation of K-value Control in 1999 (Unit: 0.1 ppb)

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Table 113 Ambient Concontration of Nitrogen Oxides after Adoption of No. Emission Controlled Cars in 1999	
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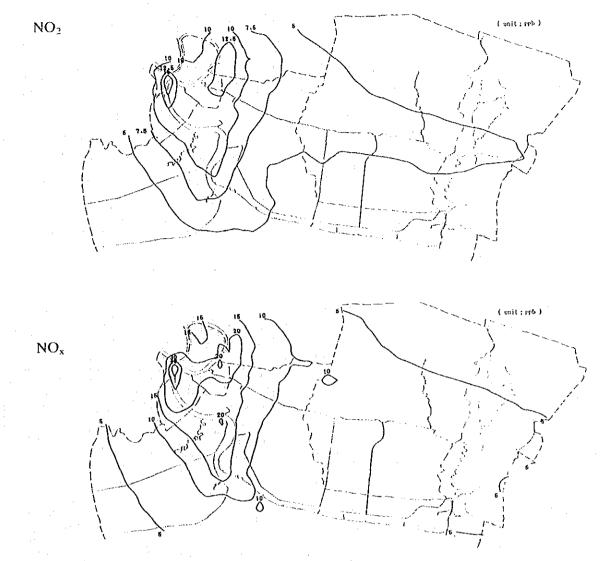


Fig. 4-5 Ambient Concentration of Nitrogen Oxides after Adoption of NO_x Emission Controlled Cars in 1999 Table 4-14 Number of Meshes by Ranking of Concentrations of Air Pollutants (When countermeasres are implemented)

n An an tao		(SO2)
Rank of	Nusab	er of	nesh
cocentra- tion (ppb)	1988	1992	1999
0.0~ 5.0	977	929	885
5.0~10.0	128	154	150
10.0~15.0	28	42	67
15.0~20.0	21	16	24
20.0~25.0	5	14	13
25.0~30.0	0	4	13
30.0~35.0	. 0	0	6
35.0~40.0	: 0	0	1
TOTAL	1159	1159	1159

			. •	
			(NO2)
	Rank of	Numb	er of	mesh
9	cocentra- tion (ppb)	1983	1992	1999
5	0.0~ 5.0	674	476	300
0	5.0~ 7.5	305	429	437
7	7.5~10.0	109	104	190
4	10.0~12.5	64	93	68
3	12.5~15.0	7	46	55
3	15.0~17.5	0	10	68
6	17.5~20.0	0	1	28
1	20.0~22.5	0	0	7
9	22.5~25.0	0	0	6
-	TOTAL	1159	1159	1159

		(NO	()
Rank of	Numb	er of	∎esh
cocentra- tion (ppb)	1988	1992	1999
0.0~ 5.0	277	223	169
5.0~10.0	676	643	544
10.0~15.0	116	141	228
15.0~20.0	79	92	68
20.0~25.0	9	51	68
25.0~30.0	2	7	61
30.0~35.0	0	1	13
35.0~40.0	0	1	6
40.0~45.0	0	0	0
45.0~50.0	0	0	1
50.0~55.0	0	0	1
TOTAL	1159	1159	1159

4.4.2 Contribution Rate and Contributory Concentration by Emission Source

Table 4-15 and 4-16 show the contributory concentrations and contribution rates by emission source for the top 8 points of the highest concentration of SO_2 and NO_2 (all below environmental control standard value) after implementation of countermeasures. As compared with contributory concentrations by emission source (Table 3-5) when no countermeasure is taken, the contributory concentration of SO_2 of sources at factory point source is lower due to K-value control for factories. Looking at NO_2 contributory concentration, it can be seen that adoption of NO_x emission controlled cars induces a reduction in the contributory concentration of cars and that the contributory concentration of factory points source is also reduced as factory stacks are made higher.

 Table 4-15
 Contributory Concentrations by Emission Sources at SO₂ High Concentration Points after Implementation of K-value Control

			and the second	
(Rank 1 - 1X, 1Y=15,	.23)	(Rank 2 1X, 11=17,23)	(Rank 5 1X, 1Y=15, 22)	(Rank 6 1X, 17-17, 24)
Type of source	Conce. Rate	Type of source Conce. Rate	Type of source Conce. Rate	Type of source Conce. Rate
SED) Coun Fact Sta. ty Ho, Ko.	contr. contr.	SED) Goun Fact Sta. contr. contr. ty No. No. (ppb) (6)	SEO) Coun Fact Sta. contr. contr. by No. No. (spb) (36)	SED) Coun Fact Sta. contr. contr. ty No. No. (ppb) (96)
Factory (Fig)			Fac- Bar- Bar- Bar- Bar- Bar- Bar- Bar- Bar	Jac Image: Section of the
h-un	18:88 78:1	Resalning stacks 6.831 22.7 Sub total 16.439 51.4	Romajning stacks 7.894 26.7 Sub Iolai 14.105 47.1	Remaining stacks 7.151 24.4 Sub total 15.917 54.3
Factory (area source) factory (industrial estate) kortonys fessels (sailing) ferrytoals (sailing) ferrytoals (sailing) back ground	1,199 1,199	Factory (area source) actory (area source) (actory (industrial estate) (actory (industrial estate)	Factory (area source) 8,533 29,2 Jactory (industrial estate) 9,000 9,000 Jactory (industrial estate) 9,000 9,000 Jactory (industrial estate) 9,000 9,000 Jactory (industrial estate) 9,000 1,000 Jactory (industrial estate) 0,000 1,000 Jactory (industrial estate) 0,000 0,000	Sectory (area source) 8.578 33.3 jetory (industrial cstate) 1.000 0.33 jetory (industrial cstate) 1.000 0.33 fencosts (sailing) 2.501 3.85 ferrybeats (sailing) 0.000 0.33 Berk groups 0.000 0.33
TOTAL	31.830 100.0	TOTAL 30.235 109.0	TOTAL 29.596 100.0	TOTAL 29.304 100.0
(Rank 3 X, Y=16,	,24)	(Rank 4 X, Y=16, 23)	(Rank 7 IX, IY=(5, 21)	(Rank 8 1X, 1Y=15,24)
Type of source	.24) Conce. Raje conir, conir. (ppb) Cal.	(Rank 4 IX, IY=16, 23) Type of source Conce. Rate SED Comp. Fact. Si.e. Contr., cont	· · · · · · · · · · · · · · · · · · ·	L
Type of source 500 Cog, Figst Sta. 310 3 75 31 75 11 31 75 12 13 75 12 13 75 12 14 1 1 150 3 12 160 30 34 10 33 34	Cerce. Bale of the control of the co	Type of source Corp.e. Rate of source SEW Gara Fact Stat. Gara G	$ \begin{array}{c c} \mbox{(Renk 7 IK, IY=15, 21)} \\ \hline \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \$	(Rarck 8 IX, IY=15, 22)
Type of source 500 Con Fact Sta. 10 3 75 11 7 11 3 75 11 7 11 7 10 3 73 11 7 11 7 11 7 11 7 11 7 11 7 11 7 11 11 7 11 11 11 7 11 </td <td>Conce. Rate of ol contr. contr. (ppb) (Xa)</td> <td>Type of source Corp.e. Rate of a source SED Gam Fact Sia. Gam Sia. Gam Sia. Gam Sia. Sia.</td> <td>(Rank 7 IX, IY=15, 21) Type of source Corre. Rate 580) Cour Fact. Sta. confr. Cost 10 Rate State 11 Rate State 12 Rate State 13 Rate State 14 Rate State 15 Rate State 16 Rate State 16 Rate State 17 Rate State 18 Rate St</td> <td>(Rank 8 IX, IY=15, 24) Type of source Cocce, Raje SED) Cove Fact Sta, colr, coff, No. Sec. Cocce, Raje</td>	Conce. Rate of ol contr. contr. (ppb) (Xa)	Type of source Corp.e. Rate of a source SED Gam Fact Sia. Gam Sia. Gam Sia. Gam Sia.	(Rank 7 IX, IY=15, 21) Type of source Corre. Rate 580) Cour Fact. Sta. confr. Cost 10 Rate State 11 Rate State 12 Rate State 13 Rate State 14 Rate State 15 Rate State 16 Rate State 16 Rate State 17 Rate State 18 Rate St	(Rank 8 IX, IY=15, 24) Type of source Cocce, Raje SED) Cove Fact Sta, colr, coff, No. Sec. Cocce, Raje

Table 4-16 Contributory Concentration by Emission Sources at NO₂ High Concentration Points after Adoption of NO_x Emission Controlled Cars in 1999

Rate Str	[~~~~								
Bate Solt	000000000000000000000000000000000000000	3.7		100.0		Set ate	500000000000000000000000000000000000000	3.02	00000000000000000000000000000000000000	100.0
Conce. of contr. (ppb)	00000000000000000000000000000000000000	0.518	00000000000000000000000000000000000000	14.027	ເຊິ່	Conce. of contr. (ppb)	83899999999999999999999999999999999999	0.182 0.491	00000000000000000000000000000000000000	1 -
Type of source SED) Coun Fact Sta.	ව ප්රීම්දීම්දී ප්රීම්දීම්දී ප්රීම්දීම්දී ප්රීම්දීම්දී ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රීම්ද ප්රී ප්රීම්ද ප්ර ප්රීම්ද ප්ර ප්ර ප්ර ප්ර ප්ර ප්ර ප්ර ප්ර ප්ර ප්ර	Remaining stacks Sub total	Factory (area source) Factory(industrial estate) Roadwary (ailing) Vessels (sailing) Ferrybats (anchoring) Farrybats (sailing) Back ground	TOTAL	(Rank 8 IX, IY=2)	Type of source SED) Coun Fact Sta. No. No.	55 55 55 55 55 55 55 55 55 55 55 55 55	Remaining stacks Sub total	Factory (area source) Factory (industrial estate) Factory (industrial estate) Nessels (sailing) Ferrybacts (anthoring) Ferrybacts (sailing) Factorats (sailing)	TOTAL
Rate Contre Contre	200000000000000000000000000000000000000	0.9 3.0	20060000	100.0		Rate Contr	000000000000000000000000000000000000000	2:9	-00-4008	100.0
Conce. of (ppb)	00000000000000000000000000000000000000	8:125		14.088	(12,	Conce. of contr (ppb)	83338888888888888888888888888888888888	0.988 0.4888		13.971
Type of source SBD) Coun Fact Sta. ty No. No.	196 196 196 196 196 196 196 196 196 196	Remaining stacks Sub total	Factory (area source) Pactory(industrial estate) Roadways (aailing) Vessels (sailing) Ferryboats (ancioring) Ferryboats (sailing) Back ground	TOTAL	(Rank 7 IX, IY=22,	Type of source SE2) Coun Fact Sta.	26 24 26 24 26 24 26 20 26 20 20	Remaining stacks Sub total	Factory (area source) Factory(industrial estate) Roedways (sailing) Ferryboats (anchoring) Ferryboats (sailing) Back ground	TOTAL
of contr. of contr. (ppb) (%)	00000000000000000000000000000000000000	8.234 5.2		10.00 100.0	(X	of of of contr. (%)	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	8:255 2:3	2225222 222525 222525 225525 225525 225525 225525 235555 2355555 2355555 2355555 2355555 2355555 2355555 2355555 2355555 2355555 2355555 2355555 2355555 2355555 23555555 23555555 23555555 23555555 23555555 23555555 235555555 2355555555	14.338 100.0
Type of source (1) SER) Coun Fact Sta. ty No. No. A.	50 50 50 50 50 50 50 50 50 50 50 50 50 5	Remaining stacks Sub total	Factory (area source) Reactory (industrial estate) Reactory Vessels (sailing) Ferryboats (anchoring) Ferryboats (sailing) Back ground	TAL	C Rank 4 IX, IY=15,	Type of source SEQ) Coun Fact Sta.	56 5 4 50 5 5 4 50000000000000000000000000	Remaining stacks Sub total	Factory (area source) Factory (industrial sstate) Redways Readways (sailing) Ferryboats (sailing) Ferryboats (sailing) Beck ground	TOTAL
Set Rate	00000000000000000000000000000000000000	1.5	နင့္ရရွိထုလိုက္ လင္လလလန်ဆံ-	0.01		Rate of contr 33	000000000000000000000000000000000000000	2.9	70.1 2000 1.0 2.5 2.5 1.0 2.5 2.5 1.0 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5	100.0
Conce. of (ppb)	20000000000000000000000000000000000000	0.734 0.785	00000000000000000000000000000000000000	17.866	(<u>8</u>	Conce. of contr, (ppb)	88588888888888888888888888888888888888	8.415		14.549
Type of source SE0) Coun Fact Sta. ty No. No.	iio iio iio iio iio iio iio iio iio iio	Remaining stacks Sub total	Factory (area source) actory (industrial estate) machans rescis (sailing) Ferrybads (anchoring) Ferrybads (sailing) Back ground	TOTAL	[Rank 3 IX, IY=22	Type of source SEQ) Coun Fact Sta. ty No. No.	55 55 55 55 55 55 55 55 55 55 55 55 55	Remaining stacks Sub total	Factory (area source) Factory (area source) Racdways Reachays Vessels (sailing) Ferryboats (ancioring) Ferryboats (sailing) Back ground	TOTAL
-	e of source Conce. Rate Type of source	c of source Conce. Part c of source Conce.	Conce. Parte Conce. <	Conce. Rate of (point) Type of source (point) Conce. Rate of (point) Type of source (point) Conce. Rate of (point) Type of source (point) Conce. Rate of (point) Type of source Conce. Rate of (point) Type of source Type of source Type of source Type of source 0.0011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 0.011 <td< td=""><td>Conce. Parte Type of source Conce. Rate Type of source Conce. Conce<</td><td>$\begin{array}{c c c c c c c c c c c c c c c c c c c$</td><td>Opene Dete Type of source Conce. Rate Sign Conce. Sign Conce. Sign</td><td>Opene Parte Conce Res Type of source Res Conce Res</td><td>Opene Desc <thdesc< th=""> Desc Desc <th< td=""><td></td></th<></thdesc<></td></td<>	Conce. Parte Type of source Conce. Rate Type of source Conce. Conce<	$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	Opene Dete Type of source Conce. Rate Sign Conce. Sign Conce. Sign	Opene Parte Conce Res Type of source Res Conce Res	Opene Desc Desc <thdesc< th=""> Desc Desc <th< td=""><td></td></th<></thdesc<>	

PART VII SPECIFIC REMEDIES FOR EMISSION SOURCES, COST ESTIMATION, AND ANALYSIS OF ECONOMIC IMPACTS

1. Outline

In view of the considerations in the preceding Part VI, if emission controls for factories are to be adopted in the future, then we feel that the K-value controls are appropriate and we came to the conclusion that the most practical method would be to increase the height of stacks. Moreover, it was found that the appropriate value of K is 13 and that the stacks, for which countermeasures are really required, are 49 units in number. Thus, this Part VII will hereafter discuss the roughly estimated expenses required to implement the countermeasures, and the impact of such investment on the economy of the Samut Prakarn regions or Thailand as a whole. Also described are overview of remedial other options for controlling SO₂ emission than making stacks taller besides the general picture of reduction techniques for NO_x and particulate matters are also described.

2. Practice of Making Stacks Taller and Their Investment Cost

2.1 Determinants of the Stack Structure

If K=13, the number of stacks to be made taller is 49 as attested by Table 4-4 of Part VI. Though these facilities are called stacks, there are some which are simply emission outlets or which, if actual stacks, do not sufficiently contribute to the diffusion of pollutants because of an umbrella placed on top. As a consequence, it is not necessarily realistic to make stacks taller. Generally, the factors for determination of a stack structure include the items specified below, which should be fully examined in light of laws and regulations or the functions of a stack.

2.1.1 Meteorological and Site Conditions

It is necessary to grasp the current and future conditions of the site surrounding stacks and examine such meteorological conditions as wind direction and wind velocity, as well as geographical features. it is further necessary to study the stack heights (over 2.5 times those of adjacent buildings) and the discharge velocity at stack mouths (over twice the wind velocity) in order to avoid adverse effects on adjacent buildings, such as downwash or downdraft.

2.1.2 Pressure Loss and Effective Draft

After considering the combustion conditions of a boiler, the capacity of a blower and pressure loss of a path to a stack, the effective draft of combustion (effective draft power) is set to determine the structure of a stack.

The effective draft power of a stack is calculated as follows:

$H_t = H_o - P_{total}$		(2-1)
$H_o = h(\rho_a - \rho_g)$	· · · · · · · · · · · · · · · · · · ·	(2-2)

VII - 1

 $P_{total} = P_{t} + P_{b} + P_{f} \qquad (2-3)$ $P_{t} = \zeta_{1} \times \frac{\varrho g \times V^{2}}{2 \times G} \qquad (2-4)$ $P_{b} = \zeta_{2} \times \frac{\varrho g \times V^{2}}{2 \times G} \qquad (2-5)$ $P_{f} = \lambda \times \frac{h}{D} \times \frac{\varrho g \times V^{2}}{2 \times G} \qquad (2-6)$

where;

- H_t : Effective draft of a stack (m)
- H_o : Theoretical draft of a stack (m)
- h : Stack height (m)
- $\rho_{\rm a}$: Specific weight of air (kg/m³)
- $\rho_{\rm g}$: Specific weight of emission gas (kg/m³)
- Ptotal: Total pressure loss
- P_t : Extrusion loss
- P_b : Curve loss
- P_f : Friction loss
- $\zeta_1, \zeta_2, \lambda$: Loss factor
- V : Flow rate of emission gas (m/s)
- G : Acceleration of gravity (m/s^2)
- D : Internal diameter of stack (m)

2.1.3 Establishment of Actual Stack Height

With effective stack height calculated, the actual stack height is established. Effective stack height can be calculated based on an emission standard (K value). That is to say, in Samut Prakarn province, the adoption of K=13 leads to the calculation of the effective stack height (He) based on the following equation (2-7):

 $He = (q \times 10^3/K)^{1/2}$

where;

q: Emission volume of SO₂ (Nm³/h)

2.2 Prerequisites for Study of Making Stacks Taller

2.2.1 Stack Structures

Roughly divided, there are the following 4 types of structures in building stacks. (See Fig. 2-1.)

(1) Self standing

This is suitable for small-size stacks. However, it is necessary to take into consideration vibration caused by Karman vortex, and this type is unfavorable when the radius of a stack is small. In addition, thermal insulation is required according to emission gas conditions.

- ② Supported by RC shell This is suitable for medium- and large-size stacks. Adiabatic insulation is required if the temperature of emission gas is high.
- (3) Supported by steel shell

This is suitable for medium- and large-size stacks. Although no thermal insulation is necessary regardless of the emission gas conditions, coating of the outer shell is required (once every 5 to 10 years).

(4) Supported by steel structure

This is suitable for medium- and large-size stacks. Thermal insulation is required according to emission gas conditions, coupled with coating of the steel structure (once every 5 to 10 years).

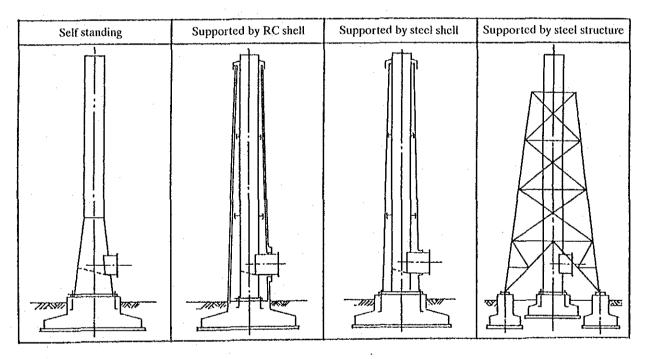


Fig. 2-1 Structures of Stacks

Since the stacks targeted in this study, as shown in Table 2-1, are in the range of 3 m to 38 m in stack height after the stacks are made taller, their structures should be decided after taking the conditions of individual cases into account. The individual conditions, however, are unknown for the present. We, therefore, decided to apply the "supported by steel shell" type to the most stacks, but the "self standing" type to the stacks listed in "2-24-2 (County code—Factory number—Stack number)" because its height is only 3 m after it is made taller.

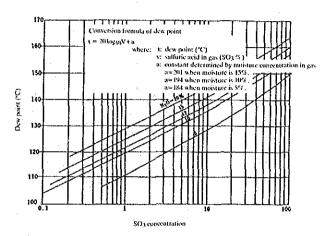
· · · ·				Present	Gas	Normal	Normal	 ;	k Dia. (m)	
SEQ	County	Factory	Stack	stack	temper-	exhaust gas	SO ₂ emission	Internal	External	New stack height
9EQ	code	No.	No.	height	ature	volume	volume	Sus	Cs	$H_{u}(m)$
				H. (m)	T (°K)	$Q (m^3/S)$	$q (Nm^3/h)$	Tube	Stack	11 ₀ (m)
1)	3	75	ľ	5	313	26.092	31.697	1.55	2.2/3.5	38.0
2)	3	. 34	. 3	5	350	2.935	5.610	0.55	1.2/1.6	17.0
3)	2	23	4	.5	350	2.697	3.281	0.53	1.2/1.2	12.5
4)	1	68	. 2	20	462	6.712	28.970	0.96	1.6/3.4	37.0
5)	3	23	5	5	333	4.349	2.633	0.65	1.3/1.3	10.0
6)	3.	24	1	7	462	0.350	1.812	0.22	0.9/1.0	10.5
7)	3 2 3	. 24	2	2	437	0,157	0.186	0.14		3.0
8)	5	96	1	5	350	5.849	4.548	0.78	1.4/1.4	13:0
9)	3,	33	2	. 6	437	0.007	0.971	0.03	0,7/0,8	8.5
10)	1	39	1	15	462	2.940	18.078	0.63	1.3/2.9	31.5
11)	2	19	2	6	523	0.519	2.019	0.28	0.9/1.0	10.5
12)	- 3	97	1	. 5	318	0.125	0.652	0.11	0.8/0.8	6.5
13)	1	68	t .	15	462	1.860	8.047	0.50	1.2/1.9	21.0
14)	1 -	66	1	.10	453	1.570	6.206	0.46	1.1/1.7	18.5
15)	3	59	2	10	443	1.852	6.647	0.49	1.1/1.7	19.0
16)	3	- UH	2	22	496	6.119	24.545	0.95	1.6/3.0	33.0
17)	1	56	2	6	448	1.482	2.703	0.44	1.1/1.1	11.0
18)	3	14	1 L _	20	483	4.587	16.464	0.81	1.5/2.5	27.5
19)	3	14	2	20	483	4.587	16.464	0.81	1.5/2.5	27.5
20)	3	- 109 1	2	12	462	0.926	4.858	0.36	1.0/1.6	17.0
21)	3	90	1	10	462	0.932	3.649	0.36	1.0/1.4	14.5
22)	1	70	3	6	437	1.639	2.567	0.46	1 1/1.1	10.5
23)	1	35	2	15	483	1.305	5.895	0.43	1.1/1.7	18.0
24)	3	54	· · 1	16	448	1.864	9.730	0.50	1.2/2.2	23.5
25)	1	35	1 I	15	483	1.305	5.857	0.43	1.1/1.7	18.0
26)	3	16	4	15	473	1.813	9.512	0.50	1.2/2.1	23.0
27)	3	102	1	13	462	. 2.319	9,008	0.56	1.2/2,0	21.5
28)	. 1	68	3	20	462	2.237	9.657	0.55	1.2/2.1	22.5
29)		66	2	14	453	2.223	8.796	0.54	1.2/2.0	21.5
30)	3.	16	3	15	473	1.449	7.608	0.45	1.1/1.9	20.5
31)	3	47	3	12	498	2.025	7.922	0.55	1.2/1.9	20,0
32)	ĩ	2	1	12	473	1.778	6.381	0.50	1.2/1.7	18.0
33)	3	109	i	15	462	1.237	6.478	0.41	1.1/1.8	19.5
34)	1	64	l	10	462	0.667	2.609	0.30	1.0/1.1	12.0
35)	1	70	2	18	573	5.406	16.113	0.96	1.6/2.2	23.5
36)	3	5	2	24	523	9.631	27.299	1.22	1.9/2.7	29.5
37)	3	16	1	15	473	1.086	5.692	0.39	1.0/1.7	18.0
38)	3	16	2	15	473	1.086	5.692	0.39	1.0/1.7	18.0
39)	1	70	1	18	573	4.317	12.890	0.85	1.5/2.0	21.5
40)	3	54	2	18	473	1.864	9.730	0.51	1.2/2.1	23.0
41)	3	54	3	18	473	1.864:	9,730	0.51	1.2/2.1	23.0
42)	3	110	2	10	462	0.556	1.994	0.28	0.9/1.0	10.5
43)	2	5	6	10	462	0.608	2.226	0.29	0.9/1.1	11.5
44)	3	28	1	10	462	0.445	1.979	0.25	0.9/1.0	11.0
45)	l	55	l l	30	393	4.230	22.098	0.70	1.3/3.3	35.5
46)	1	55	2	30	393	4.230	22.098	0.70	1.3/3.3	35.5
47)	3	14	3	20	483	2.293	8.232	0.57	1.2/1.9	20.0
48)	I	64	2	6	462	0.196	0.622	0.16	0.8/0.8	6.0
49)	3	95	2	7	333	1.141	0.886	0.33	1.0/1.0	7.0

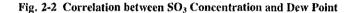
Table 2-1 Stack Height Required to Fulfill K=13

2.2.2 Materials of Stacks

Since the facilities targeted for higher stacks in the present study, though naturally, emit SO_x in high concentrations, the stacks material must be stainless steel. There is commonly a correlation between the sulfuric acid dew point and the emission gas temperature as shown in Fig. 2-2. In the case that SO_x concentration is high and the gas temperature is below 200°C as in this study, it tends

to fellow sulfuric acid dew point. Consequently, it is important that the stacks with a temperature lower than 200°C are designed so that the decline of emission gas temperature should be minimized by providing 50 mm of rock wool as adiabatic material between the internal and external shells.





2.2.3 Stack Height and Diameter

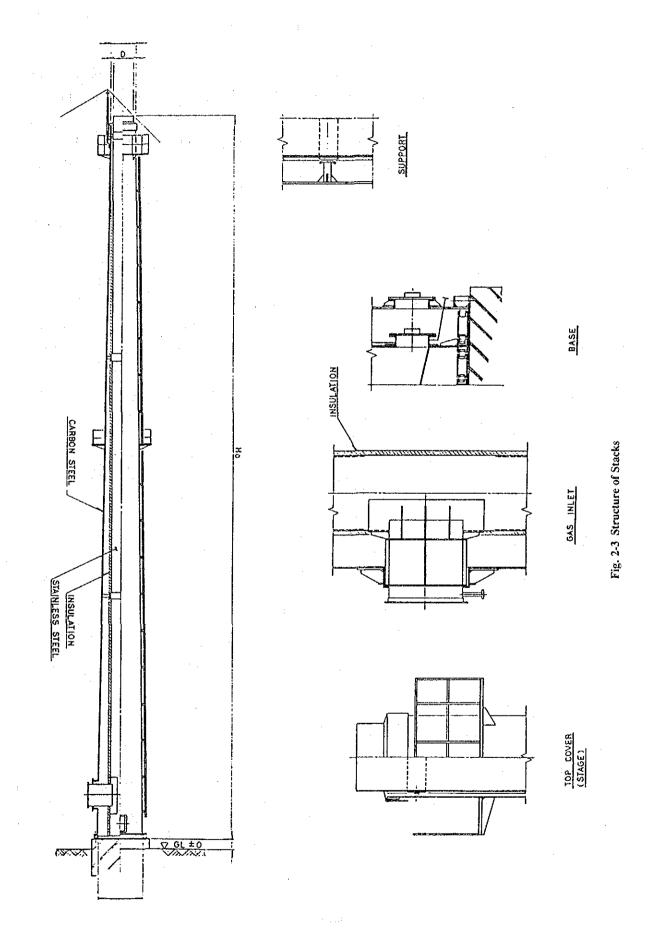
When the stack diameter is determined, pressure loss and effective draft are the main factors. If they are unknown, however, it is empirically considered economical to arrange the flow rate at the stack outlet to be 10 to 20 m/s. In this study, therefore, the stack height has been calculated based on the factors that the stack flow rate is 15 m/s and the K value is 13. The fractions in calculation were rounded up to the unit of 0.5 m. The height set for each stack is shown in Table 2-1.

2.3 Expenses for Making Stacks Taller

The expenses to be incurred for making stacks taller has been calculated based on the prerequisites in Section 2.2 as shown in Table 2-2. While the expenses include the costs for the material, assembly, and thermal insulation/coating of stacks, the costs for foundation work are not included because of unknown geological features. As shown in Fig. 2-3, in addition, the stacks will be all replaced with new ones, with no attention paid to the presence of location space for remodeling of the existing stacks and installation of new ones. According to Table 2-2, in the case that 49 stacks are renewed to be made taller, it will cost approximately 115 million baht, proving that simply making stacks taller will unavoidably require a large amount of investment. Although no operating cost is necessary, furthermore, coating of the outer shell will be required to be done once every 5 to 10 years.

·			0, J	Gas	Normal	Normal SO ₂	New	Stack	
SEQ	County code	Factory No.	Stack No.	temper- ature T (°K)	exhaust gas volume Q (m³/S)	emission volume q (Nm³/h)	Dia (m)	Height H _o (m)	Cost (×10 ³ Bahts)
		715	1	313	26.092	31.697	1.55	38.0	à 100
1)	3	75 34	13	313	26.092	5,610	0.55	17.0	8,100 2,000
2)	32	23	4	350	2.697	3.281	0.53	12.5	1,400
3)		68	2	462	6.712	28.970	0.96	37.0	6,150
4) 5)	3	23	5.	333	4.349	2.633	0.90	10.0	1,300
- 2J - 63		23	1	462	0.350	1.812	0.05	10.0	900
6) 7)	2	24	2	402	0.157	0.186	0.22	3.0	85
8)		96	1	350	5.849	4.548	0.78	13.0	2,050
0) 9)	3	33	2	437	0.007	0.971	0.78	8.5	450
10)		39	1	462	2.940	18.078	0.63	31.5	3,700
11)	2	19	2	523	0.519	2.019	0.28	10.5	1,050
12)	3	97	1	318	0.125 1.860	0.652 8.047	0.11	6.5	450
13)		68	1	462	1.600		0.50	21.0	2,300
14) 15)		66 50	1	453	1.570	6.206	0.46	18.5	1,700
:15)	3	59	2	443 496	1.852	6.647	0.49 0.95	19.0 33.0	1,950
16)	3	111	2		6.119 1.482	24.545 2.703			5,600
17)	- 1	56		448 483	4.587	16.464	0.44 0.81	11.0 27.5	1,200
18)	3	14 14	1 2		4.587	16.464	0.81	27.5	4,250
19) 20)	3	109	2	483 462	4.387	4.858	0.81	17.0	4,250
	L					· · · · · · · · · · · · · · · · · · ·			1,550
21)	3	90	1	462	0.932	3.649	0.36	14.5	2,400
22)	1	70	3	437	1.639	2.567	0.46	10.5	1,300
23)	. 1	35	2	483	1.305	5.895	0.43	18.0	1,650
24)	3	54	1	448	1.864	9.730	0.50	23.5	2,400
25)		. 35	1	483	1.305	5.857	0.43	18.0	1,650
26)	3	16	4	473	1.813	9.512	0.50	23.0	2,350
27)	3	102	1	462	2.319	9.008	0.56	21.5	2,300
28)		68	3	462	2.237 2.223	9.657 8.796	0.55	22.5	2,300
29) 30)	3	66 16	2 3	453 473	2.223	8.796 7.608	0.54 0.45	21.5 20.5	2,300 2,150
31)	3	47	3	498	2.025	7.922	0.55	20.0	2,150
32)	1	2	1	473	1.778	6.381	0.50	18.0	1,700
33)	3	109	1	462	1.237	6.478	0.41	19.5	1,900
34)	1	64	1	462	0.667	2.609	0.30	12.0	1,100
- 35) —		70	2	573	5.406	16.113	0.96	23.5	4,400
36)	3	. 5	2	523	9.631	27.299	1.22	29.5	7,100
37)	3 -	16	· 1	473	1.086	5.692	0.39	18.0	1,650
38)	3	16	2	473	1.086	5.692	0.39	18.0	1,650
39)		70	1	573	4.317	12.890	0.85	21.5	4,000
40)	3 ·	_ 54	2 ·	473	1.864	9.730	0.51	23.0	2,600
41)	3	54	3	473	1.864	9.730	0.51	23.0	2,600
42)	3	110	2	462	0.556	1.994	0.28	10.5	950
43)	2	5	6	462	0.608	2.226	0.29	11.5	1,000
44) .	3	28	1	462	0.445	1.979	0.25	11.0	950
45)		55	1	393	4.230	22.098	0.70	35.5	3,900
46)		55	2	393	4.230	22.098	0.70	35.5	3,900
47)	3	14	3	483	2.293	8.232	0.57	20.0	2,150
48)		64	2	462	0.196	0.622	0.16	6.0	100
49)	3	95	2	333	1.141	0.886	0.33	7.0	200

Table 2-2 Expenses for Making Stacks Taller





3. Improvement of SO_x Emission Sources Other than Making Stacks Taller

In the case that remedies at emission sources are worked out with K value regulation as a prerequisite, a possible way other than making stacks taller is to reduce the emission volume of SO_2 , having the following three specific methods: (1) fuel oil desulfurization to reduce the sulfur content of fuel to be used; (2) conversion of fuel to a low sulfure type; and (3) flue gas desulfurization to remove SO_2 in emission gas generated. With reference to the said three methods, the outline of the systems will be hereunder described, coupled with roughly estimated costs when they are applied.

3.1 Desulfurization of Fuel Oil (Heavy Oil)

The technics for fuel oil desulfurization include the use of microorganism, irradiation of radioactivity, metal oxides, and catalytic hydrodesulfurization. For the present, however, hydrodesulfurization alone can be performed technically and economically. Currently, hydrodesulfurization of fuel oil being industrially put into practice can be roughly divided into three methods, direct desulfurization, indirect desulfurization, and a modified indirect desulfurization combining both. Fig. 3-1 to 3-3 show the system diagrams of these methods.

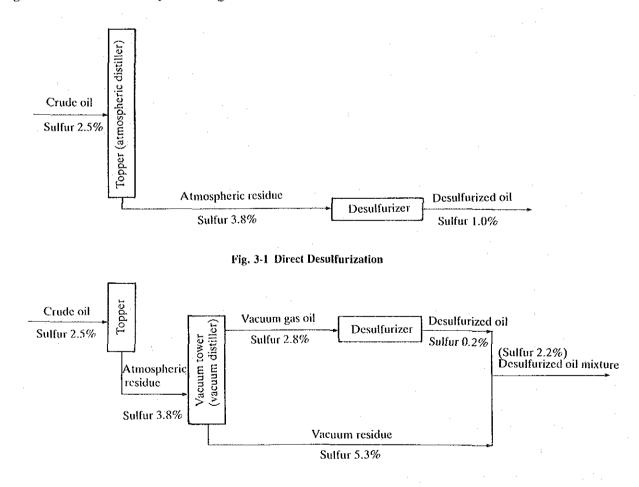


Fig. 3-2 Indirect Desulfurization

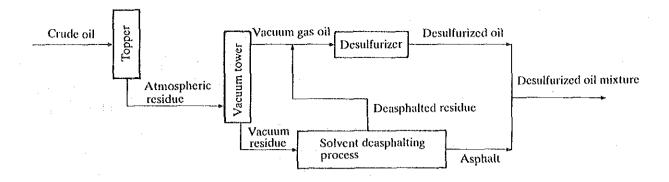


Fig. 3-3 Modified Indirect Desulfurization

3.1.1 Direct Desulfurization

In this method, the still residue (atmospheric residue) of an atmospheric distiller is introduced into a desulfurizer as it is and is then hydrodesulfurized under high temperature, high pressure, and the presence of a catalyst, reportedly enabling about 75% to be desulfurized. This method can be roughly divided into two types, namely, fixed bed and fluidized bed, depending on whether the catalyst to be used is fixed or fluidized inside the reactor. In both types reaction takes place at a reaction temperature of 350°C to 450°C, a reaction pressure of 50 kg/cm² to 200 kg/cm², and a liquid hourly space velocity (LHSV) of around 1.0. Generally the fluidized bed type is favorable for fuel oil containing an abundant asphaltene content and metallic components such as vanadium. As seen in Table 3-1, however, this type is not too desirable when there is great demand for fuel oil because produced oil becomes lighter compared with the fixed bed.

· · · · · · · · · · · · · · · · · · ·	Fluidized bed	fixed bed
Products yield (Vol%)	1.5 (Wt%)	0.4 (Wt%)
Gas, LPG Naphtha	4.3	1.2
Middle fraction	17.6	10.0
Residue	79.5 (S=1.0 Wt%)	90.5 (S=1.0 Wt%)
Hydrogen consumption (Nm ³ /kl)	113	123

 Table 3-1 Typical Products Yield and Property of Fluidized Bed and Fixed Bed

 (Quwait atmospheric residue; Sulfur 3.8 wt%)

3.1.2 Indirect Desulfurization

By this method atmospheric residue is once vacuum distilled to be separated between vacuum gas oil containing small amounts of catalyst poisoned substances (for example, asphalten content, and organic metallic compounds such as vanadium and nickel) and vacuum residue in the form of their concentration. Then, vacuum residue is mixed with desulfurized oil obtained as a result of hydrodesulfurizing only the vacuum gas oil which is easily desulfurized, resulting in the production of a low sulfur oil. As a consequence, the rate of desulfurization is as high as 90% to 95% in light of vacuum gas oil, whereas the said rate is about 40% to 45% in light of atmospheric residue.

3.1.3 Modified Indirect Desulfurization

While modified indirect desulfurization is an intermediate method between direct and indirect desulfurization, it can be said to belong to indirect desulfurization in that it separates asphalt content. As shown in Fig. 3-3, this method is the same as indirect desulfurization up till the process of vacuum distilling atmospheric residue to separate vacuum gas oil from vacuum residue. In accordance with this method, however, vacuum residue is further treated with propane or the other solvent to be separated between soluble and insoluble contents. This soluble content (deasphalted oil) is desulfurized together with vacuum gas oil and is mixed with the insoluble content (deasphalted residue), thus resulting in the production of final desulfurized oil. The application of this method enables desulfurization to the extent that the final sulfur content will become about 1.5% (about 60% in terms of the desulfurization rate).

3.1.4 Fuel Oil Desulfurization as a Improvement of Emission Sources

When fuel oil is desulfurized as a improvement of emission sources, it is necessary to solve the problems specified below.

(1) Unification of fuels in use

As shown in Table 3-2, the fuels being used at the target facilities include A grade fuel oil, B grade fuel oil, C grade fuel oil, and light oil, as well as coal, and their sulfur contents are in the range from 1.2% to 3.5%. It is therefore necessary to unify fuels used by various firms into a fuel of the same kind.

(2) Whether necessary to modify facilities with fuel conversion

A question raised in the above (1) unification of fuels in use is whether fuel conversion can be attained without structural modification. Particularly in the case that general coal is used in the factories listed in the "1-39-1 (County Code-Factory No.-Stack No.)," it is thought that substantial modification of facilities will be required.

(3) Determination of desulfurization capacity

As understandable from the emission volume of SO_2 by stack required to fulfill K=13 shown in Table 3-3, about 50% reduction is necessary even if S=1.2% in the case of the factories listed in the "2-24-2." Accordingly, the specification of the fuel to be unified must be less than S=0.6%. For other facilities, however, desulfurization to the extent that S=0.6% is not necessary because otherwise it would result in facilities with over-capacity. When desulfurization capacity (especially for the sulfur content of a product) is determined, consequently, it will be necessary to find an optimum point, in which case for some facilities, desulfurization should be performed concurrently with other countermeasures for emission sources.

Table 3-3 SO₂ Emission Volume Required to Fulfill K=13

Table 3-2 Quality and Consumption Volume of Fuel for the Facilities at which K=13 must be Achieved

SEQ

<u>କନ୍ନନ୍ନକ୍ନକ୍ଳକ୍ର୍ୟୁ କୁନ୍ତି କୁନ୍ତୁ</u>

13:0						T												Ţ		• • • • • •										
SO ₂ emission volume at K=13.0 q (Nm ³ /h)	4.576 1.076 1.001	10.990	608.0	2.199	0.472	1.026	0.337	3.303	3.562	1.703	10.600	3.225	2.466	4.U82 6.76i	4-082 6-674	6.379	1007	2.82	6.110 4.952 5.184	2.105	23.780	20.2	8.699	8.699 1.812	2.028	20.695	269.92 7	0.606	0.871	
Normal SO ₂ emission volume q (Nm ³ /h)	31.697 5.610 3.281	28:970	1.812	4.5480	120.01	2.019	0.652	6.206	6.647 24.545	2.703	16.464	4.858	3.649 2.567	c62.6	5.857	8	8.796	7.608	7.922 6.381 6.478	2.609	27.299	5.692	9,730	9.730 057.6	2.226	22.098	22.098	8,227	0.886	
Normat exhaust gas volume O (m ³ /S)	26.092 2.935 2.697	6.712	0.350	5,849	0.007	0.519	0.125	1.570	1.852	24- 24-	1.587	0.926	0.932	CUS.1	1.305	2.319	2.22	1.449	2.025 1.778 1.237	0.667 5.406	9.631	1.086	1.864	1.864 0.556	0.608	4,230	4.230	0.19	1,141	
Gus temperature T (°K)	350	462 333	3 5 1	350	437	23	318	453	54 54 54	ţ,	ç Ç	462	22 22 23 23	2 2	89 F	5	2 1 2 1	4/3	473 473 473	555 273	ន្លផ	161	473	- 473 462	69 262	393	393	33	533	
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County rode	ю IP M	e	<u>,</u> w i	N 10		7	100-		юr		<u>,</u>	~	m → -		17			~	m1 m	, 	- m m	י ניי ר		м и	(1)	n	· •	~~·	2	
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Fuel consumption ((/H)	2,400	222		0 XI	538	859 kg/H	11	7 SE	337 395	375	222	318	13 23 23 25 25 25 25 25 25 25 25 25 25 25 25 25	500	88	1 <u>2</u>	885	498	477 311	435 382	- 158 143	299 299	951 97	88	400	611	83	6 § §	267 7	46
Culory (Kcul/kg)	10.430	000,01	10,430	9,900	000'01	6,239	10,495	10.296	10.394	0.340	10,495	000.01	. 015.01	001-01	10.950	006'6	006'6	C67-01	10.394 9.900	007-01	006'6	0000	006'6	006'6	006'6	075.01	10.000	10.336	10.340	10.461
Specific gravity	0.9408	801-6-0	0.948	0.8660	0.9462	1.0(0)	0.9358	0.9561	0.9383	0.9529	006610	0.9462	0.9529	0.9764	0.9200	0066'0	0.9950	0.9558	0.9383	0.9764 0.9529	0.9950	066.0	0.9950	0.9950	0.9930	0.9529	0.9750	0.9900	0.9529	0.960)
Sulfur content (%)	3.00	2.00	380	02.1	212	18	2.76	3.00	21.00	220	0.02		999 999	2.66	1.50	3.50	02.5	28	3.50	2.66	3.50	828	3.50	2.50 2.50	3.50	2.50	5.2	3.50	220	2.50
Fuel	0HA AHO	AHO	PH4 PH4	20 5-	AHO	N S S C S C	OHA	2 H C H C H C H C	AHO PHO	0HO		OHA PHO	395	CHO	AHO AHO	0HO	P P P	AHO	2440 PHO	CHO	e H U	S S S S S S S S S S S S S S S S S S S	0HO	999	OHO UHO	D HO	BHO	295 Ferrore		0HO CHO
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(4) Determination of processing volume

About 3500 barrels/day is the processing volume of fuel oil at the factories (shown in Table 3-2) which require countermeasures for reduction of SO_2 . If this volume is regarded as the processing capacity, however, the fuel oil desulfurization facilities for 3500 barrels/day are to serve only these 49 facilities, leading to the necessity of solving the problem of locations, construction funds, or processing cost.

Since there are, as described above, many difficulties to be solved in the case of fuel oil desulfurization, this countermeasure may not be realistic for the present.

3.1.5 Expenses for Fuel Oil Desulfurization

The estimation of expenses roughly calculated, for reference in comparison with other countermeasures, amounts to about 880 million baht. The prerequisites for this case are as specified below. The construction cost is for one set excluding that for foundation work. It was decided, however, that all requirements except for local construction would be supplied from Japan.

(1) Properties of fuel oil

S=3.0%

SG=0.95

Caloric value=10300 Kcal/kg

- (2) Sulfur content after desulfurization
 S=0.6 (desulfurization rate: 80%)
- ③ Desulfurization method
 Direct desulfurization (to manage a high rate of desulfurization)
- Processing volume3500 barrels/day

3.2 Fuel Conversion

Most of the target facilities are using fuel oil. When the fuel is changed over to another type by fuel conversion, possible candidates will be natural gas, LPG and lignite. Based on discussion with ONEB, however, fuel conversion to natural gas is hereunder reviewed.

3.2.1 Properties of Natural Gas

Among naturally occurring gases, those combustible gases containing hydrocarbon as the major ingredient are commonly called natural gas, including oil field gas, gas field gas, and coal field gas, and are classified into oil soluble type, water soluble type, and free type depending upon the conditions of the gas layer forming a deposit. As shown in Table 3-4, in addition, the properties of gas lead to the major classification of dry gas and wet gas. The former is defined as a gas whose

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combustible content is almost composed of CH_4 , while the latter is defined as a gas which contains a considerable volume of C_3H_8 heavier other than CH_4 and C_2H_6 . The caloric values are about 9000 to 9300 Kcal/Nm³ and 10400 to 12200 Kcal/Nm³, respectively.

· · · · · · · · · · · · · · · · · · ·	· · · · ·				Ingredie	nt (in %)					High caloric value
						C _u H	2n+2				1
	CO ₂	O ₂ :	CO	H_2	Cl	C ₂	C ₃	C,	N_2	S	Kcal/Nm ³
Dry	3.4	0.1			94.6		—		1.9		9000
Wet	0.7	—			75.4	13.6	7.5	2.8			12200

Table 3-4 Properties of Natural Gas

3.2.2 Characteristics of Gas Combustion

As compared with the combustion of fuel oil, gas combustion has the following characteristics:

- (1) Adjustment of combustion can be performed promptly and accurately and is suited for automatic control.
- (2) Flame is stable regardless of the condition of the combustion chamber, yielding a high combustion efficiency.
- (3) It reduces excess air, facilitating the adjustment of atmosphere inside the furnace.
- (4) Concomitant use of many small-size burners makes it easy to freely adjust temperature distribution inside the furnace in terms of space or timing.
- (5) There are no harmful effects of ash and carbon accumulation on combustion chamber, burner, heated matter, and flue.
- (6) Facility cost including piping work is high.
- (7) Radiant heat is small, with a low temperature of combustion chamber.
- (8) It is in danger of causing sanitary harm and explosion due to the CO content of gas or CO produced by incomplete combustion.

3.2.3 Fuel Conversion as a Improvement of Emission Sources (Natural Gas)

In the case that fuel conversion to natural gas is performed as a improvement of emission sources, the following problems should be solved:

(1) Change in the capacity of combustion facilities accompanied by fuel conversion

Because of the small radiant heat of natural gas in comparison with fuel oil combustion as described in the item O of the preceding paragraph 3.2.2, especially the case of a steam boiler entails a possibility that there may be a decline in evaporation ability to meet the same input calorie. As a consequence, in the case of a factory in which the current facilities are almost in full operation, the fuel conversion to natural gas must be examined cautiously.

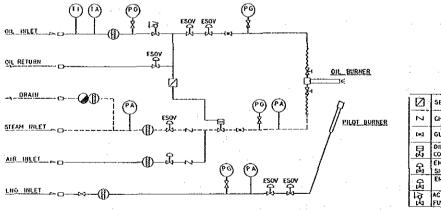
(2) Supply and storage of fuel

While the supply of natural gas is generally carried out through pipelines, if there is a distance between production facilities and the facilities in use, there are such requirements as the installation of a gas holder in the middle, thus incurring the facility cost as mentioned in the item (6) of the preceding paragraph 3.2.2. It is therefore necessary to clarify in advance who will bear this cost, and how. In regard to storage, on the other hand, it may be necessary to provide storage facilities individually depending upon the situation of each user.

3.2.4 Expenses for Fuel Conversion to Natural Gas

The required expenses varies substantially, as described in the previous section, depending upon the view of burdens stemming from the facilities including production facilities up to the gas holder. Assuming the modification of everything at the steam boiler, consequently, herein calculated was the expenses to be incurred purely for modification of burners and their surroundings except for the facility cost of the supply side. The results are shown in Table 3-5. The scope of modification work is specified below. For reference, in addition, Fig. 3-4 to Fig. 3-6 show a system diagram of a burner unit for fuel oil and gas and an illustration of a gas burner unit.

- (1) Removal of existing burners
- (2) Removal of oil pipe with an existing wind box mounted
- (3) Removal of oil spray steam pipe with an existing wind box mounted
- (4) Removal of existing spray fuel units
- (5) Installation of new gas burners
- (6) Electric wiring work
- (7) Gas piping work



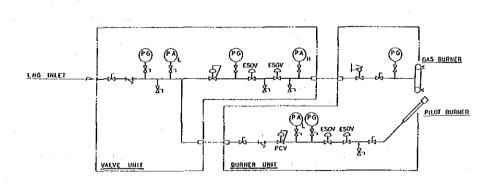
		۰.	
Z	SEAL POT	Ā	
7	CHECK VALVE	(TA)	TEMP SWITH
×1	GLOBE VALVE	PA	PRESSURE SWITH
旯	DIFF. PRESSURE	10	TEMP. GUAGE
2	EMARGENCY SHUT OFF VALVE	O	PRESSURE GUAGE
<u>द्व</u>	EMARGENCY VALVE	Ø	STEAM TRAP
Ì	AC VALVE FOR FUEL CONTROLL	0	STRAINER

Fig. 3-4 System Diagram of Fuel Oil Burners

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Table 3-5 Expenses for Fuel Conversion

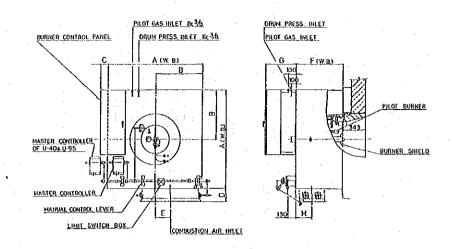
	SEQ	County code	Factory No.	Stack No.	Fuel	Sulfur content (%)	Specific gravity	Calory (Kcal/kg)	Fuel consumption (l/H)	Cost (×10 ¹ Bahts)
	1)	3	75	1	AHO	2.00	0.9408	10,430	2,400	2,280
	1)					3.00	0.9850	10,000	270	1,340
	2)	3	34	3	AHO		0.9408		248	1,340
	3)	2	23	4	AHO	2.00		10,000		1,950
ļ	4).	1	68	2	СНО	3.00	0.9561	10.296	1,440	
	5)	3	23	.5	AHO	2.00	0.9408	10,430	200	1.340
1	6)	3	24	1	СНО	3.50	0.9900	9,900	75	1,180
	7)	2	24	2	L.0	1.20	0.8660	10,950	25	1,180
	8)	3	96	1	AHO	1.28	0.9462	10,000	538	1,470
	9)	3	33.	. 2	L.O	1.20	0.8700	10,950	1	1,180
	10)	1	39	1	COAL	3.00	1.000	6,399	859 kg/H	1,470
	10	2	19	2	AHO	2.76	0.9358	10,495	111	1,180
	12)	3	97	ĩ	СНО	2.50	0.9529	10.340	40	1,180
	13)	í	68	i	СНО	3.00	0.9561	10.296	399	1,470
1	14)	li	66	i	AHO	2.80	0.9383	10,394	337	1,400
	15)	3	59	2	СНО	2.50	0,9529	10.340	398	1,470
	16)	3	l ní	2	СНО	2.50	0.9529	10,340	375	h
	10)	, ,		4 .	Cilo	3.50	0.9900	9,900	375	4,270
						3,50	0.9900	10,495	375	1
	171	1	56	2	AHO	1.28	0.9462	10,000	318	1,400
	17)		14	í	СНО	2.50	0.9529	10,340	984	6,230
	18)	3				2.50	0.9529	10,340	984	6,230
	19)	3	14	2	CHO				199	1.340
	20)	3.	109	2	СНО	3.50	0.9950	9,900		
	21)	3	90	1	CHO	2.66	0.9764	10,400	200	1,340
	22)	1	70	3	L.O	1.50	0.9200	10,950	266	1,340
	23)	1	35	- 2	AHO	2.92	0.9500	10,518	280	1,340
	24)	3	54	1	CHO	3.50	0.9900	9,900	400	1,470
	25)	1	- 35	L -	AHO	2.92	0.9500	10,518	280	1,340
	26)	3	16	4	СНО	3,50	0.9950	9,900	389	1,470
- 1	27)	. 3	102	1	AHO	2.76	0.9358	10,495	498	1,470
	28)	i i	68	3	CHO	3.00	0.9561	10.296	480	1,470
1	291	i i	66	2	AHO	2.80	0.9383	10,394	477	1,470
	30)	3	16	3 -	CHO	3.50	0.9950	9,900	311	1,400
			47	3	СНО	2.66	0.9764	10,400	435	1,470
	31)	3				2.00			382	1,400
	32)	1	2	1	CHO	2.50	0.9529	10,340	266	1,340
	33)	3	169	1	CHO	3.50	0.9950	9,900		
	34)	1	64	1	CHO	2.66	0.9764	10,400	143	1,340
1	35)	1	70	2	CHO	3.50	0.9900	9,900	663	1,600
	36)	3	5	2	AHO	2.00	0.9408	10,430	2,067	2,280
	37)	3	16	1	CHO	3.50	0.9950	9,900	233	1,340
	38)	3	16	2	CHO	3.50	0.9950	9,900	233	1.340
	39)	1	70	1	СНО	3.50	0.9900	9,900	529	1,470
	40)	3	54	2	СНО	3.50	0.9900	9,900	400	1.470
	41)	3	54	3	CHO	3.50	0.9900	9,900	400	1,470
	42)	ĩ	110	2	CHO	2.50	0.9529	10,340	119	1,340
- 1	43)	2	5	6	вно	2.50	0.9750	10,000	130	1,340
	44)	3	28	ĩ	AHO	3.00	0.9850	000,01	95	1,340
	451	ĩ	55	i	СНО	3.50	0.9900	10,336	908	1,790
	46)	ì	55	ż .	СНО	3.50	0.9900	10,336	908	1,790
Į	47)	3.	:14	3	ČНŎ	2.50	0.9529	10,340	492	1,470
1	48)	Î.	64	2	AHO	2.16	0.9609	10,461	42	1,180
	49)	3 .	95	$\tilde{2}$	CHO	2.50	0.9529	10,340	52	1,180
- 1				-						



Ŕ	Y-TYPE STRAINER	6	PRESSURE GUAGE
1 S S	AC VALVE FOR FUEL CONTROLL	PA	PRESSURE SWITH
ъб.	BALL VALVE		
£	EMARGENCY SHUT OFF VALVE		
A	PRESS. CONTROL VALVE		

Fig. 3-5 System Diagram of LNG Burners

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HARK	A	-8	C.	D.	ε	. F	G	н	OR. INLET	STEAM	ATOMIZING AIR INLET
U-40HE	715	457.5	200-	200	130	450	500	170	Rc 1/2	Rc 1/2	Rc V2
U-95KF	1220	610	200	200	200	762	500	253	Rc 1	Rc 1	Rc 1
U - 85 NF	1524	762	126	200	250	762	500	260	Rc 1	Rc11/4	Rc11/4
U-65Kf (1)	1630	915	70	200	100	920	500	260	8c1 4	Rc 11/4	Rc 1 1/4
J-65NF (2)	1830.	915	70	200	100	920	500	360	8c11/4	Rc 1 1/4	Rc 11/4
U- 60 NF	1980	990	70	500	0	1220	500	470	Rc11/2	Rc11/2	Rc 11/2

Fig. 3-6 Illustration of Gas Burner Unit

3.3 Flue Gas Desulfurization

The countermeasures for stationary emission sources include flue gas desulfurization to remove sulfur oxides from flue gas, in line with conversion to low sulfur fuels and fuel oil desulfurization. This method allows flue gas to contact an absorbent or adsorbent or to be oxidized with a catalyst, and recovers or removes a sulfur oxide in the form of sulfite, sulfate or sulfuric acid. The recovered materials include gypsum, ammonium sulfate, sodium sulfate, sodium sulfite, sulfuric acid, and sulfur.

3.3.1 Classification of Flue gas Desulfurization

There are many kinds and classifications of flue gas desulfurization. This method is roughly divided into absorption, absorption and catalytic oxidation, with the absorption method being further classified into wet and dry processes. By the absorption method, chemicals that react easily with sulfite gas are used as an absorbent to contact flue gas, leading to the separation of sulfite gas from flue gas to recovery in the form of liquid or solid compounds. The absorption method is further classified as follows:

(1) Wet process

The wet process includes a solution method in which the absorbent is dissolved in water and a slurry method in which the absorbent is suspended in water. The solution method is classified into such methods as caustic soda, sodium sulfite, ammonium, and dilute sulfuric acid, depending upon the types of absorbent. The slurry method is likewise classified into a lime method and a magnesium hydroxide method. The wet process is a method in which flue gas is washed with a solution or slurry to remove the sulfur oxide from flue gas in the form of sodium sulfite or sodium sulfate. This method has been put to practical use to treat flue gas from boilers and tail gas from such facilities as sulfuric acid plants. At present, the wet process is most popular among the methods of flue gas desulfurization. This process has advantages of a high rate of desulfurization and easy operation, and can be also applied for treatment of flue gas containing a high concentration of sulfite gas, whereas the use of water causes a decrease in the temperature of flue gas, leading to the poor diffusion of smoke. Consequently, some treatment has been added, for example, burning the waste gas.

(2) Dry process

Using various oxides including alkaline earth metals, alkali metals, and manganese as the absorbent, this method removes the sulfur oxide compounds of flue gas in the form of sodium sulfate through solid and gas phase reaction. The adsorption method allows about 100°C flue gas to pass through an activated carbon. In this method the adsorbed sulfite gas becomes sulfate anhydride through reaction with oxygen and then becomes sulfuric acid through reaction with vapor, thus being adsorbed. Activated carbon which has deadsorbed sulfuric acid is repeatedly used for desulfurization.

The catalytic oxidation is a process in which sulfite gas is catalytically oxidized with a catalyst of vanadium pentaoxide to obtain sulfate anhydride. This reaction is also used as a process of catalytic sulfate production. A method which applies this reaction to remove the sulfite gas from flue gas in the form of sulfate anhydride is called the catalytic oxidation process. The catalytic oxidation of sulfate gas is performed at 450 °C to 470 °C.

3.3.2 Wet Absorption Process

(1) Use of lime slurry as absorbent

 $CaCO_3$, $Ca(OH)_2$, carbide waste, etc. are smashed to about 200 meshes or less to be used as 5% to 15% slurry, with which flue gas is washed. Sulfite gas is converted to calcium sulfite. This is oxidized by air and recovered or removed in the form of gypsum. The rate of desulfurization varies depending upon the pH of the solution; the rate of desulfurization is high at a high pH, but accompanies concern about scaling.

(2) Use of magnesium hydroxide slurry as absorbent

Magnesium sulfite or magnesium sulfate is obtained by reaction with sulfite gas. With part of

the absorbent extracted from the circulation system, the absorbent is regenerated by thermal decomposition after being dried, and simultaneously, the resulting concentrated sulfite gas is used as a raw material for sulfuric acid or recovered as liquid SO_2 .

(3) Use of aqueous ammonium solution as absorbent

Since an aqueous ammonium solution has a high partial pressure of ammonium, undergoing loss accompanied by waste gas, the common practice is to be absorbed by sulfite gas to form an aqueous solution of sulfite ammonium. Thus, it absorbs sulfite gas and generates ammonium hydrogensulfite. With ammonium and water added to the absorbing solution which after leaving absorption tower, the said solution recirculates, but partly being fed to the recovery process. The ways of recovery include: (1) recovering ammonium sulfate and concentrated sulfite gas by adding sulfuric acid; (2) adding ammonium to obtain ammonium sulfate and then oxidizing with pressurized air to recover ammonium sulfate; (3) adding sulfuric acid and heating at 150° C, 5 kg/cm² to recover sulfur and ammonium sulfate; and (4) adding limestone or Ca(OH)₂ to recover gypsum, regenerating ammonium.

(4) Use of caustic soda or sodium sulfite as absorbent

There are the following two methods: sulfite gas is absorbed using caustic soda or sodium sulfite as the absorbing solution, and the resulting sodium hydrogensulfite is treated for recovery or removal as sodium sulfate, sodium sulfite, and gypsum; and the above sodium hydrogensulfite is treated to recover sulfite gas. For regeneration of the absorbing solution, there are several available methods such as thermal decomposition by steam or adding caustic soda.

(5) Using dilute sulfuric acid as absorbent

In this process, dilute sulfuric acid with the addition of an oxidation catalyst as an absorbing solution is used to absorb sulfite gas and thus obtain sulfuric acid. Absorbing sulfite gas at a packed tower, the absorbing solution is oxidized by air to sulfuric acid at an oxidation tower, then circulated in an absorption tower. Part of it is extracted and fed to a crystallizing vessel for reaction with limestone, followed by the recovery of gypsym.

3.3.3 Dry Absorption Process

(1) Addition of lime or dolomite in a furnace

Calcium oxide or magnesium oxide, which is produced by decomposition of limestone or dolomite at a high temperature, reacts with sulfite gas and oxygen to directly produce sulfate. While blowing the powder of limestone or dolomite, or $Ca(OH)_2$ into the combustion chamber of a boiler and transporting it with combustion gas, sulfite gas is fixed by the above mentioned reaction and is then collected with a dust collector. When the gas temperature at the blowing position is about 1050 °C, the best results can be obtained. The desulfurization rate is generally low, accounting for 20% to 40% in the case of addition in an amount equivalent to 1 to 2 times the theoretical value against sulfite gas. The adherence of the absorbent to the heating surface is a problem.

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(2) Use of alkali absorbent

Porous alumina retaining an alkali metal oxide, or sodium carbonate (light soda ash) is added to about 300°C combustion flue gas, followed by the fixation of sulfite gas as sodium sulfate. The absorbent collected by the dust collector is reduced with about 600°C hydrogen to regenerate the absorbent as well as recover hydrogen sulfide. There is another method in which a fused carbonate mixture (containing lithium carbonate, sodium carbonate, and potassium carbonate) is used as an absorbent.

(3) Use of manganese oxide as absorbent

Highly active $MnO_x \cdot nH_2O$ (x=1.5 to 1.8, n=0.3 to 1.0) is used as an absorbent. After the absorbent in the form of fine grain is added to waste gas of 135°C to 150°C, sulfite gas is absorbed while being transported by flashing, and is fixed as manganese sulfate. It is then separated from flue gas with a dust collector. Most of the collected absorbent is recycled, part of it is extracted for air oxidation under the presence of aqueous ammonium, thus resulting in the recovery of ammonium sulfate as well as the regeneration of the absorbent.

3.3.4 Adsorption Process

In the activated carbon process using activated carbon as an adsorbent, a fixed bed, moving bed and fluidized bed are used to attain the contact between flue gas and activated carbon. Activated carbon is regenerated and repeatedly used, and the regeneration methods include wash deadsorption, thermal deadsorption, and steam deadsorption. Sulfite gas, being adsorbed by activated carbon, is recovered as concentrated sulfite gas, sulfuric acid, or gypsum. There are several units of packed tower with activated carbon, which repeat adsorbing, washing, and drying by valve switching. After dust is removed, flue gas passes through a tower for the drying cycle at 130°C to 145°C, drying the washed activated carbon. This allows gas with a lowered temperature to be mixed with the original gas and then fed to the tower for the adsorption cycle at about 100°C for desulfurization. Dilute sulfuric acid is obtained from the tower for the washing cycle. This is concentrated to sulfuric acid, or limestone is added, to recover gyprum. There is another method in which activated carbon is washed intermittently and then fed to the gas cooling tower to simultaneously carry out the cooling of flue gas and the concentration of sulfur. Still another method is available in which with activated carbon as the moving bed, sulfite gas is adsorbed through the counterflow or crossflow of waste gas with it, followed by deadsorption with oxygen-free gas or superheated steam of about 300°C.

3.3.5 Catalytic Oxidation Method

After dust in flue gas is removed with the dust collector, the gas is passed through a catalyst layer at 450 °C to 470 °C for oxidation of 90% of sulfite gas to sulfate anhydride. It is then cooled with an economizer or air preheater to adsorb sulfate mist, which occurs in the meantime, with sulfuric acid.

3.3.6 Other Methods

There are other methods including that in which sulfite gas in flue gas is reacted with hydrogen sulfide and is removed as sulfur; and that in which sulfite gas in flue gas is oxidized for removal as sulfuric acid by using a nitrogen oxide as a medium for oxygen transfer as in the manufacture of sulfuric acid by lead chamber process.

3.3.7 Cost for Flue Gas Desulfurization

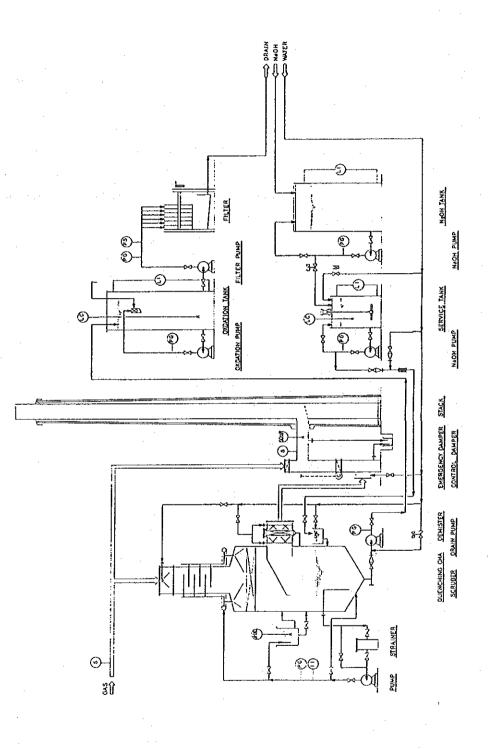
There are, as described above, various methods in flue gas desulfurization. The cost for such desulfurization has been examined by setting the cases and wet process using caustic soda is adopted finally, because of the very small volume of flue gas by plant as shown in Table 3-3 and the process is most common and its absorbent is relatively easy to obtain. Table 3-6 and Figure 3-7 show the cost of each facility and a basic flowchart of desulfurization. The operating cost includes power and caustic soda, but not including water and sludge treatment charges. In addition, the desulfurization rate was set at a value during standard minimum operation (approximately equal to 85%) due to difficult control. The construction cost includes the cost for one set excluding stacks, control dumpers (including ducts) and civil work.

						· · · · · · · · · · · · · · · · · · ·	1.1	
	1	1	1	Gas	Normal	Normal SO ₂	Running	Total
SEO	County	Factory	Stack	temper-	exhaust gas	emission	cust	cost
3EQ	code	No.	No.	ature	volume	volume		
				T (*K)	Q (m³/S)	q (Nnt³/h)	Bahts/H	(×10 ³ Bahts)
1)	3.	75	1	313	26.092	31.697	1,600	38,000
2)	3	34	3	350	2.935	5.610	320	11,500
3j	2	23	4	350	2.697	3.281	210	11.500
4)	L L	68	2.	462	6.712	28.970	1,420	16,700
5)	3	23	5	333	4.349	2.633	210	15,000
6)	3	- 24	E	462	0.350	1.812	120	7.500
7)	2	24	2 ·	437	0.157	0.186	30	4,200
8j		96	1	350	5.849	4.548	. 300	16,700
9)	3	33	2	437	0.007	0.971	60	1,700
10)	1	39	1	462	2.940	18.078	870	11,500
11)	23	19	2	523	0.519	2.019	120	7,500
12)		97.	1	318	0.125	0.652	60	4.200
13)	Ľ	68	1	462	1.860	8.047	400	9.500
- 14)	E E	66	1	453	1.570	6.206	330	9,500
15)	3	59	2	443	1.852	6.647	350	9,500
16)	.3	111	2 2	496	6.119	24.545	1,220	16,700
- 17)	1	56	[2]	448	1.482	2.703	170	9,000
18)	3	14		483	4.587	16.464	830	15,000
19)	3	14	2	483	4.587	16.464	830	15,000
20}	3	109	2 ·	462	0.926	4.858	260	7,700
21)	3	90.	1	-162	0.932	3,649	200	7,700
22)	1	. 70	3	437	1.639	2.567	170	9,500
23)	1	35	2	483	1.305	5.895	300	9.000
24)	3	- 54	{ I	448	1.864	9.730	480	9,500
25)	1	35		483	1.305	5.857	300	9,000
26)	3	16	4	473	1.813	9.512	310	9.500
27)	3	102		462	2.319	9.008	450	10,700
28)	- 1	68	3	462	2.237	9.657	490	10.700
29)	1	66	2.3	453	2.223	8.796	450	10.700
30)	3	16		473	1.449	7.608	380	9,500
3()	3	47	[3	498	2.025	7.922	420	10,700
32)	1	2	1	473	1.778	6.381	340	9.500
33)	3	109	1	462	1.237	6,478	320	9.000
34)	1	64		463	0.667	2.609	150	8.000
35)	1	70	2	573	5.406	16.113	810	16,700
36)	3	5	2	523	9.631	27.299	140	21.000
37)	3	- 16	1	473	1.086	5.692	280	9,000
38)	3	16	2	473	1.0%6	5.692	280	9,000
39)	1] 70		573	4.317	12.890	670	15.000
40)	-	54		473	1.864	9.730	480	10,700
41)	3	54	3	473	1.864	9.730	430	10,700
42)	3	110	2	462	0.556	1.994	1(0	7,500
43)	2	5	6	462	0.608	2.226	130	7,500
44).	3	28	1 1	462	0.445	1.979	110	7,000
45)		55	1	393	4.230	22.098	1,070	15,000
46)	1	55	23	393	4.230	22.098	1,070	15,000
47)		14	2	483	2.293	8.232	440	10,700
48)		64 95	2	462	0.196	0.622	50	5,400
-49)	1 3	1 95	1 4	333	1.14	0.886	80	9,000

	Table 3-6	Cost for	Flue Gas	Desulfurization	
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3.4 Reduction of Fuel Consumption through Energy Saving

3.4.1 Effects of Energy Saving

Up to this point, we have been discussing countermeasures under the assumption that some kind of methods will be implemented. In reality, however, not all of the subject factories will be able to make the capital investments which are necessary. Even if they are able to make the investments, we do not believe that they will willingly invest in something which does not lead to greater profits. Therefore, methods which do not require large investments and which will bring some advantages must be promoted. The only such method is the reduction of fuel consumption through implementing energy saving countermeasures. Since energy saving does not make visible effect in short term but require continuous efforts in long term to get its effect, it is likely disregarded as the method. It is, however, most reliable method in spite of small investment when we examine from middle to long term point of view.

Table 3-7 shows some examples of energy saving countermeasures taken in Japan and their effects. This table shows the degree to which energy base units (total of energy consumption, such as the electric power necessary to manufacture products or profits per unit volume) have decreased (improved) in different industries through energy saving countermeasures. The table shows the figures for 1987 based on an index of 100 for the year 1973. From this table, there have been savings ranging from 20 to 40 percent over a 14 year period. This means that the yearly reductions have been from 1.5 to 3.0 percent per year. If these figures are applied to the Samut Prakarn industrial district and a reduction in fuel consumption of 15 to 30 percent in a ten year period is assumed, then the K-value=13 goal will be achieved at most facilities. Table 3-8 shows, for reference purposes, an outline of the energy usage rationalization criteria which the management of plants use.

3.4.2 Costs Involved in Energy Saving Countermeasures

Although the figures are ambitious, in regard to energy saving percentage by industry, the figures in Table 3-7 for energy saving percentage in Japan have been applied in Table 3-9 to show a yearly percentage. In this table, the general criteria in Japan for the amount of investment for energy saving countermeasures have been applied, that is, investment amount is equivalent to the saving amount over a three year period resulting from the energy saving countermeasures.

As a result, the calculations show that the amount of energy saved between 1993 to 1999 if energy saving countermeasures are taken at the 49 stacks (=combustion facilities) would be 65,500 kiloliters. If this is evaluated on the basis of the projected price of fuel oil for 1999 (3960 bahts/kl), then approximately 260 million bahts, or about 1.6 times the investment (160 million bahts) can be saved.

In addition, these energy saving countermeasures will lead to a reduction of about 11 percent for all fuel oil consumed (584,000 kl) by the manufacturing sector in the Samut Prakarn district in 1999. This also means that SO_2 emissions can be reduced by 11 percent.

Detail on investment in energy saving countermeasures and its effects are described in section 6.4 of Chapter 6.

Industry	Energy (oil) base unit reduction status (FY1987/FY1973)	Outline of energy saving countermeasures	Representative energy saving facilities, etc
Steel	77.2 (26.2)	 Improvements in operation technology. Recovery of waste energy. Improvements in production processes. Improvements in energy usage efficiency. 	 Hot slab continuous casting machine. Low-pressure-loss-type blast furnace top pressure recovery power generating cquipment Coke dry type fire extinguishing equipment
Petrochemical (Ethylene division)	57.3 ^(Note) (76.0)	 Improvements in waste heat recovery. Rationalization of processes. Reduction of circulation flow ratio in the distillation system. 	 Waste heat recovery equipment for recovery of heat from waste gas from heating furnaces. Waste heat recovery equipment for recovery of heat from decomposed generated matter. High efficiency compressors
Cement	69.7 (V)	 NSP conversion Improvements at raw masterial mills and finishing mills. Utilization of waste heat. More efficient combustion control. 	 SP and NSP kilns Vertical mills Power generation using medium and low temperature waste heast.
Paper, pulp	59.6 (45.0)	 Introduction of continuous production processes. Recovery of waste heat. Greater efficiency in production processes. Increased use of old paper. 	 Spare immersion type continuous cooking devices High performance pulp washing devices High performance sizing press
Dying	63.7 (59.8)	 Introduction of thorough maintenance and control. Recovery and utilization of hot waste water and waste heat. Introduction of energy saving equipment for textile dycing, etc. Improvements in fabrication conditions. etc. 	 Spout-type dying machines Dye stuff economizer Counterflow cleaning machines
Sheet glass	73.0 (67.7)	 Thermal insulation using insulating materials. Improvements in the scaling of ovens. Improvements in heat storage efficiency. Installation of waste heat boilers. 	(1) Boilers which use waste heat.

Table 3-7 Status of Energy Saving Countermeasures in Energy Intensive Industries

(Note) The energy (petroleum) base units for the steel industry are figures from the fiscal years 1986 and 1973. The energy (petroleum) base units for the petrochemical industry (ethylene division) are figures from the fiscal years 1987 and 1976.

Table 3-8 Outlines of Energy Usage Rationalization Criteria Used by Managers Involved with Factories

	① Rationalization of the combustion of fuel	 Rutionalization of heating, cooling and thermal transfer 	 Prevention of thermal loss through radiation. conduction. etc. 	(a) Recovery and usige of waste heat.	(5) Rationalization of conversion of heat to power, etc.	Prevention of loss of cleatricity through resistance, etc.	 Rationalization of conver- sion of electricity to power, heat, etc.
Establishment of standards for improvement of control standards,	Control standards for air ratios	Standards for the tempera- tures of heated and cooled items, standards for the tem- peratures, pressures. flow rates, etc. of thermal media, and standards for the tem- perature and humidity of air conditioning.	Standards for insulation construction.	Standards for the recovery and utilization of waste heat	Standards for the adjust- ment of loads between multiple boilers and tur- bines, and standards for bines, and standards for pressure in exhaust and pressure in exhaust and back pressure turbines.	Control standards for the voltages, currents, power factors, load factors and demand factors of substations and distribution equipment.	Standards for voltages, currents, power factors and demand factors related to electric power application, electrical heating, illumina- tion equipment, etc.
implementation of instrumentation, records, etc.	Instrumentation and rec- ords, etc. for fuel supply quantities, exhaust gas temperatures, residual oxygen quantities in exhaust gases, etc.	Instrumentation and records, etc. for gaining an under- standing of thermal move- ment through temperatures, pressures, flow rates, etc., and instrumentation and rec- ords, etc. for the tempera- ture and humidity of air conditioning.	Implementation of thermal account analyses.	Instrumentation and recods. etc. for items related to understanding the status of waste heat, and investigation of effective methods for utilizing waste heat.	Instrumentation and records for the thermal efficiency of main boilers and turbines: Instrumentation and records for operation under minimum tolerated pressure.	Instrumentation and records for the values above.	Instrumentation and records for the values above. (Including the intensity of illumination.)
Implementation of multicenance and inspection.	Maintenance and inspection of combustion facilities.	Prevention of decreases in thermal conductivity performance, water quality control for boiler water, and maintenance and inspection of air conditioning facilities.	Prevention of leaking from damage in heat transfer media, mainte- nance of insulation sec- tions, and maintenance and inspection of steam traps.	Removal of grime from the thermal transfer surfaces of waste heat recovery equipment. prevention of leaking of heat transfer media from equipment, etc.	Maintenance and inspec- tion of boilers and tur- bines, maintenance and inspection of turbine blades, etc. during opera- tion under minimum tolerance pressure.	Maintenance and inspection of substations and power distribution facilities.	Reduction of mechanical loss such as friction, prevention of fluid leaks in machines which handle fluids, and maintenance and inspection for other thermoelectric, electolysis, and illumination facilities.
Improvement measures and equipment introduced for rationalization.	Adjustment of combustion loads. selection of appropriate burners. improvements in ventilation devices. installation of combustion control devices. and installation of heat accumulators.	Reviews of heat usage conditions and supply conditions, improvements in heat patterns, adjustment of loads, improvements in direct heating, multiple stage use of heat, introduction of equip- nent which have high thermal efficiency, introduction of continuous and combined processes, and the shorten- ing and removal of processes.	Improvements in insulation, reducing the size of openings, installation of covering facilities for open type equipment, rationalization of piping routes, etc.	Preventing decreases in temperatures of waste heat during transfer processes, improvements in the heat transfer uspects of waste heat eccovery devices, installation of recovery and utilization equipment to meet the uses of waste heat.	Modifications to turbines to reduce the minimum tolerance pressure. Utilization of usable surplus steam for power generation and sources of energy for work.	Improvements in power fac- tors, such as the operation of transformers at appropriate loads, using transformers with the appropriate capaci- tics, levelling of loads, and appropriate allocation of appropriate allocation of substation equipment, and improvements in three phase unbalance.	Preventing motors from running free, appropriate allocation of loads, and implementation of speed controls, etc. Installation of motors with the appropriate capacities, etc. Other improvements in equipment and the introduc- tion of other equipment.