

## **APPENDIX 9**

### **AVAILABLE ADDITIONAL SEWAGE**



## APPENDIX 9 AVAILABLE ADDITIONAL SEWAGE

### 1. Collectors Vitarte and No.21

Additional sewage through a new interceptor mentioned in Subsection 5-3-2 is obtained from the Collectors Vitarte and No.21 which is located upstream of Collector Surco (refer to FIGURE A9-1). Available sewage quantity is estimated as follows:

#### Domestic sewage

District	COVERED POPULATION		
	D/S.H	D/S.L	ID
ATE (80%)	37,760	57,150	7,140
EL AGUSTINO (20%)	3,630	21,510	2,790
TOTAL	41,390	78,660	9,930
UNIT Q(lpcd)	210	180	110
Q'ty (m <sup>3</sup> /sec)	0.101	0.164	0.013

Total Domestic Sewage Quantity : 0.278 m<sup>3</sup>/sec

#### Industrial Wastewater

30 % of Collector Surco  $0.264 \times 0.3 = 0.079 \text{ m}^3/\text{sec}$

#### Other Wastewater

Same ratio as total of domestic and industrial.  
 Q'ty of Vitarte & 21 (D+I) / Q'ty of Surco (D+I)  
 $= (0.278 + 0.079) / (1.932 + 0.264)$   
 $= 0.163$   
 then,  $0.172 \times 0.163 = 0.0283/\text{sec}$

therefore, Total Available Sewage Quantity is:

$$0.278 + 0.079 + 0.028 = 0.385 \text{ m}^3/\text{sec}$$

### 2. Emisor General Villa El Salvador

The sewage flow from Villa El Salvador is estimated as follows:

D/S.H	8,380 x 210 lpcd =	0.020 m <sup>3</sup> /sec
D/S.L	335,200 x 180 lpcd =	0.698 m <sup>3</sup> /sec
ID	75,420 x 110 lpcd =	0.096 m <sup>3</sup> /sec
TOTAL		0.814 m <sup>3</sup> /sec
		$0.814 \times 0.5 = 0.407 \text{ m}^3/\text{sec}$

Therefore, around 0.4 m<sup>3</sup>/sec is estimated to be available for the Phase I project.

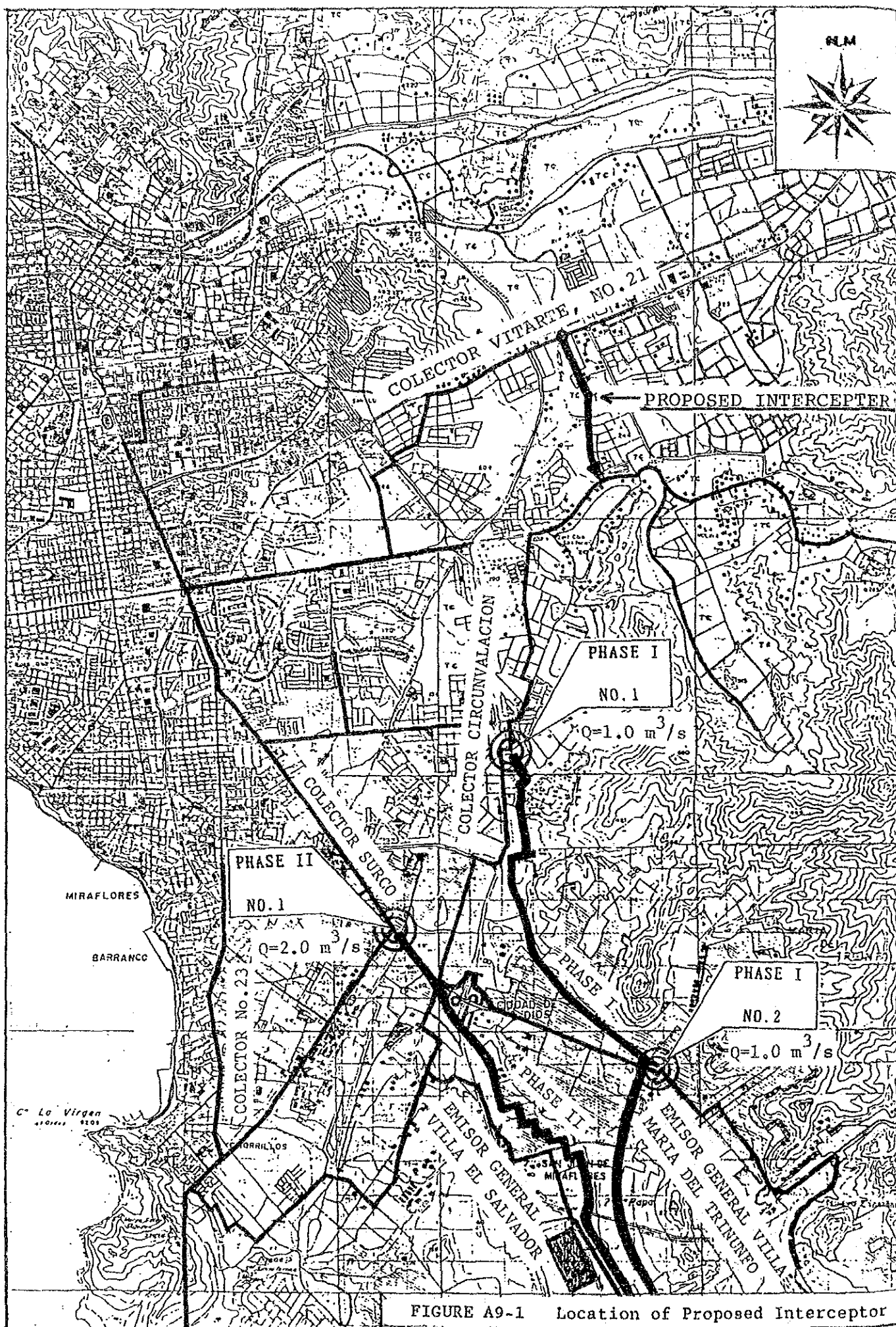


FIGURE A9-1 Location of Proposed Interceptor

## **APPENDIX 10**

### **WATER QUALITY STANDARDS AND GUIDELINES**



## APPENDIX 10 WATER QUALITY STANDARDS AND GUIDELINES

### A10.1 General

Water pollution control standards in Peru are set according to the classification of water bodies by their uses. The control of the quality of industrial wastewater discharged into sewers is also included in these standards.

### A10.2 Environmental Water Quality Standards

The Ley General de Aguas (General Law of Water, Decreto Ley No. 17752) classified the various water bodies by their general uses. The law was amended on February 11, 1983 through Decreto Supremo No. 007-83-SA which contains the following provisions.

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#### Article 81.

The effects of application of the present regulation, the quality of Peru's water bodies in general, be they inland or marine are classified according to their uses in the following manner:

- I. Water for domestic supply, simply disinfected
- II. Water for domestic supply, treated equivalent to combined processes of mixture and coagulation, sedimentation, filtration, and chlorination, approved by the Ministry of Health.
- III. Water for irrigation of vegetables to be eaten raw and for watering animals
- IV. Water for recreational area of primary contact (Baths and the like).
- V. Water for fishing zones for bivalves.
- VI. Water for zones to preserve aquatic fauna and recreational or commercial fishing.

I. BACTERIOLOGICAL LIMITS

(Maximum value of 80% of 5 or more monthly samples)

Values in MPN/100ml.

	USES					
	I	II	III	IV	V	VI
Total						
Coliforms	8.8	20,000	5,000	5,000	1,000	20,000
Fecal						
Coliforms	0	4,000	1,000	1,000	200	4,000

II. LIMITS OF BIOCHEMICAL OXYGEN DEMAND (BOD at 5 days, 20°C) AND OF DISSOLVED OXYGEN (DO)

Values in mg/l.

	USES					
	I	II	III	IV	V	VI
BOD	5	5	15	10	10	10
DO	3	3	3	3	5	4



### III. LIMITS OF THE PHYSICAL-CHEMICAL PARAMETERS WHICH INCLUDE POTENTIALLY DANGEROUS SUBSTANCES

Values in mg/l.

Parameter	USES					
	I	II	III	IV	V	VI
Aluminum	-	-	-	1(b)	1(b)	-
Arsenic	0.1	0.1	0.2	1	0.01	0.05
Barium	0.1(b)	0.1(b)	-	0.5	0.5(b)	-
Cadmium	0.01	0.01	0.05	-	0.0002	0.004
Cyanide (CN)	0.2	0.2	(c)	-	0.005	0.005
Cobalt	-	-	0.20(d)	0.2	0.2(b)	-
Copper	1	1	0.5	3	0.01	LC50x0.1
Color (unit)(b)	0	10	20	30	30	-
	5	5(d)				
Hexav. Chromium	0.05	0.050	1	5	0.050	0.050
Ethylene Esters	0.0003	0.0003	0.0003	-	0.0003	0.0003
Phenols	0.0005	0.001	(c)	-	0.001	0.1
Iron	0.03(b)	0.03(b)	0.001(b)	-	-	-
Fluoride	-	1.5(b)	1.5(b)	2.0(b)	-	-
Lithium	-	-	5(d)	5.0	5.0(b)	-
Magnesium	-	-	150(b)	-	-	-
	-	-	-(d)	-	-	-
Manganese	0.010(b)	0.010(b)	0.050	-	-	-
	-	-	-(d)	-	-	-
Mercury	0.002	0.002	0.01	-	0.0001	0.0002
Nitrates	0.01(a)	0.01(a)	0.1(a)	-	-	-
	-	-	0.01(d)	-	-	-
Nickel	0.002	0.002	(c)	0.5	0.002	LC50x0.02
pH (b)	5-9	5-9	5-9	5-9	5-9	5-9
	6-9(d)	6-9(d)	6-9(d)	6-8.5(d)	6-8.5(d)	-
Silver	0.05(b)	0.05(b)	0.05(b)	-	-	-
	-	-(d)	-	-	-	-
Lead	0.05	0.05	0.1	-	0.01	0.03
P.C.B.	0.001	0.001	(c)	-	0.002	0.002
Selenium	0.01	0.01	0.05	0.05	0.005	0.01
					0.05(d)	
Floating Solids	0.00(b)	0.00(b)	0.00(b)	invisible	moderate	-
Sulfates	-	-	400(b)	-	-	-
			-(d)			
Sulfurs	0.001	0.002	(c)	-	0.002	0.002
Zinc	5	5	25	-	0.02	LC50x0.02

#### OBSERVATIONS:

- There seems to be an error in the unit applied in the amendment to the law. Value should be multiplied by 1000.
- Information obtained from the Direccion Tecnica de Salud. Ambiental (Technical Department of Environmental Health) of the Ministry of Health.
- If presence of paramera is suspected, apply the values in column V.
- If the dumping is into sea water. The values come from (b).

Pesticides - In each use, the limit will be the water quality criteria established by the Environmental Protection Agency of the United States of America.

#### IV. LIMITS OF POTENTIALLY HARMFUL SUBSTANCES OR PARAMETERS

Parameter	USES		
	I and II	III	IV
- Material extractable in Hexane	1.5	0.5	0.2
- Active substances of blue Methylene	0.0	1.0	0.5
- Extraction of active Carbon column by alcohol	1.5	5.0	5.0
- Extraction of active Carbon column by Chloroform	0.3	1.0	1.0

#### A10.3 Effluent Standard

On November 29, 1960 the Industrial Discharge Regulation was approved through D.S.28/60 which set the permissible limits for domestic sewage discharged to a public sewer system and basically states:

All industrial wastewater which enters the public sewer network must comply without exception with the following standards:

- a) Temperature must not exceed 35°C.
- b) Vapors must be condensed to enter the drainage.
- c) Liquid grease that enter the sewer must have a concentration less than 0.1 g/l. in weight.
- d) Flammable substances that enter the drain must have an ignition point higher than 90°C and a concentration less than 1 g/l.
- e) The pH must be between 5 and 8.5. Industries that evacuate mineral acids or strongly alkaline substances must have tanks with sufficient capacity where they are neutralized.
- f) The BOD (Biological Oxygen Demand) may not exceed 1,000 ppm.
- g) Sedimentable solids must have a concentration higher than 8.5 ml/l/hour.



## **APPENDIX 11**

### **COMPARISON AND EVALUATION OF THE PROPOSED SITE**



## APPENDIX 11      COMPARISON AND EVALUATION OF THE PROPOSED SITE

The following 6 sites were judged as possible location of treatment plant for this Project, based on a field survey and in consideration of the various plans for land use and the Project's alternative sewer pipe routes.

- a)            Existing upper battery ponds in the San Juan Stabilization Pond (falls under the jurisdiction of the Ministerio de Vivienda y Construcción, Ecology Department.)
- b)            Southern Zone of San Juan Stabilization Pond (falls under the jurisdiction of the Ministerio de Vivienda y Construcción, Ecology Department)
- c)            Villa El Salvador - Parque Zonal No. 26 (falls under the jurisdiction of the Ministerio de Vivienda y Construcción, Ecology Department)
- d)            Villa Rica (belongs to an agricultural production cooperative)
- e & f)        Pampas de San Bartolo (falls under the jurisdiction of the Ministerio de Vivienda y Construcción)
- g)            Cello de Chillon at the south of the outfall of the Colector Surco (belongs to SEDAPAL)

Topographical plans of these prospective treatment plant sites are shown in FIGURES A11-1 through A11-5. TABLES A11-1 and A11-2 gives the descriptions, possibilities for adoption, and relative suitability of each of the sites.

As one of the purposes of this Project is to utilize sewage for irrigation of cultivated fields in the future, proposal (g) was not taken into account in the study.

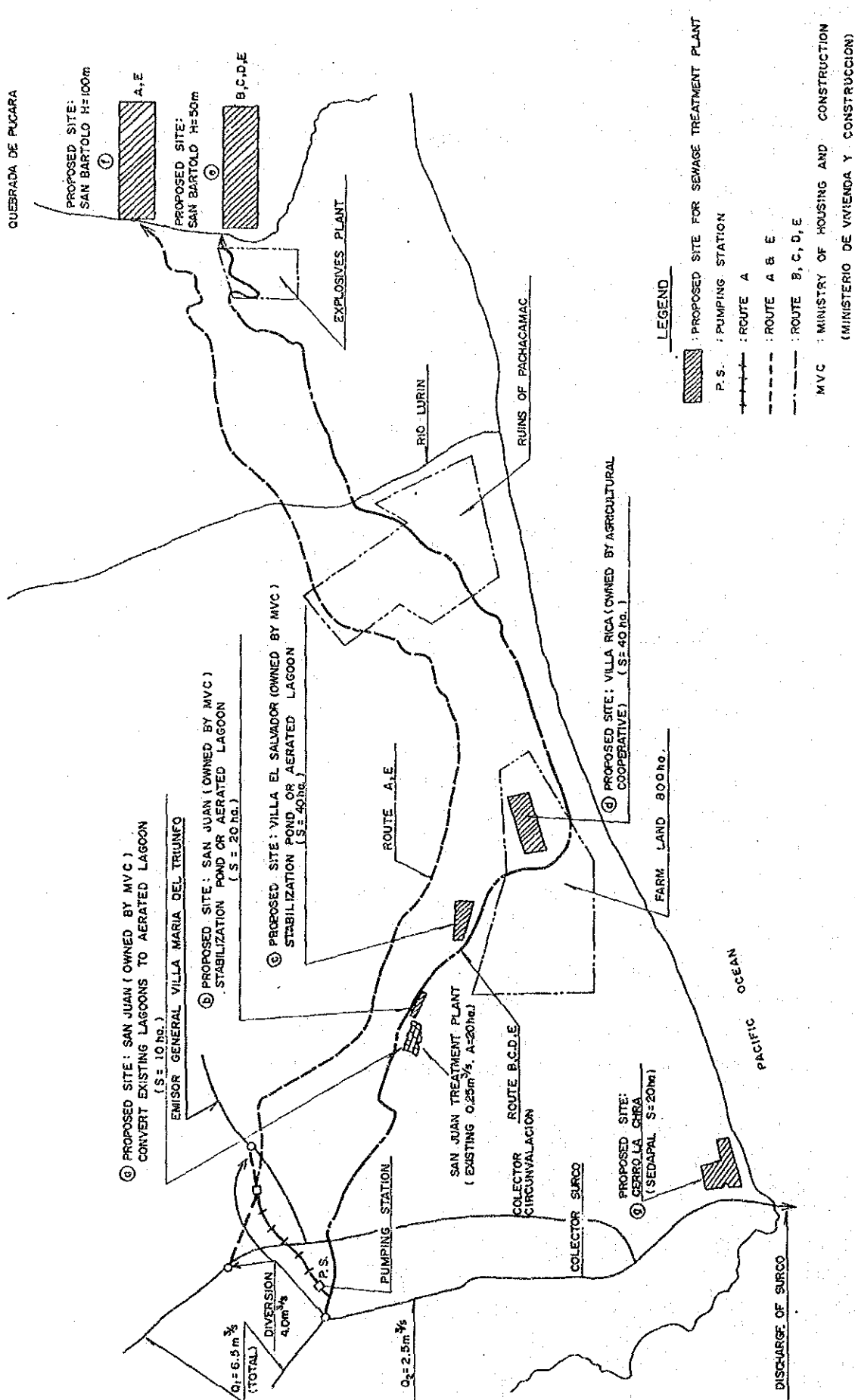


FIGURE A11-1 LOCATION OF PROPOSED SITE FOR SEWAGE TREATMENT PLANT.





FIGURE ALL-2: PROPOSED AREA (a) AND (b) FOR SEWAGE TREATMENT PLANT, SAN JUAN STABILIZATION POND.

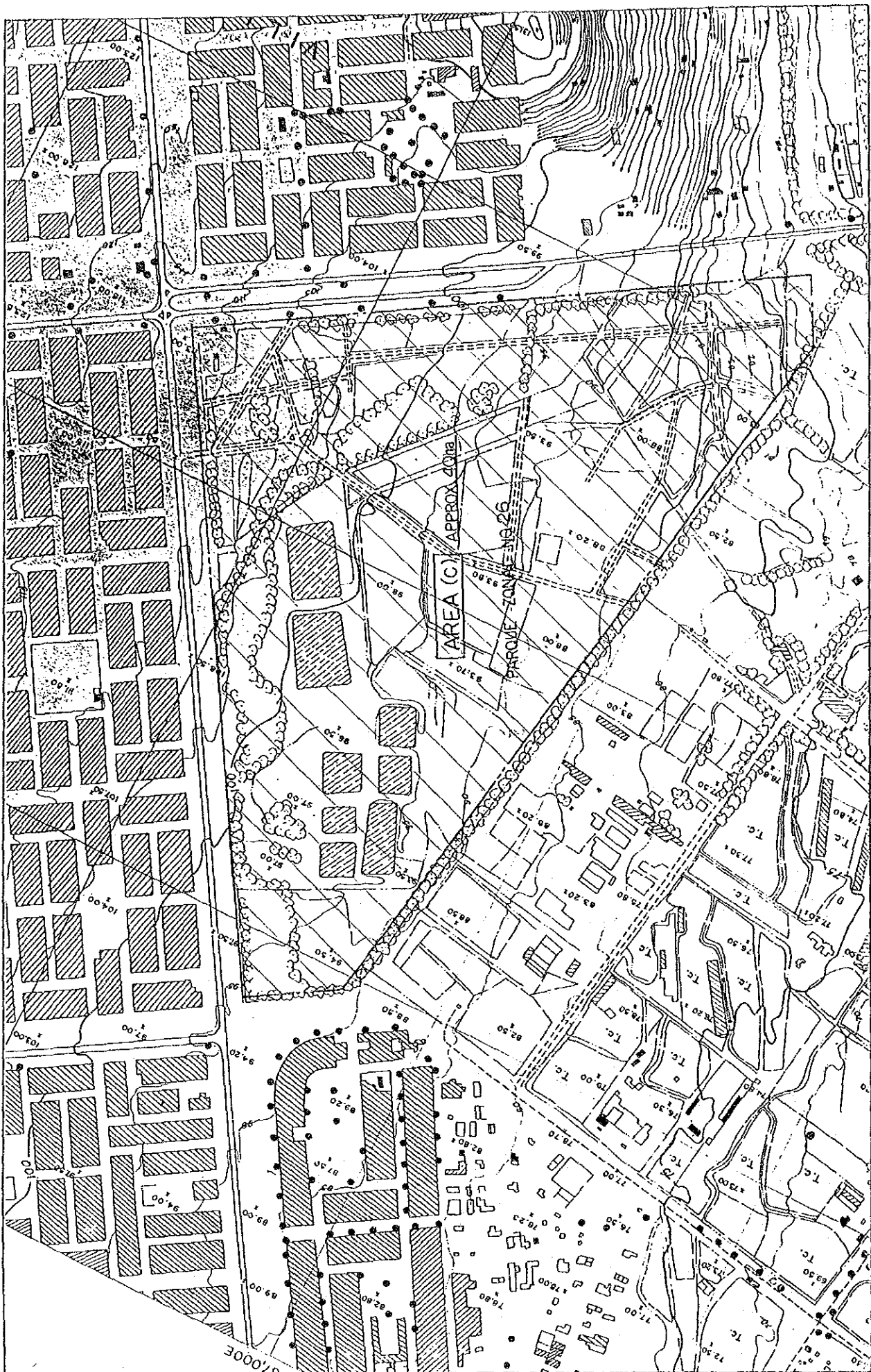


FIGURE A11-3: PROPOSED AREA (C) FOR SEWAGE TREATMENT PLANT, PARQUE ZONA NO 26, VILLA EL SALVADOR.

SCALE = 1:5000



SCALE = 1:5000

FIGURE A11-4 : PROPOSED AREA (d) FOR SEWAGE TREATMENT PLANT, VILLA RICA, VILLA EL SALVADOR.

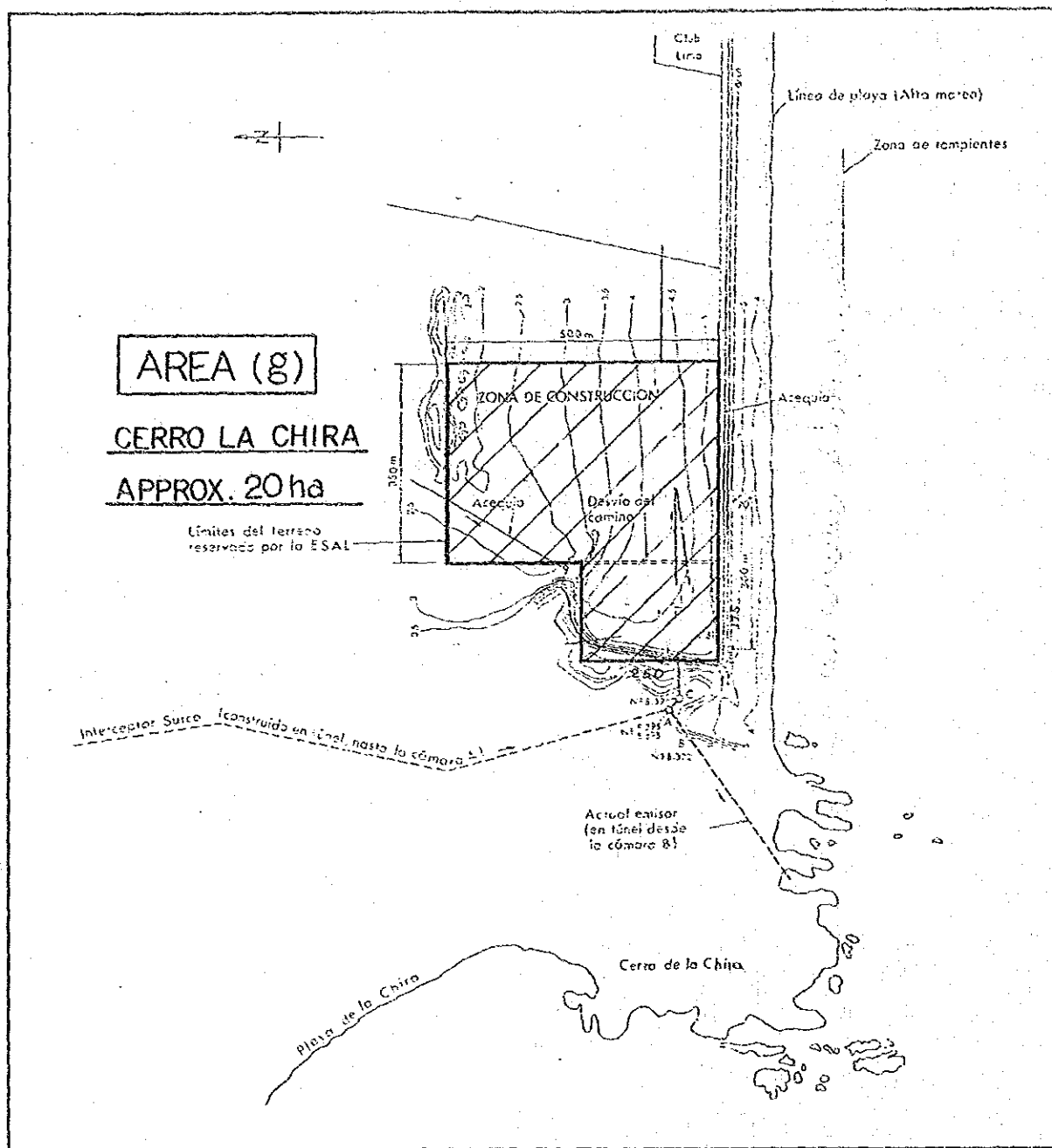
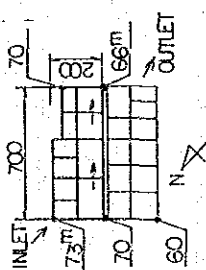
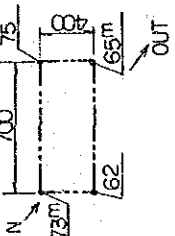
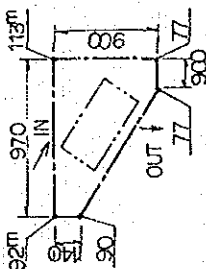
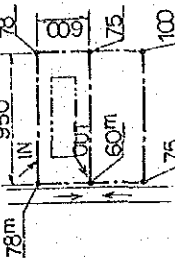


FIGURE A11-5: PROPOSED AREA (g) FOR SEWAGE TREATMENT PLANT, CERRO LA CHIRA.

TABLE A11-1 Outline of the Proposed Sites

ITEM	PROPOSED SITE	(a) EXISTING SAN JUAN STP	(b) SAN JUAN	(c) PARQUE ZONAL NO. 26	(d) VILLA RICA	(e & f) SAN BARTOLO
1	Proposed site for construction (area, altitude, inlet and outlet direction)					Specific plant site is not decided, however, it is possible to construct anywhere.
2	Outline of the site	In order to increase the capacity, re-excavate to provide 1.5 m to 3.0m of water depth and equip aerator in the existing up per battery (10ha).	Construct in the southern wooded area of the San Juan STP. Some trees need to be moved.	Construct in Parque, similar to (b), removal of trees and supplying treated water to the concerned farmers is required.	Construct in the agricultural co-operative's area. Facility must be constructed at least 100m away from house on the eastern area of site as a measure against bad odor.	8-plants (stabilization pond, approx. 55ha and 0.5 m³/s /plant) be constructed in the San Bartolo irrigation area.
Capacity	In case of stabilization pond	Effective water surface area	17.3 ha	17.0 ha	17.3 ha	
		Possible capacity $\frac{1}{1}$	0.19 m³/s	0.19 m³/s	0.19 m³/s	
	In case of aerated lagoon	Effective water surface area	14.6 ha	11.2 ha	—	
		Possible capacity $\frac{1}{1}$	1.0 m³/s	0.83 m³/s	—	

1/: Possible capacity of each proposed site is shown in TABLES A13-3 and A13-4

TABLE A11-2 Comparison and Evaluation of the Proposed Site

PROPOSED SITE SELECTION FACTOR	(a) EXISTING SAN JUAN STP	(b) SAN JUAN	(c) PARQUE ZONAL NO. 26	(d) VILLA RICA	(e & f) SAN BARTOLO
1 Facilities of collecting sewage from adjacent drainage area	A It is possible to connect using siphon on the way from intake points to San Bartolo.	B Same as (a).	C Less quantity near area, it is necessary to convey it from far Colector Surco.	C Due to high altitude, it is required to take from Colector Surco at high elevation.	D It is possible to convey to the high elevation level, but siphon is much long.
2 Proximity to drainage area	A Very good. Distance is minimal (5km).	B Located next to (a). It is the second nearest.	C Located at high land. A long line is necessary.	D Must take sewage from far distance.	D Very far (30km).
3 Benefits to the discharge area	A In the vicinity there are agricultural area, where raw sewage is being utilized due to lack of water at present.	A Most adequate. Same as (a).	A Located at high land. Wide agricultural area in lower lands.	C Very far from the planned cultivated fields. No benefit.	A The plant is located within the planned cultivated fields.
4 Facility of discharge during low demand season	C There is public bathing beach nearby. Requirement of authorization from the Ministry of Health.	C Same as (a).	C Same as (a).	B Same as (a).	B Same as (a).
5 Availability of sufficient land and facility of right-of-way and facility of right-of-way	D This plant is a center for land recovery studies. Not authorized. (Ministerio de Vivienda)	B Feasible if trees are moved. (Ministerio de Vivienda)	B Require moving at existing trees, ponds and school (Ministerio de Vivienda)	D Should acquire the land from the agricultural co-operative. Costly.	B Desert. No problem with the land.
6 Acceptability to neighboring houses/establishments	B Adequate mechanization allows forced aeration. Bad odors are reduced.	B There are houses at the west. It can be feasible if trees are planted to that area.	B The system must emit no odor. Moving trees and school is required.	C In the vicinity, ponds are abandoned due to bad odors.	B The neighbors are ranches. There is no problem.
7 Favorability of hydrogeological conditions (soil permeability and groundwater)	A There is a plenty of geological information.	B Adequate for construction.	B There are 4 stabilization ponds at present.	B Impermeable cultivated fields. Feasible.	C Sand dune. The soil condition is similar to San Juan in surface layer. But in deeper layer, high permeability.

key A : Recommendable B : Adequate C : Slightly adequate D : Not recommendable

TABLE A11-2 : Comparison and Evaluation of the Proposed Site (Cont'd)

PROPOSED SITE		(a)	(b)	(c)	(d)	(e & f)
SELECTION FACTOR	EXISTING SAN JUAN STP	SAN JUAN	PARQUE ZONAL NO.26	VILLA RICA	SAN BARTOLO	
8 Susceptibility to floods, high tide or landslides.	B Located on level ground, far from the sea. No rain. Not affected.	B Same as (a).	B Same as (a).	C There are dunes in back. Sand accumulation is a possible problem.	C Precautions against the sand accumulation are required.	
9 Adequacy for construction of the pond.	A The ground is slightly inclined in the direction of sewage flow. Construction is economical.	C Construction is more costly as the ground slopes in the opposite direction of the sewage flow.	C The ground is sloped in the opposite direction and very undulating. Cannot be utilized in an optimum manner.	C Located in a valley. As the outlet piping comes from at the lower end, it is necessary to go around the road at elevation 75m.	B The land is ample. Adequate area can be selected.	
Remarks	In this site, stabilization ponds are under construction by the Ministry of Agriculture based on the sewage reuse program. At present 4 ponds are in operation in the site. If this site is used for the Project, adjustment with that program shall be done.					

key A : Recommendable B : Adequate C : Slightly adequate D : Not recommendable

TABLE A6-3 Possible Treatment Capacity in Proposed Area (b), San Juan Experimental Area

Proposed Area	Case- I : Waste Stabilization Pond	Case- II : Aerated Lagoon
(b) San Juan	<p>-Primary Facultative Pond</p> <p>Dimension of Pond:  W 100 m x L 48 m x D 1.5 m x 22 basins  Total Water Surface Area:  = 100 x 48 x 22 = 105,600 m<sup>2</sup>  Possible Treatment Capacity:  Q1 = 105,600/565.445 x 1.0 m<sup>3</sup>/s = 0.19 m<sup>3</sup>/s</p>	<p>-Complete Mixing Aerated Lagoon</p> <p>Dimension:  W 105 m x L 46 m x D 3.0 m x 12 basins  Total Water Surface Area:  = 105 x 46 x 12 = 57,960 m<sup>2</sup> &gt; 57,600 m<sup>2</sup> (=1.0 m<sup>3</sup>/s)  Total Volume:  = 57,960 x 3.0 = 173,880 m<sup>3</sup> &gt; 172,800 m<sup>3</sup></p>
	<p>-Secondary Facultative Pond</p> <p>Dimension of Pond:  W 100 m x L 48 m x D 1.5 m x 14 basins  Total Water Surface Area:  = 100 x 48 x 14 = 67,200 m<sup>2</sup>  Possible Treatment Capacity:  Q2 = 67,200/324.000 x 1.0 m<sup>3</sup>/s = 0.21 m<sup>3</sup>/s</p>	<p>-Partial Mixing Aerated Lagoon</p> <p>Dimension:  W 105 m x L 31 m x D 3.0 m x 3 cells x 6 series  Total Water Surface Area:  = 105 m x 31 m x 3 x 6 = 58,590 &gt; 19,296 x 3 = 57,880 m<sup>2</sup>  Total Volume:  = 58,590 x 3.0 = 176,880 m<sup>3</sup> &gt; 57,888 x 3 = 173,664 m<sup>3</sup></p>
	<p>Q1 &lt; Q2, therefore, the system is able to treat <u>0.19 m<sup>3</sup>/s</u> of flow.</p>	<p>-Sedimentation Tank</p> <p>Dimension:  W 105 m x L 46 m x D 3.0 m x 6 basins  Total Volume:  = 105 x 46 x 3.0 x 6 = 86,940 m<sup>3</sup> &gt; 86,400 m<sup>3</sup></p> <p>Therefore, the system is able to treat <u>1.0 m<sup>3</sup>/s</u> of flow.</p>



TABLE A6-4 Possible Treatment Capacity in Proposed Area (c), Parque Zonal No. 26, Villa El Salvador

Proposed Area	Case- I : Waste Stabilization Pond	Case- II : Aerated Lagoon
(c) Parque Zonal No. 26	<p>-Primary Facultative Pond</p> <p>Dimension of Pond:  W 109 m x L 54 m x D 1.5 m x 18 basins  Total Water Surface Area:  = 109 x 54 x 18 = 105,948 m<sup>2</sup>  Possible Sewage Treatment Capacity:  Q1 = 105,948/565,445 x 1.0 m<sup>3</sup>/s = 0.19 m<sup>3</sup>/s</p> <p>-Secondary Facultative Pond</p> <p>Dimension:  W 109 m x L 54 m x D 1.5 m x 12 basins  Total Water Surface Area:  = 109 x 54 x 12 = 70,632 m<sup>2</sup>  Possible Sewage Treatment Capacity:  Q2 = 70,632/324,000 x 1.0 m<sup>3</sup>/s = 0.22 m<sup>3</sup>/s</p> <p>Q1 &lt; Q2, therefore, the system is able to treat <u>0.19 m<sup>3</sup>/s</u> of flow.</p>	<p>-Complete Mixing Aerated Lagoon</p> <p>Dimension:  W 105 m x L 46 m x D 3.0 m x 10 basins  Total Water Surface Area:  = 105 x 46 x 10 = 48,300 m<sup>2</sup>  Total Volume:  = 48,300 m<sup>2</sup> x 3.0 m = 144,900 m<sup>3</sup>  Possible Sewage Treatment Capacity:  Q1 = 144,900/172,800 x 1.0 m<sup>3</sup>/s = 0.84 m<sup>3</sup>/s</p> <p>-Facultative Aerated Lagoon</p> <p>Dimension:  W 71 m x L 46 m x D 3.0 m x 3 cells x 5 series  Total Water Surface Area:  = 71 m x 46 m x 3.0 x 5 = 48,990 m<sup>2</sup>  Total Volume:  = 48,990 x 3.0 = 146,970 m<sup>3</sup>  Possible Sewage Treatment Capacity:  Q2 = 146,970/173,664 x 1.0 m<sup>3</sup>/s = 0.84 m<sup>3</sup>/s</p> <p>-Sedimentation Pond</p> <p>Dimension:  W 105 m x L 46 m x D 3.0 m x 5 basins  Total Volume:  = 105 x 46 x 3.0 x 5 = 72,450 m<sup>3</sup>  Possible Sewage Treatment Capacity:  Q3 = 72,450/86,400 x 1.0 m<sup>3</sup>/s = 0.84 m<sup>3</sup>/s</p> <p>Therefore, possible capacity is <u>0.84 m<sup>3</sup>/s</u>.</p>



## **APPENDIX 12**

### **COMPARISON BETWEEN OPEN CHANNEL AND INVERTED SIPHON**



## APPENDIX 12    COMPARISON BETWEEN OPEN CHANNEL AND INVERTED SIPHON

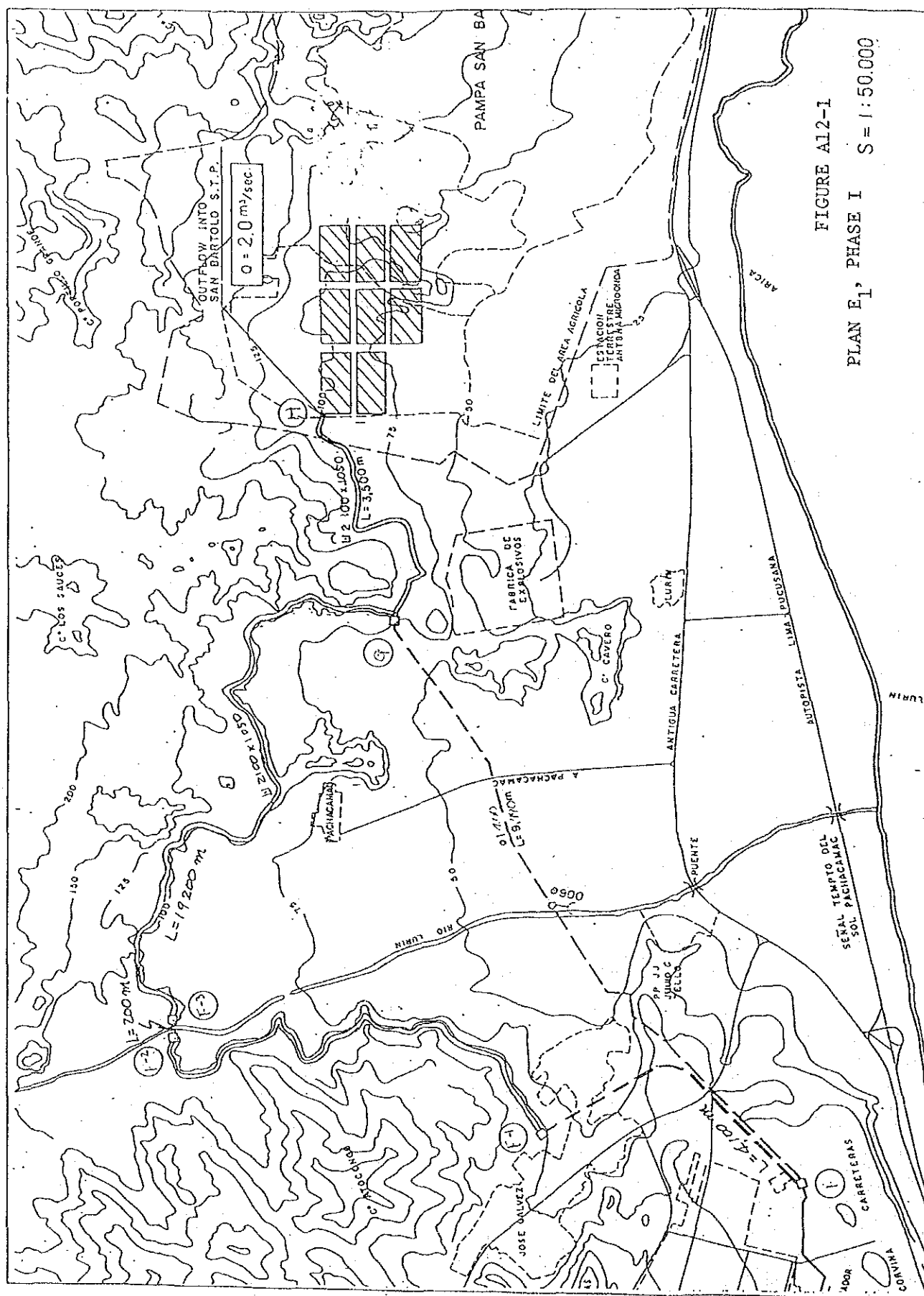
The transmission line that will cross the Lurin river can be planned to pass through the following two routes:

- 1)    A straight line with an inverted siphon structure.
- 2)    A circuitous line along the mountain foot following the Elevation 100 m contour with an open channel structure.

Since all of the alternative plans involve transmission lines traversing the Lurin river, a comparison of both routes was executed on the two alternative lines of plan E1 (refer to FIGURES A12-1 and A12-2).

The examination was conducted on the aspects of workability, influence on environment, operation and maintenance, and construction cost (refer to TABLE A12-1).

As a result of comparison, routes with inverted siphon structure were judged as superior.



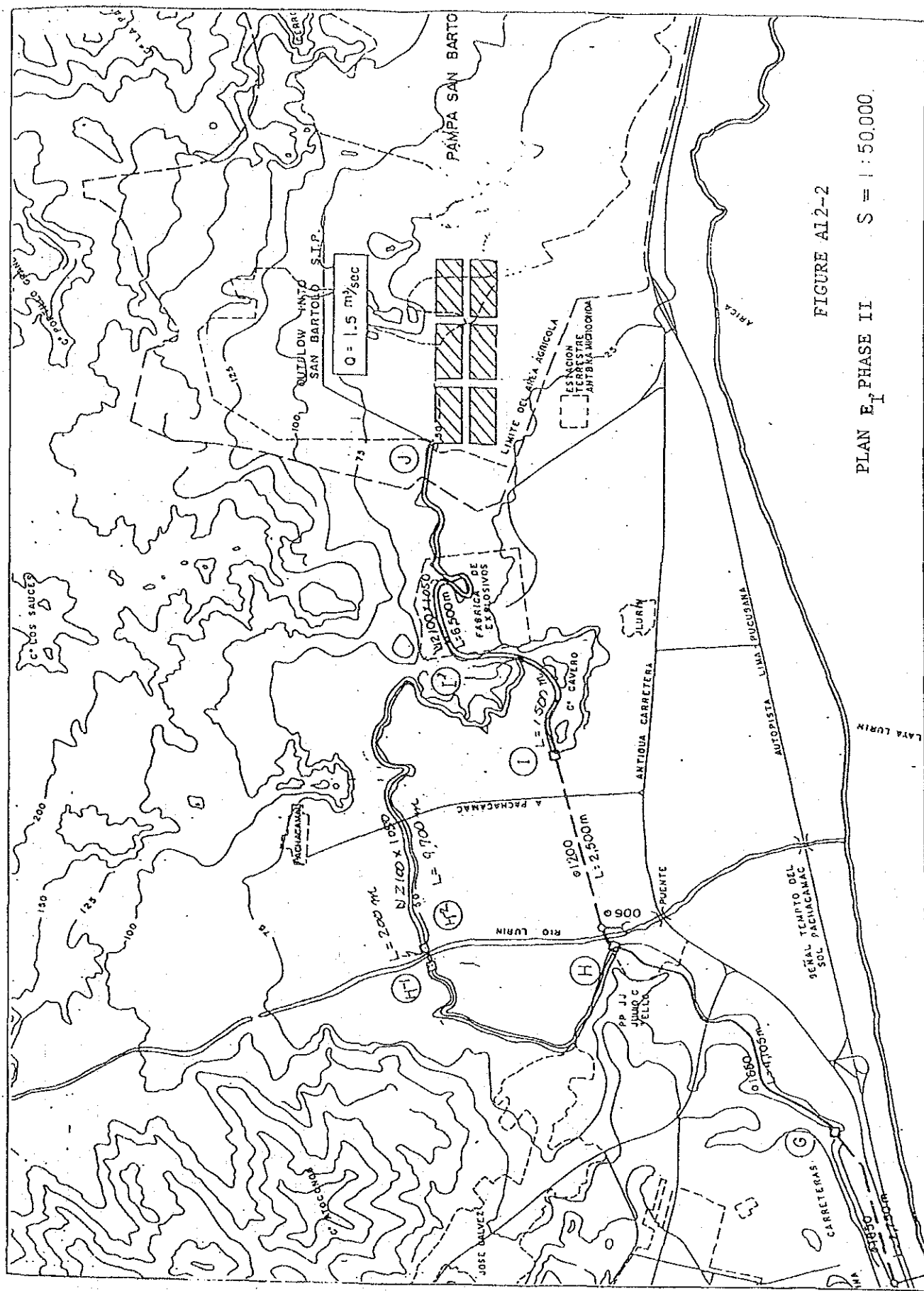


TABLE A12-1 COMPARISON BETWEEN OPEN CHANNEL AND INVERTED SIPHON

Conduit	Length	Workability	Influence on Environment	Operation & Maintenance	Construction Cost	Evaluation
Open Channel RC 2100 mm × 1050 mm F - C L = 23,500 m		<p>Advantage</p> <ul style="list-style-type: none"> <li>Easy construction work because of its simple structure.</li> </ul> <p>Disadvantage</p> <ul style="list-style-type: none"> <li>Much materials and labor are necessary due to long construction work.</li> <li>Hard work due to sandy soil and base rock at mountain foot.</li> <li>Complicated alignment along the contour line.</li> <li>Long construction period.</li> <li>Complicated structure for river crossing.</li> <li>Hard construction work on slope.</li> <li>Moving of construction equipment in desert is hard.</li> </ul>	<p>Advantage</p> <ul style="list-style-type: none"> <li>Planting and development of green zone along the channel is possible.</li> </ul> <p>Disadvantage</p> <ul style="list-style-type: none"> <li>Give an unpleasant feeling to inhabitants due to bad odor emission and flowing of filth in raw sewage.</li> <li>Hazardous to inhabitants because of exposure to pathogenic bacteria.</li> <li>Utilization of channel site for other purposes is not possible.</li> </ul>	<p>Advantage</p> <ul style="list-style-type: none"> <li>Direct maintenance and repair of channel from outside is possible.</li> <li>Easy maintenance work.</li> </ul> <p>Disadvantage</p> <ul style="list-style-type: none"> <li>Fence and other facilities for safety is necessary in residential area.</li> <li>Garbage and rubbish is apt to be dumped in.</li> <li>Illegal diversion is expected. Security of planned water amount is uncertain.</li> <li>Watching over the channel is necessary. But use of vehicle is impossible.</li> <li>Deposit of sand in the channel will occur.</li> </ul>	<p>Including TAX</p> <p>\$ 12,722,251- ( ¥1,781,115,140- )</p> <p>Excluding TAX</p> <p>\$ 11,628,102- ( ¥1,627,934,280- ) ( 124 % )</p>	
Inverted Siphon (Inner Pressure Pipe) φ 1400 mm F - C L = 9,790 m		<p>Advantage</p> <ul style="list-style-type: none"> <li>Short construction period.</li> <li>Good workability due to use of pre-cast products.</li> </ul> <p>Disadvantage</p> <ul style="list-style-type: none"> <li>Good pipe material durable for inner pressure is required.</li> </ul>	<p>Advantage</p> <ul style="list-style-type: none"> <li>Utilization of pipeline site for other purposes is possible.</li> <li>No bad odor.</li> </ul> <p>Disadvantage</p> <ul style="list-style-type: none"> <li>Blow-off of raw sewage to the Lurin River at regular intervals is necessary for maintenance.</li> </ul>	<p>Advantage</p> <ul style="list-style-type: none"> <li>Dumping of garbage and rubbish is impossible.</li> <li>Facilities for environmental preservation is not necessary.</li> <li>Regular maintenance.</li> </ul> <p>Disadvantage</p> <ul style="list-style-type: none"> <li>Maintenance work from outside is hard.</li> <li>Maintenance work for equipment such as blow-off valves and air valves is necessary.</li> <li>Blow-off work at regular intervals is necessary.</li> </ul>	<p>Including TAX</p> <p>\$ 18,318,556.53 ( ¥2,564,597,900- )</p> <p>Excluding TAX</p> <p>\$ 9,383,186.55 ( ¥1,313,646,159- ) ( 100 % )</p>	◎



TABLE A12-1 COMPARISON BETWEEN OPEN CHANNEL AND INVERTED SIPHON (CONT'D)

Conduit	Length	Workability	Influence on Environment	Operation & Maintenance	Construction Cost	Evaluation
Open Channel RC 2100 x 1050 mm	H - I $\ell = 9,700$ m	Same as Phase I	Same as Phase I	Same as Phase I	<u>Including TAX</u> \$ 5,345,187- ( ¥ 748,326,180- ) <u>Excluding TAX</u> \$ 4,910,757- ( ¥ 687,505,980- ) ( 178 % )	○
Inverted Siphon (Inner Pressure Pipe) φ 1200 mm	H - I $\ell = 2,500$ m open channel ( + 1,500 m )	Same as Phase I	Same as Phase I	Same as Phase I	<u>Including TAX</u> \$ 3,785,680- ( ¥ 529,995,200- ) <u>Excluding TAX</u> \$ 2,752,478- ( ¥ 385,346,920- ) ( 100 % )	○ ◎



## **APPENDIX 13**

### **POSSIBLE TREATMENT CAPACITY IN SAN JUAN STP WITH RECONSTRUCTION**



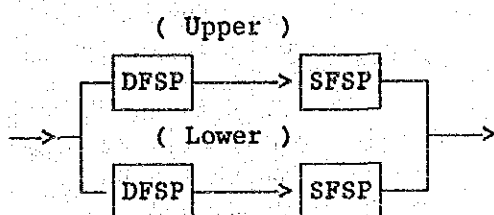
**APPENDIX 13      POSSIBLE TREATMENT CAPACITY IN SAN JUAN STP  
WITH RECONSTRUCTION**

**- In case of adoption for Anaerobic Stabilization Pond -**

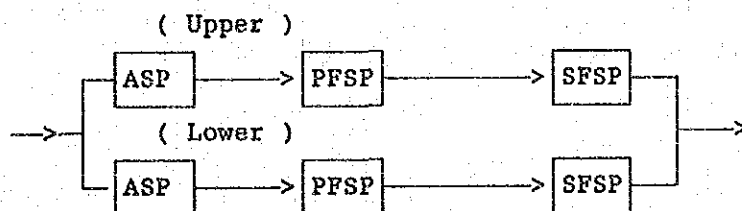
**A13.1 Basic Concept for Reconstruction**

- 1) Treatment method of PFSP-SFSP System of existing ponds shall be changed to ASP-PFSP-SFSP System in order to increase treatment capacity.

Existing Flow Diagram

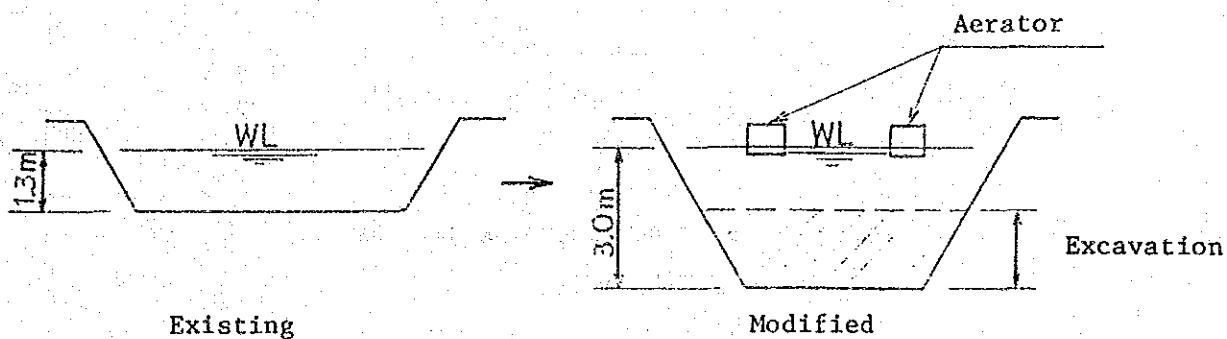


Modified Flow Diagram



Remarks: ASP-Anaerobic Stabilization Pond  
PFSP-Primary Facultative Stabilization Pond  
SFSP-Secondary Facultative Stabilization Pond

- 2) Effective water depth in some Primary Ponds shall be modified by excavation from 1.3 m to 3.0 m.



### A13.2 Upper Battery

#### 1) Volume and water surface area of ponds after reconstruction

Existing Primary Ponds P1 and P2 are changed to ASP.

No. of Pond	Water Surface Area (ha)(Depth 1.3 m)	ASP	PFSP	SFSP	Total Volume and Water Surface Area
P1	0.75	*			Total Volume of ASP
P2	0.51	*			(Depth 3.0 m)
P3	0.51		*		= 18,606 + 11,682
P4	0.81		*		= 30,288 m <sup>3</sup>
P5	0.85			*	Total Area of PFSP
P6	0.68			*	(Depth 1.3 m)
S1	2.00		*		= 5.55 ha
S2	2.23		*		Total Area of SFSP
S3	0.99			*	(Depth 1.3 ha)
S4	0.92			*	= 3.44 ha
Total	10.25	1.26	5.55	3.44	

#### 2) Study for Possible Treatment Capacity

##### a. Design Condition

- Influent BOD = 250 mg/l

##### b. ASP

- BOD Volumetric Load :  $L_v = 0.1$  to  $0.15$  kg-BOD/m<sup>3</sup>/day  
(at average temp. in coldest month, 15°C)
- Possible Treatment Capacity :  $Q_1$

$$Q_1 = \frac{30,288 \times (0.1 \text{ to } 0.15)}{250 \times 10^{-3}} = 12,115 \text{ to } 18,173 \text{ m}^3/\text{day}$$

- BOD Removal Rate in ASP : Approx. 50 %
- Effluent BOD : 250 to ( 1 - 0.5 ) = 125 mg/l

##### c. PFSP

- BOD Surface Load :  $L_s = 380$  kg-BOD/ha/day
- Possible Treatment Capacity :  $Q_2$

$$Q_2 = \frac{380 \times 5.55}{125 \times 10^{-3}} = 16,872 \text{ m}^3/\text{day}$$

According to the value of Q<sub>1</sub> and Q<sub>2</sub>, possible treatment capacity is 16,872 m<sup>3</sup>/day.

d. SFSP

- Influent BOD :

$$L = 16,872 \text{ m}^3/\text{day} \times 125 \text{ mg/l} \times (1 - 0.6) \times 10^{-3} \\ = 844 \text{ kg-BOD/day}$$

- BOD Surface Load :

$$L_s = 844 / 3.44 = 245 \text{ kg-BOD/day} \quad \text{-----ok}$$

e. Possible Treatment Capacity in Upper Battery From the result of above calculation, possible treatment capacity in Upper Battery is 16,872 m<sup>3</sup>/day.

f. Check

- Detention Time :

$$\text{ASP} : 30,288 \times 1/16,872 = 1.8 \text{ days}$$

$$\text{PFSP} : 55,500 \times 1.3 \times 1/16,872 = 4.3 \text{ days}$$

$$\text{SFSP} : 34,400 \times 1.3 \times 1/16,872 = 2.7 \text{ days}$$

### A13.3 Lower Battery

- 1) Volume and Water Surface Area in Pond after reconstruction of the Existing Pond P8 be changed to ASP. P7 and P5 are excluded in this plan since these are used for Experimental Fishculture Project.

No. of Ponds	Water Surface Area (ha)(Depth 1.3 m)	ASP	PFSP	SFSP	Total Volume and Water Surface Area
P8	1.10	*			Volume of ASP
P9	0.88		*		(Depth 3.0 m)
P10	0.69		*		= 27,590 m <sup>3</sup>
P11	0.89			*	Surface Area of PFSP
S6	1.49		*		(Depth 1.3 m)
S7	1.32		*		= 4.98 ha
S8	1.80(divide)		*	*	Surface Area of SFSP
S9	0.49			*	(Depth 1.3 m)
S10	0.53			*	= 3.11 ha
Total	9.19	1.1	4.98	3.11	

2) Study for Possible Treatment Capacity

a. Design Condition

- Influent BOD = 250 mg/l

b. ASP

- BOD Volumetric Load :  $L_v = 0.1 \text{ to } 0.15 \text{ kg-BOD/m}^3/\text{day}$   
(at average temp. in coldest month, 15°C)

- Possible Treatment Capacity :  $Q_1$

$$Q_1 = \frac{27,590 \times (0.1 \text{ to } 0.15)}{250 \times 10^{-3}} = 11,036 \text{ to } 16,554 \text{ m}^3/\text{day}$$

- BOD Removal Rate in ASP = Approx. 50%
- Effluent BOD =  $250 \times (1 - 0.5) = 125 \text{ mg/l}$

c. PFSP

- BOD Surface Load :  $L_s = 380 \text{ kg-BOD/ha/day}$
- Possible Treatment Capacity :  $Q_2$

$$Q_2 = \frac{380 \times 4.98}{125 \times 10^{-3}} = 15,139 \text{ m}^3/\text{day}$$

According to the value of  $Q_1$  and  $Q_2$ , possible treatment capacity is 15,139 m<sup>3</sup>/day.

d. SFSP

- Inlet BOD

$$L = 15,139 \text{ m}^3/\text{day} \times 125 \text{ mg/l} \times (1 - 0.6) \times 10^{-3} \\ = 757 \text{ kg-BOD/day}$$

- BOD Surface Load :

$$L_s = 757 \text{ kg-BOD/day} \quad \text{----- ok}$$

e. Possible treatment Capacity:

From the result of above calculation, possible treatment capacity in Lower Battery after reconstruction is 15,139 m<sup>3</sup>/day.

f. Check

- Detention Time :

$$\text{ASP} : 27,590 \times 1/15,139 = 1.8 \text{ days}$$

$$\text{PFSP} : 49,800 \times 1.3 \times 1/15,139 = 4.3 \text{ days}$$

$$\text{SFSP} : 31,100 \times 1.3 \times 1/15,139 = 2.7 \text{ days}$$



#### A13.4 Total Possible Treatment Capacity

Treatment Capacity	Present	After reconst.	B/A
Upper Battery	10,800 m <sup>3</sup> /day	16,872 m <sup>3</sup> /day	1.56
Lower Battery	10,800 m <sup>3</sup> /day	15,139 m <sup>3</sup> /day	1.40
<hr/>			
Total	21,600 m <sup>3</sup> /day	32,011 m <sup>3</sup> /day	1.48
	( 0.25 m <sup>3</sup> /s )	( 0.37 m <sup>3</sup> /s )	



## **APPENDIX 14**

### **CAPACITY CALCULATION OF STP**



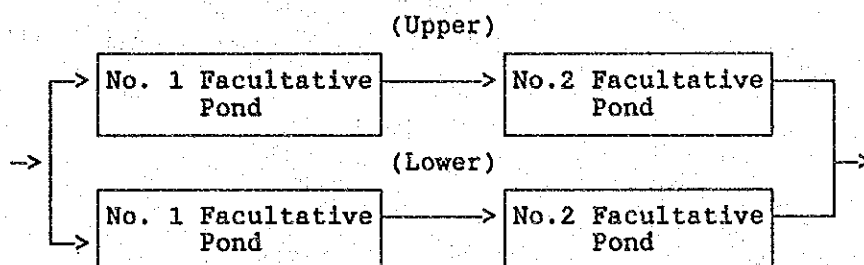
## APPENDIX 14 CAPACITY CALCULATION OF STP

### A14.1 Possible Treatment Capacity in Proposed Site (a) San Juan WSP

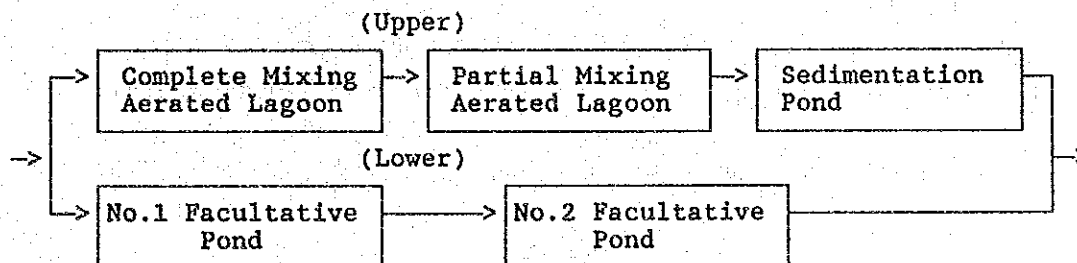
#### (1) Basic Concept for Reconstruction

- Out of the two-series treatment consisting of Upper and Lower Battery facultative ponds, treatment method of Upper Battery will be changed to Aerated Lagoon system in order to increase treatment capacity.

##### Existing Flow Diagram



##### Modified Flow Diagram



- Effective water depth in Upper Battery Pond will be modified by excavation from 1.3 m to 3.0 m.

#### (2) Treatment Capacity after Reconstruction

- Reconstruction plan and effective pond volume are shown in FIGURE A14-1 and TABLE A14-1.
- Capacity calculation for Aerated Lagoon System in modified Upper Battery based on standard detention time and effective volume is shown in TABLE A14-2. From the result of calculation, possible treatment capacity is 0.63 m<sup>3</sup>/s.

- (3) Total treatment capacity in San Juan Treatment Plant after reconstruction

	Treatment Method	Possible Treatment Capacity	Total Treatment Capacity
Upper Battery	Aerated Lagoon	0.63 m <sup>3</sup> /s	0.75 m <sup>3</sup> /s (64,800 m <sup>3</sup> /day)
Lower Battery	Facultative Pond	21,600 m <sup>3</sup> /day x 1/2 = 10,800 m <sup>3</sup> /day = approx. 0.12m <sup>3</sup> /s	

- (4) Capacity Calculation for Aerated Lagoon on Upper Battery

a. Design Criteria

- Design Flowrate  $Q_d \text{ av} = 0.63 \text{ m}^3/\text{s} = \text{approx. } 54,400 \text{ m}^3/\text{day}$
- Influent BOD<sub>5</sub>  $L_i = 250 \text{ mg/l}$
- Influent SS  $S_i = 250 \text{ mg/l}$

b. Complete Mixing Aerated Lagoon

- Detention Time  $t^* c = 1.5 \sim 2.0 \text{ days}$
- Volume  $V_c = 54,400 \times (1.5 \sim 2.0)$   
 $= 81,600 \sim 108,800 \text{ m}^3$
- Depth  $D_c = 3.0 \text{ m}$
- Water Surface Area  $A_c = V_c/D_c$   
(mid-depth)  $= (81,600 \sim 108,800)/3.0$   
 $= 27,200 \sim 36,600 \text{ m}^2$
- Dimension  $P_1, P_2, P_3, P_4, P_5, - \text{Total (Refer to P)}$   
 $27,473 \text{ m}^2 \times 3.0 \text{ m D} \times 82,419 \text{ m}^3$   
check  
 $t^* c = 82,419/54,400 = 1.52 \text{ days} \dots \text{ok}$
- Oxygen Requirement  $Or = 6.24 \times 10^{-5} \times 54,400 \times 250$   
 $= 849 \text{ kg-O}_2/\text{hr}$
- Power Requirement
  - a. as for Or  $P_1 = 849 \times 1/2.0 = 425 \text{ kW}$
  - b. as for C.M.P.  $P_2 = 82,419 \times 6 \times 1/1,000 = 495 \text{ kW}$   
 $P_1 < P_2$
- Aerator-I 4 sets per 1 basin  
Aerator-I  
 $P_a = 495 \times 1.1 = 545 \text{ kW}$   
therefore:  
 $37 \text{ kW} \times 4 \text{ sets } \uparrow$   
 $30 \text{ kW} \times 8 \text{ sets } \rightarrow (564 \text{ kW})$   
 $22 \text{ kW} \times 8 \text{ sets } \downarrow$

c. Partial Mixing Aerated Lagoon

- Detention Time  $t^*p = 1.5 \sim 3.0$  days
- Volume  $Vp = 54,400 \times (1.5 \sim 3.0)$   
 $81,600 \sim 163,200 \text{ m}^3$
- Depth  $Dp = 3.0 \text{ m}$
- Water Surface Area  $Ap = (81,600 \sim 163,200)/3.0$   
(mid-depth)  $= 27,200 \sim 54,400 \text{ m}^2$
- Dimension  $S1, S2, S3$  - Total  
 $45,404 \text{ m}^2 \times 3.0 \text{ m D} \times 136,212 \text{ m}^3$   
check  
 $t^*p = 136,212/54,400 = 2.5$  days...ok
- Power Requirement  $Pr \geq 1 \text{ W/m}^3$   
for Mixing  $P \geq 136,212 \times 1.0 = 136 \text{ kW}$
- Aerator-II 4 sets per 1 basin  
 $Pa = 136 \times 1.1$   
 $= 150 \text{ kW}$   
therefore:  
 $7.5 \text{ kW} \times 4 \uparrow$   
 $15 \text{ kW} \times 4 \rightarrow (164\text{kW})$   
 $18.5 \text{ kW} \times 4 \downarrow$

d. Chlorinator

- Chlorine Feeding Rate 3 ppm
- Total Inflow of Upper  
and Lower Battery 65,200  $\text{m}^3/\text{day}$
- Capacity  $q = 65,200 \text{ m}^3/\text{day} \times 3 \text{ ppm} \times 10^{-3}$   
 $= 195.6 \text{ kg-cl/day}$   
 $= 8.2 \text{ kg-cl/hr}$   
therefore, chlorinator will be:  
 $10 \text{ kg-cl/hr} \times 2 \text{ sets (1 set-standby)}$

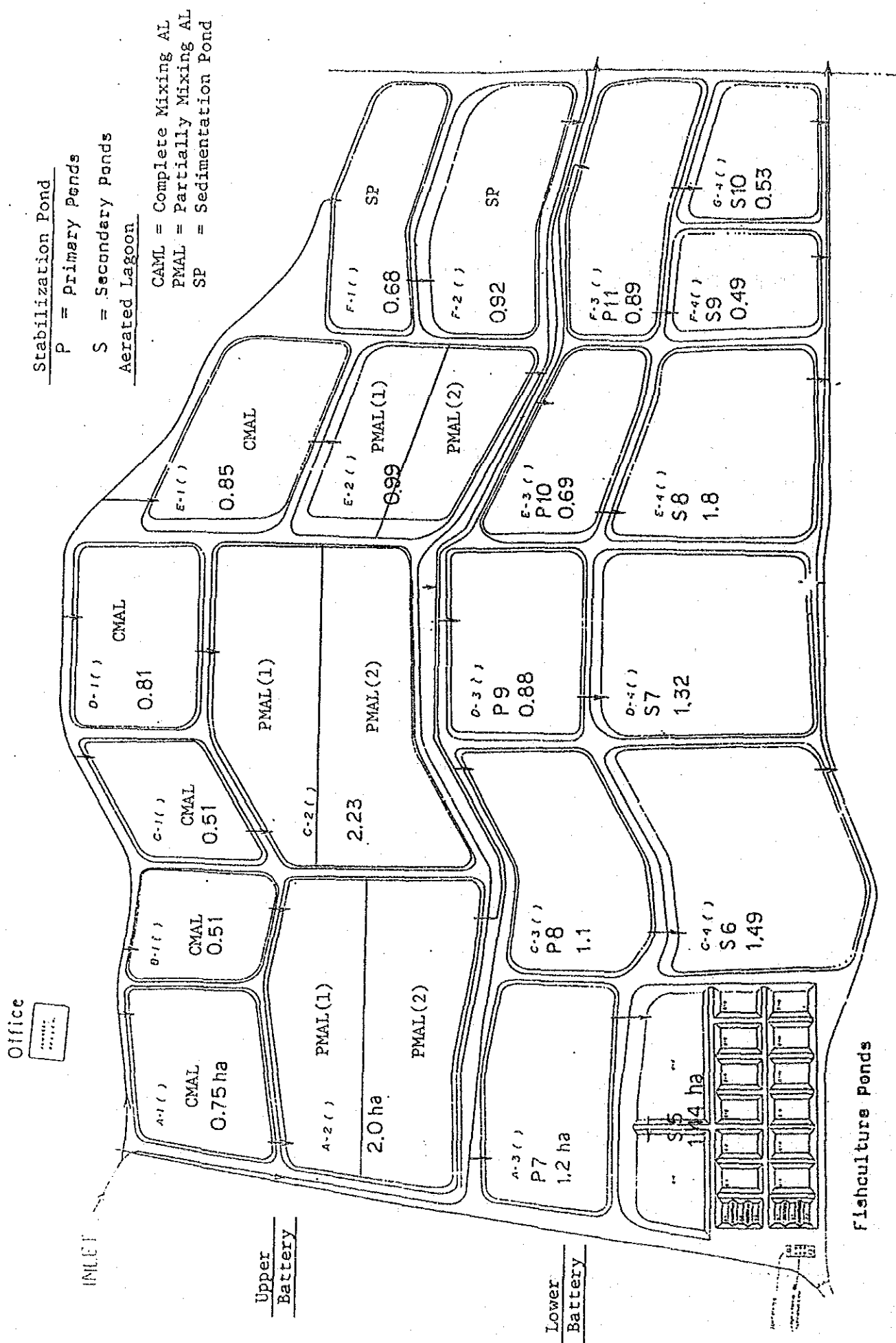


FIGURE A14-1 MODIFIED PLAN OF SAN JUAN S.T.P.



TABLE A14-1 EFFECTIVE VOLUME OF MODIFIED SAN JUAN STP  
(UPPER BATTERY, DEPTH 3m)

Pond No.	Existing Water Surface Area (m <sup>2</sup> )	Equivalent Square Length (m)	① Middle Depth Equivalent Length (m)	② Depth (m)	①×② Effective Volume (m <sup>3</sup> )
P <sub>1</sub>	7,500	86.6	77.6	3.0	18,606
P <sub>2</sub>	5,100	71.4	62.4	3.0	11,682
P <sub>3</sub>	5,100	71.4	62.4	3.0	11,682
P <sub>4</sub>	8,100	90.0	81.0	3.0	19,683
P <sub>5</sub>	8,500	92.2	83.2	3.0	20,766
P <sub>6</sub>	6,800	82.5	73.5	3.0	16,206
S <sub>1</sub>	20,000	141.4	132.4	3.0	52,590
S <sub>2</sub>	22,300	149.3	140.3	3.0	59,052
S <sub>3</sub>	9,900	99.5	90.5	3.0	24,570
S <sub>4</sub>	9,200	95.9	86.9	3.0	22,656
					( 257,493 )

TABLE A14-2

## POSSIBLE TREATMENT CAPACITY FOR AERATED LAGOON IN UPPER BATTERY

Process	Pond No.	Total Pond Volume	Standard Detention Time	Possible Treatment Capacity
Completely Mixing Aerated Lagoon	P 1	82.419	1.5	$82,419 \times 1/1.5$
	P 2		2.0	$= 54,946 \text{ m}^3/\text{day}$
	P 3		↓	$= 0.636 \text{ m}^3/\text{day}$
	P 4		1.5	
	P 5			
Partially Mixing Aerated Lagoon	S 1	136.212	3 - Cell	$136,212 \times 1/2.5$
	S 2		1.5	$= 54,485 \text{ m}^3/\text{day}$
	S 3		3.0	$= 0.631 \text{ m}^3/\text{s}$
			↓	2.5
Sedimentation Pond	P 6	38.862	1.0	$38,862 \times 1/1.0$
	P 4			$= 38,862 \text{ m}^3/\text{day}$
				$= 0.45 \text{ m}^3/\text{s}$

#### A14.2 Capacity Calculation for Aerated Lagoon in Proposed Site (b) and (c)

##### (1) Design Criteria

Design Flow Rate: 0.5 m<sup>3</sup>/s, 0.83 m<sup>3</sup>/s, 1.0 m<sup>3</sup>/s

Influent BOD<sub>5</sub> : 250 mg/l

Influent SS : 250 mg/l

##### (2) Estimate Treated Water Quality

	BOD	SS
Removal Rate	88%	76%
Water Quality	30 mg/l	60 mg/l

##### (3) Flow Diagram

Flow diagram is shown in FIGURE A14-2.

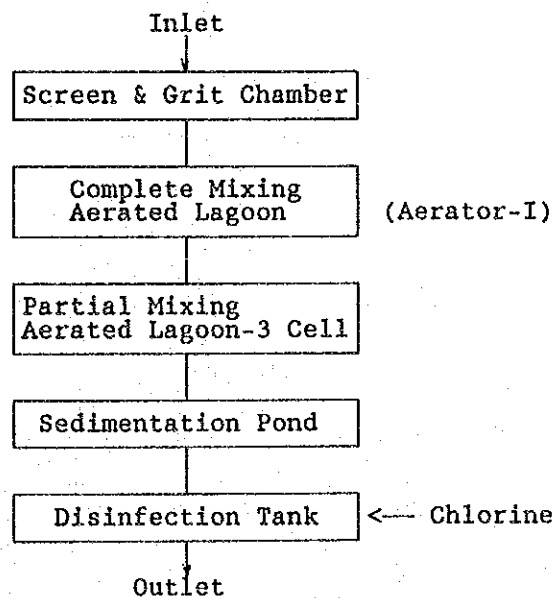


FIGURE A14-2 Flow Diagram for Aerated Lagoon (Dual Power) System

##### (4) Capacity Calculation

Capacity calculation for each proposed site are shown in TABLE A14-3.

TABLE A14-3 Capacity Calculation for Aerated Lagoon at Each Design Flow

Item	Design Flow	0.5 m <sup>3</sup> /s	0.83 m <sup>3</sup> /s	1.0 m <sup>3</sup> /s
1. Design Criteria				
- Design Flowrate		Qd av = 0.5 m <sup>3</sup> /s = 43,200 m <sup>3</sup> /day	Qd av = 0.83 m <sup>3</sup> /s = 71,700 m <sup>3</sup> /day	Qd av = 1.0 m <sup>3</sup> /s = 86,400 m <sup>3</sup> /day
- Influent BOD <sub>5</sub>		Li = 250 mg/l	Li = 250 mg/l	Li = 250 mg/l
- Influent SS		Si = 250 mg/l	Si = 250 mg/l	Si = 250 mg/l
2. Complete Mixing Aerated Lagoon				
- Detention Time		t <sup>*</sup> c = 1.5~2.0 days	t <sup>*</sup> c = 1.5~2.0 days	t <sup>*</sup> c = 1.5~2.0 days
- Volume		Vc = 43,200 x (1.5~2.0) = 64,800~86,400 m <sup>3</sup>	Vc = 71,700 x (1.5~2.0) = 107,550~143,400 m <sup>3</sup>	Vc = 86,400 x (1.5~2.0) = 129,600~172,800 m <sup>3</sup>
- Depth		Dc = 3.0 m	Dc = 3.0 m	Dc = 3.0 m
- Water Surface Area (mid-depth)		Ac = Vc/Dc = (64,800~86,400)/3.0 = 21,600~28,800 m <sup>2</sup>	Ac = (107,550~143,400)/3.0 = 35,850~47,800 m <sup>2</sup>	Ac = (129,600~172,800)/3.0 = 43,200~57,600 m <sup>2</sup>
- Dimension		100 m x 48 m x 3.0 m <sup>p</sup> x 14,400 m <sup>2</sup> x 6 basins check	105 m x 45 m x 3.0 m <sup>p</sup> x 14,490 m <sup>2</sup> x 10 basins check	100 m x 48 m x 3.0 m <sup>p</sup> x 14,400 m <sup>2</sup> x 12 basins check
- Oxygen Requirement		Total Volume Vc = 14,400 x 6 = 86,400 m <sup>3</sup> t <sup>*</sup> c = 86,400/43,200 = 2.0 days...ok Or = 6.24 x 10 <sup>-5</sup> x 43,200 x 250 = 674 kg-O <sub>2</sub> /hr	Total Volume Vc = 14,490 x 10 = 144,900 m <sup>3</sup> t <sup>*</sup> c = 144,900/71,700 = 2.0 days...ok Or = 6.24 x 10 <sup>-5</sup> x 71,700 x 250 = 1,119 kg-O <sub>2</sub> /hr	Total Volume Vc = 14,400 x 12 = 172,800 m <sup>3</sup> t <sup>*</sup> c = 172,800/86,400 = 2.0 days...ok Or = 6.24 x 10 <sup>-5</sup> x 86,400 x 250 = 1,348 kg-O <sub>2</sub> /hr
- Power Requirement		P <sub>1</sub> = 674 x 1/2.0 = 337 kW P <sub>2</sub> = 86,400 x 6 x 1/1,000 = 519 kW P <sub>1</sub> < P <sub>2</sub>	P <sub>1</sub> = 1,119 x 1/2 = 560 kW P <sub>2</sub> = 144,900 x 6 x 1/1,000 = 870 kW P <sub>1</sub> < P <sub>2</sub>	P <sub>1</sub> = 1,348 x 1/2.0 = 674 kW P <sub>2</sub> = 172,800 x 6 x 1/1,000 = 1,037 kW P <sub>1</sub> < P <sub>2</sub>
- Aerator- I		4 sets per 1 basin Aerator- I Pa = 519 kW x 1.1 = 571 kW ∴ 30 kW x 12 sets 18.5 kW x 12 sets } (582 kW)	4 sets per 1 basin Aerator- II Pa = 870 kW x 1.1 = 957 kW ∴ 30 kW x 20 sets 18.5 kW x 20 sets } (970 kW)	4 sets per 1 basin Aerator- I Pa = 1,037 kW x 1.1 = 1,141 kW ∴ 30 kW x 24 sets 18.5 kW x 24 sets } (1,164 kW)

TABLE A14-3 Capacity Calculation for Aerated Lagoon on Each Design Flow (cont'd)

Item	Design Flow	0. 5 m <sup>3</sup> /s	0. 8 3 m <sup>3</sup> /s	1. 0 m <sup>3</sup> /s
3. Partial Mixing Aerated Lagoon				
- Detention Time		$t^*p = 1.5 \sim 3.0$ days, 3-cells	$t^*p = 1.5 \sim 3.0$ days, 3-cells	$t^*p = 1.5 \sim 3.0$ days, 3-cells
- Volume		$V_p = 43,200 \times (1.5 \sim 3.0)$ $= 64,800 \sim 129,600 \text{ m}^3$	$V_p = 71,700 \times (1.5 \sim 3.0)$ $= 107,550 \sim 215,100$	$V_p = 86,400 \times (1.5 \sim 3.0)$ $= 129,600 \sim 259,200 \text{ m}^3$
- Depth		$D_p = 3.0 \text{ m}$	$D_p = 3.0 \text{ m}$	$D_p = 3.0 \text{ m}$
- Water Surface Area (mid-depth)		$A_p = (64,800 \sim 129,600)/3.0$ $= 21,600 \sim 43,200 \text{ m}^2$	$A_p = (107,550 \sim 215,100)/3$ $= 35,850 \sim 71,700 \text{ m}^2$	$A_p = (129,600 \sim 259,200)/3$ $= 43,200 \sim 86,400 \text{ m}^2$
- Dimension		$100 \text{ m} \times 33 \text{ m} \times 3.0 \text{ m}^3 \times 9,900 \text{ m}^3 \times 9 \text{ basins}$ (3 cells x 3 series)	$71 \text{ m} \times 46 \text{ m} \times 3.0 \text{ m}^3 \times 9,798 \times 15 \text{ basins}$ (3 cells x 5 Series)	$100 \text{ m} \times 33 \text{ m} \times 3.0 \text{ m}^3 \times 9,900 \text{ m}^3 \times 18 \text{ basins}$ (3 cells x 6 Series)
		check	check	check
- Total Volume		$V_p = 9,900 \times 9 = 89,100 \text{ m}^3$	$V_p = 9,798 \times 15 = 146,970 \text{ m}^3$	$V_p = 9,900 \times 18 = 178,200 \text{ m}^3$
- $t^*p$		$t^*p = 89,100/43,200 = 2.1$ days---ok	$t^*p = 146,970/71,700 = 2.0$ days ---ok	$t^*p = 178,200/86,400 = 2.1$ days ---ok
- Power Requirement for Mixing		$Pr \geq 1W/m^3$ $P \geq 89,100 \times 1.0 = 89 \text{ kW}$	$P = 146,970 \times 1.0 = 147 \text{ kW}$	$P = 178,200 \times 1.0 = 178 \text{ kW}$
- Aerator - II		2 sets per 1 cell $Pa = 89 \times 1.1$ $= 98 \text{ kW}$ $\therefore 5.5 \text{ kW} \times 18 \text{ sets (99kW)}$	2 sets per 1 cell $Pa = 147 \times 1.1$ $= 162 \text{ kW}$ $\therefore 5.5 \text{ kW} \times 30 \text{ sets (165kW)}$	2 sets per 1 cell $Pa = 178 \times 1.1$ $= 196 \text{ kW}$ $\therefore 5.5 \text{ kW} \times 36 \text{ sets (198kW)}$
4. Chlorinator		- Chlorine Feeding Rate : 3 ppm  - Capacity $q = 43,200 \text{ m}^3/\text{day} \times 3 \text{ ppm} \times 10^{-3}$ $= 129.6 \text{ kg-cl/day}$ $= 5.4 \text{ kg-cl/hr}$ $\therefore$ chlorinator 10 kg-cl/hr x 2 sets (1 set-standby)	$q = 71,700 \text{ m}^3/\text{day} \times 3 \text{ ppm} \times 10^{-3}$ $= 215.1 \text{ kg-cl/day}$ $= 9.0 \text{ kg-cl/hr}$ $\therefore$ chlorinator 10 kg-cl/hr x 2 sets (1 set-standby)	$q = 86,400 \text{ m}^3/\text{day} \times 3 \text{ ppm} \times 10^{-3}$ $= 259.2 \text{ kg-cl/day}$ $= 10.8 \text{ kg-cl/hr}$ $\therefore$ chlorinator 15 kg-cl/hr x 2 sets (1 set-standby)

A.14.3 Capacity Calculation for Stabilization Pond (Facultative Pond) in Proposed Site (e) and (f).

(1) Design Criteria

Design flowrate :  $Q = 0.5 \text{ to } 3.5 \text{ m}^3/\text{s}$

Influent BOD<sub>5</sub> : 250 mg/l

Influent SS : 250 mg/l

Influent BOD<sub>5</sub> Load :  $L_{i1} = Q \times 250 \text{ mg/l} \times 10^{-3} \text{ (kg-BOD/day)}$

(2) Estimate Treatment Water Quality

BOD<sub>5</sub> removal rate : 80%

Effluent BOD<sub>5</sub> : 49 mg/l

(3) Flow Chart

(Facultative Ponds System)

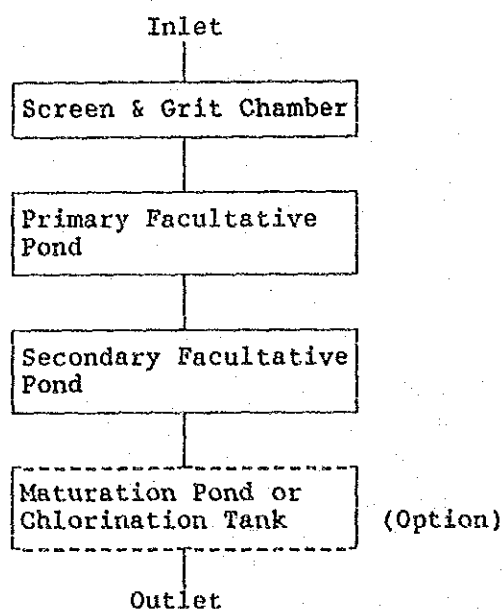


FIGURE A14-3 Flow Diagram for Stabilization Pond System

- Capacity Calculation

(i) Primary Facultative Pond

BOD<sub>5</sub> water surface load:  $Li_1 = 382 \text{ (kg-BOD/ha/day)}$   
 Water surface area :  $Ap = Q \times 250 \times 10^{-3} \times 1/382 \text{ (ha)}$   
 (mid-depth)  
 Water depth :  $Dp = 1.5 \text{ m}$   
 Volume :  $Vp = Ap \times Dp \text{ (m}^3\text{)}$   
 Detention time :  $t^*p = Vp/Q \text{ (days)}$   
 Effluent BOD<sub>5</sub> :  $Le_1 = 250 \times (1 - 0.7) = 75 \text{ mg/l}$

(ii) Secondary Facultative Pond

BOD<sub>5</sub> water surface load:  $Li_2 = 200 \text{ (kg-BOD/ha.day)}$   
 Water surface area  
 (mid-depth) :  $As = Q \times 75 \times 10^{-3} \times 1/200 \text{ (ha)}$   
 Water Depth :  $Dp = 1.5 \text{ m}$   
 Volume :  $Vp = As \times Dp \text{ (m}^3\text{)}$   
 Detention Time :  $t^*S = Vp/Q \text{ (days)}$   
 Effluent BOD<sub>5</sub> :  $Le_2 = 250 \times (1 - 0.35)$   
 $= 49 \text{ mg/l}$

Results of capacity calculation are shown in TABLE A14-4.

TABLE A14-4 CAPACITY CALCULATION FOR FACULTATIVE POND

Design Flow	Q (m <sup>3</sup> /S)	0.5	1.5	1.7	2.0	2.2	2.5	2.67	3.0	3.5
Primary Facultative Pond	Lil (kg-BOD/day)	10,800	32,400	36,720	43,200	47,520	54,000	57,672	64,800	75,600
	Ap (ha)	28.3	84.8	96.1	113.1	124.4	141.4	151.0	169.6	197.9
	Dp (m)	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5
	Vp (m <sup>3</sup> )	424,500	1,272,000	1,442,000	1,697,000	1,866,000	2,121,000	2,265,000	2,544,000	2,969,000
	t* <sub>p</sub> (days)	9.8	9.8	9.8	9.8	9.8	9.8	9.8	9.8	9.8
Secondary Facultative Pond	As (ha)	16.2	48.6	55.1	64.8	71.3	81.0	86.5	97.2	113.4
	Ds (m)	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5
	Vs (m <sup>3</sup> )	243,000	729,000	826,500	972,000	1,070,000	1,215,000	1,288,000	1,458,000	1,701,000
	t* <sub>s</sub> (days)	5.6	5.6	5.6	5.6	5.6	5.6	5.6	5.6	5.6
Total Mid-Depth Water Surface Area: Ap + As (ha)		44.5	133.4	151.2	177.9	195.7	222.4	237.5	266.8	311.3
Total Detention Time: t* <sub>p</sub> + t* <sub>s</sub> (days)		15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4



## **APPENDIX 15**

### **DAILY FLOW VARIATION AND INTAKE AMOUNT**



TABLE A15-1 PLANNED INTAKE AMOUNT

MEASURING TIME hh : mm	May 31-June 1		October 19-20		AVERAGE RATE OF 2 DATA	AMOUNT FOR 1 M3/S	
	CIRCUN.	RATE	CIRCUN.	RATE		FLOW	INTAKE
	M3/S		M3/S			M3/S	M3/S
10 : 00	1.358	1.197	1.562	1.350	1.274	1.294	1.170
10 : 15	1.358	1.197	1.578	1.364	1.281	1.301	1.170
10 : 30	1.454	1.282	1.443	1.247	1.265	1.285	1.170
10 : 45	1.345	1.186	1.462	1.263	1.225	1.245	1.170
11 : 00	1.382	1.218	1.457	1.259	1.239	1.259	1.170
11 : 15	1.321	1.164	1.440	1.245	1.205	1.224	1.170
11 : 30	1.269	1.118	1.380	1.192	1.156	1.174	1.170
11 : 45	1.269	1.118	1.372	1.186	1.153	1.171	1.170
12 : 00	1.338	1.179	1.380	1.192	1.186	1.205	1.170
12 : 15	1.294	1.140	1.365	1.180	1.160	1.179	1.170
12 : 30	1.276	1.125	1.360	1.175	1.151	1.169	1.169
12 : 45	1.276	1.125	1.343	1.161	1.143	1.161	1.161
13 : 00	1.251	1.103	1.331	1.150	1.127	1.145	1.145
13 : 15	1.251	1.103	1.321	1.141	1.123	1.141	1.141
13 : 30	1.246	1.099	1.303	1.126	1.113	1.131	1.131
13 : 45	1.271	1.120	1.289	1.114	1.118	1.135	1.135
14 : 00	1.219	1.074	1.276	1.103	1.089	1.107	1.107
14 : 15	1.219	1.074	1.299	1.122	1.099	1.116	1.116
14 : 30	1.222	1.077	1.331	1.150	1.114	1.132	1.132
14 : 45	1.227	1.081	1.274	1.101	1.091	1.109	1.109
15 : 00	1.227	1.081	1.256	1.086	1.084	1.101	1.101
15 : 15	1.246	1.099	1.254	1.084	1.092	1.109	1.109
15 : 30	1.246	1.099	1.234	1.066	1.083	1.100	1.100
15 : 45	1.271	1.120	1.202	1.038	1.080	1.097	1.097
16 : 00	1.271	1.120	1.189	1.028	1.075	1.092	1.092
16 : 15	1.214	1.070	1.177	1.017	1.044	1.061	1.061
16 : 30	1.214	1.070	1.169	1.010	1.041	1.057	1.057
16 : 45	1.209	1.066	1.179	1.019	1.043	1.059	1.059
17 : 00	1.209	1.066	1.172	1.012	1.040	1.056	1.056
17 : 15	1.174	1.035	1.187	1.025	1.031	1.047	1.047
17 : 30	1.179	1.039	1.199	1.036	1.038	1.055	1.055
17 : 45	1.202	1.059	1.189	1.028	1.044	1.061	1.061
18 : 00	1.202	1.059	1.187	1.025	1.043	1.059	1.059
18 : 15	1.259	1.110	1.182	1.021	1.066	1.083	1.083
18 : 30	1.259	1.110	1.119	0.967	1.039	1.055	1.055
18 : 45	1.174	1.035	1.132	0.978	1.007	1.023	1.023
19 : 00	1.174	1.035	1.149	0.993	1.014	1.031	1.031
19 : 15	1.129	0.995	1.147	0.991	0.994	1.009	1.009
19 : 30	1.129	0.995	1.137	0.982	0.989	1.005	1.005
19 : 45	1.134	1.000	1.092	0.943	0.972	0.988	0.988
20 : 00	1.147	1.011	1.104	0.954	0.983	0.999	0.999
20 : 15	1.149	1.013	1.099	0.950	0.982	0.998	0.998
20 : 30	1.149	1.013	1.109	0.959	0.986	1.002	1.002
20 : 45	1.134	1.000	1.104	0.954	0.977	0.993	0.993
21 : 00	1.134	1.000	1.082	0.935	0.968	0.983	0.983
21 : 15	1.139	1.004	1.089	0.941	0.973	0.989	0.989
21 : 30	1.142	1.006	1.092	0.943	0.975	0.991	0.991

TABLE A/5-1 PLANNED INTAKE AMOUNT

MEASURING TIME hh : mm	May 31-June 1		October 19-20		AVERAGE RATE OF 2 DATA	AMOUNT FOR 1 M3/S	
	CIRCUN.	RATE	CIRCUN.	RATE		FLOW	INTAKE
	M3/S		M3/S			M3/S	M3/S
21 : 45	1.137	1.002	1.077	0.930	0.967	0.982	0.982
22 : 00	1.137	1.002	1.072	0.926	0.964	0.980	0.980
22 : 15	1.112	0.980	1.062	0.918	0.949	0.964	0.964
22 : 30	1.114	0.982	1.054	0.911	0.947	0.962	0.962
22 : 45	1.087	0.958	1.015	0.877	0.918	0.932	0.932
23 : 00	1.089	0.960	1.027	0.887	0.924	0.939	0.939
23 : 15	0.923	0.814	1.012	0.875	0.845	0.858	0.858
23 : 30	0.911	0.803	0.965	0.834	0.819	0.832	0.832
23 : 45	1.034	0.912	0.938	0.811	0.862	0.875	0.875
0 : 00	1.034	0.912	0.946	0.817	0.865	0.879	0.879
0 : 15	1.027	0.905	0.919	0.794	0.850	0.863	0.863
0 : 30	1.030	0.907	0.921	0.796	0.852	0.866	0.866
0 : 45	0.865	0.762	0.916	0.792	0.777	0.790	0.790
1 : 00	0.868	0.764	0.950	0.821	0.793	0.806	0.806
1 : 15	0.906	0.799	0.938	0.811	0.805	0.818	0.818
1 : 30	0.909	0.801	0.955	0.825	0.814	0.827	0.827
1 : 45	0.911	0.803	0.978	0.845	0.824	0.838	0.838
2 : 00	0.911	0.803	0.985	0.851	0.828	0.841	0.841
2 : 15	0.909	0.801	0.987	0.853	0.828	0.841	0.841
2 : 30	0.909	0.801	1.000	0.864	0.833	0.846	0.846
2 : 45	0.911	0.803	0.997	0.862	0.833	0.846	0.846
3 : 00	0.911	0.803	0.955	0.825	0.815	0.828	0.828
3 : 15	0.916	0.807	0.894	0.773	0.790	0.803	0.803
3 : 30	0.921	0.812	0.841	0.727	0.770	0.782	0.782
3 : 45	0.916	0.807	0.846	0.731	0.770	0.782	0.782
4 : 00	0.914	0.805	0.846	0.731	0.768	0.781	0.781
4 : 15	0.839	0.739	0.841	0.727	0.733	0.745	0.745
4 : 30	0.839	0.739	0.848	0.733	0.736	0.748	0.748
4 : 45	0.884	0.779	0.843	0.729	0.755	0.767	0.767
5 : 00	0.887	0.782	0.875	0.756	0.769	0.781	0.781
5 : 15	0.887	0.782	0.877	0.758	0.770	0.783	0.783
5 : 30	0.889	0.784	0.872	0.754	0.769	0.781	0.781
5 : 45	0.923	0.814	0.904	0.781	0.798	0.811	0.811
6 : 00	0.923	0.814	0.911	0.787	0.801	0.814	0.814
6 : 15	0.941	0.829	0.990	0.855	0.843	0.856	0.856
6 : 30	0.941	0.829	1.005	0.868	0.849	0.863	0.863
6 : 45	1.005	0.885	1.097	0.948	0.917	0.932	0.932
7 : 00	1.097	0.967	1.132	0.978	0.973	0.988	0.988
7 : 15	1.092	0.962	1.194	1.032	0.998	1.014	1.014
7 : 30	1.236	1.090	1.259	1.088	1.089	1.107	1.107
7 : 45	1.239	1.092	1.316	1.137	1.115	1.133	1.133
8 : 00	1.271	1.120	1.353	1.169	1.145	1.164	1.164
8 : 15	1.345	1.186	1.411	1.220	1.203	1.222	1.170
8 : 30	1.353	1.192	1.474	1.274	1.233	1.253	1.170
8 : 45	1.387	1.222	1.562	1.350	1.287	1.307	1.170
9 : 00	1.454	1.282	1.581	1.366	1.325	1.346	1.170
9 : 15	1.387	1.222	1.583	1.368	1.296	1.316	1.170

TABLE A15-1 PLANNED INTAKE AMOUNT

MEASURING TIME hh : mm	May 31-June 1		October 19-20		AVERAGE RATE OF 2 DATA	AMOUNT FOR 1 M3/S	
	CIRCUN.	RATE	CIRCUN.	RATE		FLOW	INTAKE
	M3/S		M3/S			M3/S	M3/S
9 : 30	1.384	1.220	1.608	1.389	1.305	1.326	1.170
9 : 45	1.392	1.227	1.612	1.393	1.310	1.331	1.170
10 : 00	1.358	1.197	1.562	1.350	1.274	1.294	1.170
MAXIMUM Q <sub>ma</sub>	1.454	1.282	1.612	1.393	1.325	1.346	1.170
AVERAGE Q <sub>av</sub>	1.134	1	1.157	1	1.000	1.016	1.000
MINIMUM Q <sub>mi</sub>	0.839	0.739	0.841	0.727	0.733	0.745	0.745

Location of Measuring Point, and Measuring Date and Time

Circun.: Colector Circunvalacion, Diameter 1.31 meters

Av. Julio Calero 140, Surquillo

1st: from 10:30, May 31 to 10:30, June 1, 1989

2nd: from 8:45, October 19 to 8:30, October 20, 1989

TABLE A15-2 FLOW RATE VARIATION  
(Intake Point No.3 : Surco)

TIME hh : mm	6/06-07	10/24-25	AMOUNT FOR 2 M3/		
	Measured Data	Measured Data	AVERAGE FLOW RATE	FLOW (M3/S)	INTAKE (M3/S)
10 : 00	1.152	1.205	1.179	2.815	2.061
10 : 15	1.182	1.201	1.191	2.845	2.061
10 : 30	1.212	1.201	1.206	2.881	2.061
10 : 45	1.201	1.205	1.203	2.873	2.061
11 : 00	1.122	1.205	1.163	2.778	2.061
11 : 15	1.122	1.159	1.140	2.723	2.061
11 : 30	1.160	1.140	1.150	2.746	2.061
11 : 45	1.160	1.182	1.171	2.796	2.061
12 : 00	1.162	1.211	1.186	2.833	2.061
12 : 15	1.175	1.201	1.188	2.837	2.061
12 : 30	1.150	1.182	1.166	2.785	2.061
12 : 45	1.184	1.180	1.182	2.823	2.061
13 : 00	1.147	1.153	1.150	2.746	2.061
13 : 15	1.186	1.161	1.174	2.803	2.061
13 : 30	1.147	1.180	1.163	2.778	2.061
13 : 45	1.175	1.192	1.184	2.827	2.061
14 : 00	1.147	1.197	1.172	2.798	2.061
14 : 15	1.143	1.167	1.155	2.759	2.061
14 : 30	1.137	1.167	1.152	2.752	2.061
14 : 45	1.139	1.172	1.155	2.759	2.061
15 : 00	1.160	1.159	1.160	2.769	2.061
15 : 15	1.143	1.167	1.155	2.759	2.061
15 : 30	1.133	1.201	1.167	2.787	2.061
15 : 45	1.079	1.178	1.128	2.695	2.061
16 : 00	1.102	1.149	1.126	2.688	2.061
16 : 15	1.112	1.144	1.128	2.694	2.061
16 : 30	1.044	1.149	1.096	2.618	2.061
16 : 45	1.004	1.147	1.075	2.568	2.061
17 : 00	1.063	1.149	1.106	2.641	2.061
17 : 15	1.112	1.125	1.119	2.672	2.061
17 : 30	1.126	1.066	1.096	2.617	2.061
17 : 45	1.114	1.064	1.089	2.600	2.061
18 : 00	1.100	1.062	1.081	2.581	2.061
18 : 15	1.099	1.053	1.076	2.569	2.061
18 : 30	1.085	1.047	1.066	2.545	2.061
18 : 45	1.089	1.064	1.076	2.570	2.061
19 : 00	1.004	1.106	1.055	2.520	2.061
19 : 15	1.004	1.096	1.050	2.507	2.061
19 : 30	1.030	1.064	1.047	2.500	2.061
19 : 45	1.030	1.044	1.037	2.477	2.061
20 : 00	1.028	1.049	1.038	2.479	2.061
20 : 15	1.050	1.036	1.043	2.490	2.061
20 : 30	1.050	0.965	1.007	2.405	2.061
20 : 45	1.018	0.971	0.995	2.375	2.061
21 : 00	1.014	0.975	0.995	2.375	2.061
21 : 15	1.004	0.969	0.987	2.356	2.061
21 : 30	1.004	0.984	0.994	2.374	2.061

TABLE A15-2 FLOW RATE VARIATION  
(Intake Point No.3 : Surco)

TIME hh : mm	6/06-07	10/24-25	AMOUNT FOR 2 M3/		
	Measured Data	Measured Data	AVERAGE FLOW RATE	FLOW (M3/S)	INTAKE (M3/S)
21 : 45	0.982	0.975	0.979	2.337	2.061
22 : 00	0.980	0.965	0.972	2.322	2.061
22 : 15	1.002	0.978	0.990	2.364	2.061
22 : 30	1.000	0.904	0.952	2.274	2.061
22 : 45	0.980	0.859	0.920	2.196	2.061
23 : 00	0.984	0.865	0.925	2.208	2.061
23 : 15	1.004	0.891	0.948	2.263	2.061
23 : 30	0.982	0.883	0.932	2.226	2.061
23 : 45	0.944	0.934	0.939	2.243	2.061
0 : 00	0.944	0.941	0.942	2.251	2.061
0 : 15	0.940	0.889	0.915	2.184	2.061
0 : 30	0.920	0.835	0.878	2.096	2.061
0 : 45	0.890	0.829	0.859	2.052	2.052
1 : 00	0.872	0.853	0.862	2.059	2.059
1 : 15	0.843	0.861	0.852	2.035	2.035
1 : 30	0.843	0.846	0.845	2.017	2.017
1 : 45	0.849	0.859	0.854	2.040	2.040
2 : 00	0.799	0.863	0.831	1.985	1.985
2 : 15	0.803	0.874	0.839	2.003	2.003
2 : 30	0.785	0.881	0.833	1.989	1.989
2 : 45	0.779	0.868	0.823	1.966	1.966
3 : 00	0.785	0.816	0.801	1.912	1.912
3 : 15	0.759	0.698	0.729	1.740	1.740
3 : 30	0.763	0.665	0.714	1.705	1.705
3 : 45	0.763	0.588	0.676	1.613	1.613
4 : 00	0.554	0.594	0.574	1.370	1.370
4 : 15	0.550	0.612	0.581	1.387	1.387
4 : 30	0.591	0.622	0.607	1.449	1.449
4 : 45	0.779	0.648	0.714	1.705	1.705
5 : 00	0.755	0.663	0.709	1.693	1.693
5 : 15	0.763	0.685	0.724	1.730	1.730
5 : 30	0.779	0.673	0.726	1.734	1.734
5 : 45	0.793	0.725	0.759	1.813	1.813
6 : 00	0.793	0.761	0.777	1.855	1.855
6 : 15	0.799	0.769	0.784	1.873	1.873
6 : 30	0.815	0.823	0.819	1.955	1.955
6 : 45	0.829	0.823	0.826	1.972	1.972
7 : 00	0.855	0.868	0.862	2.057	2.057
7 : 15	0.932	0.952	0.942	2.249	2.061
7 : 30	0.964	1.025	0.995	2.375	2.061
7 : 45	1.044	1.057	1.050	2.509	2.061
8 : 00	1.071	1.096	1.083	2.587	2.061
8 : 15	1.114	1.153	1.133	2.707	2.061
8 : 30	1.171	1.159	1.165	2.782	2.061
8 : 45	1.171	1.176	1.174	2.802	2.061
9 : 00	1.173	1.217	1.195	2.854	2.061
9 : 15	1.175	1.209	1.192	2.847	2.061

TABLE A15-2 FLOW RATE VARIATION  
(Intake Point No.3 : Surco)

TIME hh : mm	6/06-07	10/24-25	AMOUNT FOR 2 M3/		
	Measured Data	Measured Data	AVERAGE FLOW RATE	FLOW (M3/S)	INTAKE (M3/S)
9 : 30	1.167	1.215	1.191	2.845	2.061
9 : 45	1.160	1.213	1.187	2.833	2.061
10 : 00	1.152	1.205	1.179	2.815	2.061
MAXIMUM Qmax	1.212	1.217	1.206	2.881	2.061
AVERAGE Qavg	1.000	1.000	1.000	2.388	2.000
MINIMUM Qmin	0.550	0.588	0.574	1.370	1.370



## **APPENDIX 16**

### **SELECTION OF PIPE MATERIALS FOR INVERTED SIPHON**



## APPENDIX 16 SELECTION OF PIPE MATERIALS FOR INVERTED SIPHON

### A16.1 General

The use of inverted siphon structure is cannot be avoided for the transmission of sewage to San Bartolo fully using elevation potential at the intake points due to the topographical feature along the proposed transmission line. However, adoption of such structure in the Project, presents several problems which need to be studied like the long span of inverted siphon section, inner pressure, and difference of elevation between the highest and lowest points. In this Study, optimum materials for pipes are selected taking these problems into consideration.

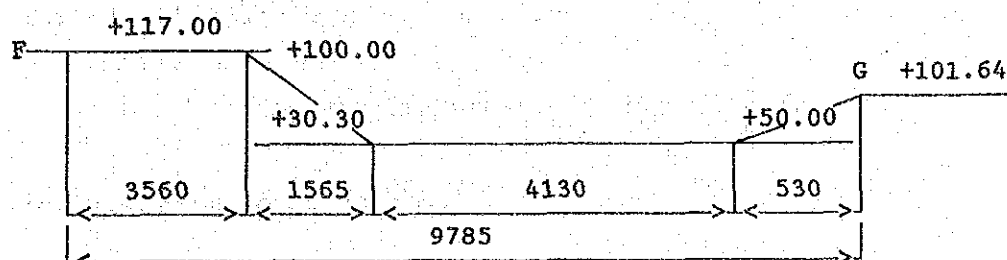
### A16.2 Conditions for Study

Following conditions are set for the Study.

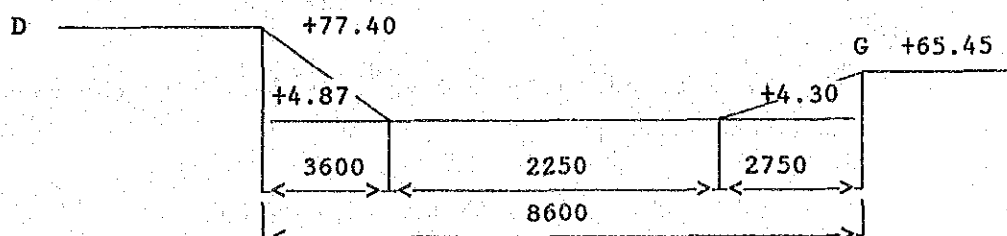
#### (1) Longitudinal Section

In the case of Plan E<sub>1</sub>, the profile of longest inverted siphon will be as illustrated below:

PHASE I  $\phi$  1,350 mm



PHASE II  $\phi$  1,200 mm



(2) Pipe Materials

(a) Pre-stressed Reinforced Concrete Pipe (PCP)

In Peru, PCP have been installed for transmission main pipe of many water supply systems. Highest inner pressure is 18 kg/cm<sup>2</sup>.

(b) Fiber-glass Reinforced Plastic Mortar Pipe (FRPM)

Import from foreign country

(c) Ductile cast Iron Pipe (DCIP)

Import from foreign country.

(3) Soil Condition

(a) Phase I (near Lurin river)

- 1) Total thickness of top soil and alluvial soil is 0.5 m and strata have loose density.
- 2) The layer between GL-2.5 and 3.0 m, which will be the foundation of pipeline consists of gravelly soil. Silty fine sand and medium gravel fine sand strata exist in places. Strata are relatively dense.
- 3) The strata to be excavated consist of gravelly soil with medium density.
- 4) Groundwater exists near Lurin River at elevation 50 m or less. Water level is at 1.0 m below ground level.
- 5) Contents of salinity and sulfate is below the level of concrete structure.

- 6) Permeability of foundation stratum is:

$$K = 7.6 \text{ cm/s}$$

It can be judged as high permeability

- 7) Based on the soil test, mechanical properties of fine sand stratum in this area is judged to be:

Internal friction Angle  $30^\circ$

Cohesion  $0 \text{ kg/cm}^2$

(b) Phase II (along coast line)

- 1) Total thickness of top soil and alluvial soil is 0.5 m and strata have loose density.
- 2) The layer between, GL-2.5 and 3.0 m, which will be the foundation of pipeline consists of medium density fine sand with slight silt contents in place.
- 3) The strata to be excavated consist of medium density fine sand.
- 4) Groundwater exists below elevation 20 m in the south area of the Cerro de Lomo de Corvina. Water level is at 1 m below ground level.
- 5) Concentrations of salinity and sulfate in the soil exceed the durable level for concrete structures from Villa Rica to Lurin River along the Pacific Ocean coast.
- 6) Permeability of foundation strata is:

$$k = 7.8 \times 10^{-3} \text{ cm/s}$$

It is considered normal value for fine sand.

- 7) Based on the soil test, mechanical properties of fine sand strata in this area is judged to be:

Internal friction Angle  $30^{\circ}$   
Cohesion 0 kg/cm<sup>2</sup>

(4) Items to be considered

Following items will be considered for selection of materials:

Characteristics and Strength,  
Anti-corrosion and durability,  
Joint performance,  
Workability, and  
Economy

A16.3 Comparison of Pipe Materials

TABLE A16-1 shows the comparison of characteristics of back pipe materials.

TABLE A16-1 COMPARISON OF PIPE MATERIALS

	Prestressed Reinforced Concrete Pipe (P.C.P.)	Fiber-glass Reinforced Plastic Mortar Pipe (FRPM)	Ductile Cast Iron Pipe (DCIP)
Characteristics and Strength	Strength for External Pressure Structure is designed to bear inner pressure by PC steel bars. Therefore strength against inner pressure is large, but rigidity, flexural strength and strength for external pressure is small.	Both rigidity and flexural strength is large. Strength for external pressure is 150% (more than $\phi 450$ mm) and 200% (less than $\phi 450$ mm) of that of PCP.	Both rigidity and flexural strength is great. Strength for external pressure is greater than that of FRPM.
	Flexural Strength 90~100	1,800~2,000	5,720
	Durable Bending Stress 200,000	125,000~135,000	1,650,000
	Impact Resistance External surface is made of mortar shotcreting. Crack on surface and breaking away of mortar will sometimes occur.	Relatively weak against impact. At the time of backfilling, rapid soil dumping shall be avoided.	Superior against impact. But too large impact breaks away inner mortar lining.
Hydraulic Characteristics	Water-tightness Durable against 6kgf / $m^2$ for $\phi 1350$ to $\phi 1500$	Durable against 10.5kgf / $m^2$ for type II, $\phi 1350$ to $\phi 1500$	Durable against 30kgf / $m^2$ for type III $\phi 1350$ to $\phi 1500$
	Roughness Coefficient (Manning's) $n = 0.013$	$n = 0.010$	$n = 0.013$
	Velocity Coefficient (Hazen-Williams) $C = 130$	$C = 150$	$C = 130$
Anti-corrosion and Durability	Anti-corrosion Weak for acid. Corrosion by hydrogen sulfide generating from sewage and electric corrosion on reinforcing bar sometimes occur.	Durable against acid. Is not affected by corrosive and acidic soil. No problem on electric corrosion.	No problem for normal soil. Coastal soil with high salinity and high acidic soil sometimes cause corrosion. No problem on electric corrosion.
	Durability Much experience in Water Works in Peru. Life is 20 years for rubber rings and more for pipes.	Experiences for several years. In Peru, it was used in Chosica Sewerage Project. Life is estimated about 60 years.	Much experience. Life is 40 years or more for rubber rings and semipermanent for pipes.

TABLE A16-1 COMPARISON OF PIPE MATERIALS - 2

	PCP	FRPM	DCIP
Anti-corrosion and Durability	<p>Accident</p> <p>Break down due to high inner pressure with 15 kgf/m<sup>2</sup> on <math>\phi</math>500 to <math>\phi</math>900mm — 2 cases in Lima southern district</p> <p>Break down due to corrosion with a pressure of 6 to 7 kgf/m<sup>2</sup> on <math>\phi</math>500 to <math>\phi</math>800mm — 2 cases in Lima southern district</p> <p>(refer to APPENDIX 1) (past 3 years)</p>	No report	No report
Joint Performance	Structure of joint	Round type rubber ring	Combined type rubber ring
	Water-tightness	Large durable bending angle and long insert length. Good water-tightness.	Large durable bending angle and long insert length. Superior water-tightness.
	Durable Bending angle	3°00' ~ 6°00'	1°30' ~ 5°00'
	Workability	Easy joint work due to light weight and utilization of puller. Experience in Chosica project proves no leakage.	Easy joint work. But skillful labor is necessary for bolt wrenching of mechanical joint due to necessity of securing equalized specified torque.



TABLE A16-1 COMPARISON OF PIPE MATERIALS - 3

		PCP	FRPM	DCIP
Workability	Weight	1,312.8 kg/m (510%)	275.5 kg/m (100%)	673.3 kg/m (260%)
		1,592.6 kg/m (500%)	320.0 kg/m (100%)	803.7 kg/m (250%)
		5	1	3
	Foundation	Sand or Concrete in accordance with loading condition.	Sand in general.	No specific foundation works.
Work Speed	1350 mm	Work speed — 21.3 m/day Pipe Fitter — 3.15 person per 10 m Labor — 6.84 person (1.00 person/m) Jib Crane 15 t	Work speed — 50.0 m/day Pipe Fitter — 0.40 person per 10 m Labor — 0.80 person (0.12 person/m) Jib Crane 4.8 t	Work speed — 20.8 m/day Pipe Fitter — 2.07 person per 10 m Labor — 2.71 person (1.00 person/m) Jib Crane 15 t
	1500 mm	Work speed — 19.2 m/day Pipe Fitter — 4.03 person per 10 m Labor — 8.87 person (1.29 person/m) Jib Crane 15 t	Work speed — 48.0 m/day Pipe Fitter — 0.42 person per 10 m Labor — 1.04 person (0.15 person/m) Jib Crane 4.8 t	Work speed — 19.2 m/day Pipe Fitter — 2.70 person per 10 m Labor — 3.58 person (0.62 person/m) Jib Crane 15 t

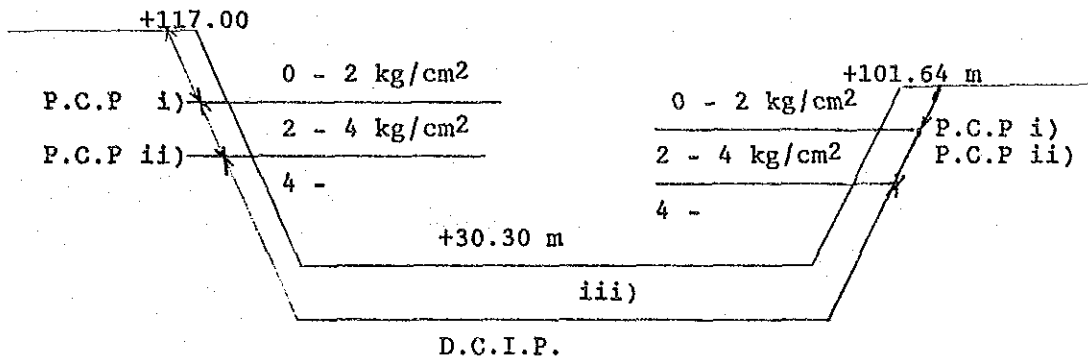
TABLE A16-1 COMPARISON OF PIPE MATERIALS - 4

Currency	PCP			FRPM			DCIP		
	INTIS	US\$	RATIO	¥	US\$	RATIO	¥	US\$	RATIO
ø 1.350	※ 1 4,021,000	692.60	% (100)	※ 2 158,735	1,133.82	※ 3 % (154)	※ 4 145,123	1,036.59	※ 5 % (150)
	—	—	—	COST x 96.65 %	—	—	COST x 110.45 %	—	—
	COST x 15 % 603,150	103.89	—	(COST + Imp. TAX) x 15 % 46,823	1,095.84	—	(COST + Imp. TAX) x 15 % 45,811	1,144.91	—
	TOTAL 4,624,150	796.49	% (100)	358,975	334.45	※ 3 % (322)	351,222	2,508.73	※ 5 % (315)
ø 1.500	5,273,000	908.21	% (100)	192,990	1,378.50	% (152)	175,851	1,256.08	% (138)
	—	—	—	COST x 96.65 %	—	—	COST x 110.45 %	—	—
	790,950	136.23	—	(COST + Imp. TAX) x 15 % 56,927	1,332.32	—	(COST + Imp. TAX) x 15 % 55,511	1,387.34	—
	TOTAL 6,063,950	1,044.44	% (100)	436,442	406.62	—	425,539	3,039.93	% (291)
Remarks	※ 1 Strength for r Inner Pressure 8 kg/m <sup>2</sup> Rate : US\$ \$ 1.00 = I / 5,805.69 US\$ \$ 1.00 = ¥ 140.00	※ 2 Type II Strength for Inner Pressure 8 kg/m <sup>2</sup> Pipe (F08 Yokohama) 92,900 ¥/m Freight, Insurance 65,835 ¥/m 158,735 ¥/m			※ 4 Type II Strength for Inner Pressure 30 kg/m <sup>2</sup> Pipe (F08 Yokohama) 103,000 ¥/m Freight, Insurance 42,123 ¥/m 145,123 ¥/m			※ 5 DCIP — x 100 % PCP	

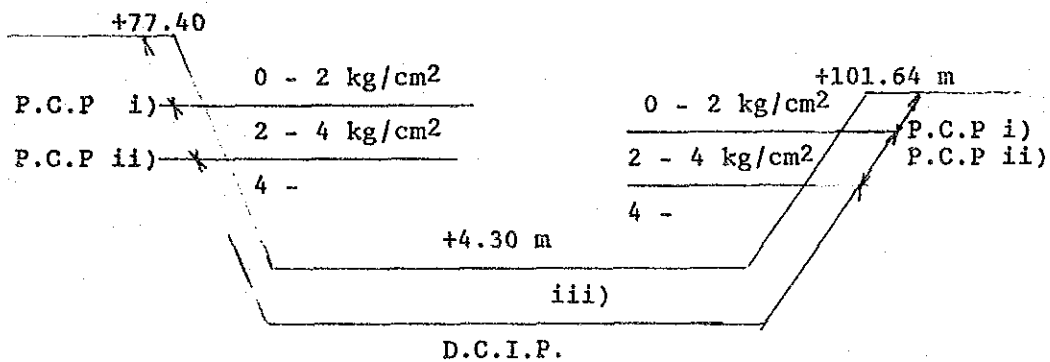
#### A16.4 Conclusion

- (1) Based on the comparison in A16.3, materials of pipes are selected as follows:

Phase I  $\phi$  1,350 mm



Phase II  $\phi$  1,200 mm



- i) Inner Pressure 0 - 2 kg /cm<sup>2</sup> : P.C.P.  
(Durable Inner Pressure 4 kg/cm<sup>2</sup>)
- ii) Inner Pressure 2 - 4 kg /cm<sup>2</sup> : P.C.P.  
(Durable Inner Pressure 6 kg/cm<sup>2</sup>)
- iii) Inner Pressure above 4 kg /cm<sup>2</sup> : P.C.I.P.

(2) Inner Pressure in Inverted Siphon Section (Plan E1)

Phase I

Section	Planned Quantity	Ground Elevation			Max. Static Water Pressure	Pipe Length	Pipe Length by Pressure		
		Upper End	Bottom	Lower End			less than 2 kg/cm <sup>2</sup>	2 - 4 kg/cm <sup>2</sup>	more than 4 kg/cm <sup>2</sup>
B - C	1.0 t/s	146.10	112.00	136.60	34.1	4,047	2,247	1,800	
D - E	2.0	137.00	100.00	129.00	37.0	5,145	3,995	1,150	
F - G	2.0	117.00	30.30	101.64	86.7	9,785	3,685	600	5,500

Phase II

Section	Planned Quantity	Ground Elevation			Max. Static Water Pressure	Pipe Length	Pipe Length by Pressure		
		Upper End	Bottom	Lower End			less than 2 kg/cm <sup>2</sup>	2 - 4 kg/cm <sup>2</sup>	more than 4 kg/cm <sup>2</sup>
A - B	2.0 t/s	92.39	76.00	85.73	16.4	3,350	3,350		
D - E	1.5	77.40		4.87		3,600	1,000	800	1,800
E - F	1.5	4.87	4.30	4.30	73.1	2,250			2,250
F - G	1.5	4.30		65.45		2,750	400	200	2,150
H - I	1.5	57.60	19.00	53.34	38.6	2,500	1,000	1,000	500

## **APPENDIX 17**

### **ACCIDENT OF PRESTRESSED CONCRETE PIPE**



## APPENDIX 17      ACCIDENT OF PRESTRESSED CONCRETE PIPE

SEDAPAL has been installing prestressed concrete pipes for inner-pressure pipeline, for water supply networks. Past records of installation and repair of pipeline using prestressed concrete pipes are summed up by SEDAPAL as shown in TABLE A17-1.

According to the table, the total length of installed prestressed concrete pipes is 63,100 meters. Out of those a length of 125 meters had been replaced due to breakage suspected to be caused by corrosion, electrical corrosion and excessive pressure. The replaced length is about 0.2 % of the total length.

Breakdown of broken pipes by cause is as follows:

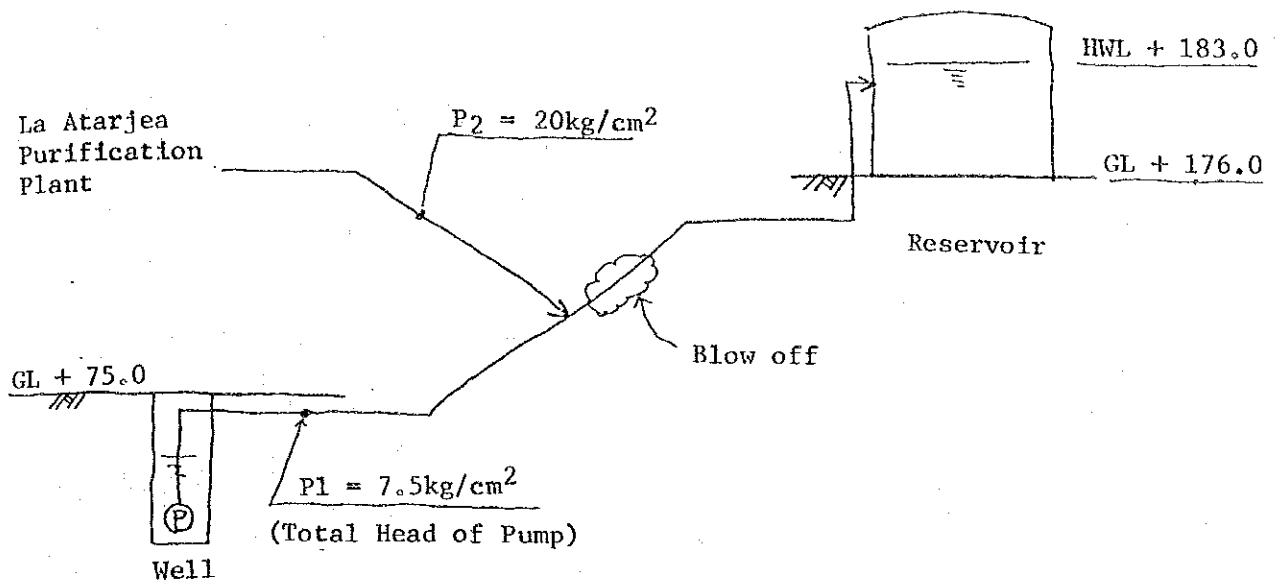
Total length of installed pipes	63,100 m
Total length of repaired pipes	125 m (6 cases)
Cause : Corrosion	100 m (3 cases)
Electrical Corrosion	10 m (1 case)
Excessive Pressure	15 m (2 cases)

Breakages of prestressed concrete pipes had been occurring at high rate even at present. Such broken pipes were installed with no corrosion protection measure nor were they provided with such protection after they had been installed. Pipelines provided with corrosion protection measure have not been damaged by corrosion. According to the staff of SEDAPAL, it has become a common practice to provide corrosion protection measure at the same time the pipe is installed. FIGURES A17-1 to A17-3 show typical breakage cases.

**TABIE A17-1**

INSTALACION INSTALLATION										REPARACIONES REPAIR				
Ubicación LOCATION	F E C H A DATE		ESPECIFICACIONES STEC.			Fabricante de los TUBERIOS MAKER	Presión de Trabajo	Ubicación LOCATION	Fecha Reparac. DATE	Long mt LENGTH	Presión al mont. de rotura	observaciones Observations		
	PIPE Tubería	C. Protección Sis. Prot. Cat.	Long ft Long (mt)	Presión de Diseño (Atm)	" Design Press.									
Atarjea - Rímac	82 - 04	82 - 04	64" - 14"	6-17 Atm	12,600	Super-Concret.	0-10 Atm	(Hasta la fecha,	ninguna	rotura)	Atm.			
Atarjea- San Juan de Miraflores(Proceres)	75 - 08	-	72" - 36"	3-15 "	14,000	Super-Concret.	0-14 "	" "	"	"	Pressure at Breachage			
Proceres - Villor S.	80 - 07	84 - 01	24"	17-20 "	7,500	Super-Concret.	8-12-0 "	Poa. Zonal Huayna	11 rotur.	50 m.	12	Corros. Avanz.		
Proceres - CR4	80 - 07	84 - 01	24"	17-20 "	6,000	Super-Concret.	2-6-0 "	Copac-S M. Sn. J. de Miraflores	Del 83-86 2 rotur. Del 87-86	10 m.	7	Corros. Avanz. se modif. proyecto presión actual		
CR4 - Villa Salvod.	85 - 02	85 - 02	20"	15-10 "	1,500	Super-Concret.	0-9 "	Vill. El Salvador	88 -03	5 m.	15	5 atm. Electric Corrosion		
Villa Salvador (cir- cuito)	- -	-	24"	15 "	5,100	Super-Concret.	4-8 "	"	87 -05	10 m.	15	Sobr. presión Excesiva Rinsure		
Proceres-Reser-2000	72 - 09	-	24" - 20"	18 - 07 "	4,500	Super-Concret.	14-0 "	Sn. J. de Miraflores	< 1980 2 roturas	10 m.	20	Corros. Avanz. Corrosion		
Argamas - Surquillo	80 - 09	80 - 09	26" - 20"	10 "	7,000	Super-Concret.	4-6 "	(Hasta la fecha,	ninguna	rotura)				
Buenos Aires-Colloco	75 - 05	75 - 05	24"	10 "	1,000	Super-Concret.	4-5 "	" "	"	"				
Zorote -C. Grande	83 - 07	85 - 01	32"	15 "	3,900	Super-Concret.	0-5 "	Av. Proc. de Indep.	6 roturas. Del 84-89	40 m.	6	Corros. Avanz. Corrosion		
										OCTUBRE 31, 1989.				





Change of main transmission line from the existing well pump line ( $P_1$ ) to the line from Atarjea ( $P_2$ ) caused breakage due to excessive pressure.

FIGURE A17-1 BREAKAGE BY EXCESSIVE PRESSURE  
(Proceres - Reser 2000)

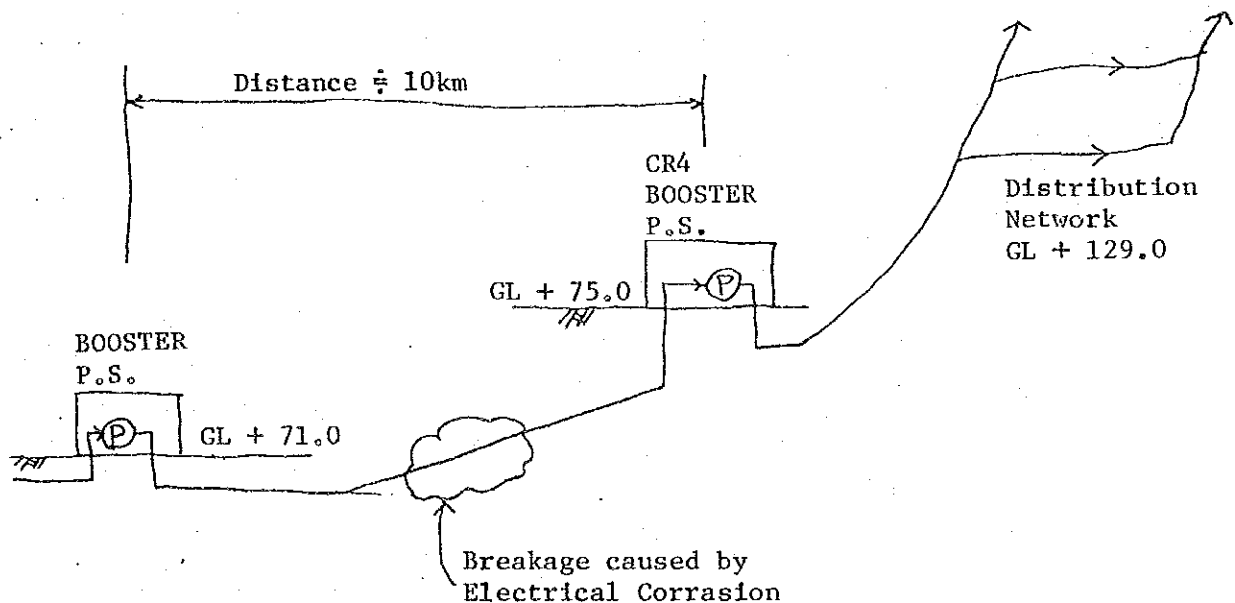
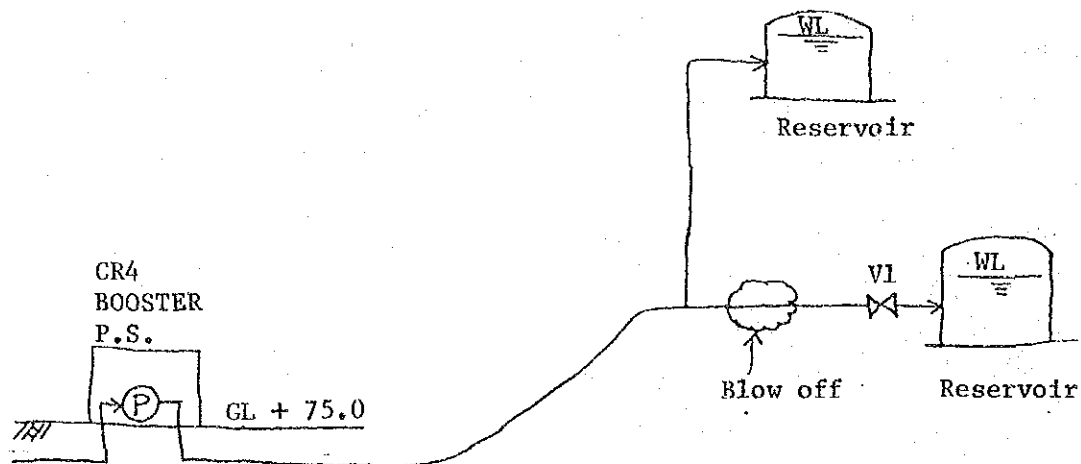


FIGURE A17-2 BREAKAGE BY ELECTRICAL CORROSION  
(Proceres - CR4)



When the booster pump was started at the time that the inlet valve of reservoir closed, increase of inner pressure broke the pipe.

FIGURE A17-3 BREAKAGE BY EXCESSIVE PRESSURE  
(CR4 - Villa El Salvador)

## **APPENDIX 18**

### **FITTINGS AND SMALL STRUCTURES FOR TRANSMISSION LINE**



## APPENDIX 18      FITTINGS AND SMALL STRUCTURES FOR TRANSMISSION LINE

Various small structures are necessary in pipeline construction. The following typical drawings show the concept of such structures.

FIGURE A18-1	Inlet Chamber for Inverted Siphon
FIGURE A18-2	Standard Type of Manhole
FIGURE A18-3	Air Valve Box
FIGURE A18-4	Inspection Manhole (Pressure Manhole)
FIGURE A18-5	Plan of Drain (Blow Off Valve)
FIGURE A18-6	Rio Lurin Underpass (Phase I)

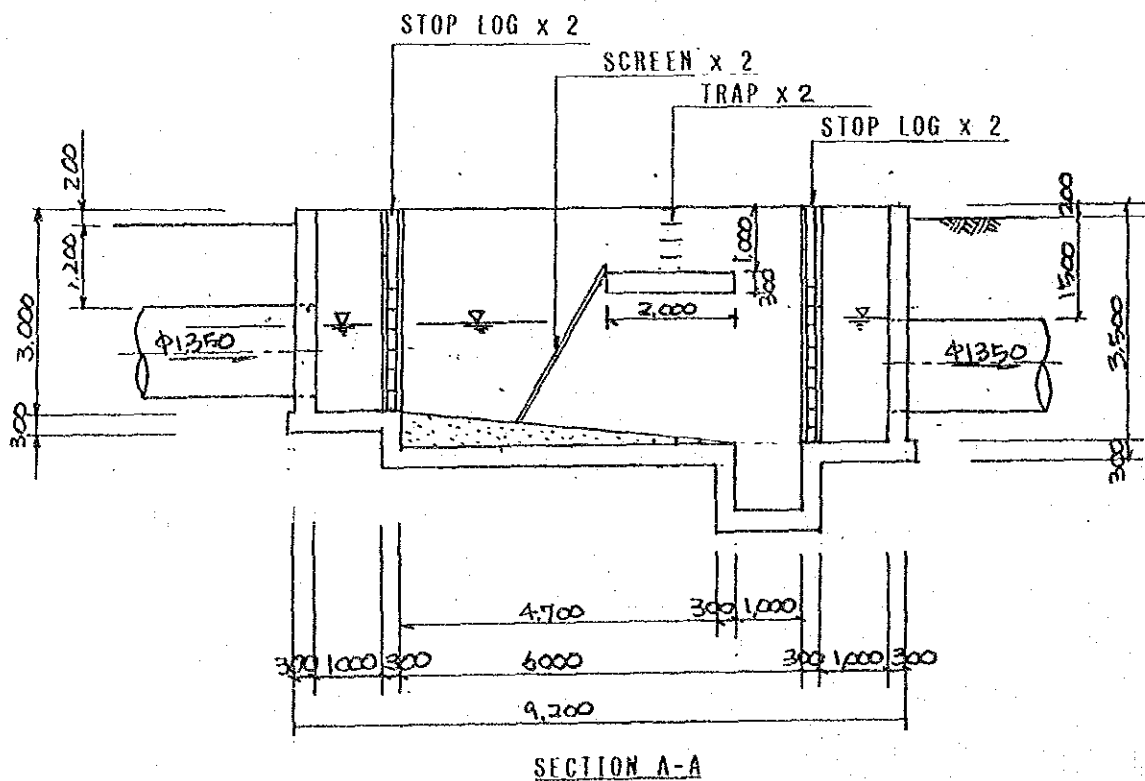
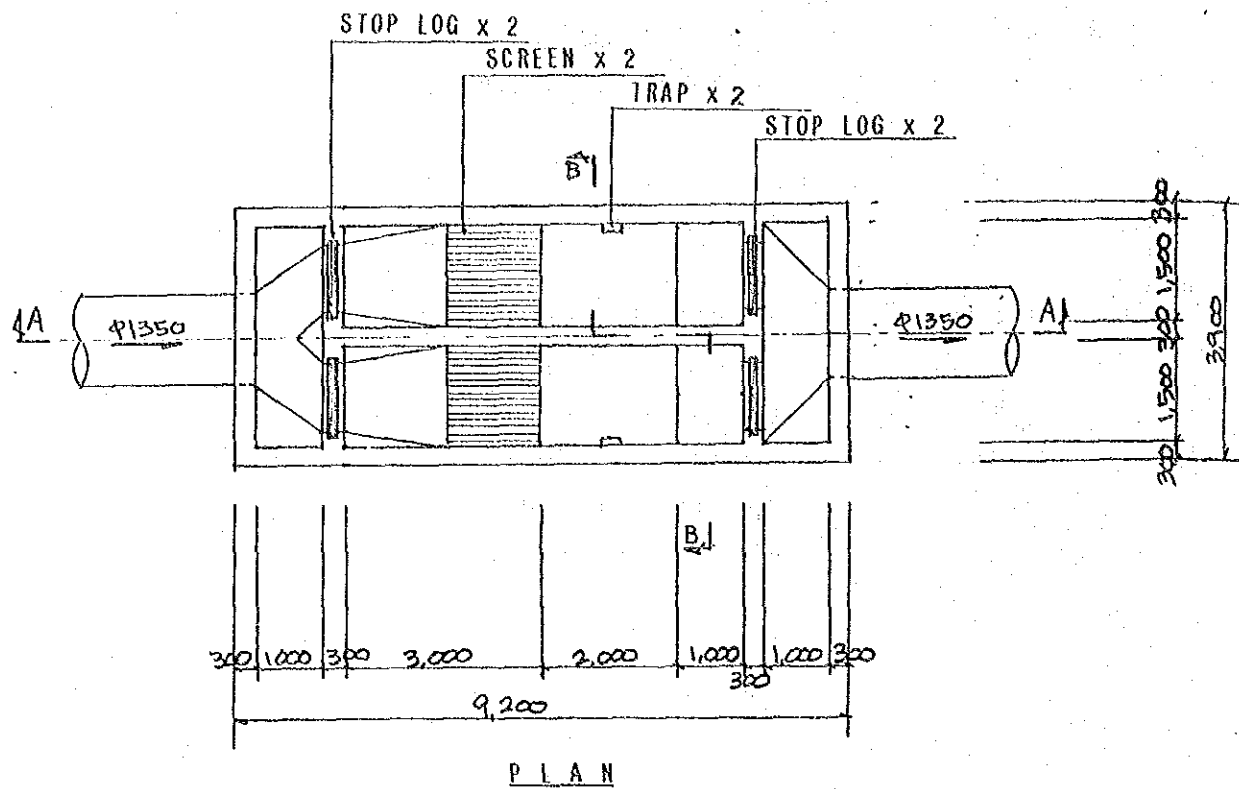


FIGURE A18-1 Inlet Chamber for Inverted Siphon

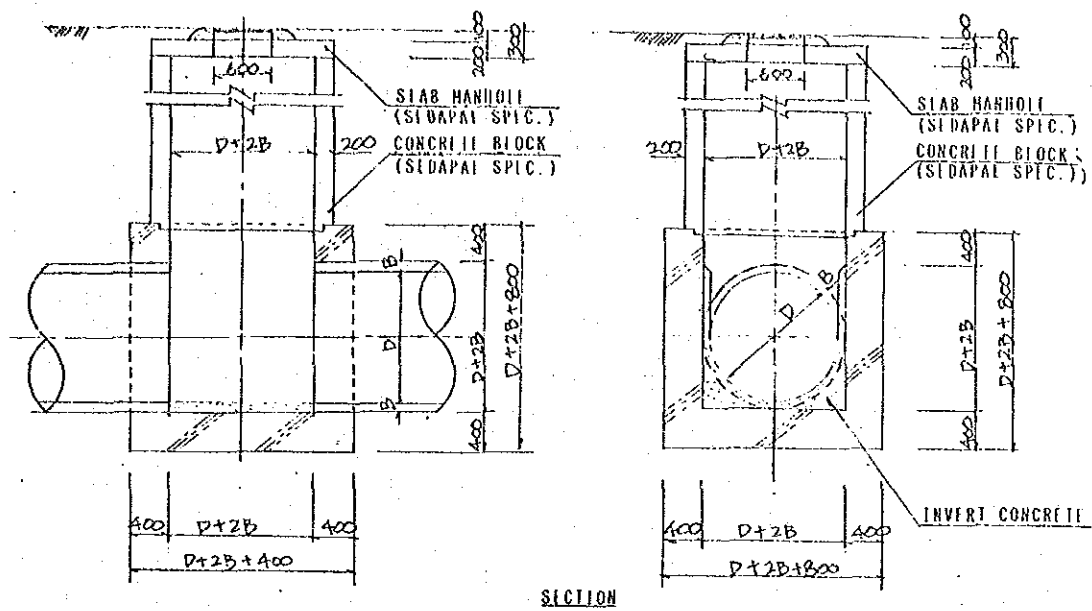


FIGURE A18-2 Standard Type of Manhole

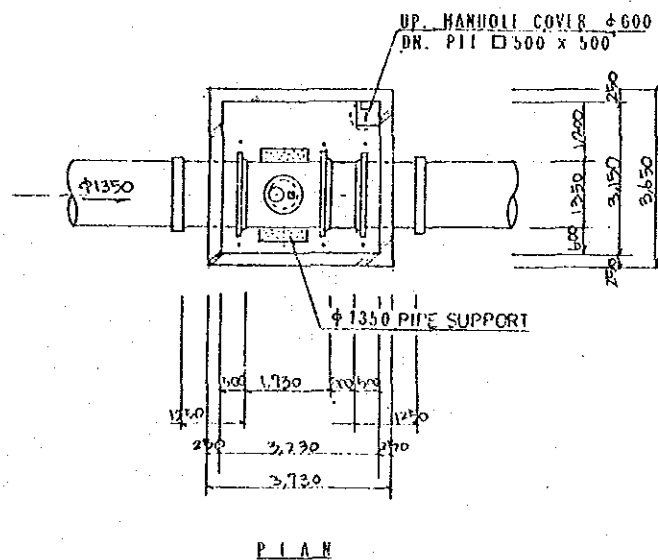


FIGURE A18-3 Air Valve Box

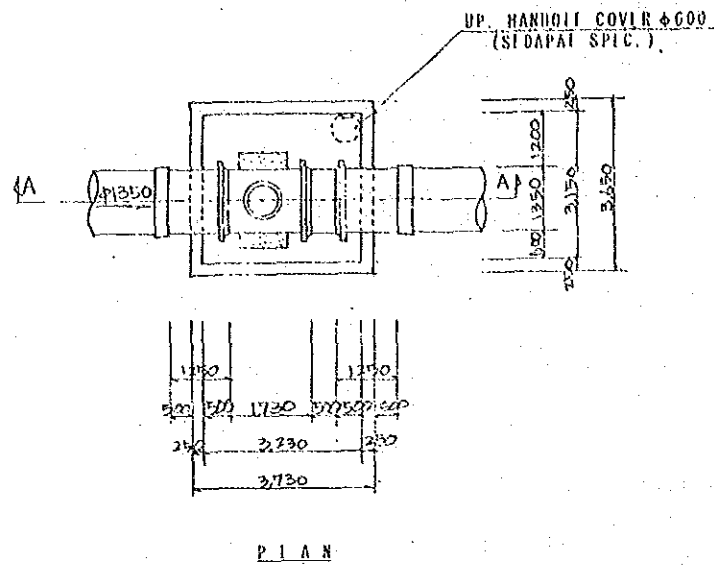


FIGURE A18-4 Inspection Manhole (Pressure Manhole)

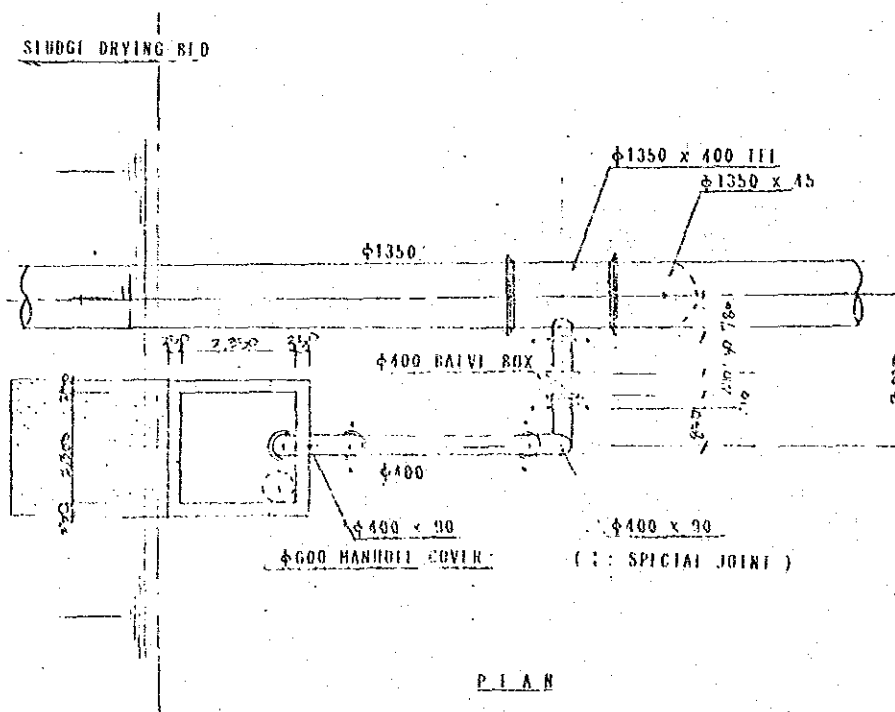


FIGURE A18-5 Plan of Drain (Blow Off Valve)



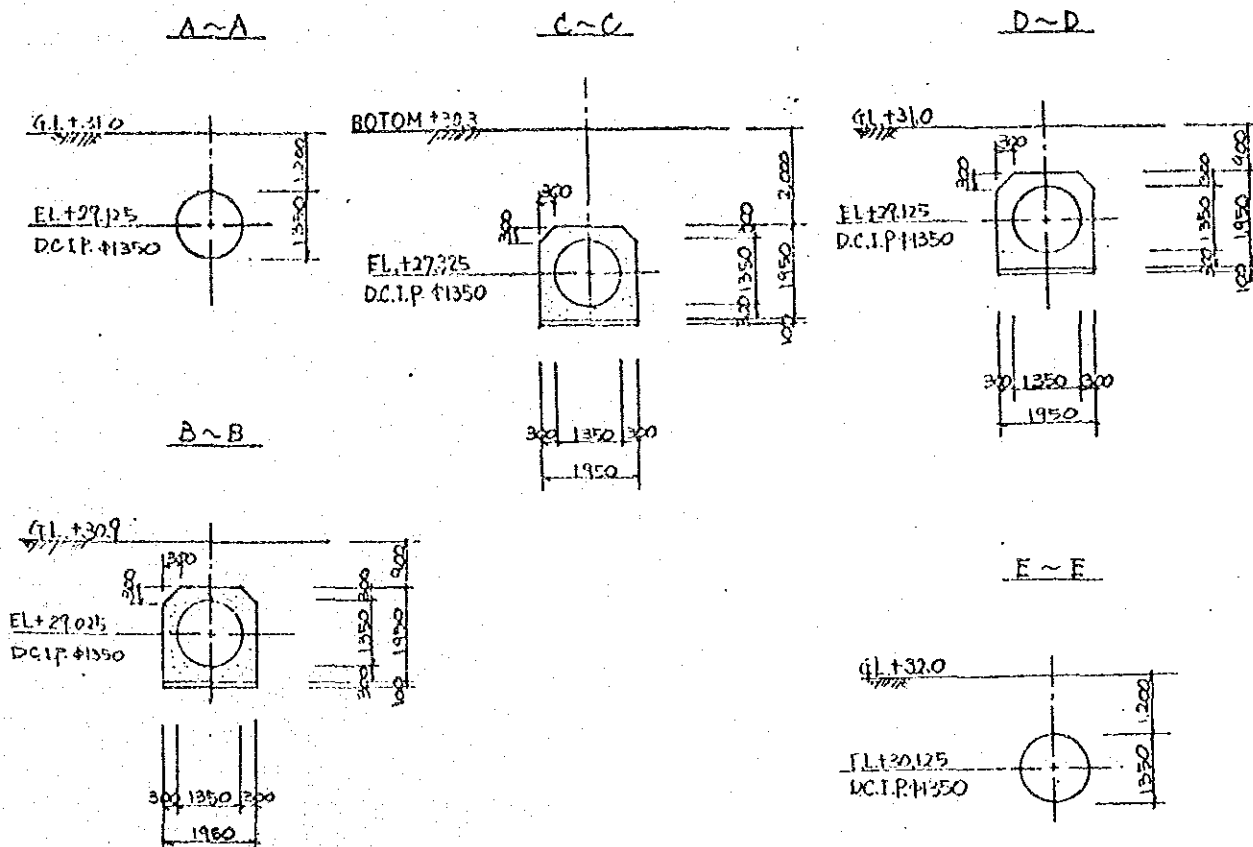
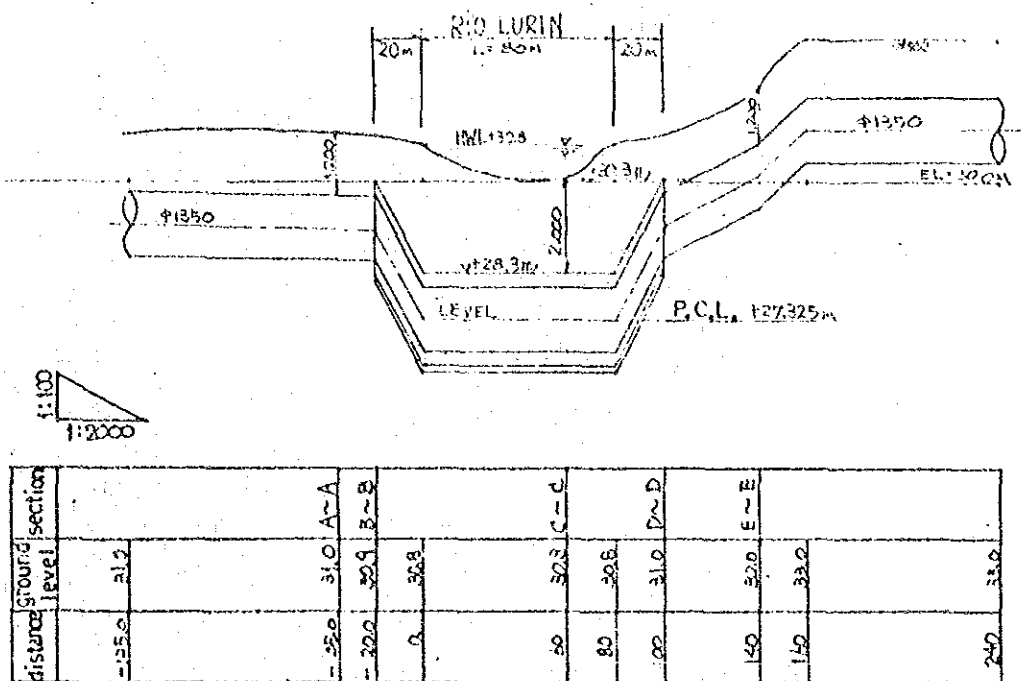


FIGURE A18-6 Rio Lurin Underpass (Phase I)

