THE FINAL REPORT FOR THE FEASIBILITY STUDY ON EFFECTIVE UTILIZATION OF BANKO COAL IN THE REPUBLIC OF INDONESIA

ATTACHMENT

March 1989

JAPAN INTERNATIONAL COOPERATION AGENCY

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PREFACE

In response to a request from the Government of the Republic of Indonesia, the Japanese Government decided to conduct a feasibility study on Effective Utilization of Banko Coal and entrusted the study to the Japan International Cooperation Agency (JICA).

JICA has sent to Indonesia a study team headed by Mr. Takehiko Sato, the Institute of Energy Economics, Japan, as many as eighteen times during the period of five years from May 9, 1984 to December 20, 1988.

The team has had a series of discussions with concerned officials of the Government of the Republic of Indonesia, and conducted field surveys, gasification tests, and so on. After the team returned to Japan, further studies were made and the present report was prepared.

I hope that this report will contribute to the development of the project and to the promotion of friendly relations between our two countries.

I wish to express my sincerest appreciation to the concerned officials of the Government of the Republic of Indonesia for their close cooperation extended to the team.

March, 1989

Kensuke Yanagiya

President

Japan International Cooperation Agency

THE FINAL REPORT FOR THE FEASIBILITY STUDY

ON

EFFECTIVE UTILIZATION OF BANKO COAL IN THE REPUBLIC OF INDONESIA

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ATTACHMENT 5-5

 A Study on Introduceable Quantity of Fuel Methanol in Indonesia
 (Evaluation and Analysis by Using LP model)

 A Study on Introduceable Quantity of Fuel Methanol in Indonesia
 (Evaluation and Analysis by Using LP model)

1. OUTLINE OF STUDY

This survey is aimed at quantitatively evaluating and analysing, in the "Effective Utilization of Banko Coal," the impacts of introducing fuel methanol into Indonesia as a substitute fuel for various oil products.

In the study, an LP model (linear programming model), which represents the crude oil and oil-product flows in Indonesia, has been prepared and used.

The presence or absence of economic benefits obtained by introducing fuel methanol into Indonesia may be determined by the difference in magnitude between the cost for introduction (namely, methanol price) and the increase in profits obtainable from the increase in the export of crude oil and oil products, etc.

In this study, the methanol introduction is evaluated by profit difference between base case (without methanol introduction) and methanol introduction cases.

2. CONSTRUCTION OF LP MODEL

2-1 Outline

The LP model used in the present survey consists of matrices comprising about 2,000 equations and about 3,500 variables. Table 1 shows the main matrices; Fig. 1 and 2 show the entire flow charts.

Matrices are composed of such parts as crude oil production, oil refining, demand location and methanol production.

Object functions are defined as profit functions, and optimization has been performed to maximize the profits.

2-2 Crude Oil

For the crude oil produced, the following six kinds of oil have been set up; and other crude oils have been included into the six crude oils according to their respective production areas:

Sumatra Light (SL)
Arjuna (AJ)
Attaka (AT)
Bekapai (BP)
Handil (HD)
Arun Condensate (AC)

The contents of inputs for the respective crude oil are as follows:

Upper limit of production

Production cost per kl (\$/kl)

Transportation cost to one of four refineries (\$/k1)

Export price (FOB: \$/kl)

Since the object functions are profit functions, the sign for the object function is minus in respect to the cost. Namely, production and transportation (domestic use) of crude oil decrease profits. Conversely, the sign of the export price for the object function is plus, and the export of crude oil and oil products will earn profit.

A quantitative balance shall be obtained by the following:

Crude oil production - Crude oil export - Domestic transportation of crude oil (Domestic consumption) = 0

Part of the crude oil production is transported to a domestic refinery, and the remainder is exported. Provided that it has been assumed that the total production of the Arun Condensate will be exported, and the upper limit of this export has been set up. Natural gas also has a set-up upper limit for export, and is used at the Balikpapan refinery for manufacturing hydrogen. For producing lubricants, it has been assumed that Arabian Light (AL) will be imported and processed at Cilacap.

2-3 Refineries

At present, there are nine refineries in Indonesia, but in the model, refineries which are in adjacent areas are grouped, and all Indonesian refineries are represented by the following four refineries:

"Refining capacity" is the total capacity of the respective grouped refineries.

The topper yield of crude oil and yields of respective refinery facilities, unit consumptions, etc., have been set up on the basis of data obtained by the site survey, and the validity of these data has been confirmed by comparing them with the actual data of oil refining in 1985.

For each refinery facility, the following data have been inputted.

Processing capacity (1,000 kg/y)
Material balance
Home-use fuel consumption
Hydrogen balance
Steam consumption
Electric power consumption
Catalysts and chemical costs

Of the above items, home-use fuel, hydrogen, steam and electric power are all provided by the refinery, and catalysts and chemicals will be purchased.

For product blending, the following restrictions have been posed.

Gasoline

Research octane number (RON) 84 (clear) or above

50% dist. temp.

88°C or above

Reid vapor pressure (R.V.P.)

9 psi or above

Gas oil

Kinetic viscosity (100°F)

1.6 cSt or above

10% carbon residue

0.1% or above

Cetane index

48 or above

Heavy oil

Kinetic viscosity (100°F)

1.250 sec or below (Redwood)

Carbon residue

10% or below

Quantity balances at the refinery are as follows:

Domestic crude oil transported - Topper crude-runs = 0

Finished-product production - Domestic product transportation - Product export

= 0

Blending stock and unfinished product balance in the refinery

It has been assumed that the finished products are transported to domestic demand regions and the remainder is exported.

The domestic transportation cost of products has been set up on the basis of the marine transportation distance from the refinery to the demand region concerned. Land transportation costs have been omitted, because they do not affect variation in profits among the various cases.

2-4 Domestic Demand

Domestic demand has been divided into eight regions according to the sales units of PERTAMINA.

Demand Region 1 Acheh, Riau, North Sumatra, West Sumatra and their

surrounding areas

Demand Region 2 Jambi, South Sumatra, West Sumatra and their surrounding

areas

Demand Region 3 Jakarta, West Java and their surrounding area

Demand Region 4 Central Java, Jogyakarta and their surrounding areas

Demand Region 5 East Java, Bali, Madura and their surrounding area

Demand Region 6 South Sulawesi, Central Sulawesi and their surrounding area

Demand Region 7 North Sulawesi, South East Sulawesi, Maluku and their

surrounding area

Demand Region 8 Irian Jaya and its surrounding areas

For each product at each demand region, the following data are inputted:

Demand quantity

Sales price

The quantitative balance is as follows:

Domestic transportation of products from 4 refineries - Demand at demand area concerned = 0

Thus, products transported from the refinery are sold at the demand region and earn profits.

Table 1 Main Matrix of LP Model

	(Type)	= Max,		0		: O	0 11	10	0	3		< Cape.	0 21		V	۸		· 0	o li	ø		Ö	
	Methanol Production	- Production Cost														-						+-	Production Level
	Methanol Trans. portation	Trans- portation Cost	·																	+		ı ·	
	Domestic Demand	+ Salos Price									٠.							-	ı	ı			Demand Lavel
	Products trans- portation	- Trans- portation Cost						- :	-	1									+				
	Oil Products Export	+ Export Price								'									:	:			
	Oil Products								í	4					!	ı							Product Specifi- cation
eries	Bleading	- 1						•	+	٠.					+ ,	+	:						
Refineries	Refining Voit	- Refining Cost					ı	+	•			+	1							-			Processing Capacity
	Refining Unit	- Refining Cost				•	+					+	1										Processing Capacity
	Crude Oil Input					+	•											ı		٠			
	Domestic Trans- portation	- Trans. portation Cost		1		•												+					
Crude Oil	Export	+ Export Price		1																			Exports Level
	Production	Production Cost		+																			Production Lavel
	Structural Variables Equation	Objective Punction (Profit)	Crude Oil Volume Balance	Crude Oil Volume	Material Balance in Refineries	Material Balance I	Material Balance 2	Unfinished Products	Oil Product Production	Oil Product Delivered	Refining Unit	Processed Volume	Own use	Product Specification	Max.	Min.	Balance of Transported Volume	Crude Oil	Oil Products	Methanol	Methanol	Methanol Production	Constraint Conditions

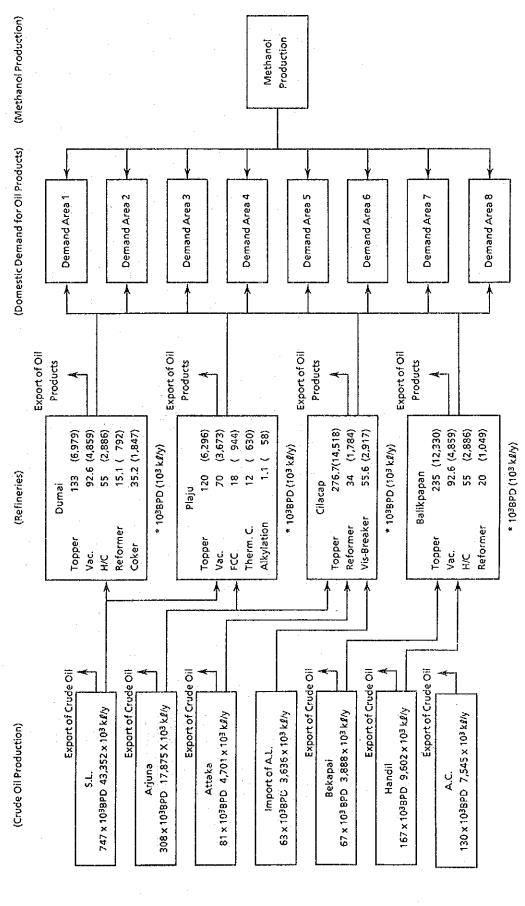


Fig. 1 Flow of LP Model in Indonesia (Existing Capacity Case)

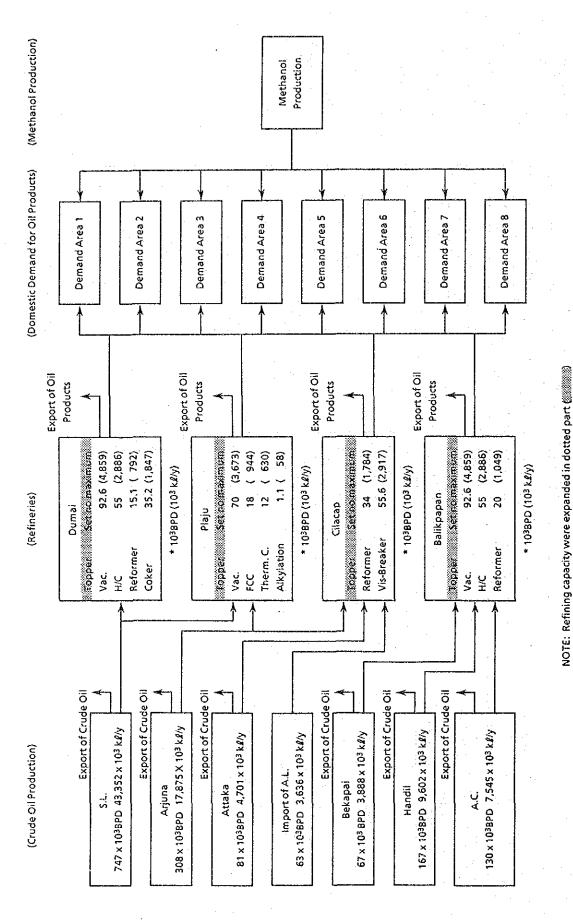


Fig. 2 Flow of LP Model in Indonesia (Expanded Capacity Case)

3. MAJOR CONDITIONS FOR CALCULATION

3-1 Scenario

The demand forecast of petroleum products in Indonesia is defined based on the BPPT study. It is shown in the Table 3.

The price of crude oil and petroleum products are forecast by each scenario as OPEC average crude oil price. 155\$/t, 165\$/t and 175\$/t are used as methanol price. The basic case for calculation is the case when fuel methanol are not introduced. In this case, petroleum products import are needed, for they can not supply in the existing refining capacity. Then as methanol introduction case, three different oil price are defined. As a reference, the expansion of topper unit in four refineries are calculated.

3-2 Crude Oil

3-2-1 Production Ceiling

SL	$747 \times 10^3 \text{ BPD}$	$43,352\times10^3~\text{k}?$
AJ	$308 \times 10^3 \text{ BPD}$	$17,875 \times 10^3 \text{ kg}$
AT	$81 \times 10^3 \text{ BPD}$	$4,701 \times 10^3 \text{ kg}$
BP	$67 \times 10^3 \text{ BPD}$	$3,888 \times 10^3 \text{ kg}$
HD	$167 \times 10^3 \text{ BPD}$	$9,692 \times 10^3 \text{ kg}$
AC	$130 \times 10^3 \text{ BPD}$	$7,545 \times 10^3 \text{ kg}$
Total	$1,500\times10^3~\mathrm{BPD}$	$87,053 \times 10^3 \text{ kg}$

3-2-2 Production Cost

SL	\$1.86/bbl	\$11.7/kg
AJ	\$9.01/bbl	\$56.7/kg
AT	\$10.49/bbl	\$66.0/kg
BP	\$4.73/bbl	\$29.7/kg
HD	\$4.50/bbl	\$28.3/kg
AC	\$1.86/bbl	\$11.7/kg

3-2-3 Transportation Cost

Wt. Av. in total Indonesia:\$3.05/kg (\$0.006/km-kg)

	Dumai	Plaju	Cilacap	Balikpapan
SL	0.0	4.32		
AJ		4.50	4.50	
AT	 -	· —	9.72	******
BP			*******	0.0
HD				0.0
AC		-	_	
AL			8.00	

The number of \$0.006/km·kl was calculated based upon wt.av. transportation cost of \$3.05/kl.

3-2-4 Export Volume

Production volume - processing volume.

3-2-5 Export Price

SL Ave. Crude Oil Price in OPEC + 0.5\$/bbl

AJ Ave. Crude Oil Price in OPEC + 1.0\$/bbl

AT Ave. Crude Oil Price in OPEC + 1.3\$/bbl

BP Ave. Crude Oil Price in OPEC + 1.3\$/bbl

HD Ave. Crude Oil Price in OPEC + 1.0\$/bbl

AC Ave. Crude Oil Price In OPEC + 1.1\$/bbl

3-2-6 Import Volume of AL

 $3,636 \times 10^3$ kg (400×10^3 of Lub demand and 11% of its yield were assumed.)

3-2-7 Import Price of AL

The price was assumed to be the same of Ave. Price of OPEC crude oil.

3-3 Oil Refining

3-3-1 Processing Capacity by Refineries

				103 kl/y
	Dumai	Plaju	Cilacap	Balikpapan
Topper	6,979	6,000	14,518	12,330
Vacuum	4,859	3,673	0	4,859
Reformer	792	0	1,784	1,049
FCC	0	944	0	. 0
Alkylation	0	58	0	0
H/C	2,886	0	0	2,886
Coker	1,847	0	0	0
Visbreaker	0	0	2,917	0

The following capacities were assumed as added refining capacities.

103 kg/y

	Dumai	Plaju	Cilacap	Balikpapan
Topper	No upper limit	No upper limit	No upper limit	No upper limit
Vacuum	4,859	3,673	0 :	4,859
Reformer	792	0 .	1,784	1,049
FCC	0	944	· · · · · · · · · · · · · · · · · · ·	4.5 m - 1.0 m - 1.0
Alkylation	0	58	0	. 0
H/C	2,886	0	. 0 ,	2,886
Coker	1,847	0	0	0
Visbreaker	0	0	2,917	0

3-3-2 Crude Oil Processed in Each Refinery

	Dumai	Plaju	Cilacap	Balikpapan
SL	0	0		<u> </u>
AJ	_	O	Ö	·
AT		_	0	
BP				О
HD			aurent.	0
AC				
\mathbf{AL}			0	

3-4 Demand for Petroleum Product

3-4-1 Petroleum Products Demand by Regions

The two demand scenarios of high and low are set for 2000, 2005 and 2010.

3-4-2 Domestic Sales Price of the Petroleum Products

(Av. Price of OPEC crude oil \times 1.05 + 6.95) \$/kl (5% is refining cost + 6.95 of ave. transportation cost)

3-4-3 Transportation Cost of Petroleum Products of Crude Oil Price

\$6.95/kg (\$0.014/km·kg)

	Dumai	Plaju	Cilacap	Balikpapan
Demand Region 1	5.60	15.40	32.20	
Demand Region 2	10.50	0.00	17.50	25.90
Demand Region 3	18.90	7.70	0.00	21.00
Demand Region 4	21.00	11.62	0.00	16.10
Demand Region 5	25.20	15.40	0.60	12.60
Demand Region 6	30.10	32.90	21.00	7.84
Demand Region 7		#X###	37.10	13.58
Demand Region 8				35.00

The number of \$0.014/km·k@ was calculated based on wt.av. transportation cost of \$6.95/k@.

3-4-4 Export Price of Products

Export prices are assumed from market prices of 1985 in Singapore.

Naphtha: Ave. Crude Oil Price of OPEC × 1.0 Kerosene: Ave. Crude Oil Price of OPEC × 1.2 Gas Oil: Ave. Crude Oil Price of OPEC × 1.2 Reformate: Ave. Crude Oil Price of OPEC × 1.3 Fuel Oil: Ave. Crude Oil Price of OPEC × 0.9

3-4-5 Import Price of Products

Gasoline: Ave. Crude Oil Price of OPEC × 1.2 + 40

Kerosene: Ave. Crude Oil Price of OPEC × 1.2 + 40

Gas Oil : Ave. Crude Oil Price of OPEC × 1.2 + 40

3-5 Cases for Introducing Methanol

3-5-1 Production Area

South Sumatra

3-5-2 Production Volume

No upper limit (Gr. 0.796)

3-5-3 Methanol Sales Price at Palembang

175\$/t, 165\$/t, 155\$/t

3-5-4 Introducing Area

One half of kerosene demand of each region was assumed to be max. for methanol demand.

As to introduction of methanol for gasoline, market and diesel oil, demand region 3 and 5 are selected because of their bigger shares in total. (without ceiling of introducing volume)

3-5-5 Substituting Volume of Petroleum Products by Methanol

Gasoline: 0.52 kl/1 kl of methanol

Kerosene: 0.49

ADO : 0.47

(calorific equivalent base)

3-5-6 Transportation Cost

The same cost in the case of petroleum product (cost per/unit volume) was assumed for this.

Table 2 The Investigation Case

Scenario		Year	Domestic demand	OPEC average crude oil price	Methanol price	
High scenario 2000	2000		Ref. Table-3	28\$/b51	No introduction	Base case (no introduction of fuel methanol)
→	→		→	→	175\$/t	Introduction case in 175\$/t (no import of petroleum products)
↑	^		→	→	165\$/t	Introduction case in 165\$/t (no import of petroleum products)
→	^		>	1	155\$/t	Introduction case in 155\$/t (no import of petroleum products)
→	->		->	7	No introduction	Refinery expansion cae (Topper) (no introduction of fuel methanol)
\$ 2002	2005		>	36\$/bb1	No introduction	Base case (no introduction of fuel methanol)
→	->	_	→	→	. 175\$/t	Introduction case in 1758/t (no import of petroleum products)
↑			>	→	165\$/t	Introduction case in 165\$/t (no import of petroleum products)
→	→		→	→	155\$/t	Introduction case in 155\$/t (no import of petroleum products)
7	1	_	1	→	No introduction	Refinery expansion cae (Topper) (introduction of fuel methanol)
1 2010	2010		>	453/65[No introduction	Base case (no introduction of fuel methanol)
→	→		- →	→	175\$/t	Introduction case in 1758/t (no import of petroleum products)
	->		>		165\$/t	Introduction case in 165\$/t (no import of petroleum products)
7	•	,		→	155\$/t	Introduction case in 155\$/t (no import of petroleum products)
→	^			↑	No introduction	Refinery expansion cae (Topper) (introduction of fuel methanol)
Low scenario 2000	2000	→	.	21\$/561	No introduction	Base case (no introduction of fuel methanol)
↑	↑	→		↑	175\$/t	Introduction case in 175\$/t (no import of petroleum products)
→	→			→]	165\$/t	Introduction case in 165\$/t (no import of petroleum products)
<i>→</i>	→	→		→	155%t	Introduction case in 155\$/t (no import of petroleum products)
↑ 2002 ↑	2005	→		25\$/bbl	No introduction	Base case (no introduction of fuel methanol)
→	→	→		>	175\$/t	Introduction case in 1/5\$/t (no import of petroleum products)
→ →	→	→		·>	165\$/t	Introduction case in 1658/t (no import of petroleum products)
→	→	→		->	155\$/t	Introduction case in 155\$/t (no import of petroleum products)
2010	2010	→		29\$/bbi	No introduction	Base case (no introduction of fuel methanol)
→	→			→	175\$/t	Introduction case in 175\$/t (no import of petroleum products)
→	→			→	165\$/t	Introduction case in 175\$/t (no import of petroleum products)
→	-				155\$/t	Introduction case in 175\$/t (no import of petroleum products)
High scenario 2000	↑ 0002	→		32~37 \$/bbl	1753/t	Analysis of the amount of methanol introduced when the oil price is changed from 32\$/bbl to 37\$/bbl in case 175\$/t of methanol price.
→	→		→	29~35 \$/bbl	165\$/t	Analysis of the amount of methanol introduced when the oil price is changed from 29\$/bbl to 35\$/bbl in case 165\$/t of methanol price.
→	→		→	28~33 \$/bbi	155\$/t	Analysis of the amount of methanol introduced when the oil price is changed from 288/bbi to 33\$/bbi in case 1558/t of methanol price.

Table 3 Domestic Demand for Petroleum Products

H Scenario					٠.	(Unit:	(Unit: 1,000 kg/y)	L Scenario			energia. Barana		-	(Unit:	(Unit: 1,000 kg/y)
(H2000)					-			(L2000)				· .			
	Dan	Gasoline	Kerosene	ADO	001	Fuel Oil	Total		LPG	Gasoline	Kerosene	AD0	OGI	Fuel Oil	Total
Demand Area 1	151.3	773.7	1,089.1	1,350.9	286.5	238.8	3,890.3	Demand Area 1	152.5	680.4	1,062.8	1,127.4	239.1	220.7	3,482.9
Demand Area 2	53.9	465.6	612.6	948.3	201,1	39.8	2,321.3	Demand Area 2	543	409.4	597.8	791,4	167.8	36.8	2,057.5
Demand Area 3	1,146.5	2,636.1	3.403.3	2,782.2	590.2	573.1	11,131.4	Demand Area 3	1,155.3	2,318.1	3,321.0	2,321.8	492.5	529.7	10,138.4
Demand Area 4	209.4	807.9	1,351.6	957.2	203.0	115.4	3,644.5	Demand Area 4	211.0	710.4	1,318.9	798.8	169.4	106.7	3,315.2
Demand Area 5	433.3	1,287.2	2,187.8	1,476.1	313.1	801.9	6,499.4	Demand Area 5	436.6	1,131.9	2,134.9	1,231.9	261.3	741.2	5,937.8
Demand Area 6	0	335.5	427.8	751.5	159.4	0	1,674.2	Demand Area 6	0	295.0	417.5	627.2	133.0	O	1,472.7
Demand Area 7	6.08	438.2	515.4	465.2	98.7	- 220.9	1,819.3	Demand Area 7	81.5	385.3	502.9	388.2	82.4	204.2	1,644.5
Demand Area 8	0	95.9	136.1	214.7	45.5	0	492.2	Demand Area 8	0	84.3	132.8	179.2	38.0	0	434.3
Total	2,075.3	6,840.1	9,723.7	8,946.1	1,897.5	1,989.9	31,472.6	Tota!	2,091.2	6.014.8	9,488.6	7,465.9	1,583.5	1,839.3	28,483.3
		-													
(H2005)				÷				(L2005)						٠	
	LPG	Gasoline	Хегозепе	ADO	001	Fuel Oil	Total		DdT	Gasoline	Kerosene	AD0 .	100	Fuel Oil	Total
Demand Area 1	238.7	861.3	1,055.8	1,548.7	328.5	269.0	4,302.0	Demand Area 1	267.6	697.0	967.0	1,191.7	252.7	232.5	3,608.5
Demand Area 2	85.0	518.3	593.9	1,087.2	230.6	44.8	2,559.8	Demand Area 2	95.3	419.4	543.9	836.5	177.4	38.7	2,111.2
Demand Area 3	1,808.4	2,934.6	3,299.2	3,189.8	676.6	645.6	12,554.2	Demand Area 3	2,027.7	2,374.8	3,021.7	2,454.3	520.7	557.9	10,957,1
Demand Area 4	330.3	\$.99.4	1,310.3	1,097.5	232.8	130.0	4,000.3	Demand Area 4	370.3	727.8	1,200.1	844,4	179.1	112.3	3,434.0
Demand Area 5	4.883.4	1,433.0	2,120.9	1,692.3	359.0	903.4	7,192.0	Demand Area 5	766.3	1,159.6	1,942.5	1,302.1	276.2	780.7	6,227.4
Demand Area 7	197.5	8784	499.6	5333	112 1	0 00 00	1,002,	Demand Area 7	143.1	394.8	657.6	41014	24.	2150	7080
Demand Area 8	0	106.7	132.0	246.2	52.2	0	537.1	Demand Area 8	0	86.4	120.8	189.4	40.1	0	436.7
Total	3,273.3	7,614.5	9,426.5	10,256.6	2,175.6	2,241.6	34,988.2	Total	3,670.3	6,162.0	8 633.4	7,891.7	1,673.9	1,937.1	29,968,4
											4				
(H2010)								(L2010)							
	LPG	Gasoline	Kerosene	ADO	DOI	Fuel Oil	Totai		LPG	Gasoline	Kerosene	ADO	IDO	Fuel Oil	Total
Demand Area 1	214.3	1,007.2	1,150.6	1,793.4	380.4	316.9	4,862.8	Demand Area 1	248.8	753.0	1,002.3	1,244.6	264.0	235.2	3,747,9
Demand Area 2	76.3	606.1	. 647.2	1,258.9	267.0	52.8	2,908.3	Demand Area 2	88.6	453.1	563.8	873.7	185.3	39.2	2,203.7
Demand Area 3	1,623.6	3,431.8	3,595,6	3,693.6	783.5	760.5	13,888.5	Demand Area 3	1,885.3	2,565.6	3,132,0	2,563.3	543.8	564.6	11,254.6
Demand Area 4	296.5	1,051.8	1,427.9	1,270.8	254.4	153.2	4,454,6	Demand Area 4	344.3	786.3	1,243.8	881.9	187.0	113.7	3,557.0
Demand Area 5	613.6	1,675.8	2,311.4	1,959.6	415.7	1,064.2	8,040.3	Demand Area 5	712.5	1,252.8	2,013,4	1,359.9	288.5	790.0	6.417.1
Demand Area 7	114.5	570.5	544.5	617.6	131.0	293.1	2.271.2	Deniand Area 7	133.0	426.5	474.3	428.6	6.08	217.6	0,656,1
Demand Area 8	0	124.8	143.8	285.0	60.5	0	614.1	Demand Area 8	0	83.3	125,2	197.8	41.9	٥	458.2
Total	2,938.8	8,904.7	10,273.0	11,876.5	2,504.1	2,640,7	39,137,8	Total	3,412.5	6,657.1	8.948.5	8,242.2	1,748.3	1,960.3	30,968.9

4. RESULT OF LP MODEL STUDY

4-1 Introduceable Amount of Methanol

4-1-1 High Scenario in 2000 (H2000)

In base case (H2000), the refining capacity reaches the maximum in all refineries, and 881 thousand kl/y of gasoline and 199 thousand kl/y of ADO is imported. On the other hand, naphtha and fuel oil are exported. The amount of methanol introduction is 0.88 million kl/y as a substitution of kerosene and 1.7 million kl/y as a substitution of gasoline in these three methanol introduction case (H2000-1 ~ 3). These amounts are equal to the import of petroleum products in base case (H2000-0).

4-1-2 High Scenario in 2005

The amounts of importation are 1,663 thousand kl/y in gasoline, 397 thousand kl/y in kerosene and 867 thousand kl in ADO in base case (H2005-0).

The amount of methanol introduction is 7,282 thousand kl/y in introduction case 1 (175\$/t of methanol). 1,721 thousand kl/y of gasoline and 1,947 kl/y of kerosene are substituted. These amounts are more than import production in base case. The profit is also more than base case. Methanol is introduced in region 2 for kerosene (606 thousand kl/y) and in region 3 for gasoline (3,309 thousand kl/y) and kerosene (3,367 kl/y).

The amount of methanol introduction is 11,744 thousand kl/y in introduction case 2 (165\$/t of methanol). 2,672 thousand kl/y of gasoline, 2,602 thousand kl/y of kerosene and 609 thousand kl/y of diesel oil are substituted. Methanol is introduced in region 3 for gasoline (1,829 thousand kl/y) and ADO (1,296 thousand kl/y) and in region 4 for kerosene (1,337 thousand kl/y) in addition to the amount in above case.

The amount of methanol introduction is 20,849 thousand kl/y in introduction case 3 (155\$/t of methanol). The methanol is introduced 505 thousand kl/y for gasoline and 5,491 thousand kl/y for ADO in region 3 and 945 thousand kl/y of gasoline and 2,164

thousand kl/y of kerosene in region 5 in addition to the amount in introduction case 2.

4-1-3 High Scenario in 2010 (H2010)

In base case, 2,954 thousand kl/y of gasoline, 2,019 thousand kl/y of kerosene and 1,763 thousand kl/y of ADO are imported.

In 175\$/t case, methanol is introduced to reach the maximum level in region 1-5. In 165 and 155\$/t case, methanol is also introduced in region 6 to the maximum level. Methanol introduction shows the high advantage in this scenario.

4-1-4 Low Scenario in 2000 (L2000)

In base case, 62 thousand kl/y of gasoline is imported. The gasoline production is 5,953 thousand kl/y. This is because expansion of gasoline production costs higher than gasoline import.

The methanol is introduced as the substitution of 48 thousand kl/y of gasoline in all three introduction cases. Gasoline production is 5,990 thousand kl/y and seems to be the maximum level.

4-1-5 Low Scenario in 2005 (L2005)

In base case, 223 thousand kl/y of gasoline is imported. The gasoline production is 5,939 thousand kl/y. This is also because expansion of gasoline production costs higher than gasoline import.

The methanol is introduced as the substitution of 330 thousand kl/y of gasoline in all three introduction cases. Gasoline production reached the same level as L2000 case of 5,990 thousand kl/y.

4-1-6 Low Scenario in 2010 (L2010)

In base case, 712 thousand kl/y of gasoline is imported. The gasoline production is 5,945 thousand kl/y. This is also because expansion of gasoline production costs higher than gasoline import.

The methanol is introduced as the substitution of 1,281 thousand kl/y in 175\$/t case, 11,348 thousand kl/y in 165\$/t case and 1,370 thousand kl/y in 155\$/t case. In 155\$/t case, the same amount methanol as gasoline import in base case is introduced.

4-2 Relation between Introduceable Quantity of Methanol and Crude Oil Price

Introduceable quantity of methanol is calculated when crude oil price moves by 1\$/bbl in high scenario in 2000. The result is shown in Fig. 3.

4-2-1 175\$/t Case (H175-32~37)

In 175\$/t case, methanol is not introduced when crude oil price is less than 32\$/bbl.

1,695 thousand k@/y of methanol is introduced in region 3 as the substitution of gasoline when oil price becomes 33\$/bbl. This is the same amount as gasoline import in H175-32 case. Product flow does not change but gasoline is not imported and methanol is introduced. Methanol cost is supposed to be almost equal to gasoline import cost.

When oil price becomes 34\$/bbl, additional 220 thousand kl/y of methanol is introduced in region 3 as gasoline substitution, and 422 thousand kl/y is introduced in region 2 as kerosene substitution. As the result, there is no need to import the petroleum products and 103 thousand kl/y of reformate is exported. Methanol introduction cost has advantage to import cost of products, but does not have advantage to their production cost. This is because crude oil refining pattern is not changed.

When oil price becomes 35\$/t, additional methanol is introduced in regions 3 as gasoline substitution and in region 2 as kerosene substitution. As the result, crude oil

refining pattern is changed and crude oil export is increased. Methanol has cost advantage compared to petroleum products in the above two regions.

When oil price becomes 36 and 37\$/bbl, methanol is introduced also in region 3 as kerosene substitution and this causes the expansion of crude oil export.

4-2-2 165\$/t Case (H165-32~37)

Methanol is not introduced when oil price is less than 29\$/bbl, and products flow shows almost the same as H2000-0 case.

Methanol introduction cost becomes equal to the gasoline import cost when oil price becomes 30 and 31\$/bbl. When oil price becomes more than 32\$/bbl, methanol introduction keeps advantage than petroleum products in region 3 as gasoline substitution and in region 2 as substitution of kerosene.

4-2-3 155\$/t Case (H155-32~37)

Methanol introduction cost becomes equal to the gasoline import cost when oil price becomes 29\$/bbl. Methanol introduction keeps its advantage compared to petroleum products in the above mentioned two region when oil price becomes higher than 30\$/bbl.

4-3 Changes of Profit Composition

The changes of profit composition are examined here. The results are shown in Table 9 and 10.

"Crude oil production cost" is not changed because crude oil production is at a maximum level in each case. When domestic refining is increased, "crude oil export amount is minus (profit decrease), "crude oil transportation cost" is plus (cost increase) and "catalyst/chemicals cost" is minus (cost increase).

As methanol has lower heat value than petroleum products, the amount of transportation is increased when methanol is introduced, and "product transportation cost" becomes less (Cost increase).

4-3-1 High Scenario in 2000 (H2000)

The amount of methanol introduced in this scenario is equal to product import in base case (H2000-0). Product import cost (271 million \$) in base case is smaller than methanol introduction cost (methanol production cost and products transportation cost).

4-3-2 High Scenario in 2005 (H2005)

Cost increase caused by methanol introduction is covered by plus factor as "product import cost" and "the amount of crude oil export". In H2005-1, 2, "the amount of product export" is minus due to export decrease of unprofitable naphtha and fuel oil. In H2005-3, "the amount of product export" also becomes plus factor due to export increase of reformate, kerosene and diesel oil in addition to the above export decrease.

4-3-3 High Scenario in 2010 (H2010)

The profit structure is the same as H2005-3, and the profit of methanol introduction is larger than base case.

4-3-4 Low Scenario in 2000 (L2000)

Gasoline import in base case is covered by increase of crude oil refining and methanol introduction. Because petroleum products are not imported in methanol introduction case. But their costs are larger then that of gasoline imports.

4-3-5 Low Scenario in 2005 (L2005)

The change of profit composition is the same as L2000.

4-3-6 Low Scenario in 2010 (L2010)

The profit composition of L2010-1 & 2 is the same as L2000. But "products export cost" is almost equal to "methanol introduction cost" in 2010-3.

4-4 Change of Products Transportation

The change of products transportation caused by methanol introduction is studied according to cases in 4-2.

4-4-1 Change of Gasoline Flow

Methanol is introduced as gasoline substitution in region 3. The change of product flow caused by methanol introduction is as follows.

- I) Gasoline is transported from Plaju and Cilacap to region 3. At first, transportation from Cilacap to region 3 is decreased. This decreased amount is transported to region 4. And gasoline transportation from Dumai to region 4 is decreased.
- II) Then the transportation of gasoline from Plaju to region 3 is decreased, and this decrease amount is sent to region 1. As the result, gasoline production in Dumai is decreased and reformate is exported.

4-4-2 Change of Kerosene Flow

As kerosene substitution, methanol is introduced firstly as kerosene substitution in region 2 and then in region 3. The change of product flow caused by methanol introduction is as follows.

- I) At present time, kerosene is transported from Dumai and Plaju in region 2. However, first of all, transportation from Dumai is decreased.
- II) Then kerosene from Plaju to region 3 is changed to supply from Cilacap, and kerosene from Plaju supply to region 2. Supply from Dumai decreased furthermore.
- III) When methanol is introduced in region 3, kerosene from Cilacap to region 3 is decreased and is supplied to region 4. As a result, kerosene from Dumai to region 4 is decreased.

Table 4 Summary of the Study (High Scenario)

Table 5 Summary of the Study (Low Scenario)

<u></u>			·····		ı —	Γ		Γ	<u> </u>		<u> </u>	ļ —	<u> </u>		ı ——	1	T	T .	I	T	1
L2010-3		29	155	0	0	1,370	0	0	Ġ	0	0	0	0	1,370	1,091	712	0	0	1		
L2010-2		29	165	0	0	1,348	0.	0	0	0	0	0	0	1,348	1,073	701	0	0			
L 2010-1		29	175	0	0	1,281	0	0	0	0	0	0	0	1,281	1,020	999	0	0			: !
L2010-0 L2010-1	Base case	29	;	1	-	-		1		!	-		i i					-	712	O	0
L2005-3		25	155	0	0	330	0	0	0	0	0	0	0	330	263	172	0	0			1
750027		25	165	0	.0	330	0	0	0	0	0	0	0	330	263	172	0	0		-	
L2005-1		25	175	0	0	330	0	0	0	Ô	0	0	0	330	263	172	0	0	1		-
L 2005-0	Base case	25	E E		<u>.</u>	1			: :	1	-	1		1		-	1 1	1	223	0	0
L2000-3		21	155	0	0	48	0	0	0	0	0	0	0	48	38	25	0	0			
L 2000-2		21	165	0	0	48	0	0	0	0	0	0.	0	48	38	25	0	0	-	-	
L 2000-1		21	175	0	Û	48	0	0	0	0	0	0	0	48	38	25	0	0	-		
L2000-0	Base case	21	-			1 1		t 1 3			-		1				1	-	62	0	0
		\$/bbl	\$/\$	1000 ke/y	1000 k£/y	1000 ke/y	1000 ke/y	1000 ke/y	1000 ke/y	1000 ke/y	1,000 k.e/y	1000 ke/y	1000 ke/y	1000 ke/y	1000 £/y	1000 ke/y	1000 ke/y	1000 k¢/y	1000 ke/y	1000 ke/y	1000 ke/y
	Case			Kerosene	Kerosene	Gasoline	Kerosene	ADO	Kerosene	Gasoline	Kerosene	ADO	Kerosene			Gasoline	Kerosene	ADO	Gasoline	Kerosene	ADO
Ċ	3	Crude Oil Price	Methanol Price	Demand Area 1	Demand Area 2	Demand Area 3			Demand Area 4	Demand Area 5			Demand Area 6	Į.	10131	Petroleum	substitution	:	Petroleum	dates mitport	
		Cru	Met		Σo	+ ,C	୯୮୦		- £+	, H O	ซฮ	ບ່ພາ	}			-	- š		مُ	2	

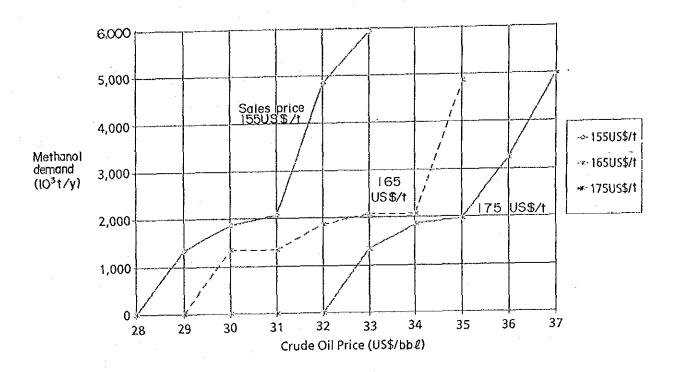


Fig. 3 Fuel Methanol Demand vs Oil Price

Table 6 Summary of the Study (Methanol Introduction v.s. Crude Oil Price \oplus)

(יותבידומווסז זוונז סממכיניסוו איזי כז מתפ	H175-32 H175-33 H175-34	Case	Crude Oil Price \$/bbi 32 33 34	Methanol Price \$/t 175 175 175	Demand Kerosene 1000 0 0 0 0 Area 1	Demand Area 2 Kerosene 1000 0 0 422	Demand Asrea 3 Gasoline 1000 0 1,695 1,915	Kerosene 1000 0 0 0 0	ADO 1,8% 0 0 0	Demand Kerosene 1000 0 0 0 0 Area 4	Demand Area 5 Gasoline Rely 0 0 0 0	Kerosene 1000 0 0 0 0	ADO 1000 0 0 0 0	Demand Aerosene 1000 0 0 0 0	1000 0 1,695 2,337	1000 0 1,349 1,860	Petroleum Gasoline 1000 0 881 996	gubstitution Kerosene $\frac{1000}{k^2 l y}$ 0 0 207	ADO 1000 0 0 0 0	Petroleum Gasoline 1000 831 0 0	TOTAL
on Frice	н175-35 н		35	175	0	487	1,988	0	0	0	0	0	0	O	2,475	1,970	1,034	239	0	o	
(3)	H175-36 H		36	175	0	625	1,988	1,453	0	0	0	0	0	c	4,066	3,237	1,034	1,018	0	0	
	H175-37		37	175	0	625	2,173	3,473	Θ.,	0	0	0	C	0	6,271	4,992	1,130	2,008	0	6	

Table 7 Summary of the Study (Methanol Introduction v.s. Crude Oil Price (2)

Case \$\frac{\chi_{0.00}}{\chi_{0.00}}\$ H165-29 F \$\frac{\chi_{0.00}}{\chi_{0.00}}\$ 0 Kerosene \(\frac{\chi_{0.00}}{\chi_{0.00}}\$ 0 Kerosene \(\frac{\chi_{0.00}}{\chi_{0.00}}\$ 0 Gasoline \(\frac{\chi_{0.00}}{\chi_{0.00}}\$ 0	H165-30 H165-31 H165-32 H165-33 30 31 32 33 165 185 165 165 0 0 0 0 0 1,695 1,695 1,915 1,988	3 H165-34 3 34 1 1,988 1 1,988	H166-35 35 36 165 0 0 625 2,007 3,473
	0 0		0
Kerosene $\frac{1000}{k\ell/y}$ Gasoline $\frac{1000}{k\ell/y}$	0 0 0 0	0 0	0
e e	0 0		0
ADO keyy Kerosene 1000 Kerosene keyy	0 0 0 0	0 0	0 0
1000 kC/y	1,695 1,595 2,342 2,613	3 2,613	6,105
1000	1,349 1,349 1,864 2,080	2,080	4,860
Gasoline 1900 Rely	881 896 1034	1,034	1,044
Kerosene 1000 ke/y	0 0 209 306	306	2,008
ADO 1000 ke/y	0 0 0 0	0 0	0
Gasoline 1000 ke/y	0 0 0	0 0	٥
Kerosene 1000 ke/y	0 0 0 0	0 0	0
ADO 1000 ke/y		0	

Table 8 Summary of the Study (Methanol Introduction v.s. Crude Oil Price 3)

H155-33		33	155	0	625	3,348	3,473	0	0	0	0	0	0	7,446	5,927	1,741	2,008	0	0	0	0
H155-32		32	155	0	625	1,988	3,473	0	0	0	0	0	0	980'9	4,844	1,034	2,008	0	0	0	0
H155-31		31	155	0	625	1,988	0	0	0	0	0	0	0	2,613	2,080	1,034	306	0	0	0	0
H155-30		30	155	0	427	1,915	0	0	0	0	0	0	0	2,342	1,864	966	209	O	0	0	0
H155-29		29	155	0	0	1,695	0	0	6	0	0	0	0	1,695	1,349	188	0	0	0	0	199
H155-28		28	155	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	881	0	199
		\$/bbl	2/\$	1000 ke/y	1000 ke/y	1000 ke/y	1000 ke/y	1000 ke/y	1000 ke/y	1000 ke/y	1000 ke/y	1000 ke/y	1000 ke/y	1000 ke/y	1000 1000	1000	1000 keyy	1000 key	1000 ke/y	1000 ke/y	1000 Fe/y
	Case			Kerosene	Кегоѕепе	Gasoline	Kerosene	ADO	Kerosene	Gasoline	Kerosene	ADO	Kerosene		=	Gasoline	Kerosene	АДО	Gasoline	Kerosene	ADO
	ပ <u>ံ</u>	Orude Oil Price	Methanol Price	Demand Area 1	Demand Area 2	Demand Area 3			Demand Area 4	Demand Area 5			Demand Area 6		Lotal	Petroleum	substitution		Petroleum	1 adim spor	
		Crud	Meth		Σo	٠.G	4 ti c		⊷ д +	2,54 O	ਰ ੜ	ი თ.	5			۳,				5	

Table 9 The Change of Profit Framework (High Scenario)

0-2 H2010-3 H2010-4	Expanding refinery	(Comparison to H-2010-0 case)	0 0 -1	21 +1,521 -2,323	+24 +24 -28	0 0	+1 +1 -4	63 +1,594 +1,248	278 32	05 -137 +143	44 -3,890 0	60 +2,560 +1,096	42 +1,395 +99
0-1 H2010-2		Compariso	0	21 +1,521	+ 77+	0	-	87 +1,563		07 -105	32 -4,144	50 +2,560	90 +1,142
0 H2010-1	61))		+1,521			+	- +1,487	- 264	- 107	4,332	- +2,560	+890
H2010-0	Base case	: :	-	1		-		-			1	-	1
H2005-4	Expanding refinery	case)	1	-727	8	0	E	+374	-21	+38	0	+393	+ 45
H2005-3		H-2005-0	0	+1,883	98 +	0	κ + 	+243	-114	-136	-2,564	+910	+261
H2005-2		(Comparison to H-2005-0 case)	0	+1,415	+26	Û	+2	-506	- 79	-94	-1,538	+910	+136
H2005-1		(Con	0	+ 499	+ 10	0	+	-254	- 54	. – 34	-1,012	+910	+ 66
H2005-0	Base case		1	1					1 1			! !	ļ
H2000-4	Expanding refinery	case)	1	+15	& +	0	-2	-30	-12	-15	0	+ 50	+ 22
H2000-3		H-2000-0 case)	0	0	0	0	0	-1	- 14	0	258	+271	1 2
H2000-2		(Comparison to	0	0	0	0	0	-1	-14	0	-275	+271	-19
H2000-0 H2000-1 H2000-2		(Con	0	0	0	0	0	-1	-15	Q	-291	+271	- 36
	Buse case			-	1		-	-	app das ofa	-	;		
Case	Item		Crude Oil Production Cost	Amount of Money of Grude Oil Export	Crude Oil Transportation Cost	Amount of Money of AL Import	Catalyst, Chemical Cost	Amount of Money of Products Export	Products Transportation Cost	Amount of Domestic Profit	Methanol Production Cost	Products Import Cost	Total

Crude oil production cost includes natural gas production cost (Natural gas is used in Balikpapan) Note) +: Profit increase or cost decrease -: Profit decrease or cost increase Products transportation cost includes methanol. Amount of petroleum products include LPG.

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Table 10 The Change of Profit Framework (High Scenario)

(million US\$)	H2010-3		2010-0	0	0	0	0	0	0	-10	O	- 169	+184	+5
(milli	H2010-2	-	(Comparison to L-2010-0 case)	0	-4	+1	0	0	+1	-10	-1-	-177	+184	9-
	H2010-1		(Compa	0	-28	0	0	0	+14	-10	+1	-178	+184	-17
	H2010-0	Base case						**************************************		-	-6-2-6			-
	H2005-3		2002-0	0	-25	0	0	0	+12	-2	+1	-41	+51	-4
	H2005-2		(Comparison to L-2005-0 case)	0	-25	0	0	0	+12	12	0	43	+51	7-
	H2005-1		(Compar	0	-25	0	0	0	+12	-2	0	-46	+51	-10
	H2005-0	Base case								1 2				1
	H2000-3 H2005-0		(Comparison to L-2000-0 case)	0	-19	-1	0	0	+10	0	+3	<u>–</u> 6	+12	-2
	H2000-2			0	-18	0	0	0	6+	-1	+2	9-	+12	-2
	H2000-1		(Compa	.0	-18	O	0	0	6+	-1	+2	-7	+12	13
	H2000-0	Base case			1 1					i . 1			***	1
	Case	Item		Orude Oil Production Cost	Amount of Money of Crude Oil Export	Crude Oil Transportation Cost	Amount of Money of AL Import	Catalyst. Chemical Cost	Amount of Money of Products Export	Products Transportation Cost	Amount of Domestic Profit	Methanol Production Cost	Products Import Cost	Total

Note) +: Profit increase or cost decrease -: Profit decrease or cost increase

Crude oil production cost includes natural gas production cost (Natural gas is used in Balikpapan)

Products transportation cost includes methanol,

Amount of petroleum products include LPG.

Table 12 Change of Products Transportation (Kerosene Flow) Table 11 Change of Products Transportation (Gasoline Flow)

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Demand Area 1					
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Demand Area 6					
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Demand Area 1	• •	- 09			
Demand Area Refinery	Dumai	Plaju	Cilacap	Balikpapan	Methanol Introduced

ATTACHMENT 6-1

1. Reference Drawings of Banko Coal Resources

1. Reference Drawings of Banko Coal Resources

- Fig. 1 Surveyed Area by Shell Mijonbow N.V. in South Sumatra
- Fig. 2 Most Promising Area around Bukit Asam Coal Mine
- Fig. 3 Basin formed in Tertiary Epoch in South Sumatra
- Fig. 4 Tectonical Structures in South Sumatra
- Fig. 5 Geological Structure in Banko-Suban Jeriji Area
- Fig. 6 Columner Sections of Boreholes Driven by Shell (1)
- Fig. 7 Columner Sections of Boreholes Driven by Shell (2)
- Fig. 8 Columner Sections of Boreholes Driven by Shell (3)
- Fig. 9 Columner Sections of Boreholes Driven by Shell (4)
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 North West Banko
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- Fig. 24 Reconnaissance Route Map and Estimated Vertical Section on the Line 10, North West Banko
- Fig. 25 Reconnaissance Route Map and Estimated Vertical Section on the Line 11, North West Banko
- Fig. 26 Reconnaissance Route Map and Estimated Vertical Section on the Line 12, North West Banko

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- Fig. 49 Isothermal Line of the Inside of No. 1 Coal Heap at AM 11:00 on 2 September, 1987 (Horizontal Section)

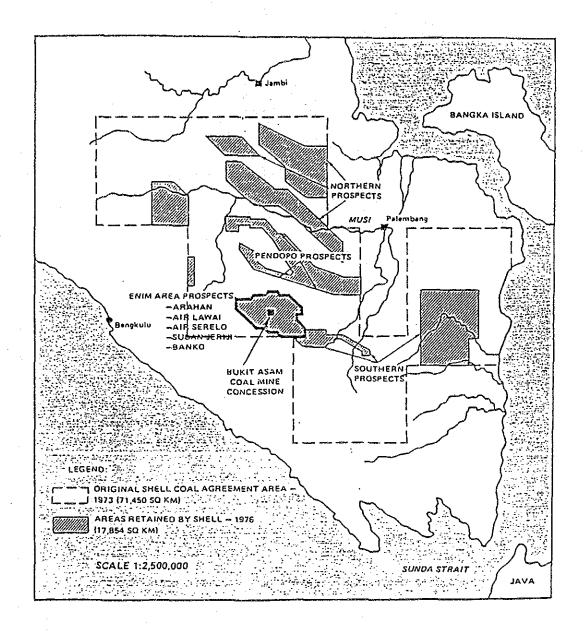


Fig. 1 Surveyed Area by Shell Mijonbow N.V. In South Sumatra

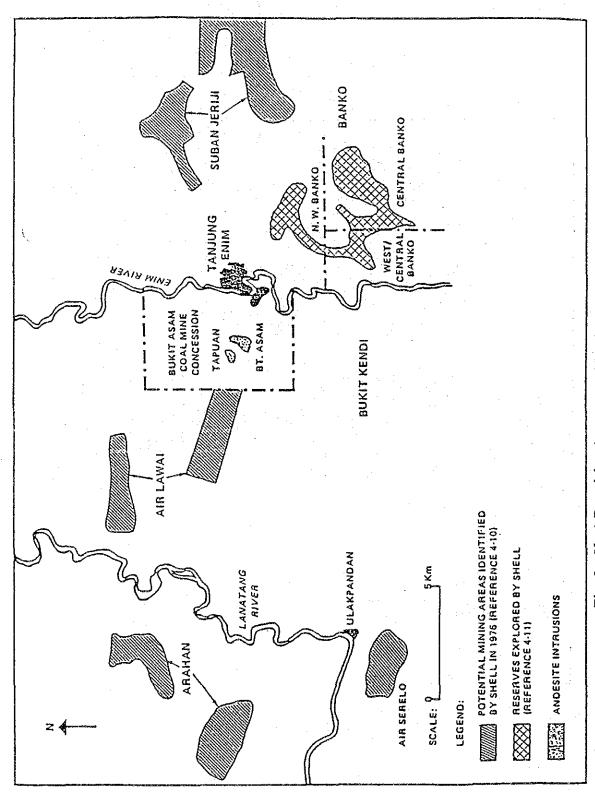


Fig. 2 Most Promising Area around Bukit Asam Coal Mine

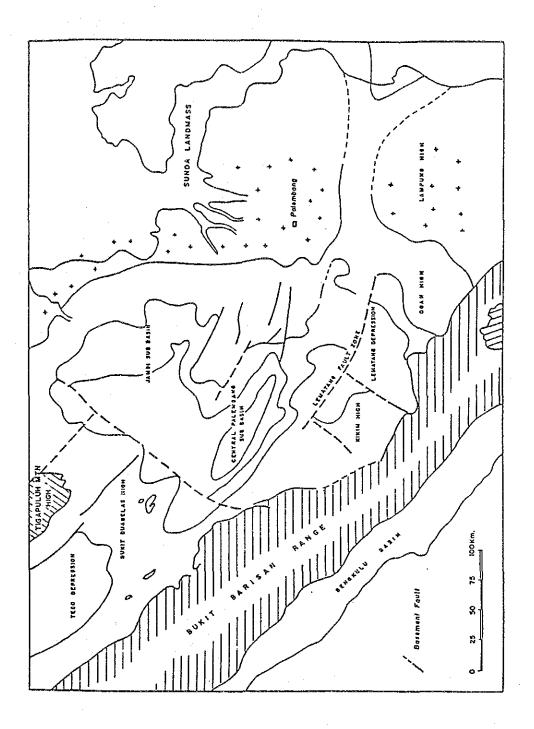
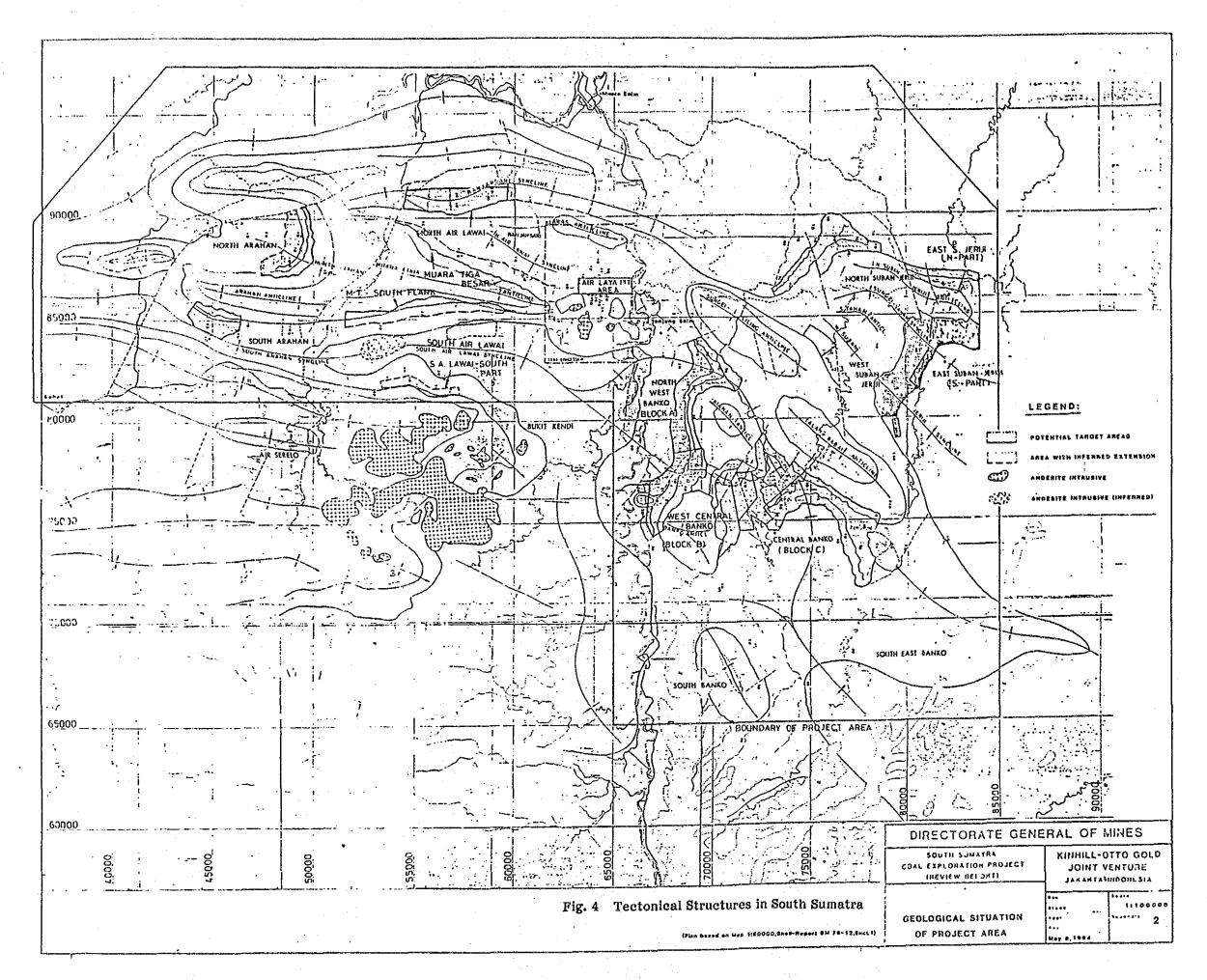
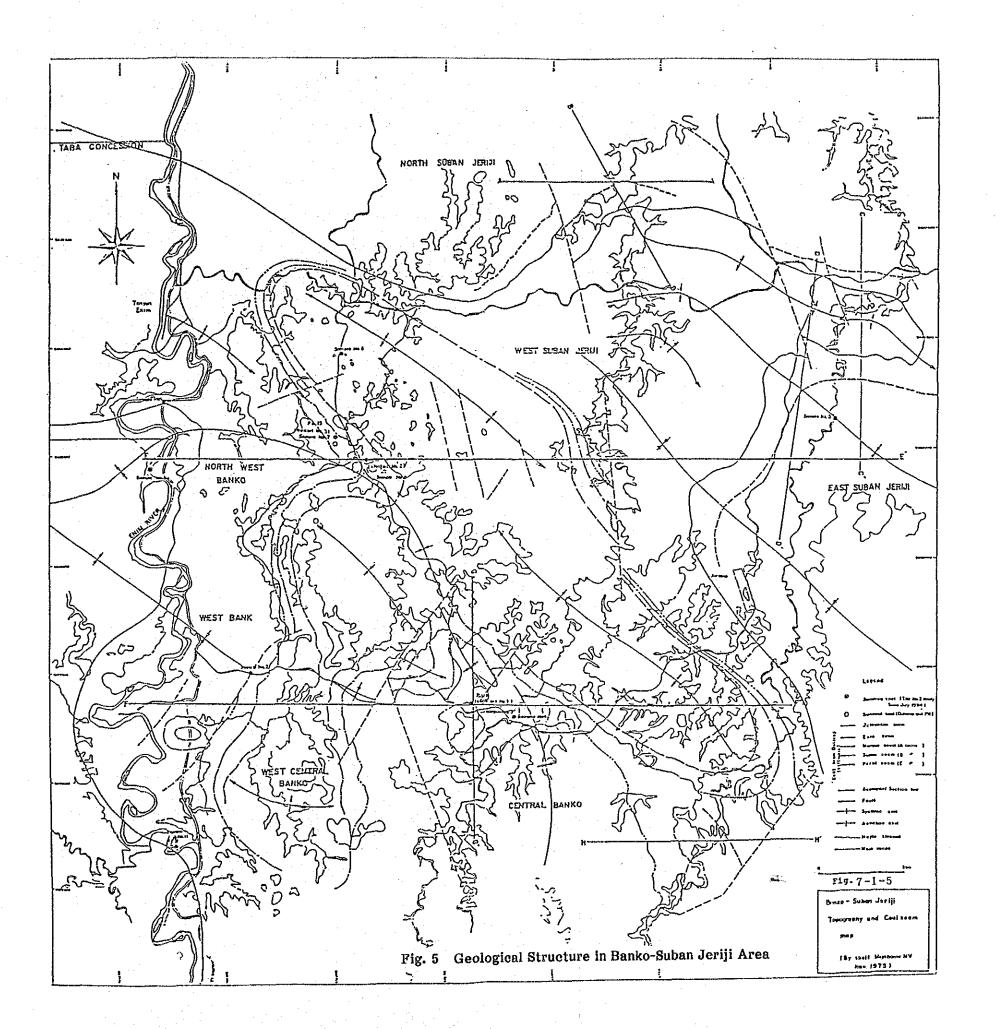


Fig. 3 Basin formed in Tertiary Epoch in South Sumatra





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Fig. 12 Columner Sections of Boreholes driven by DOC (2)

120"			•		 (2))			graphical and the second of th		
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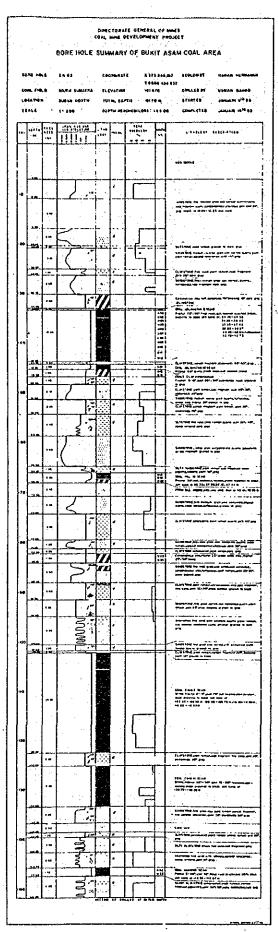
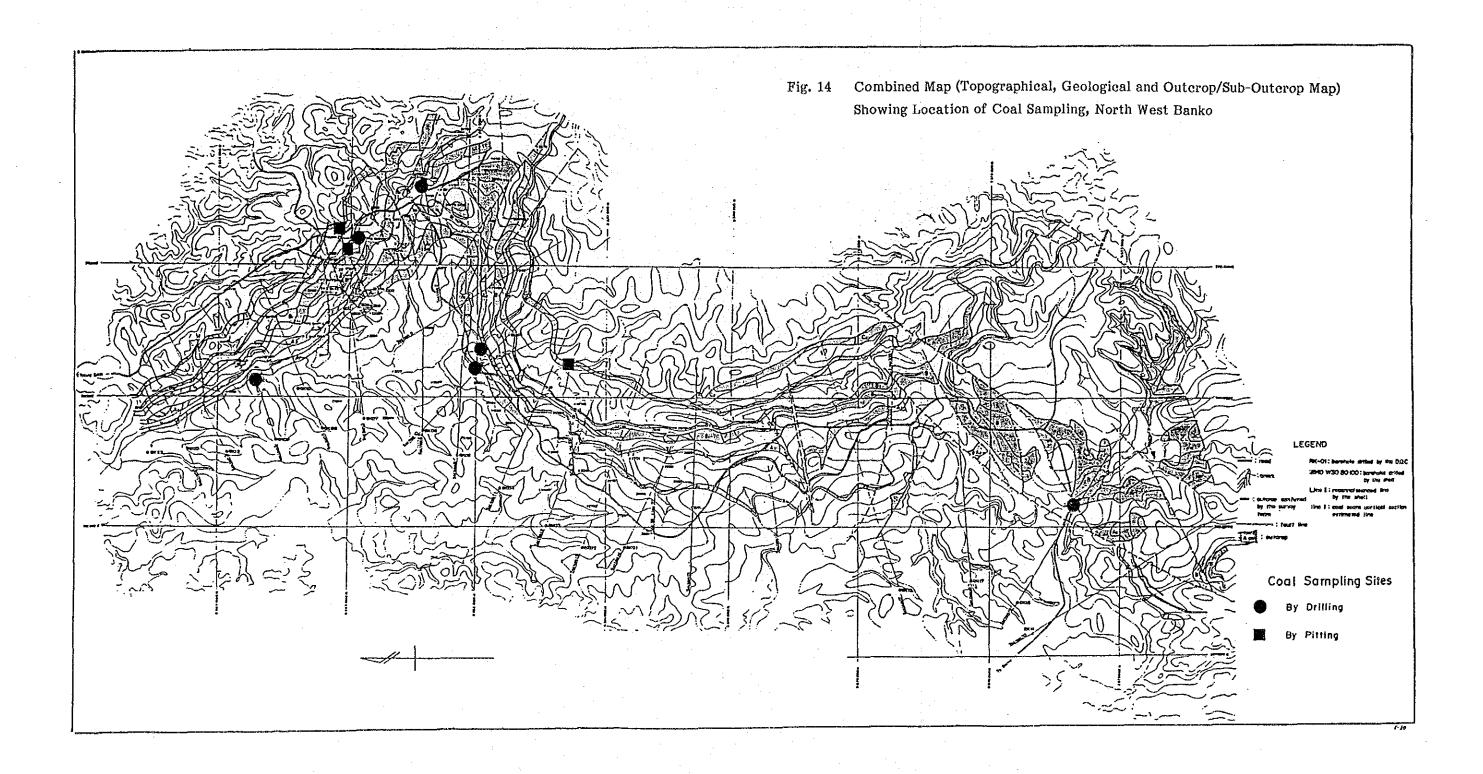
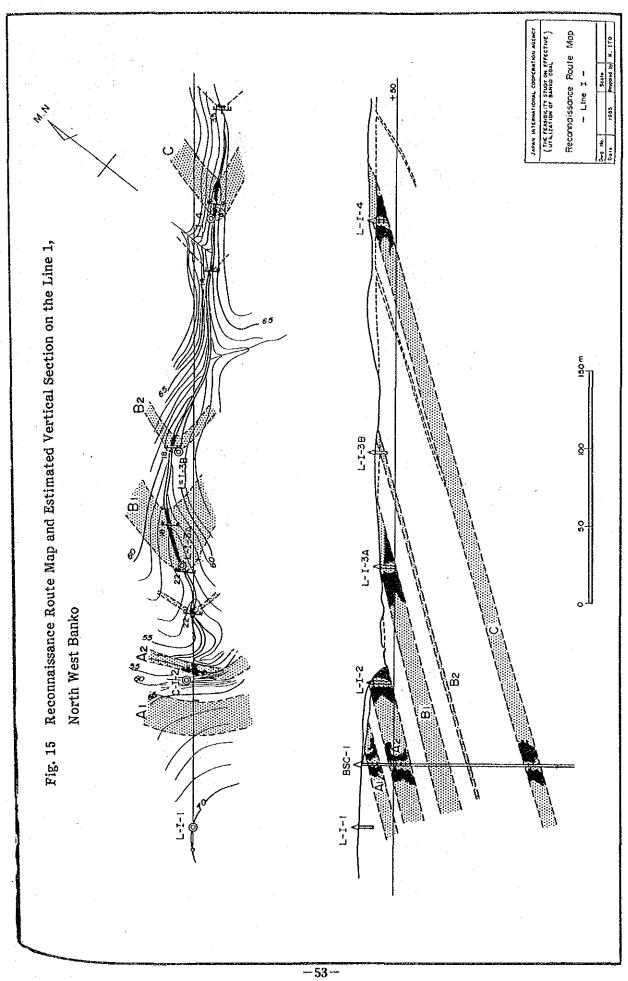
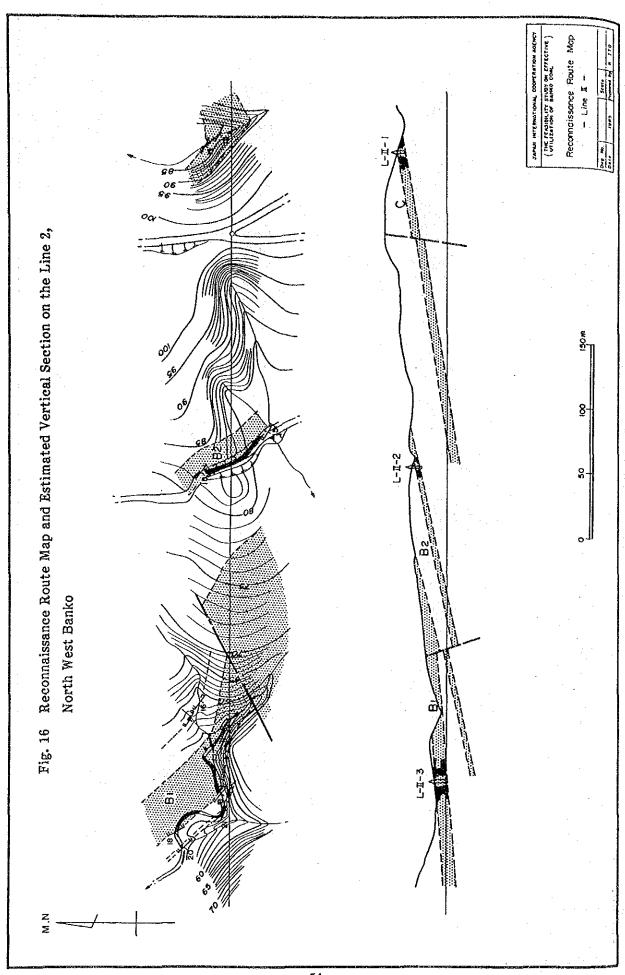
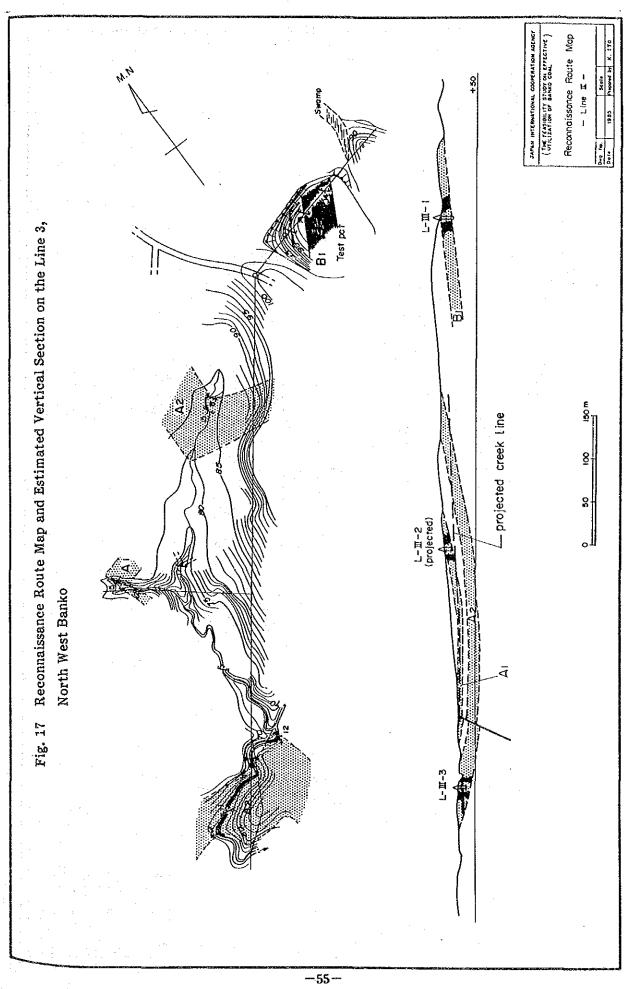


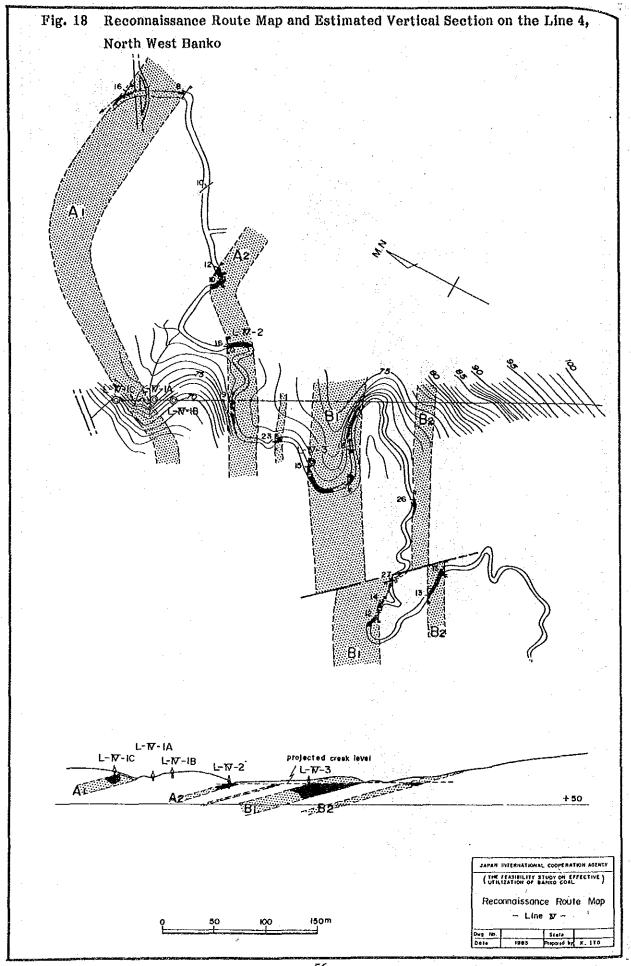
Fig. 13
An Example of Columner
Sections Prepared by DOC

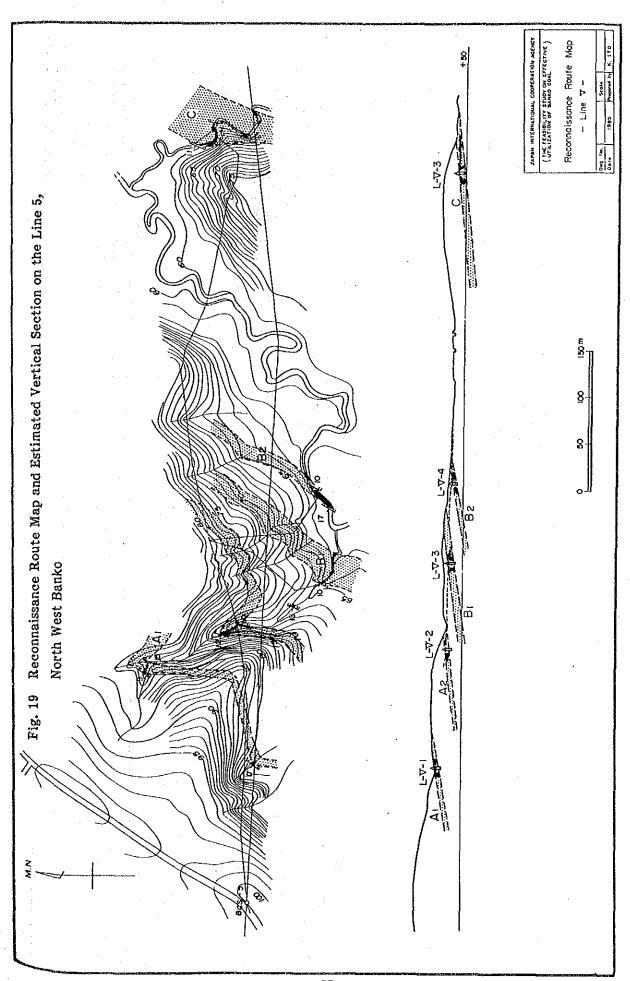


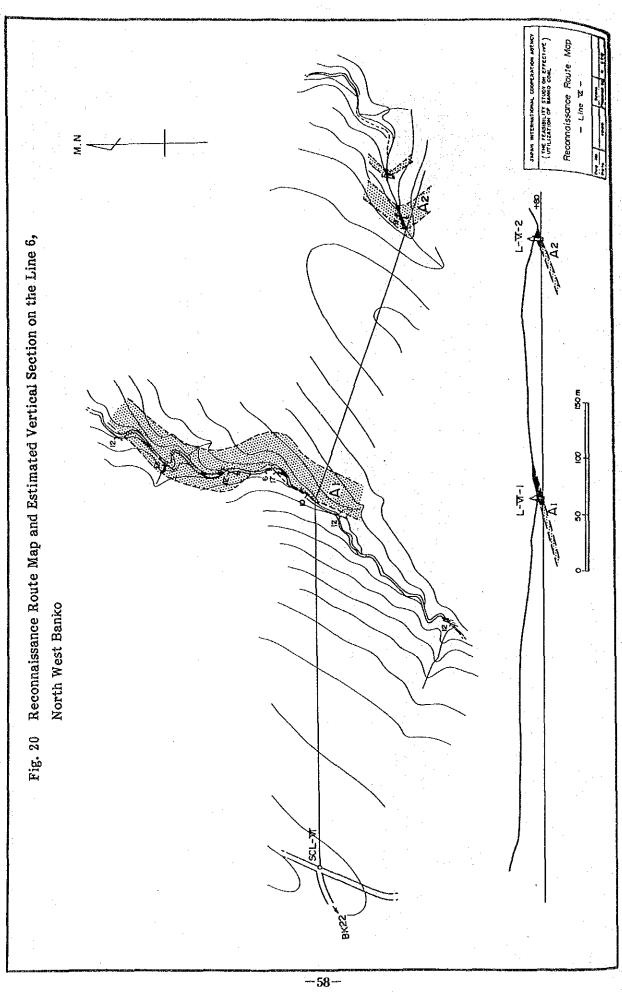


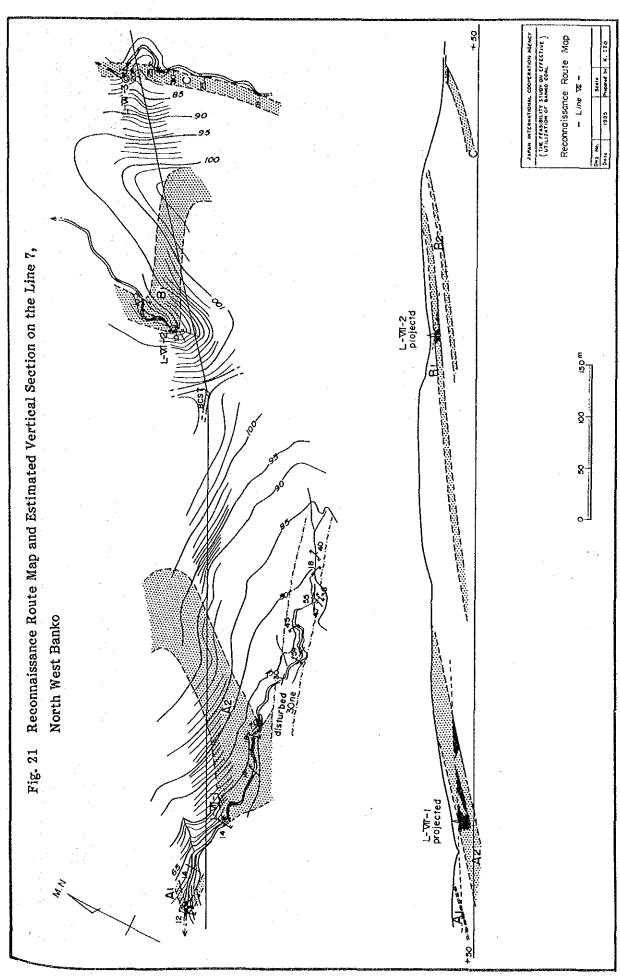


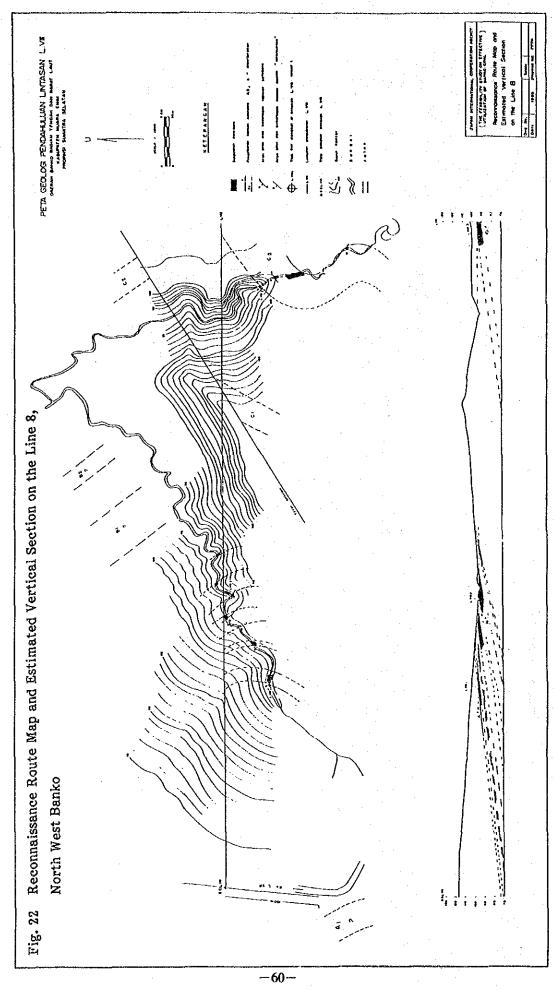


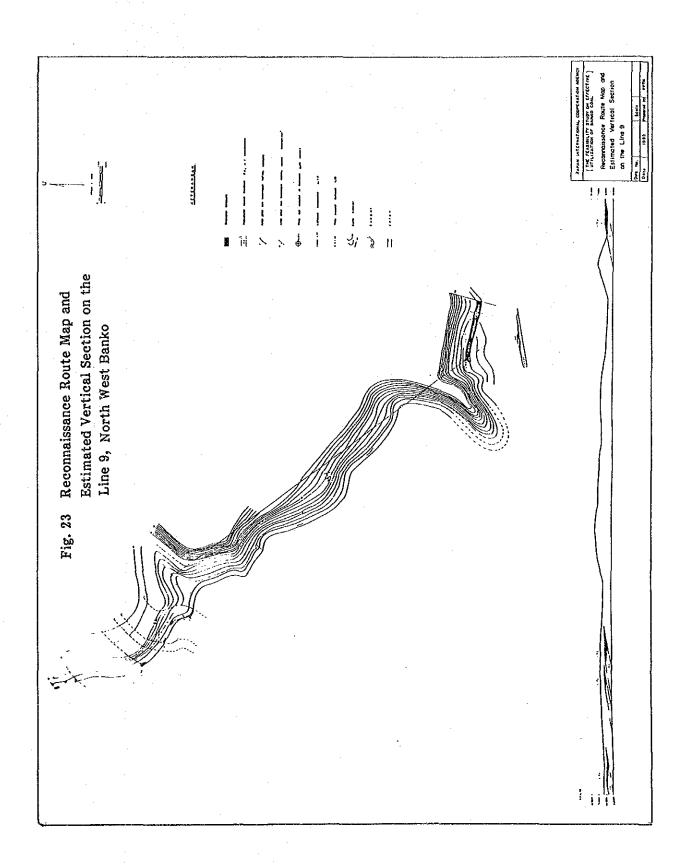


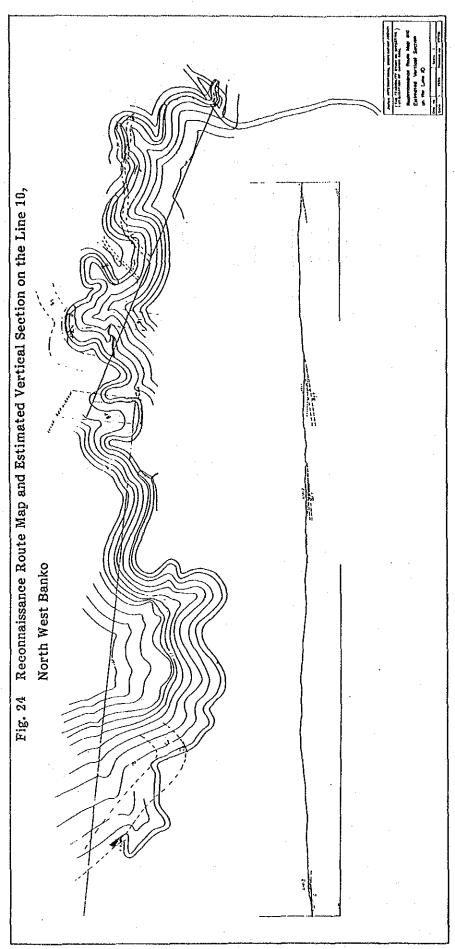












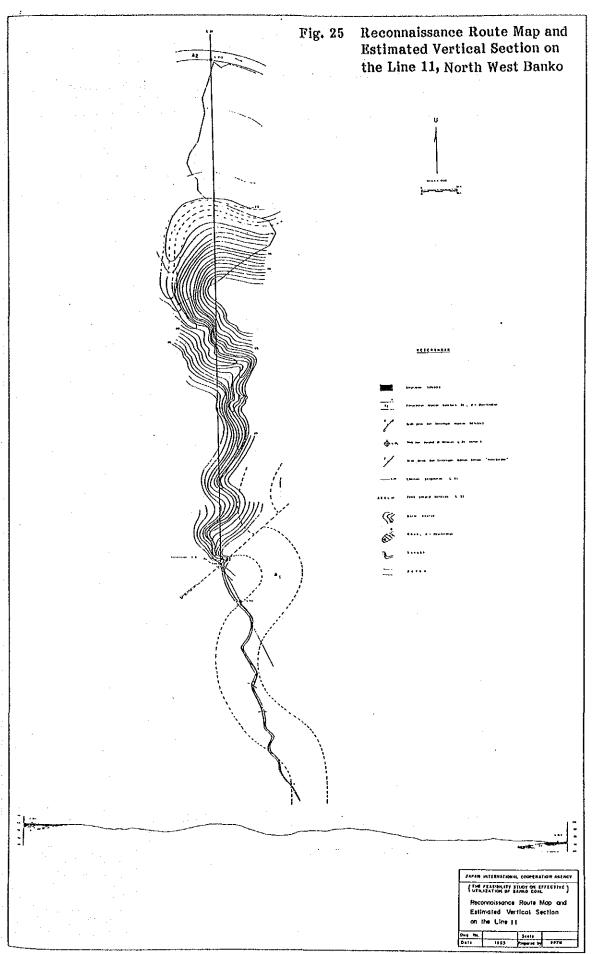
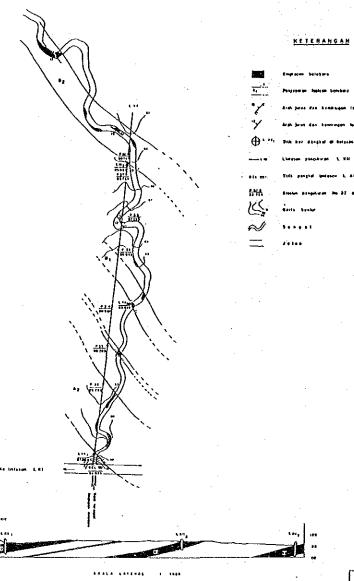


Fig. 26 Reconnaissance Route Map and
Estimated Vertical Section
on the Line 12, North West Banko

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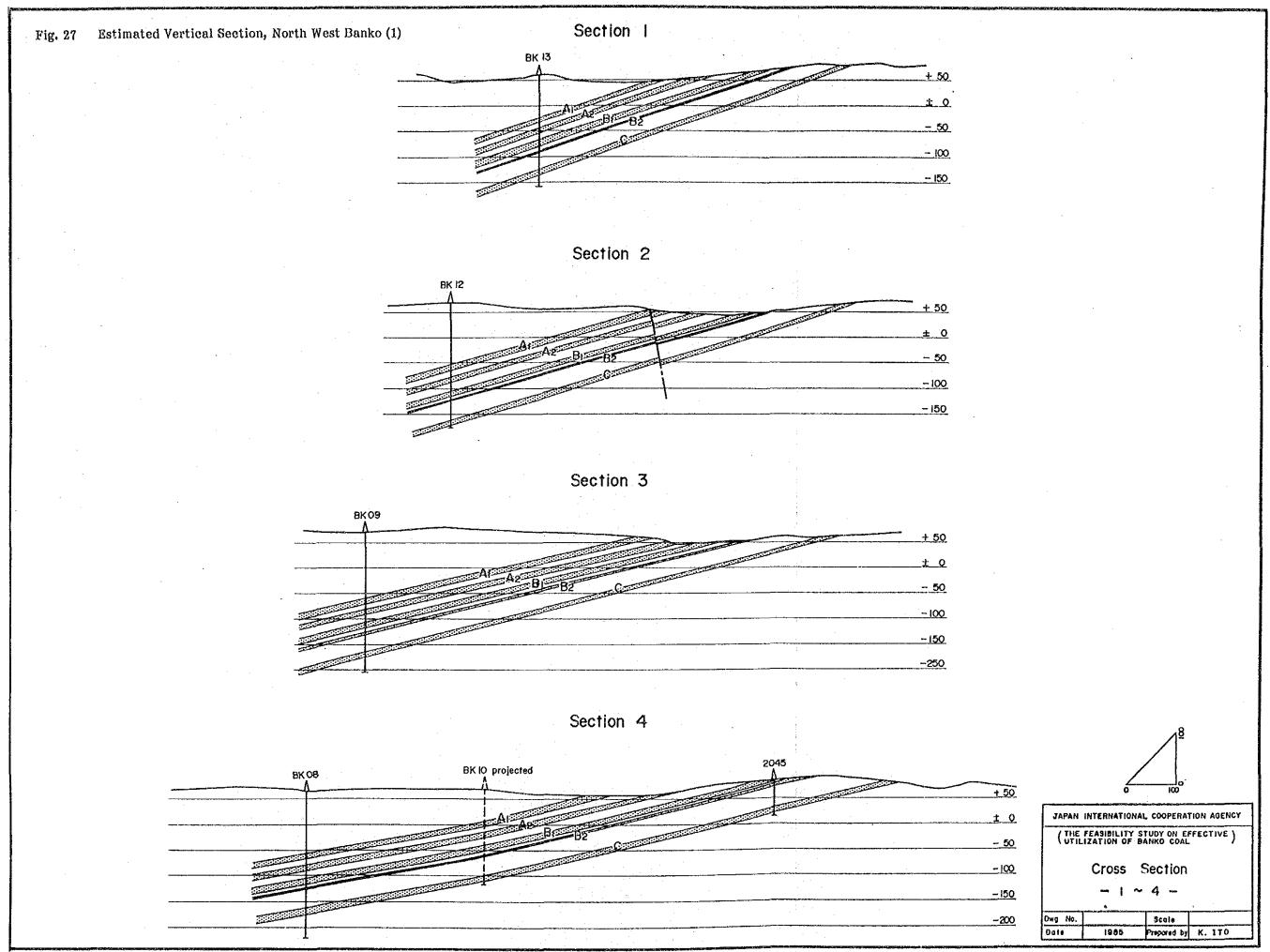
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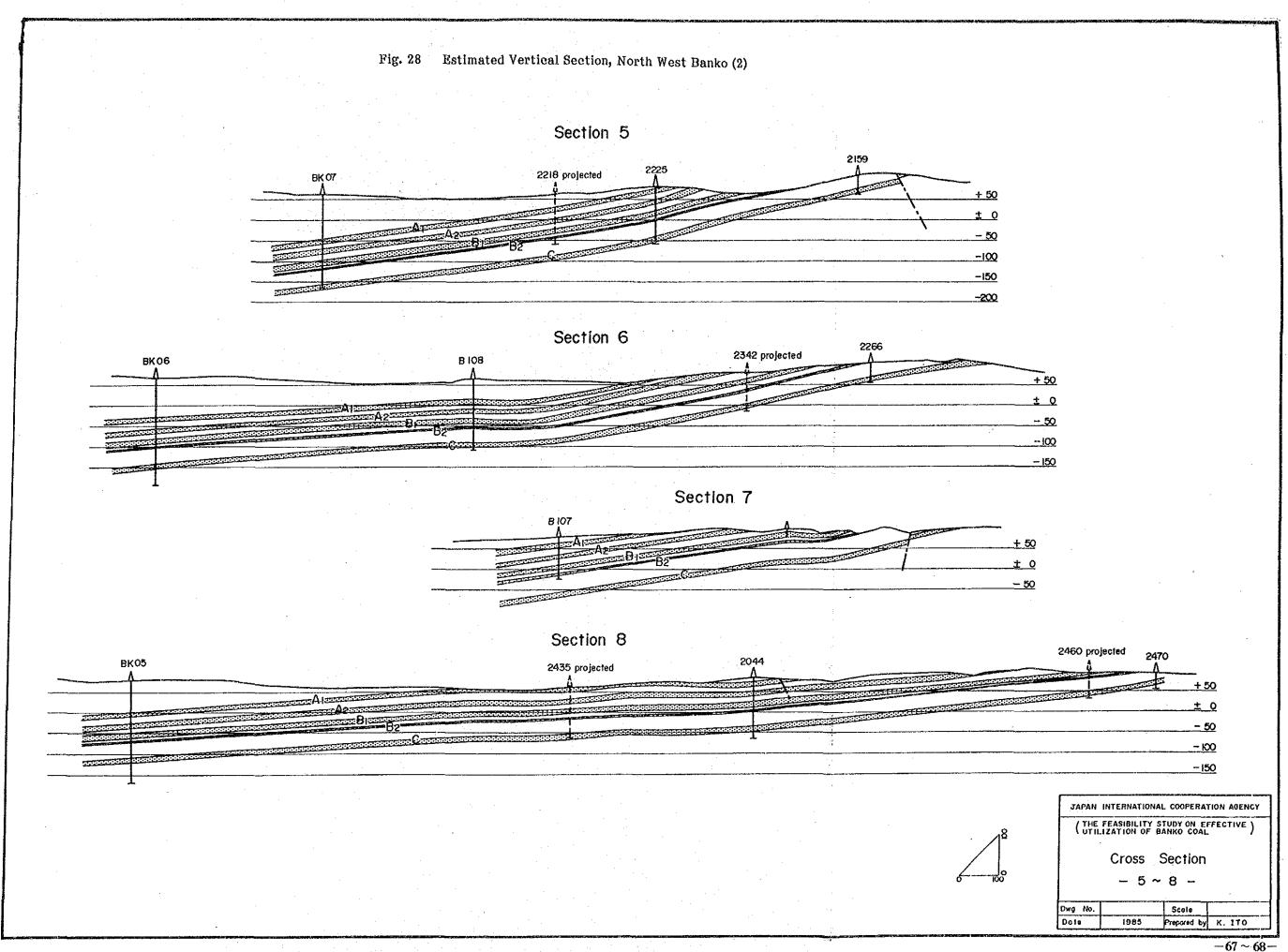
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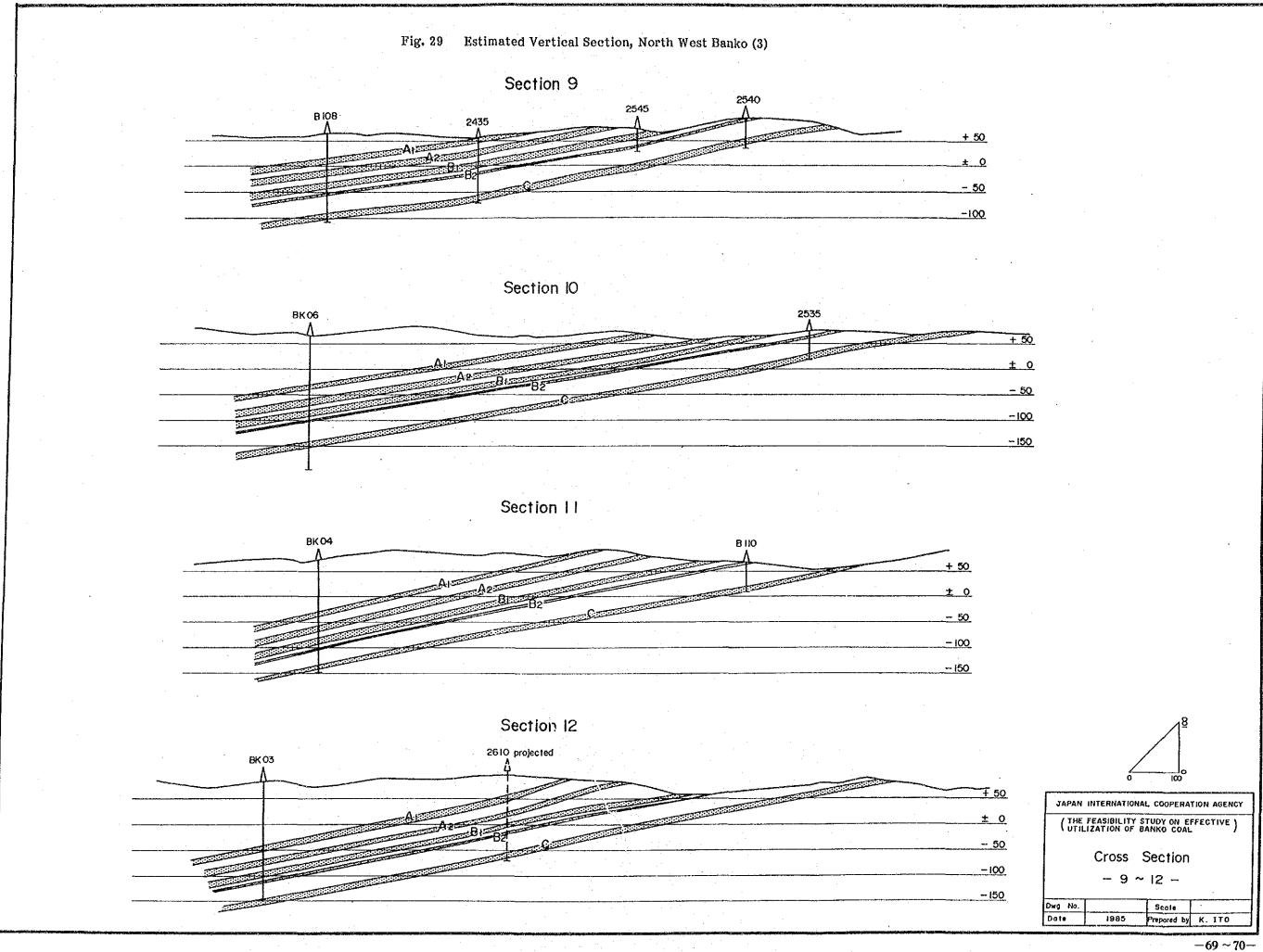
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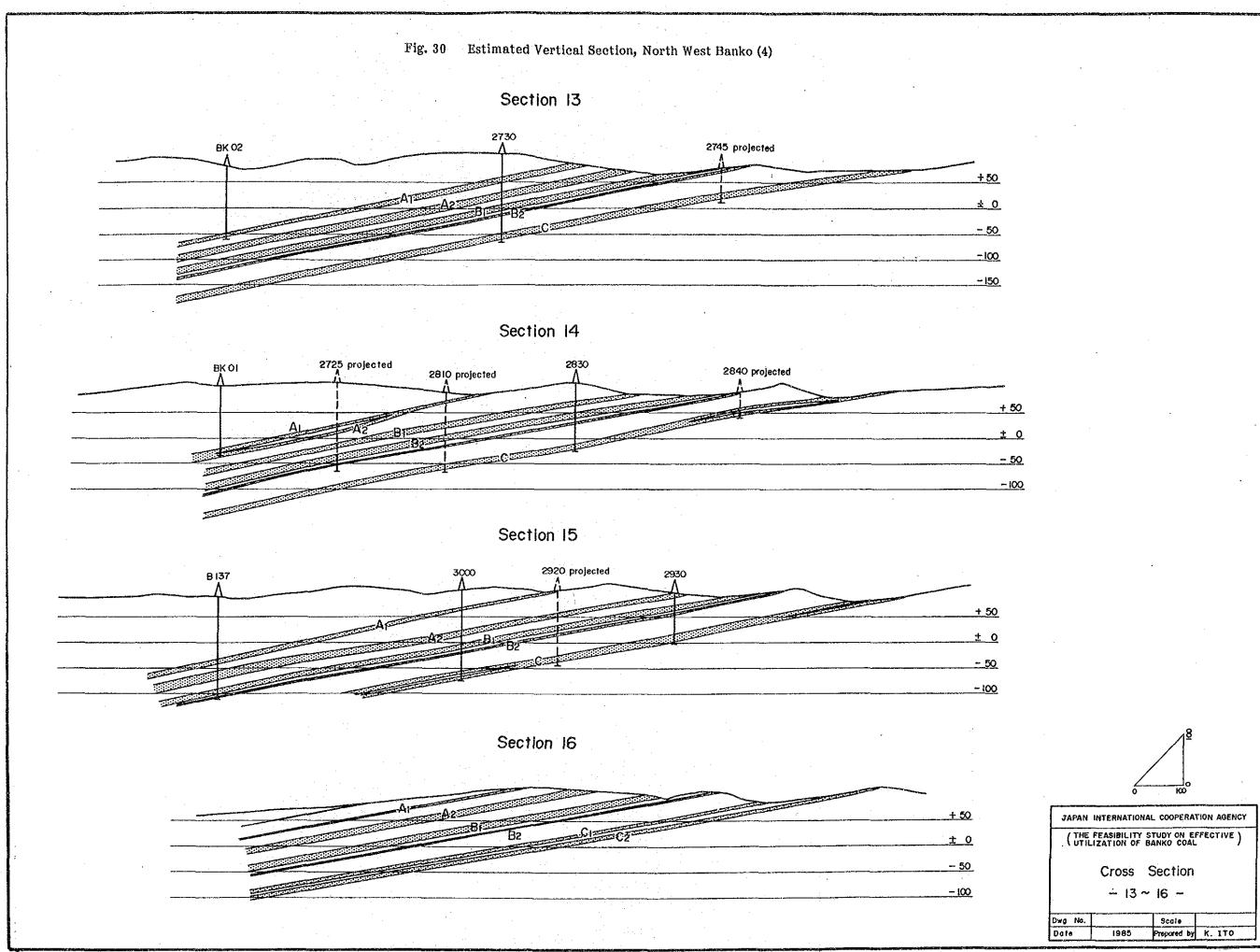
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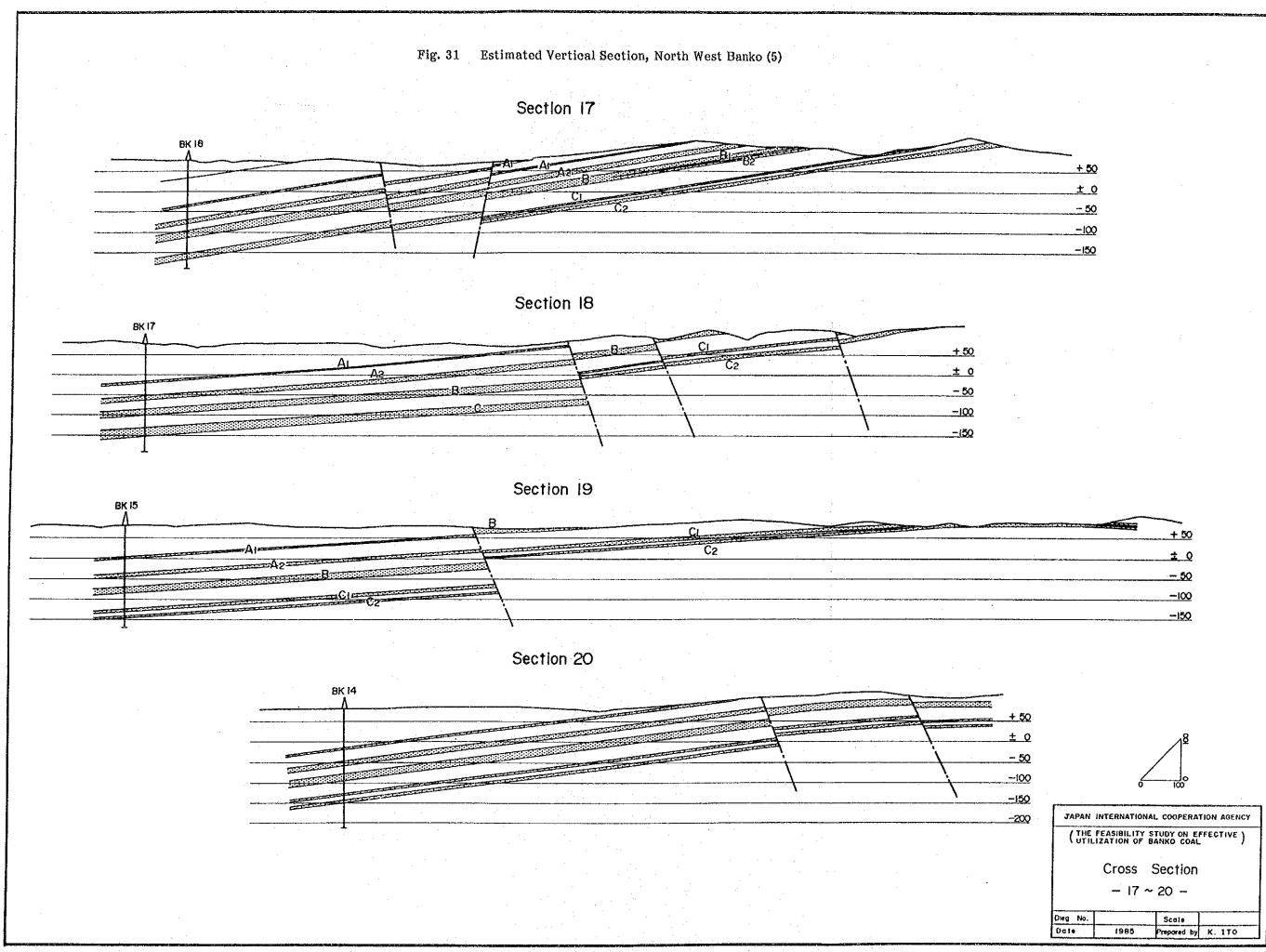
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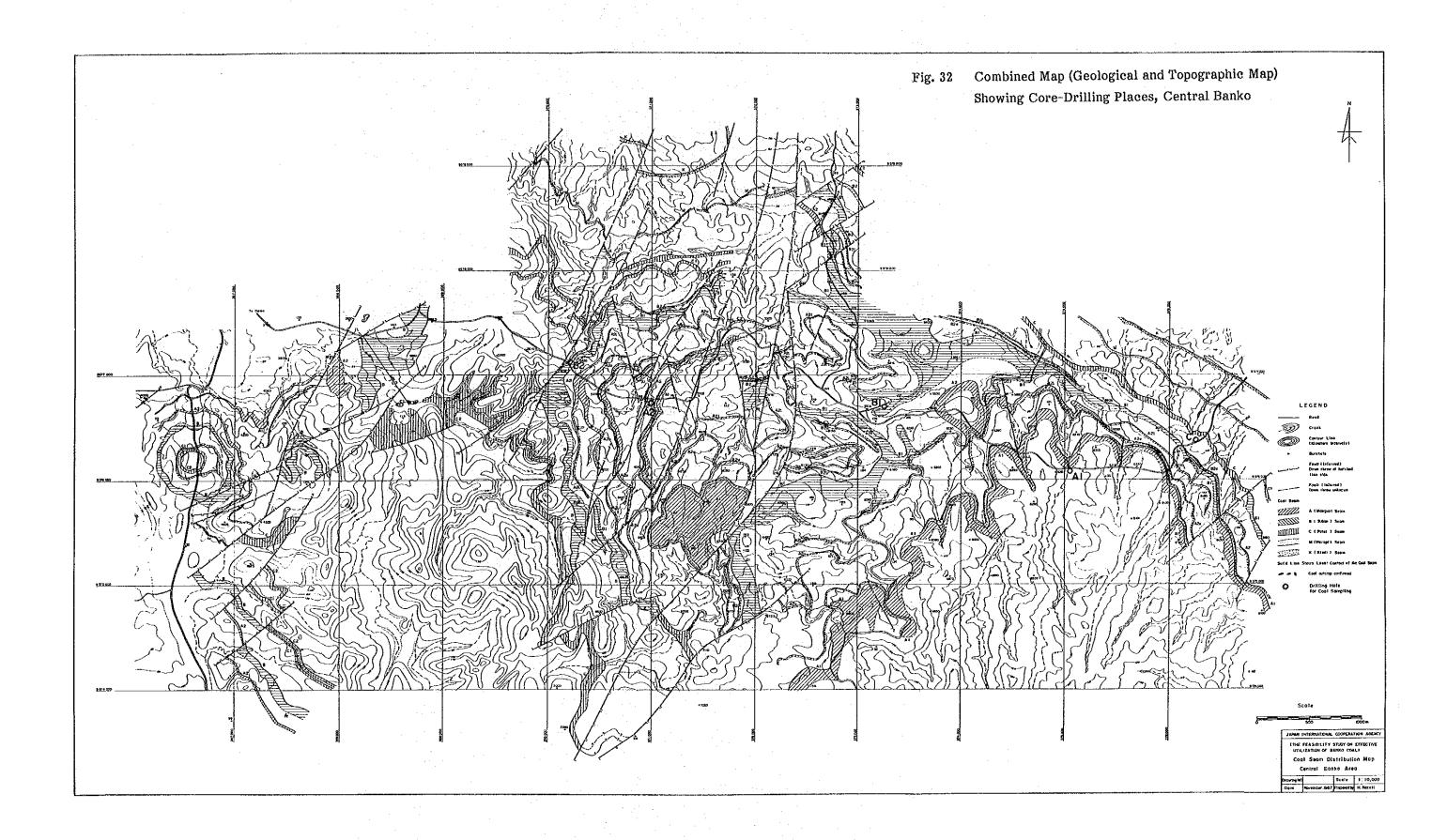


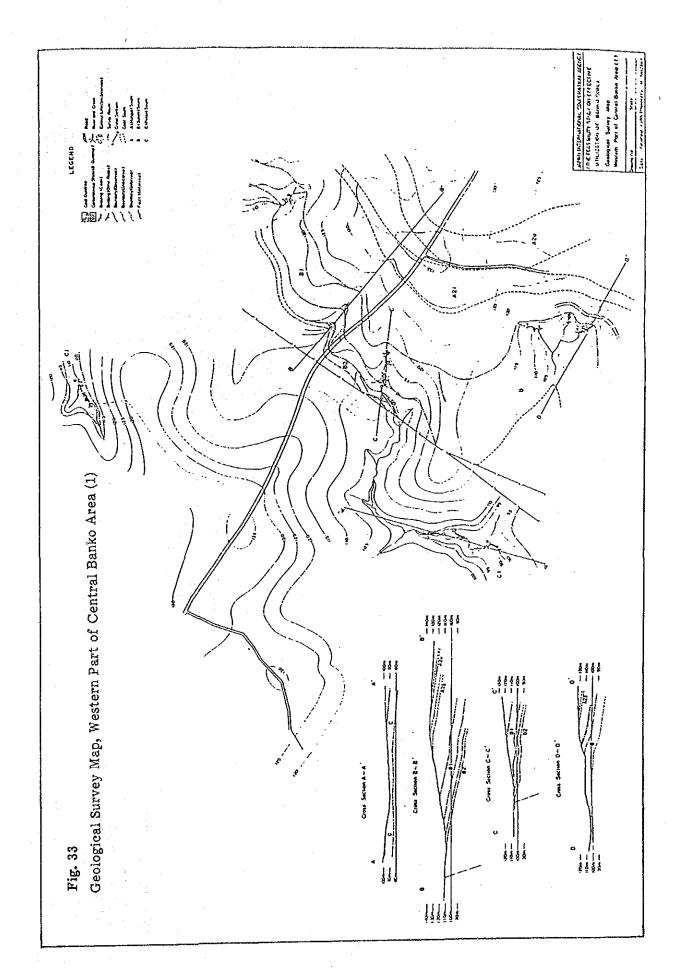


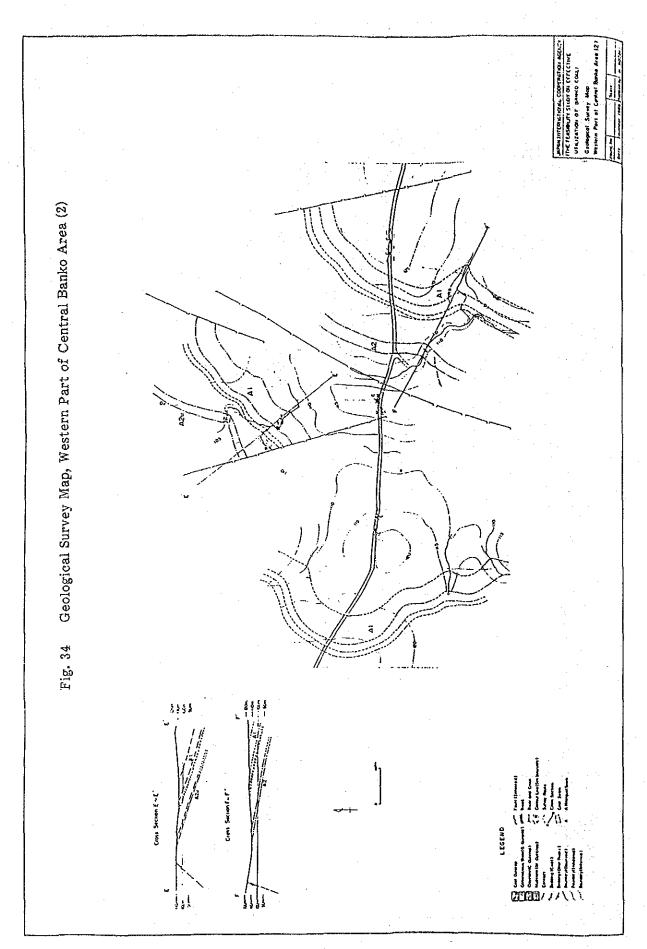












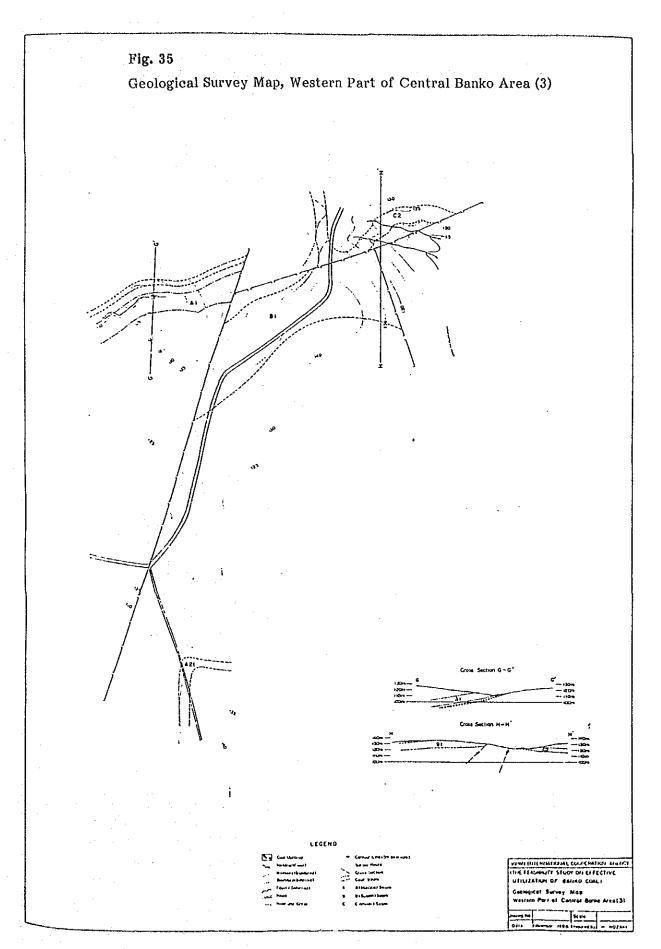


Fig. 36 Geological Survey Map, Central Part of Central Banko Area

