4.5 Distribution of Air Pollutant Emissions

Figures 4.5.1 through 4.5.10 show areal distribution of emission of SOx, NOx and Dust by various sources.

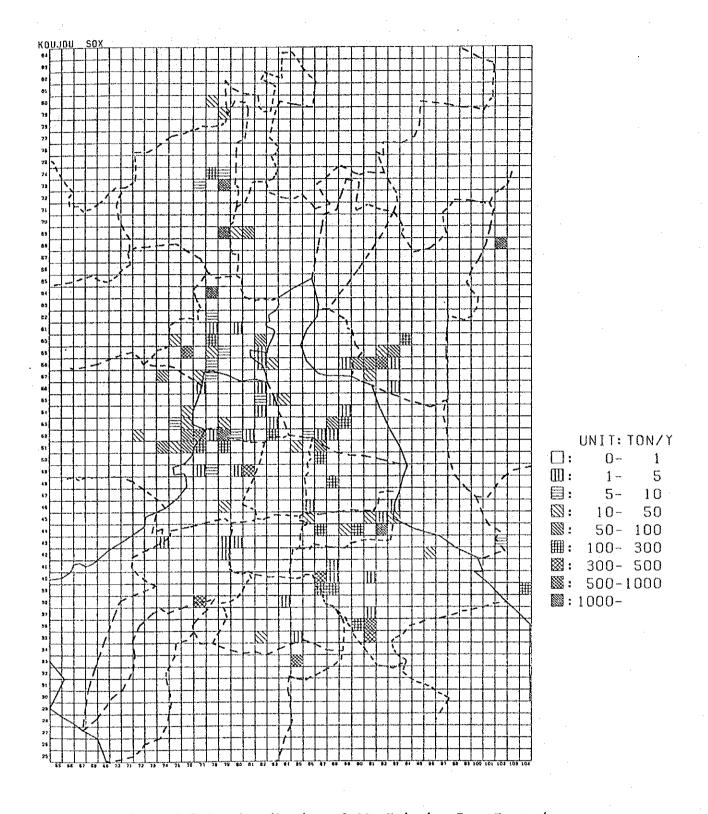


Figure 4.5.1 Distribution of SOx Emission From Factories

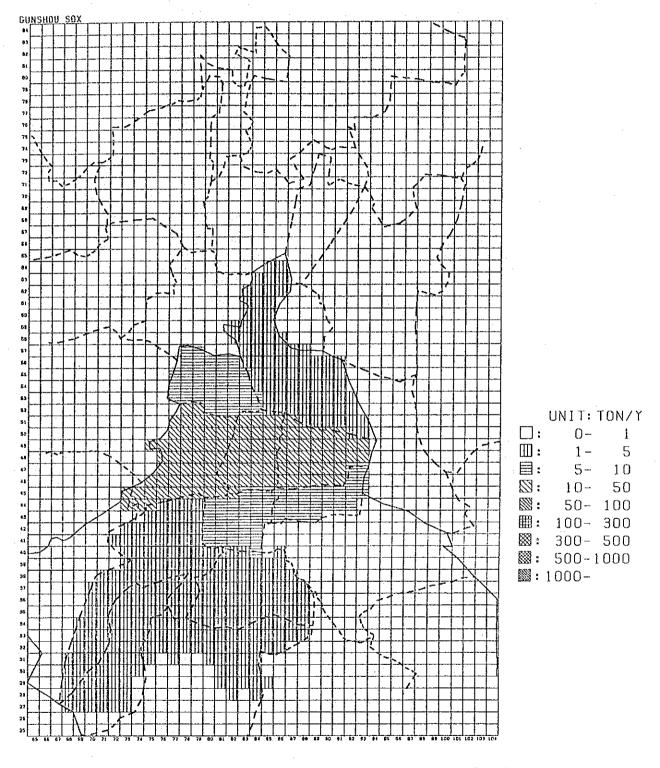


Figure 4.5.2 Distribution of SOx Emission From Service and Commercial Establishments

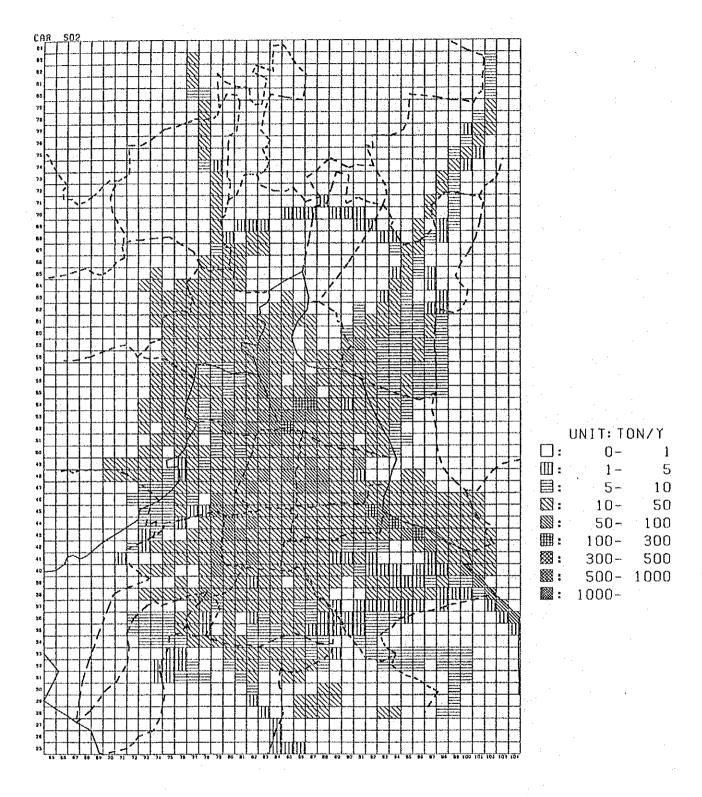


Figure 4.5.3 Distribution of SOx Emission From Automobiles

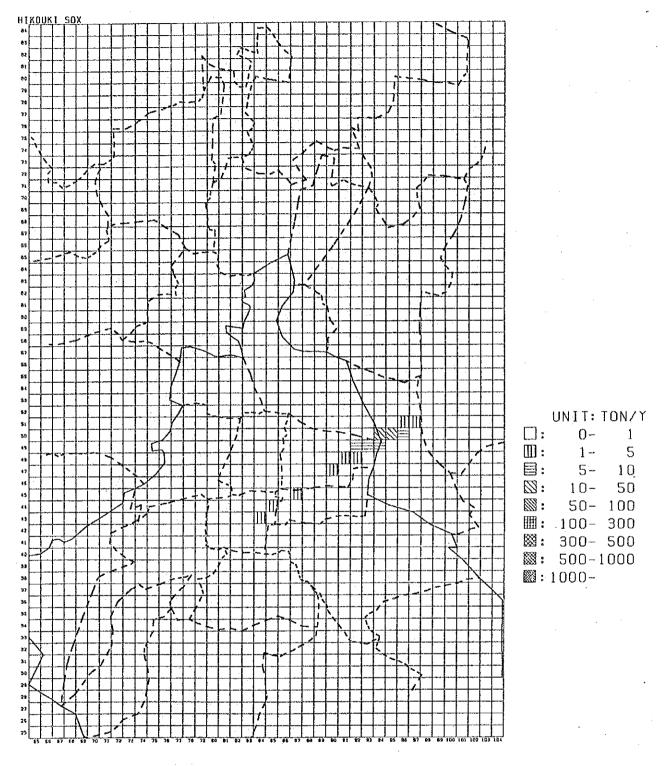


Figure 4.5.4 Distribution of SOx Emission From Airplanes

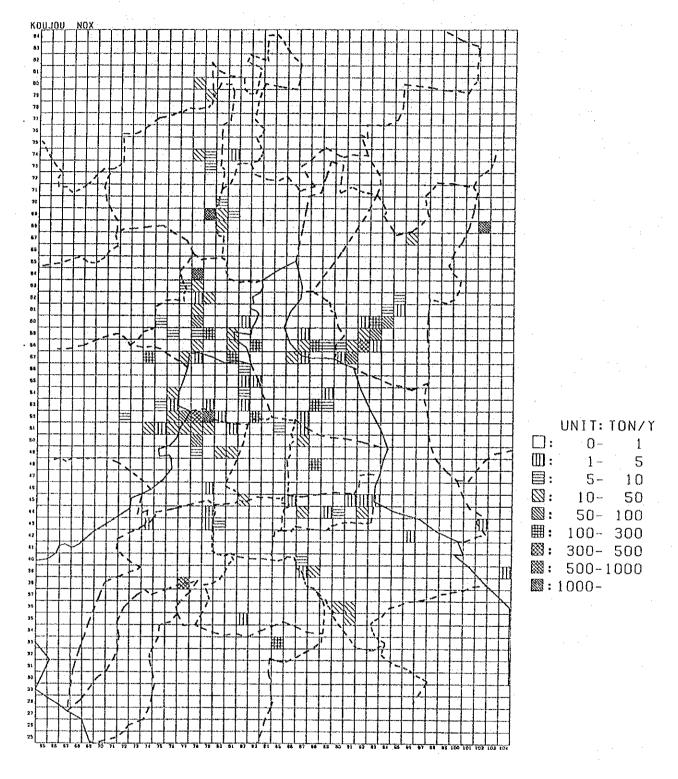


Figure 4.5.5 Distribution of NOx Emission From Factories

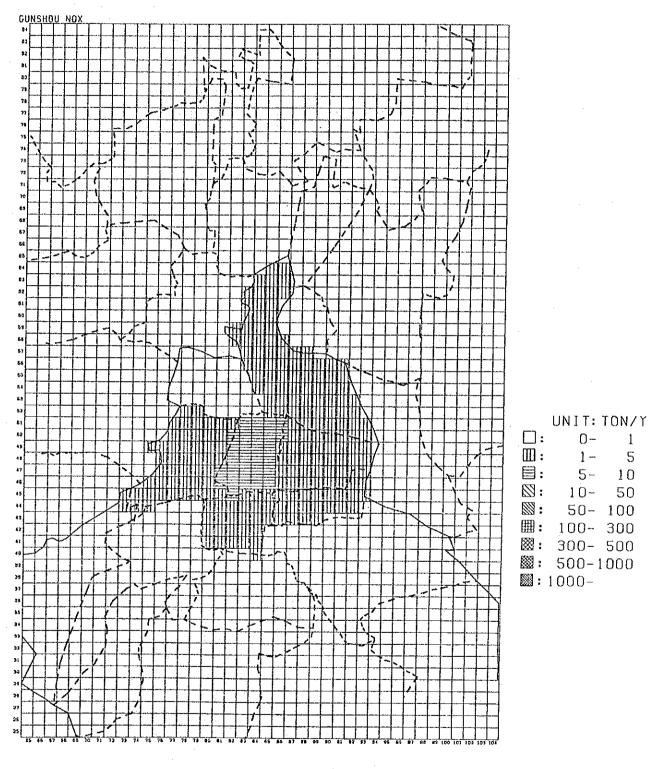


Figure 4.5.6 Distribution of NOx Emission From Service and Commercial Establishments

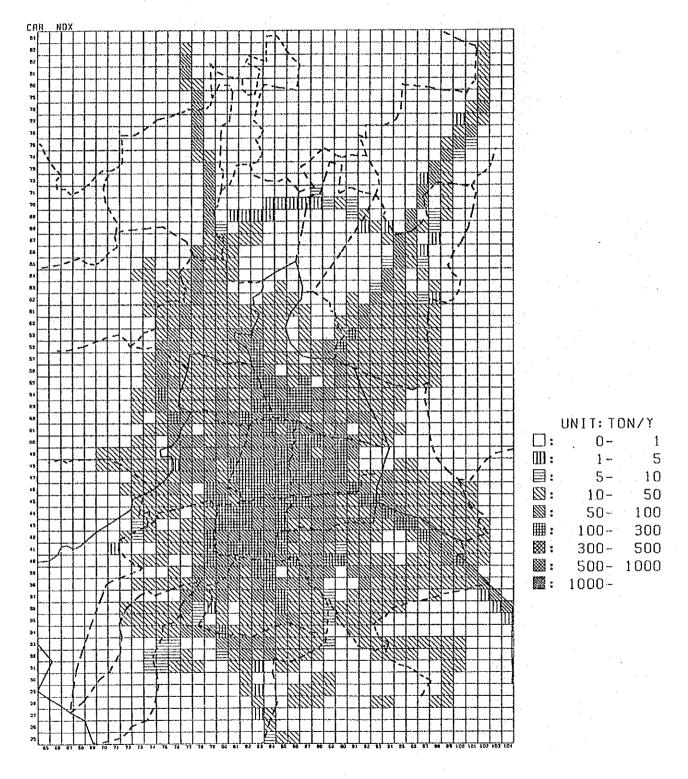


Figure 4.5.7 Distribution of NOx Emission From Automobiles

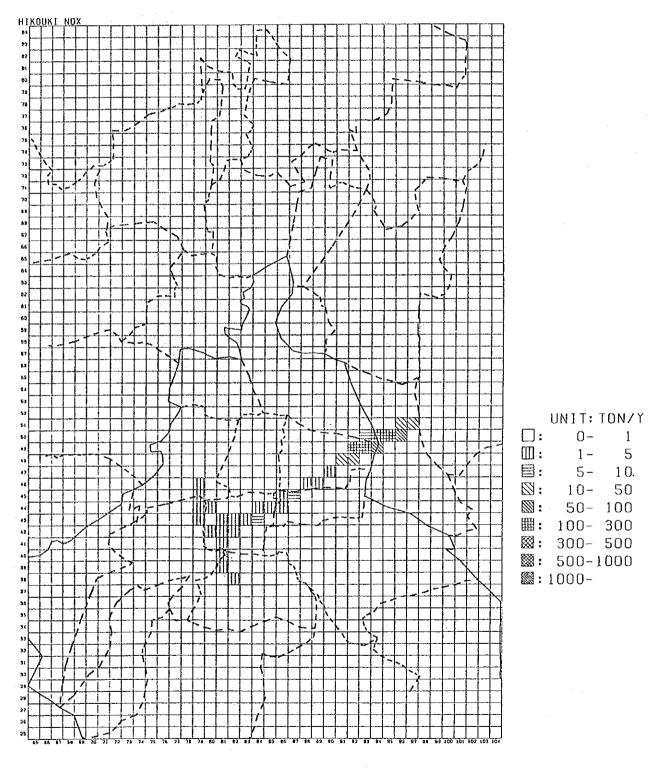


Figure 4.5.8 Distribution of NOx Emission From Airplanes

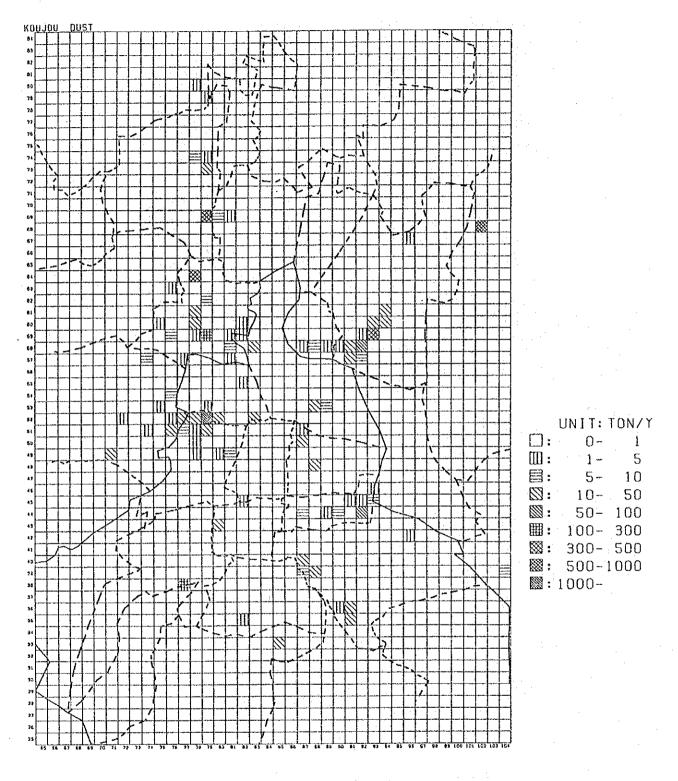


Figure 4.5.9 Distribution of Dust Emission From Factories

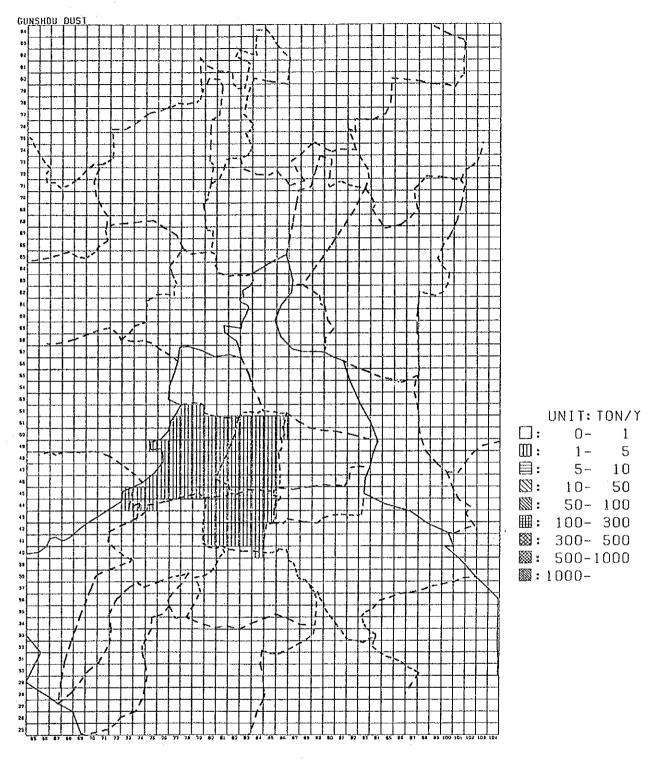


Figure 4.5.10 Distribution of Dust Emission From Service and Commercial Establishments

PART 5 AIR QUALITY SIMULATION

5.1 Air Quality Simulation Under the Present Conditions

5.1.1 Dispersion Model

(1) Effective Stack Height Model

Effective stack height of a source is determined as follows:

He = Ho $+ \Delta H$

He: effective stack height (m)

Ho: actual stack height (m)

Δ H: rise of stack gas (m)

 Δ H is computed by the following methods.

1) Windy condition

For large scale stacks (QH \geq 2 x 10^6 cal/s), the Moses & Carson equation is used.

$$\Delta H + (C_1 V_s D + C_2 Q_H^{1/2})/u$$

Atomospheric Stability	c_1	c ₂
Unstable	3.74	0.33
Neutral	0.35	0.171
Stable	-1.04	0.145

For medium to small scale stacks (Q $_{\rm H}\!<\!2$ x 10^6 cal/s), the CONCAWE equation is used.

$$\Delta H = 0.175 Q_H^{1/2} u^{-3/4}$$

2) Calm condition

The Briggs equation is used.

$$\Delta H = 1.4 Q_H \% (d\theta/dz)\%$$

QH : Heat emission due to efflux of stack gases (cal/s)

ho : Density of emitted gases at 0°C ($\simeq 1.293 \times 10^3 \text{ g/m}^3$)

Q : Emission rate of gaseous effluent (Nm³/S)

 $^{
m C}_{
m p}$: Specific heat at constant pressure (0.24 cal/ $^{
m o}$ K \cdot g))

 $\Delta\,T$: Difference between the temperature of emitted gas (Tg) and

that of atmosphere (OK)

u : Wind speed at the top of stack (m/s)

 $d\theta$ /dz: vertical potential temperature gradient of atmosphere ($^{\rm O}$ K/m) (to be set at 0.003 for daytime and 0.010 for nighttime)

 $\Gamma_{\rm d}$: Adiabatic lapse rate in the atmosphere (0.0098 oK/m)

Vs : Stack gas exit velocity (m/s)

D : Inside stack diameter (m)

(2) Dispersion Equation

Dispersion equations applied for point source, area source, and line source are as follows.

1) Point Source Equation

When windy (u > 0.4 m/s), the following plume equation is used.

C(R. z) =
$$\frac{Qp}{\sqrt{2\pi} \frac{\pi}{8} R\sigma z_{\text{U}}} \cdot [\exp{(-\frac{(z-He)^2}{2\sigma z^2})} + \exp{(-\frac{(z+He)^2}{2\sigma z^2})}]$$

C(R,z): Concentration at the location (R,z)

R : Horizontal distance (m) from a point source to a computation point

Qp : Point source intensity (Nm³/s)

u : Wind speed (m/s)

He : Effective stack height (m)

 σ z : Vertical diffusion parameter (m) (using the Pasquill-Gifford chart)

When calm ($u \le 0.4 \text{ m/s}$), the following puff equation is used.

$$C(x, y, T) = \frac{1}{(2\pi)} \int_{0}^{T} \frac{2Qp}{\sigma y^{2}\sigma z} \exp\left(-\frac{(x-ut)^{2}}{2\sigma y^{2}} - \frac{y^{2}}{2\sigma y^{2}} - \frac{He^{2}}{2\sigma z^{2}}\right) dt$$

A steady-state solution for the calm condition was applied after integrating the above equation up to $t = \infty$, with u = 0, $\sigma y = a t$, and $\sigma z = \gamma t$.

$$C(R, z) = \frac{Qp}{(2\pi)^{3/2} r} \cdot \left\{ \frac{1}{R^2 + \frac{\alpha^2}{r^2} (z - He)^2} + \frac{1}{R^2 + \frac{\alpha^2}{r^2} (z + He)^2} \right\}$$

$$R^2 = x^2 + y^2$$

a , γ : Diffusion parameters for calm

$$\sigma x = \sigma y = \alpha \cdot t$$

$$\sigma z = \gamma \cdot t$$

t: Time lapse (s)

2) Area Source Equation

When windy, the plume equation applicable to long-term average concentration is used, assuming that a square area source with a side 2a long is present in isolation.

$$C = \frac{QA}{\sqrt{2\pi} u} \int_{x-a}^{x+a} \frac{2a}{(\frac{\pi}{8}\xi + 2a) \sigma_z(\xi)} \cdot (F) d\xi$$

$$(F) = \exp \left\{-\frac{(z-He)^2}{2\sigma z(\xi)^2}\right\} + \exp \left\{-\frac{(z+He)^2}{2\sigma z(\xi)^2}\right\}$$

QA : Area source intensity (Nm^3/s)

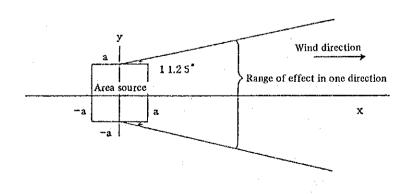
u : Wind speed (m/s)

He : Effective stack height (m)

σ z : Vertical diffusion parameter (m)

2a : Length (m) of a side of a square area source

A conceptual diagram of area source dispersion model is shown below.



When calm, the following equation is used by applying the simplified puff equation (steady-state solution) to a circular area source that has the same area as a square area source with a side 2a long.

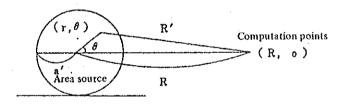
$$C = \frac{QA}{(2\pi)^{3/2}r} \int_{0}^{a'} \int_{0}^{2} \frac{1}{R'^{2} + b_{1}^{2}} + \frac{1}{R'^{2} + b_{2}^{2}}) r \cdot dr \cdot d\theta$$

$$a' = \frac{2a}{\sqrt{\pi}}$$

$$R' = (r^{2} + R^{2} - 2rR\cos\theta)^{1/2}$$

$$b_{1} = \frac{\alpha}{r} (z - He), \quad b_{2} = \frac{\alpha}{r} (z + He)$$

A conceptual diagram of area, source diffusion model is shown below.



Line Source Equation

When windy, the 2 π /16 equation which brings uniform concentration in the direction of y is used.

$$C = \begin{cases} r_z & Q_L \\ r_1 & \frac{\pi}{\sqrt{2\pi} \cdot \frac{\pi}{8}} r \sigma z (r) u \end{cases} \cdot \left[\exp \left\{ -\frac{(z - He)^2}{2\sigma z (r)^2} \right\} + \exp \left\{ -\frac{(z + He)^2}{2\sigma z (r)^2} \right\} \right) \cdot dr$$

: z coordinate (m) at the computation point

r : Distance (m) from the computation point to a line source

rl, r2: Integration interval (m) of a line source

QL : Line source intensity (Nm³ / s.m)

u : Wind speed (m/s)

He : Effective stack height (m)

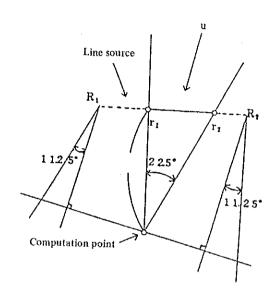
oz: Vertical diffusion parameter (m)

When calm, the following equation is used.

$$C = \int_{R_1}^{R_2} \frac{Q_L}{(2\pi)^{3/2} r} \left(\frac{1}{r^2 + b_1^2} + \frac{2}{r^2 + b_2^2} \right) dr$$

$$b_1 = \frac{\alpha}{r} (z - \text{He})$$
 $b_2 = \frac{\alpha}{r} (z + \text{He})$ $r^2 = x^2 + y^2$

R1, R2: Integration interval (m) of a line source as shown below



(3) NO-NO₂ Conversion Equation

For NO-NO2 conversion, the following exponential analogue equation will be used.

$$(NO_1) = (NO_1)_D \left(1 - \frac{\alpha}{1+\beta} \{\exp(-Kt) + \beta\}\right)$$

$$K = k \cdot u \{O_1\}_B$$

a : Initial ratio

 β : Coefficient to approximate equilibrium condition

k : Reaction constant

[03] B : Background concentration of 03 (ppm)

Parameters were set as shown below:

a: Factories
Service and commercial
establishment
Airplanes
Automobiles

β: Day time 0.3
Night time 0.0

k: Factories
Airplanes
(Climb, Approach/Landing)

0.83

0.80

0.80

(Climb, Approach/Landing)

Service and Commercial
Establishment 0.062

Airplanes
(Taxing/idling, Take-off)

Automobiles 0.23

Background concentration of O3 is set as shown in Table 5.1.1.

Table 5.1.1 Background Concentration of 03

Background Concentration of 03

(Unit:PPN)

Find Sp	eed Classes		0. 5	2. 0	3. 0	4.0	6.0	8.0	10.
(m/s)	١	ſ	ſ	ſ	. }	}	ş	}
Period	Time Zone	0. 4	1. 9	2. 9	3. 9	5. 9	7. 9	9. 9	
	Morning	0. 041	0. 041	0. 054	0. 039	0. 039	0. 039	0. 039	0. 039
Rainy	Afternoon	0.067	0. 067	0. 054	0.046	0. 036	0. 036	0. 036	0. 036
	Evening	0.012	0.012	0. 017	0. 021	0. 029	0. 020	0. 020	0. 020
	Midnight	0.013	0.013	0.014	0. 021	0. 021	0. 021	0. 021	0. 021
	Morning	0.043	0.043	0.056	0.050	0. 035	0. 035	0. 035	0. 035
Dry	Afternoon	0. 081	0. 081	0. 072	0. 050	0. 042	0. 039	0. 034	0. 032
	Evening	0.014	0. 014	0. 020	0. 022	0. 024	0. 027	0. 027	0. 027
	Midnight	0.013	0. 013	0.017	0. 024	0. 030	0. 030	0. 030	0.030

5.1.2 Evaluation of the Dispersion Model

The conditions given in Table 5.1.2 can be used to judge the agreement between computed and measured values, thereby evaluating the credibility of the dispersion mode. The SEDUE data of 1986 may be used as measured values, but these data are not enough to ensure adequate calibration of the model because of insufficient measuring achievements (the measurement time reached only about 6,000 hours a year even in a measuring station with good achievements). Therefore, the evaluation conditions in Table 5.1.2 will be regarded as the goal toward which efforts should be made.

Table 5.1.2 Conditions for Evaluation of the Accuracy of the Dispersion Model

- Individual conditions pertaining to the conformity between calculated and measured values.
- (1) a,≤1/3 (Ÿ-BG) +BG
- (2) $c_0 \leq \frac{1}{2} (\vec{Y} BG) + BG$
- 3. The inclination of a regressing line shall range from 0.8 to 1.2 and be as close to 1 as possible. In addition, the correlation coefficient shall be at least 0.71 and should possibly exceed 0.8.
- (4.) s'/Y ≤ 1/3
- (5.) s'/ٲ¼
- (6.) s'/\square

Y : Mean measured value available from a measuring station

X : Mean computed value for the measuring station

 $a_0 : \overline{Y} + \overline{X}$

BG : Background values in the nature

s'/Y : Variation coefficient obtained from Y = X/ao

- Accuracy ranking pertaining to the conformity between computed and measured values
- (a) Rank A

Either the conditions (1), (3), and (5), or (1) and (4), stated above, be satisfied. Even if the conditions (1) and (4) are satisfied, the inclination of a regressing line should be as close to (1) as possible.

(b) Rank B

The conditions (2) and (5) shall be satisfied.

(c) Rank C

The conditions (2) and (6) shall be satisfied.

Note: It is desired that the inclination of regressing lines should also be as close to 1 as possible in the caseses of Ranks B and C.

5.1.3 Computation Results for Present Ambient Air Quality

Figures 5.1.1 shows computed ambient concentration of SO₂ corresponding to all the sources. Figures 5.1.2 through 5.1.4 show contribution of each category of source to SO₂ concentration.

Figure 5.1.5 shows computed ambient concentration of CO corresponding to automobile emissions.

Figure 5.1.6 shows computed ambient concentration of NOx corresponding to all the sources. Figures 5.1.7 through 5.1.9 show contribution of each category of source to NOx concentration.

Figure 5.1.10 shows computed ambient concentration of NO_2 corresponding to all the sources. Figures 5.1.11 through 5.1.13 show contribution of each category of source to NO_2 concentration.

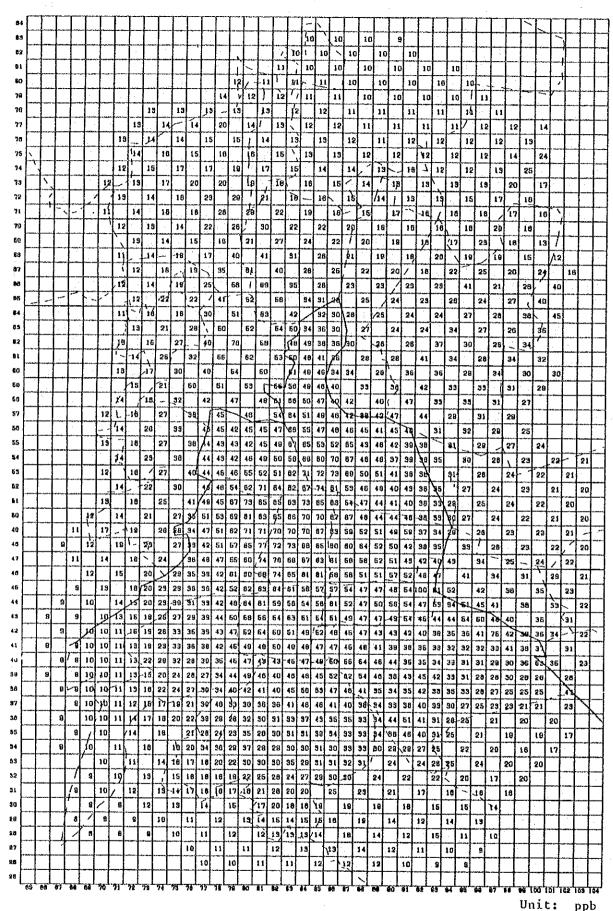


Figure 5.1.1 Ambient Concentration of SO₂ (Present, All Sources) (Background concentration of 5.87 ppb included)

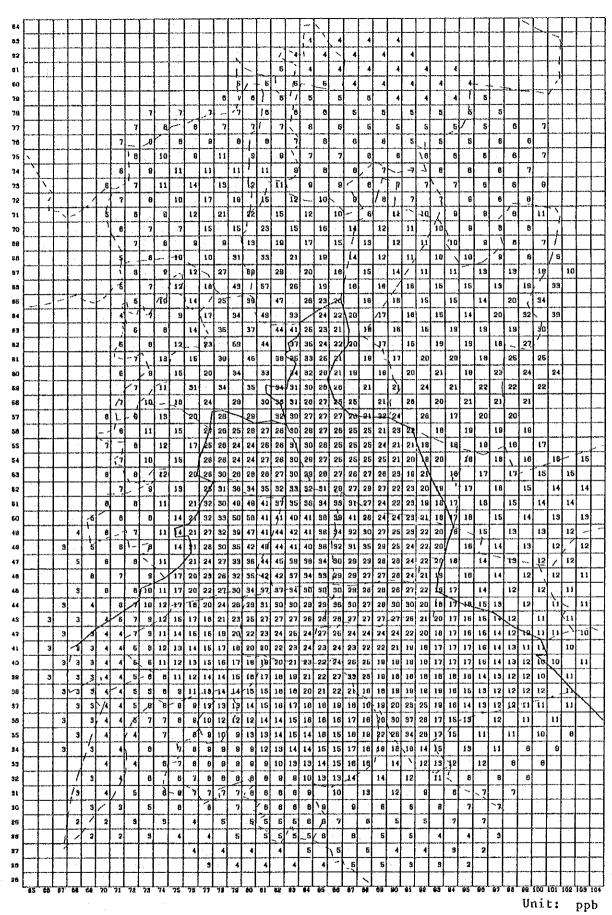


Figure 5.1.2 Contribution of Stationary Sources to SO₂ Concentration (Present)

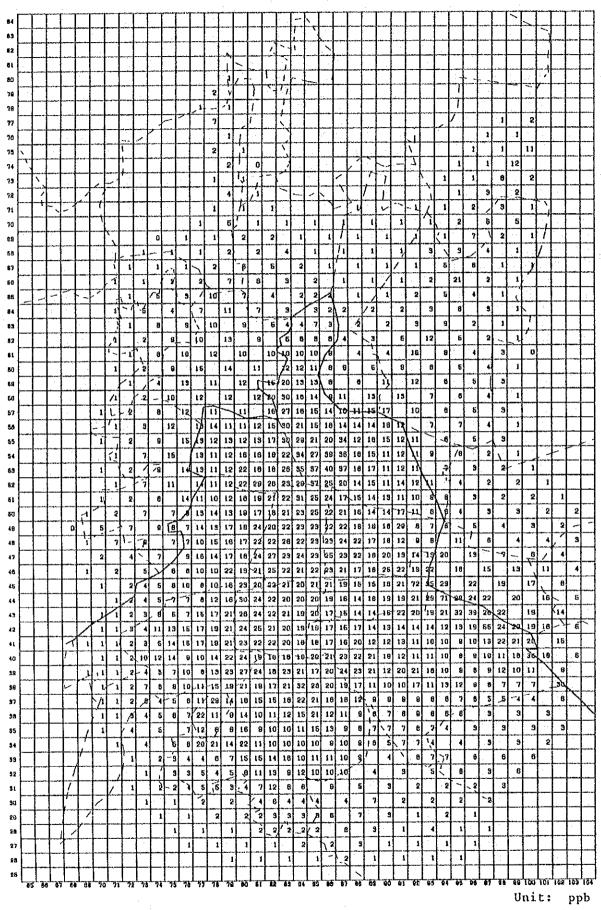


Figure 5.1.3 Contribution of Automobiles to SO2 Concentration (Present)

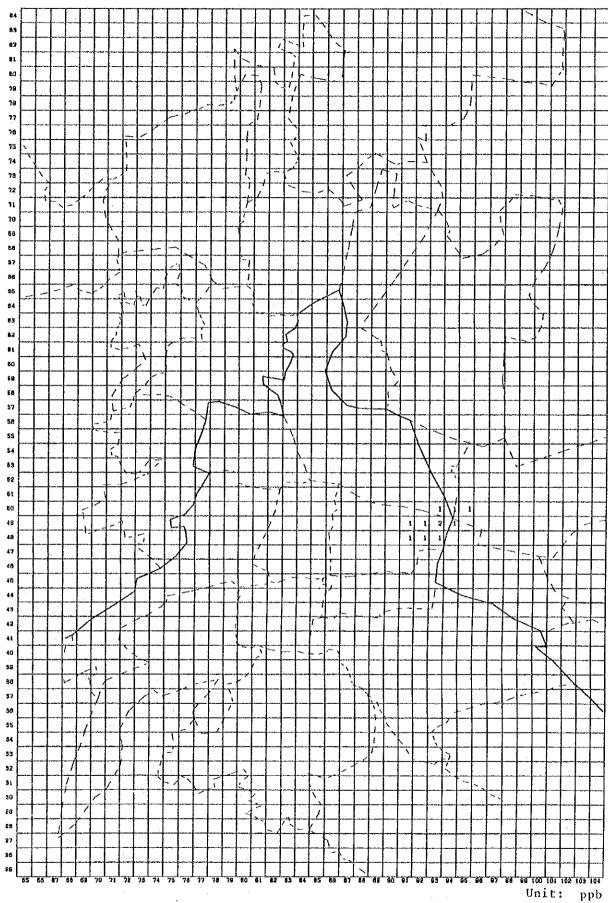
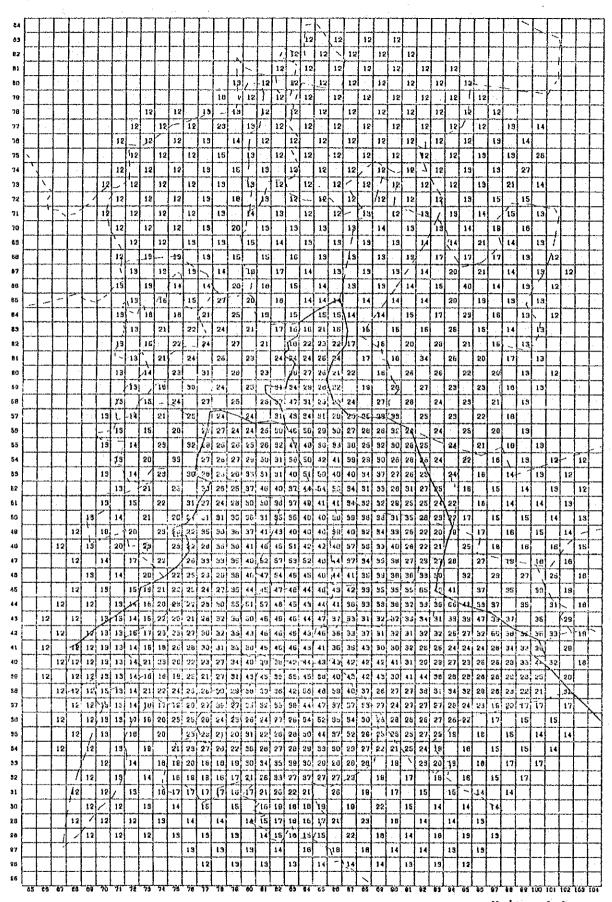


Figure 5.1.4 Contribution of Airplanes to SO₂ Concentration (Present)



Unit: 0.1 ppm Figure 5.1.5 Contribution of Automobiles to CO Concentration (Present) (Background concentration of 1.182 ppm included)

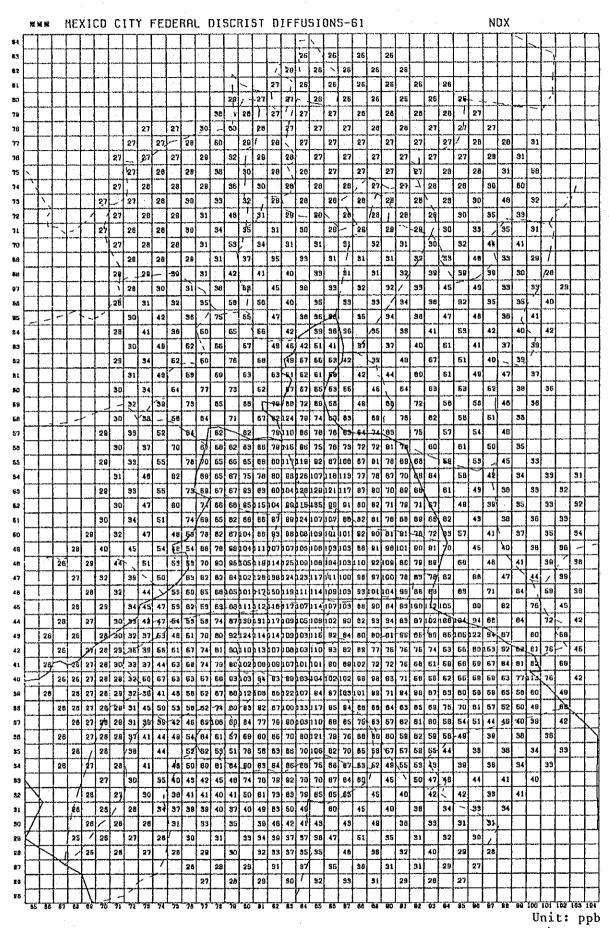


Figure 5.1.6 Ambient Concentration of NOx (Present, All Sources) (Background concentration of 24.43 ppb included)

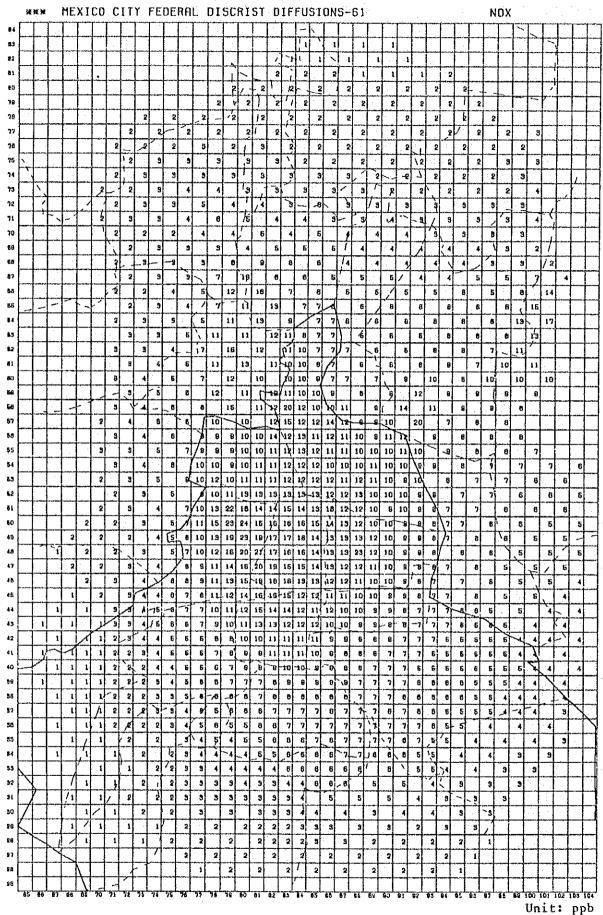


Figure 5.1.7 Contribution of Stationary Sources to NOx Concentration (Present)

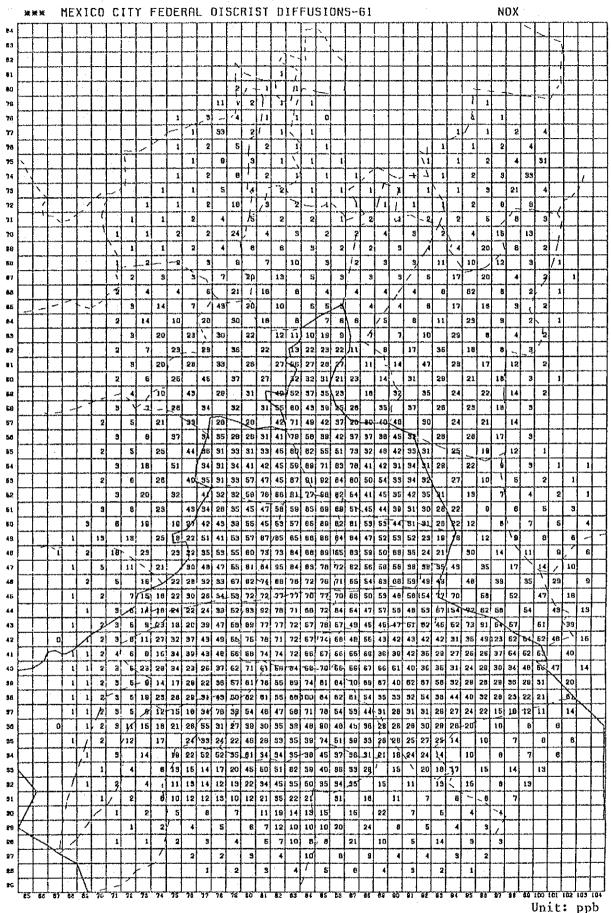


Figure 5.1.8 Contribution of Automobiles to NOx Concentration (Present)

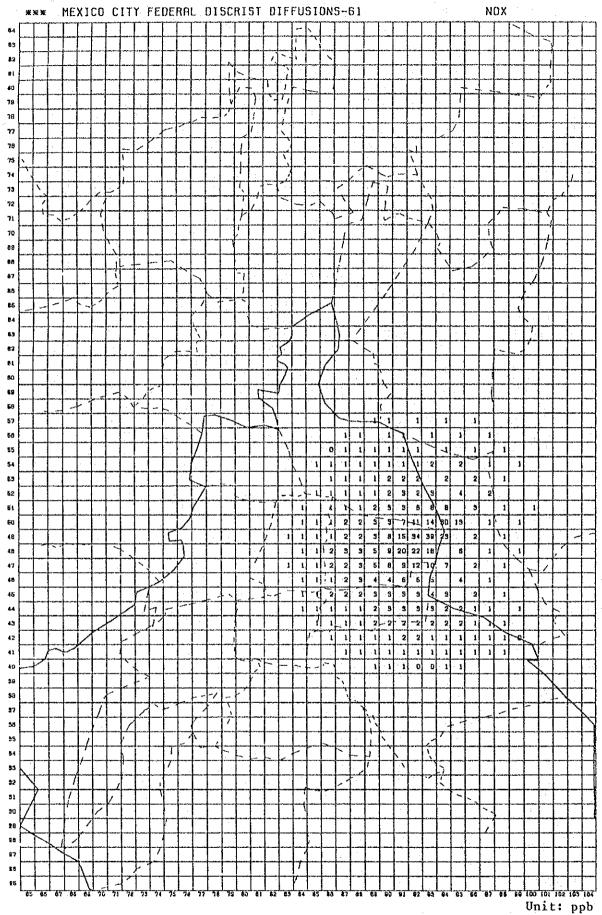


Figure 5.1.9 Contribution of Airplanes to NOx Concentration (Present)

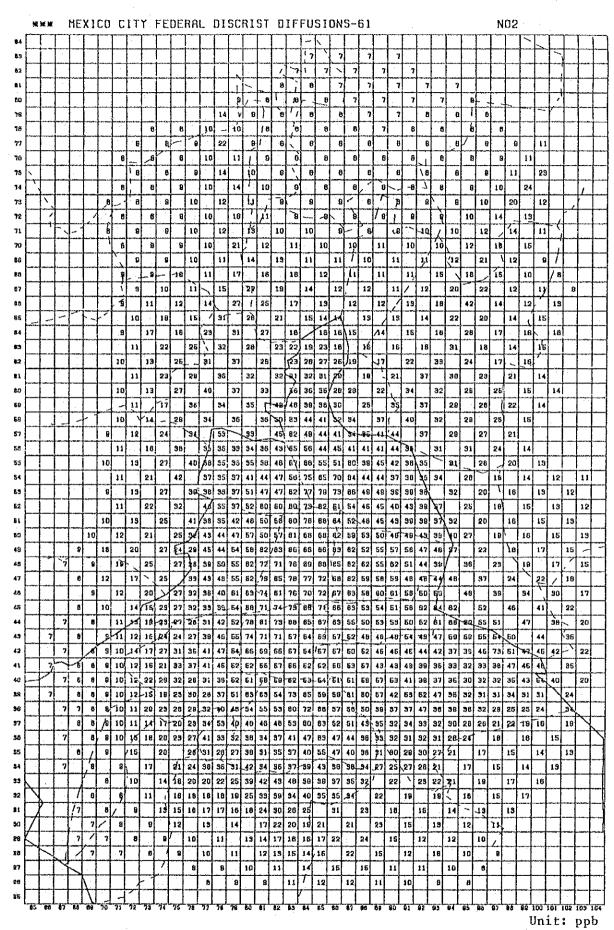


Figure 5.1.10 Ambient Concentration of NO₂ (Present, All Sources) (Background concentration of 6.06 ppb included)

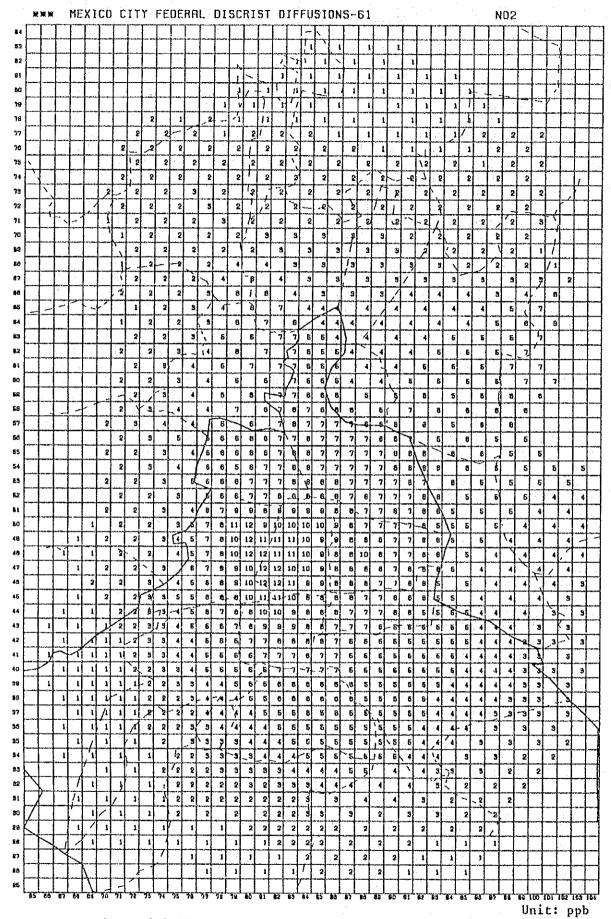


Figure 5.1.11 Contribution of Stationary Sources to NO₂ Concentration (Present)

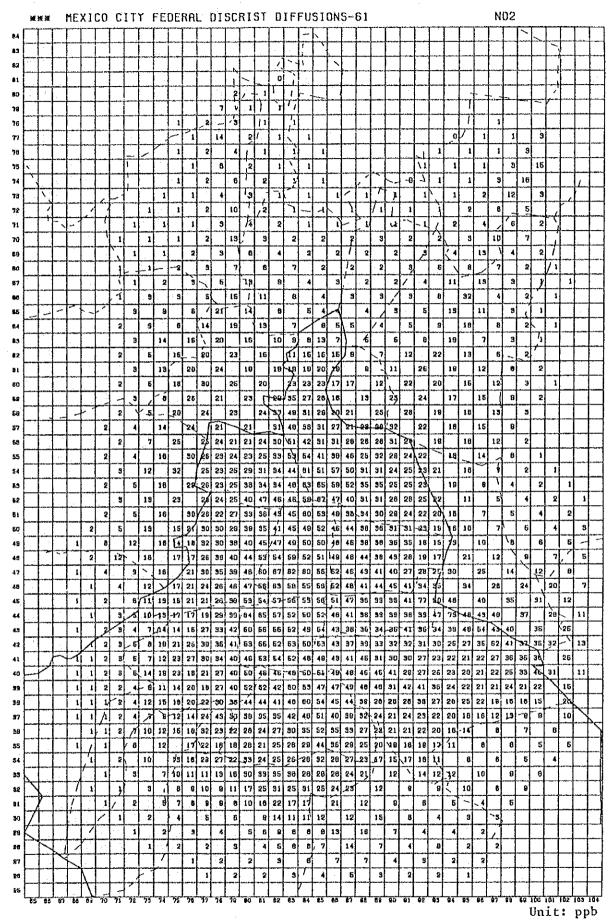


Figure 5.1.12 Contribution of Automobiles to NO2 Concentration (Present)

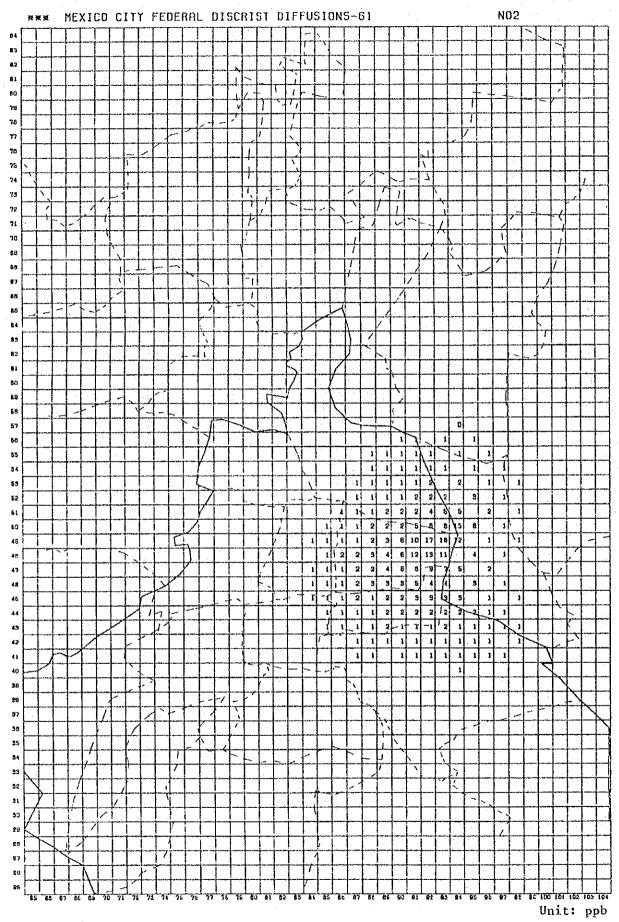


Figure 5.1.13 Contribution of Airplanes to NO₂ Concentration (Present)

5.2 Chemical Mass Balance Method for Analysis of TSP Sources

(1) Method of Analysis

Ambient concentration Ci of an element i can be expressed as follows:

$$C_{i} = \sum_{j=1}^{p} m_{j} \cdot x_{ij} \cdot \alpha_{ij}$$

 $m_{\frac{1}{2}}$: Ambient concentration contributed by the source j ($\mu g/m^3$)

X_{ij} : Ratio of the element i in particulates emitted from the source j (g/g)

ij : Coefficient for fractionation of the element i emitted from the source j in the course it reaches the ground

When several elements whose fractionation coefficient is assumed to be 1 are selected, the above equation reduces to the following. Knowing Ci and X_{ij} , contribution of the source (m_j) can be obtained through the least-square method.

$$C_{i} = \sum_{j}^{p} m_{j} \cdot x_{ij}$$

The following weighted least-square equation is used.

$$x^{2} = \sum_{i=1}^{n} \frac{\left(C_{i} - \sum_{j=1}^{n} m_{j} \cdot x_{i,j}\right)^{2}}{C_{i}^{2}}$$

(2) Input Data

1) Metallic Element Composition of Suspended Particulates

TSP samples collected by Andersen high volume air sampler at the 5 stations for 4 days monthly are analyzed for 10 selected metallic elements. Concentration of the elements and TSP in each station averaged over the entire period is shown in the following Table.

Metallic Element Composition of Suspended Particulates at Each Station (μ_g/m^3)

Element	O. CENTRAL	TACUBA	SANAGUSTIN	PEDREGAL	ESTRELLA
Fe	3.53	2.15	3,50	2.45	3.24
Zn	0.65	0.68	0.41	0.19	0.41
Ni	0.01	0.01	0.91	0.01	0.01
Pb	1.03	0.52	0.34	0.40	0.41
v	0.09	0.11	0.05	0.05	0.06
Mn	0.11	0.13	0.10	0.06	0.07
Na	2.04	1.07	1.46	0.66	0.65
Ca	4.12	2.04	3.70	1.99	4.08
ĸ	0.91	0.33	1.10	0.60	0.78
Αl	2.03	1.79	4.76	2.04	3.32
TSP	183.0	146.2	182.6	110.0	313.9

2) Metallic Element Composition of Particulates at Various Sources

Dust samples were collected at various sources in Mexico City
as shown below. Content of each element was determined for
these samples using an atomic absorption spectrophotometer.

Soil : Cement (Rotary kiln)

Sintering furnace: One rotary kiln for cement

Melting furnace : 4 glass melting furnaces

Drying oven : 9 ovens of various types

Metal smelting

furnace : One electric furnace and 4 cupolas

Boiler : One 45 ton/hr boiler

Automobiles : Exhaust particulates from automobiles in

Mexico City

Content of the elements in particulates sampled at the above mentioned sources is shown in the following Table.

Metallic Element Content in Particulates at Various Sources (%)

Element	Soil	Cement sintering furnace	Glass melting furnace	Drying oven	Metal smelting furnace	Boiler	Automobiles
1 Fe	1.7800	0.8360	1.0200	0.5040	8.7000	0.7460	0.0055
2 Zn	0.0071	0.5190	0.2300	0.1620	5.4900	0.0023	0.1340
3 Ni	0.0022	0.0000	0.0706	0.0639	0.0118	0.2830	0.0002
4 Pb	0.0020	0.4390	2.2900	0.1170	5.8800	0.0105	0.0660
5 V	0.0032	0.0000	0.0000	0.3870	0.0000	0.7490	0.0180
6 Mn	0.0347	0.0585	0.0308	0.0032	1.1700	0.0062	0.0000
7 Na	0.2090	0.0000	39.4000	8.1100	1.8100	0.1150	0.5050
8 Ca	2.6200	22.7000	0.4020	0.0842	3.3200	0.0000	0,0073
9 K	0.3050	0.1730	3.2100	0.2800	2.7900	0.0059	0.0447
10 A1	2.7200	1.4500	5.8500	10.5000	2.2300	0.0894	0.1010