8-4-2 Fuel Ethanol

(1) Market and Steps for Introduction

Market and steps for introduction will be discussed separately for penetration and ultimate stages.

1) Penetration Stage

For Jakarta and vicinity, anhydrous ethanol will be mixed in regular gasoline at the rate of 10%. The octane value improvement effect of anhydrous ethanol enables to substitute lead tetraethyl used heretofore which not only reduces the amount of gasoline consumption but expected to improve environmental effect.

Amount of ethanol consumption is estimated at 160 x 10³ kl.

2) Ultimate Stage

For the entire Republic of Indonesia, anhydrous ethanol will be mixed in regular gasoline at the rate of 20%.

This not only enables reduction of gasoline consumption but is expected to improve the environment the same as that for penetration stage. Ethanol consumption is estimated at $950 \times 10^3 \text{k}\text{i}$.

(2) Production Program

Production program fo fuel ethanol will be separately discussed for penetration and ultimate stages.

1) Penetration Stage

As stated earlier, required amount of fuel ethanol is about 160×10^3 kl/year in the penetration stage.

i) Raw materials

Main raw materials for producing about 160 x 10³ kl/year of ethanol include cassava, sugar cane, molasses, sweet potato and sago palm.

o Cassava

BPPT is running a test plant of 8 kl/day capacity at Sulusuban, Sumatra Island, under grant aid from Japan and technical problems related to ethanol plant have been solved. However, for a commercial plant operation, farms growing cassava around ethanol production plant must be secured. Additionally, since it takes

quite a while for the farmers to fully learn how to grow cassava, cassava should be considered as raw material for ultimate stage rather than for penetration stage.

o Sugar Cane

Sugar cane is generally used as raw material for sugar. In Brazil, sugar cane is used as the main raw material for fuel alcohol. In the Republic of Indonesia, as shown in Table 8-4-1, sugar is still imported. The Republic of Indonesia has a plan for increased sugar production to realize domestic supply of sugar in the future. Nevertheless, because comparatively fertile soil is required for sugar cane plantation and the Republic of Indonesia lacks in lands suitable for sugar cane, it is considered difficult to place sugar cane as raw material for fuel alcohol. In the Republic of Indonesia, as shown in Table 8-4-1, sugar is still imported The Republic of Indonesia have a plan for increased sugar production to realize domestic supply of sugar in the future. Nevertheless, because comparatively fertile soil is required for sugar cane plantation and the Republic of Indonesia lacks in lands suitable for sugar cane, it is considered difficult to place sugar cane as raw material for fuel ethanol production.

Table 8-4-1 Sugar in the Republic of Indonesia (Unit: 1000)

Fiscal year	Production	Consumption	Import
1976.5 to 1977.4	1,148	1,460	298
1977.5 to 1978.4	1,201	1,616	440
1978.5 to 1979.4	1,224	1,700	470
1979.5 to 1980.4	1,385	1,850	526
1980.5 to 1981.4	1,313	1,870	550
1981.5 to 1982.4	1,354	1,895	780
1982.5 to 1983.4	1,770	1,900	675
1983.5 to 1984.4	1,790	2,037	190
1984.5 to 1985.4	1,855	2,001	6
1985.5 to 1986.4	1,874	2,084	6

[Source: F.O Light]

o Molasses

The Republic of Indonesia has constructed seven sugar plants in 1981 through 1982 for achieving domestic supply of sugar as shown in Table 8-4-2.

Table 8-4-2 Newly Constructed Sugar Plants

Plants	Sugar Cane Milling Capacity	Location	
Sei Semayang II	4,000 T/Day	Sumatra	
Subang	3,000 "	Jawa	
Cinta Manis	4,000 "	Sumatra	
Caming	3,000 "	Sulawesi	
Takalar	3,000 "	Sulawesi	
Ketapang	4,000 "	Sumatra	
Cula Putih Mataram	10,000 "	Sumatra	

[Source: Ministry of Agriculture]

With the increased number of sugar plants now in operation, the output of sugar manufacturing plants, molasses as by-product have also increased, reaching 500×10^3 t/year in 1985. Molasses used as raw material for industrial ethanol is 120×10^3 t/year and the remaining 380×10^3 t/year are exported.

Furthermore, the Republic of Indonesia has an expansion program for eleven additional sugar plants of 3 x 10^3 to 4 x 10^3 t/day capacity, and when they are completed, the output of by-product molasses will increase to about 230 x 10^3 t/year. Adding the same to the present exports results in a total of 610 x 10^3 t/year of molasses available as raw material for fuel ethanol production.

Since 1 kl of ethanol can be produced from about 3.5 t of molasses in typical case, about 170×10^3 kl/year of fuel ethanol can be produced from the 610×10^3 t/year of molasses.

Since required amount of fuel ethanol is about 160×10^3 kl/year in the penetration stage, raw material molasses produced in the Republic of Indonesia will be enough to meet the said requirement, if additional new sugar plants are constructed.

o Sweet Potato

Although it is confirmed that BPPT's affiliated farms in Sulusban have biannual crop of sweet potatoes, it is premature to say that a large scale plantation technology regarding sweet potatoes have been established in the Republic of Indonesia because of unsolved problem of damage from insects. Presently it is difficult to consider sweet potato as raw material for fuel ethanol.

o Sago Palm

In the Republic of Indonesia, natural sago palm in marshland is considered as raw material for ethanol but it requires more than ten years from planting through harvesting and since large scale cultivation technology as industrial raw material has not been established, sago palm is considered difficult to use as raw material for fuel ethanol.

From the above mentioned reasons, molasses is studied as a subject for raw material for fuel ethanol in the penetration stage.

ii) Production Capacity for each Ethanol Plant

When molasses, the by-product of sugar plant is used as raw material for fuel ethanol, it will be advantageous to select a plant location adjacent to sugar plant to reduce the raw material transportation cost.

Table 8-4-2 shows that newly constructed sugar plants in the Republic of Indonesia 1981 onward have more than 3×10^3 t/day of sugar cane processing capacity.

In the case of 3 x 10^3 t/day sugar cane processing capacity, molasses will be produced at the rate of 4% as by-product. Assuming that 150 is the number of working days per year (average number of sugar plant working days in the Republic of Indonesia), 18×10^3 t will be the annual molasses production.

Since 1 kl of ethanol will be produced from 3.5 t of molasses, one sugar plant is able to supply raw material for about 5×10^3 kl/year of ethanol plant.

With fuel ethanol production plant, in term of production cost it is more advantageous to have larger production capacity for each plant. However, based on the actual experience in Brazil and from the standpoint of raw material availability, this study has assumed 10 x 10³ kl/year as plant capacity of each ethanol plant. In general, it is assumed that fuel ethanol plant will be constructed adjacent to newly built sugar plants and one half of raw material molasses will be supplied from the by-product molasses produced in the newly constructed sugar plants with the remaining one half shortage required to be collected from nearby sugar plants.

iii) Production Schedule

Required amount of fuel ethanol in the penetration stage is 160×10^3 kl/year. Production schedule for this will be as given below.

o First Step

Table 8-4-3 shows the status for existing ethanol plants in the Republic of Indonesia. All plants are producing industrial ethanol (94-95% purity) using molasses.

According to BPPT, major application of industrial ethanol is in the field of solvent. But, because industrial methanol, used as substitute for industrial ethanol, is recovered from textile and other industries at low cost, the ethanol market is taken over by methanol drastically lowering the rate of operation for the existing ethanol plant to as low as 50% average.

According to Table 8-4-3, the gross production capacity of existing industrial ethanol plants in the Repbulic of Indonesia is about 60×10^3 kl/year, thus increasing the production by about 30×10^3 kl/year can be easily achieved by improving the present operation rate of 50% to 100%.

Because the increased industrial ethanol production (94-95% purity) of 30 x 10^3 kl/year enables to produce fuel ethanol (99.3% purity min.) by additional investment for dehydraton facility, and it is clearly more economical than constructing new fuel ethanol plant, in the first step, production of industrial ethanol will be increased

and fuel ethanol will be produced by dehydrating the increased industrial ethanol produced.

Table 8-4-3 Ethanol Production Plants

(unit: Kl/year)

·			(unit. Kityeai)
NO.	COMPANY	LOCATION	PRODUCTION CAPACITY
1	Jatiroto I & II	Jawa Timur	7 500
2	PD. Aneka Kimia	Jawa Timur	18 000
3	PT. Madu Sari S.I.	Jawa Timur	5 250
4	PT. Malindo Raya	Jawa Timur	3 000
5	P.S.A. Comal	Jawa Tengah	5 700
6	PT. Padaharja	Jawa Barat	2 000
7	P.S.A.Madukismo	D.I. Yogyakarta	7 500
8	PT. Palimanan	Jawa Barat	3 000
. 9	PT. Nabiti Sarana	Jawa Barat	1 800
10	PT. Permata Sakti	Sumatera Utara	5 250
11	PT. Basis Indah	Sulawesi Selatan	3 600
12	P.S.A. Sari Kencana	Jawa Timur	-
13	P.S.A. Sari Murni	Sulawesi Selatan	• •
		TOTAL	62 600

[Source: BPPT]

Dehydration facility required for fuel ethanol production can be installed at the industrial ethanol production plants shown in Table 8-4-3. However, since the majority of industrial ethanol production plants shown in Table 8-4-3 are of small scale, individual installation in the industrial methanol plants is not economical. When the distribution of fuel ethanol is considered, it is more economical to construct a dehydration facility of 30 x 10^3 kl/year capacity at the Cilacap Refinery or depot-site nearly Jakarta, which is a gasoline supply base for Jakarta and its surrounding area.

In other words, about one half of the plants shown in Table 8-4-3 (equivalent to 30×10^3 kl/year industrial ethanol production plant capacity) are to continue industrial ethanol production and indus-

trial ethanol produced by the remaining one half of the plants (equivalent to 30×10^3 kl/year industrial ethanol production plant capacity) will be dehydrated by dehydration facility constructed at the Cilicap refinery site or depot-site nearby Jakarta to turn to fuel ethanol of 99.3% purity min. The fuel ethanol so produced then will be mixed at the rate of 10% in regular gasoline tanks within the Refinery or depot-site and distributed to Jakarta and adjacent areas.

Raw material molasses required for the fuel ethanol production in the first stage is about 110×10^3 t/year.

o Second Step

In the second step which is the penetration stage, 13 hydrous fuel ethanol production plants of 10×10^3 kl/year capacity will be constructed adjacent to sugar plants as stated earlier.

In this case, fuel anhydrous ethanol will be produced by dehydrating at some of large scale dehydration facilities, in the same manner.

Raw material molasses required for fuel ethanol production in the second step is about 460×10^3 t/year.

2) Ultimate Stage

Fuel ethanol required for ultimate stage is about 950 x 103 kl/year.

i) Raw Material

Cassava will be the raw material for fuel ethanol in the ultimate stage. Background for selecting cassava as the most suitable material are given below.

- o Molasses was considered as the raw material for penetration stage because of its estimated availability of 610×10^3 t/year in the Republic of Indonesia which represents about 170×10^3 kl/year of ethanol, and there will be a shortage.
- o For ethanol production process using cassava as raw material, a plant of 8 kl/day is successfully in operation at Sulusuban, Sumatra Island, and technological know-how is obtaiend.
- o In the Repubic of Indonesia, the basic national policy includes transmigration from Java Island to othe islands. Transmigrants can cultivate and sell it to ethanol plants in their neighborhood. That means development of cash earning source, which help smooth execution of transmigration policy. In addition, cassava does not require so much fertile soil for its cultiavtion, it is considered to provide enough crops in transmigration areas.

ii) Production Capacity per One Ethanol Plant

According to the FAO statistics, average crop of cassava per hectar(ha) in the Republic of Idonesia is about 9 tons/ha. When cassava is used as raw material, since 1 kl of ethanol is from about 6 tons of raw material, 1.5 kl of ethanol is produced per ha.

According to the Department of Transmigration of the Repbulic of Indonesia, transmigrants are given 2 ha. of land from the government, of which one ha. is already developed and the remaining 1 ha. is expected to be developed by transmigrants themselves.

Assuming cassava is planted in 1 ha. to be developed by transmigrants themselves, and also assuming that 10×10^3 kl/year is the production

capacity of one fuel ethanol plant, as in the case of penetration stage, required area will be about 6,700 ha. and raw material for fuel ethanol plants will be supplied by 6,700 transmigrant families planting cassava which covers the requirement.

iii) Production Schedule

Since fuel ethanol required in the ultimate stage is 950×10^3 kl/year, the following production schedule will be employed, coping with the transmigration policy.

- o Since 160×10^3 kl/year is already secured in the penetration stage, the same amount is assumed available for use in the ultimate stage.
- o For the shortage of 790 x 10³ kl/year in the ultimate stage, 79 hydrous ethanol plants using cassava as raw material will be newly constructed.
- o Those sites of 79 hydrous ethanol plants will be nearby new transmigration area.

However, concrete sites will be decided in accordance with the transmigration policy in the course.

(3) Distribution System and Relevant Facilities

1) Distribution System

i) Penetration Stage

Fuel ethanol required for the penetration stage is 160×10^3 kl/year. In the first step, the present industrial ethanol production will be increased, and by dehydrating the industrial ethanol so produced, anhydrous fuel ethanol of 30×10^3 kl/year will be produced. In the second step, 130×10^3 kl/year of anhydrous fuel ethanol will be produced. This study assumes the adoption of centralized dehydration system, which will be discussed in the distribution system.

- o Hydrous ethanol produced will be transported by barge or tank truck, for example, to the Cilacap refinery site or to one or two dehydration plants nearby Jakarta.
- o Collected hydrous ethanol (94-95% purity) will be dehydrated by dehydration plant and turned into anhydrous ethanol.
- o This anhydrous fuel ethanol will be mixed at the rate of 10% in regular gasoline tanks at the refinery or depot-site nearby Jakarta.
- o This gasohol with 10% anhydrous fuel ethanol mixed in regular gasoline will be transported to gasoline stands around Jakarta and will be sold to general consumers through the existing distribution system.
- o At gasoline stands, it will be necessary to install tanks, gauges and filling system to automobiles for Gasohol (10% anhydrous fuel ethanol mixed) in addition to the existing facilities for regular gasoline and premium gasoline.
- To prevent the use of anhydrous fuel ethanol (99.3% purity min.) to be mixed in gasoline for drinking purposes, it will be necessary to denature it with small amount of methanol, etc.

ii) Ultimate Stage

In the ultimate stage, total fuel ethanol requirement will be 950 x 10³ kl/year which will be covered by the 160 kl/year of fuel ethanol produced in the penetration stage plus the 790 x 10³ kl/year of fuel ethanol to be produced using cassava as raw material in settlements outside Java Island.

As in the penetration stage, for anhydrous fuel ethanol production, producing hydrous ethanol at each ethanol production plant will be collected to some of dehydration plants to produce anhydrous fuel ethanol.

- Hydrous ethanol produced will be transported by barge or tank truck to 3 to 4 dehydration facilities constructed in the Republic of Indonesia.
- o Collected hydrous ethanol (94 to 95% purity) will be dehydrated to anhydrous fuel ethanol at 3 to 4 dehydration facilities.
- o Anhydrous fuel ethanol produced will be transported to gasoline depot in the neighbourhood of dehydration facilities, and will be mixed in regular gasoline at the rate of 20%.
- o Gasoline will be transported by tank trucks from gasoline depot to gasoline stands through the existing gasoline distribution system, then will be sold to general consumers.
- o At gasoline stands, it will be necessary to install tanks, gauges and filling system for automobiles for gasohol (20% ethanol mixed) in addition to the existing facilities for regular gasoline and premium gasoline. In Jakarta and surrounding areas, facilities (10% ethanol mixed) set up in the penetration stage can be utilized as is.
- o To prevent the use of fuel ethanol of 99.3% purity min. to be mixed in gasoline for drinking purposes, it will be necessary to denature it with small amount of methanol, etc.

2) Distribution Facilities

As explained earlier, distribution systems for penetration stage and ultimate stage are similar, thus explanation common for both stages will be given later.

i) Distribution Facilities

o Transportation from ethanol plant to receiving tank at dehydration plant

Barges will be used for newly constructed ethanol plant outside Java Island, and tank trucks will be used for inland transportation within Java Island. For barges and tank trucks, the existing ones used in the Republic of Indonesia can be utilized.

o Hydrous ethanol storage tank

Storage tanks for hydrous ethanol transported by barges and tank
trucks have to be newly constructed.

Dehydration plant

New dehydration plants to produce anhydrous ethanol are required. Benzene or cyclohexane will be used as the dehydration agent. For this dehydration plant process flow, main equipment required and rough estimation of construction cost will be discussed later.

o Gasohol storage tank

Anhydrous ethanol produced at dehydration plant and regular gasoline will be mixed by line blender then stored in gasohol storage tank, and storage tank should be newly constructed.

o Transportation facilities from gasohol tanks to gasoline stands
Gasohol with anhydrous ethanol mixed at the rate of 10% in regular
gasoline will be transported by tank trucks to gasoline stands. The
existing tank trucks used for gasoline can be utilized.

Fig. 8-4-3 shows the flow of fuel ethanol in relation with the above related facilities.

ii) Dehydration plant

Dehydraton plant is to produce anhydrous ethanol using hydrous ethanol as its raw material with benzene or cyclohexane as the dehydration agent.

a) Process outline

Process outline using the most commonly used benzene as its dehydration agent is as follows:

- o Anhydration ethanol stored in tank will be sent to dehydration tower by pump.
- o The dehydration tower with reboiler using steam as its heat source will distill ethanol, benzene and water. Benzene and water will be distillated from the tower top and hydrous ethanol will be distillated to hydrous tank from the tower bottom via product cooler.
- o Benzene and water from the tower top will be distilled at benzene recovery column, where benzene and water will be separated, benzene from the top and water from the bottom.
- o Hydrous ethanol so produced and stored once will be mixed with regular gasoline by line blender and then will be stored in gasohol tank.

The above process outline is shown in Fig. 8-4-4, "Outline of Dehydration Plant".

b) Main equipment

Main equipment required for dehydration plant are shown in Table 8-4-4, "Main Equipment List".

Table 8-4-4 Main Equipment List of Dehydration Plant

No.	Equipment	Q'ty	Specification
1	Hydrous Ethanol Storage Tank	2	5000 m ³ , Carbon Steel
2	Hydrous Ethanol Feed Pump	1	
3	Dehydration Column	1	Stainless Steel
4	Dehydration Column Reboiler	1	Shell / Tube Type
5	Dehydration Column Condenser	2	Shell / Tube Type
6	Benzene Recovery Column Condenser	1	Stainless Steel
7	Benzene Recovery Column Condenser	1	Shell / Tube Type
8	Dehydration Column Bottom Pump	1	
9	Product Cooler	1	Shell / Tube Type
10	Benzene Tank	1	Carbon Steel
11	Anhydrous Ethanol Storage Tank	2	5000 m ³ , Carbon Steel
12	Line Blender	1	Static Mixer Type
13	Benzene Feed Pump	1	·
14	Anhydrous Ethanol Tank Pump	1	
15	Regular Gasoline Feed Pump	1	

c) Rough estimate of construction cost

Since requirement of hydrous ethanol in penetration stage is 30×10^3 kl/year in the first step and 130×10^3 kl/year in the second step, dehydration plant of 160×10^3 kl/year production capacity have to be newly constructed.

Estimated construction cost is $2.9 \times 10^6 \$$ for 30×10^3 kl/year and $8.1 \times 10^6 \$$ for 130×10^6 kl/year.

Additionally, 5 to 6 dehydration plants of 160×10^3 kl/year production capacity are required for the ultimate stage.

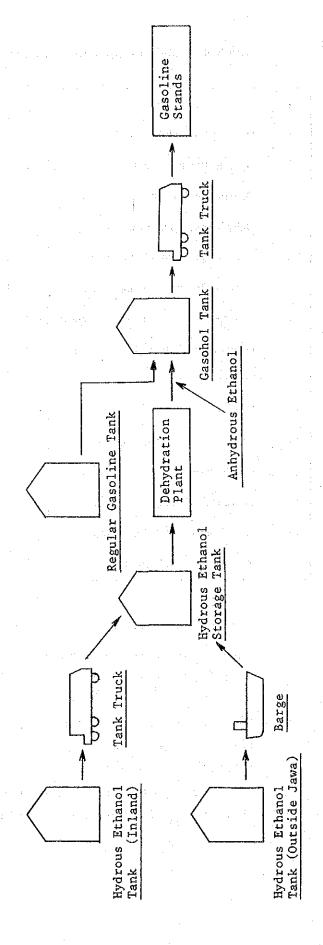


Fig. 8-4-3 Flow of Fuel Ethanol

Gasoline Tank Ethanol Storage Tank Line Blender Anhydrous Regular Gasoline Tank Benzen Tank Benzen Recovery Column Steam Vent Condenser Water Product Cooler Benzen Separator Vent Dehydration Column Condenser Reboiler Steam Drain Hydrous Ethanol Storage Tank -341-

Fig. 8-4-4 Outline of Dehydration Plant

8-5 Issues and Measures for Introducing Fuel Alcohol

8-5-1 Fuel Methanol Production and Distribution Costs

(1) Fuel methanol production cost

The production cost of fuel methanol is detailed in the Interim Report II (1985), which is summarized b elow.

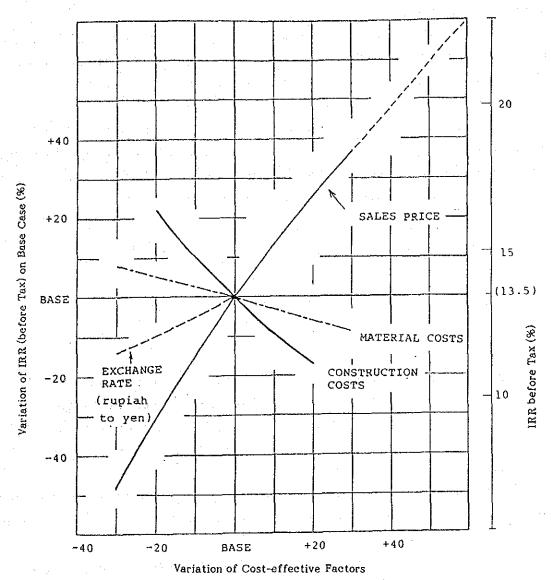
- 1) Preconditions of financial analysis
 - i) Methanol production: $1,600 \times 10^3$ t/y (project life: 30 years)
 - ii) Finance: Equity 25%

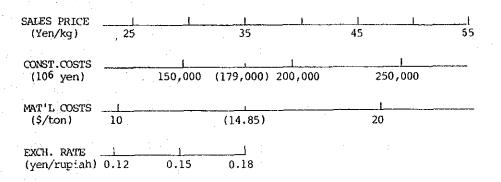
 Debts 75% (interest rate 8%)
 - iii) Exchange rates: \$1 = \text{ \text{\$\gamma}}200, \text{ Rp1} = \text{\text{\$\geq 0.18}}
 - iv) Fixed-capital investment: 989,500 x 106 Rp (¥178,600 x 106)
 - v) Raw material (coal): 16,454 Rp/t (14.85 \$/t)
 - vi) Plant gate price of methanol (assumed): 194 Rp/kg (35 ¥/kg)

2) Financial analysis results

Based on these preconditions, IRR (Internal Rate of Return) become 13.5% and the minimum shipping price of fuel methanol (IRR 8% = interest rate) 143 Rp/kg (112 Rp/l). The relation between IRR and cost factors is shown in Fig. 8-5-1. It is noted that the factors having great influence on IRR are the plant gate price of methanol and fixed capital investment.

Fig. 8-5-1 Sensitivity of Cost-effective Factors





(2) Fuel methanol distribution cost

In a project to produce fuel methanol from Banko coal, distribution is assumed as follows.

Fuel methanol is stored in Palembang, which serves as a terminal, from which it is forwarded to refineries or depots near individual consuming areas, where it is blended with gasoline and given other preparation treatments. Resultant products are supplied to fuel consumers directly or via service stations.

Based on local survey results, the marine transportation cost of fuel oil is assumed to average 6.95 \$/kl in general in Indonesia. Also considering the domestic oil flow, marine transporation costs from the Plaju refinery to major consuming area were estimated, results of which are shown below.

Plaju - Demand Region	I (Medan)	15.40 \$/kl
n ·	II (Palembang)	0
11	III (Jakarta)	7.70
n .	IV (Semarang)	11.62
11 :	V (Surabaya)	15.40
11	VI (U. Pandang)	32.90

Because Palembang adjoins Plaju and because marine transportation of fuel methanol is thought to be identical to that of fuel oil, the figures shown in the preceding table can be identical to marine transportation costs of fuel methanol from Balikpapan. Also, local survey results suggest that the land transportation cost is an estimated 0.15 \$/kl.km.

Based on these results, transportation costs of fuel methanol from Palembang to individual consuming areas located inland within 100km from the starting point were estimated, and are presented in Table 8-5-1.

Table 8-5-1 Transportation Costs from Palembang to Each Demand Region

From Palembang	Marine cost	Inland cost (100km)	Total ①+②
to Demand Region I	15.40	15.0	30.40
II	0	15.0	15.00
. III	7.70	15.0	22.70
IV	11.62	15.0	26.62
v	15.40	15.0	30.40
VI	32.90	15.0	47.90

8-5-2 Production and Distribution Cost of Fuel Ethanol

8-5-2 Production and Distribution Cost of Fuel Ethanol

(1) Production Cost of Fuel Ethanol

1) Penetration Stage

In the penetration stage, molasses is used as the raw material, and ethanol production plant production capacity is assumed to be 100×10^3 Kl/year. Production cost is computed on the following assumption.

i) Raw Material Cost

According to the study report on the effective use of sugar by-products in the Republic of Indonesia in 1983, the price of molasses in the Republic of Indonesia for 1977 to 1982 is as given in Table 8-5-2.

Table 8-5-2

					(unit:	Rp/T)
F.Y.	1977	1978	1979	1980	1981	1982
Price	15,200	20,600	33,500	65,000	55,000	20,000

It is evaluated that the unusual price up of molasses in 1980 and 1981 depends on the effect of 2nd oil crisis and, on the other hand, the decrease of the price in 1982 depends on the oversupply of molasses because of additional constructions of sugar plants in 1981 and 1982 as well as the trend of the price down of oil price in 1982.

Because the constructions of several sugar plants is planned at present time to keep self-balance in Indonesia, the supply of molasses, as byproduct of sugar, is estimated to be oversupply and the price is even or may be dropped in short and long terms.

Taking into consideration above market and price situation, the price of molasses will be assumed to be 20,000 Rp/Kl in short and long terms.

If one applies the ratio of 1110 Rp/\$, as exchange rate, the price of molasses as feedstock of fuel ethanol is equivalent to 18 \$/kl. The unit consumption of molasses per unit fuel ethanol is about 3.5 therefore the feedstock cost of fuel ethanol from molasses is estimated to be 63 \$/Kl ethanol.

ii) Utility Cost

With consideration for fuel, water, power and chemicals, and based on the report obtained from Aneka-Kimia plant in the Republic of Indonesia, utility cost of 33.20 \$/KI is applied.

iii) Labor Cost

For unit labor cost, 1,000 \$/Y as reported by PD Aneka-Kimia is applied, requiring 120 workers.

- iv) Plant Construction Cost
 Construction cost in 1985 assumed as 8.6 x 106\$.
- v) Interest
 Assumed construction cost x 10%.
- vi) Maintenance Cost
 Assumed construction cost x 3%.
- vii)Taxes and Insurances

Assumed construction cost x 0.5%.

viii) Depreciation

Salvage value after full depreciation is assumed 10% to be depreciated over 10 years period. Therefore, annual depreciation cost will be, Construction cost x 0.9 x 1/10.

- ix) Profit
 Assumed 10% of construction cost.
- Administration Cost
 Assumed labor cost x 80%.

Table 8-5-3 gives the cost of fuel ethanol in penetration stage as computed from the foregoing.

Table 8-5-3 Cost of Fuel Ethanol from Molasses (Penetration Stage)

Item	Costs	\$/K <i>1</i>
Raw Material	18 \$/T x 3.5 T/K <i>l</i>	63
Utility & Chemicals	33.20 \$/KI	33
Labor	1000 \$/man x 120 man x 1/10,000 Kl	12
Interest	8.6 x 10 ⁶ \$ x 0.10 x 1/10,000 K <i>l</i>	86
Maintenance	8.6 x 10 ⁶ \$ x 0.03 x 1/10,000 K <i>I</i>	26
Taxes & Insurances	8.6 x 10 \$ x 0.005 x 1/10,000 K <i>l</i>	4
Depreciation	8.6 x 10 ⁶ \$ x 0.9 x 1/10 x 1/10,000 K <i>l</i>	77
Profit	8.6 x 10 ⁶ \$ x 0.1 x 1/10,000 K <i>l</i>	86
Administration	1000 \$/man x 120 man x 1/10,000 Kl x 0.8	10
	Total	397

The financial analysis results shown on Table 8-5-3 could be ealuated in view of economic evaluation as 134 \$/KI as economic evaluation cost, because labour cost, tax, deprication and profit could be considered to be benefit for Indonesia.

If one assumes that the preferable impacts on environmental modification by decrease of leaded gasoline and the save of domestic oil consumption, 134 \$/Kl could be evaluated in lower evaluation cost.

2) Ultimate Stage

As stated earlier, in the ultimate stage, further $890 \times 10^3 \text{Kl/year}$ ethanol is required in addition to the $160 \times 10^3 \text{ Kl/year}$ in the penetration stage, making $950 \times 10^3 \text{ Kl/year}$ as the total requrement. For this additional $890 \times 10^3 \text{ Kl/year}$, cassava will be used as raw material and the ethanol plant production capacity will be $10 \times 10^3 \text{ Kl/year/plant}$. Production cost is calculated based on the following.

i) Raw Material Cost

According to the Bureau of Statistics of the Republic of Indonesia, the price of cassava used as raw material in the ultimate stage in 1979 to 1984 will be as follows:

Table 8-5-4 Price of Cassava

					(unit	: Rp/T)
F.Y.	1979	1980	1981	1982	1983	1984
Price	54,000	75,000	88,000	13,000	134,000	124,000

The Rp currency of the Republic of Indonesia is converted to \$ based on the International Financial Statistics and further adjusted to \$ on 1985 base using the deflator and given in Table 8-5-5.

Table 8-5-5 Price of Cassava

					: (un	it: \$/T)
F.Y.	1979	1980	1981	1982	1983	1984
Price	145.92	155.55	165.37	173.71	158.50	115.40

As shown in Table 8-5-5, although the price of cassava varies greatly, this report employs 152.40 \$/T, average price for 1979 to 1984. Therefore, raw material cost is obtained by multiplying 152.40 \$/T with 6 T/Kl required to produce 1 Kl of ethanol.

ii) Utility Cost

With consideration for fuel, power and chemicals, 61.59 \$/Kl is assumed.

iii) Labor Cost

As in the penetration stage, 1,000 \$/man is assumed using 120 men.

iv) Plant Construction Cost

Assumed construction cost as 10.12×10^6 for 1985.

v) Interest

Assumed construction cost x 10%.

vi) Maintenance

Assumed construction cost x 3%.

vii) Taxes and Insurances

Assumed construction cost x 0.5%.

viii) Depreciation

Salvage value after full depreciation is assumed as 10% to be depreciated over the 10 year period. Therefore, annual depreciation cost will be construction cost x 0.9 x 1/10.

ix) Profit

Assumed 10% of construction cost.

x) Administration cost

Assumed labor cost x 80%.

Table 8-5-6 Cost of Fuel Ethanol from Cassava (Ultimate Stage)

Item	Costs	\$/K <i>I</i>
Material	152.40 \$/T x 6 T/K <i>l</i>	914
Utility & Chemicals	61.59 \$/K <i>I</i>	62
Labor	1,000 \$/man x 120 man x 1/10,000 Kl	12
Interest	10.12 x 10 ⁶ \$ x 0.10 x 1/10,000 K <i>l</i>	101
Maintenance	10.12 x 10 ⁶ \$ x 0.03 x 1/10,000 K <i>l</i>	30
Taxes & Insurances	10.12 x 10 ⁶ x 0.005 x 1/10,000 K <i>I</i>	5
Depreciation	10.12 x 10 ⁶ \$ x 0.9 x 1/10 x 1/10,000 K <i>l</i>	91
Profit	10.12 x 10 ⁶ \$ x 0.1 x 1/10,000 K <i>l</i>	101
Administration	1,000 \$/man x 120 man x 1/10,000 Kl x 0.8	10
	Total	1,326

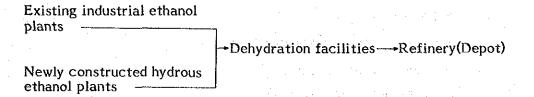
The financial analysis results shown on Table 8-5-6 could be evaluated in view of ecnomic evaluation as 220 \$/Kl as economic evaluation cost, because labor cost, tax, depreciation and profit could be considered to be of benefit to Indonesia.

Economic evaluation cost may be more lower if one considers the preferable impacts on environmental modifications and transmission policy of Indonesia as well as the decrease of domestic oil consumption.

(2) Distribution Cost of Fuel Ethanol

1) Penetration Stage

As stated earlier, in the penetration stage, hydrous ethanol produced from molasses as raw material at the existing industrial ethanol plants and newly constructed hydrous ethanol plants will be collected at the 1 or 2 dehydration facilities, dehydrated into anhydrous fuel ethanol and mixed with regular gasoline at refining depot.



Existing industrial ethanol plants are, as shown in Table 8-4-3, mostly located in Java Island, and newly constructed hydrous ethanol plants are most likely to be located in Kalimantan area, Sumatra Island as shown in Tabl 8-4-2, because they will be in the site affiliated to newly constructed sugar plants.

Hydrous ethanol will be transported from these areas to the dehydration facilities located in Java Island, thus exact calculation will be difficult, so the preset study is estimated based on the following.

i) Prerequisites

- o In the penetration stage, hydrous ethanol is assumed to be transported for an average of 300 Km offshore and 200 Km inland.
- o Marine Distribution Unit Cost

 Hydrous ethanol will be assumably transported by barges of 500 to
 1000 Kl and unit cost is estimated to be 0.02 \$/Kl·Km based on the
 same in Japan in 1985.
- o Inland Distribution Unit Cost
 Hydrous ethanol will be assumably transported by tank trucks of 6
 to 10 KI and unit cost is estimated at 0.15 \$/KI·Km as reorted by
 Aneka-Kimia, the largest ethanol plant in the Republic of Indonesia
 as of 1985.

ii) Result of Computation $0.02 \times 300 + 0.15 \times 200 = 36 \text{ $/K1}$

2) Ultimate Stage

In this stage, 790 x 10^3 KI/Y of fuel ethanol newly produced in the settlements using cassava as raw material will be used in addition to the 160×10^3 KI/Y of fuel ethanol produced in the penetration stage.

This fuel ethanol will be first produced as hydrous ethanol, transported to the 4 to 5 dehydration plants located in Java Island, then dehydrated there and mixed at the rate of 20% in regular gasoline at refinery depot near the dehydration plants.

In this stage, exact calculation of distribution cost is difficult but since most of the hydrous ethanol will be produced outside Java Island and then transported to Java Island, roughly the same as in the case of penetration stage, the present study assumes 36 \$/Kl, same distribution cost as in the penetration stage applies.

8-5-3 Safety

(1) General Properties of Alcohols

Table 8-5-7 shows the properties of methanol and ethanol. Both methanol and ethanol are saturated monohydric alcohol with hydroxyl groups, and easily blended into water, alcohols, ether, and other organic solvents. Methanol have a lower calorific value than does gasoline, and are inflammable at ambient temperature. In combustion, they have air fuel ratio rich in fuel, and the flame is invisible.

Methanol is toxic, although the degree is lower than oil. The drinking of 30 - 100 ml of methanol may cause death, and 7 - 8 ml blindness. Therefore, it must be handled with great care. It smells similarly to ethanol. Do not drink it by mistake.

(2) Dangerousness of Explosion

Methanol is liquid inflammable at 11°C. Its vapor forms explosive mixed gas in the range from 6.72 to 36.5%, when it is mixed with air.

Ethanol is liquid inflammable at 12.8°C. Its vapor forms explosive mixed gas in the range from 3.3 to 19%, when it is mixed with air.

When stored in a closed container such as a tank, can and bottle, both methanol and ethanol produce explosive mixed gas in the container in the temperature range from about 11 to 42°C. (See Fig. 8-5-2)

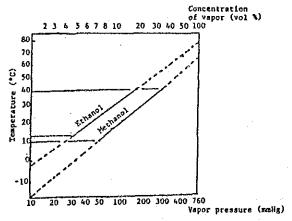


Fig. 8-5-2 Vapor Pressure and Explosion Limit of Methanol and Ethanol (Source: The Chemical Society of Japan: Guidance for Chemical Accident Prevention)

Table 8-5-7 Physical Properties of Alcohols

	Methanol	Ethanol	Gasoline	
Appearance	Colorless,	Colorless,	Colored	
	transparent	transparent	to orange	
	lìquid	liquid		
Odor	Characteristic	Characteristic	Characteristic	
	aroma	aroma	odor	
Taste	(Toxic)	Burning taste		
Boiling point				
760mmHg	64.65°C	78. 325°C	30∼200°C	
Melting point	-96°C	-114.5°C		
Density of steam		:		
(air = 1)	1, 11	1.58	3~4	
Flash point	11°C	12. 8°C	-40°C	
Ignition point	470°C	392°c		
Explosion limit				
(in the air)	6.72~36.5vol%	3.3~19vo1%	1.4~7.6vol%	
Vapor pressure	60mmHg (12, 1°C)	40mmHg (19°C)		
lleat of combustion	(HV) 173.6	(HV) 326. 6		
$(x_1, \dots, x_n) = \frac{1}{2} (x_1 + x_2) + \frac{1}$	Kcal/mol	Kcal/mol		
	(LV) 153. 6	(LV) 288. O	About	
	Kcal/mol	Kcal/mol	11,000Kcal/kg	

[Source: The Chemical Society of Japan :
Guidance for Chemical Accident Prevention)

Gasoline exceeds upper explosion limit in a closed container, since it is mixed liquid with different boiling points, and usually contains a low boiling point fraction (pentane).

Therefore, it is important to premix methanol and ethanol with the low boiling point fraction such as gasoline that contains 3-25% butane or to install a flame arrester to the opening before using methanol and ethanol to prevent inflammation.

Methanol and ethanol is similar to oils in general inflammability. They are characterized by flame during combustion that is hard to distinguish. For this, favorable results have been obtained by mixing 15% of gasoline that contains 40% aromatic into methanol, gasoline that contains 85% or more of methanol ignites when it is dropped onto a high temperature manifold of a car. Gasoline or gasoline containing methanol at a low level does not seem to ignite, when it is dropped onto the manifold, because it rolls down with keeping it dry (R. Piquette and others: 7th International Symposium on Alcohol Fuels. Paris Oct/20 - 23, 1986)

(3) Toxicity

Table 8-5-8 shows the toxicity of alcohols. As clear from the Table, methanol is toxic. Ethanol usually acts as a sedative without toxicity. This section deals with methanol that is toxic.

An oral dose of 8 - 20g of methanol may cause blindness and 30 - 50g death. The LD_{50} to methanol in rats is 12-14 mg/kg. The figure for both methanol-gasoline mixture and gasoline is 10 mg/kg in this species. The LD_{50} is comparable among the three.

Transcutaneous exposure to 200 ppm or more of methanol may produce chronic poisoning such as optic nerve disorders and multiple neuritis.

The toxic inhalation dose of methanol irritates the eyes, nose, and pharyngeal and laryngeal mucosa, which may cause poisoning symptoms. The allowable concentration is 250 ppm for exposure within 15 minutes and 200ppm or less for exposure for 8 hours a day.*

*ACGIH (American Conference of Governmental Industrial Hygienists)
Methanol toxicity may give rise to acidemia, and severe toxicity may cause ranal and liver disorders. The allowable concentration of gasoline is 500 ppm.

A comparative acute toxicity test in rats shows no marked difference in oral, transcutaneous, or inhalation toxicity between 15% methanol-gasoline mixture and gasoline.

As for action on the central nervous system, methanol-gasoline mixture has a stronger sedative action.

A subacute toxicity test shows that methanol-gasoline mixture affects the respiratory system more strongly. This returns to normal after stopping exposure.

A mutagenicity test using Salmonella Lignieres and Ames method shows no differences between methanol-gasoline mixture and gasoline; neither compound is mutagenic. The chronic toxicity, including carcinogenicity, of a low level of methanol vapor should be tested through out the life of laboratory animals as done with agricultural chemicals. For this reason, laboratory animals with a short life expectancy such as rats and mice are generally used for this test. On the other hand, monkeys, which is a primate, is suited to evaluate the effects of ethanol on human, since the toxicity of ethanol in primates is clearly different from that in other species.

In view of these, mokeys and rats and mice were selected as laboratory animals to start about 3-yearchronic toxicity test in monkeys. In addition, a lifetime toxicity test, including carcinogenicity test was done in rats and mice of a number that is required for statistical analysis.

Four levels of spray methanol, 0 (control), 10, 100 and 1000 ppm, were selected for these tests based on the results of a test of a high level of methanol that was done to determine in a short period which part of the monkey's body is affected by methanol and the industrial hygiene standard (260 ppm).

The chronic toxicity test has been done for more than one year as of the end of March, 1984. Monkeys and mice remain unchanged with 100 ppm of methanol or less.

Only monkeys have symptoms suggesting arrhythmia and irregular menstruation with 1000 ppm.

A test of a high level of methanol, which was done to understand symptoms that appeared in monkeys as described above, was done at levels of 3,000, 5,000, 7000 and 10,000 ppm for two weeks.

(Source: Nomura Research Institute: Feasibility Study on the Use of Alcohol-Gasoline Mixture in Fiscal 1980 and 1981)

Table 8-5-8 Harmfulness of Alcohols

ltems	Ethanol	Methanol
(1) General	Sedative	Poison
properties	The drinking of an appropriate	Not drinkable.
	amount of ethanol improves	Usually,
1	appetite, and stimulates the	8∼20g causes blindness
	secretion of gastric juice, which	30~50g causes death.
	helps the absorption of food. The	
·.	repeat drinking of large amount	
	irritates the gastric mucosa.	
•	Excessive drinking is harmful to	
	the nervous system.	
Blood level	Toxic symptoms	
0.05 %	Inhibitory nerve paralyzed and	
0.03 %	judgement lost	
0.1 %	Motor and sensory nerves paralyzed	-
0.2 %	All motor nerves disturbed	
0.37 %	The center of the brain paralyzed	
0.51 %	and sensory paralysis	
0.4~0.5 %	The entire sensory region of	
0.4~0.3 %	the brain affected; coma	
0.6~0.7 %	The respiration center and cardiac	
V. 0' 0. 1 %	center paralyzed; death	*
	Center paratyzeu, ucath	
(2) At handling	Relatively harmless	Harmful
	Alcohol vapor acts as an	Methanol irritates the
. # !	anesthetic. The repeated exposure	eyes and nose and
	of ethanol irritates the eyes and	pharyngolaryngeal mucosa
	bronchus, and causes headache,	Repeated contact with
	shivering, sleepiness, vomitting,	methanol causes dry,
•	and anorexia.	squamous, and crack
		dermatitis.
Allowable	15 minutes or less 1000 ppm	250 թբա
level	8 hrs/day 1000 ppm	250 ppm
(ACGIII)		

Level	Effects	Effects
1000 ppm		Acute toxicity:
		Drunkenness, pain, headache, and dim sight
1380 ppm	28 min:No effects 38 min:Headache 39 min:Slight numbness	
2300 ppm	Feels hot in the head, drunk, and cold in the arms and legs. 50 min: Sleepiness	
5000 ppm	20 ppm:Increased headache	Acute toxicity:
6000 ppm	Discomfort and slight sleepiness	Coma to death
7000 ppm	Discomfort, 30 min:Feels hot 90 min:Fatigue	
8000 ppm	Odor, burning sensation in the eyes 30 min:Patigue and sleepiness	
3) Acute toxicity		LDso(rats) 12~14 mg/kg
(4) Cutaneous absorption	Absorbed cutaneously, which may cause poisoning.	200 ppm or more causes subacute and chronic poisoning, optic nerve disorders, and multiple neuritis.

(Source: The Chemical Society of Japan :
Guidance for Chemical Accident Prevention)

8-5-4 Environment

(1) Effects of Production Processes on Environment

The methanol manufacturing plant does not have the leakage of a high level of methanol, causing no problems of environmental contamination in the surrounding area, as long as it satisfies standards for facilities for manufacturing dangerous articles.

Generally, care must be taken not to drain a high level of methanol such as fluid at the bottom of the rectifier into the general water system.

In the aspect of working atmosphere, when the manhole, which is on the facility for storing methanol, is opened, methanol vapor is present near the manhole. The worker should stand to the windward or go away from the manhole. This decreases the level of alcohol rapidly, and there is no problem.

Ethanol causes no problems, since it has no toxicity, which is found in methabnol.

However, ethanol is manufactured by biomass. Waste fluid is produced in the manufacturing process. It requires to process when it is returned to the nature. It can be processed by the methane fermentation, activated mud, the cultivation of yeast, and concentration. Residue after processing is used as a fertilizer or feed. (See Figs. 8-5-3 - 8-5-4).

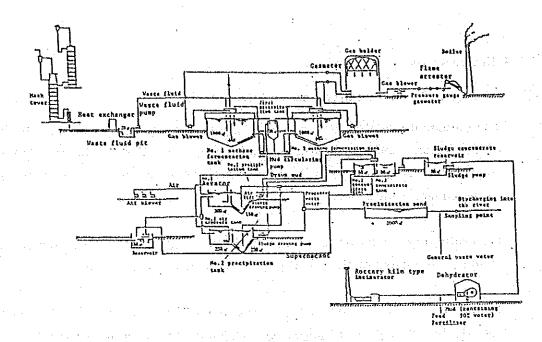


Fig. 8-5-3 Flow Chart of the Process of Waste Fluid by a Combination of the Fermentation of Methane and Activated Mud

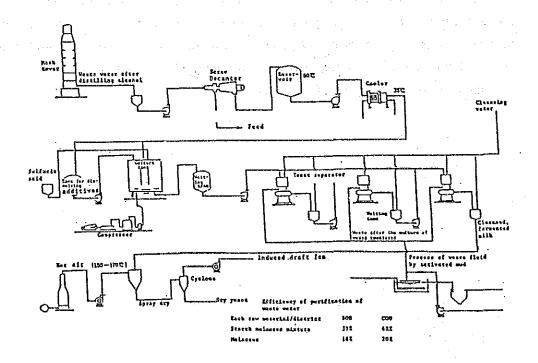


Fig. 8-5-4 Process of Waste by the Cultivation of Yeast

(2) Effect of Distribution Processes on Environment

1) Effects on an Ecosystem

A blend of gasoline and methanol or ethanol is usually made by refineries. It is distributed as a alcohol-gasoline mixture. The effects of the alcohol-gasoline mixture on the natural ecosystem during its release to the water system and the effects of methanol on aquatic life are presented here.

i) Biodegradation

The measurement of biochemical oxygen demand in the closed system that contains standard activated mud and the direct analysis of dissolved substances in the water show no differences in decomposability between 15% methanol-gasoline mixture and gasoline. The low-boiling point fraction gasoline has higher decomposability than the high-boiling point one. Methanol-gasoline mixture starts to be broken down more early.

ii) Accumulation of a Aocohols in Fish

The ratio of the amount of the representative components, which are contained in 15% methanol-gasoline mixture and gasoline, dissolved in the water and their amount accumulated in carp is some ten to some hundred times; there were no significant differences between the two.

iii) Effects of Methanol on the Life of Water

There are no knowledge available on the chronic efects of relatively long-term exposure to methanol on aquatic life, its evasion from methanol, or the effects of methanol on micro-organisms in the water. Fatal level test in Himedaka (a kind of killfish), evasion test in ear shells etc. chronic effect test in Himedaka, and growth test in plankton have been done to make an overall evaluation of these effects, particularly taking the effects of methanol on culture fishery into account etc. Red sea breams, prawns, ear shells, seaweed etc. have been selected for these tests. At present, these tests are well under way without any problems. The following tests also have been done:

- a) Fertility and teratogenicity test
- b) Mutagenicity test
- c) Metabolism test

d) Test of diffusion in the water (Source: Shizuo Takatori: Electricity and Gas 1984 Vol. 34, No.7)

2) Level of Alcohol Concentration in the Working Atmosphere

The assay of the levi of vent gas from the vent tube at the unloading of fuel in the underground tank, which is a oil supply facility, satisfies the regulation imposed by local self-governing bodies, including Tokyo. In

Japan, we are obliged to return the vapor of this vent gas that generates during unloading to the oil supply facility to a tank lorry from the standpoint of prevention of air pollution caused by the vaporization of

The maximum level of ethanol has been measured near the nose of the operator as 5.6 vol ppm, when cars are filled up with 10% ethanol-gasoline mixture. The maximum level of methanol has been measured in the same place as 48 vol ppm, when cars are filled up with 10% methanol-gasoline mixture. There results suggest no problem of working atmosphere, because these values are much lower than the allowable level, and time of

exposure to these alcohol is short.

hydrocarbons.

Table 8-5-9 shows the levels of alcohol-gasoline mixtures in the air assayed near the facilities and equipment of the small-sized distribution system.

Table 8-5-9 Work in the Process of Storage and Distribution of Alcohols and the Maximum Levels of Alcohols

Name of work	Gasoline used	Maximum level
(1) Filling up	Summer: 15% methanol- gasoline mixture	Methanol 154 ppm
meter (2) Drain from the joint after	Winter: 15% methanol- gasoline mixture	Methanol 137 ppm
loading a tank		
(3) Drain from a tank lorry joint after pouring	Summer: 15% methanol- gasoline mixture	Methanol 112 ppm
	Summer: 10% ethanol- gasoline mixture	Ethanol 415 ppm
a tank lorry (4) Opening the tank manhole	Summer: 10% ethanol- gasoline mixture	Ethanol 415 ppm

(Source: Nomura Research Institute: Feasibility Study on the Use of Alcohol and Oil Products Mixture in 1984)

(3) Effect of Exhaust from Cars

1) Present Status of Regulations

The volume of passenger traffic and carloadings increased by leaps and bounds with marked pouplarity of cars. At the same time, cityward drifting of population and extended urban districts caused a problem of traffic pollution in urban areas in many countries.

Traffic pollution is classified into two major types: air pollution and noise pollution. Air pollution includes nitrogen dioxide, nitrogen monoxide, hydrocarbon, smoke, and lead. The present status of regulations on exhaust from cars in various countries is described below.

Japan: Regulations became effective in 1973, and were intensified every year. (See Figs. 8-5-5 and 6.) (See Table 8-5-10.)

USA: Regulations became effective in 1970. They remain in force in California, where severer regulations are applied, and other states, seprately.

Germany: Regulations were enforced by the exhaut control in 1968.

Decreases in lead in gasoline was legislated in 1971.

France: The government ordinance 1974 regulates exhaut from cars.

England: Exhaust from cars was specified in the Road Traffic Art 1972, and became effective in 1973.

Regulations that was adopted by the United Nations European Economy Committee (ECE) in 1972 were introduced.

Indonesia:Basic provisions were enacted to control living environment in 1982. Tables 8-5-11 - 12 show the current criteria in Indonesia.

Fig. 8-5-5 Regulated Limit of NOx Exhaust from Cars and Environmental NOx Concentration v.s. the Number of Cars in Japan

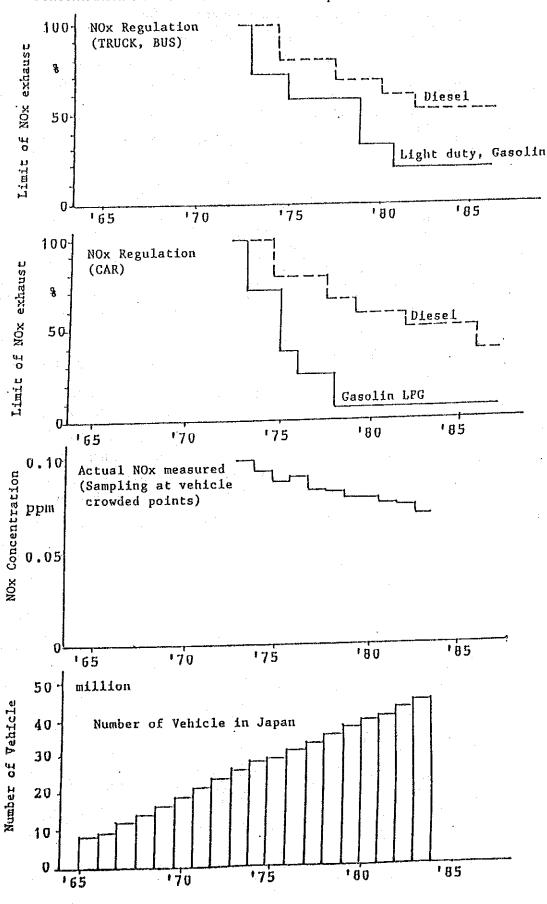
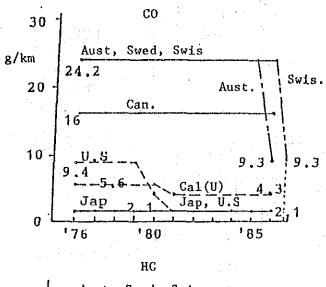
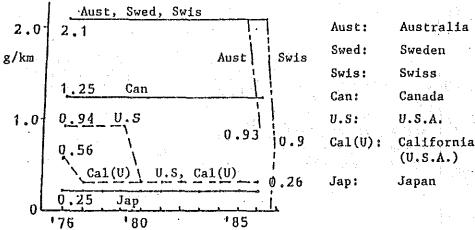


Fig. 8-5-6 Comparison of Regulations of Major Countries (Regulated Limit of Exhaust from Cars)





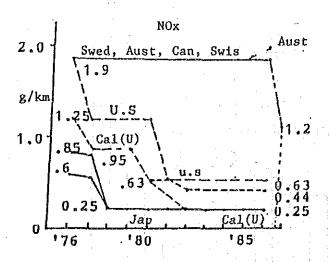


Table 8-5-10 History of Regulations on Cars, Including Those on NOx, in Japan

YEAR	TTSM TO THE TOTAL TOTAL TO THE TOTAL TOTAL TOTAL TO THE TOTAL TOTAL TOTAL TO THE TOTAL TOTAL TOT	REMARKS
1973	Regulations 1973 were enforced.	
	(Regulations on CO were intensified, and	
	regulations on NC and NOx became effe-	
	ctive.)	
1974	Regulations 1974 were enforced.	
	(Regulations on CO, NC, and NOx from	-
	diesels became effective.)	
:		
1975	Measuress to reduce a total number of	Lead-free
	cars in the three major cities were	regular
	promoted (MITI).	gasoline was
	Regulations 1975 were enforced.	put into
	(Regulations on CO, NC, and NOx were	practice.
	intensified.)	
1976	Regulations 1976 were enforced.	
-	(Regulations on NOx were intensified.)	
1977	Regulations 1977 were enforced.	
	(Regulations on NOx from diesels and	
	other cars were intensified.)	
1978	Regulations 1978 were enforced.	
-	(Regulations on NOx were intensified.)	
1979	January	
	Regulations 1979 were enforced	
	(Regulations on noise and NOx from	
	gasoline cars were intensified.)	
	April	
	Regulations 1979 were enforced.	
	(Regulations on noise and NOx from	
	diesels were intensified,)	
	1	•

1981	Regulations 1981 were enforced,
	(Regulations on NOx from light duty
	gasoline cars were intensified.)
	Regulations 1981 were enforced.
	(Regulations on NOx from intermediate
	duty gasoline cars were intensified.)
1982	Regulations 1982 were enforced.
	(Regulations on NOx from trucks,
	heavy duty gasoline cars, and
	indirect injection diesels were
	intensified.)
	Regulations 1982 were enforced,
	(Regulations on NOx from indirect
	injection diesel trucks and buses
	were intensified.)
1983	Regulations 1983 were enforced.
	(Regulations on NOx from direct injection
	diesels were intensified.)

(Source : Environment Agency : Environmental white paper '85)

Table 8-5-11 Criteria for Air Environment in Indonesia

	171	BMS		REG	ULATED	LIMIT
1	SO		0	. 10	ppm	(260 mg/m³)
2	: CO		20	. 00	ppm	(2260 mg/m³)
3	NÖ	x	0	. 05	ppm	(92,5 mg/m³)
4	03		0	. 10	ppm	(200 mg/m³)
5	Du	st .				0.26 mg/m³
6	Pb					0.06 mg/m³
7	11 2	3	0	. 03	ppm	(42 mg/m³)
8	N H .	; 3	2	.00	ppm	(1360 mg/m³)
9	ll y c	irocarbon	0	. 24	ppm	(160 mg/m³)

(Source: Environment Agency:

Environmental White Paper '85)

Table 8-5-12 Regulated Limit of Exhaust from Mobile Sources of Generation in Indonesia

			<u> </u>			<u> </u>	:	:	
					Regul	ated lim	it of ex	haust	
	Type of vehicles	Fuel	Hode	CO	g/Km	IIC g	r/Km	NOx	g/Km
			í.	Max	Mean	Max	Mean	Max	Mean
1	Nine-passenger gasoline car	Gasoline	Ten mode	28. 2	24. 6	4. 2	3, 6	3. 4	3. 1
2	Gasoline car with a weight of 2.5 tons or less	Gasoline	Ten mode	31. 4	26. 8	4.8	4. 3	3. 7	3. 3
3	Diesel Direct injection	light oil	Six mode	ppm 1050	ррт 920			ppm 1010	. ррм 920
	Indirect injection	Light oil	Six mode	ppm 1050	ррт 920	ppm 680	ppm 590	ppm 1010	ррт 920
4	Two-wheeled vehicle								
	four cycle	Gasoline	ldling	4.5%		3300		-	-
	Two cycle	Gasoline	ldling		-	7800	-	· -	_

(Source: Environment Agency: Environmental White Paper 185)

2) Effect of Fuel Alcohol in Environment

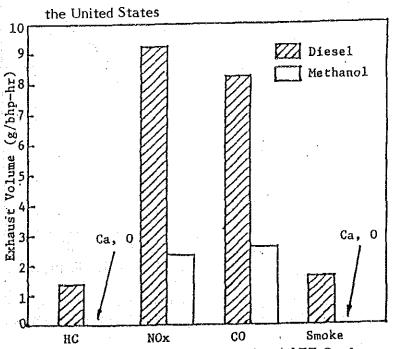
A mixture of gasoline and alcohol, clean fuel, has desirable effects on exhaust.

Air pollution in 2000 was estimated in California, USA. It is expressed by the level of ozon in the air.

		Peak O3
: "		0.333 ppm
:	. 5.	0.250 ppm
		0.285 ppm
	* * * * * * * * * * * * * * * * * * *	

Effectiveness of methanol to reduce ozone is shown on the above figures. Factors affecting air pollution include Nox, CO, HC, aldehyde, and smoke. A comparison of the volume of exhaust between diesel and methanol engines shows marked improvement in those factors, as shown in Fig. 8-5-7.

Fig. 8-5-7 Comparison of the Volume of Exhaust between Methanol Engine for Large-sized Vehicles and Diesel Engines in



(Source: Documents for the Sixth International AFT Conference)

NOx and smoke emission of diesel engines in densely populated areas is one of the biggest environmental problems. In case of diesel engine using diesel fuel, technical methods to reduce NOx, smoke and particulates cannot be found, unlike gasoline engines. On the other hand, spark assist diesel engine using fuel methanol (M100) can dramatically decrease the NOx and smoke emissions. Fig. 8-5-8 shows the estimated relation between atmospheric NOx-content and conversion ratio to methanol from diesel, which was studied on the basis of actual atmospheric NOx content of before-conversion in typical big cities in Japan and expected exhaust emission of methanol cars. According to Japanese environmental regulation in 1985, it is estimated that about 50% of diesel cars in densely populated areas must be converted to metanol from diesel oil to achieve 0.06 ppm (average of a day) of atmospheric NOx content allowed by the environmental regulation.

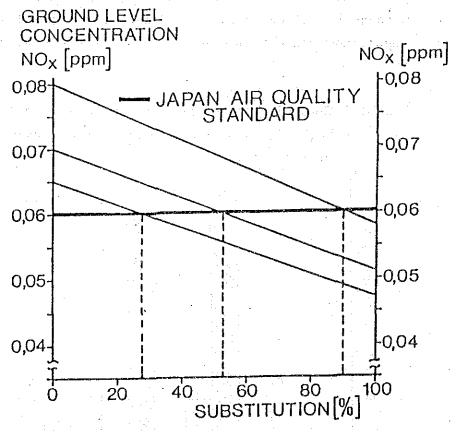


Fig. 8-5-8 Expected Improvement in Ground Level Concentration of Nox by Substitution of Diesel Fuel by Methanol in Japan (122)

Some reports on the formation of aldehde state that the level of aldehde in the exhaust is in proportion to the content of alsohol mixed. Fig. 8-5-9 show the effect of the level of motor alcohol on aldehyde exhaust (R.J. Nates: 7th International Symposium on Alcohol Fuels, Paris Oct/20 - 23 1986)

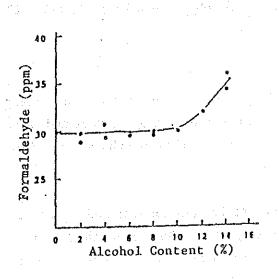
3) Test for the Effects of Aldehyde

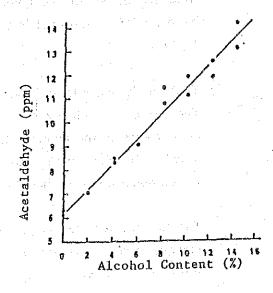
The effects of aldehyde, to which the closest attention is paid among components in the exhaust, have been evaluated using monkeys and rats, as with the chronic test, to understand the effects of exhaust caused by the combustion of methanol on human.

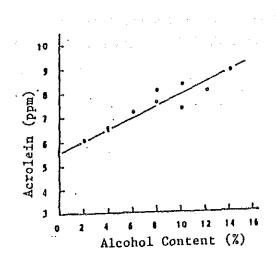
The highest test levels of aldehyde are 10 ppm for rats and 5 ppm for monkey, and the lowest level is one ppm, taking into account the fact that the level of aldehyde is 0.5 ppm or less at the outlet of a chimney and the precision of the control of test levels. Rats are exposed to aldehyde for three months and monkeys for one month.

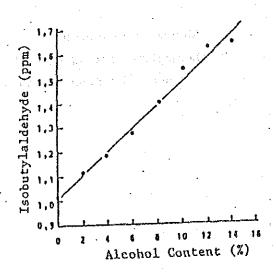
Moneys remain unchanged with one ppm of aldehyde, and showed reduced hemoglobin and ephemeral pneumonia with 5 ppm. Even one ppm of aldehyde slightly affected rats.

Fig. 8-5-9 Aldehyde vs Alcohol Content









puel: gasoline-motor alcohol mixture

(Motor alcohol: 70% C2. 21% C3, 9% C4)

Car: VW GOLF 1.6 @

8-6 Policy and Measures for Introducing Fuel Alcohol

8-6-1 Basic Policy for Introducing Fuel Alcohol

Over the last 15 years, because of economic growth, population growth, industrial expansion, and wider electricity distribution, domestic energy consumption has risen very rapidly.

The biggest problem is that the mix of energy sources in the domestic consumption pattern has grown too dependent upon oil and oil products during the same period. Unless Indonesia takes some action, she will consume all of its oil domestically, thereby depriving herself of one of the main sources of foreign currency needed for national development.

The Indonesian government has formulated a comprehensive energy policy aimed at minimizing the domestic consumption of oil and refined products and maximizing the use of non exportable energy sources.

The policy has four main pillars:

i) Intensification

To accelerate and intensify the survey and exploration of all energy resources, in an effort for a better identification of their potentials for an economic development program.

ii) Diversification

To reduce the dependence on oil in the overall domestic energy consumption and replace it with other available energy resources.

Priorities were set to develop non-exportable and renewable sources of energy: first hydropower and geothermal, followed by coal.

iii) Conservation

To economize energy use as well as to ensure its more efficient and wise use. This conservation program is being implemented through the following steps:

- a) Sectoral identification of wasteful energy use
- b) Providing information and educational programs
- c) Implementation through legislation and directives

iv) Indexation

To apply the best and most efficient energy source for each particular energy demand.

The policy is then elaborated as follows:

a) Domestic energy supply

To guarantee the domestic energy supply in amount and quality according to the demand and with a price affordable to the public, with the objective of improving the welfare of the Indonesian people and providing the necessary support for rapid socio-economic growth

b) Export of energy

To secure the supply of energy, not only for domestic use but also for export, to provide foreign exchange which can be used also for the development of new energy sources

c) Development of alternate energy sources

To develop alternate energy sources which are renewable but not exportable so as to lessen the consumption growth rate of exportable energy and ultimately repalce the non-renewable energy sources

d) Conservation of oil

Oil should be used as economically as possible, and possibly only for those application where the use of other forms of energy is not possible.

e) Protection of environment

In the development of energy resources, the protection of the environment should be maintained, to accomplish an improvement in the quality of life of the Indonesian people.

f) National resilience

The overall effort of providing energy and the management of the energy resources should bring an increase of national resilience which will enable the Indonesian people to face the future with more skill and confidence.

Fortunately, fuel methanol can be produced from natural gas and coal, including low grade coal, which are abundant in Indonesia. However, it will be the basic energy policy of Indonesia that crude oil, natural gas from large scale deposits and high quality coal shall be utilized for export to get foreign currency.

Therefore, major resources to produce fuel alcohol would be natural gas from small scale deposits, associated gas and low grade coal which would be produced by

open cut mining. The above-mentioned resources are difficult to export in view of economics and therefore will be effectively utilized to produce fuel methanol, resulting in reducing the domestic consumption of oil products.

Fuel ethanol will be produced from molasses, which is produced by the sugar industry as a by-product, and agricultural products such as sugar cane and cassava which will be produced in transmigration area.

Effective utilization of molasses will help decrease the production cost of sugar and development of the cassava market will support the transmigration policy as well as transmigrants lives.

Production of fuel alcohol will create new industry and working chances in Indonesia.

If one considers the above-mentioned energy policy and impact on economics in Indonesia, the production and utilization of fuel alcohol is strongly intended to be made part of government policy regarding energy, industrialization and transmigration.

As part of the basic policy for introducing fuel alcohol, the following steps will be recommended to have high priority in the introduction of fuel alcohol:

1st step: Fuel ethanol will be blended in gasoline up to the rate of 20%.

Raw materials will be molasses and cassava.

Dehydration facilities to produce anhydrous ethanol will be constructed. Delivery facilities such as tank lorries and service stations will also be built considering their reasonable combination with existing relevant facilities

2nd step: Neat methanol will be produced from natural gas, associated gas and/or low grade coal and consumed in gas turbine generators. Supply using the capacity of the Bunyu methanol plant will be given first priority in the 2nd stage. Necessary facilities including tanks and fuel supply system will be installed.

A fuel methanol reforming unit will also be installed if economical.

3rd step: Neat methanol will be consumed by diesel type power generators and special vehicles such as city buses, trucks and trains.

8-6-2 Production and Distribution

In Indonesia some key industries are run by the Government. Petroleum products that fall under this study are produced and distributed by PERTAMINA, together with methanol made from natural gas. The production and distribution of about 30% of the ethanol produced in Indonesia is attributable to ANEKA KIMIA. Both enterprises are wholly capitalized by the Government; the employees are treated as public service officials. Under such cirmumstances, fuel alcohol should be produced and distributed by state-run enterprises.

In establishing enterprises to produce and distribute fuel alcohol, the following basic items should be given consideration:

- The production and distribution of fuel alcohol should be based on the nation's energy, transportation, environment and transmigration policies. Such enterprises should secure a steady supply of energy.
- ii) Effective production and distribution of fuel alcohol as well as the existing fuels and products should be achieved.

With the above-mentioned items and the existing petroleum-related enterprises taken into account, the following is proposed:

a) Fuel Methanol Production

Natural gas as raw material: PERTAMINA

Coal as raw material

Coal production : Perum BATUBARA or PTBA

Methanol production : New state-run enterprise (A)

(under the Ministry of Mines and Energy)

b) Fuel Ethanol Production

Molasses as raw material: Existing sugar companies

Agricultural products as

raw material : New state-run enterprises (B)

Transmigrant should make products such as sugar cane and cassava in their settlements according to transmigaration policy, and in turn the new state-run enterprise (B) should purchase them. Hydrated ethanol should be produced by state-run enterprise (B) in the transmigration area. Then state-run enterprise (B) should make unhydrous ethanol from it to be distributed by PERTAMINA.

c) Upstream distribution

As production and distribution are inseparably connected with transportation, state-run enterprises A and B should take charge of transportation using their own facilities (storage tank, tankers, tank trucks, etc.)

d) Processing for Fuel

Judging from economic as well as technical aspects, a company (or enterprise) distributing final products should process them to make neat alcohol fuel or blend them with gasoline. For this reason, PERTAMINA should process them.

e) Downstream Distribution and Sales to End Users
In view of the convenience for end users, quality control, safety control, efficiency and so on, the role should be played by PERTAMINA.

Fig. 8-6-1 shows the roles of each entity involved in the processes ranging from the production of raw material to the distribution of final products by items.

Fig. 8-6-1 Suggested Production and Distribution Entity

	Production of raw material	Production of alcohol	Upstream distribution	Blending or processing	Downstream distribution	Sales to end users
Methanol from natural gas	PERTAMINA	PERTAMINA	PERTAMINA			
Methanol from coal	Perum BATUBARA or PTBA	New state-run enterprise(A)	(A)			
				PERTAMINA	PERTAMINA	PERTAMINA
Ethanol from molasses	Existing sugar companies	Existing sugar companies or New enterprise(B)	Existing sugar companies or New enterprise(B)		in de provinció espación de esca en anción de	i orderkki god godina bolovin godina bolovina
Ethanol from agricultural products	fransmigrants	New state-run enterprise(B)	New state-run — enterprise(B)		Elfrance George	

8-6-3 Incentives for Producers and Consumers

The above deliberations on the use of methanol in different economic regions and in the various consumption sectors have shown that the criteria for fuel alcohol use are divers. It has been shown that fuel alcohol production is in most cases economically unattractive if the price of oil is lower than \$30/bbl. However, there are other reasons to encourage or enforce the production of ethanol from molasses and cassava and methanol from natural gas and coal such as conservation of oil products, effective utilization of alternative energy sources, protection of the environment and others. The achievement of such goals requires governmental incentives and support. Although quite different strategic deliberations apply to each sector and region which might favour the use of fuel alcohol, it is nevertheless possible to define certain common policies which might be implemented by governments:

- the development of a generally acknowledged specification of fuel grade methanol
- more active research in the sector of methanol and ethanol production, with a view to reducing the production cost, with particular respect to fuel-grade alcohol
- comprehensive investigation into the use of fuel alcohol in new consumption areas, particularly the transport, heat and power, sectors;
- market analyses on the availability of raw materials, plant capacities, and general infrastructure, for the more active use of fuel alcohol;
- studies on the economic aspects of fuel alcohol production, on the basis of different raw materials;
- studies on the economic viability of fuel alcohol, as energy source for electricity and heat generation and as a transport fuel;
- studies on the repercussions from using fuel alcohol on other material currently used, e.g. in the transport sector, on the present structure of refineries or on the car industry.

Such investigations could be carried out by the governments, or possibly sponsored by governments as technology assessments.

Environmental protection is no longer a regional, but a global issue. This means that e.g. ethanol should be used as a substitute for lead in gasoline in Indonesia. Methanol combustion instead of fuel oil would substantially reduce pollutant emissions. Political measures to reinforce such targets would be e.g.:

- statutory regulations for reducing the lead content in gasoline
- government definition of emission standards could accelerate the desirable introduction of fuel alcohol
- government incentives to encourage fuel alcohol use in the transport sector

As mentioned in section 8-6-2, it is estimated that almost all producers are government enterprises and therefore a number of political decisions could be taken in the activities of each enterprise.

Incentives will be especially required for

- o Suppliers of molasses
- o Suppliers of cassava
- o Users of fuel alcohol
- o Car manufacturers

The following incentives will be recommended:

- 1) Incentives to suppliers of molasses
 - a) Competitive price setting to export molasses
 - b) Purchase commitment by ethanol producers
 - c) Tax discount for storage and transportation facilities
 - d) Financial aid for facilities
- 2) Incentives to suppliers of cassava
 - a) Reasonable price setting to support producer's life
 - b) Purchase commitment
 - c) Supply or rental of cassava production and transportation facilities

The above-mentioned incentives will be coordinated with the incentives of the transmigration policy.

- 3) End users of fuel alcohol
 - a) Tax discount for alcohol fuel cars
 - b) Price discount of fuel alcohol in view of calorific value, or price increase of oil products
- 4) Incentives to car manufacturers
 - a) Tax discounts for manufacturing facilities
 - b) Financial aid with low interest finance

As incentive to government enterprises, the required budget will be allowed in accordance with the priority of each introduction step. The following will be given higher priority:

- a) Dehydration facilities to produce anhydrous ethanol
- b) Blending, storage and distribution facilities of hydrous ethanol and blended gasoline
- c) Modification of existing gas turbine generators for fuel methanol use, including storage tanks and fuel supply system

8-7 Overall Evaluation

8-7-1 Impact on Demand for Petroleum Products

As discussed in section 8-3-2-(1) "Prospects of Long-term Demand for Fuel Alcohol", the necessary conditions for introducing all (1600x10³t, 2010x10³KL) of the fuel methanol from Banko coal is less than 111\$/kl of the methanol price under 30 \$/BBL of fixed crude oil price and should be more than 38 \$/BBL of crude oil under 139 \$/kl of fixed methanol price (the price corresponding to IRR 13.5%).

In comparison with the case of Ascope, which is the base for the LP model study, methanol volume on introduction is equivalent to 14% (810x10³kl of gas, equivalent) of demand for gasoline and 3% (222x10³kl of Kerosene equivalent) of demand for kerosene.

For ethanol introduction, 950x10³kl of ethanol (665x10³kl of gasoline equivalent), which is evaluated to the max. potential volume for the ultimate stage, is equal to 12% of gasoline demand in case of Ascope.

However, as both ethanol and methanol are to be introduced to Pertamina Supply Region III (JKT) and/or V (Surabaya), there should be some arrangement for actual introduction to the gasoline market in these regions. And also, introducing fuel alcohol into the conventional oil market should have the following impacts on the refining pattern and distribution of oil products:

As the impact of ethanol is very small, the impacts of methanol is described here.

(1) AM30 - AM37

In these cases, gasoline transportation to Supply Region III is to decrease and also gasoline transportation to Supply Region IV from Cilacap refinery is to increase because of the introduction of methanol into the gasoline market and/or kerosene market. Cilacap refinery will maintain max. production of gasoline, which has an important role to supply gasoline to Supply Region III, IV and V.

Gasoline transportation to Supply Region IV from Dumai refinery will decrease because of gasoline increase from Cilacap refinery. Although crude-runs in Dumai will decrese, reformate exports will increase.

(2) AM38

Gasoline transportation from Cilacap will further decrease compared with other cases mentioned above but will increase to Supply Regions IV and V. To make up for this gasoline, gasoline transportation to supply Region V from Balikpapan will decrease and lead to the increase of reformate exports. However, in this case, crude-runs in Balikpapan will keep the same level because of max. production of kerosen.

(3) AM-37

In this case, methanol is to be firstly introduced to the kerosene market in Supply Region II. The decrease of kerosene delivery to this region from Plaju will lead to an increase of deliveries to Supply Region III and kerosene production in Plaju will not change. And, as a result, kerosene from Cilacap to Supply Region III will decrease and increase to IV without changing its kerosene production.

Although kerosene delivery for Supply Region IV from Balikpapan will decrease with no change of crude-runs, kerosene fraction in the surplus is to be used as a blending stock for ADO and be exported.

Table 8-7-1(a) Impacts of Methanol Introduction on Gas. Flow

Case A-M-30 - A-M-37 (v.s. Case A)

			4% - 1				
To	Demand Arca 3	Demand Arca 4	Demand Area 5	Crude Oil Volume	Gasoline	Processed Volume by	
Dumai		3		1	⊕		Reformate T
Plaju				>			
Cilacap	T	T ②		>	>	→	
Balikpapan				>	••••	>	>
Demand Area for Methanol	. 0						

Table 8-7-1(b) Impacts of Methanol Introduction on Gas. Flow Case A-M-38 (v.s. Case A)

					1	<u> </u>	1	
To	Demand	Demand		Crude Oil	ļ	Processed		
	Arca	Area	Yrea	Volume	į	Volume by	Exports	
From	3	4	5	Processed	Production	Reformer		
							Reformate	T
Dumai	1	1		1	1	>	Kerosene	T
					(P)	l	ADO	1
		3					FO	<u></u>
Plaju	>			→	>	>	>	
1200						<u> </u>		
							· ·	
Cilacap	Ţ	T	. 1		>	>	→	
			:					
	0	2	②					
							Neformate	个
Balikpapan	:	1 1	1	>	1	>	ADO	1
Dattybakan			-				FO	1
			3		●	}		
Demand Area		-						
for	0							
Methanol	_							

Table 8-7-1(c) Impacts of Methanol Introduction on Kero. Flow

Case A-M-37 (v.s. Case A)

To	Demand Area 2	Demand Area 3	Demand Area	Demand Area 5	Crude Oil Volume Processed	Kerosone Production	Exports
Dumai					1	†	Reformate T Rerosene T ADO J IDO J
Plaju	9	÷ ②			>	>	<u></u>
Cilacap		© (-	†		>	****	
Balikpapan			D	>	-	(Q)	ADO T
Demand Area for Methanol	0		-				

8-7-2 Impact on Utilization of Natural Resources

If fuel methanol from Banko coal is to be introduced to the domestic oil products market in the future, 114 million tons of coal will need to be obtained from the Banko area during the thirty years of the project's life.

This utilization of non-commercial, low-grade coal will make $810 \times 10^3 \text{kl}$ of gasoline equivalent and $450 \times 10^3 \text{kl}$ of kerosene equivalent for surplus. The impacts of that introduction have already been discussed in 8-7-1.

As well as utilization of low-grade coal like Banko coal, small scale natural gas in remote areas from demand areas should be used for the conservation of existing exportable commercial energy on the one hand and export income assured on the other hand, which will aid the national interest of Indonesia.

Indonesia has a big population of more than 150 million people, of which 62% lived on Java island, which occupies less than 7% of total land as of 1980. Java island has 690 men/km² of population density compared with 77 men/km² in Indonesia as a whole. The population growth rate during 1980/1971 on Java island was almost 2.0%/annum compared during 1971/1961 with 1.9%/annum and this growth rate was rather small compared with 3.3%/annum in Sumatra, 3.2%/annum in Kalimantan and 2.8%/annum in Nusa Tenggara.

The transmigration program is construed as a multiobjective program. It is intended to provide land for the landless on Java, Bali and Lombok, to improve the distribution of population and at the same time provide manpower for the labor-scarce areas outside Java, Bali and Lombok so that the latter areas can develop as new centers of production, particularly agricultural production. The program is also seen as a vehicle to promote national stability and integration.

According to the results of general transmigration in 1981, 28% of a total 90,000 families flowed to the southern part of Sumatra, 14% to Riau (central Sumatra), 8% to the southern part of Kalimantan and 7% to south-east of Sulawesi. Transmigration from the eastern and central parts of Java is prevailing, which occupies about 40 to 60% in each region of destination. An overall trend is that from Java to Sumatra, Kalimantan and Sulawesi.

During the period of REPELITA-IV, the Government expects 750 thousand families to transmigrate. As for this transmigration plan, a voluntary transmigration program called Swakarsa is to be encouraged due to budgetary limits, and 250 thousand families will have during REPELITA-IV.

During the period of REPELITA-III, there were 527 thousand transmigration families, which surpassed the target of 500 thousand families. However, the newly established settlements are abandaned by many families.

In view of the present transmigration situation it is required to give a way for transmigration to assure an income source through cassave for ethanol production. More concretely speaking, besides a cassava price supporting policy, which will assure a certain level of income, a more detailed policy and measures to promote settlement of transmigrants will be required.

8-7-4 Impact on Environmental Policy

Indonesia is said to have a program to enforce environmental regulations on factories from 1987. Emission regulations for automobile have been enforced already, but periodical inspetion has been done only for commercial vehicles, and also, control is not severe.

In Jakarta, sometimes there are severe traffic jams and the city becomes smoggy which might be the result of poor adjustment of automobile engines and specifications of oil products.

As to the international situation on regulation of exhaust gas emissions, such materials as NO₂, NC, hydrocarbon, smoke and lead are the main targets for reducing air pollution. And also the tendency toward unleaded gasoline seems to be prevailing rapidly mainly in the U.S.A. and European countries. This issue will come to the fore in developing countries including Indonesia.

With this background, blending ethanol or methanol into gasoline as an octane booster and neat use of methanol in diesel engines in the longer term will be an effective countermeasure, which will reduce T.E.L. without deterioration of the octane number and smoke from buses and trucks, which contributes to reducing air pollution and improving the environment for people living in urban areas.

8-8 Conclusions and Recommendations

(1) Fuel Ethanol

- 1) The most preferable utilization of fuel ethanol is as automobile fuel as low blend gasoline.
- 2) The production of fuel ethanol from molasses is desirable. However, it is estimated to be difficult to commercialize by the private sector because of less profitability in view of financial analysis.
- 3) In the case of production from cassava, financial analysis shows rather worse economics than that of molasses.
- 4) On the otherhand, the production and utilization of fuel ethanol can contribute to the policies of the Indonesian Government such as transmigration policy, energy policy and environmental policy.
- 5) Taking into consideration the above-mentioned contributions, it is recommended that the concrete study for introduction of fuel ethanol be carried out in view of the following points:
 - i) Production plan including conceptual design of the related facilities and construction cost estimation
 - ii) Utilization plan including octane control system of unleaded gasoline
 - iii) Introduction policy and program of fuel ethanol in view of transmigration policy, energy policy and environmental policy

(2) Fuel Methanol

- It is recommended to utilize fuel methanol as an automobile fuel (M3 gasoline) and fuel for existing gas turbine generators, at the penetration stage.
- 2) Application of fuel methanol will be extended to gasoline engine (M85-M90) and diesel engines (neat). Such applications will be beneficial to city buses and trucks, diesel engine generators and reformed type gas turbine generators in the long-term.
- 3) The raw materials of fuel methanol will be isolated small scale deposits of natural gas and low grade coal such as Banko coal.
- 4) The enterprise for the production and up-stream distribution of fuel methanol will be a national organization of Indonesia, because the economic feasibility of methanol production is greatly influenced by the availability of low cost finance and overall energy policy of Indonesian Government.

5) The same kinds of study shown in 8-8-(1)-5) will be carried out for introduction of fuel methanol.

9. CONCLUSIONS AND RECOMMENDATIONS

(1) Conclusions

All of the studies scheduled in FY 1986 have successfully been completed.

- 1) The construction work of the pilot plant building in PUSPIPTEK was completed in September, 1986.
- Fabrication and transportation of equipment for the coal gasification test facilities as well as utilities facilities were carried out and completed in September, 1986.
- Field work of the coal gasification test facilities and utilities facilities was completed in January 1987, including acceptance inspection of equipment.
- 4) Mechanical and operation tests of the facilities, including a performance test, were successfully completed in March 1987.
 The operation test result shows that the coal gasification test can be

carried in FY1987 as scheduled.

- A coal sampling study was carried out including shallow boring and deep boring.
 - i) 2.7 tons of coal sample for mechanical and operation tests were taken by pitting in N.W. Banko.
 - ii) A total 2.2 tons of 10 coal samples for coal gasification in FY1987 were taken by a 101mm core drilling machine in N.W. Banko.
 - iii) The outcrop lines and coal seam structure in Central Banko and North Suban Jeriji were grasped, and coal sampling spots in FY1987 were decided.
- 6) The preliminary evaluation of mining cost of N.W. Banko coal were investigated. The mining cost of N.W. Banko coal is estimated to be 14.5 \$/ton-coal by shovel and truck system.
- 7) The preliminary evaluation of urea production cost has been carried out. The economics of urea production is inferior to that of methanol, and therefore it can be concluded that case II of the master plan (coproduction of methanol and urea) will be eliminated from further study in the 3rd stage.
- 8) The preliminary evaluation of electricity generation cost has been studied, applying the coal gasification-combined cycle power generation system.

IRR for sales in the Jakarta area is estimated to be 6.9 - 10.3%, on the basis of 98 RP/KWH of sales price in Jakarata as of 1985. The economics may be even or inferior to that of methanol production. It is concluded that lower cost finance than 6.9% year will be required and the study shall be investigated in more details in the 3rd stage.

- 9) Study of Market and Fuel Ethanol Distribution System
 - The most preferable utilization of fuel ethanol is automobile fuel as low blend gasoline.
 - ii) The production of fuel ethanol from molasses is desirable. However, it is estimated difficult to be commercialized by private sector because of less profitability in view of financial analysis.
 - iii) In the case of production from cassava, the financial analysis shows rather worse economics than that from molasses.
 - iv) On the other hand, the production and utilization of fuel ethanol can contribute to the policies of the Indonesian Government such as transmigration policy, energy policy and environmental policy.
 - v) Taking into consideration the above-mentioned contributions, it is recommended that a more concrete study for introduction of fuel ethanol be carried out in view of the following points:
 - a) Production plan including conceptual design of the related facilities and construction cost estimation
 - b) Utilization plan including octane control system of unleaded gaso-
 - c) Introduction policy and program of fuel ethanol in view of transmigration policy, energy policy and environmental policy
- 10) Study of Market and Fuel Methanol Distribution System
 - i) It is recommended to utilize fuel methanol as automobile fuel (M3 gasoline) and fuel for existing gas turbine generators at the penetration stage.
 - ii) Application of fuel methanol will be extended to gasoline-based engines (M85-M90) and diesel-based engines (neat). Such applications will be beneficial to city buses and trucks, reformed type diesel engine generators and reformed type gas turbine generators in the long-term.
 - iii) The raw materials of fuel methanol will be isolated small scale deposits of natural gas and low grade coal such as Banko coal.
 - iv) The enterprise for the production and up-stream distribution of fuel methanol will be a national organization of Indonesia, because the

economic feasibility of methanol production is greaty influenced by the availability of low cost finance and overall energy policy of Indonesian Government.

v) The same kinds of more concrete studies in case of fuel ethanol will be carried out for introduction of fuel methanol.

(2) Recommendations

- 1) The study in FY 1987 should be carried out in accordance with the Scope of Work
- 2) Strategic evaluation for the study as of the 2nd state should be carried out at the end of the 2nd stage.
- 3) Necessity of further study on the fuel alcohol market and its distribution system (See proposed points in Section 9-(1)-9) and 10)) will be seriously discussed by both sides.

APPENDIX I

Minutes of Meeting

MINUTES OF MEETING

THE FEASIBILITY STUDY

ON

EFFECTIVE UTILIZATION OF BANKO COAL

1. In accordance with the Scope of Work for the Feasibility Study on Effective Utilization of Banko Coal in the Republic of Indonesia, JICA sent the study team headed by Mr. Takehiko Sato to the Republic of Indonesia from June 16 to 27, 1986.

According to the prepared program, BPPT (the counterpart team) and the study team have discussed the following subjects:

- 1) The Inception Report (FY 1986)
- 2) The Interim Report II (FY 1985)
- 3) The study on market for fuel alcohol and its supply system
- 4) Construction of the coal gasification test facilities
- 5) Coal sampling schedule in FY 1986
- 2. The study team provided to BPPT 15 copies of the Inception Report illustrating the implementation plan of the Study to be carried out in FY 1986.

After discussion, BPPT and the study team agreed on the Interim Report on June 26, 1986.

Both sides confirmed mutually that the necessary budget for the Study in FY 1986 has been approved.

The major items of undertakings by each side in FY 1986 which were confirmed are as follows:

- Handling of equipments provided by JICA (by BPPT).
- (ii) Installation of utility facilities such as cooling tower and air compressor (by BPPT).
- (iii) Coal sampling in N.W. Banko and West Banko, applying machine boring (by BPPT and MTDC).
- (iv) Provision of utilities and consumerable materials required for construction and test run of the coal gasification test facilities (by BPPT).
- (v) Provision of equipment and materials of the coal gasification test facilities (by JICA).
- (vi) Construction and test run of the coal gasification test facilities (by JICA).
- 3. 15 Copies of the Interim Report II (FY 1985) summarizing the result of the study carried out in FY 1985 have been provided to BPPT by air mail.

 BPPT confirmed the acceptance and agreed on the Interim Report II (FY 1985).
- 4. The market of fuel alcohol and its supply system was discussed.
 The first Joint Meeting including the following relevant organizations was carried out on June 20, 1986 at BPPT office.

BPPT

DG of MIGAS

DG of E & NE

Ministry of Industry

Ministry of State for Population and Environment

Ministry of Communication

PERTAMINA

PLN

LEMIGAS

Central Bureau of Statistics

5. The study team prepared the Progress Report (draft), recording the results of discussion and site survey.

After discussions, BPPT and the study team agreed on the Progress Report on June 26, 1986, as shown in APPENDIX I.
15 copies of the Progress Report were provided to BPPT.

- 6. JICA study team explained the JICA's procedure of "bidding and order" of the construction work of the coal gasification test facilities to be installed at PUSPIPTEK in Serpong.
 - 1) Bidding and order will be issued by JICA INDONESIA.
 - 2) The following contractors will be invited to tender:
 - i) P.T. P.P.-TAISEI INDONESIA CONSTRUCTION
 - ii) P.T. JAYA OHBAYASHI
 - iii) P.T. WASKITA KAJIMA CORPORATION INDONESIA
 - iv) P.T. HUTAMA TAKENAKA CORPORATION INDONESIA
 - 3) The expected schedule of bidding and order is as follows:
 - . Explanation Meeting to tender: 20 June
 - . Closing date of quotation : 15 July

. Order of the work

. Arrival of JICA equipment

. Start of the work

. Completion of construction

: End of August

: Middle of September

: Beginning of October

End of January 1987

4) The following bid documents were provided and explained in details:

- . Request for Quotation
- . Requisition No. MP6-002
- . Project Specification No. MP6-002

Project Specification includes the detailed drawings for the construction work.

APPENDIX

I : Progress Report (June, 1986)

For JAPAN INTERNATIONAL COOPERATION AGENCY

For THE AGENCY FOR THE
ASSESSMENT AND APPLICATION
OF TECHNOLOGY

TAKEHIKO SATO

Leader of the Study Team Japan International Cooperation Agency pardens

26.6.86

WARDIMAN DJOJONEGORO

Deputy Chairman for

Administration

Agency for the Assessment &

Application of Technology

MINUTES OF MEETING

THE FEASIBILITY STUDY

ON

EFFECTIVE UTILIZATION OF BANKO COAL

1. In accordance with the Scope of Work for the Feasibility Study on Effective Utilization of Banko Coal in the Republic of Indonesia, JICA sent the study team headed by Mr. Takehiko Sato to the Republic of Indonesia from Aug. 13 to Sept. 11, 1986.

According to the prepared program, BPPT (the counterpart team) and the study team have studied on market for fuel alcohol and its supply system.

2. The Second and 3rd Joint Meeting including the following relevant organizations were carried out on Aug. 15 and Sept. 9, 1986 at BPPT office respectively.

BPPT

DG of MIGAS

DG of EP & NE

Ministry of Industry

Ministry of State for Population and Environment

Ministry of Communication

PERTAMINA

PLN

LEMIGAS

Central Bureau of Statistics

 The study team prepared the Progress Report (draft), recording the results of discussion and site survey. After discussions, BPPT and the study team agreed on the Progress Report on September 10, 1986, as shown in APPENDIX I. 10 copies of the Progress Report were provided to BPPT.

- 4. JICA study team explained the JICA's schedule the construction work of the coal gasification test facilities to be undertaken by JICA.
 - 1) Order will be issued by JICA INDONESIA
 - 2) The contractor will be nominated by JICA INDONESIA within this week.
 - 3) The expected schedule of construction work is as follows:

Order of the work

: Middle of September

Arrival of JICA equipment

: 21st of September

Start of the work

: Beginning of October

Completion of construction : End of January 1987

- 5. BPPT explained the BPPT's procedure of "bidding and order" of the construction work to be undertaken by BPPT
 - Bidding and order will be issued by BPPT 1)
 - 2) The contractor contracted by JICA will be invited to tender
 - 3) The schedule of construction work will be the same with JICA's work.
 - 4) request to the study team to prepare "Project Specification" to be undertaken by BPPT. The study team promissed to prepare the Project Specification as soon as possible.

6. Training for counterpart personnel in FY 1986

JICA study team explained that JICA will accept three trainees in FY 1986. The schedule of training will be around November and decided by JICA in due course. BPPT explained that the necessary official procedures by BPPT have completed on September 9.

APPENDIX

I : Progress Report (September 1986)

For JAPAN INTERNATIONAL COOPERATION AGENCY

For THE AGENCY FOR THE
ASSESSMENT AND APPLICATION
OF TECHNOLOGY

TAKEHIKO SATO

Cooperation Agency

Leader of the Study Team
Japan International

WARDIMAN DJOJONEGORO

Deputy Chairman for

Administration

Agency for the Assessment & Application of Technology

APPENDIX II

Schedule, Organization and Program,

Visited by the Study Team in FY 1986

SCHEDULE, ORGANIZATION AND PERSONNEL VISITED BY THE MINING TEAM(No. 1)

DATE	TIME	NAME OF ORGANIZATION	NAME OF ATTENDANTS
25/May (Man)	8:30-9:30 9:30-16:00	JICA Indonesia BPPT	Mr. Aoki Dr. Wardiman Djojonegoro Ir. Subagio Imam Bakri Ir. Bambang Suwondo Rahardjo Ir. Achmad Setiadi Ir. Untung Sumotarto Ir. Unggul Rriyanto Ir. Djoko Sulaksono Ir. Prapto Heljono
26/May (Tue)	10:00-14:00	PPTM	Ir. Komar Priatna Anwar Ir. Yuyun Basyuni Mr. Koen Mabsora Ir. Subagio Imam Bakri(BPPT) Ir. Bambang Suwondo Rahardjo (BPPT)
27/May (Wed)	9:00-10:30	DOC (Bandung)	Ir. Subandoro Ir. Subagio Imam Bakri(BPPT) Ir. Bambang Suwondo Rahardjo (BPPT)
	11:00-12:30	PPTM	The Same as 26/May
28/May (Thur)	9:30-11:00	PTBA (Palembang)	Mr. Zulyadin Ir. Subagio Imam Bakri(BPPT) Ir. Bambang Suwondo Rahardjo (BPPT)
	14:30-16:00	PTBA (Tanjung Enim)	Ir. Soetjipto wijadi Ir. Andi Massalangka Be. Rachman Sukardi
29/May (Fri)	10:00-12:00	CV RENE	Mr. Thalib Nasution Ir. Subagio Imam Bakri(BPPT)
	12:30-13:00	DOC (Tanjung Enim)	Mr. Parigan Ir. Subagio Imam Bakri(BPPT)
30/May (Sat)	9:30-15:00	PTBA (Palembang)	Mr. Zulyadin Ir. Subagio Imam Bakri(BPPT)
2/June (Mon)	10:00- 15:00	BPPT	Ir. Subagio Imam Bakri Ir. Bambang Suwondo rohardjo Ir. Yuyun Basyuni(PPTM) Be. Endang Yuyu Wiraatmadja, (PPTM) Mr. Mochammad Rochim(PPTM)
	17:00-18:00	JICA Indonesia	Mr. Aoki

Schedule, Organization and Personnel visited by the Study $\mbox{\it Team}$ ($\mbox{\it A}$)

DATE	TIME	NAME OF ORGANIZATION	·	NAME OF ATTENDANTS
June 17	14:00 - 17:00	BPPT		Dr. Wardiman Djojonegoro
				Mr. Subagio Imam Bakri
(Tue)				Mr. Unggul Priyanto
				Mr. Suharjono
				Mr. Untung Sumotarto
				Mr. Amiral A.
June 18	09:00 - 11:30	BPPT		Mr. Subagio Imam Bakri
(Wed)			<u></u> .	Mr. Bambang Suwondo
June 19	09:00 - 15:45	BPPT		Mr. Subagio Imam Bakri
(Thurs.)				Mr. Bambang Suwondo
		•		Mr. Unggul Priyanto
				Mr. Helmy Said
				Mr. Joko Prihiartoto
	: .			Mr. Untung Sumotarto
June 20	09:30 - 11:30	BPPT		Dr. Wardiman Djojonegoro
(Fri.)	•			Mr. Helmy Said
			* * ·	Mr. Joko Prihiastoto
			* *	Mr. Subagio I.B.
				Mr. Suharjono
		Pertamina		Mr. Torie Setiawan
		DG of E & NE		Ms. Maritje Hutapea
		C.B. of Statistic	S	Mr. Soewondo, Hp.

DG of MIGAS PLN DC of Industria	•
DG of MIGAS P L N	•
	v a at at
PC of Industria	Mr. Sudjanadi
DG of Industry	Mr. J. Purba
. "	Mr. Ir. Waluyo
LEMIGAS	Mr. Hendro Prawoto
Dept. of Communication	Mr. Maskur Effendi
Dept Of Communication	Mr. Maskur Effendi
	Mr. Mahdi Siahaan
	Mr. Soemanto
	Ms. Amala Nurhaida
BPPT	Mr. Helmy Said
BPPT	Mr. Bambang Suwondo
•	Mr. Achmad Setiadi
	Mr. Untung Sumotarto
PUSPIPTEK	Mr. Sulaiman Kurdi
BPPT	Mr. Subagio Imam Bakr
	Mr. Untung Sumotarto
	Mr. Joko Prihiastoto
BPPT	Mr. Subagio Imam Bakr
<u>.</u>	Mr. Helmy Said
DG of MIGAS	V . m . Olbanana
AND ON FRANCISCO	Mr. T. Sitanggang
	Dept. of Communication Dept Of Communication BPPT BPPT PUSPIPTEK BPPT

DATE		NAME OF ORGANIZATION	
	09:30 - 11:20		
	+ 1	Statistics	Ms. Supati
(Tue)			Mr. T.H. Suprono
		BPPT	Mr. Helmy Said
·	13:30 - 15:30	Pertamina	Mr. Torie Setiawan
		BPPT	Mr. Helmy Said
	13:30 - 15:30		Mr. Sulaiman Kurdi
: · · ·		(Jakarta)	
		BPPT	Mr. Subagio Imam Bakri
June 25	10:00 - 11:30	DG of E & NE	Mr. IGN GDE Pemayun
(wed)			Mr. M. Panjaitan
2.7	15:00 - 17:00	Mitsubishi Co.	Mr. S. Okuhara
June 26	12:00 - 13:00		Dr. Wardiman Djojonegoro
(Thurs)		6	Mr. Subagio Imam Bakri
			and all staff members.

Schedule, Organization and Personnel visited by the Study Team (C)

DATE TIME	NAME OF ORGANIZATION	NAME OF ATTENDANTS
Aug. 15 09:00 - 11:30	BPPT	Dr. Wardiman Djojonegoro
(Fri.)	·.	Mr. Bambang Suwondo
		Mr. Unggul Prijanto
		Mr. Achmad Setiadi
		Mr. Helmy Said
	•	Ms. Saraswati
		Mr. Indra Budi Susetyo
	C.B. of Statistics	Mr. L. Ginting
	MIGAS	Mr. T. Sitanggang
	PERTAMINA	Mr. L.M.L. Tobing
	D.G. of Basic Chemical Industries	Mr. J. Purba
	State Ministry for Population & Environment	Mr. Hendra Setiawan
	D.G. of Electric Power &	Ms. Maritje Hutapea
	Cilacap Refinery	Mr. R. Noerdanto
(Mon.)		Mr. B. Poediasmara
		Mr. Maskurun
		Mr. Mustofa
	·	Mr. Mohammad Yunus
		Mr. Tb. A. Alin
	(BPPT)	Mr. Suharjono
		Mr. Indra Budi Susetyo

n amis	M Than	*******		WE VE
DATE	TIME	NAME OF ORGANIZATION		ME OF TENDANTS
E-7 LA BRI EN WALLE LA .		ana ana ana may ana ana ana ana ana ana ana ana ana a		ging gina ayan asan man dann gard arab diri dirin dirin dirin dirin dirin dan asan asan dan ang arab ang ang a
Aug. 20	13:30 - 16:00	PERTAMINA	Mr	. Djoko Hernowo
(Wed.)	en e	en de la companya de La companya de la co	Mr	. Ibrahim L. Chaniago
			Mr.	. L.M.L. Tobing
* * **			Mr	. Hardono
	and the second second			
		врет	Mr	. Achmad Setiadi
Aug. 20	16:00 - 17:00	BPP'T	Ms	. Saraswati
(Wed.)			Mr	. Bambang Suwondo R.
*			Mr	. Helmy Said
			Mr.	. Indra Budi S.
Aug. 21	09:00 - 11:30	MIGAS	Mr	. E.E. Hantoro Ariadji
(Thurs.)	•		Mr.	. T. Sitanggang
			Mr	. Gono Soedimo
				. Hasyim
\$100, \$100, \$100, \$100, \$100, \$100, \$100.		ВРРТ	Mr	. Indra Budi Susetyo
Aug. 21	12:50 - 13:30	Department of Trans-	Dr	. Soedjino
(Thurs.)		migration	Mr.	. Helmy Said
Aug. 21	12:00 - 15:00	PLN	Mr.	. Hartoyo
(Thurs.)			Mr.	. P. Oka
			Mr.	. Sudja
				. Sudjanadi
	*			Suharjono (BPPT)
Aug. 23		PLN XI District Office		
(Sat.)	•		Mr.	Krisno Pandito
٠.			Mr.	. Sofyan Taca
	·	врет	Mr.	Suharjono
				•

DATE	TIME	NAME OF	NAME OF
LO CO CO LO LO LA SALES	#14 Time was time helps and then then the the time time the time the time the time time the time time the time time the	ORGANIZATION	ATTENDANTS
•			
Aug. 23	09:00 - 11:30	Balikpapan Refinery	Mr. R. Pradipto
(Sat.)	e de la Significa		Mr. Muzanulsyah
		<i></i>	Mr. Wagianto Sudargo
		BPPT	Mr. Achmad Setiadi
			Mr. Unggul Prijanto
Aug. 25	09:00 - 12:00	PD Acen Factory,	Mr. Dwipurwo Pangarso
(Mon.)		Mojokerto	
			Mr. M. Sukartono
			Mr. A. Rachman
			Mr. Oedojono
			Mr. H.M. Kholid
		вррт	Ms. Saraswati
			Mr. Bambang Suwondo
•			Mr. Indra Budi S.
Aug. 25 (Mon.)	10:00 - 12:00	Handil Oil Field,	Mr. Rako B.J.
			Mr. Madeo H.
			Mr. Dodi Budiristio
			Mr. A. Alkatili
		BPPT	Mr. Achmad Setiadi
			Mr. Unggul Prijanto
Aug. 25 (Mon.)	14:00 - 15.30	Senipah Terminal,	Mr. Rayadi
			Mr. Dodi Budiristio
		ВРРТ	Mr. Achmad Setiadi

DATE	TIME	NAME OF ORGANIZATION	NAME OF ATTENDANTS
Aug. 25	08:00 - 11:30	Power Plant, Kupang	Mr. Halomon Tobing
(Mon.)			Mr. Made Artha
	1. S. A.		Mr. Slamet Riyanto
		вррт	Mr. Suharjono
Aug. 26	11:30 - 14:00	Power Plant, Bali	Mr. A. Soetjipto
(Tues.)		and the second s	Mr. Nurbudi Rahardjo
			Mr. D. Derangin-Angin
		BPPT	Mr. Suharjono
Aug. 27	11:00 - 12:30		Mr. Maskur Effendi
(Wed.)		Communication	
		ВРРТ	Mr. Helmy Said
Aug. 28	09:00 - 10:30	LEMIGAS	Dr. Rachman Subroto
(Thurs.)		· · · · · · · · · · · · · · · · · · ·	Mr. Hendro Prawoto
			Mr. Hirwan Effendi
		ВРРТ	Mr. Bambang Suwondo
			Mr. Unggul Prijanto
Aug. 28	09:20 - 10:50	D.G. of Electric Power	Mr. Maraudin Panjaitan
(Thurs.)		& New Energy	
			Ms. Maritje Hutapea
		врет	Mr. Helmy Said

DATE		NAME OF ORGANIZATION	
Aug. 29 (Fri.)	09;30 - 10:30	D.G. of Basic Chemical Industries	Mr. Soenaryo Danusaputro
	Service Services		Mr. Jaweldin Purba
			Mr. H. Silaen
		вррт	Mr. Subagio Imam Bakri Mr. Achmad Setiadi
Aug. 29	09:15 - 11:30	PLN	Mr. Sudjanadi
		ВРРТ	Mr. Suharjono
Λug. 29		C.B. of Statistics	
(Fri.)			Mr. L. Ginting
			Mr. Helmy Said
	09:00 - 12:00		Mr. T. Sitanggang
(mon.)			Mr. Gono Soedimo
			Mr. Hasyim
Sept. 1 (Mon.)	13:30 - 16:00		Mr. L.M.L. Tobing
		врут	Mr. Achmad Setiadi
Sept. 1	16:00 - 17:00	вррт	Dr. Zuhal
(Mon.)			Mr. Subagio Imam Bakri
Sept. 2		Ministry of Communication	Mr. Maskur Effendi
•			Mr. Panal S.
-		· · · · · · · · · · · · · · · · · · ·	Mr. Soemanto
			Mr. Toga Hutabarat
	ert i de englishe en		
		ВРРТ	Mr. Helmy Said
			Mr. Unggul Prijanto

DATE	TIME	ann 300 ann àige ann àige ine an ann	NAME OF ORGANIZATION		
Sept. 2 (Tues.)	12:30	- 13:30	PLN 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	Mr.	Sudjanadi
			ВРРТ		Suharjono
	13:00		C.B. of Statistics		Soewondo Hp.
(Tues.)				Mr.	L. Ginting
		maji jenji yang kaya Bifu taun kunt nunt kata dana	ВРРТ		Helmy Said
Sept. 3	09:20	- 12:00	PERTAMINA	Mr.	Bambang Pitoyo
(Wed.)				Mr.	Javed Sumbung
	-			Mr.	Santoso Koerdi B.Sc.
	·		BPPT		Achmad Setiadi
Sept. 3	10:00		State Ministry of		Hendra Setiawan
(Wed.)			Population & Environment		
	-	•.		Ms.	Sri Hudyastuti
•	٠		ВРРТ	Mr.	Suharjono
Sept. 3	13:00	- 15:00	ВРРТ	Mr.	Ayusak Lubis
(Wed.)				Mr.	Fathor Rahman
				Mr.	Helmy Said
				Mr.	Achmad Setiadi
•					Unggul Prijanto
Sept. 4	10:00		The State Ministry for		
(Thurs.)		٠	Population & Environment		
				Ms.	Sri Hudyastuti
	11:00	- 15:00	Dumai Refinery	Mr.	Djunarto
			·		Achmadi
					Asyhab

 DATE TIME	NAME OF ORGANIZATION	NAME OF ATTENDANTS
Sept. 4 16:00 - 17:00 (Thurs.)	BPPT	Ms. Saraswati
	(PD ANEKA KIMIA)	Mr. Dwipurwo Pangarso

Schedule, Organization and Personnel visited by the Study Team (D)

Date	Time	Name of Organization	Name of Attendant
March 2	09.30 - 10.30	JICA	MR. AOKI
	13.00 - 16.00	ВРРТ	DR. WARDIMAN
			MR. SUBAGIO
		•	MR. BAMBANG
			DR. ZUHAL
March 3	09.00 - 11.00	вррт	MR. SUBAGIO
			MR. BAMBANG
			MR. SASAGURI
	15.00 - 18.00	ВРРТ	DR. WARDIMAN
			DR. ZUHAL
			MR. SUBAGIO
·			MR. BAMBANG
			MR. SETIADI
March 4	08.00 - 15.00	PUSPIPTEK	JICA OPERATION
		· .	GROUP
		• .	DR. LOLO
			MR. SUHARJONO
			MR. MAHALLY

Date	Time	Name of Organization	Name of Attendant
March 5	09 30 - 12 00		MR. SETIADI
ria; Cii J	03.30 - 12.00	•	DR. LOLO
			JICA OPERATION
		·	
er en er	·		GROUP
March 5	15.30 - 18.30	ВРРТ	DR. WARDIMAN
	•		MR. SUBAGIO
		·	MR. SETIADI
			MR. UNGGUL
			•
March 6	10.00 - 11.00	JICA	MR. ENDO
gradien Dies			(Part time)
			MR. AOKI
and the second	17.00 - 18.30	ВРРТ	MR. WARDIMAN
en de la companya de			MR. SUBAGIO
			MR. SETIADI
			MR. UNGGLE
March 7	08.30 - 16.00	PUSPIPTEK	MR. SETIADI
			MR. MAHALLY
			MR. SUBAGIO
			JICA OPERATION
AADOUL O	14.00 16.00	BUCDISTEN	
MARCH 8	14.00 - 16.00	PUSPIPTEK	MR. SETIADI

Date	Time	Name of Organization	Name of Attendant
			MR. SUHARJONO
			MR. SUBAGIO
			MR. BAMBANG
			JICA OPERATION
	•		GROUP
	•		
 March 9	08.30 - 12.00	PUSPIPTEK	(DEMONSTRATION
			CEREMONY)
	16.00 - 17.30	BPPT	DR. WARDIMAN
	-		(Part time)
			MR. SUBAGIO
			MR. BAMBANG
 March 12	08.00 - 09.30	ВРРТ	DR. WARDIMAN
•			MR. SUBAGIO
			MR. BAMBANG
			MR. SETIADI
			MR. SUHARJONO
		e de la companya de	MR. UNGGLE
			MR. EDDY
			MR. TEDDY
to the second second			
March 13	14.30 - 15.30	ВРРТ	DR. ZUHAL
			MR. BAMBANG
•	•		MR. SETIADI
	4.57 %	Alleria de Artico	MR. UNGGLE

. •				
			· • • • •	
	March 5	08.30 - 11.30	ВРРТ	IR. SUBAGIO IMAN BAKRI
				IR. UNGGLE PUJANTO
			en e	
	March 6	08.30 - 11.30	PPTM	IR. KOMAR PRIATNA ANWAR
	•			MOCHAMMAD ROCHIM B.E.
	March 7	08.30 - 14.00	PPTM	IR. YUYUN BASYUNI
•				MOCHAMMAD ROCHIM B.E.
				•
-	March 10	09.30 - 12.00	ВРРТ	IR. SUBAGIO IMAN BAKRI
				IR. ACHMAD SETIADI
		•		IR.UNGGLE PUJANTO
				IR. BAMBANG SWONDO
	March 11	10.00 - 12.00	PPTM	IR. KOMAR PRIATNA ANWAR
			ВРРТ	IR. SUBAGIO IMAN BAKRI
			·	IR. ACHMAD SETIADI

DATE	TIME	NAME OF	NAME OF
ري ندر بي ميو ندر ميا ندر خد خد مد اندر		ORGANIZATION	ATTENDANTS
March 10	10:00 - 12:00	MIGAS	T. Sitanggang
(Tues.)			Gono Sudimo
			•
		BPPT	Helmy Said
			Eddy
•	•		Novi
			Teddy
March 10	14:20 - 15:40	C.B. of Statistics	Soewondo
(Tues.)			Soeprono
			• • • • • • • • • • • • • • • • • • • •
		ВРРТ	Eddy
.*			Novi
			Teddy
		. The state of the	
March 11	09:00 - 11:30	PERTAMINA	H. Sudradjar P.K.
(Wed.)			Tobing
•		•	•
		BPPT	Helmy Said
			Eddy
·		·	Novi
			Teddy
March 12	09:00 - 10:30	PLN	Sudjanadi
(Thurs.)			
	-		
		BPPT	Helmy Said
			Dwi
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	11:00 - 12:00	D.G. of E.P & N.E	M. Hutapea
(Thurs.)		вррт	Dwi
			Novi
			A 1 1 √ ₹ -00
March 13	09:00 - 11:30	BPPT	Helmy Said
(Fri.)		•	A. Setiadi
			Eddy
			Novi
		•	Teddy
		424	Teddy Dwi

APPENDIX III

List of Documents, DWGs and Data

Submitted by the Counterpart

- 1. The Implementation of Energy Policy in Indonesia
- 2. Brochure of Cilacap Refinery
- 3. Brochure of Balikpapan Refinery
- 4. Brochure of Dumai Refinery
- 5. Energy Consumption by Sector (1975-1984)
- 6. A Field Survey Report on Social Economic Condition at Transmigration Area
- 7. Peak Load Production and Installed Capacity (April, 1986) PLN Region JAVA (Table-6)/PLN Region Outside JAVA (Table-3)
- PERKEMBANGAN PENJUALAN BBM DALAM NEGERI SELAMA III DASAWARSA 1950
 1984, by Hirwan Effendi (Lemigas) (Production of crude oil and sales of BBM in last 35 years)
- 9. Electricity supply by PLM in Indonesia 1983/84, 1984/85
- 10. IKHTISAR TARIP DASAR LISTRIK 1986 (PLM) (Tariff Table)
- 11. Review of Repelita IV (By PLN) (June 30, 1985)
 - Peak Load, Production and Installed Capacity (Java, outside Java)
 - Energy Production, Fuel Consumption and Fuel Cost (Java, outside Java)
- 12. DAEPAR KERJA PLN WILAYAH XI DENPSAR (Power Plant Map in PLM WILAYAH XI)
- 13. Number of VA Connected per Group of Tariff (June 1986)
- 14. Number of Connected per Group of Tariff (June 1986)

- 15. Number of KWH Distributed (sales) per Group of Tariff (June 1986)
- 16. Methanol Industry
- 17. Ethanol Industry
- 18. Demand for Methanol to Industrial Sector
- 19. Demand for Ethanol to Industrial Sector
- 20. Demand for Ethanol (spiritus) to Industrial Sector
- 21. Distribution System and Relevant Facilities by Ethanol Plant
- 22. Distribution System and Relevant Facilities by Ethanol Plant
- 23. System for Methanol Transportation
- 24. Projection of Methanol Consumption according to Region
- 25. Projection of Ethanol Consumption according to Region
- 26. Alcohol Industry
- 27. Energy Planning for Development (Phase II) Sep. 1985
 Energy/Development Int'l with Int'l Development and Energy
 Associates, P. T. Cipkocon
- 28. Energy Conservation in Indonesia (Final Report) by [Trans Energy for DG Listrik dan Energi Baru]
- 29. Agency for R&D in Dept of Communication Data and Energy Information for Transportation Sector (Indonesian language)
- 30. INDONESIAN MINING YEAR BOOK 1984

APPENDIX IV

Member List of the JICA Mission

STUDY TEAM A

Explanation and Discussion with Counterpart

UNDERTAKING	AREA OF EXPERTISE
Team Leader	Registered Consulting
	Engineer in Mechanical
	Engineering
Energy Demand	Evaluation of Alternative
Forecast	Energy
Methanol Production	Chemical Engineer
& Distribution Syst	em
Test Plant	Authorized Building
Building	Engineer
	Team Leader Energy Demand Forecast Methanol Production & Distribution Syst Test Plant

STUDY TEAM B

Coal Sampling for Gasification Test

NAME	UNDERTAKING	AREA OF EXPERTISE
Shozo IDA	Leader of Coal Mining	Mining Engineer
Tomoya KIKUCHI	Coal Mining	Mining Engineer
Hajime NOZAKI	Coal Mining	Mining Engineer
Atsushi NAKAI	Equipment Installation	Chemical Analyst
Tatsuya YONEMITSU	Mining Cost Estimation	Mining Engineer

STUDY TEAM C

Survey on the Supply System of the Fuel Alcohol Market

NAME	UNDERTAKING	AREA OF EXPERTISE
Takehiko SATO	Team Leader	Registered Consulting
	(x,y) = (x,y) + (y,y) = (x,y) + (x,y) + (x,y) + (x,y) = (x,y) + (x,y	Engineer in Mechanical
		Engineering
Taizo HAYASHI	Energy Demand	Evaluation of
	Forecast	Alternative Energy
Ryo SUZUKI	Methanol Production	Chemical Engineer
	& Distribution System	
Masayoshi SOGA	Demand Projection of	Chemical Engineer
	Fuel Alcohol	$\frac{\partial \mathcal{L}}{\partial x} = \frac{\partial \mathcal{L}}{\partial x} \left(\frac{\partial \mathcal{L}}{\partial x} - \frac{\partial \mathcal{L}}{\partial x} - \frac{\partial \mathcal{L}}{\partial x} \right) + \frac{\partial \mathcal{L}}{\partial x} = 0$
Satoru NISHIYAMA	Ethanol Production	Chemical Engineer
	& Distribution System	
Kenjiro TAKASE	Utilization Technology	Mechanical Engineer
	of Fuel Alcohol	
Hamao HAYASHI	Environment and Satety	Applied Chemistry
	• •	

STUDY TEAM D

Supervision of the Installation Work of the Coal Gasification Test Facilities

NAME	UNDERTAKING	AREA OF EXPERTISE
Hirotaka SASAGURI	Team Leader of the Test Plant Construction	Mining Planning
Ichiro TANIWAKI	Mechanical Construction	Mechanical Engineer
Toru MURAKAMI	Control of Electrical Work and Instrumentation	Electrical Engineer

STUDY TEAM E

Test Operation of the Coal Gasification Test Facilities

NAME	UNDERTAKING	AREA OF EXPERTISE
Takehiko SATO	Team Leader	Registered Consulting Engineer in Mechanical Engineering
Toshitaka YANAGI	Leader of Test Operation	Authorized Building Engineer
Yoshiharu NAKASITA	Design of Electric System	Electrical Engineer
Yasuaki HATAKEYAMA	Process Analysis	Technology of Coal Utilization
Koichi TANAKA	Test Plant Operation	Mechanical Operation
Shinji SUGIMOTO	Instrumentation	Electrical Engineer
Shigeharu YAMAGUCHI	Furnace Construction	Furnace
Kimikazu OTANI	Melting Furnace Controll	Furnace
Noboru ENDO	Melting Furnace Operation	Operation of Blast Furnace
Masanobu KOBATAKE	Gasification Furnace Operation	Operation of Gas Furnace

STUDY TEAM F

Explanation and Discussion with Counterpart

NAME	UNDERTAKING	AREA OF EXPERTISE
en e		
Takehiko SATO	Team Leader	Registered Consulting
		Engineer in Mechanical
		engineering
Tomoya KIKUCHI	Coal Mining	Mining Engineer
Taizo HAYASHI	Energy Demand	Evaluation of Alternative
	Forecast	Energy

APPENDIX V

BANKO COAL GASIFICATION

TEST PLANT

FINAL DRAWINGS

(Separate Volume)

APPENDIX VI

Techinical Specifications for the Construction Work (Separate Volume)

- Project Specification
 Requisition
 Request for Quotation

APPENDIX VII

Operation Procedure & Maintenance Manual (Separate Volume)

APPENDIX VIII

Computer Printout

- Urea Production Cost -

	(87/01/27	RUPIAH			6 0.5 7 221,60	7 376.177	44 67.734 64.824 64.834	3 1.68 94 5 1.29 + 0.9 8 28 + 46 11,38	7 12.9	0 16.29 0 16.29	3 279,			4 52,40	5 144.19
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			1996	193+906	0.55	,17	79.230. 67.734 3.324. 8.172. 3.345.	168,943 129,095 28,463 11,385	12,997	66+583 59+752 6+831		 	1,92	41,925	1 11
			1995	193+906	0.48	7.	7001 274574 274574 104102 34340	158.943 129.095 26.463	12+997	77,904 70,616 7,288		1	-17,094	-17,094	8 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
			1994	046	251,607	3+32	2,414 2,414 2,427 12,997 3,346 9,051	168.096 129.096 269.096 11.986	12,997	54.648 51.480 3.168	335,825	 	-72,501	-72,501	-72,50 ======
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	ANDONESIA TABOONESIA	SAS	E C	1	VOLUME (M.M.TON) PRICE (RUPIAH/TON)	REVEIRJE	VARIABLE COSTS TOTA RAW MATERIALS CATALYST/CHEMICALS PERSONALS (LUCAL STAFF) (JAPANESE:STAFF)	CONSTANT COSTS TUTA DEP 3 AMORT MAINTELANCE INSURANCE	OTHER DIRECT CUSTS ADMINISTRATIVE COST	INTEREST PAID (LONG) (SHORT)	TOTAL EXPENSES	INTEREST RECEIVED	PROFIT SEF TAX TAX	NET PROFIT	

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E P	ASE U = 3	EBOY PRICE	XICE 40000	:					UNIT=	MILLION	RUPIAH
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	376,177	1 %	376,177	76,17	76,17	76+1	10	4 40	76,17		76,
VARIABLE COSTS TOTA	74+434	74+404	74+404	74,404	74.404	74+404	74+404	74+404	74+404	74,404	74.404
CATALYST/CHEMICALS	34324	3.324	40-4-0 40-4-60	3.324	40 - 4 - 10 40 - 14 - 14	100m + m	40 E - E	461410	70.374	7,374	46/10
PERSONALS	3,346	3+346	3+346	3.346	3,346	3,346	3,346		3,346	130	
(LOCAL STAFF)	መ • መ ወ ቀ	948+8 0 0	3+8+6 0	3+340	3+346	3,346	3,345	3,346	3,346	3,346	3,346
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CONSTANT COSTS TOTA	168,943	168,943	166,943	59,977	216.65	59+977	59.977	16.6	39+848	39,548	39,848
DRT.	129,095	129+095	129,095	20-129	20,129	20,129	20,129	7.2		•	0
AALNI HAANCH	281453	28+463	28,463	20,463	28.463	28,463	28,463	တ်	4.	23,463	28+463
INSUSANCE	11,385	11,385	11,385	114385	11,385	11,395	11,385	 96	38	αj.	-4
OTHER DIRECT COSTS	12,997	12,997	12.997	12,997	12,997	12,997	12,997	12,997	12+997	12,997	12,997
ATIVE COST	6446	6 4 4 9 9	0.499	664+0	664.0	4	664.4	4	66449	4	•
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TOTAL EXPENSES	266,275	262,643	262,843	153,877	153,877	153,677	153.877	153,877	133,748	133+748	133,748
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47/01/27)	PIAH	2022	1-30	0.55	376+177		39.848 0 28.463 11.355	12,997	000	133.748	Ф	242,429	130,912	2,757,839
m	MILLION RUP	2021	1.93,906	0.56	376,177		39,848 0 28,463 11,385	12,997	ဝဝခဲ	133,748	a	242,429 111,513	130,912	2,626,927
PAGE	=LINO	2020	1.30 05.1	221,607	376,177	4400 4400	39,848 O 28,453 11,385	12,997	000	133,748	0	242,429 111,518	130,912	2,496,016
		2019	1,30	0.56 221.4607	•	4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	39 *646 0 28+463 11+335	12,997	200	133+748	၁	242,429 111,518	130,912	2,365,104 2
		2018	1.33	0.56 221.507	prof.	1	39,843 0 28,463 11,385	12,997	១ ០០	133+748	[[242,429	130,912	4,192
		2017	1.30	0456		74,4004 67,1734 87,824 87,826 87,846	39,648 0 28,463 11,385	12,997	000	133+748	 	242,429 111,518	130,912	103,280
	-	2616	1+30	0.56 221,607	1	71-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-	39,84¢ 0 28,463 11,385	12,997	000	133,748		242,429 111,518		o 11 - 11
		2015	1,33	0,56 221,007	375,17	1 + + + + + + + + + + + + + + + + + + +	39,846 3 28,463 11,385	12,997	000	133+748	.	242,429 111,518	0,91	4
5	ICE 40000	2014 1014	1.30 193,906	0.50	-	 + + + + + + + + + + + + + + + + + +	29. 20. 24. 24. 24. 24. 24. 26. 36. 36. 36. 36. 36. 36. 36. 36. 36. 3	12,997	990	133,748	9	242,429	130,912	710,5
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TOTAL	236,997	242,429	242,429	242,429	242.429	242,429	242,429	242,429	242,429	242,429	242,429
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TAX PAID	49,639	52,13	52,134	102+258	102,256	102,258	102,258	102,258	111,518	111.518	111,518
REPAYMENT TOTAL	135,799		o (:	į
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TOTAL	280+551	432,725	432+725	382+601	382+621	382+501	382+501	382+601	373+341	373+341	373,341
CASH (VET C/F)	18		100.250	4 1	140+171	140+171	140+171	- II	130+912	130,912	130,912
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	1448,432	339+127	529.423	.465+594	. 809+766		1+090+108	1,4230,280	1.361.192	1+492+103	1,623,015
RECEIVABLE ASSET INVENTURIES	526,925	504925	56+958	ં ફું	0		0	50,925	0 56.925	564925	56.925
FIXED ASSET	308+218	204+432	40.	80,517	Č+38	LC)	12				
	670.00	01000)) i:) i	, I	0 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		3	1
TOTAL ASSET	564,594	625,794	686+689	307,037	927.079	1+047+121	1.167.163	1.287,205	1,418,117	I+549,029	1.679.940
PAYABLES	0	9	3		0	· Co	G	0		0	0
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<u></u>	362,131	1562,131	H	362,131	352-131	7 * 7	 	13	2+13	5	***
ETAINED EARNINGS	202+453	263,063	24+86	444.905	76 4	α 3"	405+031		55.9	26	1,317,309
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8 AMORT. ONG) HORT) ENT TOTAL ESS)	6244262 6	242,429	242,429	545+429	242+429	242,429	242,429	242,429	242+429	242,429
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ENT TOTAL	0	0	9	0	<u>,</u> 0	O	Ö	O	0	O .
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TOTAL 373,341	. 373,341	373,541	373+341	373,341	373,341	373,341	373,541	373,341	373,341	373,341
CASH (NET C/F) 130+912	2 130,912	130,912	130,912	130+912	130,912	130,912	130,912	130,912	130+912	130,912

CASH	1+753+927	1+753+927 1,884+839	2,015,751	2,146,663	2,277,575	2+408+435	2,015,751 2,146,663 2,277,575 2,403,486 2,539,398 2,670,310 2,801,222 2,932,134 3,063,046	2,670,310	2,801,222	2,932,134	3,063,046
RECEIVABLE ASSET	၁	0	0	O	n	Ö	O	0	O	O	0
INVENTORIES	56,925	56,925	56+925	56,925		56,925 56,925	56,925	56,925	U	56+925	56+95
FIXED ASSET	၁	Ö	Ö	C	0	0	C	0	0	0	0
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TOTAL ASSET	1,410,852	1,410,852 1,941,764	2,072,076	2+203+588	2,334,500	2,465,412	2,072,076 2,203,588 2,334,500 2,465,412 2,596,323 2,727,235 2,858,147 2,989,059 3,119,971	2,727,235	2+858+147	2,989,059	3,119,971
PAYABLES	O	0	0	o	O	0	С	0	5	0	0
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EQUITY	362,131	362,131 362,131	362,131	362,131	362,131	362,131	362,131 362,131 362,131 362,131 362,131 362,131 362,131	362,131	362,131	362,131	362,131
RETAINED EARNINGS	1,448,721	1,448,721 1,579,633	1,710,545	1,841,456	1,972,363	2,103,280	1,710,545 1,841,456 1,972,363 2,103,280 2,234,192 2,365,104 2,496,016 2,626,927 2,757,839	2,365,104	2,496,016	-2,626,927	2,757,839
TOTAL LIABIL & CAP 1.810.852 1.941.764	P 1+810+852	1.810.852 1.941.764	2,072,676	2,203,586	2+334+1500	2,465,412	2.072.676 2.203.586 2.334.500 2.465.412 2.596.323 2.727.235 2.658.147 2.989.059 3.119.971	2,727,235	2,858,147	2,989,059	3+119+971

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m		362,13 2,888,75
CASH RECEIVABLE ASSET INVENTURIES FIXED ASSET UEFERRED ASSET	TOTAL ASSET	PAYABLES DEST (LONG) UEDT (SHORT) EQUITY RETAINED EARNINGS

TOTAL LIABIL & CAP 3,250,883

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	£) 1	Trr.	1999	1.30	0.0004	67,900	13+430 12+226 600 604 604	30,494 23,302 5,137 2,055	2.340	4.902 4.902 0	52+346	0	15,554	3,399	16.569
	PAGE	M =TIMU	1998	1,30	000.00	006.19	13,604 12,226 778 004	30.494 23.302 5.137 2.055	2,340	7+017 6+863	54.634	0	13,266	7,164	8+170
			1997	1.30	0456 40+090	006*19	13,953 12,226 1,127 1,127 504	30,494 23,302 5,137 2,055	2.345	9,467 8,824 . 645	57,433	0	10,467 857	9,610	1006
	ie.	·	1996	3 5 4 C	0.56	67.900	40400	30.494 23,302 5,137 2,055	2+345	12.01c 10.785 1,233	60+332		7+568 0	7,563	0 ii 4 ii 1 ii
			1995	1.1	0 • 4 8 40 • 00 0	57,715	1,2192	30,494 23,302 5,137 2,055	2,340	14,062 12,746 1,316	60.400			-3,085	,172. ======
			1994	• O O • S M	C+39	'n	11. 3.4558 4.558 1. 2.4550 1. 4.656	30.4494 23.302 5.137 2.058	2,340	15+279	60,616		3,03	-13,086	9086
	•		1993	1 0 6 1 0 6 1 0 6	000.04	9	000000	၁၁၁၈	၁ ,0	600	O	n	00	0	. II
	} -	CE 40000	1992	9.50	0°0°07	O	000000	9999	φ ÷	000	O		90	0	
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	## INDUMESIA	SAS		(NOT / YOY)	YOLUME (M.M.TON) PRICE (YEN / TUN)		VARIABLE COSTS TOTA RAM MATERIALS CATALYST/CHEMICALS PERSOWALS (LUCAL STAFF) (JAPANESE STAFF)	CONSTANT COSTS TOTA DEP 3 AMONT MAINTENAMCE INSURANCE	OTHER DINECT COSTS ADMINISTRATIVE COST	INTEREST PAID (LUNG) (SHORT)	TOTAL EXPENSES	! ا	PRUFIT BER TAX TAX	NET PRUFIT	13

** INDONESIA	ピタロピーハ	9900g	ECT						PAGE	2 (8,	87/01/27)
Ψυ	CASE U - 3	ISOV PRI	ICE 40000						UNIT=	MILLION YEN	
ļ		2002	2003	2004	2005	2002	2007	2008	2009	2010	·
4 P / L 40 L)			1 1 1 1 1 ! ! !	} 	8 8 1 1 1 1 1 1	 		H H H H	1
VOLUME (M.M.TON) PRICE (YEN / TON)	1.30 35,000	1.30	1.30	1.30	1.30	1.30 35,000	1.30	1.30	1.30	1.30	1,30
♦ IBOV VOLUME (M•M•TON)	0.56	0.56	0.56	0.56	0.56	ıc,	0.56	0.56	0.56	ın	0.56
_	40,000	40 + 000	40.000	40,000	40,000	40,000	O	40.000	40.000	40+000	40+000
REVENUE	006+19	67,900		7.9	67,900	67,900	67,900	67,900	006+19	006+19	67,900
VARIABLE COSTS TOTA	13,430	13.430		13,430	13,430	3 + 4	3+4	13+430	ļ ń	13,430	13,430
RAW MATERIALS	12,225	12,226	12,226	4.	N	12.226	2.2	\sim	12,226	12,226	12,226
CATALYSI/CHEMICALS	0 0 0	0 0 0 4	000	5000 5000 5000	000	000	600 604	000 0400	600 604	600 604	600 400 404
LUCAL STAFF)	604	409	604	404	409	400	400	409	409	400	604
JAPANESE		0	5	Ö	0	0	0	0	0	0	0
CONSTANT COSTS TOTA	36+49+	30,494	30+494	82	. 82	32	T)	Ω.	7+192	7+192	7,192
DEP & AMORT	234302	234302	23+302	ė.	.63	63	ð	÷.			
MAINTENANCE INSURANCE	54137	5+1234 2+055	5+137 5+5 5+5 5+5	5,137	2.055	7,57,57	2.055	2+055	2.055	2+055	2+055
			1			-			: :		
CTHER CIRECT CUSTS	2,340	2+340	2.340	2+346	2,346	41		m.	41	4	34.
ADMINISTRATIVE COST	11173	1+173	1+173	• 17	1.173	23.473	1 - 1 73	1.17	1.173	1+1/5	1.113
INTEREST PAID) 8 6	9	9	o	0	o	Ċ	•	¢)	O	0
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TOTAL EXPENSES	48+454	47 + 443	47+443	27+775	27+775	27+775	27,775	27,775	24.141	24,141	24,141
INTEREST RECEIVED		၀	r ɔ	5	Ö	0	C	· O	0	C	0
PROFIT BEF TAX TAX] 	20+457	0.45 9.41	0.12	127	0,12	51.62	2.4.7	3,75	•75 •12	60
NET PRUFIT	104	11,047		-	1 0	1 + 66	21,668	68	23.630	23,630	23+630
!		!!!!!!!!!!		1							

(87/10//27)	YEN	2022	1.3	40,000	67+900	13,43 12,22 60 60 60	7,192 0 5,137 2,055	2+346	000	24,141		43,758 20,129	23+630	062.784
rs W	MILLION	2021	1,30	000404	67,900	12,430 12,226 12,526 600 604 604	7,192 0 5,137 2,055	2,346	000	24,141		43,758	23+630	474,160
PAG	=LIND	2020	1.30	000404	ō	13+430 12,226 600 600 604 604	7,192 0 5,137 2,055	2,346 1,173	000	24,141	0	43,758 20,129	23,630	450,531
		ŀ	1.30	000404		11 1 2 4 4 4 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	7,192 0 5,137 2,055	2+346 1+173	000	24+141	i	43,758 20,129	23,630	426,901
		2018	1+30 35+000	0.55		12+430 12+430 12+600 6000 6006	7 * L 92 0 5 * 137 2 * 055	2,346 1,173	000	24+141		43,758 20,129	3,6	403+272
		2017	1.30	000*07	90	13,430 12,430 500 6004 004	7,192 0 5,137 2,055	2,346	500	174	! !	ואט	3 63	379+642
		2016	1+30	0.56	8	13.4430 12.226 600 604 604	7,192 0 5,137 2,055	2,346	000	24+141	i	43,758		356,012
		1	1.30. 35.000.	0.56	7 , 90	13.44 12.42.85 12.42.85 6000 6004	7+192 0 5+137 2+055	2,346 1,173	000	24,141		,75	3,63	332,383
-	CC 40005		1.30	0.0004	7,90	13.4430 12.4430 12.4430 12.4430 0000 0004	7+192 0 5+137 2+055	2,346	000	24,141		1 -1	9+63	308+753
PROJECT	IBOY PRICE	2013	1.30	95.0	67,900	13+ 12+ 12+ 12+ 12+ 12+ 13+ 143+ 15+ 15+ 15+ 15+ 15+ 15+ 15+ 15+ 15+ 15	7,192 0 5,137 2,055	2,346	990	24 - 141			63	285,124
נצבנ"ו	S - U - 3	2012	K	000404	•	13,4490 12,480 12,480 12,480 12,480 600 600 600	7+192 5*137 2,055	2,346	203	:		43,758	23+630	261,494
** INDONESIA	CASE		# P / L # # X9/-16 VOLUME (M+M+TON) PRICE (YEN / TON)	VOLUME (M.M.TON) PRICE (YEN / TON)		VARIABLE COSTS TOTA RAW MATERIALS CATALYST/CHEMICALS PERSONALS (LOCAL STAFF) (JAPANESE STAFF)	CONSTANT COSTS TOTA DEP & AMORT MAINTENANCE INSURANCE	OTHER DIRECT COSTS ADMINISTRATIVE COST	INTEREST PAID (LONG) (SHORT)		INTEREST RECEIVED	PROFIT BEF TAX TAX	NET PROFIT	RETAINED EARNING

PROJECT	3377 PRICE 40000	1		16.55	*006*445	1,0	1,27		12	++52	460+959	1,18	4	Ľ.	70+380 35+190		9 10	3+917	+040+553	0	65.5	i 🖈	† 14 † 13 † 14 † 16 † 16 † 16 † 17
עקבע מיו	ASE U - 3	2023	1+30 35+000	0+56 40+000	67+900 2	. ↓	12+220	2004	† †OO		7,192	9	5.137	S	2,346 1,173	•	.	· · · · · · · · · · · · · · · · · · ·	24.141 1		43.		521,420
ALSENDONI DOUGESIA	ບ		/ L & // / / / / / / / / / / / / / / / /	VOLUME (M.M.TON) PRICE (YEN / TON)	REVENJE	, ,	FERIALS	0.0000000000000000000000000000000000000	ריים אריים ((JAPANESE STAFF)	CONSTANT CUSTS TUTA	DEP & AMORT	MAINTENANOR	INNCANNE	OTHER DIRECT CUSTS ADMINISTRATIVE COST	; ;	CIANTON PALO	(SHONT)	TOTAL EXPENSES	INTEREST RECEIVED	PROFIT BEF TAX TAX	NET PROFIT	RETAINED EARNING H

## INDUNESIA	47E4*N	STO & d	ECT				·		PAGE	'n	37/01/27)
	ASE U - 3	و بروچے ا	RICE 40000						UNITE	MILLION YEN	.
	1990	1991	1992	1993	1994	1995	1996	1997	1998	6661	7
# C	0] 0] 7) 14 18 18 18 18 18 18 18 18	13 16 10 11 13 16 18 18 17 18	11 18 18 19 19 11	\$1 b1 \$1 \$1 \$1 \$3 \$3 \$1 \$1	10 10 10 10 11 11 10 11 11 11 11 11 11 1	12 12 16 17 18 16 16 18	11 15 14 13 14 14 15 16 16	16 16 19 17 17 18 18 18	61 91 91 91 91 91 11 11 11	()) 	11 11 11 11 11 11
NET TAX	:3 ?	9 :	5	.J	113+036	10 C	7,560	10+467	13,286	10,000	17.515
DON'THE STANDY.	16,825	17,865	5.56	7 + 3	ń) 9 •	٠ ١) () ()	0 0	n. •) 1
DEBT (LONG)	50,474	53,596	40,087	51.937	0 700	0 000	3 r	0.0	00	00	00
T T	67,299	71,462	53,449	69,249	4.51		3.3,869	33,769	30,568	38,856	40,317
CASH-DUT	! ! ! ! ! ! ! ! ! ! ! ! ! ! ! ! ! ! ! !			†	1			} } } } }		*	1
INVESTMENT TOTAL	642,18	71.462	3.14	9.24	0	0	0	0	0 (0 (o (
(SSCOURS)	40° 40°	48.300	200	202	0 (a ʻ	o ʻ	Ø 9	o 6	0 5	00
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(9212W00)		9 9	0	1 2 4	0	0 0		C. (0	ņ	0
(TANASPORTATION)	0804E	3.030	2,420	4		0		٠	0	ဂ	0
(TAAINING)	7	ဂ		90 40	0	ဝ	o	O	ວ	o .	0
CHOCK	61013	2*1*0	626*6	_	0	ဝ်	.J (Ł		u	(
CHAN TALE	·) ·	׳ כי)	Э (1	9		n c	0 1 1	1 U	
	5 7) ()) (ב כ	74.014	74.517	24.517	24.512	24.512	24.512	24.512
(SHORT)) ·J		ייי	יי			9	4.0	3+03		
TOTAL	67.293	71,462	53+449	69.249	24+512	24+512.	30.869	33.769	36,087	40.045	49.065
CASH (YET C/F)	101111111111111111111111111111111111111				9			0	2.119	7+139	i
11	11 	11 14 15 16 17 18 18 18	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	11 21 21 21 21 11 11 11 11 11	11 H H 13 14 15 17 11 11 31) F	18 10 10 10 10 10 10 10 10	(e 16 19 19 19 19 19 11 11	 	11 11 11	:
4 C	5	c	c	c	5	c	r	c	2.119	9.309	17+5-71
RECEIVABLE ASSET	ć. c	o ·5	0							. !	
EXECUTORIES	Ω #4° 64	0 0 k - 8 c ±	0 4 - 4	5.50	724	7210	210	0,27	2.57	7740	0,27
DEFERRED ASSET	5,649	15+461	27,61	45+68	41.41.	36,54	6476	27,41	22,84	+27	2
TOTAL ASSET	67,299	133,761	192.210	251,459	238,157	214,355	191,554	168,252	147,070	130,957	115+904
PAYABLES	က	o									
DEBT (LONG)	474+08	104401	144,157	196,094 0	171,582	147,071	122,559	98.044 7.404 7.404	7.3 • 6.3 0.0 0.0	49.024	24,512
EQUITY	16,825	34,690	48.052	65,365	5,36	5,36	5,36	38	65,365	65+365	5+36
RETAINED EARNINGS	0	o !		0	3,08	5.17	9 1 6 0	00	*17 -17	6,56	102
TOTAL LIABIL & CAP	67,299 138,761	138+761	192,210	261,459	238+157	21	191+554	168,252	•070	130,957	115,9
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187/0/181	Z	2011	43,75	43+75						20+17	:		57+388	23,630	1	292,954 0 10,275 0	303+22		65,365 237,865	303,22
ø	UNIT= MILLION YEN	2010	43,758	0	0) 0	00	0 0	00	20,129		ဂ	67.383	23,630		269,325 0 10,275 0	279,600	00	65,365 214,235	279,500
PAGE	UNIT	2009	43,758	43.758	0 0	,	00	ာဂ	00	20.129	5 0	0	67+388	23.	 	245,695 0 10,275 0	255,970	0 0	65,365 190,605	255,970
		2008	0+125 3+633 0000	0 43,758	00	כי כ	00	o a ·	ם כי	18+458	o o	လ	650469	25+301	 	222,065 0 10,275 0	232,340	00	65+365 166+976	232+340
	٠	1	40+125 3+633 0	0 43,753		ာ ဝ	ĊΕ	. O	a o	18,455	3 0	• •	654059	25.301		196+765 0 10+275 3+633	210+673	၁ ဝှ	65+365 145,308	210+673
		2006	40+125 3+633 0	43.758		c. c	ဝေ	9 9 1	00	15+458	OC	o	69.059		 	171,+54 0 13,275 7,267	500+65T	၁၀	5+36 3+04	189+005
		2005	40,125 3,633 0	43,758		ာဗ	ကြောင်	9 (9)	o 0	10+458	נ כי	ن	652+69		1 1 1 1 1 1	146+163 0 10+275 10+900	167,336	၁၀	65,365 101,973	167.338
		2004	40+125	0 43,758		ວເວ	o r	9 (9)	م ِم	13.450	9 (3	n	•	7	i 1 1 1 1 1 1	120+862 0 10+275 14+533	145,670		น้ำน้ำ	145+670
⊢	ICE 40000	2003	23,302	0 43+758	; 	၁ ၁	23 (1	о .э) (9+410	רבי ני	.3	75.167.	34.440		10,275 10,275 16,167	12+,003) ()	20 C	124+003
トン語つのでも	EBOY PRICE	2002	20+457 23+362 0	43.758		c. c	Э÷	ככ	o 1	7.410	⊙ • ɔ	•	76.107	1 2 4 4 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	11 15 15 16 16 16 16 16 16 16 16 16 16 16 16 16	61.212 0.10,275 30,900	112,950	(3 ·3	65°455 47.591	112,950
NEC'*	SE U 3	2001	19,476 23,302 0	0 42,778	0	o :5	э·	ל נ	ი .	64640	24.512	٠,	0 8 C + 7 C	10846		26 4 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	101,909		30,56	101,907
*¢ INDONESI4	CAS	1	# C / F * CASH-IN PROFIT SEF TAX DEPREC. & AMORT. EQUITY DEBT (LONG)	-//- (SHORT) TOTAL	CASH-DUT INVESTMENT TOTAL	(DTHER PLANT)	(SONKING)	(TRANSPORTATION)	(TRAINING)		REPAYMENT TUTAL (LUNG)	(SHORT)	TOTAL	1 1			TOTAL ASSET	PAYABLES DEST (LONG)		TOTAL LIABIL & CAP

AISENDONI DO	כמבכ"ח	PROJECT
ö	Se u-	3 IBOY PRICE
11	2023	TOTAL
BEF	43,758	65+59
•		1+1
EDUITY	0	65+36
DEBT (LONG)	၁	60.0
-//- (SHORT)	0	8+50
TOTAL	43.758	1+490+827
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(FURKING)	Ó	.5
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(TRANSPORTATION)	כי	
TRAINI	:)	
201		31.740
) 	20,129	÷
£ 74	Ö	214+080
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(SHOKT)	Ċ	10+592
TUT AL	67,389	73+33
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	25+030	570
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\$76,509 0 10,275 0	500+794	ن ب ب جوه خوه خه ۶۰۲۵ خوه ۲۵۶	1980-784 BREEFFERENCE BREEFFE
# B / S # Casy RECEIVABLE ASSET INVENTURIES FIXEU ASSET DEFERRED ASSET	TOTAL ASSET	PAYABLES UEBT (LOWG) DEBT (SHURT) EQUITY RETAINED EARNINGS	TÜTAL LIABIL & CAP =

(87/201/27)	ËN	2022	!	0.1		O	0	43.753	!	0	O	O	၀	ဂ	O	0	0	20,129	0	o	o	67,388	23+630
2	UNIT= MILLION YEN	2021	1 1	071.00	i o	ם י	0	43,758		כי	0	Ó	O	5	0	0	3	20 • 129	0	0	0	67,388	23,630
PAGE	ETIKO	2020	}	0 C	0	a	0	43,758		0	0	0	0	0	O	0	0	20,129	o	o	0	67.388	23,630
		2019	l J	0 C	0	0	0	43.758		O	0	0	0	O	G	c	0	20.129	Ö	၁	0	67,388	23.630
		2016		on:	רי ו	0	n	43,758	 	7	.3	O	O	(*)	()	n	٠,	20+129	cı	.7	n	585.75	23,430
		2017		0 (2 N = 6 f	. 0	0	0	43,753		O	O	n	٠,	0	ن.	13	o	20.129	O	ر .	၁	67,333	23+630
		2016	1 0 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	000	φ	0	ာ	43,758	; ; ; ; ;	0	9	Ċ	ن	٠,	ر.	د.	()	20.129	ن	ø	Ö	67,386	23+630
		2015	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	06.1404	0	Ó	O	43.753		2	ť	Ċ	<i>(</i>)	7	G	ი	וא	20+123	ֹכ	O	n	67,388	23,630
<u>+</u>	PRICE 40000	2014		0 (0	0.0	יס	o	43,758		Э	ာ	· つ	0	၁	n	o	ં	20+129	כי	٠,	a	67.390	23.030
PROJECT	Cac VCET	;	!	07.47	כי	0	0	43,758		Ġ	၁	· ɔ	ာ	>	·)	٠,	0	20+124	ာ	٠,	J	67,380	23,630
とならて "ハ	S - 3	2012 2013	8 5 Z 3 E 9) }	יט	9	7	43,758	; 	7	'n	· ɔ	つ	ז	Э	·ɔ	ာ	20+129	7	→	J	67,386	23,630 23,630
## INDONESIA	CASE	11		DEPREC. & AMORT.	EQUITY	DEBT (LUNG)	-//- (SHDRT)	TOTAL	CASH-JUT	INVESTMENT TOTAL	(PRUCESS)	(OTHER PLANT)	(ADRKING)	(OPENING)	(TRANSPORTATION)	(TRAINING)	(IDCP)	TAX PAID	REPAYMENT TOTAL	(LONG)	(SHORT)	TOTAL	CASH (NET C/F)

563,155	539+525	515,896	492,266	463,636	445,007	421,377	397,748	374,113	350,488	326,859 350,488	TOTAL LIABIL & CAP 326,859
497,790	474,160	450,531	426+901	403,272	379.042	356+012	332,383	308,753	285+124	261,494	RETAINED EARNINGS
65,365	65+365	65,365	65,365	65+365	65+365	65+365	65,365	65,365	65,365	65,365	EQUITY
0	0	0	0	0	0	O	O	0	0	3	DEST (SHURT)
0	0	0	Q	O	o	0	O	o	Ö		DEBT (LONG)
¢	0	0	a	o	э	э	O	0	o	ı3	PAYABLES
563,155	539,525	515,896	1	468,636		421,377	397+748	in i	350+488	326,859 350,488	TOTAL ASSET
C .	0	0	0	C	0	0	0	0	0 1		DEFERRED ASSET
٥	0	0	0	၁	0	0	0	0	0	0	FIXED ASSET
10,275	10,275	10,275	10,275	10,275	10,275	10,275	10,275	10,275	10,275	10,275	INVENTORIES
Ó	O	0	0	O	9	O	0	0	0	0	RECEIVABLE ASSET
2004700	クロン・ベンハ	7704606	166104	700+00+	ソケノキものも	701.114	7744707	4	2404040	+0000000	

APPENDIX IX

Computer Printout

- Electricity Generation Cost -

	עאבע־מ	PROJECT			:			:	PAGE	-1	(81/02/02)
CASE	m	PRICE=	11.552¥/KWH)	î					UNIT	MICLION RE	RUPIAH
	1990	1661	1992	1993	1994	1995	1996	1997	1998	6661	200
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VOLUME (SIL.KWT) PRICE (RUPIAH/KWH	00.49	64.00	00.00	64.00	2963.10	5598.05	64.00	4233.00 64.00	64*00	64.00	64.00
REVENUE	a	0	0	0	63	r-1	270,912	270+912	270,912	270.912	270+912
VARIABLE COSTS TOTA	 a	0	0	0	39,116	43,133	47.895	46,403	44,912	44,166	44.165
RAW MATERIALS	a	0	a	0	28,900	35,093	41,285	41+285	41,285	41,285	41,285
CATALYST/CHEMICALS	0	0	o	O	283	344	404	404	40 4	404	404
	0	0	0	0	9.934	7,696	6+205	41244	3+222	2,476	2,476
	a	0	a	0	2,476	2+476	2,476	2 • 476	2,476	2,476	143
(JAPANESE STAFF)	o	o	0	0	7,457	5.220	3+729	2,237	746	0	0
CONSTANT COSTS TOTA	0	0	o	0	128,515	128,515	128,515	128,515	128,515	128,515	128,515
DEP & AMORT	0	0	0	0	984886	98486	988486	98486	98,886	98,386	98.886
MAINTENANCE	0	0	Ö	0	21,163	21+163	21+163	21,163	21+163	21,163	21+163
INSURANCE	0	0	a	<i>a</i>	8,465	8+465	8,465	8 + 465	8,465	8 + 465	8 + 465
OTHER DIRECT COSTS	0	0	0	0	9.934	9*934	9.934	9 • 934	9,934	91934	9,934
ADMINISTRATIVE COST	၁	0	0	o	•	4,970	4.970	4+970	4+970	. 4,970	4.970
INTEREST PAID	. 0	0	0	0	65,764	60,886	52,581	42,027	31,266	21,433	12:632
(LONG)	a	0	0	0	63,162	54,741	46+319	37+897	29,476	21,054	12,632
(SHORT)	o	0	0	0	2,602	6,145	6,262	4+129	1,790	379	0
TOTAL EXPENSES	0	0	0	0	248,299	+43	243+894	231,849	219,596	209.018	2004217
INTEREST RECEIVED	o	} I]		Q	0	!		a	O	0
PROFIT BEF TAX		0	0		-58,661	-17,162	27,018	39,063	51,316	61,894	70,695
TAX	0	0	0	0	a	0	O.	0	19,124	28+471	32,520
NET PROFIT	o	0	ဝ		-58,661	-17:162	27,018	39+063	32, 192	33,423	38,175
17											

2 (87/02/02)	MILLION RUPIAH	2010 2011	Z33.00 423 64.00 6	270,912 270,912	44,166 44,166 41,285 41,285 404 404 2,476 2,476 2,476 2,476 0 0	29,629 29,629 0 0 21,163 21,163 8,465 8,465	9,934 9,934 4,970 4,970	000	88•698 88•698	0	182+214 182+214 83+818 83+818	98+396 98+396	864,276 962,672
PAGE	UNIT= M	2009	4233.00	270,912	44,166 41,285 404 2,476 2,476	29,629 0 21,163 8,465	9,934	000	88,698	0	182,214 83,818	98,396	765,881
	1	2008	4233.00	270,912	44,166 41,285 404 2,476 2,476 0	48,613 18,984 21,163 8,465	9,934	000	107,682	0	163,230 75,086	88,144	667.485
		2007	4233.00 64.00	270+912	44,166 41,285 404 2,476 2,476	48,013 18,984 21,163 8,465	9,934 4,970	000	107,682	C	163,230 75,085	88,144	579,341
	1	2006	4233.00 64.00	270,912	44,166 41,285 404 2,476 2,476	48,613 18,984 21,163 8,465	9*934	000 : . 	107,682		20	88+144	161.164
:	,	2005	4233.00	270,912	44,166 41,285 404 2,476 2,476	48,613 18,984 21,163 8,465	9+934	000		0	23	88,144	403+053
	KH		4233.00	164	44,166 41,285 404. 2,476 2,476	44.613 18.984 21.163 8,465	9+934	000	107,682	0	163,230 75,086	88+144	314+909
CT	11.552#/KWH)	2003	4233.00	270.912	44,156 41,285 40, 2,476 2,476 0	128*515 98*886 21*163 8*465	9.934	000	187,585		83,327 38,331	166.44	226,765
PROJECT	(PRICE=	2002	4233.00	270,912	44,166 41,285 404 2,476 2,476	128,515 98,886 21,163 8,465	9,934 4,970	000	187,585	0	83,327	166+35	181.768
C# CC *N	CASE E - 4	2001	4233.00	1640	44,166 41,285 404 2,476 2,476	128,515 98,886 21,163 8,465	9,934	4,211 4,211 0	191,795		79+11	42.7	12
## INDGNESIA	ູ້ ບໍ	ļ	# P / L # # NYF"; VOLUME (BIL.KMT) PRICE (RUPIAH/KWH)	REVENUE	VARIABLE COSTS TOTA RAW MATERIALS CATALYST/CHEMICALS PERSONALS (LOCAL STAFF) (JAPANESE STAFF)	CONSTANT COSTS TOTA DEP & AMORT MAINTENANCE INSURANCE	OTHER DIRECT COSTS ADMINISTRATIVE COST	INTEREST PAID (LONG) (SHORT)	TOTAL EXPENSES			NET PROFIT	RETAINED EARNING

3 (87/02/02)	MILLION RUPIAH	2021	233.0	0,912 270,912	44.166 44.166	S 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	476 2*	2		9,629 29,629	.163 21	446	9,934 9,934 4,970 4,970		00	69*88 88*69	0	2,214 182,214 3,818 83,818	8+396 98+396	46+627 2+045+023
PAGE 3	UNIT= MILL	2020	4233.00 422 64.00 6	270,912 27(166	41,285 41	474	476		29,629 29	21,163	.465	9.934	0	00	60	0	182,214 18: 83,818 8:	98+396	+848+232 1+94 ₁
		2019	4233.00	270,912		41+285	2+476	2+476	0	55,629	21.163	4.5	9.934	0	00	88.698	1	182,214 83,818	98,396	1+749+836 1
		2018	4233.00	270,912	44.166	41,285	2,476	2,476	၁	29,629	Ξ,	4	9,934	c	၀ ၀	88.698		182,214 83,818	98,396	1,651,440
		2017	1 00	270,912	44,166	41,285	2,476	2,476	0	29.629	21.163	8,465	9*934 4*970	0	00	88.698	1	182,214	98+396	1.553.045
		2016	4233.00	270,912	44,166	41,285		2,476		29,629	21.163		9,934	٥	0 0	88,698	1	182,214	98.396	1,454,649
	(HH)	2015	423	270+912	44.166	41.285		2,476	Φ.	29,629	21.163	8,465	9,934 4,970	O	00	88.698	1	182,214	98,396	1,356,254
<u> </u>	: 11.552¥/KWH	2014	233+0	270,912	44.166	41,285		2,476	0	29+629	21,163	8,465	9,934	0	00	88.698	-	182,214	98.396	57,858
PROJECT	. (PRICE=	. !	4233.00 4	270,912	44.166	41+285	2*476	2,476	0	29462	531-15	8+465	9,934	0	o c	869.88	0	182,214	98,396	1,159,463 1,2
N* 2382	CASE E - 4	2012	4233.00	270,912	44,166	41,285	2,476	2,476	0	29,629	21.163	8+465	9,934		0 0	88.698	1	182,214	98.396	,061,067
*÷ INDONESIA	٠		=== \$ N95"J VOLUME (BIL.KWT) PRICE (RUPIAH/KWH)	REVENUE	VARIABLE COSTS TOTA		PERSONALS	. ((JAPANESE STAFF)	CONSTANT COSTS TOTA	3 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	INSURANCE	OTHER DIRECT COSTS ADMINISTRATIVE COST	INTEREST PAID	(LONG)	TOTAL EXPENSES		PROFIT BEF TAX TAX	NET PROFIT	RETAINED EARNING 1

PROJECT	
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INDONESIA	

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PRICE=
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CASE

≎¢ INDONESIA	עמבר"ת A	PROJECT
	CASE E -	4 PRICE= 11.552#
•	2023	TOTAL
4 7 / C 4 4 10 10 10 10 10 10 10 10 10 10 10 10 10		
VOLUME (BIL.KWT) PRICE (RUPIAH/KWH)	4233.00 64.00	125085.15
REVENUE	270,912	
VARIABLE COSTS TOTA	4441	,325,61
KAW MAIEKIALS CATALYST/CHEMICALS	41,428	1,219,981
PERSONALS	57.	93.68
(JAPANESE STAFF)	0,4%	19,388
	29,62	2,65
DEP & AMORIT	0 525	83,78
INSURANCE	8+465	253,961
UTHER DIRECT COSTS	÷6646	298,006
_	4097	149,08
INTEREST PAID	0	290+801
(LONG) (SHORT)		269,493
TOTAL EXPENSES	88+698	4.0
INTEREST RECEIVED	0	0
PROFIT BEF TAX TAX	2,21	64
NET PROFIT	98	2,143,418
RETAINED EARNING		

THOMESTY	CXTC_W	rkuser I							PAGE	un.	(87/02/02)
	CASE E ~ 4	4 (PRICE=	11.552	*/KWH)					=LINO	MILLION RO	RUPIAH
i	0661	1991	1992	1993	1994	1995	1996	1661	1998	1999	2
C F C CASH-IN					 	 	 		1 1 1 1		i 1 1 1 1
PROFIT BEF TAX	0.6	0	0	0	-58,661	9 7	0.1	9	31	61.894	69
•	F69*67	001-77	- 1	,	24 CX	χ Σ	20.00	8 9 8	30	, 20 20	Š
DEBT (LONG)	218,080	231,569	173,200	219.317	0	0	0 0	•	0		•
-//- (SHORT)	0	o			65,045	23,546	C	o	0	0	
TOTAL	290,773	308+759	230,933	292,423	105,271	105,271	125,904	137,950	150+202	160,781	169,581
TOTAL	i	308.759) fr	7.47			: : : : : : :				
(PROCESS)	168,532	168,532	i un	ıκ		0	0	0	0	၁၀	
(OTHER PLANT)	85+459	85+459	ŝ	9649	•	o	0	O	0	0	Ü
CECKING	0 0	0 (0 (9,10	0 (0 (0 (0	0	0 (
(NO LEVELON (SOUTH A PER COLUMN)	000	0 0	0 , 0	4,00	3 (0 0	0 (0.0	ο (0 (•
(TRAINING)	,	•	7	2,38	, 0	,0	9 0) c		
(IDCP)	8,723	26,709	42,900	õ	0	0	0	0		0	
		0	0	0	i				19,12	28,47	+52
KEPATAGNI JOTAL	0 (0	0	0 (105,271	105 • 271	2,90	7,95	31,07	14,74	5,27
(SHORT)	מכ	50	00	00	7.00	2,40	20,633	32,	25,271	Š	02
TOTAL	290,773	308+759	i.u	2,42	105,271	105+271	125,904	137,950	150,202	178,348	201,372
CASH (NET C/E)						1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1					
1	91 11 11 11 11 11 11 11	1k 11 16 16 12 4f 10 11 11	6 19 18 16 16 18 18 18 18 18 18 18 18	11 12 13 14 14 16 10 11	10 10 31 51 91 81 81 81	0	11 31 31 31 31 11 11 31 31	14 19 10 11 11 11 11 11	11 12 13 13 14 14 14 15 16 17 18	11 12 13 14 14 16 17 18 18 18 18 18 18 18 18 18 18	
¢ B / S ¢ CASH	0	o	0	0	o	a	c	o	c	17.567	(AK - 07
RECEIVABLE ASSET	Ö	0	0	:) }
INVENIURIES FIXED ASSET	0.553.96.	0 207.503	•	39,102	39,102	39,102	39+102	39+102	~ ~	39,102	39, 10
DEFERRED ASSET		91,610	1 N	7,24	2	9,79		42.3	8,62	94	<u> </u>
TOTAL ASSET	2	599,532	651	1,122,889 1		925,116		727.343	628,456	547,137	480+042
PAYABLES		0	i	 	 	!	0	0	0	0	
DEBT (LONG) DEBT (SHORT)	218,080	6494644	622-849	842+166	736,896	631+625	ω 0	421,083	315+812	210+542	105,271
EQUITY	72+693	149,883	207,616	280,722	0.72	0.0		9 7	7,47	۲.	~
RETAINED EARNINGS	0	0			58.66	75,8	4.8.8	7.6-	22.45	55.48	40.46
TOTAL LIABIL & CAP		20		1,122,889 1	+024	925+116	826+229	727,343	628.456	547,137	740.047

								7 20	HILLIUN	LAT TOX
2001	2002	2003	2004	2005	2006	2002	2008	2009	2010	2011
9+117	Ф	83,327	ď	'n	3,23	•	163+230	182,214	182,214	182+214
94.00	96.88	98*86	98	18+984	18+984	48648I	18,984	a c	တိုင	
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178,003	182,214	182,214	132,214	182,214	182,214	182,214	182,214	182,214	182,214	182,214
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9 0	.	o c	5 C) (9 6	5 C	C	o C	• •	• с
c	• •	, c	, c	oc	oc		c			
36,394	38,33	38,331	75.086	75.086	75.086	75.085	75,086	83+818	83,818	83+318
105,271				! !	i					
5,271		၁	0	0	0		0	0	0	0
9	0	o	0	0	ο,	n	•	0	0	0
,34	326+097	326,397	289,342	289,342	289,342	289,342	289,342	280,609	280+609	280,609
36,339	1434883	143,883	107,128	107,128	107+128	107,128	107+128	98.396	98+396	98,396
1t 11 11 11 11 11	11 11 12 14 14 14 14 14	# # # # # # # # # # # # # # # # # # #)) 	U 11 11 11 11 11) 		it	H H H H H H H H H H H H H H H H H H H		
85,697	229,580	373,463	480.592	587,720	694.848	801.977	909-105	1.007.500	1,105,896	1.204.291
0		0	0			0		•		0
39,102		39,102	39+102	39,102	39,102	6	39,102	39+102	39,102	39,102
5,245	170+083	94,922	75,937	56+953	496	18+984	0		0	0
41,450	23,725	.	o	o ,	0	0	0	•	0	Φ _.
417,494	462+491	507,487	595,631	683,775	771,919	860,063	948,207	1,046,603	1,144,998	1,243,394
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O		0	0	0	0	Ω	0	0		
280 + 722	280,722	280+722	280+722	280+722	280,722	280+722	280 722	280+722	280,722	280,722
7 1 60	ij	7574077	**************************************	1000000	+74479	7124516	6044700	T004C0/	į	7)04706
417.494	107.649	507-497	505,521	482.775	771.010	860.062	200.300	1.046.603	1.144.009	1-242-204

** INDONESIA	עמבני"ח	PROJE	ECT						PAGE	2	(81/02/02)
:	CASE E - 4	+ (PRICE=	= 11.552¥/KWH)	(HH)					UNIT	UNIT= MILLION RUPIAH	ур I АН
	2012 2013	2013	2014	2015	2016	2017		2019	ı	2021	2022
CASH-IN		} 1 1 1 1 1 1 1 1 1 1	 	ı					1	 	
PROFIT BEF TAX	182,214	182,214	182,214	182,214	182,214	182,214	182,214	182,214	182,214	182,214	182,214
DEPREC. & AMORT.	0	0	a	0	0	0	, CO	0	0	0	٥
EQUITY	0	0	0	0	0		ი	0	0	0	0
DEBT (LONG)	0	0	0	0	0	0	n	0	0	0	0
-//- (SHDAT)	α.	0	O	0	0	0	ი	0	٥	0	Ġ.
TOTAL	182,214	182,214	182,214	182,214	182,214	182,214	182,214	182+214	182,214	182,214	182,214
CASH-DUT	 - - - - -		: : : : :		 	\$ } } !	; 1 1 1 1 1 1 1 1 1				
INVESTMENT TOTAL	0	0	0	0	Ö	O	٥	0	0	o	0
(PROCESS)	0	0	0	٥	0	0	C	0	0	0	0
(OTHER PLANT)	0	0	0	0	0	0	C	o	0	0	0
(NORKING)	O	0	o	o	0	0	C	0	0	0	0
(OPENING)	c	0	a	0	0	0	റ	o	0	0	0
(TRANSPORTATION)	0	0	0	o	0	0	0	o	0	0	0
(TRAINING)	0	0	0	0	0	0	C	0	0	0	o
(IDCP)	O		0	0	0	0	n	0	O	0	¢.
TAX PAID	83,818	83,818	83,818	83+818	83+818	83 + 818	83,818	83,818	83,818	83+818	83,818
REPAYMENT TOTAL	o	0	O	0	0	a	a	0	0	0	0
(FONG)	0	0	0	0	0	0		0	0	0	٥
(SHORT)	O	a	0	0	0	O	n	0	0	0	0
TOTAL	280,609	280,609	280+609	280+609	280,609	280+609	280+609	280,609	280+609	280+609	580+609
CASH (NET C/F)	984396	98,396	984396	98,396	98,396	98+396	98,396	98,396	98,396	984396	98 • 39 6
		R 11 11 11 11 11 11 11 11 11 11 11 11 11	######################################	11 11 11 11 11 11 11 11 11 11 11 11 11	11 12 31 51 51 51 51 51	11 11 11 11 11 11 11 11	10 10 10 10 10 10 10 10 10 10 10 10 10 1)) 	

2,325,745	1,538,581 1,636,976 1,735,372 1,833,767 1,932,163 2,030,558 2,128,954 2,227,349 2,325,745	2,128,954	2,030,558	1+932+163	1,833,767	1,735,372	1+636+976	1,538,581	1,440,185	1+341+789 1+440+185	TOTAL LIABIL & CAP 1,341,789 1,440,185 1,538,581 1,636,976 1,735,372 1,833,767 1,932,163 2,030,558 2,128,954 2,227,349 2,325,745
2,045,023	1,257,858 1,356,254 1,454,649 1,553,045 1,651,440 1,749,836 1,848,232 1,946,627 2,045,023	1.848,232	1,749,836	1,651,440	1,553,045	1,454,649	1,356,254	1,257,858	1.061.067 1.159.463	1,061,067	RETAINED EARNINGS
280 • 722	280+722 280+722 280+722 280+722 280+722	280,722	280,722	280+122	280,722	280+722 280+722	280 • 722	280,722	280,722 280,722	280,722	EQUITY
0		o.	0	င	0	0			0	0	DEBT (SHORT)
0	0	a	0	a	0	0	o	0	0	0	DEBT (LONG)
0	0	0	0	C	0	0	0	0	0	O	PAYABLES
2,325,745	1,341,789 1,4440,185 1,538,581 1,636,976 1,735,372 1,833,767 1,932,163 2,030,558 2,128,954 2,227,349 2,325,745	2,128,954	2,030,558	1,932,163	1,833,767	1.735,372	1+636+976	1,538,581	1+440+185	1.341.789 1.4440.185	TOTAL ASSET
0	0	0	0	0	0	٥		0	0	0	DEFERRED ASSET
0	0	Ö	0	O	0	0	o	0	0	0	FIXED ASSET
39,102	39,102	39,102	39,102	39,102 39,102 39,102	39,102		39,102	39,102	39,102 39,102	39,102	INVENTORIES
0	0	0	0	n	0	0	0	o		O	RECEIVABLE ASSET
2,286,642	1,499,478 1,597,374 1,696,269 1,794,665 1,893,060 1,991,456 2,089,851 2,188,247 2,286,642	2,089,851	1,991,456	1.893.060	1,794,665	1,696,269	1,597,874	1,499,478	1+302+687 1+401+083	1+302+687	CASH

UNIT= MILLION RUPIAH

CASE E - 4 (PRICE= 11.552#/KWH)

TOYAL
2023

												-													
0 11 11 11 11 11 11 11 11 11 11 11 11 11	3,969,293	5.0	80,72	2	59	6,264,559	,		1,122,889	-	· vo	_	4.30	29	7	6	25.87	930.7	42.16	8,59		8,649,596		0+080+7	######################################
11 11 11 11 11 11 11 11 11 11 11 11 11	182,214	0	0	0	Ċ	182,214	1 1 1 1 1 1 1 1 1 1		0	O	0	. 0	· a	. 0	· c	C	83.818		0	0		280+609	10	78,590	
4	PROFIT BEF TAX	٧.	EQUITY	DEBT (LONG)	-//- (SHORT)	TOTAL		CASH-DUT	INVESTMENT TOTAL	(PROCESS)	뽀	ORKIN	(OPENING)		RATATAGO	IDCP1	TAX PAID	EPAY	(LONG)	(SHORT)	-	TOTAL		へにへい、「川水」 じゅせい	

2,385,038	O	39,102	0	2,424,140	0	0	0	280,722
¢ B / S ¢ CASH	RECEIVABLE ASSET	INVENTURIES FIXED ASSET	DEFERRED ASSET	TOTAL ASSET	PAYABLES	DEBT (LONG)	DEBT (SHORT)	EDUITY

11.552¥/KWH)	15 %	. .	000*0	C	00	9	47679-22	9753 . 21	76002-09	69151-35	70-1700	04.9808	2992-08	5089-13	3743.00	9768.94	0100.40	75.0867	0191.08	*********	200.00	2027-600	0521.90	9288.63	161-13	170.49	300-10	535.37	863.46	273-11	154-45	298.69	898.27	546 47	237+36	965+78	727.17	517.51	333,31	ွ
2 E - 4 (PRICE=	(208) = 13.8	5	00000	S	8	8	32049,85	32049.85	88033 -23	-194720.214	*********	CQ-01925	78485.40	79976-81	81468-22	82213493	82213-93	82213-93	82213-93	64-51778 64-51778	8664545 866 866 866 866 866 866 866 866 866 86	F0'-F12'50	827131999	82213.93	82213.93	82213-93	82213-93	82213-93	82213-93	82213.93	82213-93	82213.93	82213.93	82213-93	82213-93	82213-93	82213:93	82213-93	82213,93	97026 • 44
87/02/32 CASE	I.R.R.	1	D #	, ,) IN	4	'n	\$	~	to t		07:		21		4 (13	16	7.	o 0) (2 6	7.7		24	25	26	27	20	56	30	31	35	es es	34		36		38	TOTAL

⇔⇔ INDONESIA	ビスログ・N	PROJECT	1.						PAGE	~	(87/02/02)
CAS	SE 8 - 4	(PRICE=	11.552*/KWH)	£	:	:			UNIT=	MILLION YEN	×.
	1990	1661	1992	1993	1994		1996	1997	1998	6661	200
# P / L # # # A NUTE # 7	1) 11 11 11 11 11 11 11 11	// 14 15 13 15 16 17 18 18 18 18		1) (t (t (t (t (t) (t) (t) (t)	/	D 11 0 0 11 11 11 11 11 12 11	{} {} {} {} {} {} {} {} {} {} {} {} {} {	18 41 41 41 41 11 11 11 11 11	 10 14 16 11 17 17 17 18	61 14 15 10 10 11 11 11 11	11 11 11 11 11 11 11
VOLUME (BIL.KNT) PRICE (YEN / KWH)	0.00	11.55	0.00	0.00	2963.10 11.55	3598.05 11.55	4233.00 11,55	4233.00 11.55	4233.00 11.55	4233.00	4233.00 11.55
REVENUE	0	0	0	0	34.230	41,565	48+900	48,900	48+900	48+900	48,900
VARIABLE COSTS TOTA	0	0	0	0	7,060	7,785		8,376	8+107	7,972	7,972
RAM MATERIALS	0 (0 (0 (0	5,216	6+334	7,452	7,452	7,452	7+452	7,452
PERSONALS	o o	ɔ ɑ	.	o c	1.6	1,389	1-120	2 43 25 25 25 25 25 25 25 25 25 25 25 25 25		73	73
	0	0	0	0	244	254	254	244	447	2 7 7	747
(JAPANESE STAFF)	a	0	o	0	1,346	945	673	404	135	0	0
CONSTANT COSTS TOTA	٥	Ò	o	0	23,197	23,197	23,197	23,197	23,197	23,197	23,197
DEP & AMORT	0 (O (0 (0	17,849	17,849	17,849	17,849	17,849	17.849	17.849
INSURANCE	0	. 0	5 0	o o	3,820	3,820	3,820	3,820	3,820	3,820	3,820
		•			 	1	 	! !	 - - -) - -
OTHER DIRECT COSTS ADMINISTRATIVE COST	00		00	00	1,793	1,793	1.793	1,793	1+793	1,793	1.793
INTEREST PAID	o	c	C	c	078-11	0000	. 07.0	7.586	2,443	9 0	000
(LONG)	0		0	0	11,401	9.881	8+361	6.840	5,320	3,800	2,780
(SHORT)	0		0	O,	470	1,109	1,130	145	323	68	0
TOTAL EXPENSES	0	0	0	0	44,818	44,662	44,023	41,849	39,637	37,728	36,139
INTEREST RECEIVED	0			0	0	0	0	0	0	0	0
PROFIT BEF TAX	O	0	0	0	-10.588		4.877	7.051	9.263	11-172	12,760
		0	0	a	! •		_		3,452	5,139	5.870
NET PROFIT	0	0	0	0	ô		4,377	7,051	5,811	6+033	6+891
RETAINED EARNING	0	0	0	0	-10,588	-13,686	-8,809	-1+758	4,052	10+085	16,976
#i	计设计化 医乳腺杆菌 计可以通过分 计时间 医环球球球球球球球球球球球球球球球球球球球球球球球球球球球球球球球球球球球球	11 11 11 11 11 11 11 11 11 11 11 11 11	;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;	() () () () () () () () () () () () () (11 11 11 11 11 11 11				4 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		11 11 11 11 11 11 11 11 11 11 11 11 11

INDONESIA Nº 275' PROJECT	CASE E - 4 (PRICE= 11.552#/KAH)	2001 2002 2003	4233.00 4233.00 4233.00 4233. 11.55 11.55 11.55 11.	0	VARIABLE COSTS TOTA 7.972 7.97	CONSTANT COSTS TOTA 23,197 23,197 8,775 DEP & AMORT 17,849 17,849 17,849 3,427 MAINTENANCE 3,820 3,820 3,820 INSURANCE 1,528 1,528 1,528	OTHER DIRECT COST 1,793 1,793 1,793 ADMINISTRATIVE COST 897 897 897 897	760 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	EXPENSES 34,619 33,859 33,859 19,437	. 0	PROFIT BEF TAX 14+281 15,041 15,041 29,463 TAX 6+569 6,919 6,919 13,553	7,711 8,122 8,122	60 40,931
		20	4233.00 11.55	48,900	7,972 7,452 73 447 447	8*775 3*427 3*820 1*528	1,793	G O O.	19,437		29,463 13,553	15,910	72,751
		200	4233.00 11.55	6	7,972 7,452 73 447 447	8,775 3,427 3,820 1,528	1,793	000	19,437	O	29,463 13,553	15,910	199
		2007	4233.00 11.55	48,900	7,972 7,452 73 447 447	8,775 3,427 3,820 1,528	1,793	000	19,437	0	29,463	15,910	104,571
		2008	0.00	48,900	7,972 7,452 73 447 447	34775	1,793	000	19,437	0	29,463 13,553	15,910	120,481
PAGE	UNIT=	2009	4233.00 11.55	48+900	2764-1 2782-1 447-1 744-1 0	5,348 0 3,820 1,528	1+793	000	16,010	0	32,890 15,129	17,760	138,241
2	MILLION YEN	2010	4233.	48,900	7,972 7,452 73 447 447	5+348 0 3+820 1+528	1,793	000	16,010	0	32,890 15,129	17,760	156,002
(87/02/02)	.	2011	4233+0 11+5	48+900	7,972 7,452 73 447 447	5+348 0 3+820 1+528	1+793	000	16,010	0	32,390	17+760	173+762

Ł	עאבע ארסשבר. AROJEC	 						ш	m	(87/02/02)
LAVE III	4 (PRICE=	: 11.552*/KWH)	(H3					UNIT=	MILLION YEN	z
2012	2013	2014	2015	2016	2017	2018	2019	2020	2021	2022
÷ P / L ÷ ÷ NYF*J VOLUME (BIL.#WT) 4233.00 PRICE (YEN / KWH) 11.55	4233.00 11.55	4233.00 11.55	4233.00 11.55	4233.00 11.55	4233.00 11.55	4233.00 11.55	4233.00	4233.00 11.55	423	4233.00 11.55
REVENUE 48,900	4	\$	48 + 900	48 + 900		0	48,900	48,900	48,900	48+900
VARIABLE COSTS TOTA 7+972	79.7	7,972	7+972		7,972	7,972	7+972		7,972	7,972
	7,45	7,452	7,452	7,452	7+452	7,452	7,452	٠	7,452	•
CALALISI/CHEMICAES (3 PERSONALS	- 44	44.4	447	447	744	444	447	447	447	144
STAFF)		447	244	447	0 2 4 4 7	544 C	744	447	447 0	744
CONSTANT COSTS TOTA 5+348	484 6	5,348	5,348	5+348	5,348	5,348	5+348	5+348	5,348	5,348
		0	0	0	0	0	0	0	0	0
<u>ய</u>		3,820	3,820	3,820	•	3,820	•	3,820	3,820	3,820
INSURANCE 1,528	1,52	1,528	1,528	1,528	1,528	1,528	1,528	1,528	1,528	1,52
OTHER DIRECT COSTS 1,793 ADMINISTRATIVE COST 897	1,793	1,793	1.793	1,793	1,793 897	1,793	1,793	1+793	1,793	1,793
INTEREST PAID		o	n	a	a	0	0	a	O	
(TONG)	0	•	0	0	0	Ġ	٥	0	O	0
~		0	0	0	0	a	0	Ö	0	
TOTAL EXPENSES 16,010	16,010	16+010	16.010	16,010	16,010	16+010	16.010	16,010	16,010	16,010
		0	o	a	o	O	0	O	О	0
PROFIT BEF TAX 32,890 TAX 15,129	32,89	32,890 15,129	, 89 , 12	, 12	32,890 15,129	32,890 15,129	32,890 15,129	וואוא	32,890 15,129	543
	_	17,760	ا مرا ا		-	• 76	17.760	17,760	17,760	17,760
RETAINED EARNING 191+523	209,28	227,043	20	2,564	0+325	8,085	18	3334606	351,366	369,127

UNIT MILLION YEN

{} {}

CASE E - 4 (PRICE = 11.552 x/KWH) 52,490 43,644 3,346 239,273 220,207 2,157 16,910 13,410 356,063 195,623 114,600 45,840 53,790 26,910 716,457 728,526 TOTAL 4233.00 125045.15 11.55 386,887 48+900 I+444+984 32,890 3,820 1,793 16,010 17,760 447 5,348 7,972 386,887 VARIABLE COSTS TOTA RAW MATERIALS CATALYST/CHEMICALS PERSONALS { LOCAL STAFF} (JAPANESE STAFF) CONSTANT COSTS TOTA DEP & AMORT MAINTENANCE INSURANCE VOLUME (BIL.MWT) PRICE (YEN / KWH) OTHER DIRECT COSTS ADMINISTRATIVE COST INTEREST RECEIVED RETAINED EARNING TOTAL EXPENSES PROFIT BEF TAX TAX INTEREST PAID (LONG) (SHORT) NET PROFIT REVENUE

** INDONESIA	ינצבכית ו	PROJECT	<u>+</u> ;						PAGE	5 (87	(87/02/02)
J	CASE E 4	(PRICE=	11.552¥/KWH)	KH)					UNIT= N	MILLION YEN	
	1990	1661	1992	19	199	1995	1996	19	1998	6661	. 2
C / F & C / CASH-IN	1 1 1		H H		ìI	iq 14 19 10 14 16 16 16 16 16 16 16 16 16 16 16 16 16	1 1 1 1 1 1 1 1			II II II II II II II II II II	
PRDFIT BEF TAX	0	9	O	0	-10.588	rn.	4+877	7 + 0	9,26	11+172	12,76
DEPREC. & AMORT.	0 (0 0 0	•		7.484	¥84	œ.	φ	84	7,84	₹*84
DEBT (LONG)	39,363	41,798	31,263	785 * 6E	o o	9 0		00	,	o o	00
-//- (SHORT)	o.	0			11+741	4+250	C	· o _	o,		
TOTAL	52,485		41,683	52,782	19,001	19,001	22,726	24+900	27+112	29,021	30+609
	; ;	 		į	1	1 1 1 1 1 1		! ! ! ! ! !	; ; ; ; ; ; ; ; ; ; ; ;		i ! ! !
INVESTMENT TOTAL	52,485	55,731	41,683	52,782	00	0 6	0 0	00	0 0	0 (00
(OTHER PLANT)	15,420	15,420	0,28	òò	0	0	00	0	0	o 0	
(WDRKING)	0 (0	0 1	7+058	O ·	0	0	0	0	0	_
(TRANSPORTATION)	5.070	0.0-5	0 85.4	177	o c	00	: :	o c	o c	0 0	
(TRAINING)	0)		0		o o	9 0	0	•	
	1,575	4,821	7,743	10,577	0	0	O	0		o	
TAX PAID REPAYMENT TOTAL	o c	O C	٥ ٥		Č.	0	, ,		3+452	ı, c	4,0
	0	0	0	0	100*61	19,001	19,001	19,001	8 8	19,001	19 00
(SHORT)	o	0	o	0	-	•	3,72	'n	65	.	
TOTAL	52+485	55,731	41,683	52,782	100 * 61	100461	22,726	24,900	27,112	32,192	.34
CASH (NET C/F)	3	O	0	a		0	C	0	0	3,171	
	1 3 1 1 1 1 1	[† 			14 14 14 14 15 16 16 16 16	2 1 1 1 1 1 1 1 1 1 1			11 H	
4 W / W 4		Ć		ć		•			(
CASH RECEIVABLE ASSET	.	o 0	3 0	5 0	00	o (90	5 C	o c	3,171	606+8
n	o	0		-	0.5	i,	0	_	7,058	7.058	ō
FIXED ASSET DEFERRED ASSET	45+840	91,080	122,240	152,800	139,233	125,667	112,100	98+533	84,967	71.400	57,833
				: 1 6						: '	10 4 7 1
IDIAL ASSET	72+485	108,216	144 84A	202+681	184+832	166+983	149,134	131,285	113,436	98+758	86,647
PAYABLES	0 20.05	7.	r	6		;	((0 6	0		
DEST (SHORT)	1 C	701410	674.47TT	110 + 261	3,01	4 K	0 4 C C	44,000	4004	38,003	19.00
EQUITY RETAINED EARNINGS	13,121	27,054	37,475	50+670	50.670	50,670	50,670	50,670	50.670	50+670	50,670
	-										
TOTAL LIABIL & CAP	507-65	100.214	000								

-	,	red ļ	i - 6		00	. 0	o.	i c	. 0	0	0 0		. 0	0.9	ס פ	00	, O	! <u>%</u>			in c	ာတ္ထင	> į į	ŭ i	0 0	5 C	2.2	! ഇ
(87/02/02	EN	201	, ,	•			32+89							ч	77 4 67		50+650	17.7			217437	7,05		C#+#22			50,670	224+43
•	MILLION YE	2010	11	0.	o c	0	32+890		0	0	0 0	o c	0	-	627.657 0	00	50+650	17+760			199,614	7,058		2)96907	0 (o c	50,670	206,672
PAGE	-LINO	2009		0 0 0	0 ¢	:	32,890		0	0	Φ (.	0		677467	00	50,650	17.760			181,854	7,058		1884912	0 (50,670	188,912
		2008	1	3:427	00	0	32,890	C	0	0	o 6	> 0	Ö	U		0 0	52,226	19,337	11 		164,093	7,058		7(747)7	0 (5 C	50,670	171,151
		2007	1	` rG	ი ი	0	32,890	r	C	n	חר	n	C	O 16		0 0		19,337		1	1444(5)	3,427		1554541	00	o n	50,670	155,241
		2006	20,46	3,427	n 0		32,890	0	0	0	o c		0	u V	2	0 0	52,226	19+337			125,420	7,058	, ,	1344331	0.0	.	0,67	139+331
		2005	644.00	3.42	00	Ģ	32,890	O	0	0	0 6	9	o	i.	,	00	52,226	19,337			1064083	7,058		7534457	00	3 C	2,75	123,421
	C H.B.	2004	£97.62		9 0		32,890		ò	0	9 (90	o	u	•	<i>o</i> o	•	19,337		. !	86.141	13,707	- 1	10(+)17	o (o o	50,670	107,511
CT	11.552¥/KWH)	2003		17,849	00	0	32,890	c	0	0	00	ם כ	0	5	67649	00	58,861	25.971			67+410	17,133		TOOLL	00	•	593	91,601
PROJECT	(PRICE=		1 4 5 0 6 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	17,849	00	0	32,890		0	0	0 0	9 0	0	ā	04476	00	58+361	25,971)		41,439	30,700	70744	829480	00	9 0	≻ 0	83,480
しな 日で *A	SE E 4	2001	: : : : : : : : : : :	17,849	o a	0	32,130	G G	· 🙃	0	?	o 0	o	G 23	194001	19,001	38,689	6,559	10 P P P P P P P P P P P P P P P P P P P		15,468	7,058	00040	104000	· 0 0	-	50,670	75,358
## INDONESIA	CA	Ì	1	•	DEBY (LONG)		TOTAL	CASH-OUT INVESTMENT TOTAL	(PROCESS)	(OTHER PLANT)	(WORKING)	(TRANSPORTATION)	(TRAINING)	(IDCP)		(LONG) (SHORT)	TOTAL	1		\$ S / 8 \$	CASH RECHTVARI B AAART	vo l⊷ v	ביייסטיל ביייסטיל	SUIAL ASSE	PAYABLES	DEBI (CONC) DEBI (SHORI)	TY INED EARNINGS	TOTAL LIABIL & CAP

** INDONESIA	במבכר יוו	PROJECT	<u>-</u> 1						PAGE	ļ~.	(87/02/02)
	CASE E - 4	(PRICE=	11.552¥/KWH)	EH.					=TINO	MILLION YEN	
il	2012	2013	2014	2015	2016	2017	2018	2019	2020	2021	2022
. \$, 1 1 1 1 1 1	 	\ 1 1 1 1 1 1	1 5 1 6 1 5 1 1	1 ! ! ! ! ! ! ! !	 	1 1 1 1 1 1 1	
PROFIT BEF TAX DEPREC. A AMORT.	32+890	32,890	32,890	32,890	32+890	32,890	32+890	32,890	32,890	32+890	32+890
7.4	0 0	. 0	0	0	9 9	o o	n 0	0 0	0	90	0
DEBT (LDNG) -//- (SHORT)	90	00	00	00	00	00	0 0	00	00	00	00
TOTAL	32,890	32,890	32+890	32,890	32,890	32,890	32,890	32,890	32,890	32,890	32,890
CASH-DUT INVESTMENT TOTAL	 		1 1 1 1 1 1 1 1 1 1	 							
	0	• •	0	o o	, c	0	n	0	0	, c	
(OTHER PLANT)	a	o	0	a	. 0	o	n	0	0	0	0
(WORKING)	a (0 (0 (0.	ο (0 (ဂ၊	0 (0 (0 (0 (
(TRANSPORTATIONS)	э с	o c	0 0	0 0	0 0	0 0	n c	6 C	o c	90	00
(TRAINING)	0	0	0	a	0	0	0	0	0	0	9 9
(IDCP)											
TAX PAID REPAYMENT TOTA!	15+129	15,129	15+129	15-129	15,129	15,129	15•129	15+129	15+129	15,129	15,129
	9 0	, o	0	o o	0	0		0	0	0	00
(SHDRT)	a		0	a	0	O	C	O	0	0	0
TOTAL	50,650	50,650	50,650	20+650	50,650	50+650	50,650	50+650	50,650	50,650	50,650
CASH (NET C/F)	17,760	17,750	7,760	17,760	17,760	17+760	17+760	17,760	17,760	17,760	17,76
1	 	t 	:	1 1 1 1 1 1 1		11 11 11 11 11	1 1 1 1 1 1	18 18 18 18 18 18 18	 .	12 11 11 11 11 13 14 14 14	
\$ \ S \ #											
CASH CASCATOR ASSET	235+135	252,895	270+656	288,416	306,177	323,937	341,697	359,458	377,218	394,979	412,739
ັທ	7,058	7,058	7,058	7+058	7,058	7,058	7,058	7,058	7,058	7+058	7,058
FIXED ASSET DEFERRED ASSET			-	a o	00	00	90	00	00	o o	00
TOTAL ASSET	242,193	259,953	277,714	295+474	313+235	330,995	348+755	366,516	384+276	402,037	419+797
PAYABLES	0.0	00	00	0		0 (0	0	0	0	
DEBT (SHORT)	0	0	o o	0 0	0		മര	၁ င	o c	G C	00
EQUITY RETAINED EARNINGS	50,67	50+67 09+28	50,670	50,670	50,67 62,56	5 14	r- 00	50,670	50,670 333,606	50.670 351,366	50,670 369,127
TOTAL LIABIL & CAP	242+193	259,953	277,714	295+474	313,235	330,995	348 . 755	366-516	384.276	780-504	410.707

UNIT= MILLION YEN

2023 TOTAL	32,890 716,457 0 195,623 0 50,670 0 152,011 0 15,991	30,75	0 202,681 0 101,400 0 51,400 0 7,058 0 16,900 0 24,716 0 24,716 0 15,129 329,570 0 15,901 0 152,011 0 152,011 0 152,011 0 152,91
# C / F #	SOFI SPRE SUIT	TOTAL	CASH-DUT INVESTMENT TOTAL (PROCESS) (OTHER PLANT) (WANTING) (OPENING) (OPENING) (TRANSPORTATION) (SHORT) (CASH (NET C/F)

430,499	7,05	437,557		W 14
÷ B / S ÷ CASH RECEIVABLE ASSET	SSET	TOTAL ASSET	PAYABLES DEBT (LONG) DEBT (SHORT)	RETAINED EARNINGS TOTAL LIABIL & CAP

APPENDIX X

Computer Printout

- Impact of Fuel Alcohol on Oil Refining Sector in Indonesia -

(1)Results of	methanol	Introdu	ction ca	ses					UNIT : 10*3 M
CASES	Λ	A-C	A-M	Р	P-C	P-M	К	K-C	K-M
(precondition)	HCOMPG.	100000	teone	Expanded capaci	T	0011114	Kerosene import	T	DCI ITAA
Domestic demand Grude oll export price Hethanol price [RESULT]	ASCOPE 30.55/28N No introduction	ASO)FE 30.5\$/BBL	ASODPE 1398/At	PELITA4 30,5%/PRL No introduction	PELITAA 30.5\$/88L	139\$/kt	PELITAA 30,55/88L No introduction	76L 17A4 30.55/88L	PELITAA 139\$/M
Crude oil export price	1	1	38.5\$/RRL	1	1	34.5\$/\$\$L	1	- t	38.5\$/BBL
Methanol price		111\$/W	†		12 13/ki	t		1115/kt	1
Amount of profit (10=3 \$)	18,260	18,355	23,883	18,107	18,120	20.860	18,011	18,141	23,917
Crude oil production SLC Arjuna	17:352	17:353	经验	19.88	经	43,352	17:375	13.352	17:35
Attaka Bekarai	3.701	4.701	170	1,01	1.01	1.70	1.00	1.701	4:70
Handil Arun condensate 101AL	87.753	87.05	87:63	7.535 87.653	87.63	7:535 87:053	37.053 87.053	37:535 87:053	87.05
Import of At	3,636	3,636	3,636	3,636	3,636	3,636	3,636	3,636	3,636
Crude oil processed DUMAI SLC	6,979	6,690	6.690	9,602	9.053	9.006	6,979	6,979	6,979
PLATI SLC	3: 122 3: 173	1,242	3,724	4:169 5:952	7.198	1:922	1:204	2.666 3.630	3:788
CILACAP Arjuna	6:18 1:18				1	10.509	6.181		
Arjuna Attaka Import of AL BALIKPAPAN	4,701 3,636	6.18] 3.636	6.181 3.636	11:337 3:68	1.00	1:89	3.6%	3:6%	6,181 3,636
dekarai Handi	3,888	3,888 8,442	3:88	3;892	3,88	3:882	3:332	3:838 8:442	3:33
TUTAL	40,123	39,834	39,834	53.563	49.833	49.820	40,123	40, 123	40, 123
Crude oil exports	33,251 8,520	35, 420 6,610	33.928 8.132	29,58)	33,31]	33,324	35.169 6.602	33.707 8.064	33.585 8.186
Arjuna Attaka Bekapai	8.520	6.63U	8.132	X	l 8	8	6,602 0 0	8,009 0	0.100
Handil Arum Condensate TOTAL	1.20	1.250	1.250	.z.595	,7.545	.7.592 .7.592	1.250 1.555	1.250 2.525	1.250
Natural gas exports	23:000	20,885	23:866	3.72	23:886	40:300 23:000	2.86	23:566	23.666
Production volume Propane	593	. 647	620	. 827	. 821	. 821	529	, 621	. 812
Butane Kaphtha Gasoline	3:39	1.23 5.252	1.315	1 300	\$:0%	8:0% 5:0%	4.704 5.025	1.75	333
Reformate Let fuel	. 52)	. 2		, 88	568	. 505	212 605		200
Kerosene A.D.U. I.D.O	9:535	8,430 1,540	2.53 2.53	1.83	17.83	1,83	u 33	1.87	11:33
Fuel oil L.S.W.R.	7,542	5.459 200	5,658	8,746	6,514	6,507	5,490 ani	5,490 300	5,490 300
Asphart Sulfur Cokes	374	248 248	248	37	48,200	355 331 48,209	27	36 38.86 38.86	248
Cokes	38,790 0	38, <i>5</i> 53 0	38,5%	51,850 0	48,200	48,209	38.334 4,834	38,864 4,834	38,873 4,834
Kerosene imports Total supply	38.790	38.553	38,596	51.850	48,200	48,209	43,168	43,698	43,707
Domestic demand Propane	463	. 463	463	463	463	463	463	463	463
i bitano	81	8	8	8		5.025	5.025	5 005	5 00
Paphtha Gasoline Jet fuel Kerosene	6.042 7.047	6.042 7.047	6,042 7,047	5.025 11.763	1 2.063 1 11.763	11.763	11.763	11.763	11,763
A.D.O. [.D.O.	7.138	7:170	[30	11.836	11.83	1.83	1.83	11,836	11.83
L.S.W.R. Assobalt	3.20	3,230 300	3,230 300	300	300	300	300	7,17 300 37,449	300
Asphalt TUTAL	26,133	26,433	26,433	37,449	37,449	37,449	37,449	37,449	37,449
Export volume Propane Rutane Raphtha Reformate	130 3,740	1.0%	1.012	1:361 8:393 593	1.358 1.362	358 1.362	. 13	1.013	1.010
Naphtha Reformate	l UI	4.663 1.237	4.315 2.80	8.393 593	8.028	\$: 6	4.068 217	4.731	4,721
A.D.O. Fuel oil	363 2.425 4.292	1.661 2.532 2.202	2:200 2:400 2:400	3,256	1,02Å	1,017	Ŏ Q	8	0
Kerosene A.D.O. Puel of 1 L.S.W.R. Asobalt Sulfur	. 81	ĮŠ	, , , , ,	<u>.</u> }	Š	55	8 45	43	1:30 84 84 84 84 84 84 84 84 84 84 84 84 84
Cokes TUTAL	12,357	13,132	24) 13,195	57 14,401	11.7%	11.745	5.719 5.719	7. 26 6	7,288
		· .							
Processed volume (each unit) Topping Dumai Plaju Cliecap Tall(papean TUTAL Reformer	6.279	6.69 25.50 39.883	6.690 13.538 33.834	18.89	3:053 8:186	9.006	6.979 14.518	6.979 8.238	6.970 13.518 23.128
Balispapan TUTAL	12.33	12:338	12:330	30.33	13:013 19:833		13:338 40:123	18:538 18:129	13:338 45:128
Reformer Dumai	794				702	702	, 723		
Reformer Dunai Clacap Balkpapan TUTA F.C.C. Plaju Hydro cracking Dunai Balkpapan TUTA TUTA TUTA TUTA TUTA TUTA TUTA TUT	1.83	1.789	1.22	1.025	1:19	1.783	1:784	1.025	1:72
F.C.C. Plaju	914	944	944	944	944	944	408	944	944
Dunai Bai kpapan	1.881 3.912	2.88 5.314	3,886 5,772	3.88	3.802 6,688	3.802 2:888 8:888	2.8% 5.772	2:886 5:887	2.8%
Methanol Introduction	3,912	5,314	5,772	6,715	0,688	9.088	5,112	2,081	2,112
Methanol Introduction Domand area 2 Gasol line(40, 52) Kerosene(40, 49) A.D.O. (40, 47) I.D.O. (40, 46)				١.	755	755.		755	755
A.D.O. (4), 47)		453	453		וכנו	150		130	199
		1,557	1,557					1 153	1,255
Demand area 3 Gasoline(#0.52) Kerosene(#0.49) A.D.O. (#0.47)		1,33(1,337		1,255	1,255		1.182	1,233
A.D.O. (*0.47) I.D.O. (*0.46) Total methanol volume		2,010	2,010	0	2,010	2,010	0	2,010	2,019
Oit products replaced Gasoline									· — - · · · · · · · · · · · · · · · · ·
Gasoline Kerosene	8	810 222	810 222	8	985 985	985 985	0	600 420	5 37

														-	
														· ·	
(2)Results of	mathanal	intro	which to	on one	, AG									INT	: 10+3 Af
CASES	A	A-N20	A-105	A-1026	A-121	A-X28	A-1629	A-190	A-IG1	A-1632	A-183	A-1134	A-105	A-106	A-107
(precondition) Domestic demand trute oil export price Methanol price	ASCUPE 30,58/88L	ASOTTE 30,337 ERL 13987 M	ASTOPE 13-58/881.	ASCIPE 30,337,088.	ASCOPE 27,537/BEAL 13947/AP	ASCOPE 23 ASTABL 13 M/M	ASCOPE 29,587,881.	ASTOPE 30,55/BRL 1396/H	ASODPE 11.55 / BSL	ASCOREE 32 SAVABL 1304/AB	ASCORE 33.35/SPL	ASCOPE 31.55/80t	ASODCE 35. STEEL 35.5 AL	ASCIPE SALVER SALVER	ASODE 77.55/RSL
RESULT]	No introduction	1398/Ai**	1395/62	13%7ui	1398/14	1396/kl	1391/14	1395/ht	1395/Ai	139\$/ki	1395/ki	1305/42	1595/44	139\$/W	1398/kt
Orude oil export price Nethanol price	1	†	1	t	† ·	1	1	1	1	1	t	1	1	1	1
Amount of profit (10+3 \$)	18.250	11.443	14,890	15,580	16,271	16.961	17,651	18.341	19.032	19,723	20,414	21,105	21.798	22,492	23.185
Crude oil production S. Ariuma Atlana Atlana		17.00	136	100	11.86		1:3	13	136	1:3			13.8		16
Bekapal Bandil Ann condensate WAL Import of AL	or and a	100 300 A	81.83	100 100 100 100 100 100 100 100 100 100		2000 2000 2000 2000 2000 2000 2000 200	3,63 3,63		81,05	81.63	5	81.63	9,83	81.00	1,00
Grude old processed	6,979	6,979	6,834	6,834	6.834	6.834	6.834	6.691	6.691	6.691	6,691	6,690	١.		V
MAN MAN CLAP	3 17	1:318	5:85	5.83	5:82	1.83	1.82	5:053	5:85	5:054 6:001	1.333 5.351	1.242 5:054	1	3:32	3:33
Allaka Import of AL RALIEDAN	6.181 3.63	1.68	1.730	1.6%	5.00	1.03	\$189 3:03	6.18 1.6%		6.18 3.636	6.18 3.636	6.181 3.636		6.18	6:18 3:636
Bekapal Bandil TOTAL	3.883 8.442 40.123	3.888 8.412 37.818	3,588 8,142 31.521	3.888 8.442 38.827	3,588 8,442 38,627	3, 888 8, 442 39, 978	3,888 8,442 39,978	3,888 8,412 39,835	3,858 8,442 39,835	3,888 8,442 39,835	3, 688 8, 442 39, 835	3,888 8,442 39,834		3,888 8,442 39,834	39,834
Crycle oll exports	33.251 8.520	34.828	35:889	35,278	35.276	₹.2% 8.6%	35.276		35.419 8.640	35.419 6.640	35.413	¥5.420	33.928 8.132	33.92	33.928 132
Ar Juna Attaka Rekapai Bandi J Arun Gordensale	1 200	1.20	1.20	} }233	1.20	1.38	1.20	I. X	1,33	1.7	170	1.27	1.70 28.88	1:258	1.77 23.88
Arun Condensate TUTAL Natural gas exports Froduction volume	3.88	\$:80 1.20	33.86	3,88		3.00		388	1	28,888	28.88	28:888	28:888	288	
Programe Butane Butane Butane Hashiba Gasoline Heformate Jet fuel Kerosene	7.02 7.02	3.30 3.30 3.30	370 3:52	1,000	1.00	166	1.00	1.65	1.88	1.88	188	1.85	1,000	1.00	
Reformate Jet fuel Kerosene A D O	621	621		1 (2)	اري ا	8.8	52 53 55 55 55			f∪	335		100 5.70 3.32 1.50	830	3:15
100. (80.) (81.) (81.)	7.10	1.50		5.31	5:31)	5.57	5,517	30	533					5,63 30	5:58
Asphalt Su) fur Coles TUIAL	*00 *24 *8.790	30) 35,485	35.30	30 37.561	37,561	33,672	30 28 38.672	38,532	30 28 38,53	30 38,54	30) 38,512	30 26 38,534	30, 38,97	38.59	30, 38,597
Kerosene imports Total supply	0 38,790	¥ ~	36,309	0 37.561	37,561	38,672		38,532	38,543	38,512	38,542	38.534	38.597	38,597	0 38,597
Domestic demand Propane Sutane	463 0	463	463	463	#53 0	463	463 0	463 0	463	463	463 0	463 0	463	463	463
Gasoline Let fuel	6.042 7.047	6.04 7.04	6.012 7.01	6,042 7,04	6.043 7.047	6.00 7.01	6.04 7.04	6.042 7.047	6.01	6,04 7,047	6.04 7.04	6.042 7.047	6.047 7:017 7:110	6.04 7.01	6.042 7.047
Leroscoc A.D.O. J.D.O. Jugil of I	130	1:20	1:2		1.3	3.28	120		123	1,2	138	1.20	3;25	133]; <u>1</u> 3
inel oil Such Aspoilt 1072	26, 103	26.433	25.433	26.433	26.433	26,83	25, 33	25,433	26,433	25.00	26 133	25, 333	25,433	25, 333	35.ES
Export volume Propane Butane Naphtha	130 3.740	118 3.338	127 3.457	1:97		1.83					אייי ו	1:18		1:48	1:47
Beformate Verosene A.D.O. Fuel oil	2.35 4.25	138	3.457 2.23 1.83	2.23 2.06	3,974 2,233 2,06)	1.75	1.39	1.57 2.30	1.563	1.66 2.30	1:30	1.20	4.00 2.20 2.40	1.17	3.23 2.43 2.43
ETTESTE L.D.O. L.S.W.R. ASTRALL SULTUT CARS TUTAL	3.746 2.22 4.22 12,337	10.09		11.185	l 8	12.2%	12.2%	r 11	l 8	12,348	12.240	12.42	12.513	12,513	12.78
fulli. Processed volume (each unit) Topping	/										: "				
Processed volume (each unit) Topping Tusai Flaju Cliacap Salipapan Unit. Reformer	6.50 10.12 10.12	177	6:33 12:067 17:27	12.27	13.0	12.33	6:834 13:336 33:336	6.60 14.518 37.835	\$ 50 15 15 15 15 15 15 15 15 15 15 15 15 15	550 11.51 37.83	6.69 11.58 30.88	6.690 13.518 10.831	\$ 500 111 111 111 111	11.00	1558
Reformer Dunal						39,978 788									
Reformer Dural Clacap Balispapan III A. F. C. Plajo	772 1.00 3.02 941]:23 344].78].82 94].733].235 944		753 1.93 944	723 1 693 944];22 94	723 1225 944	1:22	146 176 176 176 176 176 176 176 176 176 17
Rusei Balikpapan Wind]:33]]:33]	2.88 1.887	l .	2.886 5.314	2.8% 5,314	9	2.886 5.314	2.886 5:314		2.88 5.31	3.5% 5.3%	2.886 5.314	2.886 5.772	94 2.88 5.72	2.8% 5.772
Nethanol introduction Depard area 2 Gasol Inc (+0.52) Keroespe (+0.49) A. D. D. (+0.47) I. D. D. (+0.46)												!			453
Deand area 3 Gasoline (#0.52) Kerceare (#0.45) A.D.O. (#0.45) I.D.O. (#0.46)		74	110	110	110	110	110	119	252	252	252	656	671	671	671
Total methanol volume		74	110	110	110	110	110	119	252	252	252	656	571	671	1,124
Oil products replaced Gasoline Kerosene	8						578	62		131	131	341	349 0	349	322

(3) DI	stri	bution	cost and	volu	me of	011	proc	lucts	for	meth	anol	intr	oduct	ion	cases	3	UNIT	: 10+3 A	d/year
			Transportation cost	A	A-120	A-N25	A-X26	A-127	A-M28	A 1129	Y-100	A-XG1	A 1632	A-1633	A 104	A HBS	A-106	A-107	A-N
Demand	L.P.G.	Dani	5.60	35.64	35.64	35.64	35.64	35.61	35.64	35.64	35.64	35.64	35.64	35.64	35.64	35.64	35.64	35.64	35.64
alta.	Gasoline		5.60	660.10	650.10	660.10	660.10	660.10	660.10	160.10	1	1	660.10		•	1	660.10	660.10	
	Jet fuel Kerosene	1 ' '	. 32.20 5.60	61.40 781.50	1	61.40 781.50	61.40 781.50	61.40 781.50	61.40 781.50	61.40 781.50		1	61.40 781.50	61.40 781.50	61.40 781.50	ı	61.40 781.50	61.40 781.50	
	A.D.O.	Dani	5.60	1117.50		1117.50	1117.50	1117.50	1117.50	1117.50	1117.50	1	1117.50	1117.50	1117.50	1117.50	1117.50	1117.50	1117.50
ŀ	1.D.O.	Demol	5.60	52.40	52.40	52.40	52,40	52,40	52.40	52.40	52.40	•	52.40	52.40	52.40	52.40	52.40	52.40 152.80	1
Demand	Fuel oil	Plaju	5.60	152.80	152.80 10.80	152.80	152.80	152.80	152.80	152.80 10.80	152.80 10.80	· · · —	152.80	152.80	152.80 10.80	152.80	152.80	10.80	10.80
area 2	Gasoline			419.40	419.40	419.40	419.40	419.40	419.40	419.40	419.40	l	419.40	419.40	419.40	419.40	419.40	419.40	419.40
		Balikpapan	25.90	21.70	21.70	21.70	21.70	21.70	21.70	-21.70		ŀ	21.70	21.70 443.50	21.70 443.50	21.70 443.50	21.70 443.50	21.70 221.73	21.70
	Kerosene A.D.D.	Plaju		\$59.60	443.50 859.60	443.50 859.60	443.50 859.60	+443,50 859,60	443.50 859.60	443.50 859.60	443.50 859.60	ŀ	443.50 859.60	859.60	859.60	859.60	859.60	859.60	859.60
	1.D.O.	Omaal	10.50	124.90	124.90	124.90	124.90	124.90	124.90	124.90	124.90	124.90	124.90	124.90	124.90	124.90	124.90	124.90	
<u> </u>		Plaju	3.20	39.00	39.00	39.00	39.00	39.00	39.00	39.00	39.00		39.00	39.00	39.00	39.00	39.00	39.00	39.00
Remand area	L.P.G.	Plaju Cilacap	7.70	194:39	114.24	139:31	18.78	128:78	191.79	191:39	191:33	197.79	图:强	191:33	191:39	PH:39	194:38	19:33	191.7 <u>9</u>
	Gasotine		7.70	185:81	1331:18	88.3	183:23	1881.23	188.28	1885:翌	1890:18	1	超:第	1221:55	1871:28	183:18	1833.78	1663:18	1 1
	Jet fuel		7.70	204.80	201.80	201.80	201.80	204.80	201.80	204.80	t .	:	204.80	204.80 609.60	204.80	201.80	201.80	201.80	
	Kerosene	Filecsb		a∰:%	2555.60	1915.90	1545:30	1995.70	2031.98	1985.91		\$65.59 \$75.59	1935:91	1945.91	1985:97		256.21 256.21	1331:17	331:17
	A.D.O.	Plaju Cilacap	7.70	2313.70		2313.70	2313.70	2313.70	2227.61	2313.70	227.6	2313.70	2313.70			2227.64	2313.70	2313.70	: I
	1.D.O.	De nai Plaju Cilacap	18.50	826.16 13.11	377.94 540.96	126.21 787.11	126.21 787.41	126.2] 787.41	126.21 787.41	126-21 787-41	57.08 851.53	55.83 856.80	56.82 856.80	56.82 856.80	69.65 852.97	81.84 81.84	60.65 841.84	60.65 841.84	81.84
	Fuel oil	Plaju Cilacap	7.70	1257.88	188.87	1223:15	1223:15	1223:15	1223:14	223:14	1223:14	I	1233:14 1233:14	1223-14	223.36	331.33	2331.33 1250.33	237.37	1 1
Desand	L,P.G.	Cilacap	3.22	12.77	42.71	123.34	123.31	42.77	42.77	12.71	42.77	42.77	42.77	42.77	42.77	42.77	42.77	42.77	42.77
area 4	Gasoline	Dunal cliacar	2 <u>1</u> .00 3.22	33.13	339.59	372:35	391:76 312:81	391:75 412:04	271.76 472.76	3712:76	287:29 316:51	288.06 288.74	218-06 285-74	218:06 485:74	ez:81	703.80	703.80	703.80	703.80
	Jet fuel	Çi laçap Balikpapen	13.22 16.10	21.10	L !	21.10	21.10	21.10	21.10	21.10	21.10	21.10	21.10	21.10	21.10	21.10	21.10	21.10	21.10
		Çiləcəp Balikpapan	3.22 16.10	223. IS 790.62	743.18	177.36	JJ6:36	17.3	207.90 805.90	315.06 638.74	218.56 795.31	l	304.17 709.63	201-17 201-17	384:77	89.03 921.77	196.19 817.61	\$17.97 \$95.83	378.83
	A.D.O.	Ballikpapan Cillacap	16.10	713.78		113.46	891.51 571.33	577.37 274.93	802.30	716.24 86.06	802.30	I	716.24 86.06	716.24	716.24 86.06	802.30	716.24 86.06	716.24 86.06	716.24 86.06
	1,0.0.	Balikpapan Dumat		88.52 134.10	802.30 134.10	688.84	274.93					85.05							1 1
		Balikpapan	21.00 16.10 3.22	409.50		134.10 409.50	134.10 409.50	134.10 409.50	134.10 409.50	134.10 409.50	134.10 409.50	l .	134 i0 409 50	134.10 409.50	134.10 409.50	134.10 409.50	134.10 409.50	134.10 409.50	134.10 409.50
Dessand		Cilacap Cilacap	3.22	79.71	79.71	79.71	79.71	79.71	79.71	79.71	79.71	79.71	79.71	79.71	79.71	79.71	79.71	79.71	79.71
area 5	Gasol Inc	Cillacap Balikpapan	12.60	288.11 1072.69	1882.13	288.11 1072.69	288.11 1072.69	1002:00	1882:1) 1882:14	288:11 1072:60	1882:11	68.1	288.11 1872.16	288 II 1072 69	1872.13	288.11 1072.69	288.11 1072.69	288.11 1072.69	748.84 6(1.96
	Jet fuel	Ballkpapan	12.60	206.60	206.ED	206.60	206.60	206.60	206.60	206.60	206.60	206.60	206.60	206.60	206.60	206.60	206.60	206.60	206.60
		Ballkpapan Ballkpapan	12.60	1753.00 (497.10	I	1753.00 1497.10	1753.00 1497.10	1753.00 1497.10	1753.00 1497.10	1753.00 1497.10		i	1753.00 1497.10	1753.00 1497.10	1753.00) 1497.10	1753.00 1497.10	1753.00. 1497.10	1753.00 1497.10	1753.00 1497.10
	A.D.O.	Balikpapan Cilacap Balikpapan	12.60	294.50	291.50	4.1					1								1
	Fuel oil	Cilacan	12.60	1020.50	916.69 103.81	294.50 242.26	294.50 475.52 511.98	294.50 541.58	294.50 681.44 339.06	294.50 533:44 533:06		1	294.50 613.67 400.83		294.50 623.08 37.12	294.50 605.76	294.50 605.76 414.74	294.50 605.76	294.50 605.76 414.74
Dentendi		Balikpapan Balikpapan	12.60 7.84	15.25	103.81	778.24 15.25	514.98 15.25	541.98 15.25	539.06 15.25	3390.06 15.25	358.82 15.25	 				114.74	414.74 15.25	414.74	
area 6		Ballikpapan	. 7.84	265.23	265.23	265.23		265.23	265.23	265.23			265.23	t .	ı		265.23	265.23	1 1
	Jet fuel	Ballkpapen	7.84	57.10		57.10		57:10	57.10	57.10	1	I	l				57.10	57.10	1 1
		Balikpapan Balikpapas	7.84	260.50 286.50	260.50 286.50	260.50 286.50		250.50 286.50	260.50 286.50	260.50 286.50	E .	l	260.50 286.50	260.50 286.50	260.50 286.50		260.50 286.50	260.50 286.50	
		Balingapas Dalikpapas	7.84 7.84	260.50 15.40	287.30 15.40	15.40	15.40	15.40	15.40	15.40	15.40	1	250.30 15.40	15.40	15.40	15.40	15.40	15.40	l I
	Fuel oil	Balli kpapan	7.84	165.80	165.80	165.80	165.80	165.80	165.80	(65.80	165.80	165.80	165.80	165.80		165.80	165.80	165.80	
Demend area		Balikpapan Balikpapan		169.30 23.60	169.30 23.60	169.30 23.60		169.30 23.60	169.30 23.60	169.30 23.60		ı	169.30 23.60	169.30 23.60	169,30 23.60	169.30 23.60	169.30 23.60	169.30 23.60	169.30 23.60
'		Balikpapan		204.20	204.20	201.20		201.20	201.20	201.20			204.20		204.20		204.20	204.20	201.20
	A.D.O.	Ballikpapan	13.58	207.70	207.70	207.70		207.70	207.70	207.70			207.70	207.70	207.70	207.70	207.70	207.70	207.70
Descard area 8		Balikpapan Balikpapan	35.00 35.00	59.30 24.20	59.30 24.20	59.30 24.20	59.30 24.20	59.30 24.20	59.30 24.20	59.30 24.20	59.30 24.20		59.30 24.20	59.30 24.20	59.30 24.20	59.30 24.20	59.30 24.20	59.30 24.20	59.30 24.20
		ga i i Statesi ga i i Statesi	35.00	35.20	35.20	35.20	35.20	35.20	35.20	35.20	35.20		35.20	35.20	35.20	35.20	35.20	35.20	35.20
		8alikpepan	35.00	86.00	86.00	86.00	86.00	86.00	86.00	86.00	86.00		86.00	86.00	86.00	86.00	86.00	86.00	86.00
Transport	ation cos	st of oil pa	roducts(10*3 \$/year)	155.542	153.754	164.933	156.427	156,427	148,902	148,902	148,443	147.199	147, 199	147.199	145.482	143,987	145,715	142.838	137.033

(4) Results of CASES	A A	A-C-1	A-C-2	NIT: 10+3 & A-C-3
[Precondition]	<u> </u>	n V-1	🗸 🚜	
Domestic demand Frude oil export price thanol production area othanol price	ASCOPE 30,5\$/R8L No introduction	ASCUPE 30.55/88 Sumatra, kalimantan 7	ASCIPE 30,537881 Sumatra, kali muntan ?	ASONE 30,53788L
(RESULT)				
Crude oll export price	1	1	1	
Ethanol price		148\$/64	168\$/11	[93 \$/A 4
Amount of profit (10*3 \$)	18,250	18,352	18,342	18,33
Crude oil production S.C. At juna Attaka Bekanal Handil Ann condensate JUTAL	13 375	1125		
Import of AL	3.33	3:83	3,33	3,33
Crude oil processed				
หลับ	6,979	6,690	6,690	6,69 1.26
ci Dicas	3:17	5,05	5:853	1:24
Arjuna Attaka	6.181 3.636	6.181 3.636	\$:181	6.18 3.63
Import of AL BALIKPAPAN Retarnal			3,030 3,888	
Bekapal Handi I	8:442	3;888 8;442	3;\$\$\$ 8;\$42	\$:\$1 ***
TOTAL	40, 123	39,834	39,834	39,83
Crude oll exports SLC Arlina	33.251 8.520	35.420 6,640	35.420 6.640	35.41 6,64
SLC Ar Juna At Laka Bekanai Junali	8. */V	0.040	0,000	0,09
Handli Azun condensate TUTAL	1.250 -1.555	1.250	1:38	1:3
latural gas exports	23.666	23:888	28:888	23,88
roduction volume Propage	593	648	647	. 64
Propase Sutane Saphtha	3.740	1:05	1.056	1.00
Gasoline Reformate Jet fuel	6.042 621	3,100	2.(82)	9,93 62
Kerosene	7:30	8,708	8.35	3.3
A.D.O. 1.D.O. Fuel_oi1	1:512	1.58	1:50	1.54 5.45
L. S. W. R. Asphalt Sulfur	30ď	303	300	
Cokes TOTAL	377 38.790	2 1 61 38,534	38,536	24 38,54
Kerosene Imports	0	0	. 0	. (
îotal supply	38,790	38,534	38,536	38,54
Dogestic degand Propane	463	463	463	46
Propane Butare Butare Raphtha Gasoline Jet fuel	4 043	0 Nu 2	6,042	. د ما
Jet fuel Kerosene	7.047	7.01	7.047	7.04
A. D. O.	1:338	[138]	7.130	1.53
fuel oll L.S.W.R Asphalt	3,230 300	3,250 300	3.23U 0	3, 23 20
ion.	26,433	26.433	26,433	26,433
Export volume Tropane	130	185	184	18
Butane Naphtha Reformate	3.740	1:537	1:38	4,43
Kerosene A.D.U.	2.425	1.40	2.30	2:26 1:26
Kerosene A.D.O. I.D.O. L.S.W.R.	4; <i>2</i> 92 Q	2.209 Q	2;208 Q	2;20
Asphalt Sulfur Cokes TUTAL		,4 <u>2</u>	318	
TÜTÄL	12,357	12.654	12,380	12,21
Processed volume(each unit) Topping Dumai	, ,	سرو ر		
pusai Plaju Cilacan	6.979 13 518	5,690	6.60	6.69 19.20
Plaju Cilacap Balikpapan TOTAL	12:338 40:123	3.8	[3:33]	32.33
setomer i	. 192	792	792	74
Dusal Cilacap Balikpapan TOTAL	1:00	1,00	1:032	1:2
Plaju	944	3,023 944	944	976 116°C
iydro cracking Dumai				2.88
Balikpepen TUTAL	1:32	2.885 5;314	2.8% 5.314	2,88 5:37
thanel introduction South summitra—Demand area3 Gasoline(*0.70)		395	395	
(alimantan→Demandi area 5 Gasoline(*0.70)		395		
lasa→Besand area 3 Gasoline(#0.70)				•
Gasorine(#U. /U)		ļ <u></u>		160
otal ethanol volume	0	790	395	160

(5) <u>p</u> i	stri r et	bution hanol	cost and introducti	volum on ca	e of c	oil pro	oducts #3 Wywr
[Transportation cost (\$/ki)	A	A-C-1	A C-2	A C-3
Demand	L.P.G.	Dusai	5.60	35.64	35.64	35.64	35.64
area	Gasoline	Dunat	5.60	660.10	660.10	660, 10	660.10
.	Jet fuel	Cilacap	32.20	61.40	61,40	61.40	61.40
	Kerosene		5.60	781.50	781.50	781.50	781.50
	A.D.O. 1.D.O.	Dunazi	5.60	1117.50 52.40	1117.50 52.40	1117.50 52.40	1117.50 52.40
	fuel oil	Dunai Dunai	5.60 5.60	152.80	152.80	152.80	152.80
Demand	L.P.G.	Plaju	3.00	19.80	10.80	10.80	10.80
area 2	Gasoline	Plaju		419.40	419.40	419.40	419.40
	Jet fuel	Ballkpayan	25.90	F	21.70	21.70	21.70
	Kerosene	_		443.50	443.50	443.50	443,50
	λ.D.O.	Plaju	10.50	859.60	859.60	859.60	859,60
	1.D.O. Fuel oil	Dunai Diato	10.50	124.90 39.00	124.90 39.00	124.90 39.00	124.90 39.00
Demand	L.P.G.		7.70	193.78		181:78	101.70
area		Plaju Cilacap		1	191:79		
	Gasoline	Plaju Cilacap	7.70	1552.61	1876:31	451.39 1676.11	1840.61
	Jet foel			204.80	204.80	204.80	204.80
	Kerosene	Plaju Cilacap	7.70	2687.58	609.69 1915.91	1945.91	2031.98
	A.D.O.	Plaju Ci lacap	7.70	2313.70	2313.70	2313.70	2227.64
	1.0.0.	Dumai Plaju Cilacap	18.90 7.70	826.16 13:43	60.65 852.97	59.47 854.16	77.44 856.18
	Fuel oil		7.70				
		Cilacap		1257.88	1223.36	1223:36	1223.36
Demand area 4	L.P.G.	Cilacap	3.22	42.77	42.77	12.77	42.77
1 4	[Gasoline	Duaci Cilacap	21.00 3.22	351:68	703.80	631:18	237.12 466.68
	Jet fuel	Cilacap Balikpapan	18.70	21.10	21.10	21.10	21.10
	Kerosene	Cilacap Balikpapan	3.22 16.10	223.18 790.62	204:77 209:03	783:49°	197.11 816.69
	A.D.O.	Cilacap Balikpapan	3.22 16.10	713.78 88.52	716.24 86.06	716.24 85.06	802.30
	1.D.O.	Dumai Balikpapan	21.00 16.10	134.10	134.10	134.10	134.10
	Fuel of 1	Cllacap	3.22	409.50	409.50	409.50	409.50
Demand	L.P.G.	Cilacap		79.71	79.71	79.71	79.71
area 5	Gasol ine	Cilacap Balikpapan	12.60	1882:23	205:89	1872:4	1882:23
	Jet fuel	Balikpapan	12.60	206.60	206.60	206.60	206.60
		Balik papan	12.60	1753.00	1753.00	1753.00	1753.00
	A.D.D.	Ballkpapan	12.60	1497.10	1497.10	1497-10	1497.10
	1.D.O.	Ci lacap Balikpapan	12.60	294.50	291.50	294.50	294.50
	Fuel oil	Cilacap Balikpepan	12.60	1020.50	623.08 397.42	622.02 398.48	620.22 400.28
Demand	L.P.G.	Balikpapan	7.84	15.25	15.25	15.25	15.25
area 6		Balikpapan	7.84	265.23		265.23	265.23
	Jet fuel		7.84 7.84	57.10 260.50	57.10 260.50	57.10 260.50	57.10 260.50
1	A.D.O.	Balikpapan Balikpapan		286.50	286.50		286.50
	1.0.0.	Balikpapan		15.40	15.40	15.40	15.40
	1	Balikpapan	7.84	165.80	165.80	165.80	165.80
Demand	Gasoline	Balikpapan	13.58	169.30	169.30	169.30	169.30
area	1	Balikpapan	13.58	23.60	23.60	23.60	23.60
		Balikpapan	13.58	204.20	201.20 207.70	204.20 207.70	204.20
Demand	A.D.O.	Balikpapan Balikpapan	13.58 35.00	207.70 59.30	59.30	59.30	207.70 59.30
area		Balikpapan	35.00	24.20	24.20	24.20	24.20
		Balikpapan	35.00	35.20	35.20	35.20	35.20
	A.D.O.	Balikpapan	35.00	86.00	86.00	86.00	86.00
Transport	lation co	st of oil p	roducts(10#3 \$/year)	155,542	140,503	144,628	147,511

