# FEASIBILITY STUDY FOR THE PLANT RENOVATION OF BASUKI RACHMAT PULP AND PAPER MILL IN THE REPUBLIC OF INDONESIA (APPENDIX)

FEBRUARY, 1985

JAPAN INTERNATIONAL COOPERATION AGENCY





国際協力事業団 A '85. 8.22 108 69.5 全録No. 11855 MP1

# CONTENTS

1.	INTRO	DUCTION	. 1
2.	SUMM	ARY	. 1
	2- 1	History and Objectives of the Investigation	. 1
	2- 2	Outline of Basuki Rachmat Pulp and Paper Mill	.3
	2-3	Raw Material Availability	. 5
;	2- 4	Rate of Domestic Paper Supply in Indonesia and BRPP's Selection	.5
	2- 6	Production Scale of No. 2 Paper Machine Plant	.7
		Marketability Study	
•	2-8	Setting the Sales Price	. 8
_	2- 9	Total Investment	8
	2-10	Total Investment.	9
	2-11	Turnover Rotio of Invested Funds	9
3.	No. 21	PAPER MACHINE EXPANSION PLAN	.11
		Policy and Summary	
		Basic Conditions for the Plant	
		Paper Types and Production	
		Operation Conditions	
		Efficiencies	
		Paper Machine Specifications	
		Utilities JGN LIBRARY	
4	14140		
•-	4- 1		
	s_ 2	Machine Approach System	
		No. 2 Paper Machine (PM2)	
		Finishing Plant	
		Steam Source	
		Electric Power	
		Water Source	
		Plant Layout	
	4_9	Plant Construction Cost	
	• •	Construction Schedule and Duration	
		Technical Cooperation	
۲	OPER	RATION OF THE EXPANDED PLANT	39
.,,		Number of Operating Days	
	5.2	Number of Personnel	39
	<u> </u>	Production and Production Plan	39
6.		NCIAL EVALUATION	
0.	6- 1	Basic Polity of Financial Evaluation	
		Production and Sales Plan	
	6-2	Production Cost	
		Variable Cost	

	Fixed Cost					
6- 6	Depreciation					4
6- 7	Total Fund Requirement					4
6 8	Funds Procurement					4
6- 9	Interest and Repayment Method of Long-Term Loans		·	 		4
6-10	Corporation Tax					4
6-11	Profit and Loss Statement by Years (New Plant Only)					4
6-12	Annual Profit and Loss Statement for BRPP			,,,,,,,,,,		4
PROF	TABILITY AND ECONOMIC EFFECTS OF THE E	XPA	NSION			7
7- 1	Break-Even Point by Grades					7
7- 2	Calculation of Incoming and Outgoing Funds	• • • • • • •				
7- 3	Profit Ratio and Loan Repayment Ability				,	
7_ 4	Calculation of Internal Rate of Return					
7 5	Financial Indices				·	
CON	CLUSIONS AND RECOMMENDATIONS					

**%**.\*

# CHAPTER 1 INTRODUCTION

CHAPTER 2 SUMMARY

#### 1. INTRODUCTION

- 1-1 As described in Chapter 2, Summary, this report is presented as an Appendix to the Feasibility study Report (hereinafter called F/S Main Report) submitted to the Directorate General of Basic Chemical Industries, Department of Industry of the Republic of Indonesia (hereinafter called DGBCI) by the Japan International Cooperation Agency (hereinafter called JICA) with regard to the renovation plan for Basuki Rachmat Pulp and Paper Mill (hereinafter called BRPP).
- 1-2 This report describes the results of the investigation on the installation of No. 2 Paper Machine of BRPP.
- 1-3 The paper produced by No. 2 Paper Machine shall be for use in Insonesia as well as for export to other countries. Therefore, the selected equipment must be capable of maintaining high quality standards and must also be equipped with an effluent treatment system for environmental protection.
- 1-4 This report shall be presented to DGBCI by JICA.

#### 2. SUMMARY

- 2-1 History and Objectives of the Investigation
- 2-1-1 The Government of the Republic of Indonesia made a request to the Government of Japan for technical cooperation, relative to the renovation plan for pulp and paper plants in Indonesia.

The preliminary survey team sent by the JICA to Indonesia during period, December 21 to 28, 1983 investigated the preconditions for a full-scale feasibility study and clarified the scope of technical cooperation.

DGBCI and JICA agreed with the following Scope of the Study (hereinaster called S/S) with regard to the seasibility study, on December 26, 1983 to Jakarta.

#### 2-1-2 Scope of Study

1) Objective of the study

The objective of the study is to diagnose BRPP and PPM and to investigate the possibility of thire Renovation from technical, financial and economic points of view and to formulate the renovation programs in order to contribute to increasing production efficiency and improving products quality.

- 2) Scope of the study
  - In order to achieve the above objective, the study will cover the following items:
- (1) Present situation of and national policy on Pulp and Paper Industry in Indonesia.
- (2) Examination of management of the Mill.
  - (2)-1 operation and quality control
  - (2)-2 maintenance of machinery and equipment

- (2)-3 cost control
- (2)-4 administration
- (2)-5 education and training
- (3) Thehnical examination of machinery and equipment of the existing Mill.
  - (3)-1 pulp
  - (3)-2 stock preparation of the state of the
  - (3)-3 paper machine
  - (3)-4 finishing
- chemical recovery
  - (3)-6 utility
  - (4) Survey of raw material
- (5) Survey of domestic market requirement
  - (6) Formulation of Renovation program

The Renovation program for the existing Mill and its management will be formulated, taking into account the improvement of environmental effects.

The second of th

[韓] 医克尔勒氏 (4) 多级,多

- (6)-1 renovation plan
- (6)-2 requirement for education and training and capital investment
- (6)-3 implementing schedule
- (7) Financial analysis
- (8) Economic evaluation
- (9) Conclusion and recommendations
- 2-1-3 In its report, the JICA Preliminary Survey Team primarily focused on the installation of No.
  2 Paper Machine (hereinafter called PM2) in BRPP as an objective of renovation plan, for further investigation, in a full-scale feasibility study. The investigation team covered the following points with regard to PM2:
  - 1) Availability of raw materials
  - 2) Selection of types of paper, production capacity and marketability.
  - 3) The economic feasibility of the PM2 plan
  - 4) Effectiveness in an existing plant
  - 5) Effects on the profitability of the entire mill operation
- 2-1-4 This study group investigated the situation (as outlined in the S/S) during the period, from February 26 to March 27, 1984, and upon returning to Japan reviewed the results, and prepared an F/S. The F/S Main Report was officially submitted to DBGCl by JICA in October, 1984. This investigation team also prepared an F/S Appendix on PM2 (Expansion Plant) submitted herewith the F/S Main Report.

# 2-2 Outline of Basuki Rachmat Pulp and Paper Mill

2-2-1 History

Basuki Rachmat Mill (BRPP) started operation in 1969 to produce printing/writing paper out of bamboo pulp. BRPP is a vertically organized plant for pulp and paper, equipped with facilities for bamboo preparation and cooking and chemical recovery. The initially designed capacity was 30 tons/day.

The availability of bamboo, the primary raw material, has since become limited, forcing the mill to change from bamboo to pine and other hard woods, the current percentage of bamboo used is only about 10%, with the possibility of discontituring its use completely in the near future.

In 1976, the paper machine was renovated for faster operation from 200 to 300 m/min, resulting in an increase in daily production (designed capacity) from 30 tons to 45 tons. However, due to the unstable pulp quality and aging equipment, the average daily production in 1983 was only about 34 tons.

This plant was built from the reparations paid by Japan after the war. Hence, form its inception, it has been closely related with Japan and receives aid both from the Japanese government and from private sources.

# 2-2-2 Location Banyuwangi City, Eastern Java

## 2-2-3 Major Equipment

1) Pulp plant

Daily production capacity

: 30 ADVd

Chipper

: 4 units

Digester

: 2 units of 50 m3 vertical type

Washing and Screen

: 1 line of 3(4)-stage drums

Bleaching plant

: 1 line of 5-stage (C-E-H-E-H) bleaching facilities.

2) Papermaking and Finishing

Daily production capacity

: 45 ADt/d of a printing/writing paper as design (34 ADt/d as

actual in 1983)

Paper machine

: 2850 mm of Wire cloth width, 45~200 g/m2 of Basis weight,

60~250 m/min of Speed

Finishing equipment

: I double cutter, I winder

3) Chemical Recovery Plant

Evaporator

: 1 line of 5 body-5 effects

Recovery boiler

: 1 set

Causticizing equipment

: 1 set

4) Auxiliary Facilities

Electrolysis equipment

: 1 set (1,200 KW)

Power boiler

: 1 unit (10 t/h)

Diesel generator

: Sunits (1,500KW  $\times$  3, 2,710KW  $\times$  2)

2-2-4 Mill Site Area

: 50 ha

2-2-5 Number of Employees : 735 (as of 1984)

#### 2-2-6 Status of Mill

#### 1) Major investment made in past

1962 Toyo Menka Kaisha Ltd. concluded the plant construction contract with the Government of the Republic of Indonesia based on the Japanese reparation. (Construction cost: US\$8,500,000)

1962 Honshu Paper Co., Ltd. concluded a consulting contract with Toyo Menka Kaisha Ltd.

1976 Renovation of the paper machine for faster operation (833,000,000 Rp)

New installation of electrolysis equipment and diesel generators

Total cost: 2,302,000,000 Rp (US\$1.00=425 Rp)

#### 2) Production Trends

 $KR_{D} = 1,000R_{D}$ 

Item	Year	1980	1981	1982	1983
Production	t/y	12,873	, 12,702	12,595	11,787
Profit/loss	KR <sub>0</sub> 'y	721,160	53,105	-502,642	-1,573,936

The production rate has remained relatively constant in the past four years. Unless the equipment is updated, there will be no significant change in the production level in the future.

The mill operation showed large deficits in 1982, and 1983. The following are the reasons:

- (1) Severe competition from the larger and more modern private mills.
  - Delay in modernizing existing equipment and in implementing the necessary energy conservation measures.
- (2) Reduction of the sales price forced by a decline in product quality
- (3) Increase in costs resulting from the mills unfavorable location
- (4) High raw material cost resulting from the use of higher-cost wood chips in stead of low-cost bamboo
- (5) Decrease in general efficiency and increase in the maintenance cost of aging equipment. In the impact of these factors on BRPP was further aggravated by the overall economic depression and oil price increases.

It is evident that unless steps and taken in the near future to improve this situation, the BRPP will be irreversibly damaged within several years.

The F/S Main Report submitted by JICA in October, 1984 analyzed these problems and proposed measures to improve BRPP's profitability.

#### 2-3 Raw Material Availability

#### 2-3-1 Raw Material Procurement

1) BRPP has a pulp production plant. However, as described in the F/S Main Report on the existing plant, increase in pulp production over the current level (as of 1983) is difficult. The following are the major reasons:

(1) The collection areas for wood are moving out farther each year. -thereby-increasing trans-

portation cost.

(2) The control exercised by the Forestry Agency of the Indonesian government on the quantity and areas for logging wood limits BRPP's production plans.

(3) As of 1983, the quantity of wood that may be cut has reached the limit, and there are no

foreseeable increases in wood supply.

(4) To increase pulp production, the pulp plant, itself, including the chemical recovery system, must be improved.

This requires a substantial investment which cannot be immediately offset by adequate production.

- 2-3-2 We therefore recommed in the report that the average daily production be set at about 29 ADI and that any shortages in material be supplemented by purchase.
- 2-3-3 Under the cirumstances, our plan proposes purchasing all the pulp needed by the PM2 plant (expansion).

The prices of pulp to be purchased is as follows:

NBKP: US\$450BD1 LBKP: US\$410BD1

In the pulp prices indicated in the F/S Main Report are based on actual purchase prices:

Purchasing NBKP: US\$405.5/BDt Purchasing LBKP: US\$355.5/BDt

- 2-4 Rate of Domestic Paper Supply in Indonesia and BRPP's Selection
- 2-4-1 The paper supply and demand profile in Indonesia for 1983 is shown below:

Unit: 1,000 t

Paper	News print	Printing writings	Other types	Total
Consumption	120	193	351	664
Production	-	190	201	391
Export	_	7	3	10
Import	120	10	153	283
Self sufficiency	0%	98%	57%	59%

Source: Trade magazine "Paper", November 1984

2-4-2 The rate of domestic paper supply of printing/writing paper in Indonesia as of 1983 is high at 98%.

Currently, the 120,000 Vy of newsprint paper is all imported, however the newspaper machines, with a total capacity of 156,000 Vy (90,000 Vy by PT KERTAS LECES and 66,000 Vy by PT ASPEX), will start production in 1985.

The domestic supply meets 50 to 60% of the demand for industrial paper such as liner board paper, corrugated medium and sack paper. Once the planned project is implemented, the domestic supply of industrial paper will be able to meet a substantially larger percentage of the demand in the very near future.

- 2-4-3 The Republic of Indonesia's primary focus should be on increasing the rate of domestic paper supply of thin paper.
- 2-4-4 Printing/writing paper, liner board paper and corrugated paper, all of which are massproduction items, are not suitable new products for BRPP for the following reasons:
  - (1) The availability of the raw material, wood is very limited.
  - (2) Since BRPP is located far from the main market, the transportation cost is high, making BRPP costs less competitive.
  - (3) The large amount of water necessary for the operation is not available.
  - (4) Since the enterprises in the surrounding area are relatively undeveloped, evrything necessary for BRPP's operation must be self-generated and supported.
- 2-4-5 Thin paper is, therefore, the most suitable product for BRPP, since it can be produced on a smaller scale with higher yield on investment.
- 2-4-6 The demand for thin paper in 1983 and the forecast for 1989 are shown below. The details are given in Table 3-3-1, F/S (Main Report).

	·	1983	1989	
(1)	Manifold	7,500t/y	10,500Uy	
(2)	N.C.R	2,400t/y	3,400 <i>0</i> y	
03)	Base paper for Lamination	2,000 <i>u</i> 'y	3,800t/y	
(4)	Carbon base paper	2,000 <i>0</i> y	2,300t/y	
<b>(5)</b>	Glassine paper	1,700t/y	1,700 <i>0</i> y	
(6)	<b>Soap wrapper</b>	1,500t/y	2,1000y	
(7)	Grease proof paper	1,200 <i>0</i> y	1,300 <i>0</i> y	
	Total	18,300t/y	25,100t/y	_

- 2-5 Production Scale of No. 2 Paper Machine Plant
- 2-5-1 In 2-3 and 2-4, It was emphasized that due to the difficulty in procuring the raw material, wood, BRPP should use purchased pulp for the entire production, Furthermore the production of a variety of thin paper, each in small lots, would be more suitable for BRPP, instead of a mass production item.
- 2-5-2 Indonesia has already started projection of three types of thin paper: manifold, N.C.R. and

carbon base paper. The demand in 1983 for thin paper, excluding these three was 6,400 Vy, the projected demand in 1989 is only 8,900 Vy.

- 2-5-3 BRPP already has a license to produce 6,000 Uy of thin paper from the Indonesian Government. BRPP is also planning for the PM2 plant expansion in 1989.
- 2-5-4 Since the consumption of thin paper in Indonesia is low and a large growth in consumption rate is not anticipated, the PM2 production rate was set at 6,020 ADI/y. BRPP has already obtained approval to construct a plant with a capacity of 6,000 ADI/y from the government.
- 2-5-5 The total BRPP production is 21,740 ADt/y, (6,020 ADt/y for PM2, Item 2-6-2 and 15,720 ADt/y for PM1-see Item 2-6-4).
- 2-6 Selection of Products for No. 2 Paper Machine
- 2-6-1 The PM2 plant should produce types of paper that are not being produced in Indonesia or imported, (e.g. base paper for lamination, glassine paper, soap wrapper and grease-proof paper).
- 2-6-2 Therefore, we planned the items for PM2 production as follows:

(1) Base paper for Lamination	1,700AD <i>u</i> 'y
(2) Soap wrapper	1,800ADt/y
(3) Glassine	1,440ADt/y
(4) Grease proof paper	1,080ADt/y
Total	6,020ADvy

- 2-6-3 Among the types shown in the above table, the production of base paper for lamination and greaseproof paper, totaling 2,780 ADUy, is converted from PM1 to PM2.
- 2-6-4 The consumption of from paper (computer paper) in 1989 is expected to be 12,900 ADt/y.

  After implementing the renovation plan, the existing PM1 can increase its production to 14,245 ADt/y.

If the PMI is then used only for the production of printing/writing paper and form paper, it can increase its production to 15,720 ADUy.

#### Changes PM1 production

<u>.</u>	After ren	ovation	1989			
Grade	d/y×ADt/d	ADt/y	d/y×ADt/d	ADt/y		
Printing/writing	263	11,770	263	11,770		
Oil proof	25 × 16	400				
Base paper for	25 × 25	625	-	-		
lamination Form paper	29 × 50	1,450	79 × 50	3,950		
Total	342 d/y	14,245	342 d/y	15,720		

The profits on form paper (see table 13-4-2, F/S Main Report) is greater than that for other thin paper. Therefore, by constructing the PM2 plant and by changing the PM1 production line, the profits on the PM1 plant can be increased.

#### 2-7 Marketability Study

2-7-1 Since there is no official data on current demand or projected demand for thin paper in Indonesia.

The JICA team based its estimates on discussions with importers/exporters and local paper dealers in Indonesia. The results are shown in Table 3-3-1, F/S (Main Report).

2-7-2 The production plan for PM2 plant is shown in Table 3-3-1.

This production level satisfies more than 85% of the demand in Indonesia.

The production is scheduled to reach 100% of capacity three years from the start of operation.

However, it must be noted that the sale of thin paper is not easy and BRPP will have to take a more aggressive posture in the domestic market as well as promoting exports to other ASEAN countries. Presantly, the other ASEAN countries do not have a paper mill that can produce this type of paper. Therefore, if BRPP can successfully produce thin paper that is competitive in quality with the imported thin paper, BRPP should be able to find a significant market in the ASEAN countries.

2-7-3 Since, there are no construction plans for any other thin paper mill in the area, the construction of No. 2 Paper Machine is a valid program.

#### 2-8 Setting the Sales Price

PM2 is designed exclusively for the production of thin paper and the sales prices are set as follows:

Base paper for Laminati	ion	1,500 RP/kg
Soap Wrapper	(White)	1,600 RP/kg
,	(Colored)	1,680 RP/kg
Glassine	(White)	1,700 RP/kg
	(Colored)	1,780 RP/kg
Grease Proof paper		1,500 RP/kg

These sales prices were based on an evaluation of 1983 domestic prices in Indonesia.

#### 2-9 Total Annual Sales of No. 2 Paper Machine

2-9-1 The annual sales calculation for PM2 is based on the plan described in 2-6-2 and 2-8. The production of soap wrapper and glassine, white and colored, is set at 50% for each. PM2 is to produce thin paper at a rate of 6,020 ADUy. The total sales amount is 9,627.6 million Rp, which makes the average sales price 1,600 Rp/kg.

The details of sales amount are as follows:

(1) Base paper for Lamination

1,700 ADt/y x 1,500 RP/kg=2,550 M.RP

(2) Soap wrapper

White

: 900 ADt/y x 1,600 RP/kg=1,440 M.RP

Colored

: 900 ADt/y x 1,680 RP/kg=1,512 M.RP

(3) Glassine

White

: 720 ADI/y x 1,700 RP/kg=1,224 M.RP

Colored

: 720 ADVy x 1,780 RP/kg=1,281.6M. RP

Colore

: 1,080 ADt/y x 1,500 RP/kg=1,620 M.RP

(4) Grease proof
Total

6,020 ADVy

9,627.6M RP

# 2-10 Total Investment

- (1) Table 4-9-1 shows the total capital investment required.
- (2) The total investment is US\$26,802.873.

## 2-11 Turnover Ratio of Invested Funds

The turnover raio of invested fund is once in about 2.8 years.

CHAPTER 3 NO.2 PAPER MACHINE EXPANSION PLAN

# 3. No. 2 PAPER MACHINE EXPANSION PLAN

## 3-1 Policy and Summary

1) The purpose of an enterprise is cotinuity and growth, while, it pursues the dual objectives of making a profit and fulfilling its social responsibilities.
Particularly with BRPP, however, the emphasis is on its social responsibilities since it was originally constructed by the Indonesian Government in Banyuwangi City which was not an ideal location for the plant.

The expansion plan of PM2 has been formulated in order to be consistent with this principle.

- 2) In view of BRPP's unfavorable location, the PM2 expansion plan is designed to produce thin paper which is a small scale operation but a potentially profitable one.

  PM2 is to focus on the production of four types of base paper for lamination, soap wrapper, glassine and grease-proof paper. Any PM1 products that overlap with the production of PM2 are to be shifted to PM2. In its stead PM1 will increase the production days for form paper. The production of form paper by PM2 at the start of the operation is to be increased to 3,950 t/y from 1,450 t/y, (the forecast for demand in 1990 is 12,900 t/y which suggests that this quantity can be sold).
- 3) All the pulp necessary for the paper production is to be purchased since the availability of the raw material, wood, is tenuous.
  The production of thin paper is set at 6,020 ADUy, and the number of operating days at 315 days per year.
- 4) By installing PM2, BRPP will have two paper machines.

  This will allow BRPP more flexibility in the management of its operation in the unstable Indonesian paper market. Simultaneously, it can provide for the stabilization of employment and the stand and of living in the surrounding area of Banyuwangi City.

  It must also be noted that Indonesia is now importing the entire quantity of thin it needs. By producing it domestically, PM2 can save the foreign currency, as well as pursue Indonesia's national policy of becoming self-sufficient in the production of most types of paper.

#### 3-2 Basic Conditions for the Plant

- 1) All of pulp needed by the plant is to be purchased. The plant is to be equipped with stock preparation, paper machine and finishing equipment. Superior optimum equipment shall be selected for the production of thin paper to assure high quality and high efficiency in the plant operation.
- 2) For environmental protection the plant is to be equipped with an overall effluent treatment system (including the effluent from PM1).

# 3-3 Paper Types and Production

1) Paper types and daily production schedule.

Base paper for Lamination : 20 ADUD
Soap wrapper : 20 ADUD
Glassine : 18 ADUD
Grease proof paper : 18 ADUD
2) Annual production : 6,020 ADU

: 315 days

3) Number of operating days a year

\* Détails are shown in Table 3-3-1.

#### 3-4 Operation Conditions

1)	Furnish combination		NBKP	ī	LBKI
	Base paper for Lamination		30	:	70
	Soap wrapper	 ٠.	35	ŧ.	65
	Glassine	•	70	:	30
	Grease proof paper		70	::	30

2) Freeness at Head box (0.3 gr mothed) : 500~600 cc 3) Consistency at Head box : 0.3~0.5 %

4) Chemical consumption

\* Details are shown in Tables 3-3-2 and 3-3-3.

#### 3-5 Efficiencies

I)	Yield	Fiber	: 90.0%
		Filler	: 60.0%
2)	Total efficience	ry .	: 83, 85%
1	a) Opera	tion efficiency	98.0%
	b) Sheet	making efficiency	96.5%
	c) Finishi	ing yield	80, 90%

<sup>\*</sup> Details are shown in Tables 3-3-1 and 3-3-3.

#### 3-6 Paper Machine Specifications

1) Type of machine : Fourdrinier type paper machine

2) Machine speed

Design speed : 120~300 m/min
Operation speed : 166~239 m/min
3) Basis weight : 25~80 g/m<sup>2</sup>
4) Moisture at finished paper : 5~7 %

5) Trimmed width

Wire coth width : 2,880 mm
Width after super-calender : 2,330 mm
Width after cutter : 2,250 mm

6) Drive for Paper machine : Sectional drive by thyristor system

<sup>\*</sup> Details are shown in Tables 3-3-1 and 3-3-4.

# 3-7 Utilities

The utility consumption is set as follows:

Table 3-3-5 Utility Consumption

Paper	Steam t/t paper	Electric kWh/t paper	Water m³/t paper
Base paper for Lamination	3.5	1,800	280
Soap wrapper	3.5	2,000	280
Glassine	5.0	2,000	280
Gréase proof	4.0	1,800	280

Table 3-3-1 Production Plan for No. 2 Paper Machine

Grade	Basis	Prod	luction		Machine speed	Triuming after S/C	Theoretical production		Effic	iency		Size press	Super calend.
	weight	Amount	Daily	Operation	speed	arter 370	production	Op. eff.	Sheet. making	F. yield	Total	press	Carenor
	g/m²	ADt/y	ADt/d	Days	æ/min	D) 50	ADt/24 hr	Z.	Z	%	3		
Base paper for lamination	36.1	1,700	20.0	85	199.0	2,330.0	24.1	98.0	96.5	88.0	83.0		o
Soap wrapper (colored)	30.0	1,800	20.0	45 45	239.4	2,330.0	24.1	98.0	96.5	88.0	83.0		O
Glassin (colored)	28.5	1,440	18.0 18.0	40 40	226.8 226.8	2,330.0 2,330.0	21.69	98.0	96.5	88.0	83.0		ó
Grease proof	38.0	1,080	18.0	60	166.0	2,330.0	21.17	98.0	96.5	90.0	85.0		o
			Av.		·								_
Total	-	6,020	Av. 19.11	315	-	_	_	_		_	_	:	

Note: Operating eff. = (1440 min - T<sub>1</sub> min)/1440 T<sub>1</sub>: Stoppage due to unexpected maintenance breakdown

Sheet making eff = (1440 min - T2 min)/1440 T2: Stoppage due to unexpected product section breakdown

Finishing yield = Finished production for sold/actual net production on reel

Table 3-3-2 Furnish Combination and Chemical

Grade		nish nation		Filler				Chemical	` <b>k</b>	-	Dye stuff	Final 1	Éréeness
	NBKP	LBKP	Kaolin A	Kaolin B	Talc	Pitch control	Size pine	Sheet strength agent	Alua	Drainage accelerative	•	Freeness	Cons.
	7,	7,	kg/t.paper	kg/t.paper	kg/t.paper	kg/t.paper	kg/t.paper	kg/t.paper	kg/t.paper	kg/t.paper	kg/t. paper	csf	7,
				•		100% solid	30% solid	10% solid	8% Al <sub>2</sub> O <sub>3</sub>		(powder)		
Base paper for lamination	30	70	<b>-</b>	<u>-</u>	180	0.6	10.0	3.0	17. <b>0</b>	_		530/0.3 g	0.3 ∿ 0.5
Soáp Wrapper	35	65	:	-	50	0.6	12.0	3.0	17.0	-	4.0 kg/ADt paper as dye stuff	600/0.3 g	0.3 ∿ 0.5
Glassin	70	30	_	<del>-</del>	· <u>-</u> -	1.5		-	7.5	~		500/0.3 g	0.3 ~ 0.5
Colored glassine	:												
White milk	70	30	6.0	17.0	_	0.5	7.5	_	7.5	7.5			
Red	70	30	_	-	-	0.8	40.0	-	7.5	10.0	Scarlet 14.4 kg		
Yellow	70	30	_	<del>-</del>	-	0.8	40.0		7.5	10.0	Yellow 11.7 kg		
Orange	70	30		_		ò.8	40.0	-	7.5	10.0	Blue 10 k, violet 6.7 kg		
Chocolate	70	30	-	-		0.8	40.0	_	7.5	10.0	Scarlet 2.8 k, yellow 3.3 kg		
					·						Brown 22.2 k, violet 4.5 kg		
											Black 14.5 k		
Grease proof	70	30	-	<del>-</del>	10	1.5		_	7.5	-	Oil resisting 20 kg	500/0.3 g	0.3 ∿ 0.5

Table 3-3-3 Required Pulp and Chemical per 1 ADt Paper Products

Danawin	. Lan	Base paper	Soap		Gla	issine		Grease
Descrip	ot ron	for laminate	wrapper	Regular	Red	Yellow	White milk	proof
1. Production		-						
Amount	ADt/y	1,700.0	1,800	720		720		1,080
Daily	ADt/y	20.0	20	18.0	_	18.0		18.0
Operation	d/y	85	45 + 45	40.0		40.0		60.0
Hoisture of paper	2	6 ∿ 7.0	6 ∿ 7.0	5 ზ 6.0		5 ∿ 6.0		5 ~ 6.0
2. Finished paper	per ADt. paper							
NВКР	BDkg/ADt. paper	247 / 30	320.0/ 35	665.0/ 70	665.0/ 70	665.0/ 70	655.0/ 70	660.0/ 70
LBKP	BDkg/ADt. paper	585 / 70	590.0/ 65	285.0/ 30	285.0/ 30	285.0/ 30	281.0/ 30	284.0/ 30
Filler	BDkg/ADt. paper	108	30.0	0	0	0	14.0	6.0
Total	-	940.0/100%	940.0/1002	950.0/100%	950.0/100%	950.0/100%	950.0/100%	950.0/100%
3. Yield								
Fiber	Z	90.0	90.0	90.0	90.0	90.0	90.0	90.0
Filler	<b>%</b> .	69.0.	60.0	_	-	-	60.0	60.0
4. Required pulp								
NBKP	BDkg/ADt. paper	274.4	355.6	738.9	738.9	738.9	727.8	733.3
LBKP	BDkg/ADt. paper	650.0	655.6	316.7	316.7	316.7	312.2	315.6
Total	:	924.4	1,011.2	1,055.6	1,055.6	1,055.6	1,040.0	1,048.9
5. Required filler								
Kaolin	kg/ADt. paper	0	0	0	0	0	23.0	0
Talc	kg/ADt. paper	180.0	50.0	0	0	0	0	10.0
Total		180.0	50.0	Ó	0	0	23.0	10.0
6. Required chemical	kg-Liq/ADt. paper							
Pitch control agent	as 100% solid	0.6	0.6	1.5	0.8	0.8	0.5	1.5
Size pinė	as: 30% solid	10.0	12.0	0	40.0	40.0	7.5	0
Sheet strength agent	as 10% solid	3.0	3.0	0	0	0	0	0
Alva	as 8% Al <sub>2</sub> O <sub>3</sub>	17.0	17.0	7.5	7.5	7.5	7.5	7.5
Drainage accelerative	as 30% solid	0	0	0	10.0	10.0	7.5	0
Dye stuff	powder	None	Yes	None	Yes	Yes	Yes	Kone
Oil resisting agent	as 15% solid	0	0	0	0	0	0	20.0

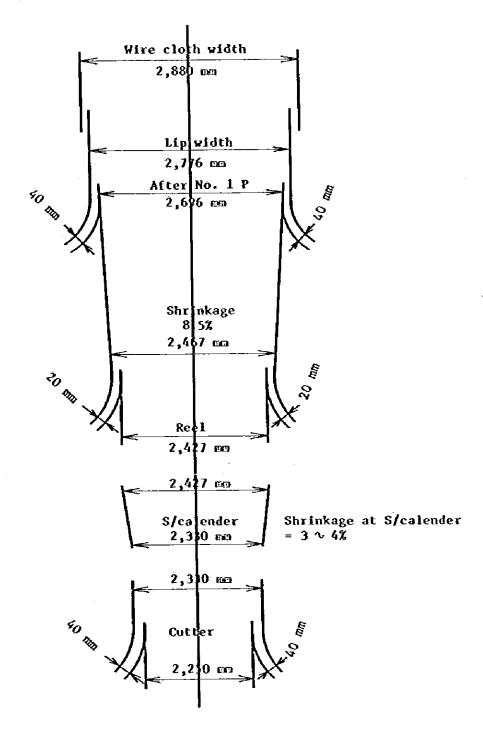
Table 3-3-4 Arrangement of Trimmed Width

1. Sheet dimension

: 750 mm × 1,000 mm

Sheet length after cutter:  $750 \text{ mm} \times 3 = 2,250 \text{ mm}$ 

Trimmed width 3.



# CHAPTER 4 MAJOR EQUIPMENT COMPONENTS

# 4. MAJOR EQUIPMENT COMPONENTS

#### 4-1 Stock Preparation

1) The stock preparation section shall have the necessary equipment for processing, including a pulper, cleaners, refiners and chemical plant.

Also, this section must have with a set of dry broke pulp line equipment as a separate line.

- 2) The pulper shall be of a batch type capable of delibering a pulp mixture, consisting of NBKP and LBKP.
- 3) Since greasy pulp of 500-600 CC (0.3 gr method) is required for the freeness final quality, in the combination of Double Disc Refiners and Deluxe Finer shall be used. The pulp shall be circulated in the refiners for 'batch type' refining.
- 4) The 5-stage mixer shall be capable of producing colored tissue of various types.
- 5) The dry broke pulp shall be prepared through a separate line and mixed with virgin pulp in the last stage of stock preparation.
- All necessary instruments and testers for production and quality control shall be installed.
- 7) Fig. 4-1-1 shows the flow chart.

#### 4-2 Machine Approach System

- The screening equipment and white water recovery equipment necessary for the final screening process shall be installed.
- 2) The fan pump shall be a DC motor drive type, with the lowest pulsation to stabilize the flow rate.
- 3) In order to stabilize the pulp consistency, the pulp and dilution water situated before the fan pump shall each have an independent head box, with a gauge to control and maintain constancy in the water level in the head box.

# 4-3 No. 2 Paper Machine (PM2)

1) Although PM2 is designed for the exclusive production of thin paper, it is also capable of producing extremely thin printing paper. It is also to be equipped with a size press to reduce chemical cost.

The paper machine model used shall be the multi-cylinder type Fourdrinier.

 In order to obtain uniformity in the products and stabilize paper quality, a B/M control system is to be installed. 3) The major specifications are show in 3-6. Other specifications are as shown below.

a) Head box at wire part

: Enclosed air cushion type

b) Press part

: Combination press type with suction pick up roll

c) Dryer part

: Multi cylinders type

d) Size press

: Inclined type

e) Recl

: Horizontal double arm surface type

f) Dryer Hood

: Open hood type

#### 4-4 Finishing Plant

1) Two sheet cutters and one super calender shall be prepared. Renovation of the winder is included in the renovation project for PM1. Since this rewinder operates at a low rate of 15 to 20%, far below its capacity, a winder, exclusively for PM2 shall not be necessary.

#### 4-5 Steam Source

- 1) The volume of steam needed for this project is approximately 4.0 t/h for the normal production of glassine, and approximately 5.0 t/h at the very maximum. Since the existing boiler has no space for supplying PM2 with steam, one new boiler shall be installed. The capacity of this new boiler is to be 10 t/h x 16 kg/cm/G to be available during an emergency for use in cooking in the digesters:
- 2) Installing a new boiler will bring the total steam generation capacity to 624 U24 hr.

Existing boiler:

(6 t/h R/B + 10 t/h O/B) x24=384 t/24 hr

New boiler:

10 t/h O/B x 24

 $=240 \, t/24 \, hr$ 

Total

624 U24 hs

The maximum volume of steam needed by No. 1 Paper Machine including the pulp plant is 338.5 Vh and the steam volume needed by No. 2 Paper Machine is 90 Vh, for making a total of 428.5 Vd. Assuming the need is 25% more at peak time, the total necessary volume is 535.6 V d.

There is an allowance of about 17% in the steam generation capacity.

In the event of a break down in one of the three boilers, the generated steam volume is min. 16  $t/h \times 24$  hr = 384 t/d. However, No. 1 and No. 2 paper machines can continue to secure enough volume of steam for their respective operations, printing paper and base paper.

NO.1 Paper machine

313.5 UD

No. 2 Paper machine

 $3.2 \text{ Ut } \times 20 \text{ t} = 64.0 \text{ UD}$ 

Total

377.5 UD

3\$4 vD>377.5 vD

#### 4-6 Electric Power

- 1) The production of soap wrapper requires the most electricities 20 ADt/d x 2,000 kWH/t=40,000 kWH/d. Even if the electricity necessary for the boiler, feed-water and drainage system and illumination is added, the total consumption is about 44,000 kWH/d (1,834 kWH/hr).
- 2) BRPP has five diesel generators, with a total generation capacity of 238,080 kWH/d.

NIIGATA :  $1500 \text{kw} \times 24 \text{ Hr} \times 3 = 108,000 \text{ kwH/D}$ 

M.B.L : 2710 kw x 24 Hr x 2 = 130,080 kwH/D

Total 238,080 kwll/D

- 3) The F/S (Main Report) indicates that three generators can generate of the necessary power even after the renovation.
- 4) According to the project estimates, four generators are sufficient to provide both No. 1 and No. 2 paper machines with the necessary electric power. This leaves one generator on standby, which is an ideal operation form.

State of the state of the state of

#### 4-7 Water Source

1) The maximum clear water consumption is calculated as follows: 20 ADt/d x 280 m/ADt=5,600 m/d.

The maximum water consumption of the existing No.1 Paper Machine is 15,000 mVd, making the maximum total water consumption 20,600 mVd.

2) The availability of water was the lowest during the dry season (November of 1983) at 21,500 m/d, even under such conditions operation is possible.

The water consumption of No. 1 Paper Machine is 300 mVADt. However, since this machine will be used for the production of printing paper and form paper only, about 2,500 mVd (50 mV ADt x 50 t/d) of clear water can be saved.

#### 4-8 Plant Layout

Fig. 4-8-1 and Fig. 4-8-2 show the layout of No. 2 Paper Machine.

#### 4-9 Plant Construction Cost

The total investment necessary to construct the plant is US\$26,802,873 (US\$185,180,000 foreign currency and US\$8,284,873 local currency).

Table 4-9-1 shows the details of the construction fund.

The details of the machinery and equipment cost and the operating funds are shown in Tables 4-9-2 and 4-9-3.

#### 4-10 Construction schedule and Duration

Fig. 4-10-1 shows the construction schedule. The total construction period is 29 months from the planning and engineering to the start of operation. The operation of existing No. 1 Paper Machine will not disturbed during the construction of the No. 2 plant.

#### 4-11 Technical Cooperation

- 1) The those planned for this project will be produced in Indonesia for the first time. Therefore, it is assumed that none of the BRPP presonnel possesses the necessary technical knowledge for operation and production control.
- 2) Equipment suitable for those production shall be selected to eliminate potential problems with the equipment. Since the market is already familiar with imported thin, the same quality will be expected from BRPP. If BRPP can produce thin paper equivalent in quality to the imports, the product will find a ready market, thus making this project a success.
- 3) The key to making this project successful is how well and how quickly the production control and operation techniques can be mastered. Therefore, it would be an advantage for BRPP to solicit the cooperation of a paper manufacturer who already has the experience and knowledge to assist in the engineering and in the training of personnel in operation techniques.
- 4) Therefore, expenses for BRPP to train its employees at a paper manufacturing plants (abroad) in for approximately 25 man-months and engineering fees for plant construction are included in the construction budget of this project.

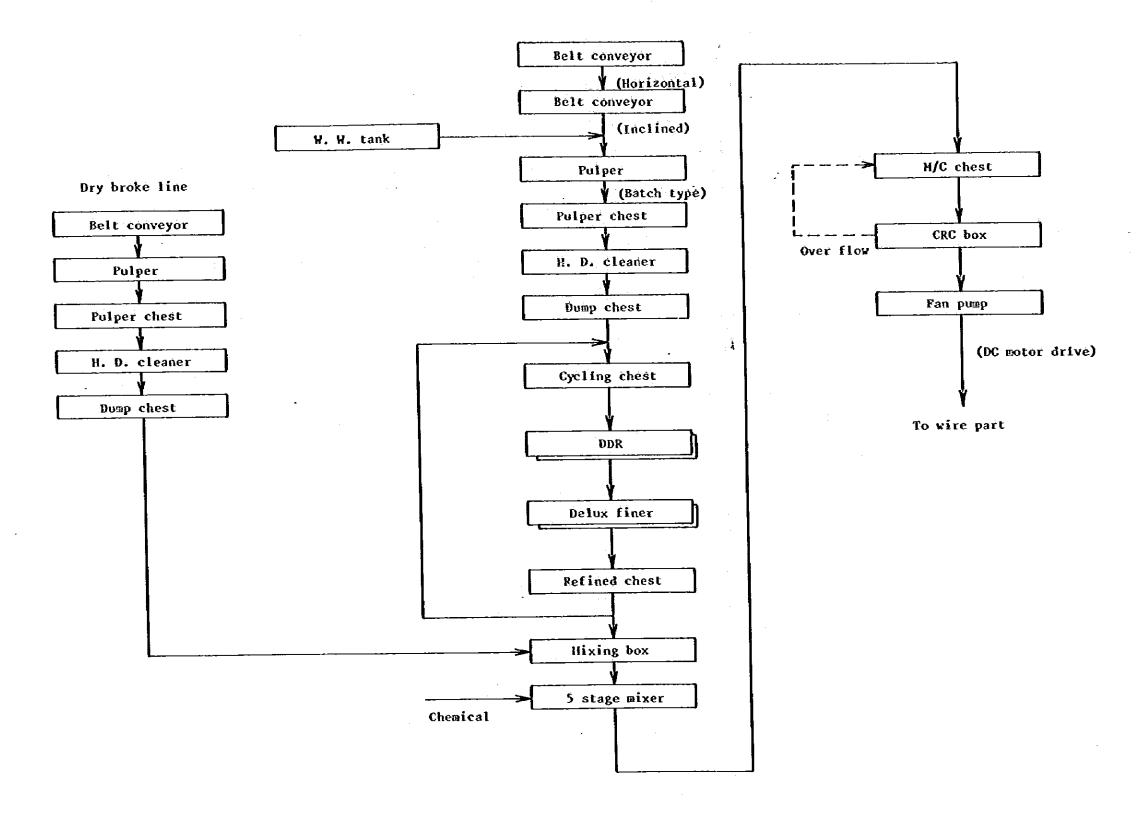


Fig. 4-1-1 Flow Chart of Stock Preparation for No. 2 Paper Hachine

Table 4-9-1 Total Funds Required for No. 2 Paper Machine Expansion

Unit: US\$

		0111.1	Tatal	Assig	nment	lst	year	2nd	year	3rd y	rear
No.	Description	Condition	Total Agount	Foreign	Local	Foreign	Lòcal	Foreign	Local	Foreign	Local
A	Direct plant cost										
1	Equipment cost	FOB price	12,878,000	12,878,000	-	3,863,000	-	9,015,000			<del></del>
2	Civil & building works	18.0% of FOB	2,318,000	1,391,000	927,000	1,391,000	278,000		464,000	-	185,000
3	Foundation works	2.0% of FOB	258,000	<u>.</u>	258,000		-	_	258,000	-	<u>-</u>
4	Installation works	10.0% of FOB '	1,288,000	193,000	1,095,000	-	<u>-</u>	193,000	1,095,000	-	
	Total (A)	-	16,742,000	14,462,000	2,280,000	5,254,000	278,000	9,208,000	1,817,000	-	185,000
В	Total plant capital cost							<u> </u>			
ì	Direct plant cost (A)		16,742,000	14,462,000	2,280,000	5,254,000	278,000	9,208,000	1,817,000	-	185,000
2	Price escallation	(A) x 4%	670,000	579,000	91,000	203,000	12,000	376,000	79,000		<del>-</del>
3	Import tax & duty	As exemption	<b>.</b>	<u>-</u>	_	_	-	<del></del> . ·	<u>-</u>		_
4	Freight & insurance	FOB x (6 + 4)%	1,288,000	773,000	515,000	281,000	63,000	492,000	452,000	-	<u>-</u>
5	Start up expenses	Wire cloth etc.	200,000	170,000	30,000	<u> </u>	-	-		170,000	30,000
6	Construction overhead	(A) x 17	167,000	144,000	23,000	53,000	3,000	91,000	20,000		-
7	Training cost		200,000	160,000	40,000	_		160,000	40,000	-	_
8	Eng. & supervision	(A) x 5%	837,000	837,000	-	460,000	. <del></del>	377,000	-	-	<u>-</u>
9	Overhead	(A) x 4%	670,000	670,000		369,000	-	301,000		-	<del>-</del>
10	Contingency	(A) x 5%	837,000	723,000	114,000	434,000	23,000	217,000	68,000	72,000	23,000
	Total (B)		21,611,000	18,518,000	3,093,000	7,054,000	379,000	11,222,000	2,476,000	242,000	238,000
С	Total capital investment										
1	Total plant capital cost	(B)	21,611,000	18,518,000	3,093,000	7,054,000	379,000	11,222,000	2,476,000	242,000	238,000
2	Interest during const.		3,039,600	_	3,039,600	-	846,480	-	2,193,120	-	-
- <del></del>	Total (C)		24,650,600	18,518,000	6,132,600	7,054,000	1,225,480	11,222,000	4,669,120	242,000	238,000
D	Working capital (D)		1,511,000	-	1,511,000	-	-			-	1,511,000
	Payment		641,273	-	641,273	-	-	-	641,273	<u> </u>	-
	Grand total		26,802,873	18,518,000	8,284,873	7,054,000	1,225,480	11,222,000	5,310,393	242,000	1,749,000

Percent of foreign portion: 18,518,000 x 100/26,802,873 = 69.1%

Percent of local portion: 8,284,873 x 100/26,802,873 = 30.9%

Table 4-9-2 Break Down Price List of No. 2 Paper Machine of BRPP

1 US = 230 Yen

Item No.	Description	Q'ty	Price ¥1,000	Price US\$	Remarks
1	Stock preparation				
	1) Stock preparation	l set	300,000	1,304,000	DDR. delux finer, pulper etc.
	2) Chemical preparation	1 set	70,000	304,000	Clay, alum, size, dye include fluorescent, starch etc.
	3) Spare parts	··· · · · ·	20,000	87,000	Disc plate for DDR and others
	Total		390,000	1,695,000	
2	Paper machine & finishing equ.				
	2-1 Paper machine				
	1) Head box	1 set	50,000	217,000	Air cushion pressurized, enclosed box type with multi-tube flow
	2) Wire part	1 sét	250,000	1,087,000	Cantilever type, shaking device, 7-suc. box, 1-dandy roll
	3) Press part	1 set	180,000	783,000	Combination press type, suc-pickup roll, grooved roll, etc.
	4) Dryer part	1 set	230,000	1,000,000	5-group dryer x 20pcs of dryer, 1,524 mm/x 2850 mmL
	5) Size press	l set	60,000	261,000	Inclined type
	6) M/C calender	1 set	80,000	348,000	
	7) Slitter	l set	8,000	35,000	Shear cutting type
	8) Reel	1 set	45,000	196,000	Horizontal double arm surface type, 1500 mms of reeling roll
	9) Drive system	1 set	120,000	522,000	Sectional drive by thyristor system
	10) BM control system	1 set	60,000	261,000	
	Sub total		1,083,000	4,710,000	
	2-2 Finishing equipment				
	1) Sheet cutter	2 sets	150,000	652,000	Double rotary cutter, 70 m/min of speed
	2) Super-calender	1 set	300,000	1,304,000	Directed loading system, 400 m/min of speed
	3) Roll grinding machine	1 set	50,000	217,000	
	Sub total		500,000	2,173,000	
	2-3 Auxiliary equipment				
	1) Vacuum system	1 set	50,000	217,000	Wire part and press part
	2) Dryer hood	1 set	50,000	217,000	Open hood type pocket ventilation system
	3) Drainage system	l set	35,000	152,000	Blow through system

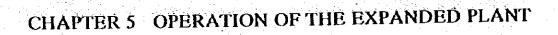
Item No.	Description	Q*ty	Price ¥1,000	Price US\$	Remarks
	4) Lubrication system	1 set	20,000	87,000	Porced circulating system
1	5) Operation panel	1 set	20,000	87,000	
}	6) Screen, white water re- covery & broke treatment	l set	65,000	283,000	3 stage centri-cleaner with vacuum pumps, vertical pressure screen, agitator of dry broke and couch pit
Ì	7) Pumps	1 set	20,000	87,000	17 pumps
	8) Instrumentation	1 set	50,000	217,000	
Ì	9) Electric equipment	1 set	80,000	348,000	
	10) Crane, paper roll handling	1 set	100,000	435,000	Overhead crane (10t+5t+5t), reel crane (2t+2t), for super calend
ł	11) Piping materials	1 set	40,000	174,000	
	12) Compresser	1 set	15,000	65,000	1 set of 6 m3/min for mill air, 1 set of 2.2 m3/m for inst. air
	13) Testing equ. for mill site	1 set	5,000	22,000	
	Sub total		550,000	2,391,000	
	2-4 Spare parts		207,000	900,000	
	Total	-	2,340,000	10,174,000	
3	Fork lift	3 sets	12,000	52,000	
4	Package boiler	1 set	60,000	261,000	10 ton/hr x 16 kg/cm <sup>2</sup> pressure with soft water treatment
5	Sub station	1 set	30,000	131,000	
6	Water & effluent treatment	l set	90,000	391,000	
7	Communication equipment	1 set	6,000	26,000	Telephone, hand-set at mill site
8	Fire fighting equipment	1 set	34,000	148,000	
	Grand total		2,962,000 include spare parts of 227,000	12,878,000 include spare parts of 987,000	

Table 4-9-3 Working Capital

Description	Raw	matérial	Calculation
Description	Price Rp/kg	Amount t/y	
1. Raw material inventory			
1-1. Import material (3 month)			·
NBKP	450	2,959.74	450 x 2,959.74 x 1/4 x 1,000 = 332,971,000
LBKP	410	3,080.84	$410 \times 3,080.84 \times 1/4 \times 1,000 = 315,786,000$
Sheet strength agent	720	10.50	$720 \times 10.50 \times 1/4 \times 1,000 = 1,890,000$
Pitch control agent	3,000	5.30	$3,000 \times 5.30 \times 1/4 \times 1,000 = 3,975,000$
Drainage accelerative	2,300	6.57	$2,300 \times 6.57 \times 1/4 \times 1,000 = 26,615,000$
Oil resisting agent	3,000	21.60	$3,000 \times 21.60 \times 1/4 \times 1,000 = 16,200,000$
Sub total ·			701,215,000
1-2. Local material (1 month)			
Clay	120	412.60	$120 \times 421.60 \times 1/4 \times 1,000 = 4,126,000$
Size	500	59.21	$500 \times 59.21 \times 1/4 \times 1,000 = 2,467,000$
Alun	90	78.40	$90 \times 78.40 \times 1/4 \times 1,000 = 588,000$
Sub total			7,181,000
Total			708,396,000
2. Product inventory (1 month)		·	Sales amount 9,627,600,000 x 1/12 = 802,300,000
Grand total			1,510,696,000 → 1,511,000,000 R

Fig. 4-10-1 No. 2 Paper Machine Expansion Schedule Plan

Description	1					lst								•					yea			:-			<u> </u>			<b></b>		3rd	yea	ır			
Description	1	2	3	4	5	6	7	8	9	10	11	12	1	2	3	4	5	6	7	8	9	10	11	12	1	2	3	4	5	6	7	8	9	10	11 12
1. Engineering works																						3.34 3													
a) Field survey for construction	=	{											-									: ,													
b) Preparation of tender specification		=																				. 5						<u> </u>				[			
c) Call for tender								<u> </u>									Ш															_			
d) Evaluation of proposal					÷	□													1			13					<u> </u>								
e) Decision of suppliers						-			<b>①</b>																										
f) Check & approval of drawing																						1 11				_	·				l				
g) Inspection and witness																		<b>5</b>		ㅁ								<u></u>							
h) Documentation																								==											
2. Construction works																																			
a) Design for machineries											+															<u> </u>									
b) Hanufacturing the machineries																			5			(s	/c)												
c) Shipping													1		1	١			<b> -</b> -					(s/	c)										
d) Erection and installation												Ī																	<u> </u>						
Paper machine, stock preparation								1							1				<b>.</b>						-										
Super calender						1																ż		<u> </u>	<b> -</b> -	{_									
Boiler and others																									<u></u>	<b>)</b>	Te	s t	<u> </u>						
e) Civil and building works						L						$\vdash$				=					E	=		<u> </u>	E	1_	<u> </u>	<u> </u>							
3. Operation works																																			
a) No load operation								Т																L.		þ									
b) Test running (Day run)							$\prod$	1																		C	1_		1_						
c) Test running (Full run)							T			Γ																		1=	1_	1_'					
d) Performance Guarantee test																													(	•	Р. С	). t	est		
4. Training at foreign country															F						ļ.								<u> </u>						
5. Operation supervision		+		-	-	-	+	-		╁-		-	-	-	-	-	1	┞	-		-	-	ig	_		-	_	1	+	+					



#### 5. OPERATION OF THE EXPANDED PLANT

#### 5-1 Number of Operating Days

The number of operating days is set at 315 days a year.

This is a reduct in from the current number of operating days on the existing plant of 342 days. This is to allow for the increased time necessary for the frequency of paper change for the production of multiple types of paper, each in small lots, and for cleaning of the chests, rolls and wire cloth for colored paper production.

#### 5-2 Number of Personnel

The total number of personnel necessary to operate this plant is 158 (details are shown in Table 5-2-1).

#### 5-3 Production and Production Plan

#### 1) Production of No. 2 Paper Machine

The nominal capacity of PM2 is set at 20 ADt/d (6,020 ADt/y). The overall efficiency of this plant is set at 83% (85% on some grades). Raising the overall efficiency to 89% or 90% can be expected in the future when the level of expertise in operation techniques is improved. The estimated annual production is then approximately 6,800 ADt.

#### 2) Operation rate

For the following reasons, the thin paper production rate is set at 50% in the first year, 80% in the second year and 100% in the third year.

- Since thin paper is produced for the first time and the quality of the production must be the same as that of imported thin, the production may not proceed smoothly in the early stages.
- 2. The Indonesian market for BRPP thin must be cultivated anew and the full scale production must wait until the market responds favorably to the product.

Table 5-2-1 Man Power Schedule

Section	Иел	bers (perso	n)				
occion	Day work	Shift	Total				
a. Stock preparation (3-shift)							
1) Chief of shift	<del>-</del> .	4	4				
2) Operators	<del>-</del>	12	12				
3) Pulper & chemical	-	-	_				
Sub total	-	16	16				
b. Paper machine (3-shift)		-					
1) Chief of section	1	: 	1				
2) Staff	1	<u>-</u>	1				
3) Laboratory in field		4 :-	4				
4) Chief of shift	_	4	4				
5) Operators	-	12	12				
Sub total	2	20	22				
c. Finishing section (3-shift)							
1) Chief of shift		. 1	- 1				
2) Super calender operators	_	16	16				
<ol><li>Sheet cutter and winder operators</li></ol>	_	24	24				
Sub total	~	40	40				
d. Finishing section (2-shift)			. !				
1) Chief of shift	<u> -</u>	<b>-</b>					
2) Soaters and counters	-	40 (F)	40 (F)				
3) Packing operators	-	20 (F)	20 (F)				
4) Stagger	-	14 (F)	14 (F)				
Sub total	_	74 (F)	74 (F)				
e. Boiler section	-	<u>±</u> 0	0				
f. Engineering section	-	<u>+</u> 0	0				

Section	Mer	mbers (pers	on)
Section.	Day work	Shift	Total
g. Laboratory	2	_	2
h. Sales section	4	-	4
Total	8	150	158

Hale : 84 persons

Female: 74 persons

Total : 158

# CHAPTER 6 FINANCIAL EVALUATION

# 6. FINANCIAL EVALUATION

# 6-1 Basic Policy of Financial Evaluation

When the project plans are executed and the effects are determined, the effects from investment on the existing mill and that from the new plant overlap making it difficult to isolate the effects of the new investment. Therefore, we evaluated the effects as follows.

- 1) The profits and losses on the installation of a new paper machine is calculated. This means that the impact on the existing plant is excluded from the calculation.
- 2) The equipment, administrative and personnel expenses that are shared by the new plant and the existing plant are divided according to the sales ratio for each paper machine. The results are added as a fixed cost.
- 3) The evaluation is to start in 1989, (the fiscal year adopted for BRPP is January-December).
- 4) All prices used for the evaluation are derived from BRPP's actual records for 1983, with some adjustments.

As a rule, no increase in the commodity prices and personnel expenses is calculated.

5) The currency used in this chapter is the Rupiah (Rp). The conversion rates are as follows:

U\$\$1.00=Rp 1,000 U\$\$1.00=¥ 230

# 6-2 Production and Sales Plan

#### 6-2-1 Conditions on Planning

- 1) The production and sales quantities are set at the same value, (estimating no stock increases or decreases).
- 2) The number of operating days is 315 days a year.
- 3) The number of operating days is calculated on each production item and the total should equal the number of annual operating days indicated above.
- 4) The current production of thin paper in the existing plant is to be stopped and the thin (two types of base paper for lamination and grease-proof paper) is to be produced by the new equipment.
- 5) The existing plant is to produce printing/writing paper and form paper only.

#### 6-2-2 Production and sales plan

Table 6-2-1 shows the production and sales plan for each product including efficiency factors in this project. The production plan includes the daily production and sales proceeds, variable cost, fixed cost and profits and losses.

Professional and the second of the

As shown in Table 6-2-1, the annual profit from the project is 493,096,000 Rp.

#### 6-2-3 Break-Even Point

Table 6-2-1 shows the break-even point for each product.

#### 6–3 Production Cost

#### 1) Production cost

The production cost is the total of the variable cost, the fixed cost and depreciation. (Table 6-3-1 shows the production cost for each product).

The average production cost is 1,309 Rp/AD kg, and the average sales price is 1,599.27 Rp/AD kg.

2) The unit prices that are used for the production cost calculation, such as the price of raw materials, personnel expenses, etc. are all based on BRPP records for 1983. The details are shown in Table 6-3-2.

The currency conversion rates are as follows:

US\$1.00=Rp 1.000

US\$1.00=Y 230

3) The consumption unit of pulp and other materials is shown in Table 3-3-2, 3-3-3 and 3-3-5.

## 6-4 Variable Cost

- 1) The average variable cost and variable cost of each product are shown in Tables 6-4-1 through 6-4-8.
- Since the power necessary to operate the plant can be supplied by the existing diesel generators, the electricity expense is calculated from the expense records for 1983 (60 Rp/kWH).

The recorded values of BRPP power generation in 1983 is 19,663,643 kWH and the diesel consumption is 5,575,300 liter.

19,663,643 kWH÷5,575,300 liter=3.5 kWH/L 210 Rp/L÷3.5 kWH/L=60 Rp/kWH

3) The necessary steam is to be supplied by the new boiler. If 13 UKL oil of steam is generated, the steam expense is 16,154 Rp/t.

210 Rp/L x 1,000 L÷13 t = 16,154 Rp/t

# 6-5 Fixed Cost

1) The fixed cost is calculated as a 'total fixed cost' by including the partial cost of the parts used in common by the existing and new plants. It is not the direct fixed cost only.

The breakdown of the total fixed cost is shown in Table 6-5-1 and the breakdown of the 'direct fixed cost' is shown in Table 6-5-2.

- 2) The fixed cost and depreciation costs for each product is shown in Table 6-5-3.
- 3) The expenses for production materials for paper making and packing materials are estimated from the records of similar plants in Japan and are set at 20 Rp/kg paper (Item 4, Table 6-5-2)
- 4) The maintenance expense is set at 1.8845% of the sales price (Item 3, Table 6-5-2).
- 5) Personnel expenses

As shown in Table 5-2-1, the total number of personnel necessary to operate this plant is 158, consisting of 84 men and 74 women. The wages for women employees are to be 65% of the wages for men. The details are shown in Table 6-5-2.

## 6-6 Depreciation

The depreciation rates are as follows:

a) Machinery and equipment

: 10 years

b) Building and fixtures

: 30 years

The fixed instalment method is used for the calculation and the remained book value will become zero. (The details are shown in Table 6-6-1).

#### 6-7 Total Fund Requirement

1) The total fund required is US\$26,802,873, (the details are shown in Table 4-9-1). The total fund requirement is summarized in the following.

No.	Description	US \$
(A)	Equipment	14,166,600
(B)	Construction	3,864,000
(C)	Price escallation	670,000
(D)	Start up expenses	200,000
(E)	Training cost	200,000
(F)	Eng. supervision fee	837,000
(G)	Overhead	837,000
(H)	Contingency	837,000
	Total	21,611,600
(1)	Interest payable during construction	3,039,000
<b>(</b> J)	Repayment	641,273
(K)	Working capital	1,511,000
	Grand total	26,802,873

- 2) The working capital is calculated as follows: three months for imported goods, one month for local goods and one month for BRPP products, (the details are shown in Table 4-9-3).
- 3) The investment schedule by years is shown in Table 4-9-1.

#### 6-8 Funds Procurement

30% of the total funds required shall be procured from equity while 70% shall be from long-term loans.

(Unit: US\$)

	Foreign	Local
Equity	—	8,039,862
Long-term loans	18,518,000	245,011

## 6-9 Interest and Repayment Method of Long-Term Loans

1) The following interest rates are set for the long-term loans:

a) Foreign currency loan

12%

b) Local currency loan

16%

# 2) Repayment of foreign currency loan

Two years of grace period will be followed by equal yearly payments for ten years. (The repayment schedule is shown in Table 6-9-1.)

# 6-10 Corporation Tax

The only corporate taxes to be paid is on the profit, which is calculated as follows:

Expressing the profit as A (=A1+A2+A3):

(1) A1 ≤ 10 million Rp

: A1 x 15/100

(2) 10 million Rp < A2 < 40 million Rp

: A2 x 25/100

(3) 40 million Rp < A3

: A3 x 35/100

Total corporate tax=0.15 A1+0.25 A2+0.35 A3

# 6-11 Profit and Loss Statement by Years (New Plant Only)

1) Table 6-11-1 shows the profit and loss statement for each year based on the conditions described below.

The upper column in the annual profit and loss statement shows the figures based on calculating total fixed cost; the lower column shows the figures based on the case calculating only the direct fixed cost.

Total fixed cost = Direct fixed cost + Fixed cost as expenses applied the to new plant for the parts used in common by the existing and new plants at a ratio corresponding to the sales ratio (43% of the fixed cost of existing plant)

- 2) When the calculation is based on the total fixed cost, the new plant generates a profit after taxes starting with the fourth year of operation. When the calculation is based on the direct fixed cost, the new plant generates a profit after taxes starting with the third year of operation.
- 3) The production rate is set at 50% of capacity in the first year, 80% in the second year and 100% from the third year.

# 6-12 Annual Profit and Loss Statement for BRPP

The annual statement for profits and losses on both the existing and new plants combined is shown in Table 6-12-1. The profit and loss figures for the existing plant is taken from Table 13-14-1 of the F/S (Main Report).

Table 6-2-1 Production and Sales Plan

Grade	Proc	luction plan	(sales)				Efficién	cies			Ur	nit pric	e/kg		Profit	& Loss			
	No. of days	Daily produc- tion	Produc- tion	Basis weight			Operating efficien- cy		Finish- ing yield	Total efficien- cy	Sales price	Varia- ble cost	Operation profit	Sales amount	Variable cost	Fixed cost	Profit/ loss	Break- even point	tion
··.	đ	t/d	t	g/m²	1223	m/min	8	7,	2	7.	Rp/kg	Rp/kg	Rp/kg	1,000Rp	1,000Rp	1,000Rp		t/d	7,
Base paper for laminate	85	20	1,700	36.1	2,330	199.0	98.0	96.5	88.0	83.0	1,500	581.76	918.24	2,550,000	988,996	1,397,424	163,580	17.9	89.5
Soap wrapper	90	20	1,800	30.0	2,330	239.4	98.0	96.5	88.0	83.0	1,640	654.85	985.15	2,952,000	1,178,721	1,479,625	293,654	16.7	83.5
Glassine (Regular)	40	20	720	28.5	2,330	226.8	98.0	96.5	88.0	83.0	1,700	668.30	1,031.70	1,224,000	481,174	657,611	85,215	15.9	88.3
(Red)	13	18	234	28.5	2,330	226.8	98.0	96.5	88.0	83.0	1,780	824.40	955.60	416,520	192,909	213,724	9,887	17.2	95.6
(Yellow)	13	18	234	28.5	2,330	226.8	98.0	96.5	88.0	83.0	1,780	802.80	977.20	416,520	187,854	213,724	14,942	16.8	93.3
(White)	14	18	252	28.5	2,330	226.8	98.0	96.5	88.0	83.0	1,780	682.22	1,097.78	448,560	171,919	230,164	46,477	15.0	83.3
Subtotal	80	18	1,440	28.5	2,330	226.8	98.0	96.5	88.0	83.0	1,740	717.96	1,022.04	2,505,600	1,033,856	1,315,223	156,521	16.1	89.4
Grease proof	60	18	1,080	38.0	2,330	166.0	98.0	96.5	90.0	85.0	1,500	698.37	801.63	1,620,000	754,242	986,417	Δ120,659	20.5	113.9
Total	315	194	6,020	-	-	-	-	_	-	-	1,599.27	657.11	942.16	9,627,600	3,955,815	5,178,689	493,096	17.4	91.1

# o Fixed cost breakdown (annual)

*1 Occurring fixed cost	2,753,104,000 Rp	
Distributed fixed cost	1,288,051,000 (application of common's fixed cost from existing mill.)	)
Interest payable	1,137,534,000 (average of 11 years)	_
Total	5,178,689,000 Rp	_

# \* Detail of \*1 (Direct cost and Depreciation)

1)	Personnel expenses	243,064
2)	Water cost	16,856
3)	Maintenance cost	181,432
4)	Others cost	120,400
	Sub total	561,752
5)	Depreciation	2,191,352
	Total	2,753,104

Table 6-3-1 Calculation for Production Cost

	Paper		Base paper	Soap		Gla	ssine		Grease
Cost Rp/AD	okg. paper	Average	for lamination	wrapper	Regular	Red	Yellow	White milk	proof
Variable cos	st	657.11	581.76	654.85	668.30	824.40	802.80	682.22	698.37
	Case of total fixed cost	287.88	275.09	275.09	305.65	305.65	305.65	305.65	305.65
Fixed cost	Case of direct fixed cost	(93.31)	(89.17)	(89.17)	(99.07)	(99.07)	(99.07)	(99.07)	(99.07)
Depreciation	ń	364.01	347.83	347.83	386.48	386.48	386.48	386.48	386.48
	Case of total fixed cost	1,309	1,204.68	1,277.77	1,360.43	1,516.53	1,494.93	1,374.35	1,390.50
Total	Case of direct fixed cost	(1,114.43)	(1,018.75)	(1,091.85)	(1,153.85)	(1,309.95)	(1,288.35)	(1,167.77)	(1,183.92)
Sales price		1,599.27	1,500	1,640	1,700	1,780	1,780	1,780	1,500
	Total fixed cost	290.27	295.32	362.23	339.57	263.47	285.07	405.65	109.50
Difference	Direct fixed cost	(484.84)	(481.25)	(548.15)	(546.15)	(470.05)	(491.65)	(612.23)	(316.08)

Note: 1) Total fixed cost = Direct fixed cost + Application of common's fixed cost from existing mill

2) Direct fixed cost

Table 6-3-2 List of Raw Materials Price

Raw i	naterials	Act. price in 1983, BRPP	Setting price
1. Pulp and fi	ller		
NBKP	Rp/BDkg	405.5	450
LBKP	Rp/BDkg	355.5	410
Clay	Rp/kg	72.67	120
2. Chemical			
Size pine	Rp/kg	443.67	500
Alum	Rp∕kģ	169.90 (as 18% Al <sub>2</sub> 0 <sub>3</sub> )	90 (as 8% Al <sub>2</sub> 0 <sub>3</sub> )
			202.5 (as 18% Al <sub>2</sub> O <sub>3</sub> )
Pitch cont	rol agent Rp/kg	-	3,000
Sheet stre	ngth agent Rp/kg	-	720
Drainage a	ccelerative Rp/kg	-	2,300
Oil resist	ing agent Rp/kg	-	3,000
Dye stuff	Rp/kg	-	8,000
3. Fuel			
Diesel oil	Rp/kg	126.45	210
Fuel oil	- Rp/kg	126.45	210

Table 6-4-1 Average Variable Cost

Description	Unite	consumption	Quantity kg	Unit price	Amount Rp	Remarks
1. Pulp cost NEKP		BDkg/ADC	2,959,742.8	æ	1,331,884,260	l Pulp total
Lake	ı	BDkg/ADt	3,080,842.8	410 Rp/BDkg	1,263,145,220	) 6,040,584.8 kg
Clay		BDkg/ADc	412,596	Ro/kg	49,511,520	
Sub total	1		6,453,180.8		2,644,541,000	
2. Chemical cost			,			
1~	6	kg/ADt	5,300.4	3,000 Rp/kg	15,901,200	
1.4		kg/ADt	10,500	720 Rp/kg	7,560,000	
se accel	•	ke/ADt	6,570	2,300 Rp/kg	15,111,000	
Oil resisting agent	•	kg/ADt	21,600	3,000 Rp/kg	64,800,000	
Size pine	1	kg/ADt	59,210	500 Rp/kg	29,605,000	
A. Marian	i	kg/ADt	78,400	RD.	7,056,000	
Dye stuff		ks/vdt	13,307.4	8,000 Rp/kg	106,459,200	
Sub cost		1	194,887.8	•	246,492,400	
3. Raw material cost			6,648,068.6		2,891,033,400	
4. Steam cost	•	t/ADt	23,260	16,154 Rp/t	375,742,040	
5. Blectric cost	1	kwh /AD t	11,484,000	60 Rp/kWh	689,040,000	
6. Grand total			•		3,955,815,440	
7. Variable cost/kg paper					657.11 Rp/ADkg paper	
8. Daily production	11.61	AD:c/D				
9. Number of operation	315	d/y				
10. Production	6,020	ADt/y.	and the second of the second o	E. M. C.	ende societas extrementos em faces constituidos	community management of the second of the se
		1				

Table 6-4-2. Variable Cost of Base Paper for Lamination.

-						
	Deserron	Unit consumption	Quantity kg	Unit price	Amount Rp	Remarks
٠;	Pulp cost	274.4 BDkg/ADt	087.997	450 Rp/BDkg	209,916,000	Pulp
	D. C. V.		1.105,000	410 Rp/BDkg	453,050,000	11.571,480 kg
	LBK	180.0 BDkg/ADC	306,000	120 Rp/kg	36,720,000	
	Sub rotal		1,877,480	-	699,686,000	
2	Chemical cost	0.6 kg/ADT	1,020	3,000 Rp/kg	3,060,000	
		3.0 kg/ADt	5,100	720 Rp/kg	3,672,000	
		- kg/ADτ	ı	-		
	Oil resisting agent	- kg/ADt	-	- Rp/kg	000 003 0	
	Size bine	10.0 kg/ADt	17,000	500 Rp/kg	9,500,000	
	A1um	17.0 kg/ADt	28,900	90 Rp/kg	7,001,000	
	Dye stuff	- kg/ADt	2	RP/KR		
	Sub cost	1	52,020	1	17,833,000	÷
3	Raw material cost		1,929,500		717,519,000	
		3.2 c/ADt	5,440	16,154 Rp/t	87,877,760	
;   <sub>^</sub>	Electric cost	1,800 kWh/ADt	3,060,000	60 Rp/kMh.	183,600,000	
9	Grand total				988,996,760	
1.	Variable cost/kg paper				581.76 Rp/ADkg paper	
80	Daily production	20 ADt/d				
6	Number of operation	85 d/y				
ខ្ព	Production	1,700 ADt/y				

Table 6-4-3 Variable Cost of Soap Wrapper

Description	Unit consumption	Quantity kg	Unit price	Amount Rp	Remarks
1. Pulp cost NEKP	355.6 BDkg/ADt	080.079	450 Rp/BDKg	288,036,000	) Pulp
LBXP	655.6 BDkg/ADC	1,	410 Rp/BDkg	483,832,800	J 1,820,160 kg
Clay	50.0 BDkg/ADt	000,06	120 Rp/kg	10,800,000	
Sub total		1,910,160		782,668,800	
2. Chemical cost	0.6 ks/ADE	080-1	3,000 Rp/kg	3,240,000	
Sheet strength agent	3.0 kg/ADt	5,400	720 Rp/kg	3,888,000	
Drainage accelerative	- kg/ADt		- Rp/kg	•	
Oil resisting agent	- kg/ADt		- Rp/kg	1	
Size pine	12.0 kg/ADt	21,600	500 Rp/kg	10,800,000	
Alum	17.0 kg/ADt	30,600	90 Rp/kg	2,754,000	
Dye stuff	- kg/ADt		= Rp/kg	i	
Sub cost		088*59	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	78,282,000	
3. Raw material cost		1,976,040		860,950,800	
4. Steam cost	3.5 t/ADt	008,3	16,154 Rp/t	101,770,200	
	2,000 kWh/ADt	3,600,000	60 Rp/kWn	216,000,000	
6. Grand cotal				1,178,721,000	
7. Variable cost/kg paper				654.85 Rp/ADkg paper	
8. Daily production	20 AD=/d				
9. Number of operation	4/۶ و				
10. Production	1,800 ADT/y		to the second se	reduced discuss of description of the second	A STATE OF THE STA
			:		

Table 6-4-4 Variable Cost of Glassine (Regular)

Description	Unic consumption	Quantity kg	Unit price	Amount Rp	Remarks
1. Pulp cost	728 9 8D/co/AD#	532,008	450 Rp/BDkg	239,403,600	
NEW TONG	316.7 BDkg/ADt	228,024	410 Rp/BDkg	93,489,840	
Clay	- BDkg/ADt	L	- Rp/kg		
Sub total		760,032		332,893,440	
2. Chemical cost	1.5 kg/AD	1,080	3,000 Rp/kg	3,240,000	
ATTENDED TO THE TOTAL TOTAL	- kg/ADt		ਤਮ/da -	•	
Sections appropries	- Kg/ADt	1	- Rp/kg	1	
Oil resisting agent	- kg/ADT	1	- Rp/kg	8	
	- kg/ADt	1	- Rp/kg		
21114 2216 M. L. A.	7.5 kg/ADt	2,400	90 Rp/kg	486,000	
Dve stuff	307/8X -			•	
tsoo qns	1	087*9	I	3,726,000	
3. Raw material cost		766,512		336,619,440	
4 Steam cost	5.0 t/ADt	3,600	16,154 Rp/c	58,154,400	
1	2,000 kWh /ADt	1,440,000	60 Rp/kWh	86,400,000	
6. Grand total	-			481,173,840	
7. Variable cost/kg paper				668.30 Rp/ADkg paper	
8. Daily production	18 ADt/d				
9. Number of operation	40 d/y				
10. Production	720 ADT/y				
1					

Table 6-4-5 Variable Cost of Glassine (Red)

Description	Unit consumption	Quantity kg	Unit price	Amount Rp	Remarks
1. Pulp cost	738.9 BDkg/ADt	172,902.6	450 Rp/BDkg	77,806,170	
TBKP	316.7 BDkg/ADt	74, 107, 8	410 Rp/BDkg	30,384,198	
Clay	= BDkg/AD⊄		- Rp/kg	1	
Sub rotal		247,010.4		108,190,368	
2. Chemical cost	0.8 kg/AD#	187.2	3.000 Rp/kg	\$61,600	:
	TOV/XX	1	- Rp/kg	1	
	10.0 kg/ADt	2,340	2,300 Rp/kg	5,382,000	
Oil resisting agent	- kg/ADt		- Rp/kg	1	
Size pine	40.0 kg/ADt	9,360	500 Rp/kg	4,680,000	And the second second
Alum	7.5 kg/ADt	1,755		157,950	
Dye stutt	2CV/8x 7.71	9*698*8	8,000 Rp/kg	26,956,800	·
asop ens	1	8-110-71	-	37,738,350	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
3. Raw material cost		264,022.2		145,928,718	
4. Steam cost	5.0 t/ADt	1,170	16,154 Rp/t	18,900,180	
S. Blectric cost	2,000 kWh/ADt	768,000	60 Rp/kwa	28,080,000	
6. Grand total				192,908,898	
7. Variable cost/kg paper				824.40 Rp/ADkg paper	
8. Daily production	18 ADt/d				
9. Number of operation	13 d/y				
10. Production	234 ADt/y			See a se	The second of the second

Table 6-4-6 Variable Cost of Glassine (Yellow)

		· 44.				
	Description	Unit consumption	Quantity kg	Unit price	Amount Rp	Remarks
<u> </u> -	1000 Mark 1000 M					
÷.	Mary Costs	738.9 BDkg/ADt	172,902.6	S.	77,806,170	
	TRICE	316.7 BDkg/ADt		410 Rp/BDkg	30, 384, 198	
	Clay	- BDkg/ADC		- Rp/kg		
	Sub total		247,010.4		108,190,368	
8	Ł	#UV/~? 6 0	187.2	3.000 Rb/kg	561,600	
	Price control agent	- ke/ADt		- Ro/kg	4	
	Drainge accelerative	10.0 kg/ADt	2,340	2,300 Rp/kg	5,382,000	
	Or Toniering Doese		6	- Rp/kg	3	
		40.0 kg/ADc	9,360	500 Rp/kg	4,680,000	
	0440 D4110	7.5 kg/ADT	1,755	90 Rp/kg	157,950	
	A TOTAL	11.7 kg/ADt	2,737.8	8,000 Rp/kg	21,902,400	
1	270 000		16,380	5	32,683,950	
_	Sub cost					
6	Raw moterial cost					
4	Steam cost	5.0 t/ADt	1,170	16,154 Rp/t	18,900,180	
Ŋ		2,000 kWh/ADC	000,897	60 Rp/kWh	28,080,000	
٥					140,874,318	
~	Variable cost/kg paper				802.80 Rp/ADkg paper	
ω,	Daily production	18 ADt/d				
9	Number	13 d/y				
ဒ္	. Production	234 ADt/y				

Table 6-4-7 Variable Cost of Glassine (White milk)

Description	Unit consumption	Quantity kg	Unit price	Amount Rp	Remarks
1. Pulp cost	727.8 8Dkg/ADt	183,405.6	450 RP/BDKg	82,532,520	A consequence of the consequence of the
LBKP	312.2 BDkg/ADt		410 Rp/EDkg	32,256,504	
Clay	23.0 BDkg/ADt	5,796	120 Rp/kg	695,520	
Sub total		267,876		115,484,544	
2. Chemical cost	+Cv/	761	29/ 48 000 E	378 000	
Sheer strongth agent	- kg/kgc	A77 -	- RD/Kg		
Drainage accelerative	7.5 kg/ADt	1.890	2 300 Rp/kg	7347 000	
Oil resisting agent	- kg/ADt	ı	- Rp/kg	£	
Size bine	7.5 kg/ADt	1,890	500 Rp/kg	945,000	
Altm	7.5 kg/ADC	1,890	90 Rp./kg	170,100	
Dye stuff	- kg/ADt		- Rp/kg	•	
Sub cost		5,796		5,840,100	
3. Raw material cost		273,672		121,324,644	
4. Steam cost	5.0 c/ADc	1,260	16,154 Rp/t	20,354,040	
5. Blectric cost	2,000 kWh/ADt	204,000	60 Rp/KWh	30,240,000	
6. Grand total				171,918,684	
7. Variable cost/kg paper				682.22 Rp/ADkg paper	
8. Daily production	18 ADt/d				
9. Number of operation	14 d/y				
10. Production	252 ADt/y				

Table 6-4-8 Variable Cost of Grease Proof

		Onantity kg	Unit price	Amount RP	Remarks
Description		C			
1. Pulp cost	100 0 00T		450 Rp/BDkg	356,383,800	
NBKP	135.5 500 XXXXX	1	410 Rp/BDkg	139,747,680	
2382	313 - 6 BUKK/ AUT	10,800	120 Rp/kg	1,296,000	
Clay	DOWNER OF OTHER	Ŀ		497, 427, 480	-
Sub total		1,143,612			
2. Chemical cost	* CV / T-1 3 F	1,620	3.000 Rp/kg	4,860,000	
	1.3 KX/XX - 1.4 AD#		Rp/kg	•	
Sheet strength agent	200/80 =	,	Rp/kg	\$	
Drainage accelerative	300/88 - 00 100/82 0 00	21,600	3,000 Rp/kg	64,800,000	
Oil resisting agent	2007 SX 0007				
Size pine	7 S	8 100	90 Rp/kg	729,000	
Alum	708/88 C./			5	
Dye stuff	- [			70 389 000	
Sub cost	•	31,320		200, 200, 201	
טפיר איזיא יייס כ		1,174,932		567,816,480	
	*U4/ * O ?	4,320	16,154 Rp/c	69,785,280	
4. Steam cost	١,		1. N. T.	114 640 000	
5. Electric cost	1,800 kWh/ADt	1,944,000	DWN/GW OG	0004044	
				754,241,760	
.				698.37 Rp/ADkg	
7. Variable cost/kg paper				paper	
a haily production	18 ADt/d				
1	A) 6/4				
9. Number of operation	1				
10. Production	1,080 ADT/y				

Table 6-5-1 Detail of Total Fixed Cost

Description	1 (1991)	2 (1992)	3 (1993)
<ol> <li>Application expenses to new plant apart from fixed cost in existence (exclude selling expenses)</li> </ol>	772,556	1,046,688	1,171,294
2. Direct fixed cost (Table 6-5-2)	561,752	561,752	561,752
Total fixed cost	1,334,308	1,608,440	1,733,046
Detail for application expenses Distributing ratio for application expenses by sales amount existing plant	10,645,408 (69%)	10,645,408 (58%)	10,645,408 (53%)
New plant	4,813,800 (312)	7,702,080 (42%)	9,627,600 (472)
1. Personnel expenses 795,592	?		
a) Total personnel expenses in existence = 1,018,954		Ì	
b) Personnel expenses for operators of existing paper machine and pulping plant = 223,362			
c) $\therefore$ 1,018,954 - 233,362 = 795,592			
2. Depreciation of existing	<b>)</b>		
3. Others fixed cost 918,572	2		
4. Administrative expenses 777,95	1		
Fixed cost for existing (A) 2,492,11	5 772,556 (Ax31%)	1,046,688 (Ax42%)	1,171,294 (Ax47%)
5. Selling expenses (B) 248,41	9 77,010 (Bx31%)	104,336 (Bx42%)	116,757 (Bx47%)

Note: Base figures of detail for application be collected from Table 13-14-1 in F/S main report.

Table 6-5-2 Detail of Direct Fixed Cost

	Description	Annual amount (1000 Rp)	Calculation
;	Personnel expenses	243,064	
7,	Water treatment cost	16,856	2.8 Rp/kg. paper x 6,020 ADt/y = 16,856
65	Maintenance cost	181,432	As 1.8845% of sales amount 9,627,600 x 0.01884 = 181,432
4.	Orhers.	120,400	20 Rp/kg. paper × 6,020 ADt/y = 120,400
	Total	561,752	Average 93.31 Rp/kg. paper

Note: Calculation of personnel expenses for No. 2 Paper Machine

Male : 84 persons x 1,840,000 Rp/y - 154,560,000 Rp/y

Female: 74 persons x 1,840,000 Rp/y x 0.65 = 88,504,000 Rp/y

Total 158 persons

243,064,000 Rp/y

# CHAPTER 7 PROFITABILITY AND ECONOMIC EFFECTS THE OF EXPANSION

Table 6-5-3 Detail of Fixed Cost and Depreciation for Each Paper

		Number	Production	Total	fixed cost	Direct	fixed cost	Deprecia	ation
Paper		of operation (days)	(ADt/y)	Amount (1,000Rp)	Unit Rø/kg paper	Amount (1,000Rp)	Unit Rp/kg paper	Amount (1,000Rp)	Unit Rp/kg paper
Base paper	r .	85	1,700	467,647.1	275.09	151,583.9	89.17	591,317.1	347.83
Soap wrapp	per	90	1,800	495,156.0	275.09	160,500.6	89.17	626,100.6	347.83
	Regular	40	720	220,069.3	305.65	71,333.6	99.07	278,266.9	386.48
	Red	13	234	71,522.5	305.65	23,183.4	99.07	90,436.8	386.48
}	Yellow	13	234	71,522.5	305.65	23,183.4	99.07	90,436.8	386.48
Glassine	White milk	14	252	77,024.3	305.65	24,966.7	99.07	97,393.4	386.48
:	Sub total	80	1,440	440,138.6	305.65	142,667.1	99.07	556,533.9	386.48
Grease pr		60	1,080	330,104.0	305.65	107,000.4	99.07	417,400.4	386.48
Tota	<del></del>	315	6,020	1,733,046.0	Av. 287.88	561,752.0	Av. 93.31	2,191,352.0	Av. 364.01

Note: 1) Total fixed cost = Direct fixed cost + Application expenses to new plant apart from fixed cost in existing mill

2) Direct fixed cost

Table 6-6-1 Calculation of Depreciation

(Unit: 1,000 Rp)

Ко.	Description	Detail	Amount to be depreciated	Depreciation years	Annual depreciation amount	Remarks
A	Equipment					
· -1	Equipment cost	A-1, B-4, B-6, B-9	15,003,000		·	
-2	Spare parts cost		(-) 987,000			
-3	Installation cost	A-4	1,288,000			
-4	Poundation cost	A-3	258,000			
-5	Price escallation	B-2	670,000			
	Sub total		16,232,000	10 years	1,623,200	
В	Civil and building cost	A-2	2,318,000	30 years	77,267	
c	Other expenses					
-1	Training and engineering	B-7, B-8	1,037,000			
-2	Contingency	B-10	837,000			
-3	Interest during const.	C-2	3,039,600			
-4	Payment		641,273			
	Sub total		5,554,873	10 years	555,487	
	Total		24,104,873		2,255,954	

Depreciation period = 
$$\frac{24,104,873}{2,255,954}$$
 = 10.7 years ••11 years

Annual depreciation amount = 
$$\frac{24,104,873,000}{11}$$
 = 2,191,352,000 Rp/y

Table 6-9-1 Repayment Schedule of Poreign Currency Loans and Interest

(1,000 Rp)Total Loan on 1st year Loan on -1st year Loan on -2nd year Interest Balance at Balance at Balance at Balance at Remarks i paid Balance Balance the begin-Amount of the begin-Amount of Amount of | Balance the begin-Amount of the begin-Balance at term-end ning of repayment ning of repayment at term-end repayment at term-end ning of at term-end ning of repayment the period the period the period the period Preconditions 7,054,000 846,480 7,054,000 7,054,000 \_ -2 7,054,000 1. All loans are 2,193,120 641,273 17,634,727 18,276,000 11,222,000 11,222,000 made at the 6,412,727 -1 7,054,000 641,273 beginning of 16,215,272 2,145,207 17,876,727 1,661,455 10,201,818 242,000 242,000 1,020,182 11,222,000 each term 6,412,727 641,273 5,771,454 1 (January 1). 14,531,817 1,945,833 16,215,272 1,683,455 22,000 220,000 242,000 10,201,818 | 1,020,182 9,181,636 641,273 5,130,181 2 5,771,454 2. The repayment of loans and 1,743,818 1,683,455 12,848,362 22,000 198,000 14,531,817 220,000 9,181,636 1,020,182 8,161,454 641,273 4,488,908 5,130,181 3 interest payment are at 11,164,907 1,541,803 22,000 176,000 12,848,362 1,683,455 198,000 1,020,182 7,141,272 641,273 3,847,635 8,161,454 4,488,908 4 the end of each term 11,164,907 1,683,455 9,481,452 1,339,789 22,000 154,000 176,000 7,141,272 1,020,182 6,121,090 641,273 3,206,362 3,847,635 5 (December 31). 132,000 9,481,452 1,683,455 7,797,997 1,137,774 22,000 154,000 1,020,182 5,100,908 6,121,090 3. The interest 641,273 2,565,089 3,206,362 shall be paid 7,797,997 1,683,455 6,114,542 935,760 110,000 22,000 4,080,726 132,000 5,100,908 1,020,182 2,565,089 1,923,816 for the past 641,273 7 period. 1,683,455 4,431,087 733,745 6,114,542 88,000 110,000 22,000 1,282,543 4,080,726 1,020,182 3,060,544 641,273 1,923,816 4. The interest 1,683,455 2,747,632 531,730 rate shall be 66,000 4,431,087 88,000 22,000 1,020,182 2,040,362 3,060,544 1,282,543 641,273 641,270 9 12% yearly. 1,064,180 329,716 2,747,632 1,683,452 1,020,180 22,000 44,000 2,040,362 1,020,182 66,000 5. Equal annual 641,270 Ó 641,270 10 repayment a 22,000 127,702 22,000 22,000 1,064,180 1,042,180 44,000 1,020,180 0 1,020,180 period of 10 11 years after 2 2,640 22,000 0 0 22,000 22,000 22,000 years grace. 12 0 15,555,117 18,518,000 242,000 0 0 (11,222,000) 11,222,000 7,054,000 Total

Talbe 6-11-1 Annual Statement of Profit and Loss of New Plant

(Unit: 1,000 Rp)

	(1989) -2	(1990) -1	(1991) 1	(1992) 2	(1993) 3	(1994) 4	(1995) 5	(1996) 6	(1997) 7	(1998) 8	(1999) 9	(2000) 10	(2001) 11
(Sales quantity)		-	(3,010t)	(4,816t)	(6,020t)	(6,020t)	(6,020t)	(6,020t)	(6,020t)	(6,020 <sub>€</sub> )	(6,020t)	(6,020t)	(6,020t)
Sales amounts	-	-	4,813,800	7,702,080	9,627,600	9,627,600	9,627,600	9,627,600	9,627,600	9,627,600	9,627,600	9,627,600	9,627,600
Variable cost		. <b>–</b>	1,977,908	3,164,652	3,955,815	3,955,815	3,955,815	3,955,815	3,955,815	3,955,815	3,955,815	3,955,815	3,955,815
Fixed cost	-		1,334,308	1,608,440	1,733,046	1,733,046	1,733,046	1,733,046	1,733,046	1,733,046	1,733,046	1,733,046	1,733,046
Depreciation	-	-	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352
Production cost total	-	_	5,503,568	6,964,444	7,880,213	7,880,213	7,880,213	7,880,213	7,880,213	7,880,213	7,880,213	7,880,213	7,880,213
Sales expenses	_	-	77,010	104,336	116,757	116,757	116,757	116,757	116,757	116,757	116,757	116,757	116,757
Interest payable	<b>-</b> ·	. –	2,145,207	1,945,833	1,743,818	1,541,803	1,339,789	1,137,774	935,760	733,745	531,730	329,716	127,702
Profit before tax	-	<b></b>	-2,911,985	-1,312,533	-113,188	88,827	290,841	492,856	694,870	896,885	1,098,900	1,300,914	1,502,928
Corporation tax	-	-	_	<del>-</del>	_	26,089	96,794	167,500	238,205	308,910	379,615	450,320	521,025
Profit after tax	-		-2,911,985	-1,312,533	-113,188	62,738	194,047	325,356	456,665	587,975	719,285	850,594	981,903
(Case of excludi	ing distri	outed cost)							· · · · · · · · · · · · · · · · · · ·		·	· ·	
Sales amounts	· <b>-</b>	-	4,813,800	7,702,080	9,627,600	9,627,600	9,627,600	9,627,600	9,627,600	9,627,600	9,627,600	9,627,600	9,627,600
Variable cost	-	-	1,977,908	3,164,652	3,955,815	3,955,815	3,955,815	3,955,815	3,955,815	3,955,815	3,955,815	3,955,815	3,955,815
Fixed cost	-	-	561,752	561,752	561,752	561,752	561,752	561,752	561,752	561,752	561,752	561,752	561,752
Depreciation	-	-	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352
Production cost total	_	-	4,731,012	5,917,756	6,708,919	6,708,919	6,708,919	6,708,919	6,708,919	6,708,919	6,708,919	6,708,919	6,708,919
Sales expenses	-	-	77,010	104,336	116,757	116,757	116,757	116,757	116,757	116,757	116,757	116,757	116,757
Interest payable	-	-	2,145,207	1,945,833	1,743,818	1,541,803	1,339,789	1,137,774	935,760	733,745	531,730	329,716	127,702
Profit before tax	-	-	-2,139,429	-265,845	1,058,106	1,260,121	1,462,135	1,664,150	1,866,164	2,068,179	2,270,194	2,472,208	2,674,222
Corporation tax		-	-	-	365,337	436,042	506,747	577,453	648,157	718,863	789,568	860,273	930,978
Profit after tax	-	-	-2,139,429	-265,845	692,769	824,079	955,388	1,086,697	1,218,007	1,349,316	1,480,626	1,611,935	1,743,244

Table 6-12-1 Annual Statement of Profit and Loss for All Existing and New Plants

		(1989) -2	(1990) -1	(1991) 1	(1992) 2	(1993) 3	(1994) 4	(1995) 5	(1996) 6	(1997) 7	(1998 <b>)</b> 8	(1999) 9	(2000) 10	(2001) 11
Profit from ex machines (befo		-408,242	-71,621	304,957	387,344	469,731	552,118	634,505	716,888	1,778,397	1,834,649	1,835,314	1,835,314	1,835,314
Profit from ne excluding dist costs (before	ributed	-	<del>-</del>	-2,139,429	-265,845	692,769	824,079	955,388	1,086,697	1,218,007	1,349,316	1,480,626	1,611,935	1,743,244
Total profit b	efore tax	-408,242	-71,621	-1,834,472	121,499	739,740	1,376,197	1,589,893	1,803,585	2,996,404	3,183,965	3,315,940	3,447,249	3,579,558
Corporation ta	ix	0	0	0	37,525	253,909	476,669	551,463	626,255	1,043,741	1,109,388	1,155,579	1,201,537	1,247,495
Profit after t	ax (A)	-408,242	-71,621	-1,834,472	83,974	485,831	899,528	1,038,430	1,177,330	1,952,663	2,074,577	2,160,361	2,245,712	2,331,063
	existing mashine	1,527,552	1,273,313	979,122	979,122	979,122	979,122	979,122	979,122	<u></u>	-	-	-	-
Depreciation	new mashine	<u>-</u>	-	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352
Total (B)		1,527,552	1,273,313	3,170,474	3,170,474	3,170,474	3,170,474	3,170,474	3,170,474	2,191,352	2,191,352	2,191,352	2,191,352	2,191,352
(A) + (B) pro depreciation	fit before	1,119,310	1,201,692	1,336,002	3,254,448	3,656,305	4,070,002	4,208,904	4,347,804	4,144,015	4,265,929	4,351,713	4,437,064	4,522,415
Loan	existing mashine	686,552	686,552	686,552	686,552	686,552	686,552	686,552	686,552	468,769	5,530	-	-	-
repayment	new mashine	-	-	1,661,455	1,683,455	1,683,455	1,683,455	1,683,455	1,683,455	1,683,455	1,683,455	1,683,455	1,683,455	1,683,455
Total		686,552	686,552	3,348,007	2,370,007	2,370,007	2,370,007	2,370,007	2,370,007	2,152,224	1,688,985	1,683,455	1,683,455	1,683,455

# 7. PROFITABILITY AND ECONOMIC EFFECTS OF THE EXPANSION

# 7-1 Break-Even Point by Grades

The figures for the break-even point are shown in Table 6-2-1. The average break-even point is 17.4 ADUd (average daily production of 19.1 ADI), which is not a too favorable figure.

## 7-2 Calculation of Incoming and Outgoing Funds

1) The annual statement of profits and losses for the new plant is shown in Table 6-11-1. The new plant can show a profit begining with the fourth year of operation.

The statement of the total profit and loss for both the existing and the new plants is shown in Table 6-12-1. With the two combined, the operation shows a profit even during the new plant construction period.

2) The estimated cumulative profits after taxes in the six years from 1994 to 1999 is as follows: Table 7-2-1 Estimated Cumulative Profit after Taxes over a Six-year Operation Period

	1994 ~ 1999
A) New plant only	2,346,066,000 Rp
B) Existing plant only	4,808,716,000 Rp
Total	7,154,782,000 Rp
C) Profit from (A + B)	9,302,889,000 Rp
D) Balance	2,148,107,000 Rp

This table indicates that the average annual profit after taxes is 391,011,000 Rp for the new plant and 801,425,667 Rp for the existing plants if the operation results are calculated separately, for a total average annual profit of 1,192,436,667 Rp. However, if the results of the operation these two plants are combined, the average annual profit is 1,550,481,500 Rp, about a 30% increase in profit.

#### 7-3 Profit Ratio and Loan Repayment Ability

- 1) The annual profit ratio and the loan repayment ability are shown in Table 7-3-1.
- 2) This project can begin loan repayments from the third year; the average ability over eleven years is about 135%.

#### 7-4 Calculation of Internal Rate of Return (IRR)

- 1) The internal rate of return for this project is shown in Table 7-4-1. The estimated IRR is a rather low, 5.3%.
- 2) The changes in IRR when the sales price only is changed can be shown by the following expression:

 $Y (IRR) = 34/100 \times X + 5.3$ 

X%: Increase ratio of sales price

3) The changes in IRR when the sales price and the total investment are both changed are shown in Table 7-4-2.

If the sales price is increased by 10% and the investment is reduced by 20%, the IRR is 10.7%.

# 7-5 Financial Indices

The financial indices used in these calculations are shown in Table 7-5-1.

	Rate of net	Before-tax	Loan
Year	profit on	profit rate	repayment
	sales (%)	on investment (%)	ability (%)
1 (1991)	-60.5	-12.6	37.4
2 (1992)	-17.0	-5.7	77.8
3 (1993)	-1.2	-0.5	111.5
4 (1994)	0.7	0.4	117.7
5 (1995)	2.0	1.3	123.2
6 (1996)	3.4	2.1	129.5
7 (1997)	4.7	3.0	136.8
8 (1998)	6.1	3.9	145.3
9 (1999)	7.5	4.8	155.4
10 (2000)	8.8	5.6	167.5
11 (2001)	10.2	6.5	282.2

Table 7-3-1 Profit Ratio and Loan Repayment Ability Calculation by Year (Foreign currency portion)

Year	Production ADt/y	Operation rate (%)	Sales amount (1,000 Rp/y)	Profit (1,000 Rp/y)		Profit ratio on sales (%)		Turnover ratio of investment	Before-tax profit ratio	Loan repayment
				Before tax	After tax	Before tax	After tax	(2)	on investment	ability (%)
1 (1991)	3,010	50.0	4,813,800	-2,911,985	-2,911,985	-60.5	-60.5	17.96	-12.6	34.72
2 (1992)	4,816	80.0	7,702,080	-1,312,533	-1,312,533	-17.0	-17.0	28.74	- 5.7	77.83
3 (1993)	6,020	100.0	9,627,600	-113,188	-113,188	-1.2	-1.2	35.92	- 0.5	111.52
4 (1994)	6,020	100.0	9,627,600	88,827	62,738	0.9	0.7	35.92	0.4	117.69
5 (1995)	6,020	100.0	9,627,600	290,841	194,047	3.0	2.0	35.92	1.3	123.22
6 (1996)	6,020	100.0	9,627,600	492,856	325,356	5.1	3.4	35.92	2.1	129.54
7 (1997)	6,020	100.0	9,627,600	694,870	456,665	7.2	4.7	35.92	3.0	136.83
8 (1998)	6,020	100.0	9,627,600	896,885	587,975	9.3	6.1	35.92	3.9	145.34
9 (1999)	6,020	100.0	9,627,600	1,098,900	719,285	11.4	7.5	35.92	4.8	155.40
10 (2000)	6,020	100.0	9,627,600	1,300,914	850,594	13.5	8.8	35.92	5.6	167.48
11 (2001)	6,020	100.0	9,627,600	1,502,928	981,903	15.6	10.2	35.92	6.5	282.16

Total fund invested: 26,802,873,000 Rp

Annual loan repayment ability = Depreciation + Profit after tax + Interest paid

Loan repayment + Interest paid

Table 7-4-0 Annual Statement of Profit and Loss Expansion Plant, Basuki Rachmat Will (for IRR calculation)

			-	-					(Unit	(Unit: 1,000 Rp)	
Year	1 (1991)	2 (1992)	3 (1993)	4 (1994)	5 (1995)	6 (1996)	7 (1997)	8 (1998)	9 (1999)	1 O (2000)	1 1 (2001)
Production (t/y)	3010	4816	6020	6020	6020	6020	6020	6020	6020	6020	6020
Sales amount	4813800	7702080	9627600	9627600	9627600	9627600	9627600	9627600	9627600	9627600	9627600
Production cos	st	•	•		•						£ <b></b>
Variable cost Fixed cost Depreciation	1977908 1334308 2191352	3164652 1608440 2191352	3955815 1733046 2191352	3955815 1733046 2191352	3955815 1733046 2191352	3955815 1733046 2191352	3955815 1733046 2191352	3955815 1733046 2191352	3955815 1733846 2191352	3955815 1733046 2191352	3955815 1733046 2191352
Total	5503568	6964444	7880213	7880213	7880213	7880213	7880213	7880213	7880213	7880213	7880213
Sales expense	s 77010	104336	116757	116757	116757	116757	116757	116757	116757	116757	116757
Interest payable	2145207	1945833	1743818	1541803	1339789	1137774	935760	133745	531730	329716	127702
Profit before tax	-2911985	-1312533	-113188	88827	290841	492856	694870	896885	1098900	1300914	1502928
Corporation tax	0	0	0	26089	96794	167500	238205	308910	379615	450320	521025
Profit after	-2911985	-1312533	-113188	62738	194047	325356	456665	587975	719285	850594	981903
tax											

TAble 7-4-1 IRR of Expansion Plant, Basuki Rachmat Mill .

א	Nе	t flow	·	5.	3 %		5.	4 %	
		1000RP	-			1000RP			1000RP
-1	-13 2 3 3 3 3 3	433000 698000 566426 490878 139143 139143 139143 139143 139143			0.950 0.902 0.856 0.813 0.772 0.734 0.697 0.662 0.597 0.567	1872955 1778685 1689159	-		-7052182 -12330365 -483750 2018320 2413282 2289641 2172335 2061039 1955445 1855261 1760210 1670028
	3						<b>-</b> -		0.532 0.505

IRR determined from the above ----- 5. 3 %

Table 7-4-2 Sensitivity Analysis of Expansion Plant, Basuki Rachmat Mill

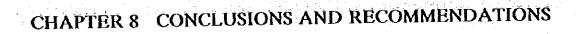
The internal rate of return from the expansion based on changes in sales prices and investment is calculated as shown below.

Internal Rate of Return (I.R.R.)

(Vnit: %)

			Interna	I hate or	• • • • • • • • • • • • • • • • • • • •				
Sales price Investment	-10%	-7.5%	-5%	-2.5%	0%	+2.5%	+5%	+7.5%	+10%
-20%	2.3	3.5	4.6	5.7	6.8	7.8	8.8	9.8	10.7
-15%	2.1	3.2	4.3	5.4	6.4	7.4	8.3	9.3	10.1
-10%	1.9	3.0	4.0	5.0	6.0	6.9	7.9	8.8	9.6
-5%	1.7	2.7	3.7	4.7	5.6	6.6	7.4	8.3	9.1
0%	1.5	2.5	3.5	4.4	5.3	6.2	7.1	7.9	8.7
+5%	1.4	2.3	3.3	4.2	5.0	5.9	6.7	7.5	8.3
+10%	1.3	2.2	3.1	3.9	4.8	5.6	6.4	7.2	7.9
+15%	1.1	2.0	2.9	3.7	4.5	5.3	6.1	6.8	7.6
+20%	1.0	1.9	2.7	3.5	4.3	5,1	5.8	6.5	7.2

Sales price + .... Increase
- .... Decrease
Investment + .... Increase
- .... Decrease



#### 8. CONCLUSIONS AND RECOMMENDATIONS

8-1 The results of our investigation of the renovation plan (F/S Main Report) has already been reported.

The report was prepared to assist BRPP in curing its deficits, strengthen its management foundation and contribute to developing the district as a viable industrial area. The following is the basic proposal.

- a) In product Quality
- b) Increase efficiency while reducing cost
- c) Gradual conversion from the production of printing/writing paper to products of higher yield and value, to increase profit

This report describes our proposal for the installation of a new paper machine for specialized thin production, which is a product of a higher added value, after the implementation of the renovation plan and the stabilization of the BRPP management.

- 8-2 The plan for the a installation new paper machine (PM2) is outlined below.
  - The existing No. 1 Paper Machine is to be used for the production of printing/writing paper and form paper only.
  - 2) The installation of an additional paper machine (PM2)

A special paper machine with daily production a capacity of 20 ADt shall be installed to produce and sell 6,020 ADt of special thin paper. The machine will produce the four grades of base paper for lamination, soap wrapper, glassine and greaseproof paper.

- The existing pulp plant is not be renovated, nor shall a new pulp plant be constructed. All of pulp the needed is to be purchased.
- 4) An effluent treatment system for each, including effluent treatment for the existing plant and auxiliary equipment such as the boiler shall be installed.
- 5) Employee training and technical cooperation.

Some employees shall be sent abroad for training. For proper construction of the facilities, BRPP shall also receive technical assistance from experienced engineers from foreign paper companies.

Total funds required: US\$26,892,873 (including the foreign currency portion of US\$18,518,000)

7) Annual proceeds for sales amount

: US\$9,627,600

8) Construction period

: 29 months

9) Number of additional Employees

: 158

#### 8-3 Market

The scheduled production wil satisfy 85% or more of the total thin consumption in Indonesia. For the project to be cost effective, it requires 85% or more of the market share. Since this cannot be accomplished easily, BRPP must plan on exporting a portion of its production to the other ASEAN countries.

大大,大大的林树,还是有好好,不知时间,我们会说。

#### 8-4 Expected Profit after Implementing Expansion plan

1) IRR after Taxes: 5.3%

The projected IRR when the fixed cost of the existing plant is distributed according to the sales ratio (194.57 Rp per kg of product) is 5.3%.

2) IRR after Taxes (Sensitivity analysis)

a) When the sales price only is increased by 10% : 8.7%

b) When the investment only is decreased by 20%: 6.8%

c) When both a) and b) are applied : 10.7%

#### 3) Profits after taxes

This project generates a profit starting with the fourth year of the operation However, if the calculation is based on the total proceeds from both the existing and the new plants, BRPP can generate profit through the entire period.

#### 4) Financial status

This project shows a deficit up to the second year after the start of operation. The loan repayment ability is low, at 110 to 167% which is not indicative of sound financial status.

#### 8-5 Conclusions and Recommendations

- 1) Based on the results of the investigation described above, this expansion plan can not be considered economically feasible. The major reasons are as follows:
  - a) The cost of new plant is extremely high since it must share the fixed cost of the existing plant. The fixed cost of the new plant averages 287.88 Rp/kg paper, of which 67% (194.57 Rp/kg paper) is for the existing plant.
  - b) The depreciation is extremely high (average 364.01 Rp/kg paper).
    These two factors increase the cost, thus reducing the profit and the IRR.
- 2) However, if the following measures are taken and governmental support is obtained, the IRR can be raised to approximately 10.3, which would make the expansion plan feasible.
  - a) Relative to Item

Only the direct fixed cost (93.31 Rp/kg paper) should be applied to the fixed cost. In other words, the fixed cost on the existing plant has already been calculated as the fixed cost of the plant. Therefore this project should share the cost needed to install a new plant within BRPP.

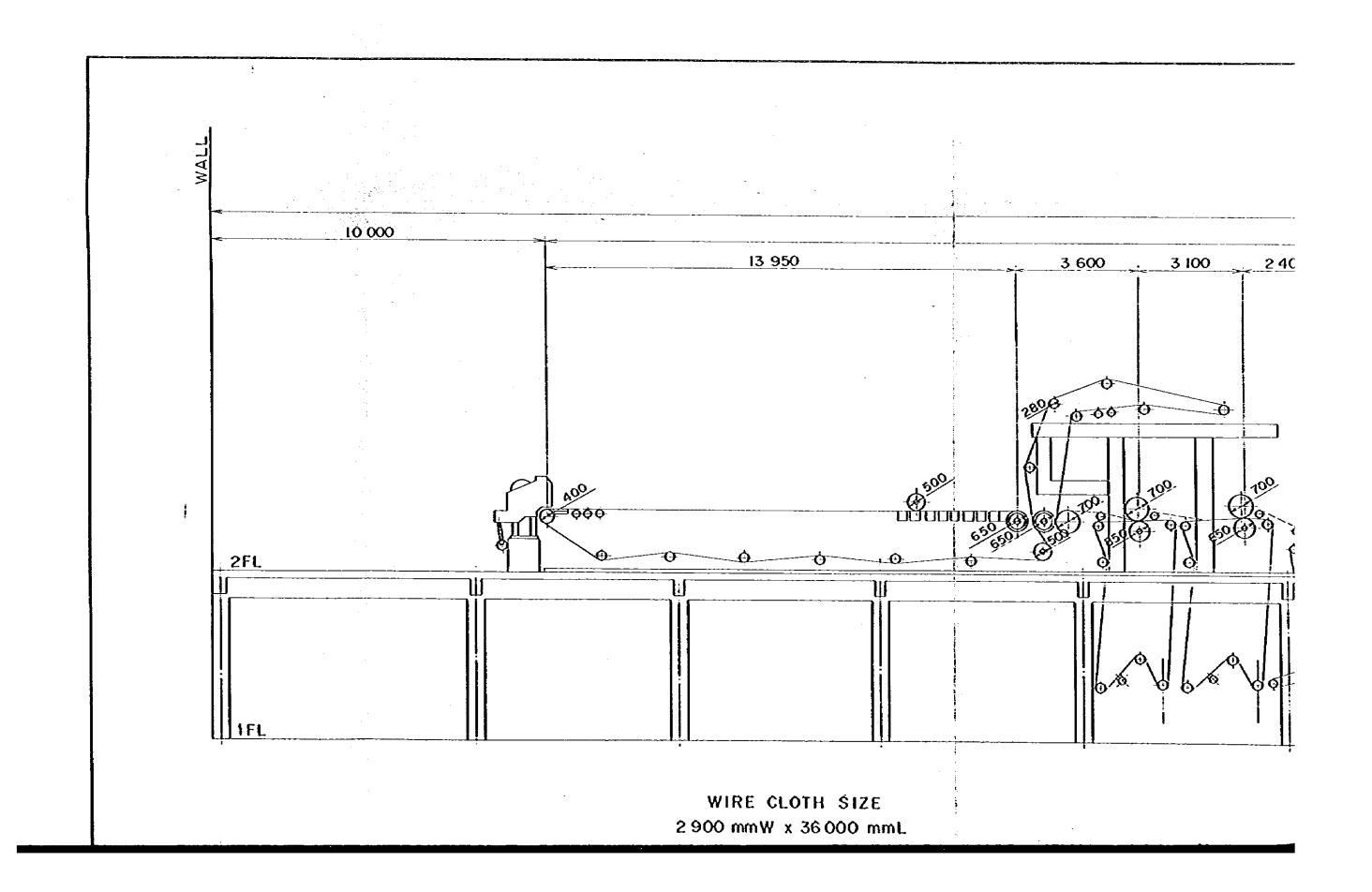
b) Relative to Item

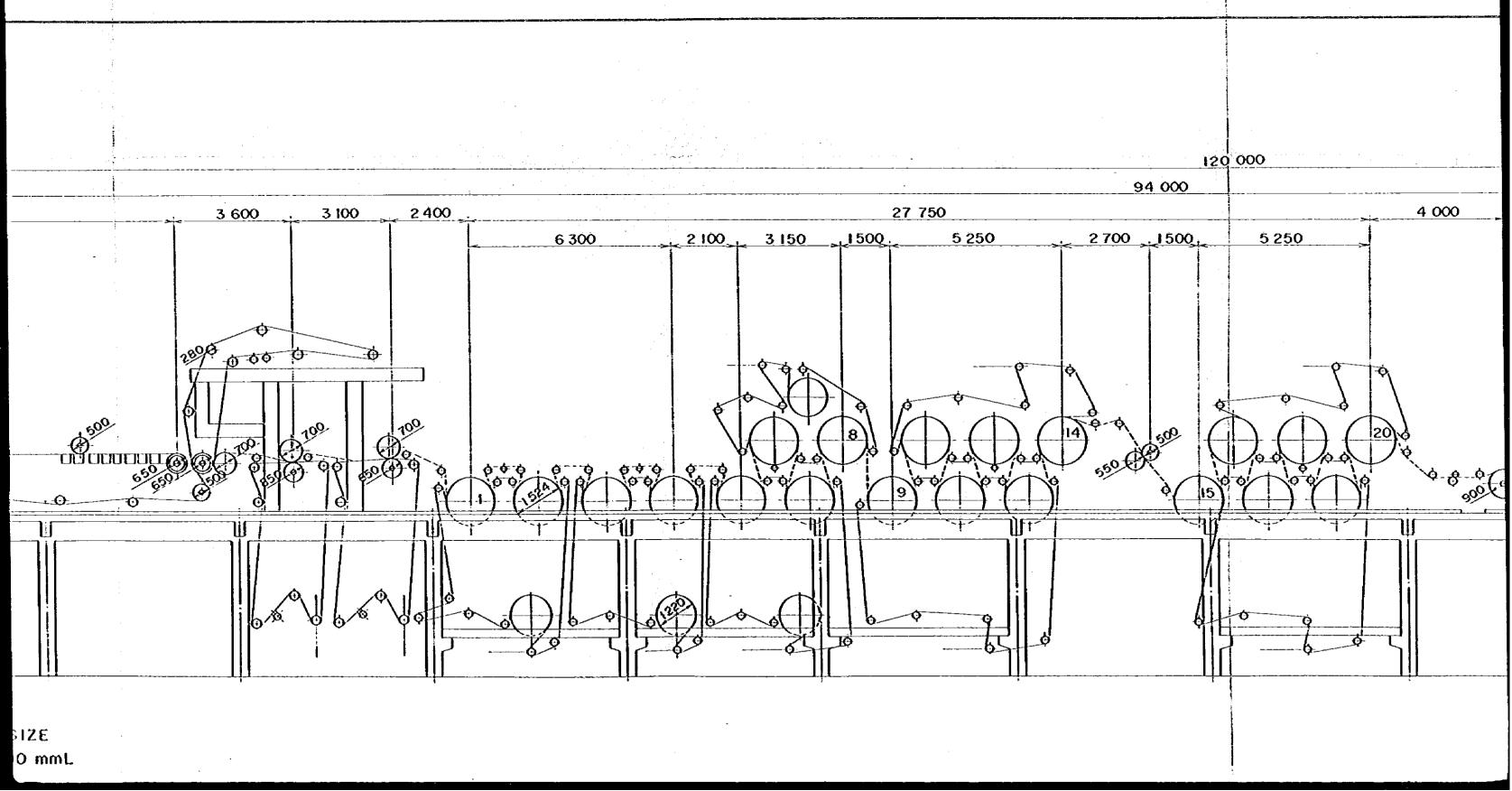
The waste water treatment facilities should be installed with the funds from the existing plant. The installation of a BM control system and a size press should be postponed.

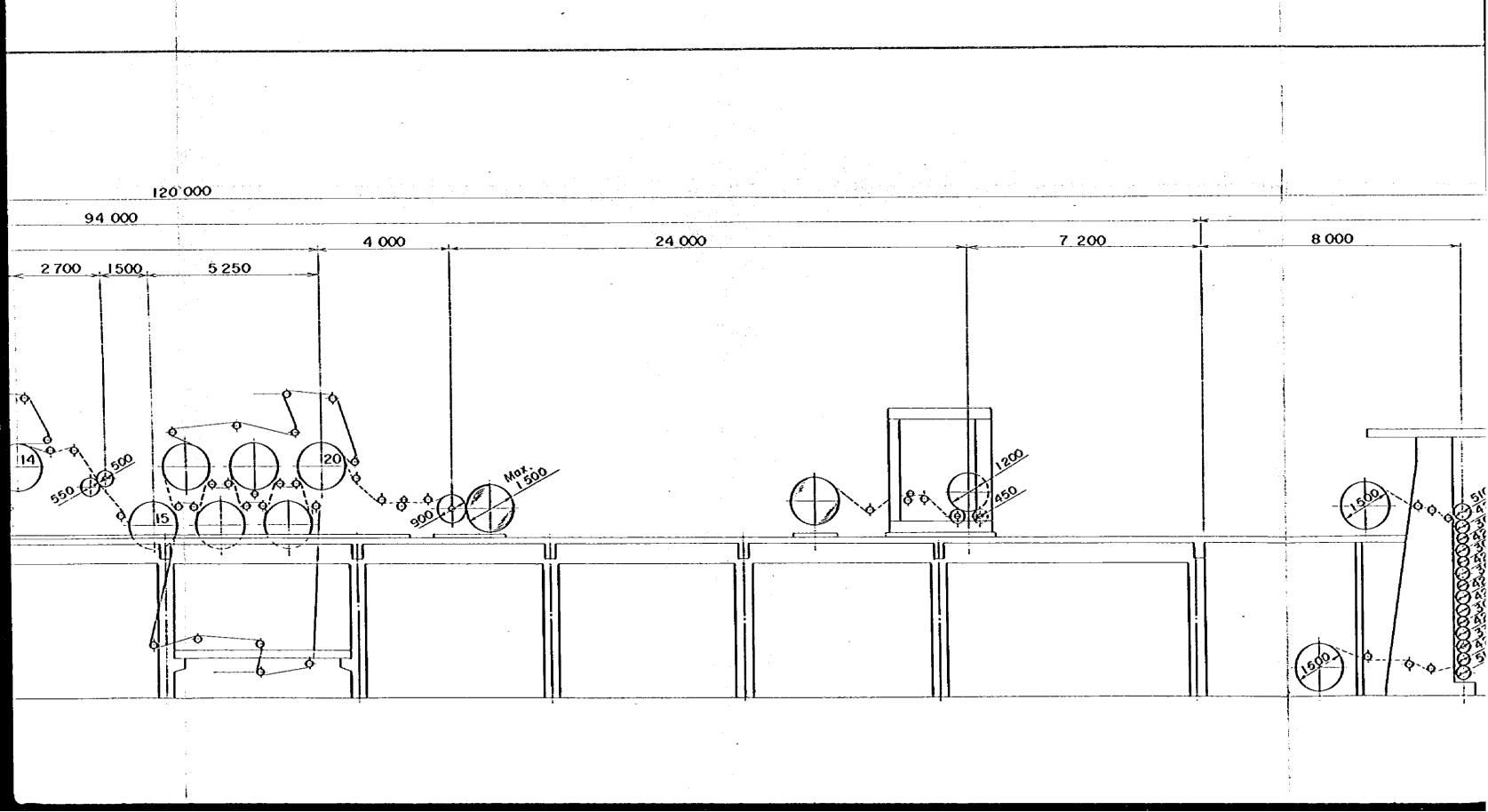
c) If these three items are excluded from the project, approximately US\$2,000,000 can be saved in the total investment.

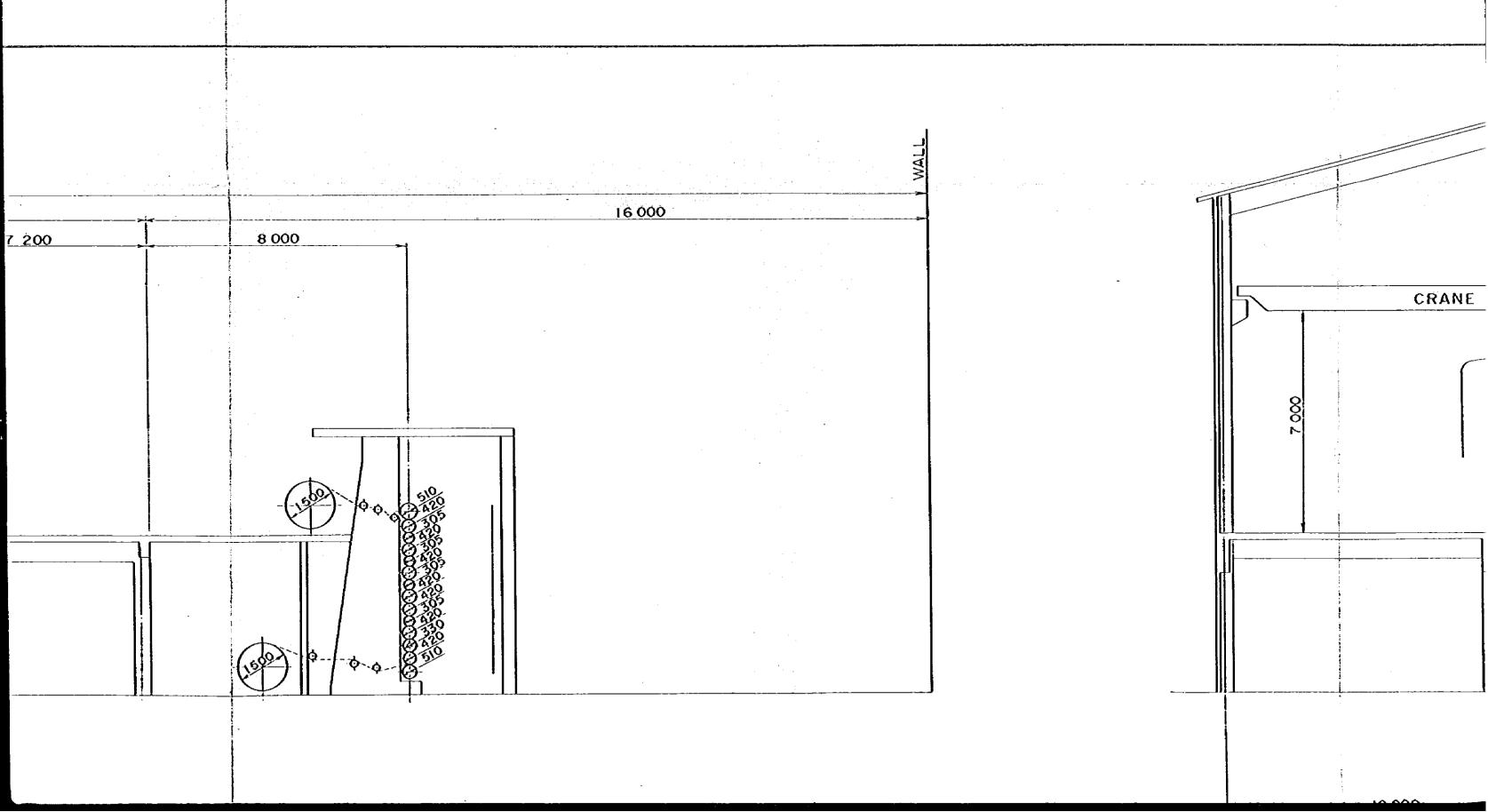
If the measures a), b), and c) are implemented and the interest rate on foreign currency loans is quaranteed by the government, at 8% to 10% this expansion plan can be feasible.

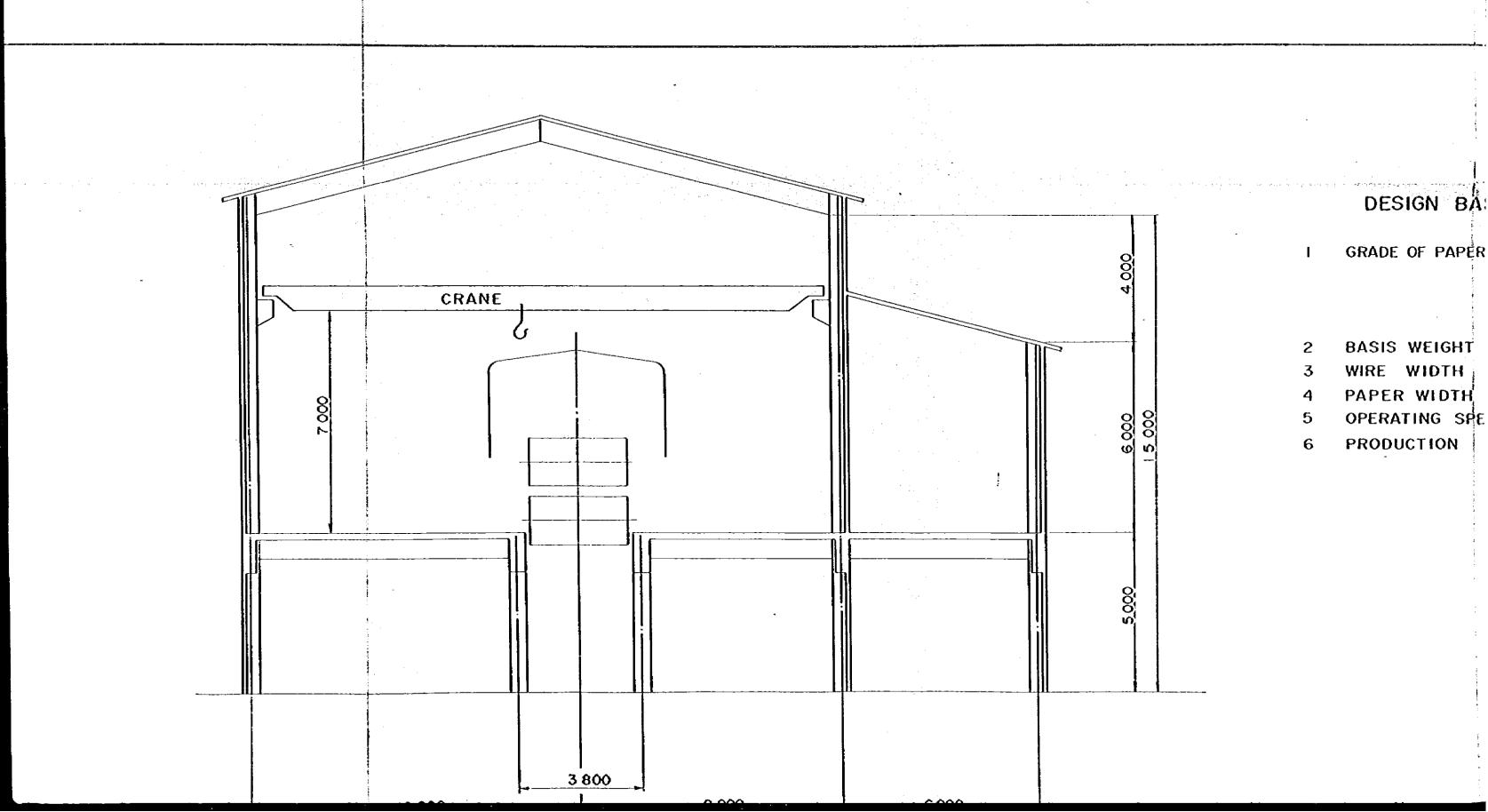
- 3) Indonesia should pursue this expansion program as a matter of national policy, for the following reasons:
  - a) BRPP is a national plant and plays a significant role in the promotion and stabilization industry and employment in the district.
  - b) There are no national plants in Indonesia that have paper machines other than BRPP. The BRPP's burden of fixed costs must be reduced. BRPP also must acquire flexibility and diversity in its operation by installing an additional paper machine. We firmly believe that this additional installation is necessary for achieving the basic objectives, of maintaining healthy management and continuing growth.
- 4) The renovation program contained in the F/S (Main Report) should be implemented. We recommend that this expansion plan be executed at an opportune time to minimize the risk, under the strong guidance and support of the Indonesian government.

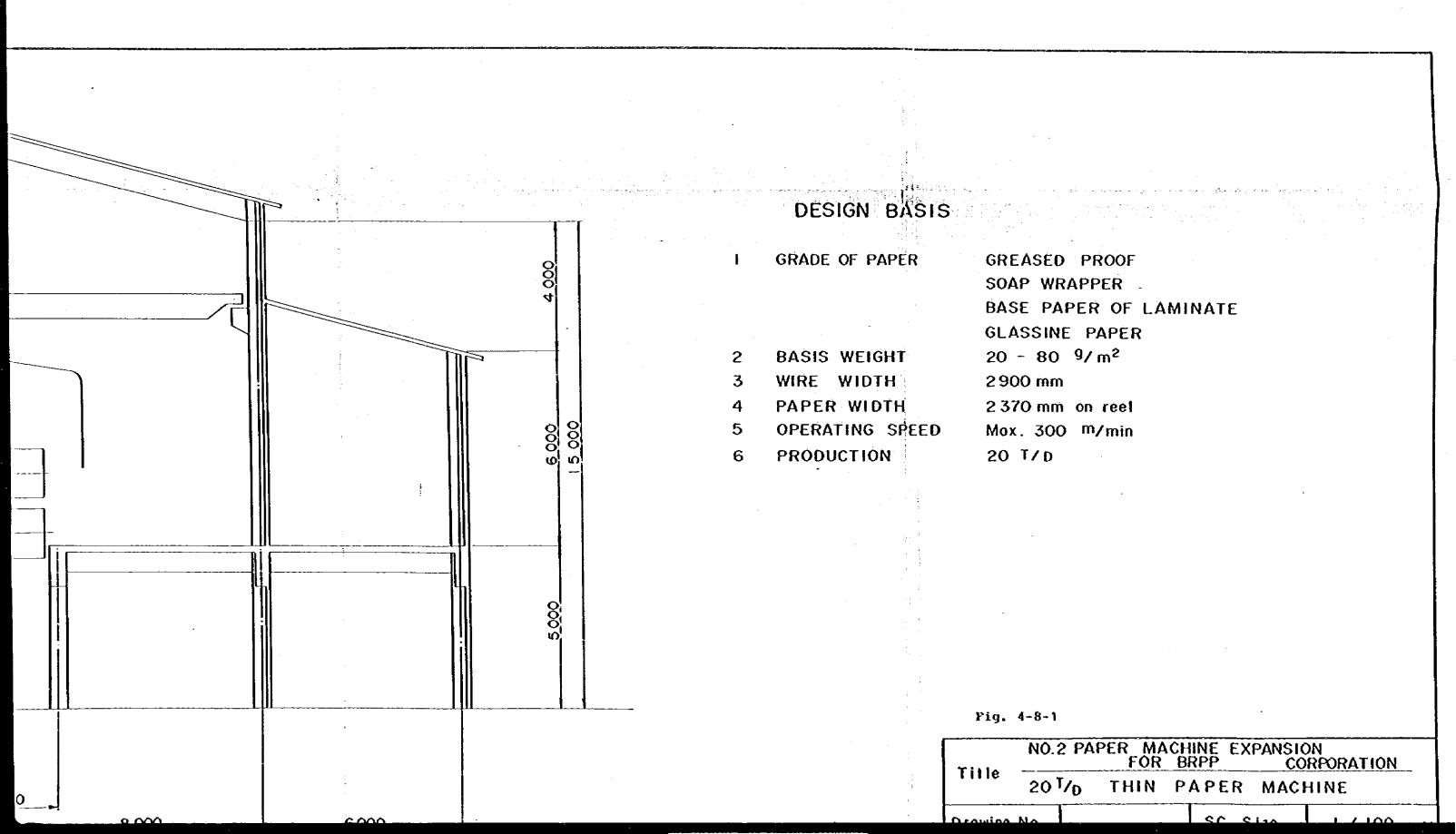


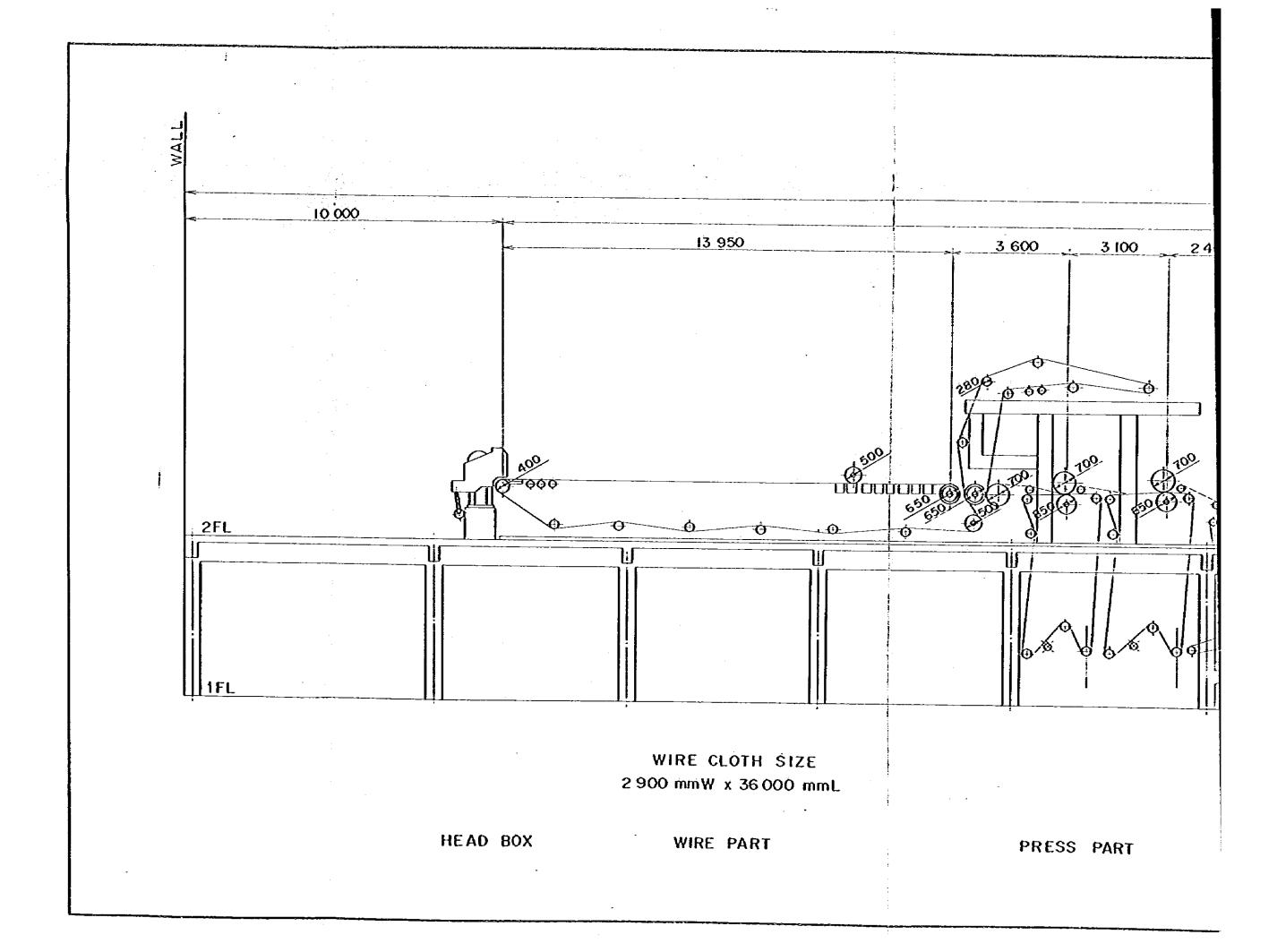


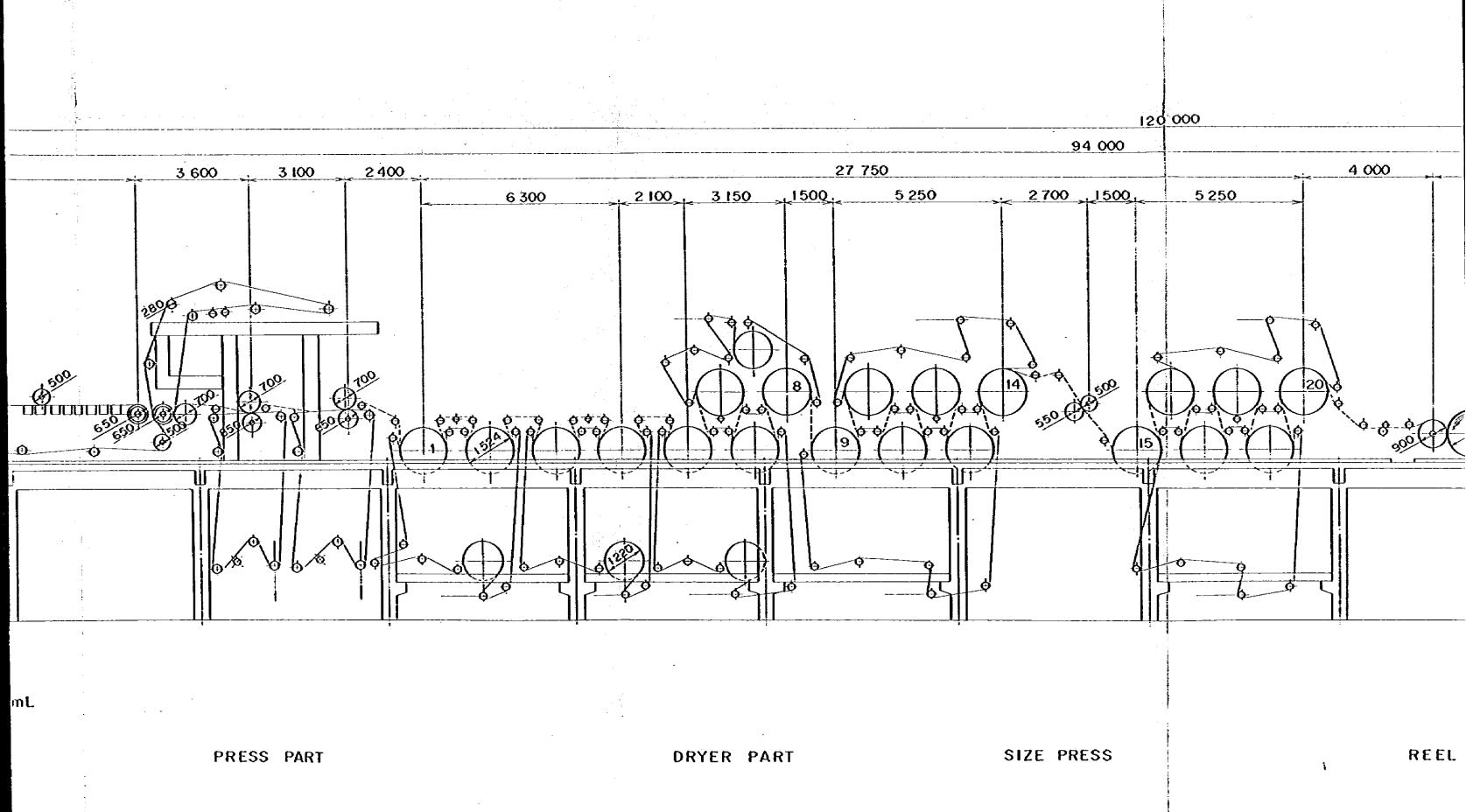


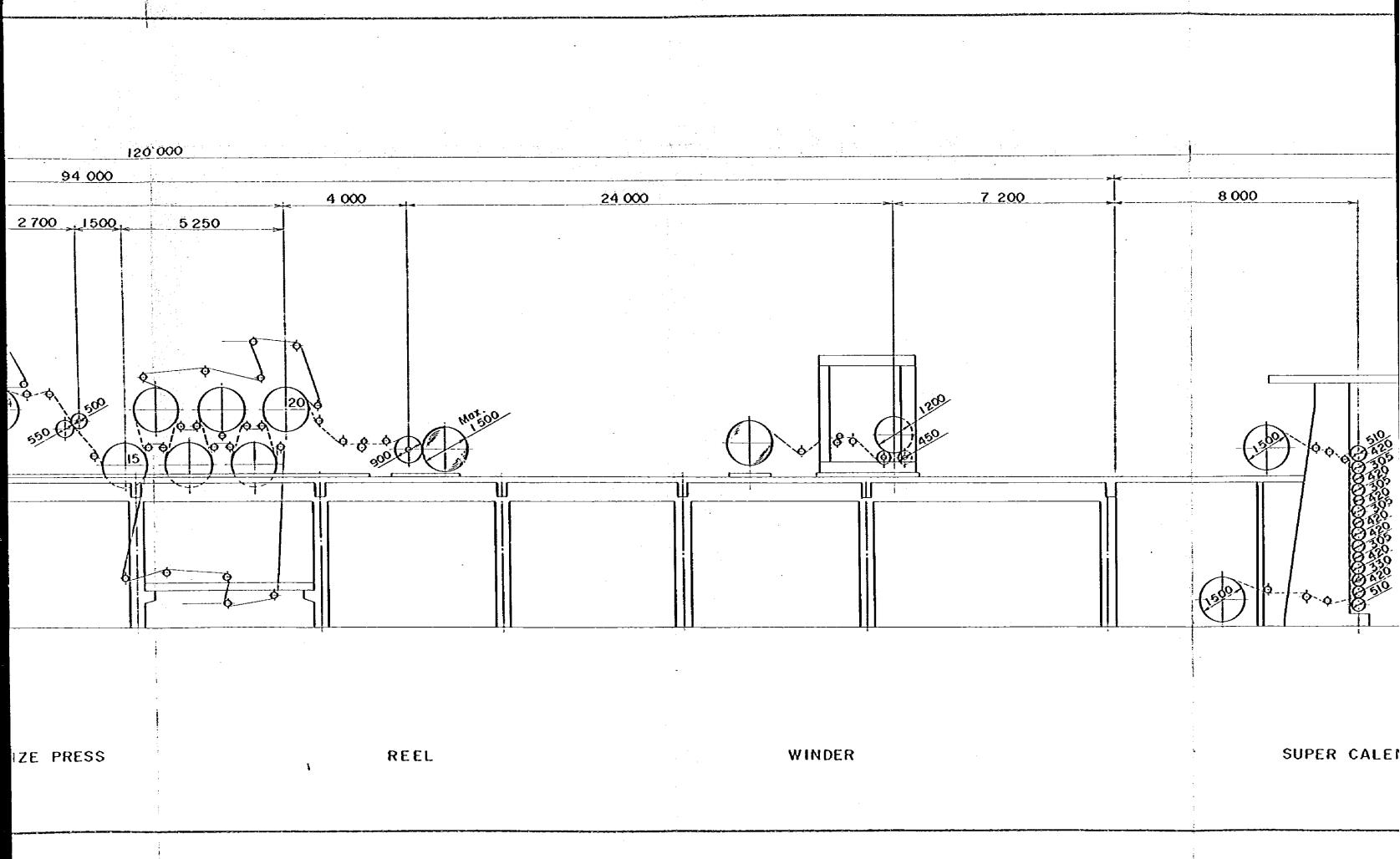


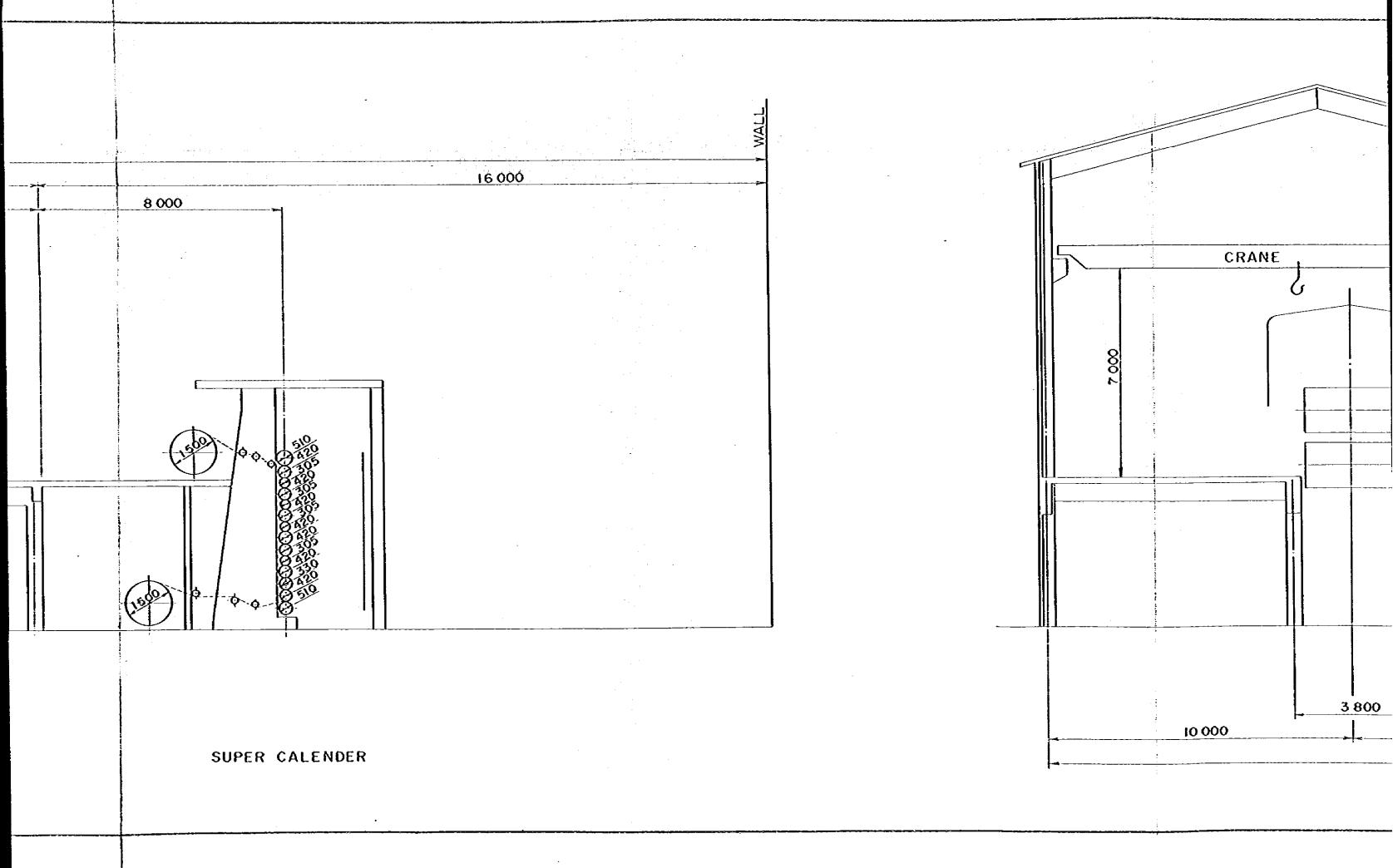


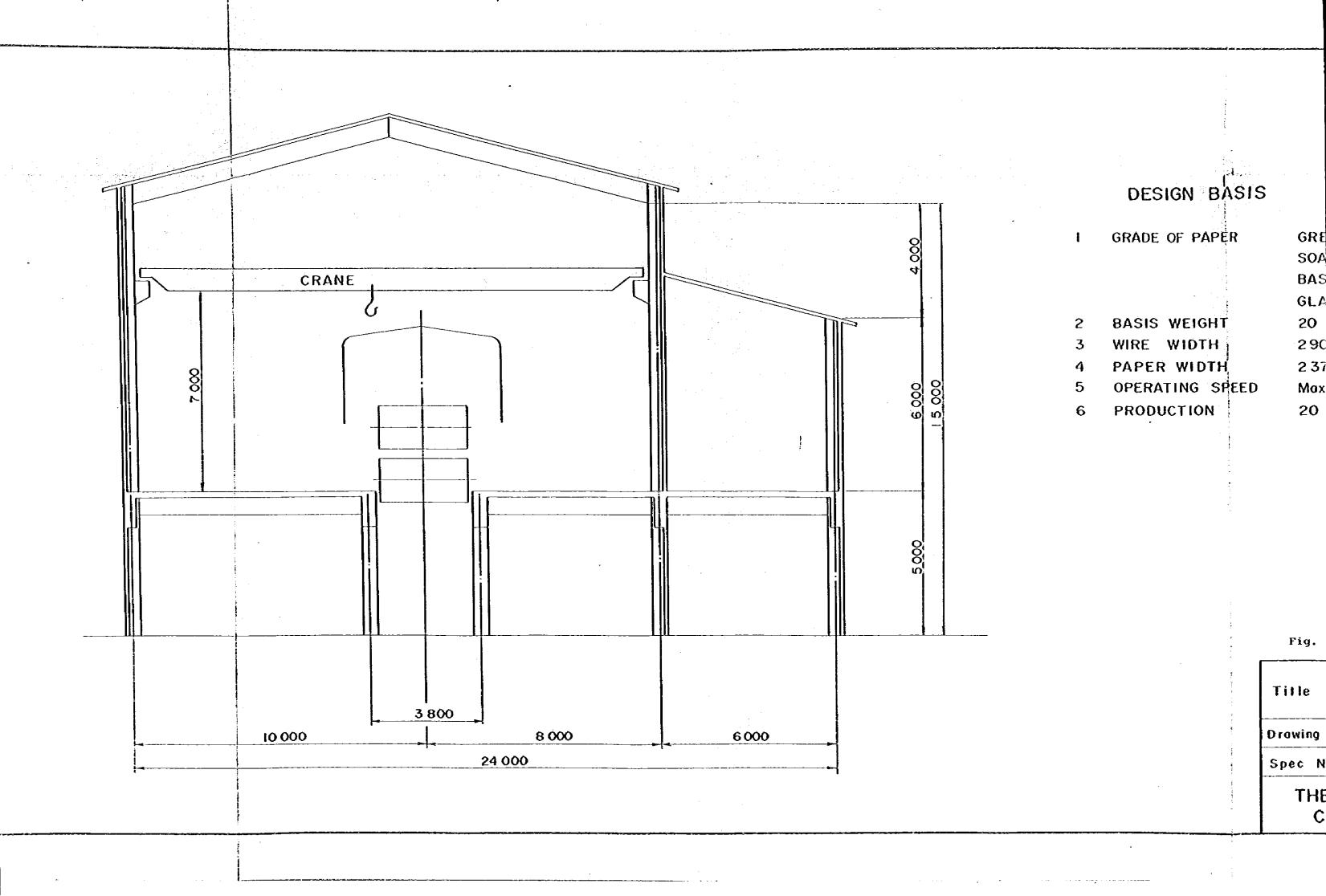


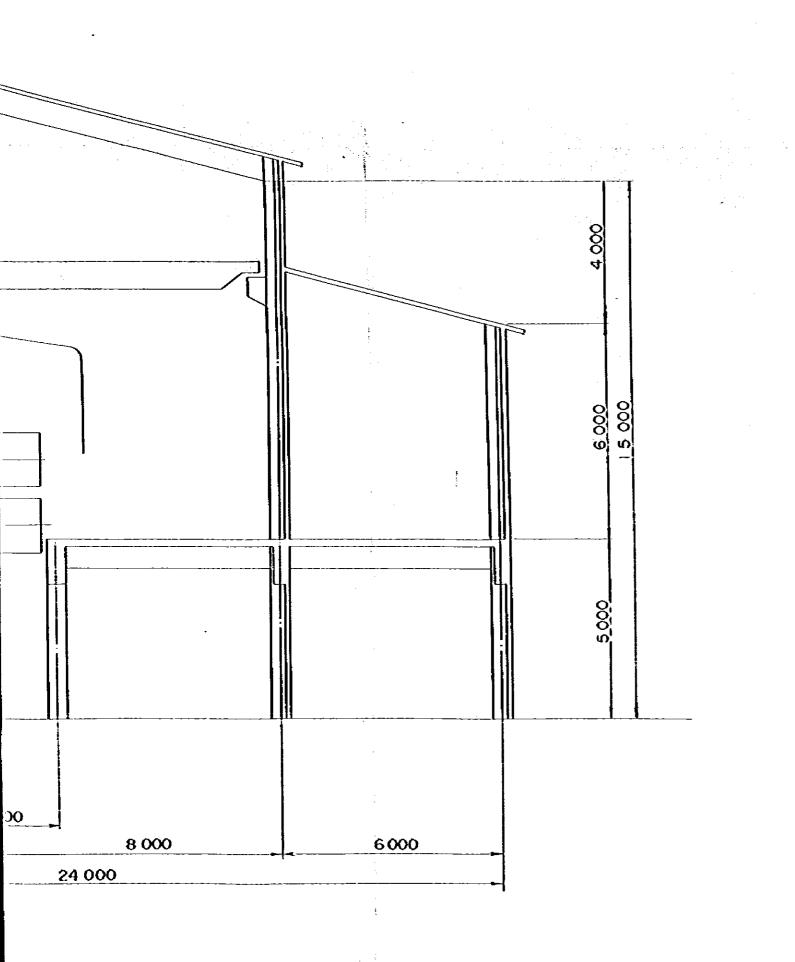












## DESIGN BÄSIS

i	GRADE OF PAPER	GREASED PROOF
		SOAP WRAPPER .
		BASE PAPER OF LAMINAT
		GLASSINE PAPER
2	BASIS WEIGHT	20 - 80 <sup>9</sup> /m <sup>2</sup>
3	WIRE WIDTH	2 900 mm
4	PAPER WIDTH	2 370 mm on reel
5	OPERATING SPEED	Max. 300 m/min
6	PRODUCTION	20 T/D

Fig. 4-8-1

Tiala	NO.2 PAPER MACHINE EXPANSION FOR BRPP CORPORATION			
Title	20 TO THIN PAPER MACHINE			
Drawing	No.	SC Size	1 / 100	
Spec N	ło.	Drawing Da	ote	
		N INTERNATIONA ATION AGENCY	AL TOKYO	

