#### Chapter 7 Improvement and Development of Training Activities

On the basis of the discussions developed in the previous Part III concerning the training activities of the Centre, major recommendations are enumerated below for further improvement and development of the Centre's training activities. Besides, increased opportunities for the assistance of foreign consultants and experts, and the training of the Centre's teaching staff, are also recommendable.

This Chapter also presents at its end a proposal on the contents of the new courses for inspection and maintenance supposed to be commenced/offered by the Centre in the near future.

- (1) It is recommendable that the syllabus for the regular and short courses be successively revised through "Aims and Objectives" technique. For this purpose, it is necessary to grasp job and duty of corresponding course level. Further collaboration with the clients will make it possible to grasp clearly the job analysis and job description.
- (2) It is recommendable to prepare successively curriculum and programme during the "industrial training" period (in the companies and institutions from which the students/trainees are dispatched to the Centre) within the frame of the present sandwich system. A close cooperation with the clients is also needed for this purpose.
- (3) The implementation and development of the above item (1) and (2) is not necessarily easy, especially in a short term. Therefore, assistance of consultants and experts specializing in the field of training development would be necessary and useful. In this respect, dispatch of experts or consulting firm staff in a long term under the technical and financial assistance from specialized agencies in the world would be considered as one of the realistic measures.
- (4) As for the teaching/learning method, it is desirable that students/trainees be involved as more in depth in lessons (as more student-oriented) as possible. It is recommended to utilize more overhead projectors and slides by arranging in advance teaching materials such as figures, tables illustrations, etc. It is

also recommendable to arrange training programme by means of video-system. For this purpose, the video-editing/compilation system would become useful. In order to prepare videotape teaching materials, considerable experience and skill is required. Therefore, training of teaching staff members who would take care of this is also important. It is desirable that both dispatch of experts from equipment manufacturers to the Centre and training of the Centre's staff in the equipment manufacturers would be desired.

- (5) In the training practice in the laboratories, it is desirable not only to give all the necessary instructions in advance to the students/trainees but also to adopt a method of training practice in which the students/trainees have to think, assemble and investigate themselves. By means of this, they would be able to be educated/trained to develop potential ability to use the already acquired knowledge in the solution of practical problems in the near futrue.
- (6) It is recommendable that the training of the teaching staff for increasing their capability be kept up continuously and with more frequent opportunities so far as possible. It is especially important to keep up with the progress in modern technologies and also to master industrial minds.
- (7) It is also desired that great attention be given to maintenance of the laboratory equipment and workshop machine. As for newly introduced equipment/machine to the Centre, it is recommendable to make maintenance contract with equipment/machine manufacturers and suppliers.
- (8) It is desired that the existing library be more fully prepared, especially taking into account the development of the Cepu Oil and Gas Training Centre as a regional centre in the future. A complete list of technical books, magazines and other publications potentially needed for the Centre should also be prepared by fields of specialization.
- (9) In the present day of Indonesia that the oil and gas industry is being steadily developed, the major problem from now can be considered as how to execute effectively and efficiently maintenance of process facilities and equipment.

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In order to solve this problem and to satisfy the needs, it is highly desired that the Centre establish and offer a training course for inspection and diagnosis of facilities and equipment, and a training course for maintenance technology and practice. In addition to these subjects, it is realized that material science and energy management discipline are also needed by the Centre for further development of the Centre's training activities. For this reason, presented below is a proposal for contents of these new training courses. Both courses are expected to exceed 600 hours of training, and therefore, could be implemented as short courses ranging from 4 months to 6 months. Would-be students/trainees are requested to participate in both courses so far as possible.

#### Non-destructive Inspection Course

This new course may be arranged to have the following training subjects and instruction hours.

		Recomme	ended
	Training Subject	Instruction	Hours
a)	Radiographic Testing Method		
	- Introduction	12	
	- Physical Principles	30	
	- Radiation Source	18	an de la composition de la composition Composition de la composition de la comp
	- Radiation Detection	18	e e e e
	- Personnel Safety and Radiation	18	the second second
	Protection		
	- The Radiographic Process	48	a garagan
	- Test Result Interpretation	40	•
	- Practice	30	
	Sub-Total	214	hours

### b) Ultrasonic Testing Method

이렇게 물건을 가지 않는 것을 하는 것을 가지 않았다. 그는 말에서 가지 않는 것이 가지 않는 것이 하는 것이 없다.	
- Fundamental Properties of Sound	10
- Principles of Wave Propagation	15
- Generation of Ultrasonic Waves	15
- Ultrasonic Testing Methods	15
- Ultrasonic Testing Equipment	5
- Operation of Specific Equipment	20
- Specific Testing Procedures	35
- Variables Affecting Test Results	20
- Practice	35
Sub-Total	170 hours

#### c) Magnetic Particle Testing Method

3 - Principles of Magnets and Magnetic Fields - Characteristics of Magnetic Fields 3 6 - Effect of Discontinuities on Materials 6 - Magnetization by Means of Electric Current - Selecting the Proper Method of 6 Magnetization 3 - Inspection Materials 3 - Principles of Demagnetization 6 - Magnetic Particle Test Equipment - Types of Discontinuities Located by 3 Magnetic Particle Testing 12 - Magnetic Particle Test Indications and Interpretation 15 - Practice Sub-Total 66 hours

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## d) Liquid Penetrant Testing Method

	ن کې	× .		
-	Int	rodu	ictio	ſ
			1 Q V X Q I	

- Liquid Penetrant Processing

- Selection of Penetrant Test Method

- Liquid Penetrant Test Equipment

- Liquid Penetrant Indications

- Inspection Procedures and Standards

- Practice

# Sub-Total

## e) Eddy Current Testing Method

- Introduction	3		
- Theory of Eddy Current Testing	5	t the	
- Type of Sensitivity Element	. 199. <sup>1</sup> 19 <b>7</b>	·	•
- Element Affected by Coil Impedance	7		
- S/N Ratio	4		
- Selection of Frequency	4		
- Coupler	6		
- Magnetic Field Strength and it's selection	6		• • •
- Consideration of Equipment	6	•	
- Reading Device	.6		
- Application	8	n de la composition de la comp	
- Standard and Operating Procedure	15	in dij	ta sa
- Practice	35	· : .	
Sub-Total	112	hours	
and the second			

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6

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6

15

49 hours

#### f) Condition Monitering Method

- Introduction for each Equipment	a - 1 - 1 - 1 - 6 - 1 - 1 - 1 - 1 - 1 - 1
- Handling of each Monitering Equipmen	(1, 1, 2, 2, 3, 8, 4) is a constant
- Interpretation of monitering Data	<b>16</b>
- Inspection and Maintenance of Rotatin	${f g}$ , define the set ${f 8}_{ab}$ , ${f d}_{ab}$ , define the set
Machine	anny godin i Changadaan ar
Sub-Total	38 hours

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# g) Other Testing Method

- Introduction (for each testing)	3
- Theory (for each testing)	3
- Characteristic and Selection of eac	eh 4
Testing	
- Operating Procedure	5
- Standard and Interpretation	5
- Practice	10
Sub-Total	30 hours
Grand Total:	679 hours

Note: The instruction hours are estimated assuming that the students/trainees have already basic technical knowledge equivalent to that of high school graduates.

# Maintenance Course

	Training Subject			ended Hours
a)	Introduction	· .		
	- Material Science		25	· .
	- Energ Management		10	· · · ·
	Sub-Total		35	hours
b)	Maintenance Scheduling			
	- Training of Critical Pass Method		30	
	- Daily Maintenance Scheduling	· . • .	10	
	- Shut Down Maintenance Scheduling	· ·	· .	
	. Grasp of work details		10	
	. Estimation of standard man-power	· ·	30	n an an agus an Tartainn an a
	. Planning of schedule		50	
	Sub-Total		130	hours

# c) Preventive Maintenance

- Estimation of Corrosion Rate		15	·
- Estimation of Life	· · · · · · · · · · · · · · · · · · ·	15	
Sub-Total		30	hours
) Maintenance of General Equipment			
- Towers and Vessels	· · ·	15	
- Reactor	· ·	15	
- Heat Exchangers		30	
- Furnaces		20	
- Pumps	. •	50	
- Compressor	· · ·	50	•
- Fire Extinguisher		15	•
- Pipings	- - -	20	
- Wirings		10	
Sub-Total		225	hours
Maintenance of Special Equipment	·		
- Instruments		50	
- Diesel Engines	· · ·	: 50	
- Generator		50	
- Boiler		30	
- Electrical Motor		10	
- Electrical Facilities		15	•
- Water Treater		20	
- Cooling Tower		5	
- Oil Separator	· · · · · · · · · · · · · · · · · · ·	5	
Sub-Total		235	hours
Grand Total:	<u></u>	655	hours

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# PART V

# FUNDS REQUIREMENTS AND EVALUATION

OF RENOVATIONS PLANS

## Part V FUNDS REQUIREMENTS AND EVALUATION OF RENOVATION PLANS

#### Chapter 1 Estimation of Required Funds for Renovation Plans

#### 1.1 Refinery (Atmospheric Distillation Unit)

Required funds have been estimated for each of the three alternative renovation plans for the refinery (atmospheric distillation unit) of the Centre as proposed in chapter 2 of the previous Part IV. The results of estimation is indicated all together in Table V-1-1. Total required funds are estimated as follows:

	(Express	ed in milli	on Yen)
Alternative Plans	Foreign Portion Rp.	Portion	<u>Total</u>
Plan-I (New Installation)	1,073.7	302.2	1,375.9
Plan-II (Partial Renewal)		· · · ·	
Plan-II(A):	870.2	272.9	1,143.1
Plan-II(B):	979.0	322.3	1,301.3

It is observed that in the cases of the partial renewal of the existing refinery (atmospheric unit), no significant saving in funds requirements can be expected as compared to the complete renewal, and that, as a result, there is not much difference between Plan-II and Plan-I in terms of the amount of required funds. This is principally attributable to the following reasons:

- (1) In any case, major equipment of the existing atmospheric distillation unit has to be renewed.
- (2) In case of the partial renewal (Plan-II(A) and Plan-II(B)), FOB equipment/materials cost and other related cost are expected to become less expensive than those of the new installation (complete renewal), while, on the other hand, the field erection cost which includes cost for removal of the existing equipment, becomes considerably higher.

ESTIMATED FUNDS REQUIREMENTS FOR THE RENOVATION OF REFINERY (ATMOSPHERIC DISTILLATION UNIT)

(Unit in million Yen)

lable V-1-1

(18.1) 1, 301.3 1, 301.3 55.6 ( 5.2) 172.8 123.6 0.88 132.6 44.9 1,072.9 239.7 26.0 683.8 418.1 Total ന (16.7) 5.8) 322.3 322.3 15.2 44.0 26.0 263.1 8.3 14.7 19.0 Rp Portion 195.1 221.1 Ħ P [ A H -(15.9) ( 5.0) 979.0 128.8 979.0 44.6 36.6 108.9 69.0 132.6 809.8 40.4 418.1 462.7 Portion Foreign (54) (16.1) 151 8 50.7 940.6 366.3 196.4 22.0 115.8 84.3 1, 143, 1 1,143.1 38.7 117.1 584.7 Total (16, 8) (2.9) 272.9 272.9 37.2 22.0 14. 7 160.0 182.0 7.2 14.2 17.6 Rp Portion Ħ 221 PLAN-(2:0) (15.9) 101.6 719.6 36.0 114.6 870.2 870.2 366.3 36.4 31.5 66.7 402.7 117.1 Portion Foreign 5.4) (15.7) 1, 375.9 61.6 82.0 1, 135.9 178.4 1, 375. 9 512.9 155.2 81.0 117.3 47.4 140.1 749.1 Totaj (16.9) (0.2) 302.2 243.9 41.2 302.2 123.0 81.0 204.0 14.2 17.6 17.1 Rp Portion <del>8</del>.7 1 P.L A N (15.4) 5.0) 44.5 1,073.7 1,073.7 512.9 32.2 39.3 64.4 140.6 892.0 137.2 103.1 Portion 545.1 Foreign (1) Equipment/Materials & Spareparts B. Transportion & Insurance Sase Project Cost (BPC) F. Physical contingency D. Supervising service E. Engineering service G. Price contingency A. Plant Direct Cost (in Jan. 1986 prices) (in Jan. 1989 prices) Total Project Cost C. Project expense (2) Erection work Erected Plant Cost (% of BPC)(5.0) Civil work Sub Total (% of BPC) ଡ

(3) Due to the complicated, troublesome work expected for the partial renewal, such expenses as for supervision, project expense and engineering fees, other than equipment/materials cost and field construction cost, do not have special elements which would make the partial renewal of renovation considerably inexpensive.

Summarized below are the basis and assumptions for the estimation of required funds for the implementation of renovation plans.

- (1) FOB Equipment/Materials
  - a) Plan-I (New Installation)

All the equipment and materials stipulated in the equipment list and flow sheet presented in Section 2.2 of Chapter 2, Part IV are included, and assumed to be imported from Japan.

- b) Plan-II (Partial Renewal)
  - Including equipment listed in Section 2.3 and 2.4 of Chapter-2, Part IV, pipings, electricals, instruments and insulations, etc. needed for the partial renewal. All equipment and materials are assumed to be imported from Japan.

(2) Spareparts

It is assumed that, as necessary spareparts after the renovation, a 10% on the FOB equipment/materials cost is included for each case assuming the import from Japan. Chemicals and lubricants are not included in this estimate by assuming that they are already available in the Centre.

(3) Erection work

A big crane is needed for the removal of old/superannuated equipment and installation of new equipment. In this estimate, it is assumed by, taking into account local conditions, that it will be hired from Singapore on a rental basis. The field erection will be done relatively easily, because the atmospheric unit is neither of a facility operated at high temperature and pressure, nor made of special alloy. It is assumed that an Indonesian contractor will take care of the erection under the supervision of foreign experts.

#### (4) Civil work

It is assumed that all civil materials such as concrete pile, cement, sand, gravel, and steel bar and frame, are made available in Indonesia, and that the work will be done by an Indonesian contractor under the supervision of foreign experts.

#### (5) Transportation and insurance

Costs for Ocean transportation with marine insurance, from Japan to Surabaya, and for local handling which includes unloading in the port and inland transportation are estimated based on freight-ton of imported equipment and materials.

#### (6) Project expense

This expense consists of those costs for trips, communication, printings, books, use of computer required for the project execution in the prime contractor's home office and field office, in addition to those costs required for the temporary work, erection insurance, export insurance, insurance for third parties, etc.

#### (7) Supervising service

This includes all the fees and expenses such as trips, transportation, daily subsistence, insurance, etc. needed for supervising local construction work by foreign experts.

(8) Engineering fee

The following services are included:

- a) Basic engineering
- b) Detail engineering
- c) Preparation of engineering standards for specified jobs
- d) Procurement services of equipment and materials
- e) Transportation services of equipment and materials
- f) Preparation of manuals, etc.

(9) Physical contingency

This cost provides for unforeseen increase of the required funds which could be caused by change of the conceptual design and unexpected factors which were not grasped precisely during the field survey in Indonesia.

(10) Price contingency

This makes provision for future price escalation of goods and services. The following escalation rates are assumed from October 1985 when the estimation is made, to the mechanical completion and start-up of the atmospheric distillation unit.

1986:	4%
1987:	5%
1988:	6%

1.2 Workshop Machine, Laboratory Equipment, and Tools for Inspection and Maintenance

Funds requirements for the implementation of the renovation plans as proposed in the previous Part IV for the workshop machine, laboratory equipment, and equipment for inspection and maintenance have been estimated and presented in Table V-1-2. Total required funds for each of the above categories are summarized below:

	(Exp	ressed in milli	on Yen
	Foreign		
	Portion	Rp. Portion	Total
Workshop Machine	н М		
Alternative Plan-I:	103.6	0.8	104.4
Alternative Plan-II:	437.4	2.8	440.2
Laboratory Equipment <sup>*</sup> :	297.7	0.3	298.0
Inspection Tool:	101.6	0.2	101.8
Maintenance Tool:	62.9	0.2	63.1
rotal			
in case of alternative Plan-I		n de la composition de la comp	
of workshop machine:	565.8	1.5	567.3
in case of alternative Plan-II			
of workshop machine:	899.6	3.5	903.1

\* Including Training Aids for AKAMIGAS

These estimates for the required funds are made based on the same basis and assumptions applied to those for the refinery.

REQUIRED FUNDS FOR RENOVATION OF HORKSHOP MACHINE, LABORATORY EQUIPMENT, Table V - 1 - 2

Maintenance (Unit in Million Yen) 54.6 °? • 3.0 .0 0.2 54.8 63.1 50.7 T 00 | Inspection 101.8 82.6 87.9 13.9 87.7 0.2 ŝ 1001 Laborototy Equipment 0.3 298.0 257.3 40.7 257.0 AND EQUIPMENT FOR INSPECTION AND MAINTENANCE Alternalive-II Work shop Machine 377.2 2.8 380.0 60.2 440.2 Alternalive-I Work shop Machine 90.214.2 104.4 89.4 0.8 Total Cost (in Jan. 1989 price) Base Cost (in Jan. 1986 price) Inland transportation Freight & Insurance Price contingency ΞIΟ f 0 8

# Chapter 2 Evaluation and Comparative Advantage of Alternative Renovation Plans

In Part IV and in Chapter 1 of Part V, the renovation plans for the refinery (atmospheric distillation unit), laboratories, workshop, and equipment for inspection and maintenance have been formulated and analysed, resulting in the estimation of required funds for each renovation plan. This chapter discusses evaluation and comparative advantage of the renovation plans.

#### 2.1 Refinery (Atmospheric Distillation Unit)

On the basis of the results of inspection and disgnosis described in Part II and Part III, the three alternative renovation plans have already been formulated. For further clarification of the problem, the following chart is given to systematically indicate several options to be taken, and a flow reaching to, and relative positions of, these options. Inspection and Diagnosis of the Existing Refinery (Atmospheric Distillation Unit)

Start

Great Difficulty encountered in further utilization of the Existing Unit without major rehabilitation, especially for safety reasons.

INSPECTION AND DIAGNOSIS

JUDGEMENT

Permanent Shutdown and Scrapping

Renovation

New Installation of Atmospheric Unit (Complete Renewal) Partial Renewal

COUNTERMEASURES

Plan-II(B) Plan-II(A)

CONCLUSION

Plan-I

The size (2,000 BPSD) of the existing atmospheric unit and of the proposed new installation is extremely small as compared to the economical scale of modern new refineries that is usually considered as around 100,000 to 200,000 BPSD. It is therefore quite obvious that any renovation plans which include a complete renewal/new installation, can not be justified at all from commercial point of view, in other words, based on financial analysis applied to an ordinary industrial feasibility study $\frac{1}{}$ .

If the investment costs required for the construction of 2,000 BPSD and 100,000 BPSD capacity atmospheric units are assumed to be  $I_1$  and  $I_2$  respectively, the following approximate relation generally exists between  $I_1$  and  $I_2$ .

$$I_1 = I_2(2,000/100,000)^n = I_2(1/50)^n$$

where, n is called scale factor (usually 0.6 to 0.7).

If the investment requirements per unit BPSD of crude oil are expressed as  $i_1$  and  $i_2$  respectively for 2,000 BPSD and 100,000 BPSD atmospheric units, the following equations are then obtained:

 $i_1 = I_1/2,000 = (I_2/2,000) (1/50)^n$  $i_2 = I_2/100,000$ 

Consequently, the investment cost ratio per unit BPSD between the two different capacity of atmospheric units can approximately be expressed as follow:

 $i_1/i_2 = (100,000/2,000) (1/50)^n = (50)^{1-n}$ 

If n is assumed to be equal to 0.65,

$$i_1/i_2 = (50)^{0.35} = 4$$

Note: 1/ Interim Report and Minutes of Meeting, July 1985.

In other words, the investment requirements per unit BPSD of crude oil for 2,000 BPSD atmospheric distillation unit is around 4 times higher than that for a commercial, economic size of modern atmospheric distillation unit having 100,000 BPSD capacity. It is therefore expected that, in case of 2,000 BPSD unit, fixed cost portion of erude oil processing cost will also become 4 times. It is self-evident that such size of atomospheric unit can not be justified from commercial point of view.

It has to be moreover noted that most of the products from the existing refinery of the Centre are not transacted on a commercial basis, but instead are transferred free of charge to PERTAMINA, which is, in turn, paying training fee to the Centre independently of such transfer of products. It has to be also pointed out that there is no applicable pricing system for crude and utilities and that, therefore, no definite basis exists for financial analysis of such small scale unit being operated principally for the training purpose of the Centre.

Therefore, the evaluation and justification of the renovation plans for the refinery (atmospheric distillation unit) has to be made based on intangible factors which, from practical point of view, are not quantified or can not be quantified at a reliable level of preciseness.

Now, as indicated in the previous flow chart, if an option of permanent shutdown and scrap of the existing unit without doing any renovation were to be taken, either one of the following two measures will inevitably have to adopted:

- a) Permanent stop of crude oil production in Cepu.
- b) Transportation of crude oil produced in Cepu to a PERTAMINA's existing refinery or crude oil terminal.

In any case, the on-the job training of AKAMIGAS refining courses could no longer be carried out in the Centre. This would constitute a great obstacle to smooth implementation of these refining courses by the Centre themselves. In addition, despatching students/trainees to PERTAMINA's refineries would cause further increase of expenditure.

There would be additional problems in the supply of wax and batching oil distillate, etc. to local industries in the proximity of Cepu, and also in the availability of home fuel for the Centre.

Moreover, if the crude oil production were to be stopped in Cepu, those training courses related to oil fields, which are considered more important, could not be smoothly implemented either, because the practice and on-the-job training concering oil fields operation could no longer be conducted in Cepu. Again, a large number of students/trainees would have to be despatched to other oil fields Such hypothetical but critical situation mentioned above would in Indonesia. simbolize complete loss of the background and significance of the location/site of Cepu and, therefore, collapse of the fundamental reasons for being of the Cepu Oil and Gas Training Centre that has so far made a growing and remarkable contribution to the development of country's oil and gas industry in terms of It has to be clearly understood that, despite the future education and training. oil production in the proximity of Cepu is projected at as low as 2,000 BPSD even taking into account the application of enhanced recovery programme presently planned by the Centre, the Centre must continue the exploration, drilling, production and exploitation activities of crude oil from educational and training point of view. In other words, the Centre is in a position never to be able to stop oil production, even from the oil fields which have already reached to the end of commercial life.

In case of the above (b), the problems of means and cost of transportation of crude oil from Cepu to PERTAMINA's existing refinery or crude terminal would have to be solved. However, this idea is also unrealistic, because, in actuality, there is no economically suitable and effective transportation method of crude oil to one of the PERTAMINA's refineries and crude terminals, all of which are located remote from the Centre.

It is therefore a logical conclusion that the Centre must continue processing crude oil produced in Cepu regardless of its volume. The option of parmanent shutdown and scrapping of the existing unit would bring to the Centre as a critical influence as one that the foundation of the Centre itself would be undermined. Practically, therefore, this option can never be adopted, for the reason of its extremely great influence. Consequently, the renovation of the existing refinery (atmospheric unit) which includes new installation, should be considered "indispensable option" and "must". Now, the main question in the

subsequent discussions is which alternative renovation plan would be the most suitable and recommendable one for the Centre, that is, which is more suitable, the new installation/ complete renewal or the partial renewal. This choice can easily be made based on the discussions and results so far developed. The followings comparatively summarize major advantages and disadvantages/problems of the three alternative renovation plans for the refinery (atmospheric unit) of the Centre.

(1) Required funds for renovation

There is not much difference in the amount of required funds among the three alternative plans, although the alternatives of the partial renewal require, of course, relatively less funds.

(2) Problems related to shutdown period of the refinery

In case of Plan-I, a new atmospheric unit is installed in the area adjacent to the existing one, while maintaining the existing refinery as it is. Therefore, as far as it is operated with great care for a while until the completion of the new atmospheric unit, no special problem will occur as to the processing of crude oil produced in Cepu during the implementation of the renovation.

이번 실패 승규님에 지난 것 가지? 나라고 예약되었어? 이 나는 것도 가지 않는 것이 것 같아. 나라는 것 같아요.

However, in case of the partial renewal of the existing atmospheric unit (Plan-II), at least one year's stop of the refinery is unavoidable. Therefore, during this period, problems will happen in relation to the crude oil production as to whether it is stopped or continued, in connection with the execution of training programmes, or in relation to the transportation of crude oil from the Centre to PERTAMINA refineries or crude terminals, if the crude production is continued during this period.

Such complicated/troublesome problems should be solved in case of Plan-II(A) or Plan-II(B).

#### (3) Suitability as training facility

In case of the partial renewal, the refinery after its renovation still carrys such problems as lack of control system and instruments for operation data analysis as well as lack of availability of spareparts as pointed out before. Apparently, the new atmospheric distillation unit designed based on the concept described in Part IV is much more superior to the partially renewed existing unit, as a training facility for those who are supposed to work in modern refineries.

#### (4) Energy saving and running cost

The new unit will make it possible to considerably decrease utilities consumption and to increase yield of products as compared to the partial renewal of the existing unit, resulting in a decrease of running cost. It is considered as one of the most important training objectives to bring up trainees who are supposed to work in modern refinery to have energy saving and cost conscious minds. In this respect, the renovation plans based on the partial renewal can not display such training effect.

#### (5) Operation, inspection and maintenance

Checking and open inspection, and maintenance can easily be done in case of the new installation. And this easiness and convenience displays significant training effect. For the purpose to establish and newly offer the training courses for inspection and maintenance as recommended before, this kind of training facility is useful and indispensable. However, in case of the partial renewal, problems of inconvenience for open inspection and maintenance still remain unsolved.

(6) Safety and performance of facility

In case of the new installation, both perfomance guarantee of equipment and guarantee for the total process can be assured. In case of the partial renewal, however, only performance guarantee for unit equipment renewed is obtained. This problem will relate to the problem of safety of the refinery. On the basis of the results and discussions so far made, it is concluded that the renovation of the refinery of the Centre should be implemented by installing a new 2,000 BPSD atmospheric unit in the adjacent area to the existing refinery, while leaving the existing unit either as it is or scrapped after the completion of the new unit.

# 2.2 Workshop Machine, Laboratory Equipment, and Equipment for Inspection and Maintenance

As for the workshop machine, although the two alternitve plans were studied, it is basically desirable to select the greater extent of renovation plan, so far as funds can be made available. However, it is more reasonable that these two alternative plans are not considered as exclusive options, but instead considered as two successive steps of renovation.

It is judged that such machine and equipment as listed before under the renovation plans for the workshop and laboratories should be newly introduced to the Centre as a matter of course if taking into consideration the training need arising from, and situation of, the oil and gas industry surrounding the Centre and also the important roles having been played by the Centre in the Indonesian oil and gas industry.

Chapter 3 Tentative Implementation Schedule

A tentative implementation schedule for renovation of the existing refinery (atmospheric distillation unit) is presented in Figure V-3-1 (Plan-I) and Figure V-3-2 (Plan-II). There is no significant difference between Plan-I and Plan-II.

ITEM	1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 0 13 1 22 23 24 25	
Presentation of Renovation Report		Heleclae Telne
Studies of the report		
chainee		
Bid term of the service		
Order of the service		
Working of the service		
Basic & detailed desian		
Take-off of bill of quantity		
Estimation & booking		
Studies of the service report		
Studies of the fund for the project		
Frederation of the tender of the		
assue of the tencer by Indonesian side		
Bid term of the tender		
Evaluation of the bid by Indonesian side		
Order of the project		
Detailed design		
Procurement of the equipment		
Procurement of the bulk materials		
Transportation		
Civil works		
Installation works		
Piping works		
Electric & instrument works		
Test & flushing works		
Insulation & painting works		
oil in the second		
<b>LEGEND</b>		PLANT PPT MIGAS Cept Tzzining Center
	Cep8	Indonesia

/			Months				
ITEM	1 2 3 4 5 6 7 8 9 10 11 12 13 1	14 15 16 17 18 19 20	21 22 23 24 25	26 2728 29 30 31 3	32 33 34 35 36 37 3	38 39 40 41 42 43 44	4 45 46 47 48
Presentation of Renovation Report							
Studies of the report							
Studies of Engineering Service							
Bid term of the service							
Order of the service							
Working of the service							
fBasic & detailed desion							
Take-off of bill of quantity							
Estimation & booking							
Studies of the service report							
of the fund for the project							
Preparation of the tender of the project by Indonesian Side the							
f the tender by Indonesian side							
term of the tender							
Evaluation of the bid by redensein of do							
Order of the project							
Detailed design							
Procurament of the equipment							
Procurement of the bulk materials							
Transportation							
Removal work							
Installation works							
Piping works							
Electric & instrument works							
Test & flushing works							
Insulation & painting works							
Oil in							
		<u>ਹ</u> ਦ	CUSTOMER (LOCATION)	PPT MICAS	PLANT Cepu	ou Treining Center	
				Cepu Indonesia		к С Н	
					Figure V-	- <b>1</b> -	FROVISIONAL IMPLEMENTATION
				-			

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# PART VI

2. 1948년 - 1948년 1971년 - 1971년 1971년 - 1971년 -

# CONCLUSIONS AND RECOMMENDATION

학교들의 관련을 가 주요?

#### Part VI CONCLUSIONS AND RECOMMENDATION

Based on the results of all the studies and discussions made in the previous parts of the report, the JICA study team concludes and recommends as follows. It is noted that the recommendation presented here has been made in accordance with the basic policy of the Government of Indonesia for further development of the Cepu Oil and Gas Training Centre:

- (1) The Cepu Oil and Gas Training Centre, which belongs to the Directrate General of Oil and Gas, Ministry of Mines and Energy of the Republic of Indonesia, is an important governmental institution for the planning and implementation of educational and training activities in the fields of oil and gas industry.
- (2) The clients of the training activities/courses offered by the Cepu Oil and Gas Training Centre consist of i) PERTAMINA, the national oil company, ii) foreign oil contractors contracting with PERTAMINA and operating in Indonesia, iii) oil and gas related companies, iv) oil and gas related institutions, and v) developing countries. Above all, PERTAMINA is the biggest client among them. In this respect, it is considered that the Centre acts as a servicing institution for PERTAMINA in terms of education and training.
- (3) The core/key role played in the national economy of Indonesia by, and the recent development of, the oil and gas industry has been creating an extensive and intensive training need, both in terms of quantity and quality.
- (4) In order to substantiate such training need raised by the clients and to implement training, it is essential to establish a good reputation as a training institution and to have the clients' confidence. The Centre's training activities and performance have already acquired and are enjoying, a highly reputable confidence from the clients and other relevant organizations. In this sense, therefore, the Centre's foundation for further development of training activities, --- the Centre being an important and indispensable institution within the framework of domestic educational and training system ---, has already been satisfactorily established.

(5) Reflecting such situation, an increasing training need to the Centre is also arising abroad. The growth of the training need from developing countries requires and makes it possible for the Centre to carry out/offer training courses under the TCDC programme and ASEAN-Pacific programme, and forms an appropriate background situation which requires the Centre to act, in its nature, as a regional training centre as well.

Under such circumstance, the Centre is strongly requested by the Government not only to be an indispensable institution under the domestic education/training system, but at the same time to become a regional training centre for the oil and gas industry, especially for ASEAN-Pacific region.

- On the other hand, the existing training facilities and equipment, which (6)constitute hardware of the Centre, are in a quite unsatisfactory and unsufficient condition. The existing refinery (atmospheric distillation unit with nominal capacity of 2,000 BPSD), and most of the workshop machine and laboratory equipment are technologically behind and too old/out-of-date to be properly used more in training practice. Especially, the existing refinery is extremely old (50 - 60 years) and unsuitable for those who are supposed to work in modern refineries. Moreover, it has recently caused fire accidents several times due to the supperannuation of major equipment. longer operation of the existing refinery is no Therefore, further recommendable.
- (7) These problems encountered in the existing facilities and equipment constitute the greatest obstacle to the implementation and development of more effective training activities to play the important role as required above. Apparently, the existing training facilities and equipment of the Centre can not suitably/properly respond to the potential need from the oil and gas industry in Indonesia.
- (8) The renovation plans proposed in this study not only solve such problems of the Centre and to improve its situation, but at the same time, should be considered indispensable and 'must' for the Centre. In other word, without the realization of the proposed renovation plans, not only would the Centre be unable to satisfy the growing need of the clients, but also the Centre

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itself would lose the historical background and foundation of its existence as a training centre.

- (9) As for the renovation of the existing refinery (atmospheric distillation unit), two alternative renovation plans have been studied; total renewal (new installation) and pertial renewal. In view of such essential factors as required funds for renovation, problems related to shut-down period of the refinery, suitability as training-facility, energy saving and running cost, easiness of inspection and maintenance, and safety and performance of facility, it is concluded and recommended that the renovation of the refinery of the Centre should be implemented by installing a new 2,000 BPSD atmospheric distillation unit in the adjacent area of the existing refinery.
- (10) As for the curriculum and syllabus of the Centre, detailed diagnosis and recommendations for further improvement and development are made under the assistance of UNDP. Especially, the development of curriculum and programme for the on-the-job training conducted in the clients' companies, which characterizes the present sandwich system of training, is very essential. Naturally, educational/training effects are influenced by various factors. Above all, however, they depend, to the greatest extent, upon the teaching staff's nature and capacity. In this respect, the present efforts being made for the trainers' training should be continued.
- (11) The amount of funds required for the implementation of the proposed renovation plans is estimated at 1,376 million yens (of which the foreign portion is 1,074 million) for the refinery (atmospheric distillation unit) and at 903 million yens (of which the foreign portion is 900 million) for the workshop machine, laboratory equipment, and equipment for inspection and maintenance. Therefore, the total equirements amount to 2,279 million yens, of which the foreign exchange portion is estimated at 1,974 million.
- (12) Not as in the case for ordinary renovation of commercial plants, the proposed renovation of those facilities and equipment of the Centre is totally incapable of generating cash. Under the present budgeting and financial management system of the Centre, it is absolutely impossible to

newly create any funds necessary for the realization of renovation by its own hands based on the Centre's financial operation, or to generate any available cash used for repayment of loan after the realization of the renovation (in case that the renovation is implemented based on loan). In any case, regardless of whatever the possible financial sources are, it is an essential and indispensable condition that such funds for renovation should not constitute any burden to the Centre.

(13) Recognizing the importance and significance of long-term role and responsibility of the Centre in connection with the overwhelmingly dominant position of the oil and gas industry in the framework of the national economy of the country, it is highly desired that the proposed renovation plans which have proved to contribute to the significant increase of the training effectiveness of the Cepu Oil and Gas Training Centre, be urgently implemented.

# ANNEX

- 18<sup>5</sup>

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ANNEX I

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# Annex I-1-1

# Scope of Work for the Study

on

the Renovation of Cepu Training Center (CTA-159) in

the Republic of Indonesia

agreed upon between

the Directorate General of Oil and Gas

Ministry of Mining and Energy

and

the Japan International Cooperation Agency

Jakarta, March 6, 1985

Keiichi TAKEDA Leader of Japanese Survey Team JICA Ir. MUCHTISAR DAENG PUTRA Director of Cepu Oil & Gas Training Centre

#### INTRODUCTION

Ι.

In response of the request of the Government of the Republic of Indonesia, the Government of Japan has decided to conduct a study on the Renovation (hereinafter referred to as "the Study") of Cepu Training Center, "PPT MIGAS" (hereinafter referred to as "CTC") in accordance with the laws and regulations in force in Japan.

The Japan International Cooperation Agency (hereinafter referred to as "JICA"), the official agency responsible for the implementation of the technical cooperation programs of the Government of Japan, will undertake the Study, in close cooperation with the authorities concerned of the Government of the Republic of Indonesia.

The Directorate General of Oil and Gas, Ministry of Mining and Energy (hereinafter referred to as "DGOG") shall act as a counterpart agency and also designate CTC as the executing body to the Japanese study team (hereinafter referred to as "the Team") in relation with other governmental and non-governmental organizations concerned for the smooth implementation of the Study. The present documents set forth the scope of work with regard to the Study.

#### II. OBJECTIVE OF THE STUDY

The objective of the Study is to diagnose CTC and to investigate the possibility of their renovation from technical, financial and economic points of view and also from the viewpoint of effectiveness of training in order to contribute to improvement of the ability of CTC as a training center.

### III. SCOPE OF THE STUDY

In order to achieve the above objective, the Study will cover the following items:

1. Policy of the Government of the Republic of Indonesia with respect to the renovation of CTC.

- 2. Diagnosis of management of CTC
  - 2-1 operation of the refinery, training school and associated facilities
  - 2-2 maintenance of the refinery, training school and associated facilities
  - 2-3 process control, quality control, pollution control, safety control and cost control
  - 2-4 training activities
  - 2-5 purchasing practice and inventory control of spare parts
  - 2-6 administration

3. Technical diagnosis of the existing facilities

- 3-1 conditions of the processing, offsite and auxiliary facilities including selected surface production facilities.
  3-2 conditions of the facilities for training for the facilities for training for the machine tools, workshop, warehouse of spare parts and other buildings
- 4. Study on the process
  - 4-1 present process scheme
  - 4-2 crude oils processed
  - 4-3 products quality
  - 4-4 modification of the processing scheme
  - 4-5 offtake by Pertamina of the products in relation to the quantity and quality of the products
  - 4-6 effectiveness of training in relation to the processing scheme

- 5. Study on the training activities
  - 5-1 need of training

5-2 the training curriculums and methods

- 5-3 training equipment
- 6. Formulation of renovation program

6-1 renovation plan

- 6-2 capital requirement
- 6-3 implementation schedule

7. Evaluation

- 7-1 financial analysis
- 7-2 economic evaluation
- 7-3 evaluation of the effectiveness of training
- 8. Conclusion and recommendation

IV. STEPS AND SCHEDULE OF THE STUDY

- 1. Steps
  - Step 1: Preparatory office work in Japan
  - Step 2: Field work in Indonesia
  - Step 3: Home office work in Japan
  - Step 4: Presentation of and Discussion on the Draft Final Report
- 2. Schedule

As shown in Annex

V. REPORTS

JICA will prepare and submit the following reports written in English to the Government of the Republic of Indonesia:

Progress Report at the end of Step 2: 10 copies
 Draft Final Report and its summary within 3.5 (three and a half) months after the commencement of Step 2: 15 copies
 Final Report and its summary within 2 (two) months after the receipt of comments on the Draft Final Report by DGOG 30 copies

### VI. UNDERTAKING OF THE GOVERNMENT OF THE REPUBLIC OF INDONESIA

The Government of the Republic of Indonesia shall accord privileges, immunities and other benefits to the Team and, through the authorities concerned, take the following necessary measures to facilitate the smooth implementation of the Study:

1. The Government of the Republic of Indonesia shall make necessary arrangements with the cooperation of other governmental and non-governmental organizations concerned for the following:

1-1 to secure the safety of the Team

- 1-2 to permit the members of the TEam to enter, leave and sojourn in Indonesia for the duration of their assignment therein, and exempt them from alien registration requirements
- 1-3 to exempt the members of Team from taxes, duties and other charges on requirement, instrument and other materials brought into Indonesia for the implementation of the Study
- 1-4 to exempt the members of the Team from income taxes and other charges of any kinds imposed on or in connection with any emoluments or allowances paid to the members of the Team for their services in connection with the implementation of the Study
- 1-5 to provide the necessary facilities to the Team for the remittance as well as utilities of fund introduced in Indonesia from Japan in connection with the implementation of the Study
- 1-6 to provide medical services as needed and its expenses will be chargeable on the members of the Team
- 1-7 to secure permission to take all data and documents related to the Study (including photographs) out of Indonesia to Japan by the Team
- 2. The Government of the Republic of Indonesia shall, at its own expenses, provide the Team with the following, in cooperation with other agencies concerned, if necessary:

2-1 counterpart personnel

2-2 suitable office spaces with necessary equipment including telephone in Cepu

- 2-3 credentials or identification cards
- 2-4 necessary vehicles with drivers, fuel and spare parts in the projected areas
- 2-5 necessary personnel for the Study

3. The Government of the Republic of Indonesia shall bear claims, if any, which may arise against the membes of the Team resulting from, occurring in the course of, or otherwise connected with the discharge of their duties in implementation of the Study, except when such claims arise from gross negligence or willful misconduct on the part of members of the Team.

VII. UNDERTAKING OF THE GOVERNMENT OF JAPAN

For the implementation of the Study, the Government of Japan will, through JICA, take the following measures:

 To dispatch, at its own expense, the Team to Indonesia
 To pursue technology transfer to the Indonesian counterpart personnel in the course of the Study

VIII. CONSULTATION

JICA and DGOG will consult with each other in respect of any matter that may arise in the interpretation of implementation of the present arrangement.

Tentative Schedule of the Study

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Annex

Year & Month					1985				•	19	1986	
Iten	Мау	June	ζυιγ	Aug.	Sep.	Oct.	Nov.	Dec	Jan.	Feb.	Mar.	Apr.
Preparatory Office Work (Step 1)												
Field Work (Step 2)								· · · · · · · · · · · · · · · · · · ·				
llome Office Work (Step 3)	•••	• •• •• •• •• •• •• •		· · · · · · · · · · · · · · · · · · ·	• • • • • • • • •				••••••••••••••••••••••••••••••••••••••			
Presentation of Draft Final Report (Step 4)	 ti	•						••••				
Submission of Final Report					• • • • •	••••	· · · · · · · · ·		$\triangleleft$			
						•						-

In Indonesia

In Japan

Toyo Engineering Corp. Team Leader Susumu Nakagawa Toyo Engineering Corp. Sub-leader Takashi Uchiyama Cosmo International Corp. Shoji Odagiri Koa Oil Co. Ltd. Hirofumi Tokumoto Minoru Takada Cosmo International Corp. Yoshiaki Nakamura UNICO International Corp. P.I.M-1/ Soichi Sato P.I.M<sup>1</sup>/ Shunsaku Kondo Toyo Engineering Corp. $\frac{2}{}$ Tetsuo Kanamori Mitoshi Higashiuchi Toyo Engineering Corp.<sup>2/</sup>

Note:

1/

For field inspection

2/ For home office work

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# Annex 1-2-2 PPT MIGAS COUNTERPART TEAM MEMBERS

Name	Background	Assigned work
Messers.		
Muchtisar DP	Chemical Engineer	Overaal management and Coordination
Soepanan	Chemical Engineer	Renovation Programme - Product Quality
Koesmartono	Chemical Engineer	Renovation Programme
		management and ad- ministration (CTC).
Parjono	Chemical Engineer	Renovation Programme
Sumaryo	Mechanical Engineer	Management and train+ ing system.
Sakino Ng	Economics	Education and training system
R. Hartojo	Mechanical Engineer	" AKAMIGAS ".
		Training system AKAMIGAS
MD. Hartanto BP. Simandjuntak	Ag- Aldahuc Civil Engineer	Inspection and
		maintenance, Coordi- nation.
		Buildings structur and foundation.
Djoko Purnomo	Instrument Engineer	- Inspection and measuring.
R. SumarsonoBcM	Mechanical Engineer	- Instrumentation Inspection and
		measuring
Wisnu Priyanto BcM	Mechanical Engineer	Work Shop
Sandjojo BE	Mechanical Engineer	Work Shop
Indrawan	Electrical Engineer	- Inspection and
an an tao ao amin' a Amin' amin' amin		measuring - Electrical fa-
and a start of the		silities. - Electrical power fasilities.

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# Zuhdan Fathoni F.X. Suwar Sulistijanto Hermadi S. Mustakim

Name

Asmorowati

#### Sulindrijo

Suparno Winarno BcM Ichsan Muchtar Praseno

#### Sunarhadiyanto

Suparto

Kuskun Purwanto

IP. Lubis

Warimin W.BSc

Jan Pieter

Santosa Suparma Sumadi A. Chemical Engineer Technician Chemical Engineer Industrial Engineer Chemical Engineer

Background

Chemical Engineer Chemical Engineer Chemical Engineer Chemical Engineer Chemical Engineer Chemical Engineer Mechanical Engineer

#### Mechanical Engineer

Technician Technician

Business Administration

Business

Administration

Legal &

Administration Fishery Engineer Linguist

Assigned Work Safety Control Safety Control Pollution Control Pollution Control - Process study, coordination - Simulator - Cut off model Laboratories Library Process study Process study Refinery Operation Refinery Operation Product Quality Technical Disaigns. Pumps, Compressors Well pump and driver Gathering Tank, storage tank. Piping Boiler. Water receiving and distributing facilities Maintenance Maintenance Purchasing, inventory control of sparepart Financial Analysis

Administration

Affiliation Section English Instructor

# ANNEX 11

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### ANNEX II-2-1 FINANCIAL SITUATION OF THE CEPU OIL AND GAS TRAINING CENTRE

The financial situation of the Centre for the fiscal year 1984/1985 is summarized below:

(1) Annual Revenue

Government Budget

Routing Budget: 3,562 Development Budget 855 Sub-Total: 4,417

(Unit in million Rp.)

Non-governmental Sources of Funds

化合物学生 医乳液性外的 化合物化合物 化合物	
Training Fee from PERTAMINA	1,901
Training Fee from Other Companies	
and Institutions:	1,084
Own Sales of Products:	2,294
Other Miscellaneous Income:	241
	un de la composición de la composición En esta en en esta en es
Sub-Total:	5,520
Rest Beginning	1,990
de la presidencia de la contra d La contra de la contr	
Total Annual Revenue:	11,927
Annual Expenditure	
Personnel Expenditure:	2,593
Goods Expenditure:	3,515
Maintenance Expenditure:	962
Itinerary/Office Tour Expenditure:	328
Assets Expenditure:	866
Other Expenditure:	
<u>dener</u> <u>hxpendreure</u>	82

(3) Rest Ending

3,581

For further reference, trends in the financial status of the Centre are indicated in Table Al-1 during the past five fiscal years from 1980/81 to 1984/85.

The sources of operating funds of the Centre can be divided into the government and non-government ones. The government budget consists of the routine budget and development budget (or project budget). The non-government funds consist of training fee from PERTAMINA, training fee from other companies and institutions, the Centre's own sales (such products as gasoline, kerosene, gas oil and fuel oil are transferred to PERTAMINA free of charge, and the remaining products as wax, solvent, batching oil distillate and some residue are directly sold by the Centre to local industries.) and other income such as obtained through the supply of power and water to a part of Cepu town and by the use of the hospital and guest house by people outside of the Centre.

The routine budget is for the following five items of expenditure:

- Personnel expenditure

- Purchasing of goods (including fee for non-regular lecturers of AKAMIGAS)
- Repair and maintenance
- Transportation and daily subsistence for travels of the staff members
  - Others

On the other hand, the development budget is for the following items of expenditure (but tax is excluded from the fiscal year 1984/85:

- Expenditure/fee for project personnel

- Purchase/acquisition of land
- Purchasing of routine materials
- Purchasing of equipment

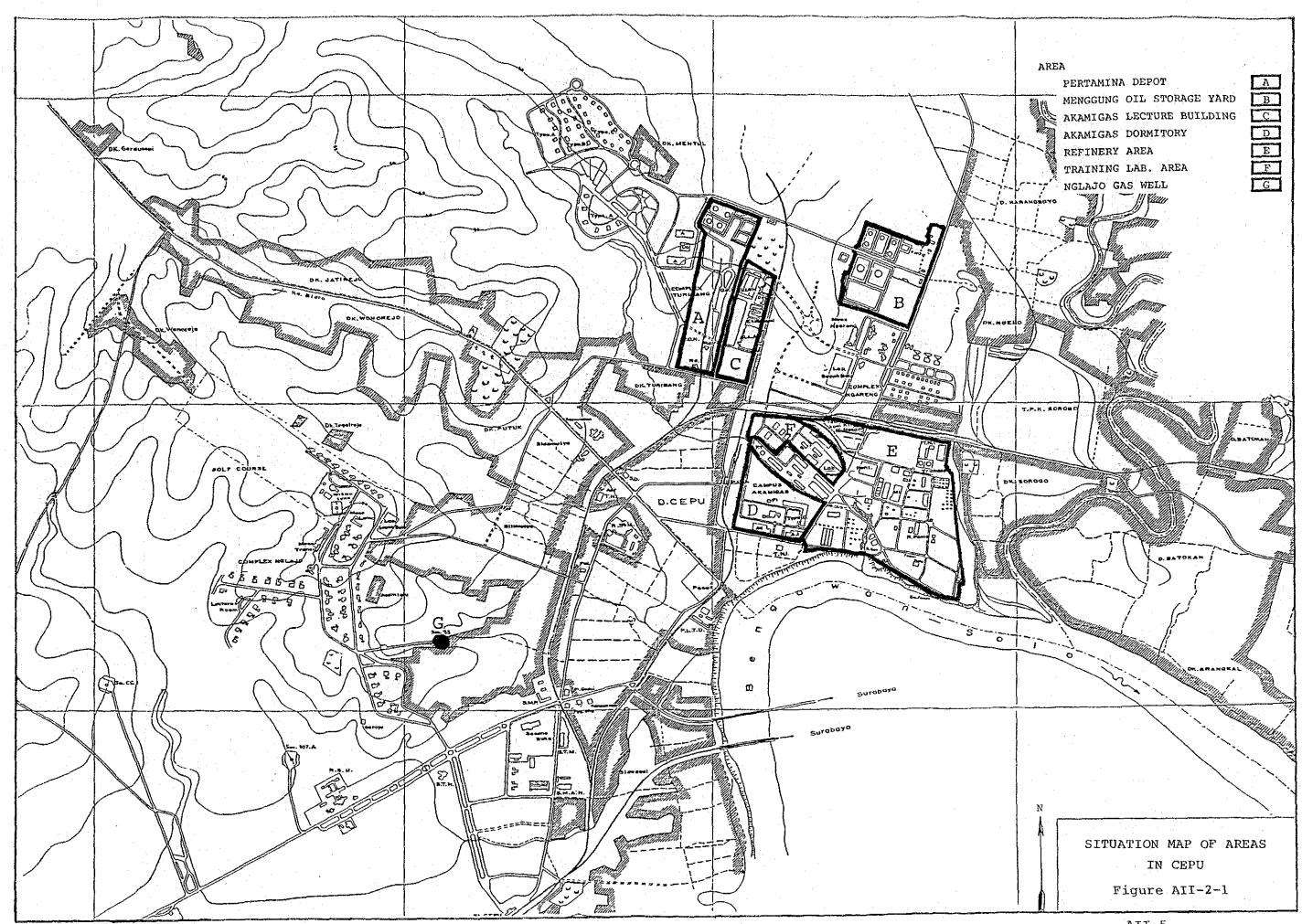
Table AII-1-1 FINANCIAL SITUATION OF CEPU OIL AND GAS TRAINING CENTRE (Fiscal Year 1980 - 1984)

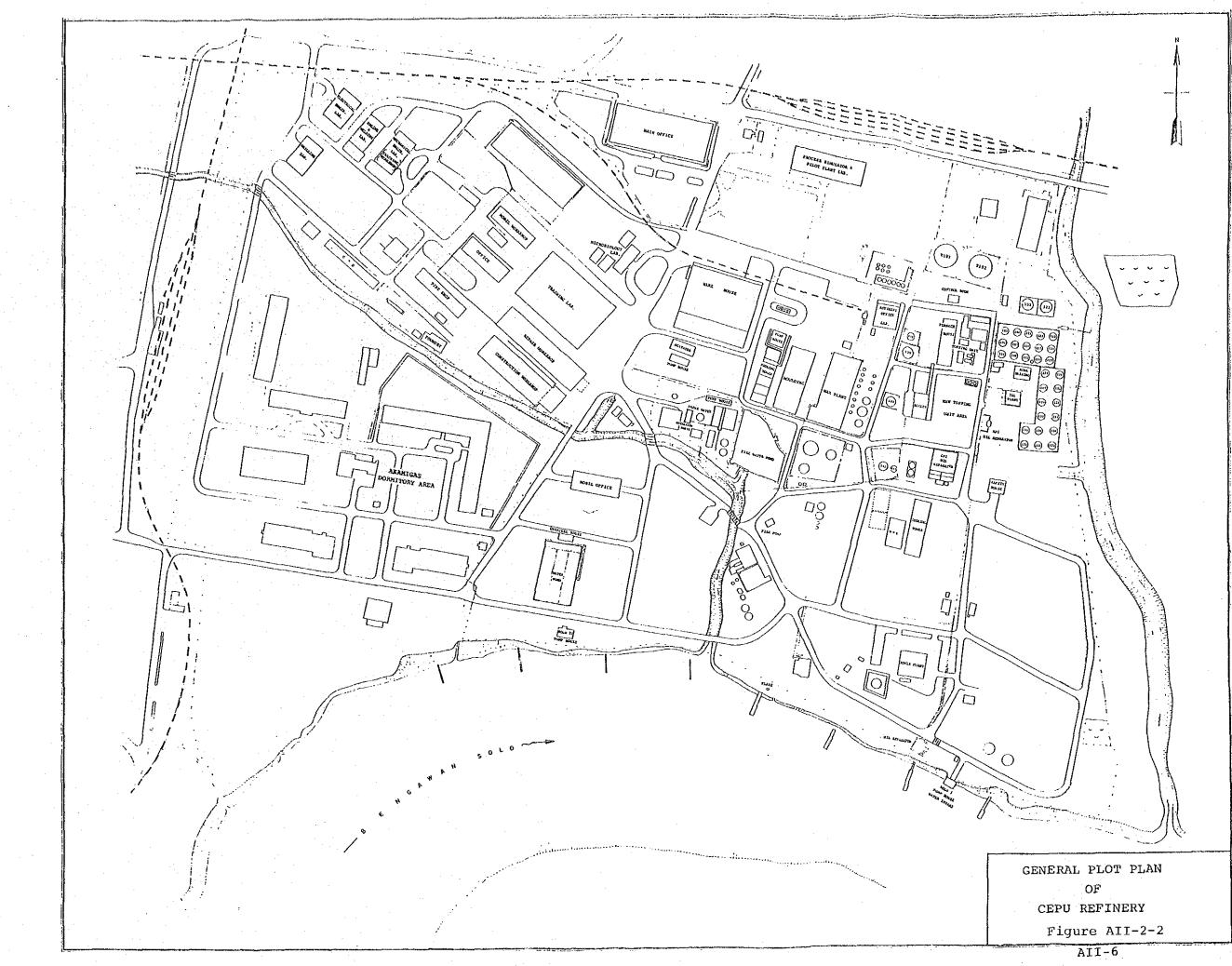
962,241.0 327,568.1 865.640.8 3,581,379.6 82,115.4 8, 345, 359.0 11, 926, 738.6 ,989,978.5 293,606.8 241, 324.9 2,593,251.6 , 562, 459.3 854,660.8 9,936,760.1 3,514,542.1 ,084,056,3 ,900,652.0 1980/81 - 1984/85 1984/1985 MAR. 31 Ì, PERIOD: APR, 1 9,691,495.4 7,701,516.9 3, 138, 631.2 928, 129.5 289, 997.2 1,989,978.5 3, 457, 865.4 1, 134, 863.8 577.8 8,767,917.6 769, 233.0 1,214.6 583, 526, 6 60,899.8 2,574,311.4 883,461.3 1983/1984 ,547,300. YEAR: 923, 5 1,463,257.3 852.6 2,580,023.9 2,903,891.7 784,615.5 317,973.7 8,284,905.0 8,974,192.6 8,050,614.8 923, 577.8 689,287.6 2,868,914.2 ,172,857.8 ,085,552.3 ,565,580.7 ,499,268.4 1982/1983 92, 731. OF CAPITAL GOVERNMENT GOVERNMENTAL BUDGET  $\begin{array}{c} 1.\,911,\,502\,.1\\ 2,\,405,\,162\,.2\\ 705,\,291.7\\ 310,\,492.8 \end{array}$ 149,369.8 78,045.9 694,230.3 2,580,350.3 930,102.6 5,559,864.5 689.287.6 5,554,921.8 6,249,152.1 568, 165.4 613,997.1 800,321.3 61,985.1 1981/1982 CASH FLOW 1,318,451.9 1,539,110.0 521,367.9 213,617.8 2,074,980.8 723,132.6 98,480.7 117,030.7 578, 128, 9 863, 045. 4 54, 305. 0 SOURCE /NON 4,502,289.3 3,808,059.0 694,230.3 208,696.6 4,293,592.7 1980/1981 [tenarery/Office Tour Expen-Maintenance Expenditure Trainning Fee Pertamina FINANCIAL DEPARTMENT Explanation Personal Expenditure 2 -**Frainning Fee Other** Assets Expenditure PPT MIGAS CEPU Goods Expenditure Other Expenditure + Income: Routine Project က 1 0 Rest Beginning Other Income Expenditure: Rest Ending Total Total Own Sales Total diture Number ഹ് ė 4

Note: Unit of Scale = Rp 1,000,-

- Construction
- Tax
- Others

It is understood that the development budget is basically utilized for similar type of expenditure related to projects, with the exception of the formation of fixed assets such as procurement of equipment and land, and construction which represents the major difference from the routine budget.





### RESPONSE TO QUESTIONNAIRE FOR AKAHIGAS GRADUATES' IMMEDIATE SUPERIOR (1) (Number of Respondents: 22) Annex 11-3-1

No.	Question	Answer, Percentag	₹ <del>0</del>	Summary
. 1	Has he enough knowledge on applied science and industrial science to carry out his Job?	Sufficient 40% Good 45%		Considered as sufficient and good.
2	In relation to the above-mentioned question when looked from the point of view of:	1) Sufficient 69% Good 13%	82%	ditto
	<ol> <li>Management</li> <li>Performance</li> <li>His awareness toward budget</li> </ol>	2) Sufficient 56% } Good 31% }	87%	ditto
	and spending policy	3) Sufficient 50% } Good 25% }	75%	ditto
3	Has he enough basic knowledge to carry out his job?	Sufficient 43% Good 48% }	91%	ditto
4	Has he enough general knowledge and leadership to carry out his job?	Sufficient 62% Good 29%	91%	ditto
	Lecture on subjects which are considered as not sufficiently given?	English Principle on Supervision	42% 42%	These 2 subjects are considered as not sufficiently given and expected its development be increased.
6	On the duration of 50 days practical/field work?	Sufficient55%Good19%	74%	Longer duration is needed but not too long.
7	Site of field work?	Other area within own company:	87%	Field work other area within the company is desirable.
8	Ability and Performance in holding preliminary post?	Sufficient 78% } Good 17% }	95%	Considered as able.
9	Matters in which he is not capable to perform well?	Decision making	16% 27%	The matter received much attention.
	n an	Organizing English (language)	14% 19%	
10	Matters which show his incapability?			Minimum response, not valid.

## Annex 11-3-1

#### RESPONSE TO QUESTIONNAIRE FOR AXAMIGAS GRADUATES' IMMEDIATE SUPERIOR (2) (Number of Respondents: 22)

No.	Question	Answer,	Percentage	Summary
11	Act of creativeness?	Sufficient Good	50% } 90% 40% }	Considered as sufficient and good.
12	Working spirit?	Sufficient Good	18% } 95% 77% }	ditto
13	Spirit of endurance?	Sufficient Good	59% } 100% 41% }	ditto
14	Act of decisiveness?	Sufficient Good	82% } 100% 18% }	ditto
15	Communication with superior?	Sufficient Good	46% } 100% 54% }	ditto
16	Communication with colleague?	Sufficient Good	46% } 100% 54% }	ditto
17	Communication with subordinate?	Sufficient Good	50% } 100% 50% }	ditto
18	Ability to analyse?	Şufficient Good	77% } 86% 9% }	Considered as sufficient and good.
19	Act of cooperativeness?	Sufficient Good	36% } 100% 64% }	ditto
20	Sense of responsibility?	Sufficient Good	45% } 100% 55% }	ditto
21	Attitude of flexibility?	Sufficient Good	73% } 100% 27% }	ditto
22	Ability to control suboridinates?	Sufficient Good	68% ) 95% 27% )	ditto
	Ability to take decision after 1-2 years occupying the post?	Sufficient Good	68% } 100% 32% }	ditto
4	Ability to take decision after 2-4 years occupying the post?	Sufficient Good	59% } 100% 41% }	ditto
5	Ability to take decision after 4 years occupying the post?	Sufficient Good	13% ) 95% 82% )	Recognized as good.

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		QUESTIONNAIRE		GRADUATES'	IMMEDIATE	SUPERIOR	(3)
· · · · ·	(Number of	Respondents: 2	(2)				
and the second	· · · · ·						

No.	Question	Answer, Percentage	Summary
26	What medium is suitable to keep alumnus always in touch with latest technological development?	Post AKAMIGAS 18% University 9% Short Course 68%	Short courses are considered as suitable medium.
27	Content of suggestion ever submitted?	Fair         50%         86%           Good         36%         86%	Considered as fair.
28	Sensibility toward environment, its situation and condition?	Fair 73% } 95% Good 22% }	ditto
29	Effort to develop own capability?	Sufficient45%Good36%	Considered as sufficient and good.
30	Level of one's knowledge which will help him to hold higher post?	Sufficient         68%         91%           Good         23%         1	ditto
31	Type of education most suitable for the job in the field?	AKAMIGAS (Oil system) 23% AKAMIGAS (New system) 54%	AKAMIGAS (Sandwich system) is desirable.

Annex II-4-1 RESPONSE TO QUESTIONNAIRE FOR AKAMIGAS GRADUATES (1)

No.	gues tion	lnput	Respondent Percentage	Summary
1	Types of Responder	a. AKAMICAS (Old system) b. AKAMICAS (New system) c. Crash Program Course d. Special Course for Graduates Total	24 23% 40 38% 34 33% 6 62 104 100%	Major responders are AKAMIGAS graduates (New system)
	When latest post held after graduation?	a. 1 year b. 2 years c. 3 years d. 4 years e. 5 years f. 6 years b. 8 years i. 9 years	0000 000 000 000 000 000 000 000 000 0	New post were held between 1 and 2 years after graduation
24	Present rank?	a. Level 4 b. Level 5 c. Level 6 d. Level 6 d. Level 8 f. Level 9 g. Level 10	0 4 19 14 16 21 21 0	Majority are in the lower rank. (Level 9) Note: 1) First graduate came out in 1970. 2) Refer to Manpower pattern of PERTAMINA regarding the rank level.
m .	Relation between studied subject and job	a. Applicable b. Of little use c. Non applicable	83 17 0 0	Applicable is the answer of almost all.
4	Is additional OJT necessary?	a. Necessary b. Not necessary	51 52% 48%	Nearly half answered it is necessary and another half not necessary.
o N	Suggestion on given subjects	<ul> <li>Applied and industrial subjects</li> <li>Basic knowledge subjects</li> <li>General knowledge and</li> <li>leadership subjects</li> </ul>	28 39% 31 43% 13 18%	Contents of subject should be increased. English language lesson should be increased.
9 9	Type of education desired after graduation from AKAMIGAS	a. Post AKAMIGAS (Grade 1V) b. Unlversity c. Other level of education	51 54% 32 34% 12 13%	AKAMIGAS graduates wanted this type of education. Crash program course graduates wanted this type of education. Responders of the 6th rank level group wanted this type of education.
~	Has responder been promoted?	a. Not yet b. Has been promoted	34 34% 66 66%	Responders just graduated within 2 years. Responders graduated more than 3 years ago

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Annex 11-4-1 RESPONSE TO QUESTIONNAIRE FOR AKAMIGAS GRADUATES (2)

	Question	Input	Number of Respondent	Percentage	Sussary
rele sduc	Your present job has any relevancy with your education?	a. Has relevancy b. No relevancy	89 12	88% 12%	In general jobs are relevant to their education:
Handic works?	Handicap faced in day-to-day works?	<ul> <li>a. English language barrier</li> <li>b. Difficulty in working procedure</li> <li>c. No handicap situation</li> </ul>	32 24 27	38% 28% 32%	Responder's most complained handicap. Responder's complained handicap. Responders which belong to 6th rank group.
Han	Handicap in developing own capability?	a. Language (Engligh) barrier b. No guidance c. No opportunity d. No handicap	15 6 28 28 28	18% 7% 33%	Being kept busy by routine work. Some responders give no comments.
ls Jen	Is subject of management beneficial to you?	a. Very helpful b. Quite helpful	30 65	30% 56%	) It is realiy very helpful.
Sug	Suggestion on how to have better education system	a. Should have better curriculum b. Upgrading of instructor's	23 14	28% 17%	Expecting better and upto-date content of subjects.
1.1		c. Betterment of process of education	25	25%	Visit of quest lecturers is independable.
		d. Upgrading of teaching aids e. Upgrading of supporting facilities f. Encouragement on act of discipline	10 4.0	10 10 10 10 10 10 10 10 10 10 10 10 10 1	Expecting upgrading of sports facilities for students activity.

Annex II - 4 - 2 INSTRUMENTATION & ELECTRONICS LABORATORY EQUIPMENT LIST

		No. of	Year of	Present	
VO.	Name of Equipment	Unit	Purchase	Condition	Remarks
1	Panel Educational Process Controller	1 unit	1975	40%	Out-of-use
•	Electronic "EQUIPHENT"				
2	Process Control Training Unit	1 unit	1978	80%	Good
3	Old Type Panel Process Control	1 unit	1974	70%	Good
4	Pneumatic Controller "FOXBORO" H130	2	1975	75%	Good
	Consotrol Controller with Shelves		1975	25%	Broken
5	Pneumatic Controller "FOXBORO" M40	1	1975	75%	Good
	Stabilog Controller				
6	Pneumatic Recorder "FOXBORO" M40	1	1975	25%	Broken
: 1	Type: Diaphragm meter				
7	Pneumatic Recorder "FOXBORO" M124	2	1975	60%	Good
	Type Hultipoint Recorder		1975	40%	Out-of-use
8	Differential Pressure Transmitter,	2	1975	75%	Good
	12A "FOXBORO"				
9	Differential Pressure Transmitter,	1	1975	75%	Good
	13FA "FOXBORO"				lan dagi seri da seri Seri da seri da
10	Pneumatic Transmitter "FOXBORO" H45P	1	1975	75%	Good
11	GEC Elliot Transducer	1	1975	25%	Broken
12	Kent Foster Cambride Potentiometer PP332	1	1976	80%	Good
13	YEW Potentiometer Type 2727	1	1980	80%	Good
14	Dead Weight Tester Budenberg Gauge	1	1970	60%	Usable
15	Ashcroft Portable Dead Weight Tester	1	1980	80%	Good
16	Indicator FOXBORO M5001, Ribbon Type	1	1975	75%	Good
17	Sart Control Valve, Size: 1 1/2"	3	1979	75%	Good
18	Masoneilan Control Valve, Size: 2"	1	1978	75%	Good
19	FOXBORO Control Valve	1	1975	75%	Good
20		10	1975	75%	Good
21	William M. Wilson/sons Flow meter	1	1974	60%	Usable
22	Oscilloscope GOLD Type OS 250 B	8	1975	60%	2 units: usable
				25%	6 units: broken
23	Ocilloscope Philips Type PM 3233 0-10 MHZ	3	1976	70%	Good
24	Demonstration Oscilloscope Leybold	1	1970	40%	Out-of-use
25	Oscilloscope Philips Type PH3110, 0-10 MHZ	1	1972	25%	Broken
26	Oscilloscope Telequipment	1	1968	25%	Broken
27	Oscilloscope TRIO Memory Type	2	1982	90%	Good

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	(a) A state of the state of	No. of	Year of	Present	
No	Name of Equipment	Unit	Purchase	Condition	Remarks
28	Function Generator AC Philips Model PM5167	3	1977	40%	Out-of-use
29	AC Hill-Voltmeter Philips Type PH2454B	3	1977	60%	Good
30	Low Frequency Generator Philips Type PM5106,	. 5	1977	45%	4 units: Out-of-us
	0-10 KHZ				1 unit: broken
31	Generator Signal Sinus Leybold, 0-300 KHZ	1	1968	45%	Out-of-use
32	Dual Type Power Supply 0-30 V, DC	8	1974	50%	Usable
33	Sweep/Function Generator TRIO Model FG271,	3	1974	50%	2 units: usable
	0-2MHZ			25%	1 unit: broken
34	Frequency Counter TRIO Model FC-756	3	1983	80%	Good
35	PAL TV Pattern Generator Type PM5509 Philips	1	1977	75%	Good
	White & Black and Color	e ta			
36	Multimeter Philips Model PH2503	4	1977	25%	3 units: out-of-us
		n an Ng			1 unit: broken
37	Digital Multimeter AlphaII, ADVANCE INSTRUMENT	8	1975	40%	6 units: out-of-us
				25%	2 units: broken
38	SANWA Multimeter Analog Model 501-ZX-TR	6	1980	40%	Out-of-use
39	SANWA Multimeter Analog Model AX-303-TR	2	1980	25%	Broken
40	Phasor Meter J. J.	1	1973	40%	Out-of-use
41	Netravo 3 Multimeter Analog	1	1968	25%	Broken
42	Capacitance Hi-Tester Type HIOKI 3501	1	1984	80%	Good
43	DIP Heter TRIO	4	1984	90%	Good
44	Power Supply Unit Leybold 0-300V	1	1968	25%	Broken
45	Penyedia Daya AVUS/Tegangan Leybold	1	1968	25%	Broken
46	Alat Tester Tabung Electronic Leybold	1	1968	25%	Broken
47	Geiga Counter Tabung Leybold	1	1968	25%	Broken
48	J. J. Demonstration Unit For Electrical *1	1	1968	25%	Broken
49	Ward Leonard Control System with Amplifier	1	1968	25%	Broken
	Control PLT. 60-6011				
50	Komputer Daser Taran (panel)	8panel	1968	60%	Usable
51	Servo Unit (nanel)	8panel	1968	60%	Usable
52	Unit Transceiver Signal Lapangan Udara	lunit	1982	40%	Out-of-use
· · ·	EX. Pertamina Cilacap				
53	Unit Transceiver ISB EX. Telkom Pertamina Pusat	2unit	1985	40%	Out-of-use
54	AKD 741 Extension 50 point Telephone	1unit	1984	40%	Out-of-use
<u>т</u>	EX. Pertamina Pusat				
55	Telex Model T100 EX. Pertamina Pusat	4unit	1984	40%	Out-of-use
00					1

<b>[</b> ]		No. of	Year of	Present	
No.	Name of Equipment	Unit	Purchase	Condition	Remarks
56	Panel LB & CB Telephone	2unit	1984	40%	Out-of-use
57	Panel Kabel-Kabel Telecommunication	1unit	1984	40%	Out-of-use
58	Panel Peraga Electronic Tabung Tavan	30unit	1968	40%	Out-of-use
59	Panel Praktikum Micro Electronica Linear	6unit	1982	85%	Good
	EX. ITS Surabaya				e altri di chi di chi e di chi e. Nga Mana di chi chi chi e tetta di chi
60	Panel Praktikum Teknik Digital	11unit	1982	85%	Good
	EX. ITS Surabaya				
61	Panel Praktikum Telecommunication	11unit	1968	60%	Good
62	Panel Praktikum Pengukuran/Rangkaian	4unit	1974	40%	Out-of-use
	LISTRIK EX. TO ELECTRONICS INGGRIS		1974	40%	Out-of-use
			1974	40%	Out-of-use

Note: \*1 Those units of equipment under No. 48 to No. 62 are "used equipment" provided by PERTAMINA and the universities which is presently utilized as teaching models or for demonstration purposes.

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# Annex 11-4-3 COOLING TECHNIQUE LABORATORY EQUIPMENT LIST

		No. of	Year of	Present	
No.	Name of Equipment	Unit	Purchase	Condition	Remarks
1	Training Unit (Commercial Refrigration Model	lunit	1973	70%	Good
	9051)			.,,,	
2	Refrigeration Training System with Open Type	1unit	1983	80%	Good
	Unit Compressor				
3	Refrigeration Training System AC Unit(made by	1unit	1984	80%	Good
	Trainees)				
4	Freezer Unit for Training (made by Trainees)	lunit	1984	80%	Good
5	Refrigration Cylinder Demonstration Unit	2unit	1983	80%	Good
			1985		
6	Charging Cylinder	1	1983	80%	Good
7.	Vacuum Pump	3unit	1973		
			1983	90%	Good
			1984		
8	Charging Hainfold	3unit	1973	70%	
			1983	80%	Good
			1984	100%	· · · · · · · · · · · · · · · · · · ·
9	AVC Meter, SANHA	2	1985	100%	Good
10	Pain Type Ampere Heter	2	1973	80%	Good
			1985	100%	
11	Electronic Thermometer	3	1973	40%	2 units: out-of-use
			1973	70%	1 unit: good
12	Thermal Vacuum Check	3	1973	25%	2 units: broken
				70%	1 unit: good
13	Electronic Checking Equipment	1	1973	60%	Usable
14	Thermal Hermetic Check	1	1973	60%	Usable
15	Soldering Gun	1	1973	70%	Usable
16	Flaring Tools	3unit	1973	80%	Good
17	Flaring & Swagging tools	4unit	1983	80%	2 units: good
			1984	80%	2 units: good
18	Swagging tools punch type	2unit	1973	80%	Good
· .			1984	90%	
19	Supporting tools for repair		1985		Decided to purchase

		No. of	Year of	Present	
No	Name of Equipment	Unit	Purchase	Condition	Remarks
1	Retort Kit	3		60%	Usable
н 1				60%	Usable
				40%	Out-of-use
2	Analytical Balance	2	·····	50%	Narrowly usable
		n Second	ne este de	20%	Broken
3	Electrical Balance	1		40%	Out-of-use
4	Mud Nixer	4		60%	
				60%	3 units: usable
				50%	
		- 		40%	1 unit: out-of-use
5	Hud Balance	3		60%	2 units: usable
		• ;		60%	
				40%	1 unit: out-of-use
6	Harsh Funnel	1		60%	Usable
7	PH Meter	3		70%	Good
		-		70%	uvvu
· .				50%	Lack of spareparts
8	Viscometer	4	••••	50%	Narrowly usable
				50%	
		н. 		40%	Out-of-use
				25%	Broken
9	Rheoneter	1		50%	Narrowly usable
10	Resistivity Meter	1	•••••	50%	Narrowly usable
	Filter Press	2		50%	Narrowly usable
				50%	Inditoută dounie
12	HPHT Filter Press	1		40%	Lack of spareparts
	Sand Content	2		50%	Narrowly usable
	n an an the second s			40%	Out-of-use
14	Fluorescent Lamp	2	н н. 1	60%	Usable
				50%	Narrowly usable
15	Turbidity Meter	1		50%	Incomplete
16		1	•••••	50%	Lack of spareparts
17	Oven	1		60%	Usable
18		1		50%	Narrowly usable

# Annex II - 4 - 4 PRODUCTION LABORATORY EQUIPMENT LIST

		No. of	Year of	Present	
NO.	Name of Equipment	Unit	Purchase	Condition	Remarks
19	Not Plate	4		60% 60%	lisable
				30%	Out-of-use
				40%	
20	Sieve Shaker	2		50%	Usable
			2.	50%	
1	Hydraulic Press	1		30%	Out-of-use
2	Vicat	1		40%	Out-of-use
3	Mercury Pump	2		?	From Lemigas,
				?	Jakarta
4	Vacuum Pump	1		50%	Narrowly usable
25	Permeameter	1		50%	Narrowly usable

# Annex II - 4 - 5

CHENICAL LABORATORY EQUIPMENT LIST

T		No. of	Year of	Present	
Na	Name of Equipment	Unit	Purchase	Condition	Remarks
1	Analytical Balance	1	1975	90%	Good
2	Constant Temperature Bath	1	1975	10%	Broken
3	Water Distillation Apparatus	1	1980	50%	Narrowly usable
4	Driver (1) Drying Machine	1	1978	75%	Good
	(2) Desicator	12	1975	50%	Narrowly usable
5	Stop Watch	3	1982	90%	Good
6	Manometer	2	1975	40%	Out-of-use
7	Vacuum Pump	: 1	1975	30%	Broken
8	Centrifugal Machine	1	1984	90%	Good
9	Thermometer	80	1975	90%	Good
10	Measuring Glass Ware (Pipette, Funnel, etc.)	110	1975	90%	Good
11	Heater (1) Gas Burner	15	1975	70%	Good
	(2) Electric Heating Mantle	8	1972	40%	Out-of-use
12	Reagent Storage Cabinet	2	1972	30%	Out-of-use
13	Acid Cupboard	2	1972	50%	Narrowly usable
14	Sulphur Content Measurement	1	1972	50%	Narrowly usable
15	Polarimeter	1	1972	40%	Out-of-use
16	Six Paddle Stirrer	1	1984	99%	New
17	Bansh & Lomb Spectronic 20 Spectrophotometer	1	1980	70%	Good
18	Turbidimeter	1	1983	80%	Good
19	PH Neter	4	'83/'84	70/90%	Good
20	Hot Plate Stirrer	6	1982	80%	Good

Annex II - 4 - 6 OIL LABORATORY EQUIPMENT LIST

		No. of	Year of	Present	
Na	Name of Equipment	Unit	Purchase	Condition	Remarks
1	ASTM Distillation	3 unit	1972	40%	Out-of-use
2	Penetrometer	1 ûnit	1969	50%	Narrowly usable
3	Carbon Residue Conradson	1 unit	1971	40%	Out-of-use
4	Ductility	1 unit	1971	40%	Out-of-use
5	R.V.P. Constant Temperature Bath	1 unit	1972	40%	Out-of-use
6	Aniline Point APP.	1 unit	1974	50%	Narrowly usable
	Kinematic Viscosity Bath	1: unit:	1974	50%	Narrowly usable
8	Water Content Dean & Stark APP.	1 unit	1972	40%	Out-of-use
9	Flash Point Abel Pensky	1 unit	1971	40%	Out-of-use
10	Smoke Point APP.	1 unit	1972	30%	Broken
11	Redwood Viscometer	2 unit	1972	60%	Usable
12	Centrifuge	1 unit	1969	30%	Broken
13	Saybolt Viscometer	1 unit	1972	30%	Broken
14	ASTH Color Measurement	1 unit	1974	60%	Usable
15	Existent Gum APP	1 unit	1972	40%	Out-of-use
16	Bomb Calorimeter	1 unit	1969	50%	Narrowly usable
17	Flash Point Tester	1 unit	1969	40%	Out-of-use
18	Saybolt Chromometer	1 unit	1969	50%	Narrowly usable
19	Fractional Distillation Unit	1 unit	1972	50%	Narrowly usable
20	Constant Temperature Bath	1 unit	1976	50%	Narrowly usable
21	Flash Point Tag.	1 unit	1972	40%	Out-of-use
22	Flash Point Cleaveland Open Cup	1 unit	1972	40%	Out-of-use
23	Copper Strip Corrosion Bath	1 unit	1972	40%	Out-of-use
24	Oxidation Stability APP.	1 unit	1973	40%	Out-of-use
25	Lovibond Tintometer	1 unit	1984		Not yet installed
26	Pour Point APP.	1 unit	1976	50%	Narrowly usable
27	Melting Point APP.	1 unit	1974	40%	Out-of-use
28	Huffle Furnace	1 unit	1973	40%	Out-of-use
29	Drying Oven	1 unit	1973	30%	Broken
30	Engler Visimeter	1 unit	1973	30%	Broken
31	Cooperative Fuel Research Machine	1 unit	1976	90%	Good

ANNEX II-5-1 STUDY FOR OIL VELOCITY OF CRUDE FURNACE TUBE

It is widely known that the lower oil velocity of furnace tube not only promotes the formation of scale and coke which is accompanied by the rise of the pressure drop of furnace tube, but also decreases the efficiency of heat transfer.

If there is a growing coke formation, the tube skin temperature goes up sharply and becomes very dangerous.

Further there have been some papers described on the hot spot of furnace tube and the oil leakage from it.

In order to avoid this condition the size of heating tube is designed so as not to underrun the lower limit of the allowable velocity.

(1) Existing Tube Velocity

The crude charge heaters are now operated in parallel. The three calculations below is carried out under the following conditions

2,000 BPSD

- Crude oil through-put

- Fluid properties

- Size of tube

Sp.Gr (60/60°F) 0.853
Viscosity 7.5 cSt @60°F
4 inches (Sch. 80)
OD: 114.3mm, Thickness: 8.6mm
Cross section area: 74.05cm<sup>2</sup>

(H.S. Bell's Criteria)

U > 0.143 d.u
U: Flow rate (Gal/min), d: ID of tube (inches)
µ: Viscosity (Sec.Saybolt)

 $\mu = 7.5 \text{ cSt} = 50 \text{ Sec.Saybolt}$ 

d = 97.1mm = 3.8 in

 $0.143 \text{ d.}\mu = 0.143 \text{ x } 50 \text{ x } 3.8 = 27.2 \text{ Gal/min}$ 

This value is the minimum oil velocity for a turbulent flow,

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 $U = 2,000 \ge 0.159 \ge 264.19/(24 \ge 60 \ge 2) = 29.2$  Gal./min Above result shows the velocity for a turbulent, but the value is near the lower limit of the allowable velocity.

(W.L. Nelson's Criteria)

 $V = 2,000 \times 0.159 \times 10^{6} / (24 \times 60 \times 60 \times 30.48 \times 2)$ = 0.8 ft/sec

Topping to 600°F	2 - 5 ft/sec
Topping to 800°F	3 - 4 ft/sec
(over 60% vaporization)	

The calculated value does not satisfy above two criterias. In case of using two furnaces in series the calculated value is 1.6 ft/sec, still it can't reach to the minimum allowable velocity.

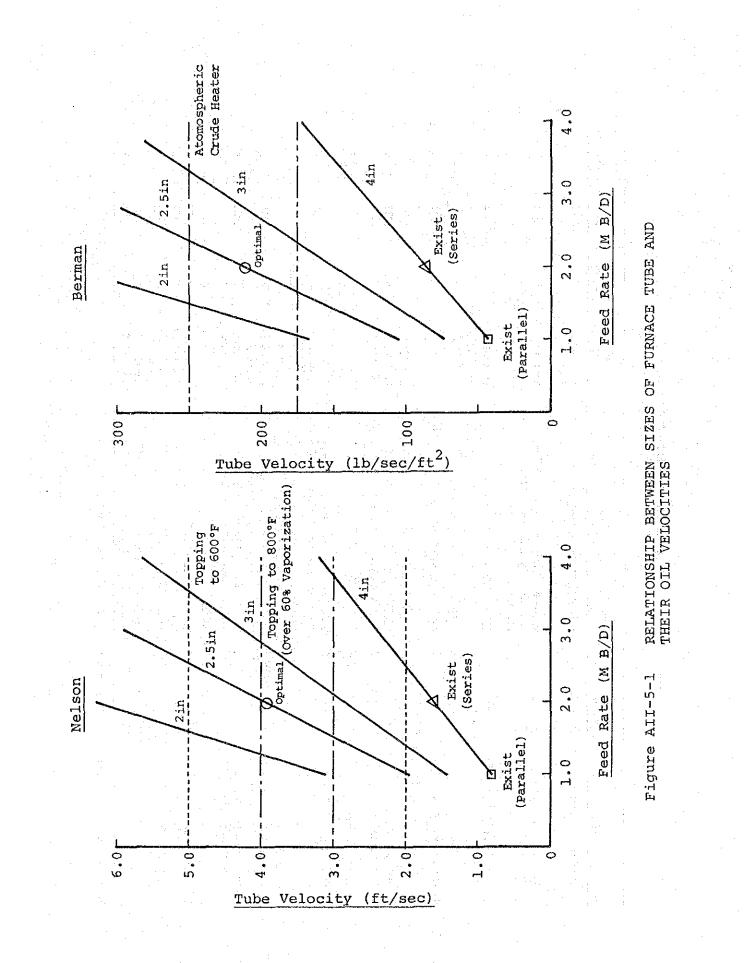
(H.L. Berman's Criteria)

 $V = \frac{2,000 \times 0.159 \times 0.853 \times 2.205 \times 10^3 \times 0.5}{24 \times 60 \times 60 \times 74.05 \times 10.764 \times 10^{-4}} = 87 \text{ lb/s/ft}^2$ 

The allowable mass velocity as the criteria is  $175 - 250 \text{ lb/s/ft}^2$ . In case of using two furnaces in series the calculated value also can't reach to the minimum allowable velocity.

## (2) Optimum Size of Furnace Tube

The relationship between the sizes of furnace tube and their oil velocities in two cases of Nelson's and Berman's criteria is shown in Fig. AII-5-1. This figure makes us understand that the arrangement of two furnaces should be modified from the parallel one to the series one and present 4 in. size of furnace tube should be replaced by 2.5 in. size of one.



Annex II-5-2 LIST OF LABORATORY EQUIPMENT AND APPARATUS (1) (011 Laboratory in the Refinery)

No.	Name	Test Method Q'ty	SPEC.	Maker Automatic & Model /Manual	Purchased Year	Judgement
~	Sampling Apperatus	ASTM D270 3	Weighted copper beaker, 1 quart	karl Kolb (Germany)	1972	<b></b>
<b>C</b> 1	Analytical Balance		Range 0 - 150g, Precision ±0.05mg, Mechanical weight application and optical scale range	Mettler (USA); H10	1974	₹
en	Refrigerator		257 1, 220 V, 50 Hz, 150 W	General Electric (Germany)	1984	4
<b>N</b> 1	Laboratory Table	<b>ی</b>	Percelein, Dimention 6,000x1.500x800		1972	đ.
റ	Drier (1) Drying Oven (2) Desicator	- 100 -	Temperature range: 40 - 250°C ID 150mm, Net weight 2.55 Kg	Karl Kolb. M (Gerwany)	1973 1972	U 🛩
-1 0	6 Draft Chamber 7 Stop Watch	<b>3</b>	Large dial subdivided in 30 sec. and small dial subdivided in 1/10 sec.	Ran Hard Fisher, AMICO(USA)	• • • • • • • •	<b>ez:</b>
$\mathbf{x}$	Pump (1) Air Pressure Pump (2) Precision Vacuum/ Pressure Air Pump	22 m	Single stage cap. 126 1/min. Single stage cap. 126 1/min. 228 V. Max. Belivery 2,500 1/h max. pressure bar. ultimate max. vacuum 1 bar.	Karl Kolb (Germany) Karl Kolb (Germany)	1975 1985	<b></b>
<b>б</b>	The rmometer	ASTM 5F ASTM 5F ASTM 15F ASTM 10F ASTM 2C ASTM 7C ASTM 7C	Range -36 to +120°F Range -112 to +70°F Range +30 to +180°F Range +200 to +700°F Range -2 to +400°C Range -2 to +300°C	Analis (USA) Analis (USA) Analis (USA) Analis (USA) Analis (USA) Analis (USA) Analis (USA)	1978 1978 1978 1978 1978	द्ध की ब्द को की दा

Note: A = Good condition, B = Barely in use, C = Out of order or not in use

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Annex II-5-2 LIST OF LABORATORY EQUIPMENT AND APPARATUS (2) (011 Laboratory in the Refinery)

No.,	Name	Test Method	0'ty			SPEC.			Maker & Model	er del	Automatic /Manual	Purchased Year	d Judgement
10	Measuring Glass Ware - Measuring cylinder		each 20	Cap.	10, 25,1	10, 25,100, 250 ml	m1.	, i.i.	byrex, Yer	Yena (USA)		1975	4
	- Volumetric flask		<b>_</b>	Cap.	500, 1,1 25, 50,	500, 1,000 ml. 25, 50, 100, 250	] ml.	nda fila	1.7	Yena (USA) Yena (USA)		1975 1975	44
	- Beaker glass		each 5 each 25	Cap.	500, 1,0 100, 250	1,000 ml. 250, 500 ml		, ido f.		Yena (USA) Yena (USA)		1975	`बद ⊲द ≪
:	0440		eacn 10	- 1 - E	1,000,2	<b>č, UUU, Š</b>	ά <b>ν η (10 Β. Β.).</b>		ryrex, ter	tena (uoh)	· ·	CIST	<b>±</b> t .
<b>-</b> -	other blass ware - Measuring pipettes - Reagent bottles - Burettes	• • • • • • • • • • • • • • • • • • •	each 5 each 5 each 2 each 2	Cap. Cap.	10, 25 ml. 250, 500 ml 25, 50 ml.	al. 30 al.		yanı yike bile	Pyrex, Yer Pyrex, Yer Pyrex, Yer	Yena (USA) Yena (USA) Yena (USA)		1975 1975 1975	লা ব্যা ব্য
12	Heater (1) Gas Burner		ى م	High	Temperature	ture			Karl Kolb			1978	
	(2) Electric Heating Mantle	le		Type	Fish	÷.	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	<b>-</b> .	Germany		8 - -		.*
	- Globe		4	Cap.	250, 50(	500 ml, 220/110 V,	0/110 V, 700 W		Karl Kolb		4	1978	-
	1 1 1		4	Long	3 m. 11(	110 V, 270/	270/500 W		Karl Kolb (Germany)			1978	<b>43</b>
13	13 Reagent Storage Cabinet		~			· · · · ·							~4
14	<pre>14 Specific Gravity (1) Hydrometer</pre>	ASTM D1298		Appli	Application for	for crude	crude oil and				æ		đ
	· · ·	ASTM D941		petro Appli oil a	petroleum oil Application fo oil and petro	petroleum oil Application for high pour oil and petroleum wax	pour point fuel x	leI		· · · ·	<b>X</b>		< <b>1</b>
12	15 Distillation	ASTM D86	(C)	Appli	ication 1	for gaso	Application for gasoline, Kerosine		Karl Kolb		*	1972	<u>6</u>

Note: A = Good condition. B  $\sim$  Barely in use, C = Out of order or not in use

Annex II-5-2 LIST OF LABORATORY EQUIPMENT AND APPARATUS (3) (011 Laboratory in the Refinery)

No.	Маме	Test Method	Q'ty	SPEC.	Maker & Model	Automatic /Manual	Purchased Year	Judgement
16	Flash Point (1) Tag Closed Tester	ASTN D56		Application for crude oil and kerosine	Labline Instru-	2 - 2 - 2 - 2	1972	. ບ
	(2) Aber Tester	IP 170		Application for crude oil and kerosine	ment Co., USA Sette Stanhope,	×	1972	<b>63</b>
	(3) Pensky-Martens Closed Testor	ASTM D93	н	Application for gas oil and fuel oil	Labline Instru-	<b>36</b> ,	1969	ы U
	(4) Cleveland Open Cup Tester	ASTM D92	<b>-</b>	Application for petroleum wax	Labline Instru- ment Co., USA	₹.	1972	ပ ပ
21	17 Smoke Point	ASTM D1322	<b>H</b>	Application for kerosene	Sette Stanhope (USA)		1972	U
8	18 Reid Vapor Pressure	ASTM D323	⊷ ⊷	Application for crude oil and gasoline, constant temperature bath has 5 testing, compartment	E.C.O.(USA) 120 - 14	<b>36.</b>	1968	ပ
19	Redwood Viscosity	15 70	Ħ	Application for fuel oil with 50 ml flask, gas heating bath, stirrer, etc.	Sommer & Runge KG (Germany)	36	1972	«ť,
20	Pour Point	ASTM D97	-	Application for crude oil, gas oil and fuel oil	Karl Kolb (Germany)	¥.	1968	ບ
	21 Water Content	ASTM D95		Application for crude oil, gas oil and fuel oil	Karl Kolb (Germany). Sba-II-4 plates	<b>**</b>	1972	U
23	22 Water and Sediment	ASTM D96	-	Application for crude oil, gas oil and fuel oil	Karl Kolb (Germany), UJ.3	×	1968	່ບ

LIST OF LABORATORY EQUIPMENT AND APPARATUS (4) (011 Laboratory in the Refinery) Annex II-5-2

<ul> <li>23 Conradson Carbon Residue ASTM D189 1 Application for crude oil, gas oil Karl Kolb M 1958 C</li> <li>24 Ash ASTM D482 1 Application for crude oil, gas oil Heraeus M 1973 B</li> <li>25 Copper Corrosion ASTM D130 1 Application for crude oil, gas oil Karl Kolb M 1959 C</li> <li>25 Copper Corrosion ASTM D130 1 Application for gasoline, kerosine Karl Kolb M 1959 C</li> <li>26 Color (1) ASTM ASTM D1500 1 Application for gas oil CurpE</li> <li>27 Aniline Point IP 17 1 Application for gasoline and kerosine Karl Kolb M 1969 C</li> <li>27 Aniline Point ASTM D1321 1 Application for gasoline and kerosine Karl Kolb M 1969 C</li> <li>28 Needle Penetration ASTM D1321 1 Application for gasoline and kerosine Karl Kolb M 1969 C</li> </ul>	No.	Nage	Method	g'ty	SPBC.	& Model	/Manual	/Manual Year	Judgement
ASTM D482       1       Application for crude oil, gas oil       Heraeus       M       1973         ASTM D180       1       Application for gasoline, kerosine       Karl Kolb       M       1969         ASTM D180       1       Application for gasoline, kerosine       Karl Kolb       M       1969         ASTM D1500       1       Application for gas oil       Germany), K2531       M       1974         ASTM D1500       1       Application for gas oil       SETA(England), M       M       1974         ASTM D1501       1       Application for gas oil       Germany), K2531       M       1974         ASTM D1501       1       Application for gas oil       Germany), K2531       M       1974         ASTM D1501       1       Application for gas oil       Germany), K2531       M       1974         ASTM D511       1       Application for gasoline and kerosine       Karl Kolb       M       1969         ASTM D1321       1       Application for petroleum wax       Sommer & Runge       M       1969	<b>67</b>	Conradson Carbon Residu	e ASTM D189		Application for crude oil, gas oil and fuel oil	Karl Kolb (Germany)	<b>S</b>	1368	<b>U</b>
ASTM D130 1 Application for gasoline, kerosine Karl Kolb M 1969 ASTM D1500 1 Application for gas oil (Germany), K2531 M 1974 ASTM D1500 1 Application for gas oil (GL-PE Lovinbond M ASTM D611 1 Application for gasoline and kerosine Karl Kolb M (Bagland) M 1969 (Germany) Commer & Runge M 1969 (Germany) M 1961 1 Application for petroleum wax Sommer & Runge M 1969	5	Ash	ASTM D482	<b>H</b>	Application for crude oil, gas oil and fuel oil	Heraeus (Gerwany)	<b>5</b>	1973	ស
ASTM D1500 1 Application for gas oil SETA(England), M bond IP 17 1 Application for Kerosine (Lovinbond M (England) ASTM D611 1 Application for gasoline and kerosine Karl Kolb M Germany) (Germany) 1 Application for petroleum wax Sommer & Runge M	ດ່	Copper Corrosion	ASTM D130	-	Application for gasoline, kerosine and gas oil	· .	81 81	1969	C)
<ul> <li>(2) Lovinbond IP 17 1 Application for Kerosine Lovinbond Mulline Point AsTM D611 1 Application for gasoline and kerosine Karl Kolb M</li> <li>Aniline Point ASTM D611 1 Application for gasoline and kerosine Karl Kolb M</li> <li>(Germany)</li> <li>Needle Penetration ASTM D1321 1 Application for petroleum wax</li> <li>Sommer &amp; Runge M</li> <li>KG, Germany</li> </ul>	G	Color (1) ASTM	ASTM DI500	-	Application for gas oil	SETA (England),	<b>7</b> <b>7</b> <b>1</b> <b>1</b> <b>1</b> <b>1</b> <b>1</b> <b>1</b> <b>1</b> <b>1</b> <b>1</b> <b>1</b>	1974	• <b>ei</b> ;
Aniline Point ASTM D611 1 Application for gasoline and kerosine Karl Kolb M (Germany) Needle Penetration ASTM D1321 1 Application for petroleum wax Sommer & Runge M		(2) Lovinbond	IP 17	<b>.</b>	Application for Kerosine	Levinbond (England)	1 <b>5</b> 1		-
ASTM D1321 I Application for petroleum wax Sommer & Runge M		Aniline Point	ASTM D611	<b>1</b>	Application for gasoline and kerosine	Karl KoIb (Germany)	W	1969	ц С
	80	Needle Penetration	ASTH DI321	ъч	Application for petroleum wax	Sommer & Runge KG, Germany	<b>5</b> 2	1969	ບ

Annex II-5-3 LIST OF LABORATORY EQUIPMENT AND APPARATUS (1) (Analytical Laboratory in Refinery)

Nare	Test Method B°ty	SPEC.	Maker Automatic & Model /Manual	Purchased /Manual Judgement
I Analytical Balance	<b>80</b>	Range 0 - 160 g, Precision +0.05 mg		1974
2 Draft Chamber				
Laboratory Table	S			
Glass Ware		10 ml in 1/10	Kimax (USA)	1978
	ν <b>α</b>	Burrets cap. ZD mi in L/10 ml Burrets cap. 10 ml in 1/10 ml	Kimax (USA) Dewarex	1969
	LC,	coloured glass	(England) Vimay (1154)	1078
	סיי	Volumetric pippettes 25 ml	Kimax (USA)	1978
	10	Erlenmeyer cap. 250 ml (Graduated) Test tubes red 19 ml	Duran (Germany) Vimev (NSA)	1976
	3 <b></b> 1		Kimax (USA)	1978
	8	Flat bottom flask	Kewarex	1969
	30	Petri dish ø 3"	(England) Kimax (USA)	1978
	່ວວ	Watch glass ø 1 - 2"	Kimax (USA)	1978
	10 4	Stirring rods Beaker glass cap. 258 ml	- Kimax (USA)	1978 1978
		Beaker glass cap. 25 ml		1978
	<b>C3</b> C3	Wash bottles made of plastics Measuring cylinder graduated.	- Cenco (USA)	1967
	3	cap. 100 ml in 1/100 Volumetric Flask cap. 100 ml	Cepco (USA)	1986
				2
	က် က	Funnel # 5 Desicator inside diameter		1966 1366
		Desicator inside diameter 150 mm net weight 2.55 Kg		

Note:  $\dot{A}$  = Good condition, B = Barely in use, C = Out of order or not in use

Annex II-5-3 LIST OF LABORATORY EQUIPMENT AND APPARATUS (2) (Analytical Laboratory in Refinery)

No.	Naac	Test Method	0'ty	SPEC.	Maker & Model	Automatic /Manual	Purchased /Manual	Judgemen t
ŝ	Turbidity	ASTM D1889	- <b></b> -	Application for boiler water, cooling Hellige Inc. water and drinking water	Hellige Inc., (USA)	5. 5.	1961	u
9	pH by glass electrode ASTM D12	ASTN D1293	-	Application for boiler water, cooling Methrom He Risau water, drinking water and waste water (Switzerland), pH Range 0 - 14, 110 - 125 volt, 80 W E350B	Methrom He Risau (Switzerland), E350B	2010 2010 2010 2010 2010 2010 2010	1961	U
-	Dissolved Oxygen		-	Application for boiler water	Electronic Inst- ments Ltd. (England), model 1519	<b>F</b>	1961 1961	un production de la composition de la c
$\infty$	8 Soild Content	AST# D1888		Application for boiler water, cooling water and waste water	Gallenkamp (Germany), LMB 5	<b>1</b>	1362 1362	U
თ	Incubator	ASTM	1	Application for drinking water	Memeurt (Germany)	<b>x</b> `	1976	-
0	10 Rot Plate with Magnetic Stirrer	•	~1	Application for proparating titration reagent, etc	Cenco (USA) Catalogue No. 34532-1	×	1961	U
П	Spectrophotometer		<b>استو</b> ر .	Application for metal content in water	Hach company (USA)	× <b>×</b>	1984	4
ž	Note: A = Good condition, B	e Bar	in us	ely in use, $C = 0$ ut of order or not in use			in the second	

	RESPONSE ANALYSIS, SHELL STRESS CALCULATI	ON		· · · · · · · · · · · · · · · · · · ·
1.	SECTION NUMBER			1
***	DESIGN CONDITION ***			·
3. 4.	HIGHT OF CALCULATION LEVEL (FROM BASE PLATE) OPERATING PRESSURE OPERATING LOWER PRESSURE DESIGN TEMPERATURE	SPRS	M Kg/cm2 Kg/cm2 °C	0.5 0.5 0.0 350.0
	SHELL 6. INSIDE DIAMETER (COR.) 7. PLATE THICKNESS (COR.) 8. MATERIAL NAME (CLASS)	SDIL STHK	MM MM	2033.4 7.8 (3) 5541
	11. ELASTIC MODULUS ROOM. TEMP.	SY Sem	KG/MM2 KG/MM2 KG/MM2	17.0    17700.0  
	12. TENSILE STRENGTH 13. YIELD POINT		KG/MM2 KG/MM2	
	· · · · · · · · · · · · · · · · · · ·	SWEF Sangl		0.2 0.0
×**	RESPONSE ANALYSIS ***			na an Taonairtí Ríos an Salaine an Salain
16. 17. 18.	HORIZONTAL RESPONSE COEFF. IN CASE H < = 16 IN CASE 16 < H < = 35 IN CASE 35 < H DESIGN ACCEL. BETA4*RKGH	BETA4 RKSH		2.33 0.0 0.0 0.31
21.		TWGTW	KG KG KG	19132.29 19132.29 5739.68
***	COMPUTED AND ALLOWABLE STRESS ***			
23. 25. 26. 27.	SEISMIC MOMENT MEAN DIAMETER (COR.) ALLOW. TENSILE STRESS SMALLER VALUE (SY. SYO) ALLOW. BUCKLING STRESS ALLOW. COMPRESSIVE STRESS	SDML ASTEN SYDAS SDAS	KG*MM Mn Kg/MM2 Kg/MM2 Kg/MM2 Kg/MM2	3.19 17.70 8.12
	COMPUTED STRESS AND EVALUATION 33. COMPUTED TENSILE STRESS 34. EVALUATION 35. COMPUTED COMPRESSIVE STRESS 36. EVALUATION	a di l	KG/MM2 KG/MM2	1.4; OK 1.8' OK
	IARKS: ALLOWABLE STRESS	 S	KG/MM2	15.9

nex II-5-4 BUCKLING STRESS CALCULATION

					······································
	RESPONSE ANALYSIS, SHELL S	STRESS	CALCULATI	ON	······
l.	SECTION NUMBER				2
**	DESIGN CONDITION ***				· · · · · · · · · · · · · · · · · · ·
KII	RT TYPE		JSWLD		A (PRESSURE)
2.	MATERIAL NAME (CLASS)	•			(3) 5541
<b>}.</b> .	PLATE THICKNESS	· .	STHK	MM	7.81
1.	MEAN DIAMETER	÷	SDML	MM	2041.20
	DESIGN TEMPERATURE		STMP	°C	350.00
	DESIGN TEMP.				
-	6. TEMSILE STRENGTH		SU	KG/MM2	41.00
	7. YIELD POINT		I SY I	KG/MM2	17.70
	8. ELASTIC MODULUS		I SEM	KG/MM2	17700.00
	ROOM, TEMP.		1		
-	9. TENSILE STRENGTH		I SUO I	KG/MM2	41.00
•	10. YIELD POINT		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	KG/MM2	
 i	OPENING WIDTH		I SYOPSMI	 мм	0.0
	SEISMIC MOMENT			KG*MM	4.08571E 07
	WEIGHT	- 1 J	TWGTW		20146.80
	HALF APEX ANGLE		I SANGL	and the second	0.0
**	COMPUTED AND ALLOWABLE STRRES	***			
••	SKIRT TYPE A (WELDED TO PRESS	JRE PAR	TS)		
	27. ALLOW, TENSILE STRESS		ASTEN	KG/MM2	3.19
	28. SY' : MIN (SY, SYO)		I SYDAS	KG/MM2	17.70
	29. Allow. buckling stress		SDAS	KG/MM2	8.12
	30. $P := MIN (SYO, 0.75*SUO)$		I F		
	31. ALLOW. COMPRESSIVE STRESS		I ASCON		
	32. COMPUTED COMPRESSIVE STREE			KG/MM2	
	39. EVALUATION	1			OK OK
	SKIRT TYPE B (WELDED TO NON PI	ESSURE	PARTS)		· · · · · · · · · · · · · · · · · · ·
	34. F : = MIN (SYO, 0.7 *SUO)		F I	KG/MM2	0.0
	35. SY' : = MIN (SY, SYO)			KG/MM2	
	36. ALLOW. BUCKLING STRESS	1 A.	SDAS		
	37. ALLOW. COMPRESSIVE STRESS		I ASCON	and the second	
·	38. COMPUTED COMPRESSIVE STRES		SCCON		
	39. EVALUATION	• • • •			0.0
-	<u> </u>		A		<u> </u>

	000000	EVAL.	9K	0K
	I SS	ALLO. (KG/MM2)	8.121 OK	8.12
	COMMPLESSIVE STRESS	SEISMICI (KG/MM2)	1.871	2.001
	COMMPLE	WIND   (KG/MM2)	3.191 1.751	1.87
	SS	ALLO.   (XG/MM2)	a t	3.19
IRT)	TENNSIL & STRESS	MOMENT   WIND   SEISNIC  ALLO.   WIND   SEISNIC  ALLO.   WIND   SEISNIC  ALLO.   WIND   (KG/MM2)  (KG/MA)  (KG/MM2)  (KG/MA)  (KG/MA)	1.43	0.0 0.0
SHELL & SK	TENN	HIND (KG/MM2)	1.32	0.0
RESULT SUMMARY (1) (SHELL & SKIRT)	LOAD	MOMENT (KG*MM)	I 2 1 CYLN113010.01 2033.41 2049.01 7.801 7.801 5.067E 031 3.500E 071	7.80 5.215E 03 3.757E 07
RESULT SUI	WIND LOAD	FORCE (KG)	5.067E 03	5.215E 03
		DESIGN THK. (MM)	7.80	7.80
	ION		7.80	1.80
	SHAPE DIMENSION	INSULA. INIT 0.DIA. THK (MM) (MM	2049.8	2   4   STRAI 500.0  2049.0  2049.0  7.
	SHAL	DIA.	2033.4	2049.0
		LENGTH (MM)	13010.0	500.0
		TYPE	CALN	I STRA
	 	SECT COMP.	5	
		SECT NO.	1	\$7

4.0MM Top of Deflection for Seismic Top of Deflection for Wind Remarks:

3.5MM

ANNEX II-5-5 RECORDS OF TROUBLES IN THE POWER GENERATORS

GENERATOR NO. I/ELECTRICAL

•		
2	ЪĽ,	
r	• •	
	1	
•	1	
	÷.,	
•	÷.	

	Trouble	Cause	Date	Solution
tor tor e in e in	<ol> <li>Generator switch off</li> <li>Failure in Exciter</li> <li>Generator switch off</li> <li>Failure in switch gear</li> <li>Failure in emergency stop</li> <li>Failure in electric motor of water pump</li> </ol>	Reverse power relay is not correct Can not off The exciter is suddenly off 0.C.B. is not running well Solenoid is broken Short circuit	6 May, 1975 21 March, 1982 18 July, 1983 23 July, 1983 2 May, 1984 2 May, 1984 17 May, 1985	To be adjusted Repair Replacement the contacted Replacement Replacement
		DIESEL ENGINE NO. 1		
	Trouble	Cause	Date	Solution
The abilit Shut down Leaking fu Engine is Failure in	<ol> <li>The ability to support the load is decrease Governor is not correct</li> <li>Shut down</li> <li>Leaking fuel</li> <li>Leaking fuel</li> <li>Bagine is not running well</li> <li>Seals of the fuel inject</li> <li>Failure in cylinder No. 1</li> </ol>	Governor is not correct Temperature of cooling water is too high One fuel delivery pipe is crack Seals of the fuel injection pump of cylinder No. 4. 5 & 6 are broken Cylinder head No. 1 is crack	5 April, 1976 12 April, 1976 27 July, 1980 14 May, 1982 18 April, 1983	Governor is adjusted/repair Clean the cooler Replacement Replacement Replacement
4. 17 4. 17 4. 17 4. 17 7 10 7 10 7 10 7 10 7 10 7 10 7 10 7	<ol> <li>Start of operation; 25 May, 1973</li> <li>The first overhaul; 31 October, 1979</li> <li>The second overhaul; 3 January, 1984</li> <li>A. In overhaul, measuring devices and re</li> </ol>	3 1979 1984 d relays are calibrated/test.		

GENERATOR NO. II/ELECTRICAL

<ol> <li>Failure in switch gear</li> <li>Failure in electric motor of cooling tower</li> <li>Pailure in electric motor of cooling tower</li> <li>Failure in electric motor of aw water pump</li> <li>Failure in electric motor of raw water pump</li> <li>Exciter can not be adjusted</li> <li>No. Trouble</li> <li>Shut down</li> <li>Trouble</li> <li>The ability to support the load is decrease</li> </ol>	cooling tower cooling	Short circuit because of mouse inside Short circuit Short circuit	6 February, 1974		ĺ
		Short circuit Short circuit		To close the air cooling	
			29 November, 1975 18 July, 1982	noie by wire screen Rewinding Rewinding	
	of governor raw water pump	Motor speed short circuit Short circuit Adjuster winding is broken	26 September, 1982 7 April, 1983 6 November, 1984	Rewinding Rewinding Replacement	
	· · · ·	DIESEL ENGINE NO. 11			
<ol> <li>Shut down</li> <li>Failure in turbo charger</li> <li>The ability to support the lo</li> </ol>		Cause	Date	Solution	
4. Failure in cylinder No. 4	ad is decrease	Cooling water is over temperature The bearing is loose Governor is not correct The spring of fuel injection pump	10 May, 1976 21 June, 1976 26 June, 1981 20 June, 1982	Clean the cooler Replacement the bearing Governor is adjusted Replacement	
5. Failure in cooling system 6. Leaking fuel		is broken The bearing of water pump is broken One fuel delivery pipe is crack	20 July, 1982 6 August, 1982	Replacement Replacement	
Notes: 1. Start of operation; 25 May, 1973 2. The first overhaul; 12 January, 1980 3. The second overhaul; 24 February, 1984	25 May, 1973 12 January, 1980 24 February, 1980				

GENERATOR NO. III/ELECTRICAL

No.	Trouble	e		•		Cause			Date	Solution	
- ~ ~	<ol> <li>The load is out</li> <li>Failure in switch gear</li> </ol>				citer is ectric mo	Exciter is not running well Electric motor of 0.C.B. is	vell is	11 16	11 Jaunary, 1980 Repair 16 August, 1983 Replace	Repair Replacement	
<b>α</b> . Δ	<ol> <li>Railure in emergency stop</li> <li>Failure in electric motor of cooling tower</li> </ol>	top tor of coc	oling towe	· · · ·	snort circuit Solenoid is broken Short circuit	cuit broken it	•	22 18	22 October, 1984 18 May, 1985	Replacement Rewinding	· .
					DIE	DIESEL ENGINE NO. III	). III				
Р.	Trouble	e				Cause			Bate	Solution	G

I. Leaking Iuel		One fuel delivery pipe is crack	20 March, 1978	Replacement
2. Engine is not running well	· ·	Failure in Booster pump	17 May, 1979	Repair
3. Leaking fuel	· ·	Fuel valve of cylinder No. 1 and 2	23 May, 1982	Replacement
		are loose.		
4. The ability to support the load i	is decrease	the load is decrease The cooler is closed up	6 October, 1984 To be cleaned	To be cleaned

Notes: 1. Start of operation; 2 December, 1977 2. The first overhaul; 30 June, 1982 3. In overhaul, measuring devices and relays are calibrated/test

Annex II-5-6 TANK DATA

Walt         F. Sivet         Trace         No.         Hickness         Hicknes         Hicknes         Hicknes<			Size	(1)		Joint	Year	of.	Leak			Roo	100		2	Lower shell plate	ell pla	tte.
Dia.         Hight         (W)         W. Mail         Continue         Doi:         A         B         C         C         C           Menneam Crude         9:04.7         9:12         2:16         R         1928         -         7256         5:17         5:2         2:4         100           Menneam Crude         9:04.7         9:12         2:16         R         1928         -         7256         5:17         5:2         2:2         2:2         7:2         5:17         5:2         2:2         7:2         5:2         7:2         5:2         7:2         5:2         7:2         5:2         7:2         7:2         5:2         7:2	Tanl				Volume	Я.	Į,		from	Bottom pla	ate	thi		(III)	۲. ۱	thickness	s (the state)	
Kureneran Crucle         19.1         2.743         R         1228          Trace         No         2.4         2.4         1.0         4.5         2.4         1.0         4.5         2.4         1.0         4.5         2.4         1.0         4.0	. ov		Dia.	Hight	(.c¤)	з	Ŭ	Rost Repair	Joint	condition	· .	Ori- sin			Ori- gin	<b>A</b> I	ß	<b>U</b>
Slow         Slow <th< td=""><td>TOT</td><td>Kawengan Crude</td><td></td><td></td><td></td><td></td><td>1928</td><td><b>1</b></td><td>Trace</td><td>No scod</td><td></td><td></td><td>•</td><td></td><td>10.0</td><td>8.1</td><td>8.5</td><td>8.5</td></th<>	TOT	Kawengan Crude					1928	<b>1</b>	Trace	No scod			•		10.0	8.1	8.5	8.5
Siler         519         2.87         79.5         R         1928         -         Trane         Siler/19         5.0         2.2         2.7         5.5           Rull         5.9         2.87         79.5         R         1928         -         Trane         No         May         2.13	102	Ledok Crude					1978		Trace	Verv vood				c	8.0	7.1	1.1	1.7
Roisr         5:9         2:87         79:5         R         1928         -         Trace         100         2:1<	103	Slop	50°.5				1928	1	Contractor T	Slightly	0000			) ur		5	1	
Fuel         5:99         2:02         7:93         R         1928         C         Trace         No cool         2:02         2:13         2:14         2:13         2:14         2:13         2:14         2:13         2:14         2:13         2:13         2:14         2:15         2:15         2:15         2:14         1:13         1:13         1:15         2:15         2:13         2:14         2:15         2:14         2:15         2:14         2:15         2:14         2:15         2:14         2:15         2:14         2:15         2:14         2:15         2:15         2:14         2:15         2:16         No         No         Correction holes         2:15         2:15         2:16         No         No         Correction holes         2:15         2:14         2:15         2:14         2:15         2:14         2:15         2:14         2:15         2:14         2:17         2:16         2:16         2:16         2:16         2:16         2:16         2:17         2:17         2:16         2:17         2:17         2:17         2:17         2:17         2:17         2:12         2:13         2:13         2:11         2:11         2:11         2:11         2:11         2:11 <td>104</td> <td>Solar</td> <td>00</td> <td></td> <td></td> <td></td> <td>1928</td> <td>4</td> <td>Trace</td> <td></td> <td></td> <td>1</td> <td>j.</td> <td>ŝ</td> <td>Ì.,</td> <td>1</td> <td></td> <td></td>	104	Solar	00				1928	4	Trace			1	j.	ŝ	Ì.,	1		
Kerosene         6.09         2.02         32.1         R         1373          Trace         No         Mary corrocion         holes           Gas 011         5.99         2.02         79.5         W         1928         1937         Trace         No         pood         Mary corrocion         holes           Gas 011         5.99         2.02         79.5         W         1928         1937         Trace         No         pood         Mary corrocion         holes           Gasoline         5.99         2.02         79.5         W         1928         1957         Trace         No         pood         Mary corrocion         holes           Gasoline         5.99         2.02         79.5         W         1973          Trace         No         pood         Mary corrocion         holes           Gasoline         5.99         2.02         79.5         W         1973          Trace         No         pood         Mary corrocion         holes           Gasoline         5.09         2.02         79.5         K         1973          Trace         No         pood         Mary corrocion         holes         faite	105	Fuel	66.5				1928	ļ	Trace	pood		÷		. en	t 	1	ı	I
Kurseene         6.00         2.82         8.2.1         8         1373          Frace         No         conditionant of the solution of t	·	-			-	-				•		1	:		•			
Gas 011         5-99         2.82         79.5         W         1928         1971         Trace         No         Mary         correction holes           Rawy         Gas 011         5-99         2.82         79.5         W         1923         1967         Trace         No         Mary         correction holes           Gasoline         5.99         2.82         79.5         W         1923         15         Trace         No         Mary         correction holes           Gasoline         5.99         2.82         79.5         W         1973         -         Trace         No         Mary         correction holes           Gasoline         5.99         2.82         79.5         W         1973         -         Trace         No         Mary         correction holes           Gasoline         5.99         2.82         79.5         W         1973         -         Trace         No         No         Mary         correction holes           Gasoline         6.09         2.82         79.5         W         1973         -         Trace         No         No         Mary         correction holes           Gasoline         6.09         2.82	106	Kerosene	6.09		82.1		1973	ł	Trace		÷					•		
Gasoline         5.99         2.82         79.5         W, R         1928         1967         Trace No good Gasoline         Many corrocion holes           Gasoline         5.99         2.82         79.5         W, R         1928         1967         Trace No good Gasoline         Many corrocion holes           Gasoline         5.99         2.82         79.5         W, R         1923         -         Trace No good Many corrocion holes           Gasoline         5.99         2.82         79.5         W, R         1973         -         Trace No good Many corrocion holes           Gasoline         5.99         2.82         79.5         W, R         1973         -         Trace No good Many corrocion holes           Gasoline         5.99         2.82         79.5         W, R         1973         -         Trace No good Many corrocion holes           Gasoline         6.09         2.82         79.5         K         1923         -         Trace No good Many corrocion holes           F.H. Solar         7.49         4.25         79.5         K         1923         -         Trace No good Many corrocion holes           P.H. Solar         7.49         4.25         79.5         K         1928         -         Trace N	107	Gas Oil	5.99	÷			1928	1977	Trace			Many c	orrocio	a holes				
Remy Gasoline         5:99         2.02         79:5         W         1973          Trace         No         Many corrocion holes           Gasoline         5:99         2.02         79:5         W,         1923         1         Trace         No         Many corrocion holes           Gasoline         5:99         2.02         79:5         W,         1973          Trace         No         corrocion holes           Gasoline         5:99         2.02         79:5         W         1973          Trace         No         corrocion holes           Gasoline         5:99         2.02         79:5         W         1973          Trace         No         corrocion holes           Gasoline         5:99         2.02         79:5         W         1973          Trace         No         corrocion holes           Gasoline         6:09         2.02         79:5         K         1923          Trace         No         000         Many corrocion holes           Gasoline         5:00         2.03         7         Trace         No         000         10:17         2:3         2:3         2:3         2:1 <td>108</td> <td>Gas Oil</td> <td>5.99</td> <td>÷</td> <td>а 1.</td> <td>3</td> <td>1928</td> <td>1982</td> <td>Trace</td> <td></td> <td></td> <td>• • •</td> <td></td> <td></td> <td></td> <td>-</td> <td></td> <td></td>	108	Gas Oil	5.99	÷	а 1.	3	1928	1982	Trace			• • •				-		
Gasoline         5:99         2.82         79.5         N. R.         1928         1967         Trace         No         No         Corrocion holes           Gasoline         5:99         2.82         79.5         R         1923         -         Trace         No good         Many corrocion holes           Gasoline         5:99         2.82         79.5         W         1973         -         Trace         No good         Many corrocion holes           Gasoline         5:99         2.82         79.5         W         1973         -         Trace         No good         Many corrocion holes           Gasoline         5:99         2.82         79.5         W         1973         -         Trace         No good         Many corrocion holes           Gasoline         5:99         2.82         79.5         W         1973         -         Trace         No good         3.5         2.2         2.2         2.8           Gasoline         6:09         2.02         79.5         R         1928         -         Trace         No good         3.5         2.2         2.8         5.9         2.2         2.8         5.9         2.2         2.8         5.9         2.2	109	Heavy Gasoline		2.82	÷.		I973	:	Trace									•
Gasoline         5.99         2.82         79.5         R         1928         -         Trace         No good         Many corrocion holes           Gasoline         5.99         2.82         79.5         W, R         1973         -         Trace         No good         Many corrocion holes           Gasoline         5.99         2.82         79.5         W, R         1973         -         Trace         No good         Many corrocion holes           Gasoline         5.99         2.82         79.5         W, R         1973         -         Trace         No good         Many corrocion holes           Gasoline         6.09         2.82         82.1         W         1973         -         Trace         No good         Many corrocion holes           Gasoline         6.09         2.82         82.1         W         1973         -         Trace         No good         Many corrocion holes           Gasoline         5.49         4.25         79.5         R         1928         -         Trace         No good         Many corrocion holes           Gasoline         5.49         4.25         79.5         R         1928         -         Trace         No good         1.1	110		5.99	۰.		н. Н	1928	1967	Trace				orrocio	n holes				
Gasoline         5.99         2.82         79.5         R         1928         -         Trace         No pool         Mary correction holes           Gasoline         5.99         2.82         79.5         N         1973         -         Trace         No pool         Mary correction holes           Gasoline         5.99         2.82         79.5         N         1973         -         Trace         No pool         Mary correction holes           Gasoline         5.09         2.82         79.1         N         1973         -         Trace         No pool         Mary correction holes           Gasoline         6.09         2.82         79.5         R         1973         -         Trace         No pool         Mary correction holes           Gasoline         6.09         2.82         79.5         R         1973         -         Trace         No pool         Mary correction holes           F.H. Solar         5.49         4.25         79.5         R         1973         -         Trace         No pool         10.7         2.2         2.3         3.1         2.2         2.3         3.1         2.2         2.3         3.2         2.2         2.3         3.3 <td< td=""><td></td><td>÷</td><td></td><td></td><td></td><td></td><td></td><td></td><td></td><td></td><td></td><td></td><td></td><td></td><td></td><td>· .</td><td></td><td></td></td<>		÷														· .		
Gasoline         5.09         2.82         82.1         W         1973          Trace         No pool         Mary corrotion holes           Gasoline         5.99         2.82         79.5         W,         1973          Trace         No pool         Mary corrotion holes           Gasoline         5.99         2.82         79.5         W,         1973          Trace         No pool         Mary corrotion holes           Gasoline         6.09         2.82         82.1         W         1973          Trace         No pool         Mary corrotion holes           Gasoline         6.09         2.82         82.1         W         1973          Trace         No pool         Mary corrotion holes           Gasoline         6.09         2.82         79.5         R         1928          Trace         No pool         Mary corrotion holes           Gasoline         5.49         4.25         79.5         R         1928          Trace         No good         3.1         2.1         2.3         3.1         3.7         3.2         2.3         3.7         3.2         2.8         6.8         7.2         2.8 <td< td=""><td>111</td><td>Gasoline</td><td>5.99</td><td>2.82</td><td></td><td></td><td>1928</td><td>ı</td><td>Trace</td><td></td><td></td><td></td><td>orrocio</td><td>n holes</td><td>-</td><td></td><td></td><td></td></td<>	111	Gasoline	5.99	2.82			1928	ı	Trace				orrocio	n holes	-			
Gasoline         5.99         2.82         79.5         W         1973         -         Trace         No         No         Carcocion         Doles           Gasoline         5.99         2.82         79.5         W         1973         -         Trace         No         No         Carcocion         Doles           Gasoline         5.99         2.82         82.1         W         1973         -         Trace         No         No         Carcocion         Doles           Gasoline         6.09         2.82         82.1         W         1973         -         Trace         No         No         Amay correction         Doles           Gasoline         6.09         2.82         79.5         R         1928         -         Trace         No         No <td>112</td> <td>Gasoline</td> <td>6.09</td> <td></td> <td></td> <td></td> <td>1973</td> <td>1</td> <td>Trace</td> <td>No N</td> <td>•</td> <td></td> <td>orrocio</td> <td>n holes</td> <td></td> <td></td> <td></td> <td></td>	112	Gasoline	6.09				1973	1	Trace	No N	•		orrocio	n holes				
Gasoline         5.99         2.82         79.5         W. R         1973          Trace         No good         3.0         1.7         1.8           Gasoline         6.09         2.82         82.11         W         1973          Trace         No good         Mary         Gorrecion         holes           Gasoline         6.09         2.82         82.11         W         1973          Trace         No good         Mary         Gorrecion         holes           Gasoline         6.09         2.82         82.11         W         1973          Trace         No good         3.5         2.9         2.3         3.1         2.9         2.8         3.5         2.9         2.3         3.3         2.8         3.3         2.8         3.3         2.8         3.3         2.9         2.3         3.3         3.2         8         3.5         2.9         2.3         3.3         3.2         8         8         0         3.5         2.9         2.3         3.3         3.3         3.2         8         8         8         0         3.1         2.7         3.8         1.9         8         0         2.1         2.	113	Gasoline	5.99				1973		Trace	°N N	· · ·		orrocio	n holes				
Gasoline         6.09         2.82         82.1         W         1973          Trace         No< good         Many corrotion holes           Casoline         6.09         2.82         82.1         W         1973          Trace         No< good	114	Gasoline	5.99			3	1928	1967	Trace				1.7.1	8	•	•		
Gasoline         6.09         2.82         82.1         W         1973         Trace         No good         Many corrosion holes           P.H. Solar         5.49         4.25         79.5         R         1973         -         Trace         No good         3.5         2.4         3.3         2.3         2.8           P.H. Solar         5.49         4.25         79.5         R         1928         -         Trace         No good         3.5         2.4         3.3         2.8         2.3         2.3         2.8         3.1         2.7         3.2         8         3.5         2.4         4.25         7.3         8         1928         -         Trace         No good         3.5         2.4         3.3         2.3         3.3         3.3         2.8         3.3	115	Gasoline	6.09			3	1973	1	Trace	No good			OLTOCIO	n holes	•			
Gasoline       6.09       2.82       82.1       W       1973       Trace       No good       Many       corrosion holes         F.H. Solar       5.49       4.25       79.5       R       1973       Trace       No good       3.5       2.4       2.32       3.1       3.3       3.3       3.3       3.4       3.3       3.3       3.3       3.4       3.3       3.3       3.3       3.1       3.5       3.4       3.5       3.4       3.5       3.4       3.5       3.4       3.5       3.4       3.3       3.3       3.3       3.3       3.3       3.3       3.3       3.5       3.4       3.5       3.4       3.5       3.4       3.5       3.4       3.5       3.4       3.5       <			-		•							· .		 				
Gasoline         6.09         2.82         82.1         W         1973         Trace         No good         3.5         2.4         3.5         2.4         3.5         2.9         2.3         3.1           P.H. Solar         5.49         4.25         79.5         R         1928         -         Trace         No good         3.5         2.9         2.2         2.8         3.1         3.7         2.9         2.3         3.1         3.7         2.9         5.3         3.3         3.3         3.3         3.3         3.3         3.1         3.1         2.7         2.9         2.2         2.8         5.3         3.3         3.1         3.1         2.7         2.9         2.3         3.3         3.1         3.1         2.7         2.9         2.3         3.3<	116	Gasoline	6.09				1973	ł	Trace	No good			OLLOSIO					
P.H. Solar       5.49       4.25       79.5       R       1928       -       Trace       No       3.5       2.9       2.3       3.1       2.7       2.9       2.3       3.1       3.7       2.9       2.3       3.1       3.7       2.9       2.3       3.1       3.7       2.9       2.3       3.1       3.7       2.9       2.3       3.1       3.7       2.9       2.3       3.1       3.7       2.9       2.3       3.1       3.7       2.9       2.3       3.1       3.7       2.9       2.3       3.1       3.7       2.9       2.3       3.1       3.7       2.9       2.3       3.3       5.4       4.25       7.7       3.7       3.9       5.3       5.3       7       1928       -       Trace       No       good       4.0       1.7       2.3       3.3       5.3       5.3       7       2.9       2.3       3.3       5.4       5.4       5.4       4.4       3.1       7       2.9       2.3       3.3       5.8       7.8       1928       -       Trace       No       good       4.0       1.7       2.1       3.3       5.6       7.5       7.5       7.6       16.5       7.5	117	Gasoline	60.9	÷	:		1973	1	Trace	No good								
P.H. Solar       5.49       4.25       79.5       R       1928       -       Trace       No       3.5       2.9       2.3       3.1       3.7       3.9       6.8         B.O.D.       5.49       4.25       79.5       R       1928       -       Trace       No       3.1       2.7       2.9       2.8       5.3       3.7       3.9       6.8         Residue       8.40       5.31       290.3       R       1928       -       Trace       No good       3.1       2.7       2.9       2.3       3.3       3.7       3.9       6.8         Residue       8.40       5.31       290.3       R       1928       -       Trace       No good       4.0       1.7       2.3       3.3       3.7       3.9       6.8         Fuel       7.99       6.41       321       R       1928       -       Trace       No good       4.0       1.7       2.3       3.3       3.9       6.8         Fuel       7.99       6.45       538       R       1928       -       Trace       No good       4.0       2.7       2.9       2.8       16.5         F.L. Solar       11.90       8.	118	P.H. Solar	5.49		•		1928	۰ ا	Trace	No good		3.5						
Solar       5.49       4.25       79.5       R       1928       -       Trace       Sood       3.1       2.7       2.9       2.8         B.O.D.       5.49       4.25       79.5       R       1928       7       Trace       No       3.1       2.7       2.9       2.8       6.8         Residue       8.40       5.31       234.2       R       1928       7       Trace       No good       4.0       3.7       2.7       2.9       2.8       6.8         Residue       8.40       5.31       324.2       R       1928       7       Trace       No good       4.0       3.7       2.7       3.1       3.1       3.7       3.6       8       3.1       3.1       3.7       3.6       3.7       3.7       3.7       3.7       3.7       3.7	119	P.H. Solar	5.49		÷	•	1928		Trace	No good								
B.0.D:       5.49       4.25       R       1228       Trace No good       3.1       2.7       2.9       2.8       5.9       5.8       5.9       5.8       1228       Trace No good       4.0       1.7       2.3       3.9       6.8         Residue       8.40       5.31       294.2       R       1928       Trace No good       4.0       1.7       2.3       3.9       6.8         Reel       7.99       6.41       321       R       1928       Trace No good       4.0       1.7       2.3       3.3       6.8         Fuel       9.49       7.13       548       R       1928       Trace No good       4.0       1.7       2.3       3.3       6.8         Ruel       9.49       5.367       R       1928       Trace No good       4.0       2.7       2.5       5.3       6.8         P.H. Solar       9.00       8.45       538       R       1928       Trace No good       4.0       2.6       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1 <td< td=""><td>120</td><td>Solar</td><td>5.49</td><td></td><td></td><td></td><td>1978</td><td>ŧ</td><td></td><td>- Poor</td><td></td><td></td><td>in the second se</td><td>÷</td><td></td><td></td><td></td><td></td></td<>	120	Solar	5.49				1978	ŧ		- Poor			in the second se	÷				
B.O.D.       5.49       4.25       79.5       R       1928       -       Trace       No.good       3.1       2.7       2.9       2.8       5.3       5.9       5.8       1928       -       Trace       No.good       4.0       3.7       3.7       3.7       3.9       6.8         Residue       8.40       5.24       290.3       R       1928       -       Trace       No good       4.0       1.7       2.3       3.3       6.8       6.8       5.367       R       1928       -       Trace       No good       4.0       1.7       2.3       3.3       5.3       6.8       7.3       5.3       7.3       5.3       7.3       5.3       7.3       5.3       7.3       8       1928       -       Trace       No good       4.0       1.7       2.3       3.3       6.8         P.H. Solar       11.98       6.25       705       R       1928       -       Trace       No good       4.0       2.6       3.2       16.5         P.H. Solar       9.00       8.45       538       R       1928       -       Trace       No good       4.0       2.6       3.1       3.1       3.1       3.1 <td< td=""><td></td><td></td><td></td><td></td><td></td><td></td><td></td><td></td><td></td><td></td><td>:</td><td></td><td></td><td></td><td></td><td></td><td></td><td></td></td<>											:							
Residue         8.40         5.31         294.2         R         1928         -         Trace         No good         4.0         3.7         3.7         3.9         6.8           Fuel         7.99         6.41         321         294.2         R         1928         -         Trace         No good         4.0         3.7         3.7         3.3         6.8           Fuel         7.99         6.41         321         R         1928         -         Trace         No good         4.0         1.7         2.3         3.3         6.8           Fuel         7.99         6.41         321         R         1928         -         Trace         No good         4.0         1.7         2.3         3.3         6.8           P.H. Solar         11.98         6.25         705         R         1928         -         Trace         No good         4.0         2.6         3.2         2.6         16.5           P.H. Solar         11.98         6.45         538         R         1928         -         Trace         No good         4.0         2.6         3.2         2.6         16.5           Filter Oil         9.00         8.45	121	B.O.D.	5.49	4	79.5	· • •	1928	t	Trace	No good		i.	ī.	1.4	•	 		
Residue         8.40         5.24         290.3         R         1928         -         Trace         No good         4.0         1.7         2.3         3.3           Fuel         7.99         6.41         321         R         1928         -         Trace         No good         4.0         1.7         2.3         3.3           Fuel         9.49         7.73         548         R         1928         -         Trace         No good         4.0         1.7         2.3         3.3           Residue         23.91         11.95         5,367         R         1928         -         Trace         No good         4.0         2.3         3.1         3.1         3.1         3.2         2.6         16.5           P.H. Solar         9.00         8.45         538         R         1928         -         Trace         No good         4.0         2.6         3.1	122	Residue	8.40	ŝ	294.2	•	1928	1	Trace						φ	6.2	•	
Fuel       7.99       6.41       321       R       1928       -       Trace       No       good         Residue       23.91       11.95       5,367       R       1928       -       Trace       No       good         Residue       23.91       11.95       5,367       R       1928       -       Trace       No       good         P.H. Solar       9.00       8.45       538       R       1928       -       Trace       No       good         Filter Oil       9.00       8.45       538       R       1928       -       Trace       No       good         Filter Oil       9.00       8.45       538       R       1928       -       Trace       No       good         Fulter Oil       9.00       8.45       538       R       1928       -       Trace       No       good         Kawengan Crude       23.50       11.82       5,127       R       -       Trace       No       good       4.0       2.6       16.5         Kawengan Crude       23.50       11.82       5,144       R       -       Trace       No       good       4.0       2.6       16.5	123	Residue	8.40	n	290.2		1928	- <b>I</b>  -	Trace						· .	. *		
Fuel       7.99       6.41       321       R       1928       -       Trace       No       good         Fuel       9.49       7.73       548       R       1928       -       Trace       No       good         Residue       23.91       11.95       5,367       R       1928       -       Trace       No       good         F.H. Solar       9.00       8.45       538       R       1928       -       Trace       No       good         F.H. Solar       9.00       8.45       538       R       1928       -       Trace       No       good         Filter Oil       9.00       8.45       538       R       1928       -       Trace       No       good         Fulter Oil       9.00       8.45       538       R       1928       -       Trace       No       good         Kawengan Crude       23.50       11.82       5,127       R       -       Trace       No       good       4.0       2.6       3.1       3.1       3.1       3.2       2.6       16.5         Kawengan Crude       23.50       11.82       5,144       R       -       Trace       N	-		i				y 1,					•	:	•.				
Fuel       9.49       7.73       548       R       1928       -       Trace       None       No good         Residue       23.91       11.95       5,367       R       -       None       No good         P.H. Solar       11.98       6.25       705       R       1928       -       Trace       No good         F.H. Solar       9.00       8.45       538       R       1928       -       Trace       No good         Filter Oil       9.00       8.45       538       R       1928       -       Trace       No good         Filter Oil       9.00       8.45       538       R       1928       -       Trace       No good         Kawengan Crude       23.50       11.82       5,127       R       -       Trace       No good       4.0       2.6       3.2       2.6       16.5         Kawengan Crude       23.50       11.82       5,127       R       -       Trace       No good       4.0       2.6       3.2       2.6       16.5         Kawengan Crude       23.50       11.82       5,144       R       -       Trace       No good       4.0       3.8       3.3       3.0	138	Fuel	. 7.99	6.4	321	P24	1928	I	Trace				:		2	•		
Residue       23.91       11.95       5,367       R       -       None       No good         P.H. Solar       11.98       6.25       705       R       1928       -       Trace       No good         Filter 0il       9.00       8.45       538       R       1928       -       Trace       No good         Filter 0il       9.00       8.45       538       R       1928       -       Trace       No good         Kawengan Crude       23.50       11.82       5,127       R       1928       -       Trace       No good       4.0       2.6       3.2       2.6       16.5         Kawengan Crude       23.50       11.82       5,127       R       -       Trace       No good       4.0       2.6       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.5       3.1       3.1       3.5       3.1       3.1       3.5       3.6       5.5       4.5       4.5       5.6       4.5       5.6       4.5       5.6       4.5       5.6       4.5       5.6       4.5       5.6       4.5       5.6       4.5       5.6       4.5       5.6       2.6	139	Fuel	6 4 6	-	548	<b>M</b>	1928	i	Trace		÷ * .							
Rescue       23.91       11.93       6.25       705       R       1928       -       None       No good         Filter 0il       9.00       8.45       538       R       1928       -       Trace       No good         Filter 0il       9.00       8.45       538       R       1928       -       Trace       No good         Filter 0il       9.00       8.45       538       R       1928       -       Trace       No good         Kawengan Crude       23.50       11.82       5,127       R       -       Trace       No good       4.0       2.6       3.2       2.6       16.5         Kawengan Crude       23.50       11.82       5,144       R       -       Trace       No good       4.0       2.6       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.1       5.5       16.5         Residue       20.05       8.42       2.658       R       -       Trace       No good       4.0       2.6       3.2       3.6       2.4       5.4         Residue       20.05       8.42       2.658       R       -       Trace       No good       4.0 <td>0.71</td> <td></td> <td></td> <td></td> <td>ç</td> <td>ſ</td> <td></td> <td></td> <td></td> <td></td> <td>j . a</td> <td></td> <td></td> <td></td> <td>\</td> <td></td> <td></td> <td></td>	0.71				ç	ſ					j . a				\			
P.H. Solar       11.98       6.25       705       R       1928       -       Trace       No good         F.H. Solar       9.00       8.45       538       R       1928       -       Trace       No good         Filter Oil       9.00       8.45       538       R       1928       -       Trace       No good         Kawengan Crude       23.50       11.82       5,127       R       -       Trace       No good       4.0       2.6       3.2       2.6       16.5         Kawengan Crude       23.50       11.82       5,144       R       -       Trace       No good       4.0       2.6       3.2       16.5         Residue       20.05       8.42       2.658       R       -       Trace       No good       4.0       3.3       3.0       7.5         Residue       20.05       8.42       2.658       R       -       Trace       No good       4.0       3.3       3.0       7.5         Residue       20.05       8.42       2.658       R       -       Trace       No good       4.0       2.6       3.2       2.6       2.6         Ledok Crude       29.99       11.47	0 5 4	anorsav	14.07	<u>,</u>	<u>,</u> .	¥.		1	anon			•			•			
F.H. Solar       9.00       8.45       538       R       1928       -       Trace       No       good         Filter Oil       9.00       8.45       538       R       1928       -       Trace       No       good         Kawengan Crude       23.50       11.82       5,127       R       -       Trace       No       good       4.0       2.6       3.2       2.6       16.5         Kawengan Crude       23.50       11.82       5,144       R       -       Trace       No       good       4.0       2.6       3.2       2.6       16.5         Kawengan Crude       23.50       11.82       5,144       R       -       Trace       No       good       4.0       3.5       3.1       3.1       3.1       3.2       16.5         Residue       20.05       8.42       2.658       R       -       Trace       No       good       4.0       3.3       3.0       7.5         Residue       20.05       8.42       2.658       R       -       Trace       No       good       4.0       3.3       3.0       7.5         Ledok       Crude       29.99       11.47       8,102	201		11 98				1928	° 1	Trace					•	•	•	ł	:
Filter Oil       9.00       8.45       538       R       1928       -       Trace       No       good       4.0       2.6       3.2       2.6       16.5         Kawengan Orude       23.50       11.82       5,127       R       -       Trace       No       good       4.0       2.6       3.2       2.6       16.5         Kawengan Orude       23.50       11.82       5,144       R       -       Trace       No       good       4.0       2.6       3.1       3.1       3.1       3.1       3.1       3.1       3.1       3.5       16.5         Kawengan Crude       23.50       11.82       5,144       R       -       Trace       No       good       4.0       3.5       3.1       3.1       3.1       3.2       16.5         Residue       20.05       8.42       2.658       R       -       Trace       No       good       4.0       3.3       3.0       7.5         Ledok Crude       29.99       11.47       8,102       R       -       Trace       No       good       4.0       3.3       2.6       2.4       25.4         Ledok Crude       29.99       11.47       8,102 </td <td>202</td> <td></td> <td>00-6</td> <td></td> <td></td> <td>R</td> <td>1928</td> <td><b>I</b></td> <td>Trace</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td>	202		00-6			R	1928	<b>I</b>	Trace									
Filter Oil       9.00       8.45       538       R       1928       -       Trace       No       good       4.0       2.6       3.2       2.6       16.5         Kawengan Crude       23.50       11.82       5,127       R       -       Trace       No       good       4.0       2.6       3.2       2.6       16.5         Kawengan Crude       23.50       11.82       5,144       R       -       Trace       No       good       4.0       3.5       3.1       3.1       3.2       16.5         Residue       20.05       8.42       2.658       R       -       Trace       No       good       4.0       3.3       3.0       7.5         Ledok Crude       29.99       11.50       8,123       R       -       Trace       No       good       4.0       3.3       3.6       2.4       25.4         Ledok Crude       29.99       11.47       8,102       R       -       Trace       No       good       4.0       3.3       2.6       2.4       25.4																		
Kawengan Crude       23.50       11.82       5,127       R       -       Trace       No       good       4.0       2.6       3.2       2.6       16.5         Kawengan Crude       23.50       11.82       5,144       R       -       Trace       No       good       4.0       2.6       3.2       2.6       16.5         Rewengan Crude       23.50       11.82       5,144       R       -       Trace       No       good       4.0       3.5       3.1       3.1       3.2       16.5         Residue       20.05       8.42       2.658       R       -       Trace       No       good       4.0       3.3       3.0       7.5         Ledok Crude       29.99       11.50       8,102       R       -       Trace       No       good       4.0       2.9       3.2       2.6       4.4         Ledok Crude       29.99       11.47       8,102       R       -       Trace       No       good       4.0       3.3       2.6       2.4       25.4	216	Filter Oil	00.6	8.4	538	ж	1928	1	Trace									
Kawengan Crude       23.50       11.82       5,144       R       -       Trace       No       good       3.5       3.1       3.1       3.2       16.5         Residue       20.05       8.42       2.658       R       -       Trace       No       good       4.0       3.8       3.3       3.0       7.5         Ledok       Crude       29.99       11.50       8,123       R       -       Trace       No       good       4.0       3.3       3.2       25.4         Ledok       Crude       29.99       11.47       8,102       R       -       Trace       No       good       4.0       3.3       2.6       2.4       25.4         Ledok       Crude       29.99       11.47       8,102       R       -       Trace       No       good       4.0       3.3       2.6       2.4       25.4	931	Kawengan Crude			5,1	p:		. 1	Trace		• .	0 7			16.	15.5	15.9	15.9
Kawengan Grude       23.50       11.82       5,144       R       -       Trace       No       good       3.5       3.1       3.1       3.2       16.5         Residue       20.05       8.42       2,658       R       -       Trace       No       good       4.0       3.8       3.3       3.0       7.5         Ledok Crude       29.99       11.50       8,123       R       -       Trace       No       good       4.0       2.9       3.2       2.5.4         Ledok Crude       29.99       11.47       8,102       R       -       Trace       No       good       4.0       3.3       2.6       2.4       25.4         Ledok Crude       29.99       11.47       8,102       R       -       Trace       No       good       4.0       3.3       2.6       2.4       25.4																		
Residue       20.05       8.42       2.658       R       -       Trace       No       good       4.0       3.8       3.3       3.0       7.5         Ledok       Crude       29.99       11.50       8,123       R       -       Trace       No       good       4.0       3.3       3.0       7.5         Ledok       Crude       29.99       11.47       8,102       R       -       Trace       No       good       4.0       3.3       2.6       2.4       25.4         Ledok       Crude       29.99       11.47       8,102       R       -       Trace       No       good       4.0       3.3       2.6       2.4       25.4	933	Kawengan Crude			5,144	p4		I.	Trace			3.5				15.5	13.8	15.5
Ledok Crude 29.99 11.50 8,123 R - Trace No good 4.0 2.9 3.2 3.2 25.4 Ledok Crude 29.99 11.47 8,102 R - Trace No good 4.0 3.3 2.6 2.4 25.4	369	Residue	20.05	8.42		, M		ł	Trace			0.4	00	ŝ		5.9	5.2	6.1
Ledok Crude 29.99 11.47 8,102 R - Trace No good 4.0 3.3 2.6 2.4 25.4	176	Ledok Crude	79.90			24	۰.	. 1	dret T	No ocod	•	c ;;	Ō			72.7	0 20	22 8
	942	Ledok Crude	29.99			223		ţ	Trace	No good		0.4	i ui	1.64		23.9	23.5	23.8

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	•	Annex II-5-7	EQUIPMENT LIST	[REPAIR WORKSHOP EQUIPMENTS	(I) I (I) I
Item	Object	Kind of Object	Short Spec.	Purpose of Use C	Condition Year Remark
No.	No.		- 1		
, ,	3057	Lathe Machine	ight(H) =	General purpose n	movable 1938 Bad condition
:			Length(L) = 1.300 mm. Chuckdia(D) = 45 mm		
~	3060	Lathe Machine	H = 250  mm, L = 750  mm, D = 45  mm	General purpose u	unmovable 1938 Out of use
m	3063	High Speed Lathe Machine	$H = 180 \text{ mm}_{\text{F}} \text{ L} = 1.500 \text{ mm},$ D = 45  mm	Precion high speed m lathe, Small size	movable 1938 Bad condition
4	3065	Lathe Machine	H = 220  mm, L = 1,500  mm, D = 70  mm	Surfacing and screw m cuttig	movable 1938 Bad condition
'n	3068	Lathe Machine	H = 300  mm, L = 2,000  mm, D = 50  mm	Surfacing and screw v cuttig	unmovable 1938 Out of use
e	8	Lathe Machine	H = 175 mm, L = 1,400 mm, D = 35 mm	General purpose	movable Bad condition
<b>7</b>	3088	High Speed Lathe Machine	H = 175  mm, L = 1,400  mm, D = 35  mm	General purpose	movable 1938 Bad condition
80		Lathe Machine	H = 160  mm, L = 2,600  mm, D = 70  mm	General purpose	good 1971 Good condition
ወ	3078	Hgih Speed Lathe Machine	H = 190 mm, L = 1,500 mm, D = 50 mm	Shaft threading n	movable 1937 Bad condition
01	3075	Lathe Machine	H = 180  mm, L = 1,300  mm, D = 70  mm	Shaft threading .	unmovable 1929 Out of use
н г	3071	High Speed Lathe Machine	H = 280  mm, L = 1,800  mm, D = 45  mm	General purpose u	unmovable 1929 Out of use
12	3104	Lathe Machine	H = 300  mm, L = 1,500  mm, D = 52  mm	General purpose n	movable 1928 Bad condition, unusable
м Н	3113	High Speed Lathe Machine	H = 325 mm, L = 2,000 mm, D = 66 mm	General purpose	unmovable 1930 Out of use
14 1	3109	High Speed Lathe Machine	H = 400 mm, L = 4,000 mm, D = 65 mm	General purpose, n Big size	movable 1928 Bad condition
с Г	3136	Vertical Lathe Machine	H = Dia.Max = 70 cm Speed Max = 730 rpm	Lining cylinders r	movable 1929 Bad condition,

n Year Remark	1929 Bad condition. unusable	1929 Bad condition	Bad condition	1920 Bad condition	1929 Bad condition unusable	e Out of use	1929 Baď condition	1926 Bad condition	1971 Good condition	e 1920 Out of use	1.920 Almost not us Bad condition	1920 Almost not us Bad condition	1920 Almost not used. Bad condition	Almost not us Bad condition	e 1920 Out of use
Condition	movable	aldavom	movable	movable	movable	unmovab1e	movable	movable	goođ	unnovable	movable	movable	movable	movable	unmovable
Purpose of Use	Reaming cylinders and bore surfaces	Gears Pins etc.	Plane and universal	Facing surface	Drilling holes	Facing surfaces	Facing surfaces	Plain and universal	Plain and universal	Remove or install piston & bearings	Drilling holes	Drilling holes, small size	Remove or install piston & bearing	Testing valves & cocks	Precise surfacing
Short Spec.	Max.H = 630 mm, Max.Speed = 730 rpm	Stroke = 300 mm	Table: 12" x 42"	H = 30", W(Width) = 30" L = 8 ft	Bore Max. = 4", Column = 11"	Stroke = 16"	Stroke = 32"	Table: 335 x 115 mm	Table: 300 x 1,200 mm	Stoke = 3.2 m	Bore.Max = 25 mm, Stroke = 90 cm	Bore = 2 - 10 mm Stroke 25 cm	Stroke = 1.3 m	Capacity Max. = 25 kg/cm <sup>2</sup>	Table: 0.5 x 1.0 m Dia = 0.3 m
Kind of Object	Horizontal Boring Machine	Slotting Machine	Horizontal Milling Machine	Planing Machine	Radial Drilling Machine	Shaping Machine	Shaping Machine	Vertical Milling Machine	Vertical Milling Machine	Horizontal Jack	Drilling Machine	Drilling Machine	Vertical Jack	Jack Pump	Clean Table
Object No.	3136	3140	3098	3132	3124		3121	3118		3150	3155	3157	3149		3151

Use Condition Year	good	good 1983	good 1983	1- - 		1	ł	:	<b>1</b> -	1	2	1
e S			υ <sup>ν</sup> .	good	good	good	goođ	10 00 00	good	i doog	good 1974	good 1974
rurpose or	General purpose	General purpose	Plane and universal	Sawing materials	Sawing materials	Sawing materials	Reaming cylinders & bore surfaces	Reaming cylinders & bore surfaces	Reaming cylinders & bore surfaces	Welding metals	Welding metals	Welding metals
Short Spec.	D = 50 cm, L = 300 cm, Max.Speed = 1,180 rpm	D = 20  cm, L = 100  cm, Max.Speed = 2,000  rpm	Max.Speed = 2,000 rpm	Capacity = 8"	Capacity = 1.5 KW Max.Speed = 1,420 rpm		Strokcey = 125 mm, Max.Speed = 2,400 rpm	Max.Speed = 2,500 rpm	Max.Speed = 1,960 rpm	Capacity = 19 KW, 40V (load)	Capacity = 40 - 80 V, 100 - 300 A	Capacity = 105 KW, 32, 6 V, 250 A
KING OI UDJECT	Lathe Machine	Lathe Machine	Milling Machine	Hacksaw Machine	Hacksaw Machine	Hacksaw Machine	Boring Machine, Type 430	Boring Machine, Type KID-420	Boring Machine, Type LC-14	AC-Arc Welding Machine	AC-Arc Welding Machine	AC-Arc Welding Machine
No. No.	 TE	32	33	34	35	36	37	38	68	40	41	42
KING OT UDJECT Short Spec.	No.	No. Lathe Machine $D = 50 \text{ cm}$ , $L = 300 \text{ cm}$ , Max.Speed = 1,180 rpm	No. Lathe Machine $D = 50 \text{ cm}$ , $L = 300 \text{ cm}$ , Max.Speed = 1,180 rpm Lathe Machine $D = 20 \text{ cm}$ , $L = 100 \text{ cm}$ , Max.Speed = 2,000 rpm	No. Lathe Machine $D = 50 \text{ cm}$ , $L = 300 \text{ cm}$ , $L = 1,180 \text{ rpm}$ ——— Lathe Machine $D = 20 \text{ cm}$ , $L = 100 \text{ cm}$ , $Max.Speed = 2,000 \text{ rpm}$ ——— Milling Machine Max.Speed = 2,000 rpm	No.Lathe MachineD = 50 cm, L = 300 cm,Lathe MachineMax.Speed = 1,180 rpmLathe MachineD = 20 cm, L = 100 cm,Max.Speed = 2,000 rpmHacksaw MachineMax.Speed = 2,000 rpmHacksaw MachineCapacity = 8"	No. No. No. Lathe Machine $D = 50 \text{ cm}$ , $L = 300 \text{ cm}$ , 31  Lathe Machine $D = 50  cm$ , $L = 100  cm$ , 32  Lathe Machine $D = 20  cm$ , $L = 100  cm$ , 33  Milling Machine $Max.Speed = 2,000  rpm34 $ Hacksaw Machine Capacity = 8" 35  Hacksaw Machine Capacity = 1.5 KW Max.Speed = 1.420  rpm	No. Lathe Machine D = 50 cm, L = 300 cm, Lathe Machine D = 20 cm, L = 100 cm, Max.Speed = 2,000 rpm Max.Speed = 2,000 rpm Hacksaw Machine Capacity = 8" Hacksaw Machine Capacity = 1.5 KW Max.Speed = 1.5 rW Max.Speed = 1.5 rW	No. No.       No. No.       Lathe Machine       D = 50 cm, L = 300 cm, General         31       Lathe Machine       Max.Speed = 1,180 rpm       General         32       Lathe Machine       D = 20 cm, L = 100 cm, General       General         33       Lathe Machine       D = 20 cm, L = 100 cm, General       General         33       Hacksaw Machine       Max.Speed = 2,000 rpm       Plane an         34       Hacksaw Machine       Capacity = 8"       Sawing m         35       Hacksaw Machine       Capacity = 1.5 KW       Sawing m         35       Hacksaw Machine       Capacity = 1.5 KW       Sawing m         36       Backsaw Machine       Capacity = 1.5 KW       Sawing m         37       Boring Machine, Strokcey = 1.5 mm, sawing m       Sawing m	No. No.       No. No.       No. No.       Lathe Machine       D = 50 cm, L = 300 cm, General         31       Lathe Machine       D = 20 cm, L = 100 cm, General       General         32       Imathe Machine       D = 20 cm, L = 100 cm, General       General         33       Imathe Machine       D = 20 cm, L = 100 cm, General       General         33       Imathe Machine       Max.Speed = 2,000 rpm       Plane an         34       Imathe Machine       Capacity = 8"       Sawing m         35       Imathe Machine       Capacity = 1.5 KW       Sawing m         35       Imathe Machine       Capacity = 1.5 KW       Sawing m         35       Imathe Machine       Capacity = 1.5 KW       Sawing m         36       Imathe Machine       Capacity = 1.5 KW       Sawing m         37       Imathe Machine       Capacity = 1.5 KW       Sawing m         36       Imathe Machine       Capacity = 1.5 KW       Sawing m         37       Imathe Machine       Imathe Machine       Imathe Machine       Imathe Machine         38       Imathe Machine       Max.Speed = 2,400 rpm       Reaming         38       Imathe Machine       Imathe Machine       Imathe Machine       Imathe Machine         38	No.No.No.31Lathe MachineD = 50 cm, L = 300 cm,32Lathe MachineMax.Speed = 1,180 rpm33MathineD = 20 cm, L = 100 cm,33MathineD = 20 cm, L = 100 cm,34Hacksaw MachineMax.Speed = 2,000 rpm35Hacksaw MachineCapacity = 8"36Hacksaw MachineCapacity = 1.5 KW37Boring Machine,Strokcey = 1.5 Am,38Boring Machine,Max.Speed = 2,400 rpm38Boring Machine,Max.Speed = 2,500 rpm39Boring Machine,Max.Speed = 2,500 rpm39Boring Machine,Max.Speed = 1,960 rpm	No.No.No.31Lathe MachineD = 50 cm, L = 300 cm,32Lathe MachineMax.Speed = 1,180 rpm33Max.Speed = 2,000 rpm34Hacksaw MachineCapacity = 8"35Hacksaw MachineCapacity = 1.5 KW36Hacksaw MachineCapacity = 1.5 KW37Backsaw MachineStrokcey = 1.5 KW38Backsaw MachineMax.Speed = 2,400 rpm38Boring Machine,Strokcey = 125 mm,39Boring Machine,Max.Speed = 2,500 rpm39Boring Machine,Max.Speed = 2,500 rpm40AC-Arc WeldingMax.Speed = 1,960 rpm	No.No.No.31Lathe MachineD = 50 cm, L = 300 cm,32Lathe MachineD = 20 cm, L = 100 cm,33Milling MachineD = 20 cm, L = 100 cm,34Max.Speed = 2,000 rpm35Hacksaw MachineCapacity = 8"35Hacksaw MachineCapacity = 1.5 KW36Hacksaw MachineCapacity = 1.420 rpm37Hacksaw MachineStrokcey = 1.5 KW38Boring Machine,Max.Speed = 2,400 rpm39Boring Machine,Max.Speed = 2,500 rpm39Boring Machine,Max.Speed = 2,500 rpm40Strokcey = 1.960 rpm41AC-Arc WeldingCapacity = 19 KW,41AC-Arc WeldingCapacity = 19 KW,

Bad condition, usable Almost out of use Almost out of use Almost out of use Remark Out of use of use out of use [CONSTRUCTION WORKSHP EQUIPMENTS] Out Year 1929 1.938 1925 1926 1933 1929 1925 1925 1 1 ľ 1 ł ł 1 1 unmovable unmovable Condition broken movable movable movable movable movable usable broken usable broken proken **broken** broken broken broken broken broken Forging materials Forging materials Grinding surfaces Grinding surfaces Sawing materials Sawing materials Úse Shearing plates Punching plates Bending plates Welding metals Welding metals Drilling holes Handling heavy materials Welding metals Welding metals Welding metals Welding metals Drilling holes Redheat steel ч £١ Purpose თ н ы 18V, 220/250A, 3 phase 18V, 220/250A, 3 phase £-; Capacity: 10" z Short Spec. E2) Ē 2,000 kg Σ 250 1111 p, 1 ы þ α ы Radial Drilling M. Radial Drilling M. Shield Arc Welder Funching Machine of Object Shearing Machine Hacksaw Machine Arm Chain Hoist Hacksaw Machine Annex II-5-7 Bending Roller Steam Hammer Steam Hammer Arc Welder Arc Welder Arc Welder Furnance Grinder Grinder Kind Welder Welder Object No. 3226 3250 3236 3233 3232 3225 3212-3216 3227, 3230 3270 3273 3243 3241 Item Ъ Ч 50 Ч Ч ŝ 14 ŝ г-г-і 18 0 H од Z

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• • • Annex II-5-7 EQUIPMENT LIST [PIPE SHOP EQUIPMENTS]

	Remark	Bad condition, Almost not-used	Bad condition, Almost, not-used	Bad condition, Almost not-used				
•	Year	1929	1929	1938	1929	626T	1929	
	Condition	movable	movable	movable	movable	movable	movable	movable
	Purpose of Use	Pipe threading	Pipe threading	Pipe threading	Pipe threading	Pipe threading	Pipe threading	Pipe threading
	Short Spec.	D = 24"	D = 10"	For pipes 4" - 4"	For pipes 2 <sup>1</sup> " - 12"	For pipes 1" - 6"	For pipes d" - 6"	Capacity = 100 Ton
· · ·	Kind of Object	Pipe threader (Lathe Machine)	Pipe threader (Lathe Machine)	Pipe threader (Dies Machine)	Pipe threader (Dies Machine)	Pipe threader (Dies Machine)	Pipe threader (Dies Machine)	Pipe Press
•	Object No.	3304	3309	3312	3315	3318	332I	
	Item No.	Ħ	3	m	4	<b>ب</b> م.	Q	2